

A STUDY OF HEAT TRANSFER AND FLUID FLOW
IN THE ELECTROSLAG REFINING PROCESS

by

MANOJ KUMAR CHOUDHARY

B. Tech. Hons. (Chemical Engineering)
Indian Institute of Technology, Kharagpur
(1974)

M.S. (Chemical Engineering)
State University of New York at Buffalo
(1976)

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Signature of Author _____

Department of Materials Science
and Engineering, May 2, 1980

Certified by _____

Juliah Szekely
Thesis Supervisor

Accepted by _____

Regis M. Pelloux
Chairman, Departmental Committee
on Graduate Students

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Submitted to the Department of Materials Science
and Engineering on May 2, 1980
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ABSTRACT

A mathematical model has been formulated to describe the electromagnetic field, fluid flow, heat transfer and solidification phenomena in electroslag refining systems.

The formulation is based on the simultaneous statement of Maxwell's equations written for the MHD approximation, the equations for turbulent fluid flow in the slag as caused by both electromagnetic and natural convection forces (due to temperature gradients) and the differential thermal energy balance equations with allowances made for the spatial distribution of heat generation rate in the slag, for the moving interfaces, for the transport of heat by metal droplets falling through the slag and for the release of latent heat in the mushy zone. The effective viscosity and the effective thermal conductivity in the slag are calculated by using a two equation model for turbulence. The equations are first stated in vector notations and then simplified for an axi-symmetric cylindrical coordinate system. An outline of the computational approach is also included.

The theoretically predicted pool profiles and temperature fields are found to be in reasonable agreement with experimental measurements reported in literature for a laboratory scale system. The predictive capability of the model makes it possible to relate the heat generation pattern, the temperature and the velocity fields, the casting rate and the pool profiles to the operating power and current, to the amount of slag used and to the geometry of the system.

Thesis Supervisor: Dr. Julian Szekely

Title: Professor of Materials Engineering

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CHAPTER I
INTRODUCTION

In recent years there has been a growing interest in the development of mathematical models for the representation of heat transfer and fluid flow phenomena in the electroslag refining process. While the earlier models concentrated on the calculations of pool profiles and temperature fields in the ingot, a more fundamental approach was taken in recently reported models where allowance has been made for the thermally and electromagnetically driven flow in the system. However, these latter models were primarily of theoretical interest because the shape and size of the molten metal pool had to be specified and because heat transfer in the mushy zone and in the ingot was neglected.

The work to be described in this thesis represents an attempt towards developing a predictive model for flow and thermal characteristics of the ESR process. The model developed in this work seeks mathematical representations for the electromagnetic field, for the turbulent recirculating flow in the slag (due to both electromagnetic and natural convection forces) and for heat transfer with phase change. It therefore involves the simultaneous statement of Maxwell's equations, equations for turbulent motion and the differential thermal energy balance equations. The model is then used to make predictions for a laboratory

scale system reported in literature. The predictive capability of the model is utilized to investigate the interdependence of principal operating parameters.

Regarding the organization of this thesis, it is divided into six chapters in the following manner:

In Chapter 2, a literature survey is presented, which reviews mathematical models on ESR and on turbulent recirculating flow in metallurgical systems.

The formulation of the mathematical model is given in Chapter 3. After discussing the basic processes involved and the assumptions made, the governing differential equations are first written in vectorial forms so that some general conclusions can be drawn regarding the behavior of ESR systems. Then they are presented in the cylindrical coordinate system with axial symmetry. Boundary conditions are discussed and some dimensionless parameters are derived.

Numerical procedure used to solve the governing differential equations is outlined in Chapter 4.

Computed results on current distribution, heat generation pattern, velocity and temperature fields and pool profiles are discussed in Chapter 5. Wherever possible, these results are compared with experimental measurements available in literature.

Concluding remarks and some suggestions for further work in modelling of ESR process are made in Chapter 6.

Appendix A contains a brief note on phasor notation used for AC operation. Derivations of vorticity boundary conditions are discussed in Appendix B. Calculation of radiation view factors is outlined in Appendix C. The use of a temperature dependent electrical conductivity for slag is discussed in Appendix D and a listing of the computer program is presented in Appendix E.

CHAPTER II

LITERATURE SURVEY

The past decade has seen a rapid increase in the application of electroslag process in this country and in other industrialized nations. During the same period numerous papers dealing with both physical and mathematical modelling of ESR have been published. These models have resulted from a need to have a better understanding of the relationships among key process parameters so as to be able to devise effective strategies for controlling structure and composition of remelted ingots.

Mathematical models for the ESR process can be classified into two groups -- (1) those dealing with physical phenomena such as heat transfer, fluid flow and solidification (i.e. thermal and fluid flow models) ¹⁻²² and (2) those dealing with chemical and electrochemical reactions (i.e. chemical models) ²³⁻²⁶. The review presented here is restricted to thermal and fluid flow models for this is the category into which the present work falls.

From the point of view of mathematical modelling, the electroslag refining process represents a complex group of problems involving turbulent recirculating flow driven by electromagnetic and buoyancy forces, heat and mass transfer phenomena and phase change (both melting and solidification) with free boundaries. Because of the way ESR model described in this thesis has evolved, it appears

best to divide this chapter into two sections. The first section reviews mathematical models for ESR and the second section presents an overview of literature on the mathematical modelling of turbulent recirculating flows in metallurgical systems.

2.1 Mathematical Models for ESR

Some of the earliest modelling work on ESR dealt with temperature distributions in the electrode. These involved the solution of one dimensional^{2,3} or two dimensional^{1,7} heat conduction problems with experimentally established boundary conditions. While these models were helpful in visualizing the relative magnitudes of various heat transfer mechanisms (i.e. conduction, convection and radiation) so far as the electrode was concerned, they could not provide insight into the local or the overall heat transfer rate between the electrode and the slag. The heat transfer coefficient between the electrode and the slag was, instead, used as an adjustable parameter to interpret measured temperature distributions in the electrode.

Most of the early models on ESR^{4-12,18} have concentrated on the representation of thermal field in the ingot. While these models may differ in the form (e.g. transient vs. quasi steady state) or in the type of boundary conditions chosen (e.g. specified flux vs. specified temperature at the slag-metal interface) or in the way the release of

latent heat is accounted for (e.g. adjustment of specific heat in the mushy zone vs. use of solidification models), the unifying themes behind these models are:

1) transport processes taking place in the slag are ignored with the boundary condition at the slag-metal interface being considered adjustable.

2) casting rate is used as an input to the model.

and 3) an effective thermal conductivity is used to account for convection in the metal pool.

These models then reduce to a set of heat conduction equations (with movement of slag-metal interface being accounted for) for the metal pool, for the mushy zone and for the solid ingot with appropriate boundary conditions. Some of these earlier models have been reviewed by Mitchell et al.⁹ and by Ballantyne and Mitchell¹². The models presented by Sun and Pridgeon⁴, Carvajal and Geiger⁸, Paton et al.^{5,10}, Ballantyne and Mitchell¹² and Jeanfils et al.¹⁸ are transient in nature. While all these authors used the transient models to study the development of isotherms from the initial stages of remelting up to the attainment of quasi-steady state, Jeanfils et al.¹⁸ also utilized their model to investigate the response of the system (as characterized by change in pool depth and mushy zone thickness) to specified changes (e.g. ramp, sinusoidal) in the melt rate.

Elliott and Maulvault¹¹ noted that the thermal conditions in an ESR system became reproducible in time after the ingot had grown to sufficient length (e.g. about 2.5 times the radius of the ingot when casting steels and other metals with similar conductivities) and developed a quasi steady state model for calculating thermal field in the ingot. This reduced the dimensionality of the problem without seriously affecting the scope of the model. Furthermore, the numerical scheme chosen by Elliott and Maulvault¹¹ allowed for arbitrary grid configurations. This in turn enabled them to concentrate the nodes in critical areas without excessive grid requirements.

Apart from being successful in the interpretation of experimental measurements on pool depth and on local solidification time in the mushy zone, these models^{4-12,18} illustrated the influence of casting rate and the effective thermal conductivity on thermal fields in the ingot. Furthermore many of these papers provided measurements which were needed for model validation.

The inability of these models to generate predictive relationships among key process parameters such as power input, geometry, slag depth on one hand and melting rate, pool depth, width of the mushy zone etc. on the other hand stems from ignoring transport processes in the slag. The calculation of thermal fields in the slag necessitates the

solution of electromagnetic field equations in order to obtain the local rate of heat generation in the slag. Furthermore there is vigorous convection in slag. The driving force for flow is provided by both electromagnetic and buoyancy forces and the flow, in general, is turbulent. The use of a spatially independent effective conductivity will not provide a realistic representation of convection in the slag. Thus a predictive model for the ESR process will have to seek additional mathematical representations for the electromagnetic force field, turbulent fluid flow field and for convective heat transfer in the slag.

This more fundamental approach has been taken in models published by Dilawari and Szekely^{13,14,15}, Kreyenberg and Schwerdtfeger¹⁶ and Inoue and Iwasaki²¹. A review of these recent models as well as a survey on measurements of temperature and electric potential reported in the literature have been made by Kawakami and Goto¹⁷.

The basic approach taken by the three groups of investigators is to first calculate the current paths for an assumed electrode melting tip shape (flat in references 13-16 and conical in reference 21) and then to solve fluid flow and convective heat transfer equations. Among these, Kreyenberg and Schwerdtfeger¹⁶ considered fluid flow and heat transfer in the slag phase only while the other two groups examined the behavior of both metal and slag phases.

The approach of Kreyenberg and Schwerdtfeger ¹⁶ necessitated an assumed temperature distribution at the slag-metal interface. This assumed boundary condition was found to have a strong effect on calculated flow and temperature fields in the slag. The formulation presented by Dilawari and Szekely ¹⁵ was particularly comprehensive since it allowed for the turbulent nature of flow (in both liquid pools) and accounted for heat transfer between the slag and the falling metal droplets. Although the models put forward by Dilawari and Szekely ¹⁵ and Inoue and Iwasaki ²¹ were of fundamental interest, their practical use was limited because the shape and the size of the molten metal pool had to be specified and heat transfer in the mushy zone and in the solid ingot was neglected. These models, therefore, could not be addressed to the metallurgically important question of how to relate the shape and the size of the metal pool and the mushy zone to the operating parameters. Furthermore, the arbitrarily assumed pool shape precluded a meaningful comparison of experimentally measured temperature profiles below the slag-metal interface with predictions based on the model.

The work described in this thesis represents a significant step in our continuing efforts to develop a predictive model for ESR operations. The nature of the model, its scope and limitations are detailed in subsequent chapters.

Some applications of the model described in this thesis have already been published ^{19,20,22}.

Before closing this section it should be pointed out that some studies have been made ^{27,28} to calculate segregation in ESR by solving interdendritic flow and temperature fields in simulated ESR ingots. The latter paper, in fact, investigated the suppression of macro-segregation by rotating the ingot. In both these papers, no account was taken of motion in the metal pool above the liquidus isotherm and electromagnetic effects were either avoided or ignored. Recently, however, Mehrabian and Ridder ²⁹ have extended their model to account for motion in the metal pool (laminar motion caused by natural convection) and have elaborated on the important influence of fluid motion in the metal pool on solute redistribution in ingots. It will be a worthwhile exercise to combine some aspects of the model to be described in this thesis with models for calculating segregation so as to minimize uncertainties in specifying various boundary conditions in the latter models.

2.2 Turbulent Recirculating Flows in Metallurgical Systems

Some of the recent models of ESR (13-16, 19-22) have involved the solution of turbulent recirculating flow. These models have benefited greatly from experiences gained with modelling of such flows in connection with various

metallurgical processes such as continuous casting (Szekely and Yadoya³⁰), argon stirring (Szekely et al.³⁴), deoxidation in the ASEA-SKF furnace (Szekely and Nakanishi³¹), induction stirring and melting (Szekely and Chang³², Tarapore and Evans³³) etc. It is to be noted that the computation of flow profiles in the latter two cases involved the simultaneous solution of Maxwell's and the Navier-Stokes equations. A growing interest in ladle metallurgy³⁷ operations to achieve bath homogenization (with respect to temperature and composition), deoxidation, degassing, inclusion removal, desulfurization etc. is likely to enhance the application of transport fundamentals in these systems. A detailed review of mathematical and experimental tools available for the study of transport phenomena in agitated ladle systems has been presented by Szekely³⁸.

The basic approach in the papers mentioned above has been to model the eddy transport terms through the use of an eddy viscosity (i.e. Boussinesq's proposal) which in turn is computed by solving additional equations. Unlike boundary layer flows or simple one dimensional flows where the spatial dependence of eddy viscosity can be given by an algebraic expression (e.g. mixing length hypothesis) or by a one equation model (which uses a differential equation for k , the turbulence kinetic energy and some suitable algebraic expression for l , the length scale of

turbulence), turbulent recirculating flows, in general, require a two equation model (which uses two differential equations - one for k and another for some appropriate parameter of turbulence). Launder and Spalding³⁶ have reviewed various mathematical models of turbulence. Except Szekely and Yadoya³⁰ who used a one equation model, the rest of the papers listed above used a two equation model (Spalding's k - W model, where W is a statistical characteristic of turbulence). The computational algorithm employed in these papers used the Stream function-vorticity technique as detailed by Gosman et al.³⁹ Experimental proof for the predictions reported in these papers was in terms of tracer dispersion rates or in terms of surface velocities (for both laboratory and industrial systems) and thus was not very direct. Szekely et al.³⁴ measured velocity and turbulence kinetic energy in the water model of an argon stirred ladle. This study however was not conclusive because of the uncertainties regarding boundary conditions at the gas-liquid interface and because of inherent experimental inaccuracies involved in determining low velocities using a hot film anemometer.

In a recent study Szekely et al.³⁵ have reported accurate measurements (using a laser doppler anemometer) of time averaged and fluctuating velocities in a system in which recirculating motion was created by a moving belt.

They also refined the mathematical model by incorporating wall functions to represent momentum transfer in the vicinity of solid surfaces. This refinement is all the more necessary because the transport processes taking place in the vicinity of bounding surfaces are usually of more practical interest. A good agreement between measurements and predictions is found in this paper.³⁵

In conclusion, it may be stated that while a great deal more work needs to be done to characterize gas agitated systems, the mathematical treatment of turbulent recirculating flows in single phases and for axial symmetry is relatively well developed and is supported by measurements made in both laboratory and plant scale systems.

CHAPTER III

FORMULATION OF MATHEMATICAL MODEL

In this chapter, a mathematical model is developed to describe flow and heat transfer phenomena in ESR systems. A brief description of the electroslag refining process is first presented so as to provide a clear perspective on the processes and components involved in the system.

3.1 Process Description

A detailed technical description of the ESR process is available in literature ^{40, 41}. Figure 3.1 shows a sketch of a typical ESR system. As seen here a solid consumable electrode of the primary metal which may be cast or wrought or be composed of scrap is made one pole of a high current source (AC or DC) and a water cooled base plate is the other pole. A slag bath contained in the water cooled mold acts as ohmic resistance and the Joule heating produced in it melts the electrode tip. The metal droplets fall through the slag and collect in a pool on the base plate to solidify. The electrode is fed into the slag bath and the liquid metal solidifies progressively forming an ingot which now acts as the secondary electrode. An important feature of the process is that a slag skin is formed at the inner surface of the mold, which provides an electrical insulation separating the mold from the molten slag, the metal pool and the solid-

ifying ingot. The most usual slag compositions fall within the system $\text{CaF}_2 + \text{CaO} + \text{Al}_2\text{O}_3$ and fulfill the basic requirements imposed by electrical and thermal conductivity, high temperature stability and phase behavior.

Refining takes place because of reactions between the metal and the slag in three stages:

- i) during formation of a droplet on the electrode tip
- ii) as the droplet falls through the slag, and
- iii) at the slag-molten metal pool interface.

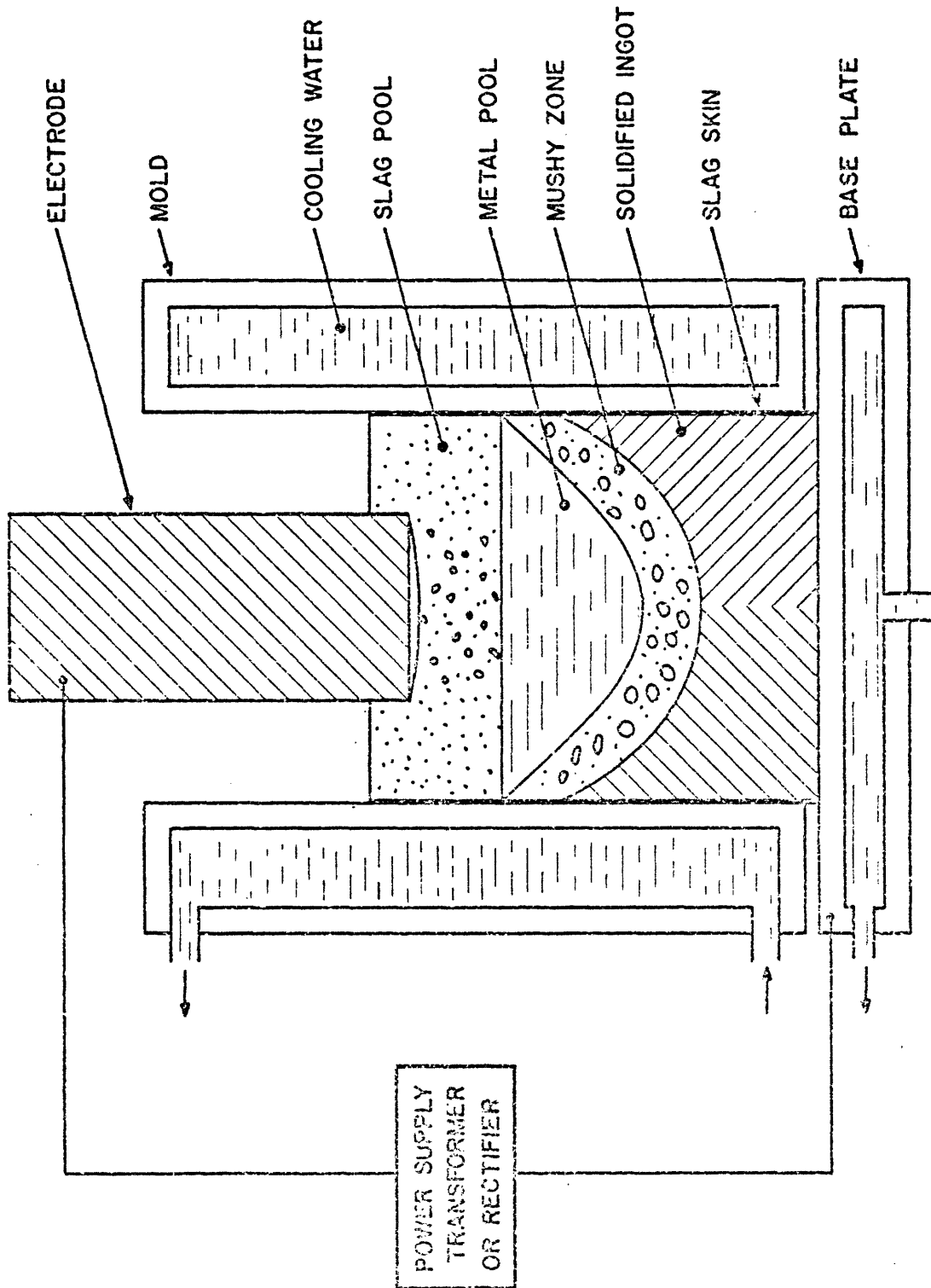
By suitable choice of slags, chemical and electrochemical reactions can either be encouraged or inhibited.

3.2 Summary of Basic Processes

The basic processes taking place during electroslag refining can be summarized as follows:

- 1) Passage of electric current through conducting media. This gives rise to spatially distributed joule heating in the slag. The interaction between current and the induced magnetic field results in Lorentz forces which cause circulation in slag and in metal pools.

- 2) Heat transfer, melting and solidification. Convective heat transfer takes place in the slag and in the metal pool. Metal droplets extract heat from the slag and get superheated. This superheat is released in the molten metal pool. Heat transport in other portions of



3.1 Schematic sketch of the electroslag refining process.

an ESR unit is characterized by conduction with account being taken of the movement of various interfaces. The electrode tip melts and solidification takes place in the mushy zone. Heat is removed through the mold by cooling water and there is radiative exchange of thermal energy between the free surface of the slag, the outer surface of the electrode and the inner surface of the mold.

3) Recirculation. There is recirculating motion in the slag and in the metal pool due to the combined effect of electromagnetic (Lorentz) and buoyancy (due to thermal gradients) driving forces. The fluid motion is, in general, turbulent.

4) Chemical and electrochemical reactions. This aspect of the ESR operation is not considered in the present work. The implications of ignoring chemical and electrochemical effects while modelling the thermal character of ESR are detailed in the next section.

3.3 Assumptions Made in Model

The physical concept of the process model is sketched in Fig. 3.2 which shows the coordinate system and the assumptions made regarding the geometry of the system.

The assumptions are as follows:

1) Cylindrical symmetry.

2) Slag-electrode and slag-metal boundaries are represented by horizontal surfaces. The assumption of a planar electrode melting tip is thought to be reasonable for large scale systems ⁴². However, we have retained this assumption even for the small scale system considered in this work.

Other key assumptions made in the model are as follows:

3) Quasi-steady state.

4) The slag-metal interface is modelled as a rigid wall. This is thought to be reasonable in view of the modelling work reported by Campbell ⁴².

5) Fluid flow equations are solved for the slag phase only. Motion in the metal pool is accounted for by using an effective thermal conductivity. However, an attempt is made to deduce this parameter from the calculated flow field in the slag phase.

6) In most of the calculations electrical conductivity of the slag is assumed uniform. However, in some calculations the temperature dependence of electrical conductivity of slag is approximately accounted for.

7) The effect of metal droplets on the motion of the slag is neglected.

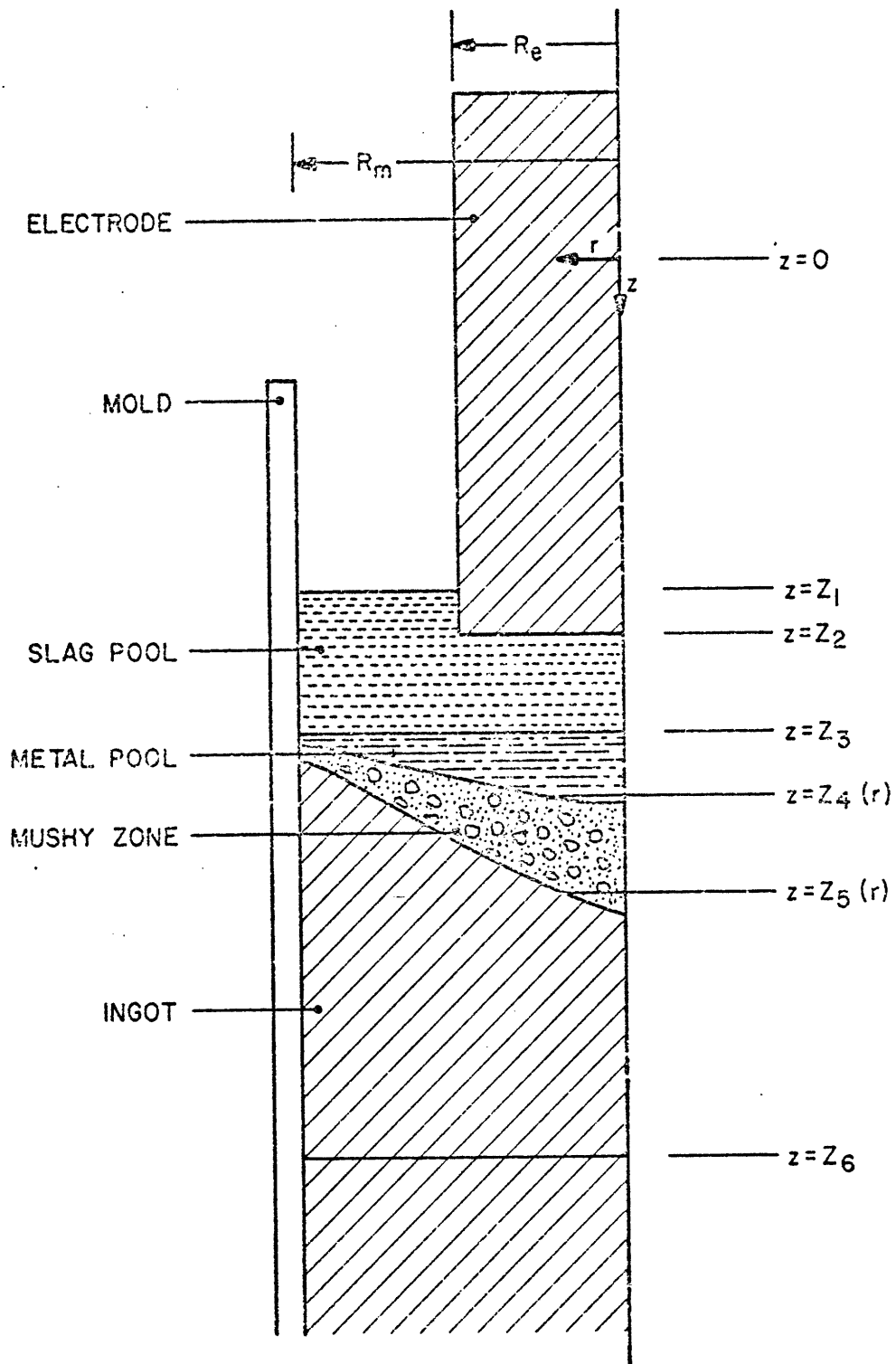
8) Effects associated with chemical and electrochemical reactions are not considered. There are two

aspects to these effects. The first is the influence of these processes on the nature of heat release in the slag and on motion of the slag. The second is the refining of metal as it is melted, passed through the slag, and collected in a pool at the top of the ingot. Since the present work is concerned with the flow and the thermal characteristics of ESR, the second aspect (i.e. refining) is not important here. It should be recognized, however, that even though the amount of matter involved in exchange reactions is quite small as compared to the total amount of metal being transferred from the electrode to the ingot, the thermal effects arising from concentration polarization and the enthalpy involved in various exchange reactions may influence the net heat supply rate in the regions of the slag near its interfaces with the electrode and the metal pool. These, in turn, will affect the melting rate of the electrode and the depth of molten metal pool.

9) The interaction between the electromagnetic force field and the turbulent fluctuations is neglected in absence of satisfactory methods for treating it.

10) An insulating slag skin is assumed to form on the interior surface of the mold.

Mathematical statements of these assumptions together with assumptions made in formulating the boundary conditions will be presented at appropriate places.



3.2 Physical concept of the process model.

3.4 Statement of the Mathematical Tasks

In context of the assumptions outlined above, the model to be developed in this work seeks mathematical representation for the following physical phenomena:

(1) Electromagnetic field

This is represented by the magnetohydrodynamic form of Maxwell's equations written for different portions of an ESR system and interconnected through boundary conditions. Solution of these equations gives spatial distributions of current densities, Joule heat and Lorentz forces.

(2) Recirculating flow in slag

This is represented by the turbulent Navier Stokes equations with due allowance for body forces (electromagnetic and natural convection). Turbulent viscosity is computed by solving two additional differential equations.

(3) Heat transfer and phase change

The mathematical statement of heat transfer phenomena in the system is given by convective heat transport equations. The convection terms in these equations account for heat transfer due to turbulent recirculating flow in the slag and heat transfer due to movement of various interfaces. In the slag, allowance has to be made for Joule heat generation and heat extraction by metal droplets and in the mushy zone account has to be taken of the release of latent heat.

3.5 Governing Equations for Flow and Heat Transfer Phenomena in the Electroslag Refining Process

Equations mentioned in the previous section are now presented. First the vectorial forms of these equations are given in order that some general conclusions can be obtained and then the equations are stated in the cylindrical coordinate system with axial symmetry.

3.5.1 Maxwell's Equations

Upon applying the MHD approximation, Maxwell's equations take the following form⁴³:

$$\text{(Faraday's Law)} \quad \nabla \times \vec{E} = - \frac{\partial \vec{B}}{\partial t} \quad (3.1)$$

$$\text{(Ampere's Law)} \quad \nabla \times \vec{H} = \vec{J} \quad (3.2)$$

$$\nabla \cdot \vec{B} = 0 \quad (3.3)$$

$$\nabla \cdot \vec{J} = 0 \quad (3.4)$$

Here,

\vec{E} is the electric field, Volt/m

\vec{B} is the magnetic flux density, Weber/m² (or
Teslas)

\vec{H} is the magnetic field intensity, Amp/m

\vec{J} is the current density, Amp/m²

t is time, s

Furthermore, we have

$$\vec{J} = \sigma (\vec{E} + \vec{V} \times \vec{B}) \quad (3.5)$$

and

$$\vec{B} = \mu_0 \vec{H} \quad (3.6)$$

Where σ is the electrical conductivity in 1/Ohm-m, μ_0 is the magnetic permeability of free space in Henry/m and \vec{V} is the velocity of medium in m/s.

In brief, the meaning of these equations is as follows:

Eq. (3.1) relates the change in the magnetic flux density to the induced emf. Eq. (3.2) is Ampere's circuital law which relates the induced magnetic field intensity to current in the circuit. Eqs. (3.3) and (3.4) represent the continuity of the magnetic lines of force and conservation of current respectively.

Eqs. (3.1) through (3.6) can be combined ⁴³ to give:

$$\frac{\partial \vec{H}}{\partial t} = \eta \nabla^2 \vec{H} + \vec{\nabla} \times (\vec{V} \times \vec{H}) \quad (3.7)$$

where $\eta = \frac{1}{\sigma \mu_0}$ is called the magnetic diffusivity.

Terms arising from the spatial dependence of σ have been neglected. Eq. (3.7), along with Eq. (3.4), contains all the information about \vec{H} included in Maxwell's equations.

By using dimensional relation, the ratio of the terms on the r.h.s of Eq. (3.7) is:

$$\frac{|\nabla \times (\nabla \times \underline{H})|}{|\eta \nabla^2 \underline{H}|} = \frac{\text{magnetic convection}}{\text{magnetic diffusion}} \approx 0 \left(\frac{V_0 H_0 / L}{\eta H_0 / L^2} \right)$$

$$= 0 \text{ (Re}_m \text{)} \quad (3.8)$$

where $\text{Re}_m = V_0 L \sigma \mu_0$ is called magnetic Reynolds number. L and V_0 are characteristic length and velocity respectively. In Eq. (3.8) the symbol $0(Q)$ stands for the order of magnitude of a physical quantity Q . For ESR systems, in general, $\text{Re}_m \ll 1$ and hence the convection term can be neglected¹³. The magnetic field equation then reduces to,

$$\frac{\partial \underline{H}}{\partial t} = \eta \nabla^2 \underline{H} \quad (3.9)$$

The electromagnetic body force (in N/m^3) is given by:

$$\underline{F}_{be} = \underline{J} \times \underline{B} = \mu_0 \underline{J} \times \underline{H} \quad (3.10)$$

In cylindrical coordinate system with axial symmetry

($H_r = H_z = \frac{\partial}{\partial \theta} = 0$), Eq. (3.9) can be written as

$$\sigma \mu_0 \frac{\partial H_\theta}{\partial t} = \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial}{\partial r} (r H_\theta) \right] + \frac{\partial^2 H_\theta}{\partial z^2} \quad (3.11)$$

In order to account for AC operation, phasor notation^{43,44} (explained in Appendix A) is used. In this notation

$$\begin{aligned} H_{\theta} &= \hat{H}_{\theta} e^{j\omega t} \\ J_r &= \hat{J}_r e^{j\omega t} \\ \text{and } J_z &= \hat{J}_z e^{j\omega t} \end{aligned} \quad (3.12a,b,c)$$

Where \hat{H}_{θ} , \hat{J}_r , \hat{J}_z are the complex amplitudes of H_{θ} , J_r and J_z respectively, ω is the angular frequency and j is $\sqrt{-1}$. The momentary physical values of H_{θ} , J_r and J_z are the real parts of the complex functions given above.

In phasor notation, Eq. (3.11) takes the following form:

$$j\sigma\mu_0\omega\hat{H}_{\theta} = \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial}{\partial r} (r\hat{H}_{\theta}) \right] + \frac{\partial^2 \hat{H}_{\theta}}{\partial z^2} \quad (3.13)$$

which has to be solved for the real and imaginary parts. After solving Eq. (3.13) with appropriate boundary conditions, Eq. (3.2) can be used to calculate current densities as follows:

$$\begin{aligned} \hat{J}_r &= - \frac{\partial \hat{H}_{\theta}}{\partial z} \\ \text{and } \hat{J}_z &= \frac{1}{r} \frac{\partial}{\partial r} (r\hat{H}_{\theta}) \end{aligned} \quad (3.14a,b)$$

Using Eq. (3.10) and averaging ^{43,44} over the period $\frac{2\pi}{\omega}$ gives the following relationships for the time averaged components of electromagnetic body force:

$$F_r = -\frac{1}{2} \mu_0 \operatorname{Re}(\hat{H}_\theta \overline{\hat{J}_z})$$

$$\text{and } F_z = \frac{1}{2} \mu_0 \operatorname{Re}(\hat{H}_\theta \overline{\hat{J}_r}) \quad (3.15a,b)$$

where Re stands for the real part and the overhead bar denotes the complex conjugate. Similarly the time averaged heat generation rate per unit volume is given by:

$$Q_j = \frac{1}{2} \operatorname{Re} \left[\frac{\hat{J}_r \overline{\hat{J}_r} + \hat{J}_z \overline{\hat{J}_z}}{\sigma} \right] \quad (3.16)$$

The electrical power input to the system is computed by using:

$$W = 2\pi \int_z \int_r Q_j(r,z) r dr dz \quad (3.16a)$$

3.5.2 Fluid Flow Equations

Turbulent motion in the system is represented by the time-smoothed equations of continuity and motion (i.e. Navier-Stokes equations) written below in vectorial form ⁴⁵:

$$\nabla \cdot \vec{V} = 0 \quad (3.17)$$

$$\rho (\overline{\nabla \cdot \nabla}) \overline{\nabla} = - \overline{\nabla \overline{P}} - \overline{\nabla \cdot \overline{\tau}} + \overline{\mathbf{F}_b}$$

inertial force pressure force viscous and Reynolds forces body force

(3.18)

Here

ρ is the (average) density of the fluid
 $\overline{\nabla}$ is the velocity vector
 \overline{P} is the pressure
 $\overline{\tau}$ is the stress tensor, which includes both viscous and Reynolds stresses $\overline{(\rho v_i' v_j')}$
 $\overline{\mathbf{F}_b}$ is the body force (per unit volume) vector which incorporates both electromagnetic and buoyancy driving forces and is given by

$$\overline{\mathbf{F}_b} = \overline{\mathbf{J} \times \mathbf{B}} + \rho [1 - \beta (\overline{T} - T_0)] \mathbf{g} \quad (3.19)$$

Here

β is the coefficient of volume expansion
 \mathbf{g} is the acceleration due to gravity
 \overline{T} is the temperature at a given location in the fluid
 T_0 is a reference temperature

The overhead bar in the above equations represents time-smoothed parameters. An assumption inherent in writing equations (3.17) and (3.18) is that the density variations due to temperature gradients are of importance only in

producing buoyancy forces and density ρ is supposed to be evaluated at the reference temperature T_0 .

Following Boussinesq⁴⁵, turbulent or Reynolds stresses can be computed using the same relationships which exist for viscous stresses in a Newtonian fluid but by replacing molecular viscosity of the fluid with a scalar turbulent viscosity. As mentioned in the previous chapter, turbulent viscosity is computed by using a suitable model of turbulence. In the present work a two equation model of turbulence, called the $k - \epsilon$ model⁴⁶ is used. Here k is the turbulence kinetic energy per unit mass and ϵ is the dissipation rate of turbulence energy. As pointed out by Launder and Spalding⁴⁶, a wide variety of flows may be adequately represented by this model without adjustments to model parameters in the near wall regions. Also a comparison of the predictions of various models, with each other and with experiments has shown⁴⁶ the $k - \epsilon$ model to be surpassed only by more complex "Reynolds - Stress" models. It should be noted, furthermore, that the equation for ϵ contains fewer terms, the exact form of the equation can be derived relatively easily and that ϵ appears directly as an unknown in the equation for k . The model postulates:

$$\mu_t = C_d \rho k^2 / \epsilon \quad (3.20)$$

(turbulent viscosity)

Here C_d is a dissipation constant.

Distributions of k and ϵ in the flow field are represented by transport equations for scalar quantities. In vectorial form, these can be represented as ^{36,46} :

$$\rho (\bar{\mathbf{V}} \cdot \nabla \phi) = \nabla \cdot \left(\frac{\mu_{\text{eff}}}{\sigma_{\phi}} \nabla \phi \right) + S_{\phi} \quad (3.21a,b)$$

convective transport viscous and source
 turbulent
 diffusive transport

Here ϕ represents k or ϵ , σ_{ϕ} is the effective Prandtl number for transport of ϕ , μ_{eff} is the effective viscosity and is the sum of molecular viscosity (μ) and turbulent viscosity (μ_t) and S_{ϕ} represents the net rate (volumetric) of generation of ϕ .

Equation of motion and the transport equations for k and ϵ will now be given for an axisymmetric cylindrical coordinate system.

Upon introducing the vorticity, ξ

$$\xi = \frac{\partial \bar{V}_r}{\partial z} - \frac{\partial \bar{V}_z}{\partial r} \quad (3.22)$$

and the stream function, ψ

$$\begin{aligned} \bar{V}_r &= - \frac{1}{\rho r} \frac{\partial \psi}{\partial z} , \\ \bar{V}_z &= \frac{1}{\rho r} \frac{\partial \psi}{\partial r} \end{aligned} \quad (3.23 a,b)$$

the equation of motion [Eq. (3.18)] can be written as the vorticity transport equation given below ³⁹.

$$r^2 \left(\frac{\partial}{\partial z} \left(\frac{\xi}{r} \frac{\partial \psi}{\partial r} \right) - \frac{\partial}{\partial r} \left(\frac{\xi}{r} \frac{\partial \psi}{\partial z} \right) \right) - \frac{\partial}{\partial z} \left(r^3 \frac{\partial}{\partial z} (\mu_{\text{eff}} \frac{\xi}{r}) \right) - \frac{\partial}{\partial r} \left(r^3 \frac{\partial}{\partial r} (\mu_{\text{eff}} \frac{\xi}{r}) \right) + r^2 \left(\frac{\partial \bar{F}}{\partial r} \frac{z}{r} - \frac{\partial \bar{F}}{\partial z} \frac{r}{r} \right) = 0 \quad (3.24)$$

Using Eqns. (3.19), (3.15a,b) and (3.14a,b), the last term in the above equation can be shown to take the following form:

$$r^2 \left(\frac{\partial \bar{F}}{\partial r} \frac{z}{r} - \frac{\partial \bar{F}}{\partial z} \frac{r}{r} \right) = - \left(r \mu_0 \text{Re} (\hat{H}_\theta \bar{J}_r) \right) + r^2 \rho \beta g \left(\frac{\partial \bar{T}}{\partial r} \right) \quad (3.25)$$

electromagnetic buoyancy
contribution contribution

In addition the following relationship exists between ξ and ψ :

$$\xi + \frac{\partial}{\partial z} \left(\frac{1}{\rho r} \frac{\partial \psi}{\partial z} \right) + \frac{\partial}{\partial r} \left(\frac{1}{\rho r} \frac{\partial \psi}{\partial r} \right) = 0 \quad (3.26)$$

Transport equations for k and ϵ , in the axisymmetric cylindrical coordinate system, are given below:

Transport Equation for k

$$\frac{\partial}{\partial z} \left(k \frac{\partial \psi}{\partial r} \right) - \frac{\partial}{\partial r} \left(k \frac{\partial \psi}{\partial z} \right) - \frac{\partial}{\partial z} \left(r \frac{\mu_{\text{eff}}}{\sigma_k} \frac{\partial k}{\partial z} \right) - \frac{\partial}{\partial r} \left(r \frac{\mu_{\text{eff}}}{\sigma_k} \frac{\partial k}{\partial r} \right) = r S_k \quad (3.27)$$

$$\text{where } S_k = G - D \quad (3.28)$$

$$G = 2\mu_t \left[\left(\frac{\partial \bar{V}_z}{\partial z} \right)^2 + \left(\frac{\partial \bar{V}_r}{\partial r} \right)^2 + \left(\frac{\bar{V}_r}{r} \right)^2 + \frac{1}{2} \left(\frac{\partial \bar{V}_r}{\partial z} + \frac{\partial \bar{V}_z}{\partial r} \right)^2 \right] \quad (3.29a)$$

$$\text{and } D = \rho \epsilon \quad (3.29b)$$

Transport Equation for ϵ

$$\frac{\partial}{\partial z} \left(\epsilon \frac{\partial \psi}{\partial r} \right) - \frac{\partial}{\partial r} \left(\epsilon \frac{\partial \psi}{\partial z} \right) - \frac{\partial}{\partial z} \left(r \frac{\mu_{\text{eff}}}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial z} \right) - \frac{\partial}{\partial r} \left(r \frac{\mu_{\text{eff}}}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial r} \right) = r S_\epsilon \quad (3.30)$$

where

$$S_\epsilon = C_1 \frac{\epsilon}{k} G - C_2 \rho \frac{\epsilon^2}{k} \quad (3.31)$$

As seen from Eqn. (3.28), the source S_k of the turbulence kinetic energy is made up of two terms G and D . The generation term, G , represents kinetic energy exchange between the mean flow and the turbulence. The dissipation term, D , represents the rate at which viscous stresses perform deformation work against the fluctuating strain rate. The origin and the form of these terms are discussed by Tennekes and Lumley⁴⁷ and by Hinze⁴⁸.

The source of ϵ , S_ϵ is also made up of a positive and a negative term. As in the previous case for S_k , the terms in Eqn. (3.31) represent interaction of turbulence with the mean flow and the self interaction of turbulence. The parameters σ_k , σ_ϵ , C_1 , C_2 originate because of the assumptions made in representing diffusive action of

turbulence by means of a gradient law (e.g. $\rho \overline{u'k'} = -\frac{\mu_t}{\sigma_k} \frac{\partial k}{\partial y}$) and in modelling source terms. The

significance of these parameters and their estimation are discussed in reference 36.

3.5.3 Heat transfer equations

Equations for heat transfer phenomena taking place in different portions of an ESR system are given below.

3.5.3A Heat transfer in slag

The vectorial form of the convective heat transfer equation is written as ⁴⁵:

$$\rho C_p (\vec{V} \cdot \nabla \bar{T}) = \nabla \cdot \vec{K}_{eff} \nabla \bar{T} + S_T \quad (3.32)$$

convective	laminar and	source
transport	turbulent diffusive	
	transport	

Here

C_p is the specific heat of slag

\bar{T} is the time-smoothed temperature

S_T is the net volumetric heat generation rate
in the slag

K_{eff} is the effective thermal conductivity in the
slag.

S_T , the source term in Eqn. (3.32) consists of two terms as shown below:

$$S_T = Q_j - Q_d \chi \quad (3.33)$$

where Q_j is the volumetric rate of Joule heat generation given by Eqn. (3.16) and Q_d is the rate at which heat is extracted (per unit volume) from the slag by the falling metal droplets. An expression for Q_d will be derived subsequently. χ in Eqn. (3.33) is defined as follows:

$$\begin{aligned} \chi &= 1 && \text{when } r \leq R_e \\ \chi &= 0 && \text{when } r > R_e \end{aligned} \quad (3.34a,b)$$

where R_e is the radius of the electrode. Conditions (3.34a,b) reflect the fact that droplets remove heat from the central column of the slag which has a radius equal to that of the electrode.

The effective thermal conductivity, K_{eff} is given by

$$K_{eff} = \underset{\substack{\text{molecular} \\ \text{conductivity}}}{K} + \underset{\substack{\text{turbulent} \\ \text{conductivity}}}{K_t} \quad (3.35)$$

After μ_t , the turbulent viscosity, has been calculated using the k- ϵ model, K_t can be evaluated by using,

$$\sigma_t = \frac{C_p \mu_t}{K_t} \approx 1 \quad (3.36)$$

where σ_t is the turbulence Prandtl number. The convective transport term in Eqn. (3.32) accounts for the fluid velocity as well as the rise of the slag.

In the axisymmetric cylindrical coordinate system and using Eqns. (3.23a,b), Eqn. (3.32) can be written as:

$$r\rho C_p V_c \frac{\partial \bar{T}}{\partial z} + C_p \left[\frac{\partial}{\partial z} \left(\bar{T} \frac{\partial \psi}{\partial r} \right) - \frac{\partial}{\partial r} \left(\bar{T} \frac{\partial \psi}{\partial z} \right) \right] =$$

$$\frac{\partial}{\partial r} \left(K_{\text{eff}} r \frac{\partial \bar{T}}{\partial r} \right) + \frac{\partial}{\partial z} \left(K_{\text{eff}} r \frac{\partial \bar{T}}{\partial z} \right) + r S_T \quad (3.37)$$

where V_c is the casting rate.

3.5.3B Heat transfer in other portions of ESR

The temperature distribution in the electrode, the molten metal pool, the mushy zone and the solid ingot can be expressed by the following general equation:

$$\rho_i C_{p_i} (\vec{V}_i \cdot \nabla T) = \nabla \cdot K_i \nabla T + S_{T,i} \quad (3.38 a, b, c, d)$$

where, $i = e$ (electrode), l (metal pool),

m (mushy zone), s (solid ingot)

and \vec{V}_i accounts for the rise of the ingot surface (i.e. casting rate) and the downward movement of the electrode. \vec{V}_i has only the axial (i.e. z-direction) component.

For the coordinate being used, Eqn (3.38) can be written as:

$$r \rho_i C_{p_i} V_i \frac{\partial T}{\partial z} = \frac{\partial}{\partial r} \left(K_i r \frac{\partial T}{\partial r} \right) + \frac{\partial}{\partial z} \left(K_i r \frac{\partial T}{\partial z} \right) + r S_{T,i} \quad (3.39 a,b,c,d)$$

For the electrode, we have

$$V_e = V_t + V_c \quad (3.40)$$

where V_t is the speed of travel of electrode

$$S_{T,e} = 0 \quad (3.41)$$

For the metal pool

$$V_l = V_c \quad (3.42)$$

$$S_{T,l} = 0 \quad (3.43)$$

$$\begin{aligned} K_l &= \text{effective thermal conductivity in} \\ &\quad \text{the metal pool} \\ &= (1 + \Lambda) K_{m\ell} \end{aligned} \quad (3.44)$$

where $K_{m\ell}$ is the atomic thermal conductivity of molten metal. The evaluation of Λ will be discussed in Chapter V.

For the mushy zone

$$V_m = V_c \quad (3.45)$$

$$S_{T,m} = V_c \rho_m \lambda \frac{\partial f_s}{\partial z} \quad (3.46)$$

where λ is the latent heat of fusion and f_s is the fraction of solids in the mushy zone. $S_{T,m}$ represents the rate of heat release (per unit volume) due to solidification.

For simplicity, a linear relationship will be assumed between f_s and T^* , i.e.

$$f_s = \frac{T_{\ell,m} - T}{T_{\ell,m} - T_{s,m}} \quad (3.47)$$

where $T_{\ell,m}$ and $T_{s,m}$ are the liquidus and solidus temperatures of the metal. Then Eq. (3.36) can be written as

$$S_{T,m} = - \frac{V_c \rho_m \lambda}{T_{\ell,m} - T_{s,m}} \frac{\partial T}{\partial z} \quad (3.48)$$

For the ingot we have,

$$V_s = V_c \quad (3.49)$$

$$S_{T,s} = 0 \quad (3.50)$$

It is to be noted that Joule heating has been ignored everywhere except in the slag. This is reasonable because electrical conductivity of the metal is very large.

The melting rate of the electrode is calculated by making a heat balance at the slag-electrode interface;

* The use of more complex relationships (e.g. solidification models) can be easily accommodated.

$$V_{me} = (q_{se} - K_e \left. \frac{\partial T}{\partial z} \right|_e) / (\rho_e \lambda_e) \quad (3.51)$$

where

q_{se} is heat flux from the slag to the electrode surface

$K_e \left. \frac{\partial T}{\partial z} \right|_e$ is heat flux conducted into the electrode

λ_e is the latent heat for melting of electrode.

q_{se} in Eq. (3.51) is evaluated either by using wall flux relation to be described later or by using

$$-q_{se} = -K \left. \frac{\partial T}{\partial z} \right|_{sl} \quad (3.52)$$

3.5.4 Droplet Behavior

In this section, expressions are developed to calculate heat transport by metal droplets falling through the slag. The treatment given here follows that of Dilawari and Szekely¹⁵.

3.5.4A Droplet radius, r_d

For large electrodes, it has been suggested by Campbell⁴² that metal droplets are formed at discrete locations on the tip of the electrode. The droplet

radius r_d is, therefore, assumed independent of R_e . Then from dimensional arguments and by using experimental results, Campbell has given the following relationship,

$$r_d = \left(\frac{2.04\gamma}{g \Delta \rho} \right)^{1/2} \quad (3.53a)$$

where γ is the interfacial tension between liquid slag and liquid metal, $\Delta\rho$ is the difference in density between the two liquids and g is the acceleration due to gravity.

For small electrodes, the following relation is deduced by equating gravitational and surface tension forces:

$$r_d = \left(\frac{1.5\gamma R_e}{g \Delta \rho} \right)^{1/3} \quad (3.53b)$$

3.5.4 B Droplet motion in the slag

Considering the slag to be stagnant (it is shown later that the slag velocity is substantially lower than the average falling velocity of the drop) and assuming the droplet to be a rigid sphere the equation describing the droplet motion takes the following form⁴⁹:

$$\frac{4}{3} \pi r_d^3 \left(\rho_d + \frac{\rho}{2} \right) \frac{dU}{dt} = \frac{4}{3} \pi r_d^3 \Delta \rho g - C_D \pi r_d^2 \rho \frac{U^2}{2} \quad (3.54)$$

where

ρ_d is the density of metal droplet
 ρ is the density of slag

C_D is the drag coefficient
 U is the velocity
 and $\Delta\rho$ is the difference in densities of the drop
 and the slag (i.e. $\rho_d - \rho$).

Eq. (3.54) can be written as follows:

$$\frac{dU}{U^2 - a^2} = - \frac{3}{8} \frac{C_D}{r_d} \frac{\rho}{\rho_d + 0.5\rho} dt \quad (3.55)$$

$$\text{where } a^2 = \frac{8}{3} \frac{\Delta\rho}{\rho} \frac{gr_d}{C_D} \quad (3.56)$$

On integration, Eq. (3.55) yields:

$$U = \sqrt{\frac{\bar{A}}{B}} \frac{e^{2\sqrt{AB}t} - 1}{e^{2\sqrt{AB}t} + 1} \quad (3.57)$$

where $A = [\Delta\rho / (\rho_d + 0.5\rho)] g$

$$\text{and } B = \frac{3}{8} \frac{C_D}{r_d} \frac{\rho}{\rho_d + 0.5\rho} \quad (3.58a,b)$$

It follows from Eq. (3.57) that the terminal velocity of the droplet is given by:

$$U_t = \sqrt{\frac{\bar{A}}{B}} \quad (3.59)$$

Thus Eq. (3.57) can be written as

$$U = U_t \frac{e^{Ct} - 1}{e^{Ct} + 1} \quad (3.60)$$

where $C = 2A/U_t$ (3.61)

If L_1 is the distance from the electrode tip to the slag-metal interface and τ is the residence time of the droplet, then

$$L_1 = \int_0^{\tau} U dt \quad (3.62)$$

Substituting Eq. (3.60) in the above equation gives:

$$\frac{(1 + e^{C\tau})^2}{4 e^{C\tau}} = e^{CL_1/U_t} \quad (3.63)$$

from which, the following expression can be deduced,

$$\tau = 1/C \ln [(m-1) + \sqrt{m^2 - 2m}] \quad (3.64)$$

where $m = 2e^{2AL_1/U_t^2}$ (3.65)

In the equations given above, C_D , the drag coefficient is not known and thus U_t is unknown. Following Dilawari and Szekely¹⁵, U_t is estimated by using a correlation proposed by Hu and Kintner⁵⁰ who studied the steady motion of single drops of various organic liquids falling through stationary water. They concluded that the droplet motion can be represented in terms of two variables defined below:

$$Y = C_D We P_d^{0.15} \quad (3.66)$$

$$X = (Re_d/P_d^{0.15}) + 0.75 \quad (3.67)$$

where

$$We = \text{Weber number} = \frac{U_t^2 d_d \rho}{\gamma}$$

$$P_d = \text{a physical property group} = \frac{\rho \gamma^3}{g \mu^4} \frac{\rho}{\Delta \rho}$$

$$Re_d = \text{droplet Reynolds number} = \frac{U_t d_d \rho}{\mu}$$

$$d_d = \text{diameter of a droplet}$$

From Eq. (3.54) one can derive,

$$C_D = 4/3 \frac{\Delta \rho g d_d}{\rho U_t^2} \quad (3.68)$$

Using definitions of C_D and We , Eq. (3.66) can be written as;

$$Y = 4/3 \frac{g d_d^2 \Delta \rho}{\gamma} P_d^{0.15} \quad (3.69)$$

Thus Y depends on physical properties of the system only.

Hu and Kintner⁵⁰ proposed the following relationships between Y and X :

$$X = (0.75Y)^{0.784} \quad \text{for} \quad 2 < Y \leq 70$$

$$X = (22.22Y)^{0.422} \quad \text{for} \quad Y \geq 70 \quad (3.70a,b)$$

Once X is calculated using one of the above equations, U_t can be calculated as follows:

$$Re_d = (X - 0.75) P_d^{0.15}$$

which gives

$$U_t = \frac{Re_d \mu}{d_d \rho} \quad (3.71)$$

3.5.4C Rate of heat removal by droplets from the slag

By assuming that heat transfer from the slag to a droplet can be characterized by a single heat transfer coefficient, h and an average temperature of the slag between the electrode tip and the slag-metal interface (T_B), one can write the following equation for heat balance on a single drop:

$$\frac{4}{3} \pi r_d^3 \rho_d C_{P,d} \frac{dT_d}{dt} = h (T_B - T_d) 4\pi r_d^2 \quad (3.72)$$

With the initial condition, $t = 0$, $T_d = T_{me}$ where, T_d is the temperature of the drop and T_{me} is the melting temperature of the electrode.

The heat transfer coefficient, h can be estimated using the average velocity, U_{av} ($=L_1/\tau$) of the droplet in the slag, from suitable correlations⁵¹. In the present work a correlation proposed by Spelles⁵² is used. This correlation is given below:

$$\frac{hd_d}{K} = 0.8 \left(d_d U_{av} \rho / \mu \right)^{1/2} (C_p \mu / K)^{1/3} \quad (3.73)$$

where ρ , K , C_p , μ are respectively the density, the thermal conductivity, the specific heat and the viscosity of the slag.

Eq. (3.72) can be integrated to give the following expression for the final temperature, T_f of a droplet:

$$T_f = T_B - (T_B - T_{me}) e^{-S\tau} \quad (3.74)$$

where

$$S = \frac{3h}{r_d C_{p,d} \rho_d} \quad (3.75)$$

The rate at which heat is removed from the slag by the falling droplets is given by:

$$Q_s = \pi R_e^2 V_{me} \rho_e C_{p,d} (T_f - T_{me}) \quad (3.76)$$

Where V_{me} , as defined by Eq. (3.51) is the melting rate of the electrode. Q_d , appearing in Eq (3.33) is obtained from:

$$Q_d = \frac{Q_s}{\pi R_e^2 L_1} \quad (3.77)$$

i.e. droplets are assumed to remove heat uniformly from the volume of slag forming a central column of radius R_e and height L_1 .

3.6 The Boundary Conditions

In this section expressions are developed for the dependent variables (or their gradients) on the bounding surfaces sketched in Fig. 3.2.

3.6.1 Boundary conditions for the magnetic field equation

Boundary conditions for Eq. (3.13) have to express the following physical constraints ⁴³:

(1) the continuity of the tangential component of the electric field across the phase boundaries, i.e.

$$\underline{n} \times [\underline{E}_1 - \underline{E}_2] = 0 \quad (3.78)$$

where \underline{n} is the unit vector normal to the boundary separating media 1 and 2. Eq. (3.78) is obtained by applying the integral form of Eq. (3.1) across the phase boundary.

(2) the statement of Ampere's Law [obtained by applying Stoke's theorem to Eq.(3.2)], i.e.

$$\oint \underline{H} \cdot d\ell = \int \underline{J} \cdot d\mathcal{S} \quad (3.79)$$

Eq. (3.79) states that the line integral of \underline{H} around the path enclosing an area through which a current is passing is equal to the current.

Constraints 1 and 2 are the statements of physical laws derivable from Maxwell's equations. In addition, the following assumptions have to be made:

$$(3) \text{ axial symmetry gives } \hat{H}_\theta = 0 \text{ at } r = 0 \quad (3.80)$$

- (4) at the free slag surface ($z = Z_1, R_e \leq r \leq R_m$)
 $\hat{J}_z = 0$
- (5) at the upper boundary of electrode ($z = 0, 0 \leq r \leq R_e$) $\hat{J}_r \approx 0$
- (6) at the lower boundary of ingot ($z = Z_6, 0 \leq r \leq R_m$) $\hat{J}_r \approx 0$.

Mathematical statements for these assumptions in terms of the magnetic field intensity, \hat{H}_θ are given below:

- (1) at $z = 0, 0 \leq r \leq R_e$, (upper boundary of electrode)

$$\frac{\partial \hat{H}_\theta}{\partial z} = 0 \quad (3.81)$$

$$(\hat{J}_r = 0)$$

- (2) at $r = R_e, 0 \leq z \leq Z_1$ (surface of electrode above slag)

$$\hat{H}_\theta = I_0 / (2\pi R_e) \quad (3.82)$$

(Statement of Ampere's Law)

where I_0 is the maximum value of the total current.

- (3) at $r = R_e, Z_1 \leq z \leq Z_2$ (vertical surface of electrode immersed in slag)

$$\frac{1}{\sigma} \hat{J}_z \Big|_e = \frac{1}{\sigma} \hat{J}_z \Big|_{sl} \quad (3.83)$$

(Continuity of \hat{E}_z)

(4) at $r = R_m$, $Z_1 \leq z \leq Z_6$ (slag-mold interface)

$$\hat{H}_\theta = \frac{I_0}{2\pi R_m} \quad (3.84)$$

(Ampere's Law)

(5) at $z = Z_2$, $0 \leq r \leq R_e$ (slag- electrode interface)

$$\frac{1}{\sigma} \hat{J}_r \Big|_e = \frac{1}{\sigma} \hat{J}_r \Big|_{sl}$$

(Continuity of \hat{E}_r)

which gives,

$$\frac{1}{\sigma} \frac{\partial \hat{H}_\theta}{\partial z} \Big|_e = \frac{1}{\sigma} \frac{\partial \hat{H}_\theta}{\partial z} \Big|_{sl} \quad (3.85)$$

(6) at $z = Z_1$, $R_e \leq r \leq R_m$ (free surface of slag)

$$\hat{H}_\theta = \frac{I_0}{2\pi r} \quad (3.86)$$

(from $\hat{J}_z = \frac{1}{r} \frac{\partial}{\partial r} (r \hat{H}_\theta) = 0$)

(7) at $z = Z_3$, $0 \leq r \leq R_m$ (slag-metal interface)

$$\frac{1}{\sigma} \frac{\partial \hat{H}_\theta}{\partial z} \Big|_{sl} = \frac{1}{\sigma} \frac{\partial \hat{H}_\theta}{\partial z} \Big|_l \quad (3.87)$$

(continuity of \hat{E}_r)

(8) at $z = Z_6$, $0 \leq r \leq R_m$ (lower boundary of ingot)

$$\frac{\partial \hat{H}_\theta}{\partial z} = 0 \quad (3.88)$$

$$(\hat{J}_r = 0)$$

It is to be noted that boundary conditions are stated in terms of \hat{H}_θ from which real and imaginary parts can be separated.

3.6.2 Boundary conditions for the fluid flow equations

In a physical sense the boundary conditions for the fluid flow equations have to express the following:

(1) Symmetry about the centerline

(2) The "no-slip" condition for the velocity at the solid boundaries (i.e. zero velocity at the stationary solid boundaries). As discussed in section 3.3, the slag-metal interface is assumed to be a rigid interface

(3) At the free surface of the slag, the fluxes of momentum and turbulence quantities (k and ϵ) are assumed to be zero.

Since we use the vorticity transport equation, the above conditions have to be stated in terms of vorticity (ξ) and stream function (ψ). Furthermore, boundary conditions have to be stated for k and ϵ as well. The expressions for boundary conditions in terms of ξ and ψ .

are derived in texts on computational fluid dynamics^{39,40} and a brief summary of these derivations are given in Appendix B. In this chapter, only the final form of the expressions are given. Also the wall function treatment for the turbulence quantities is discussed in the next chapter. With reference to Fig. 3.2 the boundary conditions for the flow equations are as follows:

$$(1) \quad \text{at } r = 0, \quad z_2 \leq z \leq z_3$$

$$\psi = \frac{\partial k}{\partial r} = \frac{\partial \epsilon}{\partial r} = 0$$

and

$$\left(\frac{\xi}{r}\right)_0 = \frac{8}{\rho} \left[\frac{\psi_0 - \psi_2}{r_2^2} + \frac{\psi_1 - \psi_0}{r_1^2} \right] / (r_2^2 - r_1^2) \quad *$$

(3.89a,b)

where suffixes 0, 1, 2 denote the points on the axis of symmetry and the adjacent grid nodes in the r-direction respectively.

$$(2) \quad \text{at } z = z_1, \quad R_e \leq r \leq R_m \quad (\text{free slag surface})$$

$$\psi = \frac{\xi}{r} = \frac{\partial k}{\partial z} = \frac{\partial \epsilon}{\partial z} = 0 \quad (3.90)$$

$\psi = 0$ follows from $\bar{V}_z = 0$ and $\xi = 0$ follows from

$$\mu_{\text{eff}} \left(\frac{\partial \bar{V}_r}{\partial z} + \frac{\partial \bar{V}_z}{\partial r} \right) = 0 \quad \text{and from the definition of } \xi \text{ (Eq.3.22).}$$

* Derivation given in Appendix B

(3) at $z = z_2$, $0 \leq r \leq R_e$ (slag-electrode interface)

$$\psi = 0 \quad (3.91a)$$

$$k = \varepsilon = 0 \quad ** \quad (3.91b)$$

and

$$\left(\frac{\xi}{r}\right)_0 = \frac{3 (\psi_0 - \psi_1)}{\rho r^2 (z_1 - z_0)^2} - \frac{1}{2} \left(\frac{\xi}{r}\right)_1^* \quad (3.91c)$$

where suffixes 0 and 1 refer to a grid node on the boundary and to the adjacent node in z - direction, respectively.

(4) at $z = z_3$, $0 \leq r \leq R_m$ (slag-metal interface)

$$\psi = 0 \quad (3.92a)$$

$$k = \varepsilon = 0 \quad ** \quad (3.92b)$$

and

$$\left(\frac{\xi}{r}\right)_0 = \frac{3 (\psi_0 - \psi_1)}{\rho r^2 (z_1 - z_0)^2} - \frac{1}{2} \left(\frac{\xi}{r}\right)_1^* \quad (3.92c)$$

where suffixes have the same meaning as in the case of Eq. (3.91c).

* derivation given in Appendix B

** alternate and more realistic formulation through the use of wall functions is discussed in next chapter.

(5) at $r = R_e$, $z_1 \leq z \leq z_2$ (vertical surface of electrode immersed in slag)

$$\psi = 0 \quad (3.93a)$$

$$k = \epsilon = 0 \quad ** \quad (3.93b)$$

and

$$\begin{aligned} \left(\frac{\xi}{r}\right)_0 &= \frac{3}{\rho} \frac{(\psi_0 - \psi_1)}{(r_1 - r_0)^2 r_0 r_1} - \frac{1}{2} \left(\frac{\xi}{r}\right)_1 \\ &+ \frac{\rho g \beta}{4R_e \mu_{eff,1}} (r_1 - r_0) (T_0 - T_1) \quad * \quad (3.93c) \end{aligned}$$

where suffixes 0 and 1 refer to a grid point on the boundary and to the adjacent node in r - direction, respectively.

(6) at $r = R_m$, $z_1 \leq z \leq z_3$ (slag-mold interface)

$$\psi = 0 \quad (3.94a)$$

$$k = \epsilon = 0 \quad ** \quad (3.94b)$$

and

$$\begin{aligned} \left(\frac{\xi}{r}\right)_0 &= \frac{3}{\rho} \frac{(\psi_0 - \psi_1)}{(r_1 - r_0)^2 r_0 r_1} - \frac{1}{2} \left(\frac{\xi}{r}\right)_1 \\ &+ \frac{\rho g \beta}{4R_m \mu_{eff,1}} (r_1 - r_0) (T_0 - T_1) \quad * \quad (3.94c) \end{aligned}$$

* derivation discussed in Appendix B

** alternate and more realistic formulation through the use of wall functions is discussed in next chapter.

where suffixes have the same meaning as in the case of Eq. (3.93c).

3.6.3 Boundary conditions for temperature

These boundary conditions have to express the following physical constraints:

- (1) symmetry about the centerline
- (2) continuity of heat fluxes at all the external surfaces and at the slag-metal interface.
- (3) the electrode tip is at the liquidus temperature.

Again, with reference to Fig. 3.2, boundary conditions for the temperature equations can be written as follows:

- (1) at $r = 0$, $0 \leq z \leq Z_6$

$$\frac{\partial T}{\partial r} = 0 \quad (3.95)$$

- (2) at $z = 0$, $0 \leq r \leq R_e$ (upper boundary of electrode) and at $z = Z_6$, $0 \leq r \leq R_m$ (lower boundary of ingot)

$$\frac{\partial T}{\partial z} = 0 \quad (3.96)$$

- (3) at $r = R_e$, $0 \leq z \leq Z_1$ (surface of electrode above slag)

$$\begin{aligned}
 -K \left. \frac{\partial T}{\partial r} \right|_e &= h_c [T(R_e, z) - T_a] + \epsilon_e \delta [T(R_e, z)]^4 \\
 &\quad \text{I} \\
 &\quad - \epsilon_s F_{es}(z) T_{s,av}^4 - \epsilon_m F_{em} T_m^4] \quad (3.97) \\
 &\quad \text{II}
 \end{aligned}$$

where

- T_a is the temperature of the gas
 δ is the Stefan-Boltzmann constant
 $\epsilon_e, \epsilon_s, \epsilon_m$ are the emissivities of the dry electrode surface, the free surface of the slag and the inner surface of the mold respectively.
 T_m is the temperature of the inside surface of the mold above the slag
 $T_{s,av}$ is the average temperature of the free surface of the slag
 F_{es} is the view factor between the electrode element and the slag surface
 F_{em} is the view factor between the electrode element and the mold wall.

It is understood here that the temperatures are in the absolute scale. The first term in Eq. (3.97) represents the convective exchange between the electrode surface and the ambient gas whereas the second term represents

the radiative exchange between the electrode surface, the free slag surface and the inner surface of the mold. In order to facilitate the calculation of view factors, the slag surface is represented by a single temperature,

$T_{s,av}$ which is calculated from the following equation:

$$T_{s,av} = \frac{2 R_e \int_{R_e}^{R_m} T(r, z_1) r dr}{(R_m^2 - R_e^2)} \quad (3.98)$$

(4) at $z = z_1$, $R_e \leq r \leq R_m$ (free surface of slag)

$$K_{eff} \left. \frac{\partial T}{\partial z} \right|_{sl} = \delta \epsilon_s [T_{s,av}^4 - \epsilon_m F'_{sm} T_m^4 - \epsilon_e F'_{se} T_{e,av}^4] \quad (3.99)$$

where $T_{e,av}$ is the average temperature of the dry electrode

F'_{sm} is the view factor between the slag surface and the mold wall

and F'_{se} is the view factor between the free surface of the slag and the dry surface of the electrode.

As seen from Eq. (3.99), the convective heat loss from the slag surface to the ambient gas has been neglected. Also, in order to simplify calculations the slag surface and the electrode surface have been represented by their average temperatures.

View factors appearing in Eqns. (3.97) and (3.99) are calculated using the techniques discussed by Leunberger and Person⁵⁴. The calculation procedure is outlined in Appendix C.

(5) at $r = R_e$, $Z_1 \leq z \leq Z_2$ (vertical surface of electrode immersed in slag)

$$K \left. \frac{\partial T}{\partial r} \right|_e = K \left. \frac{\partial T}{\partial r} \right|_{sl}^* \quad (3.100)$$

(6) at $z = Z_2$, $0 \leq r \leq R_e$ (slag-electrode interface)

$$T = T_{m,e} \quad (3.101)$$

(7) at $z = Z_3$, $0 \leq r \leq R_m$ (slag-metal interface)

$$-K_{eff} \left. \frac{\partial T}{\partial z} \right|_{sl}^* + \frac{Q_s}{\pi R_e^2} \chi = -K_\ell \left. \frac{\partial T}{\partial z} \right|_\ell \quad (3.102)$$

where Q_s is defined by Eq. (3.76) and χ is defined by Eq. (3.34a,b); i.e. the heat extracted by droplets from the slag is given uniformly to the liquid metal over an area πR_e^2 .

* Alternate expressions for these fluxes can be given by wall function approach discussed in the next chapter.

$$(8) \quad \text{at } r = R_m, \quad z_1 \leq z \leq z_3 \quad (\text{slag-mold interface})$$

Since a solidified slag layer is assumed to exist at the inside wall of the mold, the temperature condition can be specified as $T = T_{\ell,s}$ (3.103a)

where $T_{\ell,s}$ is the melting temperature of the slag.

Alternatively one may write

$$-K \left. \frac{\partial T}{\partial r} \right|_{s\ell}^* = h_{W,s} (T - T_W) \quad (3.103b)$$

where $h_{W,s}$ is the overall heat transfer coefficient which describes the heat transfer from the molten slag/slag skin interface to the cooling water in the mold.

T_W is the average temperature of the cooling water.

$$(9) \quad \text{at } r = R_m, \quad z_3 \leq z \leq z_6$$

$$-K \left. \frac{\partial T}{\partial r} \right|_i = h_{W,i} (T - T_W) \quad (3.104)$$

where i stands for interfaces between various media (i.e. metal pool, mushy zone, solid ingot) and the mold.

$h_{W,i}$ represents overall heat transfer coefficient at these interfaces.

* Alternate expressions for these fluxes can be given by wall function approach discussed in the next chapter.

3.7 General Nature of Solutions

The mathematical statement of the model is now complete. Before presenting the detailed results, it is worthwhile to discuss the general nature of solutions. The governing equations (in vectorial form) for the system are grouped together in Table 3.1.

3.7.1 The nature of stirring

Using Eqns. (3.10), (3.2) and (3.6), the electromagnetic body force \vec{F}_{be} can be written as follows:

$$\begin{aligned}\vec{F}_{be} &= \vec{J} \times \vec{B} = \frac{1}{\mu_0} (\vec{\nabla} \times \vec{B}) \times \vec{B} \\ &= -\vec{\nabla} \left(\frac{1}{2\mu_0} B^2 \right) + \frac{1}{\mu_0} (\vec{B} \cdot \vec{\nabla}) \vec{B}\end{aligned}\quad (3.105)$$

Upon operating with $\vec{\nabla} \times$ (i.e. curl) on the r.h.s. of Eq. (3.105), the first term vanishes. i.e.

$$\vec{\nabla} \times \left[-\vec{\nabla} \left(\frac{1}{2\mu_0} B^2 \right) \right] = 0 \quad (3.106)$$

while in general,

$$\vec{\nabla} \times \left[\frac{1}{\mu_0} (\vec{B} \cdot \vec{\nabla}) \vec{B} \right] \neq 0 \quad (3.107)$$

It follows therefore that the term I (called the magnetic pressure), cannot do any work on a circulating fluid and that the second term (II) is responsible for doing work.

Table 3.1 Governing equations for fluid flow and heat transfer in the ESR process

1. Maxwell's equations

$$\begin{aligned}
 \nabla \times \vec{E} &= - \frac{\partial \vec{B}}{\partial t} & \frac{\partial \vec{H}}{\partial t} &= \eta \nabla^2 \vec{H} \\
 \nabla \times \vec{H} &= \vec{J} & \text{OR} & \\
 \nabla \cdot \vec{B} &= 0 & \nabla \cdot \vec{J} &= 0 \\
 \nabla \cdot \vec{J} &= 0
 \end{aligned}$$

Constitutive equation

$$\vec{B} = \mu_0 \vec{H}$$

Ohm's law

$$\vec{J} \cong \sigma \vec{E}$$

2. Equations for fluid flow (in slag)

Equation of continuity

$$\nabla \cdot \vec{V} = 0$$

Equation of motion

$$\rho (\vec{V} \cdot \nabla) \vec{V} = -\nabla \bar{p} - \nabla \cdot \bar{\tau} + \left[\frac{1}{2} \text{Re} (\hat{J} \times \bar{B}) - \rho (1 - \beta (\bar{T} - T_0)) \underline{g} \right]$$

Transport equation for k and ϵ

$$\rho (\vec{V} \cdot \nabla) \phi = \nabla \cdot \left(\frac{\mu_{\text{eff}}}{\sigma_{\phi}} \nabla \phi \right) + S_{\phi}$$

where $\phi = k$ or ϵ

3. Thermal energy equations

Heat transfer in slag

$$\rho_p C_p (\vec{V} \cdot \nabla \bar{T}) = \nabla \cdot K_{\text{eff}} \nabla \bar{T} + \frac{1}{2\sigma} \text{Re}(\hat{J} \cdot \bar{J}) - Q_d \chi$$

Heat transfer in other portions of ESR

$$\rho_i C_{p_i} (V_i \cdot \nabla T) = \nabla \cdot K_i \nabla T + S_{T,i}$$

where $i = e$ (electrode), l (metal pool),

m (mushy zone), s (solid ingot)

and V_i accounts for movement of various interfaces.

The inertial force in the equation of motion [Eq. (3.18)] can be written as

$$\rho (\bar{\nabla} \cdot \bar{\nabla}) \bar{\nabla} = \rho \left[(\bar{\nabla} \times \bar{\nabla}) \times \bar{\nabla} \right] + \rho \bar{\nabla} \left(\frac{\bar{\nabla}^2}{2} \right) \quad (3.108)$$

Introducing the definition of vorticity,

$$\xi = \bar{\nabla} \times \bar{\nabla} \quad (3.109)$$

we can rewrite Eq. (3.108) as follows:

$$\rho (\xi \times \bar{\nabla}) = -\rho \bar{\nabla} \left(\frac{\bar{\nabla}^2}{2} \right) + \rho (\bar{\nabla} \cdot \bar{\nabla}) \bar{\nabla} \quad (3.110)$$

vortex force

From Eqs. (3.105) and (3.110), the analogy between F_{be} and the vortex force is evident.

3.7.2 Relationship between velocity and current

Let us assume that the buoyancy driving force is small compared to the electromagnetic driving force (i.e. we operate with high current and with a small fill ratio) then Eqs. (3.18) and (3.19) can be combined to give:

$$\rho (\bar{\nabla} \cdot \bar{\nabla}) \bar{\nabla} = -\bar{\nabla} \bar{P}_t - \bar{\nabla} \cdot \bar{\tau} + \bar{J} \times \bar{B} \quad (3.111)$$

where \bar{P}_t represents the sum of static pressure and gravitational force. If the inertial forces dominate (i.e. at high Reynolds number) then as a first approximation we may neglect the first two terms on the r.h.s. of Eq.(3.111). The order of magnitude of the remaining terms are:

$$O \left[\rho (\bar{V} \cdot \nabla) \bar{V} \right] \approx \frac{\rho V_0^2}{L}$$

$$O \left[\underline{J} \times \underline{B} \right] \approx J_0 \times \mu_0 J_0 L \quad (3.112a,b)$$

where J_0 is a characteristic current density of the system.

From Eqs. (3.112a) and (3.112b) we can write

$$\frac{\rho V_0^2}{L} \sim \mu_0 J_0^2 L \quad (3.113)$$

i.e.

$$V_0 \sim J_0 \sqrt{\frac{\mu_0}{\rho}} L$$

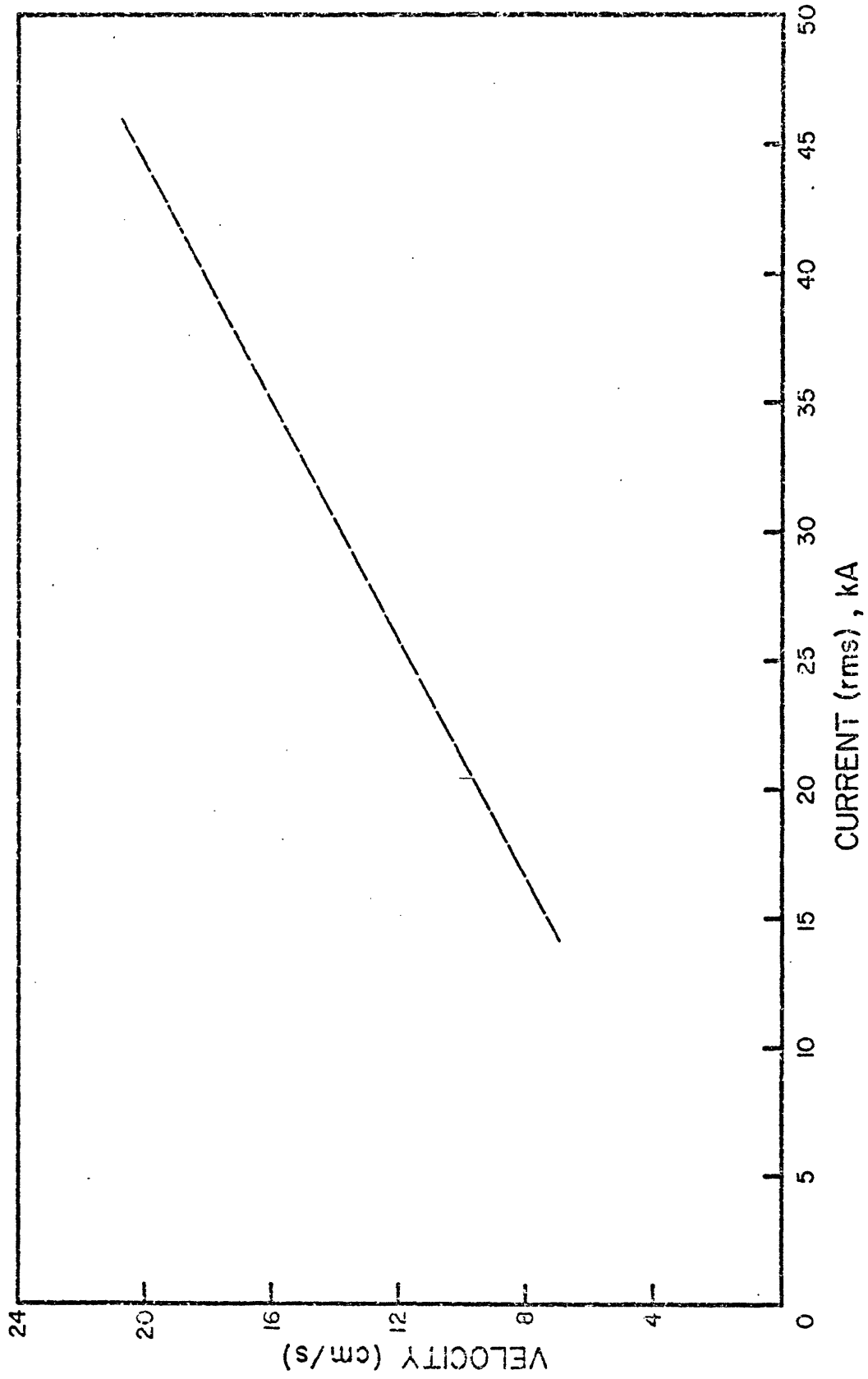
which indicates that the characteristic velocity is proportional to the current. Figure 3.3, taken from Dilawari and Szekely¹⁵ shows the effect of current on the velocity in the slag phase. As seen here, under the isothermal conditions (i.e. in the absence of buoyancy driving forces) the relationship between the velocity and the current is linear.

3.7.3 Heat input vs. energy for stirring

From dimensional arguments it may be shown that:

$$\frac{\text{energy input for stirring}}{\text{energy input for heating}} \approx O \left[\frac{(\underline{J} \times \underline{B}) \cdot \underline{V}}{J^2 / \sigma} \right] \quad (3.115a)$$

$$\approx O \left[\frac{J_0^2 \mu_0 L V_0 \sigma}{J_0^2} \right] \quad (3.115b)$$



3.3 The effect of current on the maximum value of the linear velocity in the slag (from Dilawari and Szekely¹⁵).

$$\sim \left(\frac{\mu_0^3}{\rho} \right)^{1/2} L^2 \sigma J_0 \quad (3.115c)^*$$

For illustrative purposes, let us assume $L = 0.5 \text{ m}$,
 $\sigma = 250 \text{ (ohm-m)}^{-1}$, $\rho = 3.0 \times 10^3 \text{ kg/m}^3$, $J_0 = 40 \text{ kA/m}^2$

$$\begin{aligned} \left(\frac{\mu_0^3}{\rho} \right)^{1/2} L^2 \sigma J_0 &= \left[\frac{(1.25 \times 10^{-6})^3}{3 \times 10^3} \right]^{1/2} \times 250 \times 250 \times 4 \times 10^4 \\ &= 6.5 \times 10^{-5} \ll 1 \end{aligned}$$

3.7.4 Dimensionless form of governing equations

Let us now make the vector form of the governing equations dimensionless. This will generate parameters characterizing the behavior of the system.

3.7.4A Dimensionless form of magnetic field equation

Let us introduce the following dimensionless variables:

$$\begin{aligned} \tilde{\nabla}^* &= L \tilde{\nabla} & \hat{\tilde{H}}^* &= \hat{\tilde{H}}/H_0 \\ H_0 &= I_0/L & J_0 &= I_0/L^2 \end{aligned} \quad (3.116)$$

then the magnetic field equation (Eq. (3.9)) can be written, in the phasor notation, as:

$$j\alpha \hat{\tilde{H}}^* = \tilde{\nabla}^{*2} \hat{\tilde{H}}^* \quad (3.117)$$

where

* Using eq. (3.114)

$$\begin{aligned}
\alpha &= \omega \sigma \mu_0 L^2 \\
&= \frac{L^2 \sigma \mu_0}{(1/\omega)} \\
&= \frac{\text{characteristic time for magnetic diffusion}}{\text{characteristic period for electric current}}
\end{aligned}
\tag{3.118}$$

3.7.4B Dimensionless form of flow equations

In addition to dimensionless variables already defined in Eq. (3.116) let us introduce

$$\begin{aligned}
V^* &= \bar{V}/V_0 & P^* &= (\bar{P} - P_0)/\rho V_0^2 \\
k^* &= k/V_0^2 & \epsilon^* &= \epsilon L/V_0^3 \\
T^* &= (\bar{T} - T_{\ell,s})/(T_{\ell,m} - T_{\ell,s}) \\
J^* &= \bar{J}L/H_0
\end{aligned}
\tag{3.119}$$

then the equation of motion (Eq. (3.18)) can be written as

$$(\bar{V}^* \cdot \bar{\nabla}^*) \bar{V}^* = -\bar{\nabla}^* P^* - \bar{\nabla}^* \tau^* + \left[N_1 \frac{1}{2} \text{Re}(\hat{J}^* \times \hat{B}^*) + \{N_2 - N_3 (T^* - \gamma)\} \frac{g}{g} \right]
\tag{3.120}$$

where

$$\tau^* = \tau/\rho V_0^2 = (\text{viscous} + \text{Reynolds force})/(\text{inertial force})
\tag{3.121}$$

$$N_1 = \mu_0 H_0^2 / \rho V_0^2 = (\text{Lorentz force}) / (\text{inertial force}) \quad (3.122)$$

$$N_2 = gL / V_0^2 = (\text{Gravitational force}) / (\text{inertial force}) \quad (3.123)$$

$$N_3 = \beta g (T_{\ell, m} - T_{\ell, s}) L / V_0^2 \quad (3.124)$$

$$= (\text{Buoyancy force}) / (\text{inertial force})$$

$$\gamma = \frac{T_0 - T_{\ell, s}}{T_{\ell, m} - T_{\ell, s}} \quad (3.125)$$

similarly, the transport equations for k and ϵ [Eqs. (3.21a,b)] can be written as

$$\tilde{V}^* \cdot \tilde{\nabla}^* k^* = \frac{1}{\text{Re}_f} \tilde{\nabla}^* \cdot \left(\frac{\mu_{\text{eff}}^*}{\sigma_k} \tilde{\nabla}^* k^* \right) + S_k^* \quad (3.126)$$

where $\text{Re}_f = \frac{\rho V_0 L}{\mu}$ (Reynolds no.)

$$\mu_{\text{eff}}^* = \frac{\mu_t}{\mu} + 1 = \frac{\text{Effective viscosity}}{\text{Molecular viscosity}}$$

$$S_k^* = S_k L / \rho V_0^3 \quad (3.127a, b, c)$$

and

$$\tilde{V}^* \cdot \tilde{\nabla}^* \epsilon^* = \frac{1}{\text{Re}_f} \tilde{\nabla}^* \cdot \left(\frac{\mu_{\text{eff}}^*}{\sigma_\epsilon} \tilde{\nabla}^* \epsilon^* \right) + S_\epsilon^* \quad (3.128)$$

where $S_\epsilon^* = S_\epsilon L^2 / \rho V_0^4$ (3.129)

3.7.4C Dimensionless form of the heat transfer equation

Using dimensionless variables defined in Eqs. (3.116) and (3.119), the convective heat transfer equation for slag [Eq. (3.32)] can be written as,

$$\begin{aligned}
 (\tilde{V}^* \cdot \tilde{\nabla}^* T^*) &= \frac{1}{Pe} \tilde{\nabla}^* \cdot K_{eff}^* \tilde{\nabla}^* T^* + N_T \left[\frac{1}{2} \operatorname{Re}(\hat{J}^* \cdot \bar{J}^*) \right. \\
 &\quad \left. - Q_d \chi \sigma / J_0^2 \right] \quad (3.130)
 \end{aligned}$$

where

$$\begin{aligned}
 K_{eff}^* &= \frac{K_t}{K} + 1 = \frac{\text{Effective thermal conductivity}}{\text{Molecular thermal conductivity}} \\
 &= \operatorname{Pr} \frac{\mu_t}{\mu} + 1 \\
 &= \operatorname{Pr} (\mu_{eff}^* - 1) + 1 \quad (3.131)
 \end{aligned}$$

where $\operatorname{Pr} = \frac{C_p \mu}{K} = \text{Prandtl no.}$

$$\begin{aligned}
 N_T &= \frac{J_0^2 / \sigma}{\rho C_p V_0 (T_{l,m} - T_{l,s}) / L} \\
 &= \frac{\text{Heat generation by Joule effect}}{\text{Heat transport by convection}} \quad (3.132)
 \end{aligned}$$

$$\begin{aligned}
 Pe &= \frac{\rho C_p V_0 L}{K} = \text{Peclet no.} = \operatorname{Re}_f \operatorname{Pr} \\
 &= \frac{\text{Heat transport by convection}}{\text{Heat transport by conduction}}
 \end{aligned}$$

By using the approach outlined here on Eq. (3.38), we can similarly define Peclet numbers for other portions of ESR. For example, below the slag-metal interface, we can define

$$Pe_{\ell} = \frac{\rho_{\ell} C_{p,\ell} V_{c,0} L}{K_{\ell}} \quad (3.133)$$

where

$V_{c,0}$ is a reference casting rate

and

K_{ℓ} is effective thermal conductivity in metal pool.

Similarly, a group of other dimensionless parameters can be derived by considering the boundary conditions (e.g. Biot number at the ingot-mold interface).

The dimensionless parameters developed here and their physical interpretations are summarized in Table 3.2.

3.8 Concluding Remarks

A mathematical model has been formulated to describe the current distribution, fluid flow and heat transfer phenomena in the electroslag refining process. The model involves simultaneous statement of Maxwell's equations, equations for turbulent motion and convective heat transfer equations. The limitations of the model, in the form of assumptions made, are listed in section 3.3. On the positive side, the model accounts for some of the features of the ESR process which are considered

Table 3.2 Dimensionless parameters deduced from the governing equations

σ	$\omega \sigma \mu_0 L^2$	<u>characteristic time for magnetic diffusion</u> <u>characteristic period for electric current</u>
N_1	$\mu_0 H_0^2 / \rho V_0^2$	Lorentz force/Inertial force
N_2	$g L / V_0^2$	Gravitational force/Inertial force
N_3	$\beta g \Delta T L / V_0^2$	Buoyancy force/Inertial force
Re_f	$\rho V_0 L / \mu$	Inertial force/Viscous force = Reynolds Number
N_T	$\frac{J_0^2 / \sigma}{\rho C_p V_0 \Delta T / L}$	<u>Heat generation rate due to Joule effect</u> <u>Heat transport rate by convection</u>
Pr	$C_p \mu / K$	Momentum diffusivity/Thermal diffusivity = Prandtl number
Pe	$\rho C_p V_0 L / K$	Heat Transport by convection/Heat transport by conduction = Peclet number
Pe_i	$\frac{\rho_i C_{p,i} V_{c,i} L}{K_i}$	Heat Transport due to movement of interface/ Heat Transport by conduction

crucial from the point of view of flow and heat transfer in the system. Thus, allowance has been made for both electromagnetic and buoyancy driving forces, for the spatial distribution of Joule heat release, for heat transport by metal droplets and for the release of latent heat in the mushy zone, etc.

Boundary conditions for the governing differential equations have been stated in section 3.6. Finally, brief discussions have been given on the general nature of the solution and the dimensionless parameters for the system.

Nomenclature

B \sim	Magnetic flux density
C_1, C_2	Constants in $k - \epsilon$ model
C_d	Dissipation rate constant
$C_p, C_{p,e}, C_{p,\ell}$ $C_{p,m}, C_{p,s}, C_{p,d}$	Specific heat of slag, electrode, molten metal, mushy zone, solid ingot and metal droplet
C_D	Drag coefficient
d_d	Diameter of a droplet
D	Dissipation term for turbulence kinetic energy
E \sim	Electric field
f_s	Fraction of solids in the mushy zone
F_b \sim	Body force (per unit volume) vector
F_{be} \sim	Electromagnetic (Lorentz) body force vector
F_r, F_z	Radial and axial components of body force
F_{es}, F_{em}	Radiation view factors between the electrode element and slag,

Nomenclature (cont'd)

	electrode element and mold
F'_{sm}, F'_{se}	Radiation view factors between the slag surface and the mold, slag surface and the dry surface of electrode
g	Acceleration due to gravity
G	Generation term for turbulence kinetic energy
h	Heat transfer coefficient between the slag and a droplet
$h_{W,s}$	Overall heat transfer coefficient at the slag - mold interface
$h_{W,i}$	Overall heat transfer coefficients for the regions defined in equation (3.104)
$\tilde{H}, H_{\theta}, \hat{H}_{\theta}, H_0$	Magnetic field intensity, its component in the θ -direction, complex amplitude of H_{θ} , reference value
I_0	Amplitude of total current, also reference value for current

Nomenclature (cont'd)

j	$\sqrt{-1}$
$\tilde{J}, J_r, J_z, \hat{J}_r, \hat{J}_z$	Current density components in r- and z- direction and their complex amplitudes
\bar{J}	Complex conjugate of \hat{J}
J_0	Reference current density
k	Kinetic energy (per unit mass) of turbulence
K, K_e, K_ℓ, K_m, K_s	Thermal conductivity of slag, electrode, molten metal (effective value), mushy zone and ingot
$K_{m\ell}$	Thermal conductivity (atomic) of molten metal
K_{eff}	Effective thermal conductivity (sum of molecular and turbulent contributions) in slag
K_t	Turbulent thermal conductivity in slag
L_1, L	Depth of slag below the electrode, characteristic length scale

Nomenclature (cont'd)

n	Normal vector
N_1	Ratio of (Lorentz force/ inertial force) Eq. (3.122)
N_2	Ratio of (Gravity force/ inertial force) Eq. (3.123)
N_T	Heat generation rate / Heat transport by convection, Eq. (3.132)
\bar{P}, P_0	Time - smoothed pressure, its reference value
Pe	Peclet no. for slag
Pe_ℓ	Peclet no. for metal pool
P_d	A physical property group for droplets
Pr	Prandtl no. for slag
Q_j	Rate of Joule heating (per unit volume)
Q_d	Rate of heat extraction (per unit volume) from slag by metal droplets

Nomenclature (cont'd)

Q_s	Rate of heat extraction from slag by metal droplets
r	Radial coordinate
r_d	Radius of a metal droplet
R_e	Radius of the electrode
R_m	Radius of the mold
Re_m	Magnetic Reynolds number
Re_f	Reynolds number for flow
Re_d	Droplet Reynolds number
S_T	Source term for temperature equation
S_k, S_ϵ	Source terms for k, ϵ
t	Time
\bar{T}, T	Temperature in the slag (time smoothed), elsewhere
T_a	Temperature of gas above the slag surface
T_B	Bulk temperature of the slag in the region $0 \leq r \leq R_e$

Nomenclature (cont'd)

T_f	Final temperature attained by a droplet
T_d	Temperature of a droplet
$T_{l,m}$	Liquidus temperature of the metal
$T_{l,s}$	Melting temperature of the slag
$T_{m,e}$	Melting temperature of electrode
$T_{s,m}$	Solidus temperature of the metal
T_W	Temperature of the cooling water
$T_{s,av}$	Average temperature of the slag surface
$T_{e,av}$	Average temperature of the dry electrode surface
U	Velocity of a metal droplet
U_{av}	Average velocity of a droplet
U_t	Terminal velocity of a droplet
$V_c, V_{c,0}$	Casting rate, its reference value
V_t	Rate of travel of electrode
\bar{V}, V_0	Time-smoothed velocity vector, its reference value

Nomenclature (cont'd)

\bar{V}_r, \bar{V}_z	Radial and axial components of velocity vector
W	Input power
We	Weber no.
X	Variable defined in Eq. (3.67)
Y	Variable defined in Eq. (3.66)
z	Axial coordinate
Z_1, Z_2, Z_3, Z_6	Position of free slag surface, melting tip of electrode, slag-metal interface, lower boundary of ingot
GREEK SYMBOLS	
α	Characteristic time for magnetic diffusion / Characteristic period for electric current
β	Coefficient of thermal expansion of slag
γ	Interfacial tension between liquid metal and liquid slag
δ	Stefan - Boltzmann constant

GREEK SYMBOLS

ε	Dissipation rate of turbulence energy
$\varepsilon_e, \varepsilon_s, \varepsilon_m$	Emissivity of electrode, slag, mold
ξ	θ - component of the vorticity vector
η	Magnetic diffusivity
λ	Latent heat of fusion of metal
Λ	Defined by Eq. (3.44)
μ	Viscosity of slag
μ_0	Magnetic permeability of free space
μ_{eff}	Effective viscosity of slag
ψ	Stream function
$\rho, \rho_e, \rho_l, \rho_m, \rho_s, \rho_d$	Density of slag, electrode, metal pool, mushy zone, solid ingot and droplet
$\sigma, \sigma_e, \sigma_m$	Electrical conductivity of slag, electrode and metal

Nomenclature (cont'd)

GREEK SYMBOLS

$\sigma_k, \sigma_\epsilon$	Prandtl number for k, ϵ
σ_t	Turbulence Prandtl number
$\bar{\tau}$	Sum of viscous and Reynolds stresses
τ	Residence time of a droplet
ω	Angular frequency of current
χ	Defined by Eqs. (3.34a,b)

Superscript

*	Dimensionless quantities
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CHAPTER IV

NUMERICAL SOLUTION OF GOVERNING EQUATIONS

This chapter presents an outline of the numerical technique used for solving the differential equations developed in the previous chapter. After discussing the derivation of finite difference equations for the dependent variables, a brief treatment on the use of wall functions for representing heat and momentum transfer in the near wall regions is presented. The computational scheme and the computer program are discussed at the end of the chapter.

4.1 Summary of Governing Equations and Boundary Conditions

4.1.1 Equations for magnetic field

Let $\hat{H}_{\theta R}$ and $\hat{H}_{\theta I}$ denote the real and imaginary parts of \hat{H}_{θ} respectively, then Eq. (3.13) can be decomposed to give:

$$\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r \hat{H}_{\theta R}) \right) + \frac{\partial^2 \hat{H}_{\theta R}}{\partial z^2} = - \sigma \mu_0 \omega \hat{H}_{\theta I} \quad (4.1)$$

and

$$\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r} (r \hat{H}_{\theta I}) \right) + \frac{\partial^2 \hat{H}_{\theta I}}{\partial z^2} = \sigma \mu_0 \omega \hat{H}_{\theta R} \quad (4.2)$$

It should be noted that,

$$|\hat{H}_{\theta}| = \left(\hat{H}_{\theta R}^2 + \hat{H}_{\theta I}^2 \right)^{1/2}$$

and that the phase angle

$$\beta_H = \tan^{-1} \left(\frac{\hat{H}_{\theta I}}{\hat{H}_{\theta R}} \right) \quad (4.3a,b)$$

Similarly from Eq. (3.14a,b) one can write;

$$\begin{aligned} \hat{J}_{rR} &= \text{Re}(\hat{J}_r) = - \frac{\partial \hat{H}_{\theta R}}{\partial z} \\ \hat{J}_{rI} &= \text{Im}(\hat{J}_r) = - \frac{\partial \hat{H}_{\theta I}}{\partial z} \\ |\hat{J}_r| &= \left(\hat{J}_{zR}^2 + \hat{J}_{zI}^2 \right)^{1/2} \end{aligned} \quad (4.4a,b,c)$$

and

$$\begin{aligned} \hat{J}_{zR} &= \text{Re}(\hat{J}_z) = \frac{1}{r} \frac{\partial}{\partial r} (r \hat{H}_{\theta R}) \\ \hat{J}_{zI} &= \text{Im}(\hat{J}_z) = \frac{1}{r} \frac{\partial}{\partial r} (r \hat{H}_{\theta I}) \\ |\hat{J}_z| &= \left(\hat{J}_{zR}^2 + \hat{J}_{zI}^2 \right)^{1/2} \end{aligned} \quad (4.5a,b,c)$$

4.1.2 Equations for fluid flow and heat transfer

Eqs. (3.24) , (3.27) , (3.30) , (3.37) , (3.39a,b,c,d) constitute the mathematical statement of the fluid flow and heat transfer phenomena in the system. These equations can be represented by the following general elliptic partial differential equation:

$$a_{1\phi} r \frac{\partial \phi}{\partial z} + a_{\phi} \left(\frac{\partial}{\partial z} \left(\phi \frac{\partial \psi}{\partial r} \right) - \frac{\partial}{\partial r} \left(\phi \frac{\partial \psi}{\partial z} \right) \right) - \frac{\partial}{\partial z} \left(b_{\phi} r \frac{\partial (c_{\phi} \phi)}{\partial z} \right) -$$

$$\frac{\partial}{\partial r} \left(b_{\phi} r \frac{\partial (c_{\phi} \phi)}{\partial r} \right) - r S_{\phi} = 0 \quad (4.6)$$

where ϕ stands for the dependent variables $(\frac{\xi}{r}, \psi, k, \epsilon, T)$. Values of the coefficients $a_{1\phi}, a_{\phi}, b_{\phi}, c_{\phi}$ and the source term S_{ϕ} are listed in table 4.1.

4.1.3 Boundary conditions

Boundary conditions for the magnetic field intensity, \hat{H}_{θ} are stated in Fig. 4.1. Boundary conditions for fluid flow variables (i.e. $\frac{\xi}{r}, \psi, k$ and ϵ) are summarized in Fig. 4.2 and finally, boundary conditions for temperature are given in Fig. 4.3. In these figures the symbols $e, s, \ell, m,$ s stand for electrode, slag, metal pool, mushy zone, and solid ingot respectively.

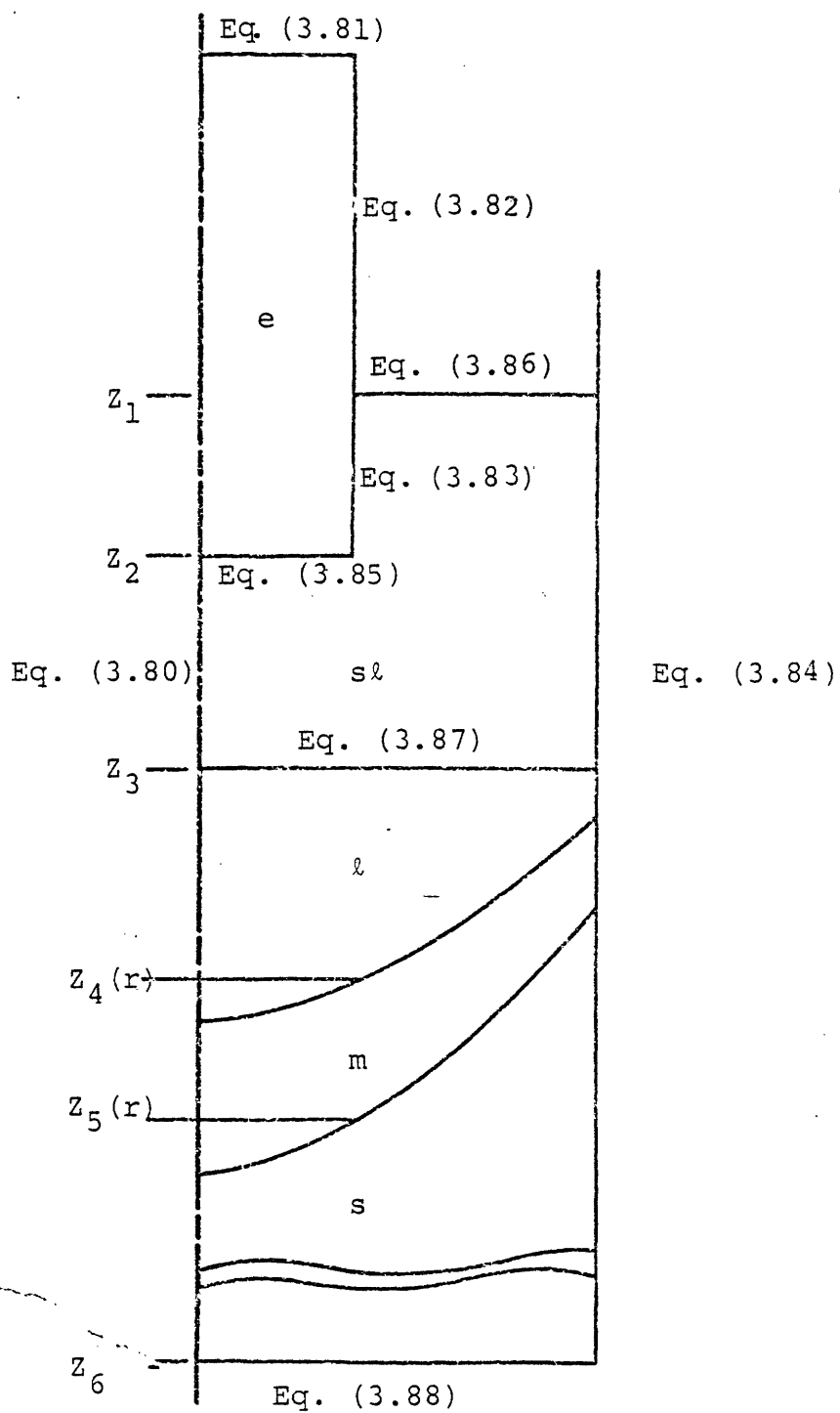
4.2 Derivation of the Finite - Difference Equations

In this section, transformation of differential equations listed in section 4.1 to finite - difference forms is presented. This transformation involves the following steps:

- 1) The domain of integration is represented by a two dimensional (r, z) array of points called a grid.
- 2) A set of algebraic equations is derived, from the differential equations and the boundary conditions, which connect the values of the dependent variables at the grid nodes (points of intersection of grid lines)

Table 4.1 Summary of governing differential equations in cylindrical coordinate system

ϕ	$a_{1\phi}$	a_{ϕ}	b_{ϕ}	c_{ϕ}	S_{ϕ}
$\frac{\xi}{r}$	0	r^2	r^2	μ_{eff}	$\mu_0 \text{Re}(\hat{H}_{\theta} \hat{J}_r) + r\rho\beta g \left(\frac{\partial T}{\partial r}\right)$
ψ	0	0	$\frac{1}{\rho r^2}$	1	$\frac{\xi}{r}$
k	0	1	$\mu_{\text{eff}}/\sigma k$	1	$S_k [\text{Eqs}(3 \cdot 28) \cdot (3 \cdot 29a \cdot b)]$
ϵ	0	1	$\mu_{\text{eff}}/\sigma \epsilon$	1	$S_{\epsilon} [\text{Eqs}(3 \cdot 29a) \cdot (3 \cdot 31)]$
T	$\rho C_p V_c$	c_p	K_{eff}	1	$Q_j - Q_d X$
	$\rho C_{p,e} V_e$	0	K_e	1	0
	$\rho C_{p,\ell} V_{\ell}$	0	K_{ℓ}	1	0
	$\rho C_{p,m} V_m$	0	K_m	1	$-V_c \rho C_m \lambda (T_{\ell,m} - T_{s,m}) \frac{\partial T}{\partial z}$
	$\rho C_{p,s} V_{s,c}$	0	K_s	1	0



4.1 Boundary conditions for the magnetic field intensity.

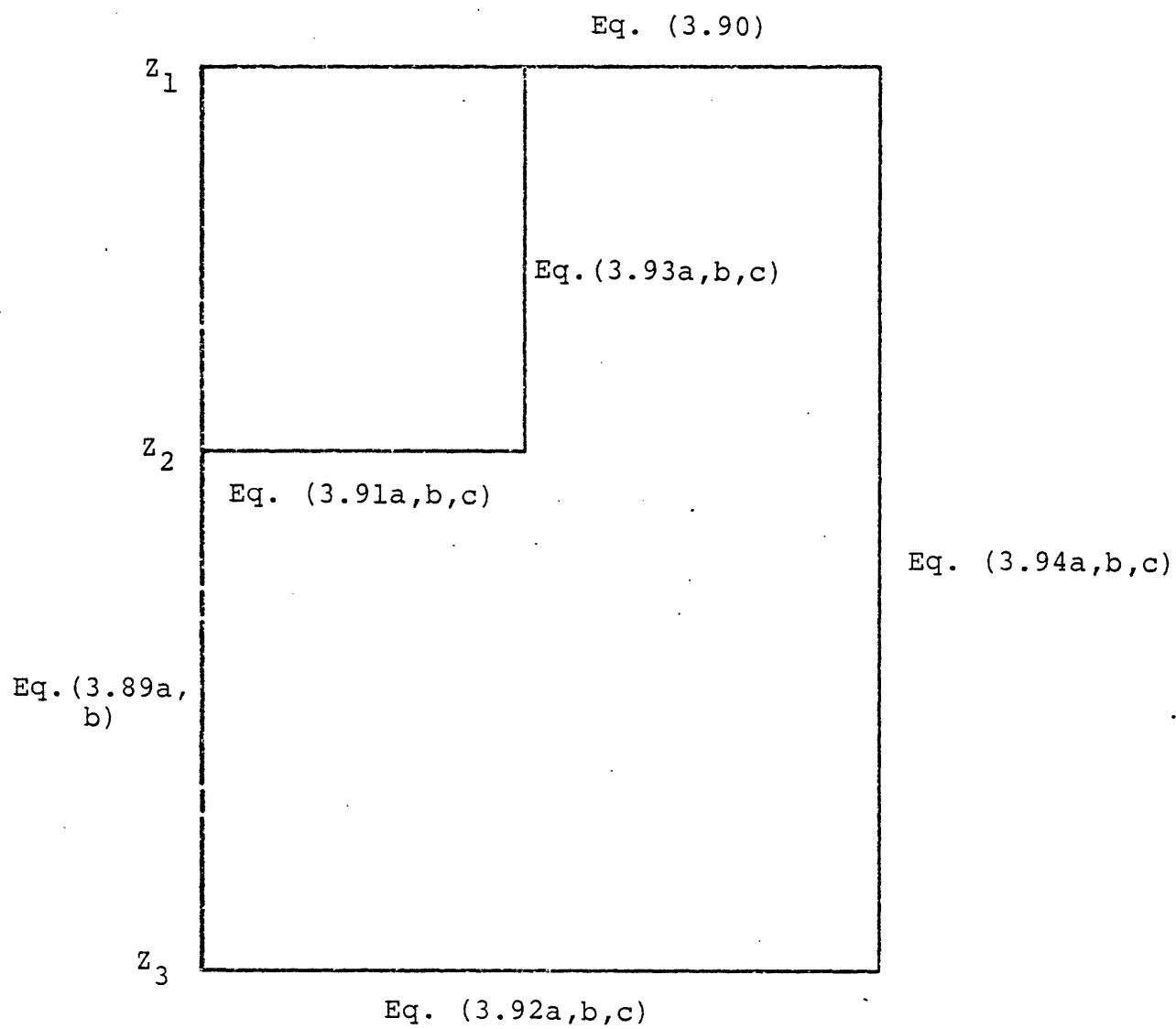


Fig. 4.2 Boundary conditions for fluid flow variables.

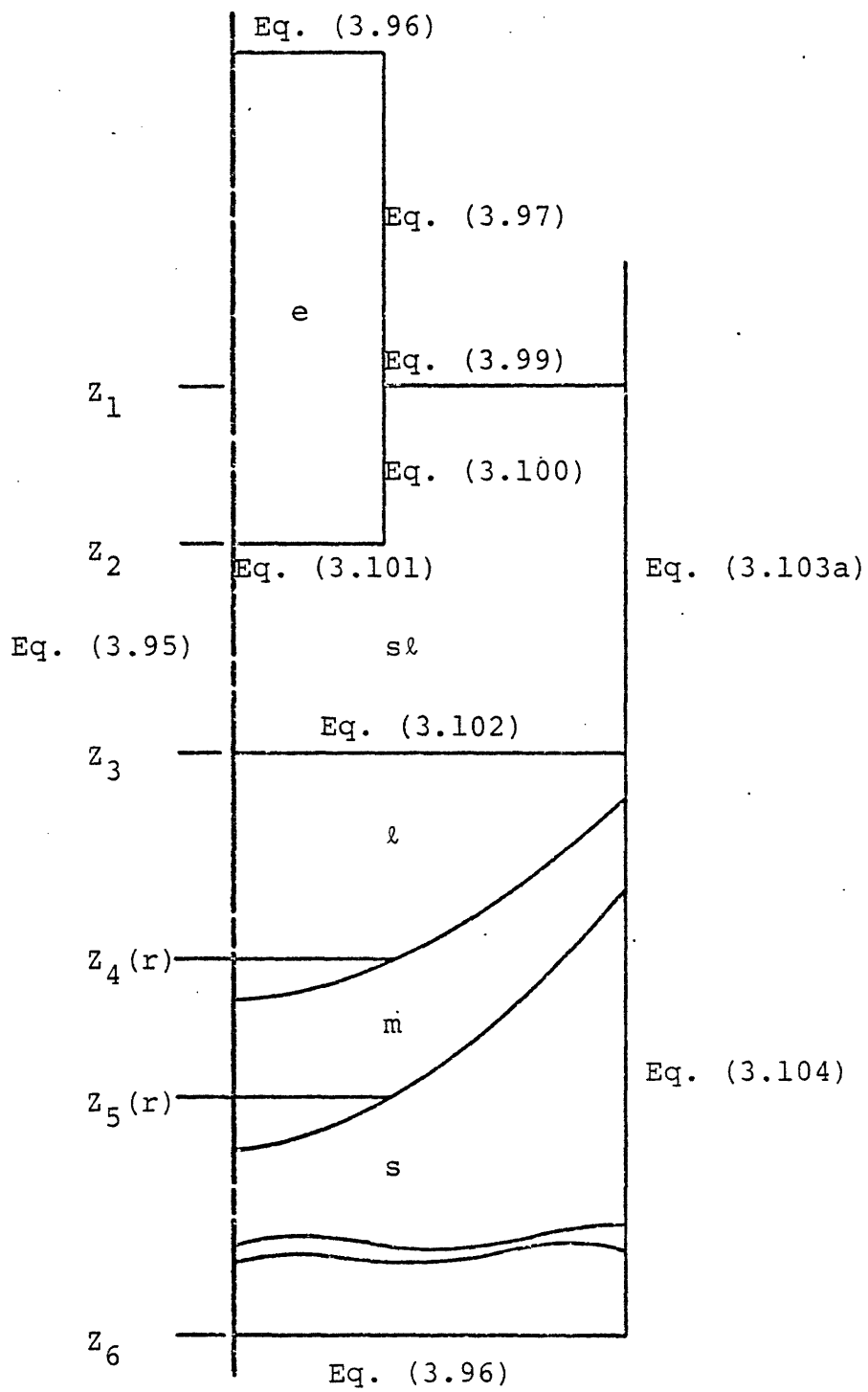


Fig. 4.3 Boundary conditions for temperature.

with each other and with other quantities.

4.2.1 Expressions for interior nodes

Fig. 4.4 shows a part of the orthogonal grid; with a typical node P and the surrounding nodes E, NE, N, NW, W, SW, SE. The neighboring nodes need not be equally spaced. The finite-difference equations are derived by using the technique described by Gosman et al ³⁹. A brief outline of this technique is presented with respect to the general elliptic equation [Eq. (4.6)]. The derivation of finite difference equations for the magnetic field intensity $(\hat{H}_{\theta R}, \hat{H}_{\theta I})$ is analogous and only the final results will be given.

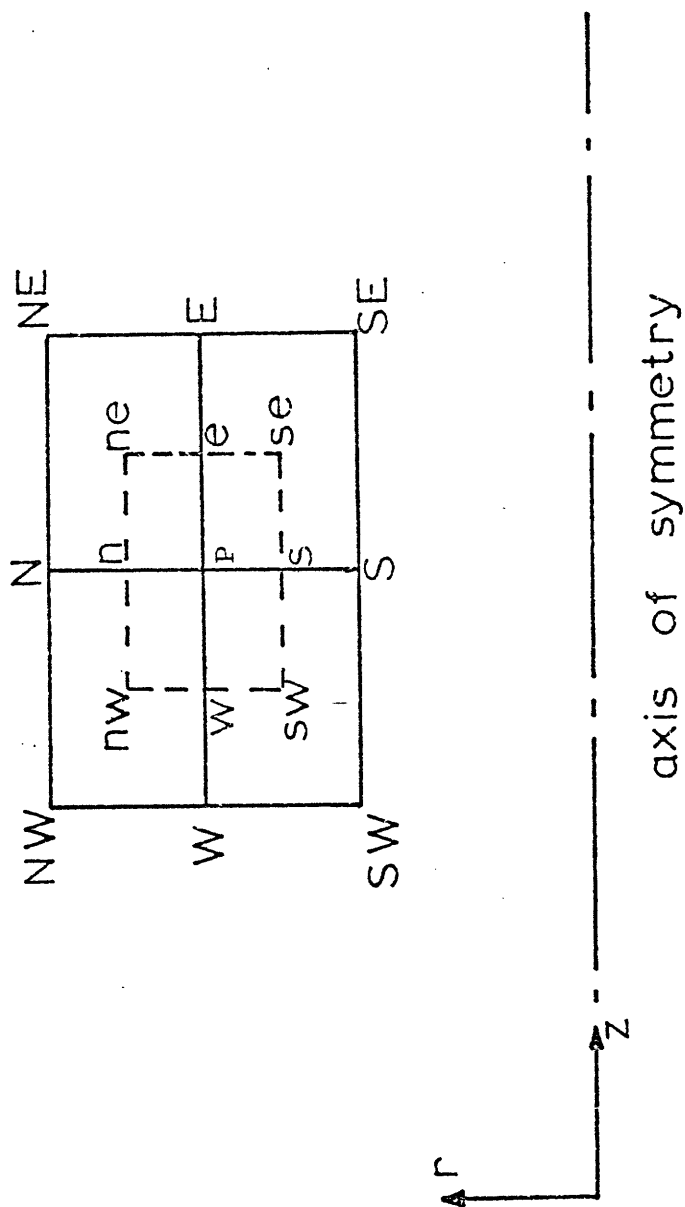
Let us proceed by integrating Eq. (4.6) over the area enclosed by the small rectangle, shown by the dotted lines in Fig. 4.4, which encloses the point P. The sides of this rectangle lie midway between the neighbouring grid lines. The double integral to be evaluated is

$$\int_{r_s}^{r_n} \int_{z_w}^{z_e} \left[a_{1\phi} r \frac{\partial \phi}{\partial z} + a_{\phi} \left(\frac{\partial}{\partial z} \left(\phi \frac{\partial \psi}{\partial r} \right) - \frac{\partial}{\partial r} \left(\phi \frac{\partial \psi}{\partial z} \right) \right) \right] dr dz$$

—————convection terms—————/

$$- \int_{r_s}^{r_n} \int_{z_w}^{z_e} \left[\frac{\partial}{\partial z} \left(b_{\phi} r \frac{\partial (c_{\phi} \phi)}{\partial z} \right) + \frac{\partial}{\partial r} \left(b_{\phi} r \frac{\partial (c_{\phi} \phi)}{\partial r} \right) \right] dr dz$$

—————diffusion terms—————/



4.4 A portion of the finite-difference grid.

$$- \int_{r_s}^{r_n} \int_{z_w}^{z_e} r S_\phi dr dz = 0 \quad (4.7)$$

——source term——

Following the details given by Gosman et al ³⁹ and after some algebraic manipulation, we obtain the following successive substitution formula for ϕ which is valid for any interior point P in the integration field:

$$\phi_P = \frac{\sum_{j=N,S,E,W} \left\{ \left[A_j' + c_{\phi,j} (b_{\phi,j} + b_{\phi,P}) B_j' \right] \phi_j \right\} + S_{\phi,P}}{\sum_{j=N,S,E,W} \left\{ A_j' + c_{\phi,P} (b_{\phi,j} + b_{\phi,P}) B_j' \right\}} \quad (4.8)$$

where

$$A_j' = (A_j + A_{1j}) / V_P \quad (4.9)$$

$$B_j' = B_j / \{ V_P (b_{\phi,j} + b_{\phi,P}) \} \quad (4.10)$$

with

$$\begin{aligned} A_E &= \frac{a_{\phi,P}}{8} \left[(\psi_{SE} + \psi_S - \psi_{NE} - \psi_N) + |\psi_{SE} + \psi_S - \psi_{NE} - \psi_N| \right] \\ A_W &= \frac{a_{\phi,P}}{8} \left[(\psi_{NW} + \psi_N - \psi_{SW} - \psi_S) + |\psi_{NW} + \psi_N - \psi_{SW} - \psi_S| \right] \\ A_N &= \frac{a_{\phi,P}}{8} \left[(\psi_{NE} + \psi_E - \psi_{NW} - \psi_W) + |\psi_{NE} + \psi_E - \psi_{NW} - \psi_W| \right] \\ A_S &= \frac{a_{\phi,P}}{8} \left[(\psi_{SW} + \psi_W - \psi_{SE} - \psi_E) + |\psi_{SW} + \psi_W - \psi_{SE} - \psi_E| \right] \end{aligned} \quad (4.11a,b,c,d)$$

$$A_{1E} = -\frac{1}{4}a_{1\phi,P}(r_N - r_S) \quad (4.12a)$$

$$A_{1W} = \frac{1}{4}a_{1\phi,P}(r_N - r_S) \quad (4.12b)$$

$$A_{1N} = 0 \quad (4.12c)$$

$$A_{1S} = 0 \quad (4.12d)$$

$$B_E = \frac{b_{\phi,E} + b_{\phi,P}}{8} \frac{r_N - r_S}{z_E - z_P} (r_E + r_P) \quad (4.13a)$$

$$B_W = \frac{b_{\phi,W} + b_{\phi,P}}{8} \frac{r_N - r_S}{z_P - z_W} (r_W + r_P) \quad (4.13b)$$

$$B_N = \frac{b_{\phi,N} + b_{\phi,P}}{8} \frac{z_E - z_W}{r_N - r_P} (r_N + r_P) \quad (4.13c)$$

$$B_S = \frac{b_{\phi,S} + b_{\phi,P}}{8} \frac{z_E - z_W}{r_P - r_S} (r_S + r_P) \quad (4.13d)$$

and

$$V_P = \frac{1}{4}(z_E - z_W)(r_N - r_S)r_P \quad (4.14)$$

The form of the convection coefficients A_{jS} , as given by Eqs. (4.11a,b,c,d) arises because of the "upwind differencing" used in representing the convection terms in Eq. (4.7).

Similarly Eqs. (4.1) and (4.2) can be integrated over the area enclosed by the rectangle sw,se,ne,nw in Fig. 4.4 and the two resulting algebraic equations can be

solved to give the following expressions for $\hat{H}_{\theta R}$ and $\hat{H}_{\theta I}$ at any interior node P,

$$\hat{H}_{\theta R, P} = \sum_{j=N, S, E, W} \left\{ D_1 \left(\frac{r_j}{r_p} D_j \hat{H}_{\theta R, j} \right) + D_2 \left(\frac{r_j}{r_p} D_j \hat{H}_{\theta I, j} \right) \right\} \quad (4.15)$$

$$\hat{H}_{\theta I, P} = \sum_{j=N, S, E, W} \left\{ D_1 \left(\frac{r_j}{r_p} D_j \hat{H}_{\theta I, j} \right) - D_2 \left(\frac{r_j}{r_p} D_j \hat{H}_{\theta R, j} \right) \right\} \quad (4.16)$$

where

$$D_1 = \frac{S_1}{S_1^2 + S_2^2} \quad (4.17)$$

$$D_2 = \frac{S_2}{S_1^2 + S_2^2} \quad (4.18)$$

$$S_1 = \sum_{j=N, S, E, W} D_j \quad (4.19)$$

$$S_2 = 0.5 \mu_0 \omega \sigma_P \quad (4.20)$$

with

$$D_N = \frac{2r_p}{r_N + r_p} \cdot \frac{1}{(r_N - r_p)(r_N - r_S)}$$

$$D_S = \frac{2r_p}{r_S + r_p} \cdot \frac{1}{(r_p - r_S)(r_N - r_S)}$$

$$D_E = \frac{1}{(z_E - z_P)} \cdot \frac{1}{(z_E - z_W)}$$

$$D_W = \frac{1}{(z_P - z_W)} \cdot \frac{1}{(z_E - z_W)} \quad (4.21a,b,c,d)$$

4.2.2 Expressions for boundary nodes

The successive substitution formulae given by Eqs. (4.15), (4.16) and (4.8) are valid for interior nodes. At the boundary nodes, the substitution relationships have to be derived using the boundary conditions shown in Fig. 4.1, 4.2 and 4.3. These boundary conditions are of the following general types:

$$(1) \quad \phi = \alpha_1$$

i.e. the value of the variable at the boundary is a specified constant. For example, w.r.t. Fig. 4.1,

$$\hat{H}_\theta = 0 \quad (\text{at } r=0, \quad 0 \leq z \leq z_6)$$

$$\hat{H}_\theta = \frac{I_0}{2\pi R_e} \quad (\text{at } r=R_e, \quad 0 \leq z \leq z_1) \quad \text{etc.}$$

similarly w.r.t. Fig. 4.2

$$\psi = k = \varepsilon = 0 \quad \text{at all rigid boundaries}$$

and w.r.t. Fig. 4.3

$$T = T_{m,e} \quad \text{at } z = z_2, \quad 0 \leq r \leq R_e$$

$$T = T_{l,s} \quad \text{at } r = R_m, \quad z_1 \leq z \leq z_3$$

$$(2) \quad f(\phi_i) = 0$$

i.e. a functional relationship is specified among the dependent variables. The functional relationship f is such that it is possible to solve explicitly for a variable ϕ_j at the boundary node in terms of variables at the same and adjacent nodes. For example, w.r.t. Fig. 4.2

$$\left(\frac{\xi}{r} \right)_0 = \frac{3(\psi_0 - \psi_1)}{\rho r^2 (z_1 - z_0)^2} - \frac{1}{2} \left(\frac{\xi}{r} \right)_1 \quad \text{at } z = z_3, 0 \leq r \leq R_m$$

where suffixes 0 and 1 refer to a grid node on the boundary and to the adjacent node in the z -direction, respectively.

$$(3) \quad p \frac{\partial \phi}{\partial n} + qF(\phi) = 0$$

where $\frac{\partial \phi}{\partial n}$ is the gradient, normal to the boundary surface.

These boundary conditions contain statements for the flux, normal to the bounding surfaces. For example, the symmetry boundary conditions, i.e.

$$\frac{\partial k}{\partial r} = \frac{\partial \varepsilon}{\partial r} = \frac{\partial T}{\partial r} = 0 \quad (p=1, q=0)$$

fall in this class.

Other examples are (w.r.t. Fig. 4.3)

$$K \left. \frac{\partial T}{\partial r} \right|_i + h_{W,i} (T - T_W) = 0 \quad \left(p=K_i, q=h_{W,i}, F(T)=T-T_W \right)$$

at $r = R_m, z_3 \leq z \leq z_6$

$$K_{\text{eff}} \left. \frac{\partial T}{\partial z} \right|_{s1} - \delta \epsilon_s \left[T_{s,av}^4 - \epsilon_m F'_{sm} T_m^4 - \epsilon_e F'_{se} T_{e,av}^4 \right] = 0$$

at $z = z_1$, $R_e \leq r \leq R_m$

$$(4) \quad p_1 \left. \frac{\partial \phi}{\partial n} \right|_1 + u = p_2 \left. \frac{\partial \phi}{\partial n} \right|_2$$

i.e. continuity of fluxes (or electric field) across an interface between media 1 and 2. For example, w.r.t. Fig. 4.1

$$\frac{1}{\sigma} \left. \frac{\partial \hat{H}_\theta}{\partial z} \right|_e = \frac{1}{\sigma} \left. \frac{\partial \hat{H}_\theta}{\partial z} \right|_{s1} \quad \text{at } z = z_2, \quad 0 \leq r \leq R_e$$

and

$$-K_{\text{eff}} \left. \frac{\partial T}{\partial z} \right|_{s1} + \frac{Q_s}{\pi R_e^2} \chi = -K_\ell \left. \frac{\partial T}{\partial z} \right|_\ell$$

at $z = z_3$, $0 \leq r \leq R_m$

Boundary conditions of type 1 are specified, once and for all, at the beginning of the computation. The rest of the boundary conditions need updating after every iteration. Boundary conditions (3) and (4) involve calculating first order derivatives in a direction normal to the boundary. The calculation is illustrated below:

With reference to Fig. 4.5, let us suppose that AA' represents a boundary surface and that we wish to evaluate $\left. \frac{\partial \phi}{\partial n} \right|_0$ at node 0. Let 1 and 2 be adjacent nodes in the direction normal to AA' and that $01 = n_1$ and $02 = n_2$. Let us denote

the values of ϕ at nodes 0,1, and 2 by ϕ_0 , ϕ_1 , and ϕ_2 respectively. Assuming a quadratic profile for ϕ we can write

$$\phi = \phi_0 + an + bn^2 \quad (4.22)$$

Then,

$$\phi_1 = \phi_0 + an_1 + bn_1^2 \quad (4.23)$$

and

$$\phi_2 = \phi_0 + an_2 + bn_2^2 \quad (4.24)$$

From Eqs. (4.23) and (4.24) we get,

$$\left. \frac{\partial \phi}{\partial n} \right|_0 = a = \frac{n_2^2(\phi_1 - \phi_0) - n_1^2(\phi_2 - \phi_0)}{(n_2 - n_1)n_1n_2} \quad (4.25)$$

For the case when $\left. \frac{\partial \phi}{\partial n} \right|_0 = 0$ (e.g. symmetry, free surface

boundary conditions for k, ε) we get,

$$\phi_0 = \left(\frac{n_2^2}{n_2^2 - n_1^2} \right) \phi_1 - \left(\frac{n_1^2}{n_2^2 - n_1^2} \right) \phi_2 \quad (4.26)$$

To illustrate let us consider the boundary condition for the energy equation at the free slag surface, i.e.

$$K_{\text{eff}} \left. \frac{\partial T}{\partial z} \right|_{s1} = \delta \varepsilon_S \left[T_{s,av}^4 - \varepsilon_m F'_{sm} T_m^4 - \varepsilon_e F'_{se} T_e^4 \right] \quad (3.99)$$

By using Eq. (4.25) we get,

$$\begin{aligned} \left. \frac{\partial T}{\partial z} \right|_0 &= \frac{n_2^2(T_1 - T_0) - n_1^2(T_2 - T_0)}{(n_2 - n_1)n_1n_2} \\ &= \frac{n_2^2T_1 - n_1^2T_2 - (n_2^2 - n_1^2)T_0}{(n_2 - n_1)n_1n_2} \end{aligned} \quad (4.27)$$

Putting this in Eq. (3.99) gives,

$$T_0 = \frac{n_2^2}{n_2^2 - n_1^2} T_1 - \frac{n_1^2}{n_2^2 - n_1^2} T_2 - \frac{n_1n_2}{n_1 + n_2} \delta \epsilon_S \left[T_{s,av}^4 - \epsilon_m F'_m T_m^4 - \epsilon_e F'_e T_e^4 \right] \quad (4.28)$$

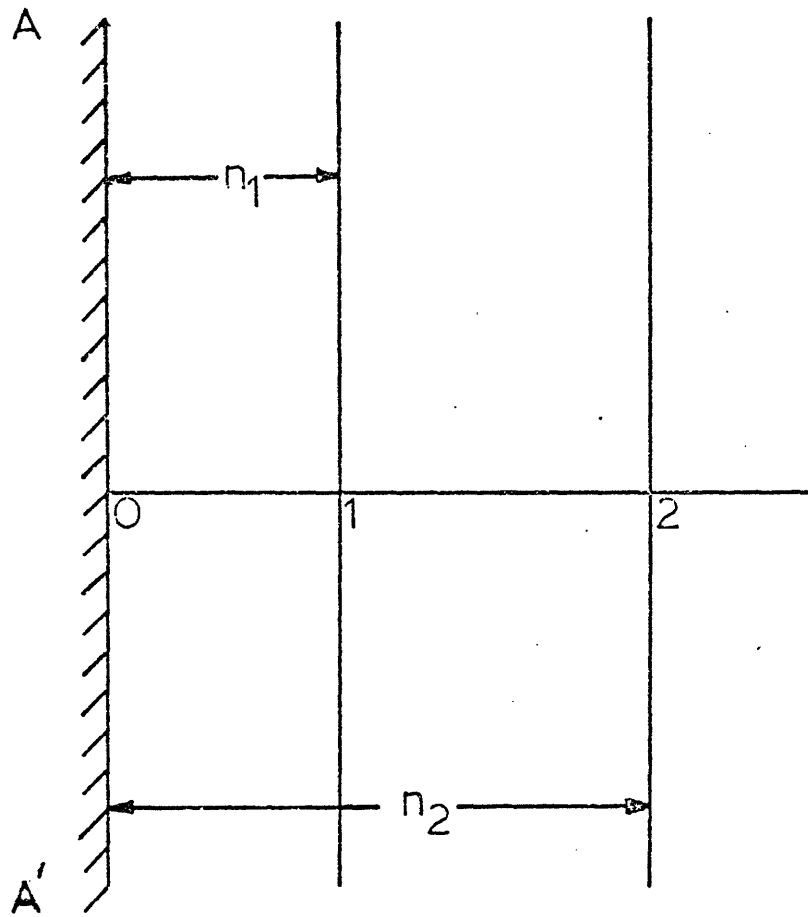
Thus at the end of an iteration, temperature at a node lying on the free surface of the slag can be updated using the above equation.

4.3 Wall Function Approach

One of the assumptions inherent in deriving the successive substitution formulae [Eq. (4.3)] is that the transport properties of the fluid vary so little between grid points that its value at a point such as *e* in Fig. 4.4 can be given by the arithmetic mean of the values at *P* and *E*. Thus,

$$b_{\phi,e} \approx \frac{b_{\phi,P} + b_{\phi,E}}{2} \quad (4.29)$$

It is known however that steep gradients of transport properties occur near the walls which bound a turbulent stream. In the immediate vicinity of the wall, the fluid



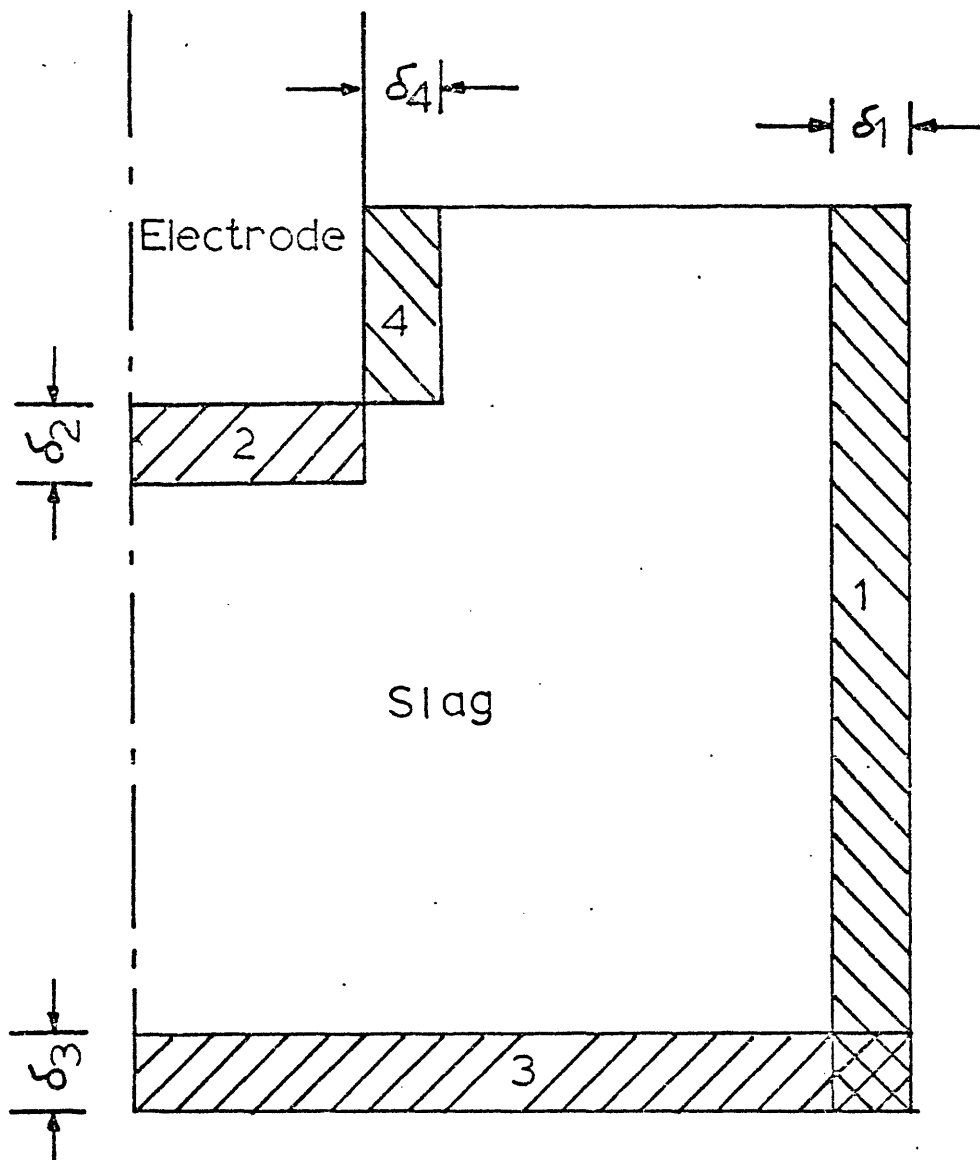
4.5 Illustration for calculating first order derivatives at boundaries.

is in laminar motion and the effective viscosity and thermal conductivity are very much lower than they are at even a short distance from the wall. The behaviour of the near wall region can be modelled either by using the low Reynolds number modelling method or by using the wall function method⁴⁶. The latter method has been used more widely. It economizes computer time and storage and allows the introduction of additional empirical information in special cases, as when the wall is rough.

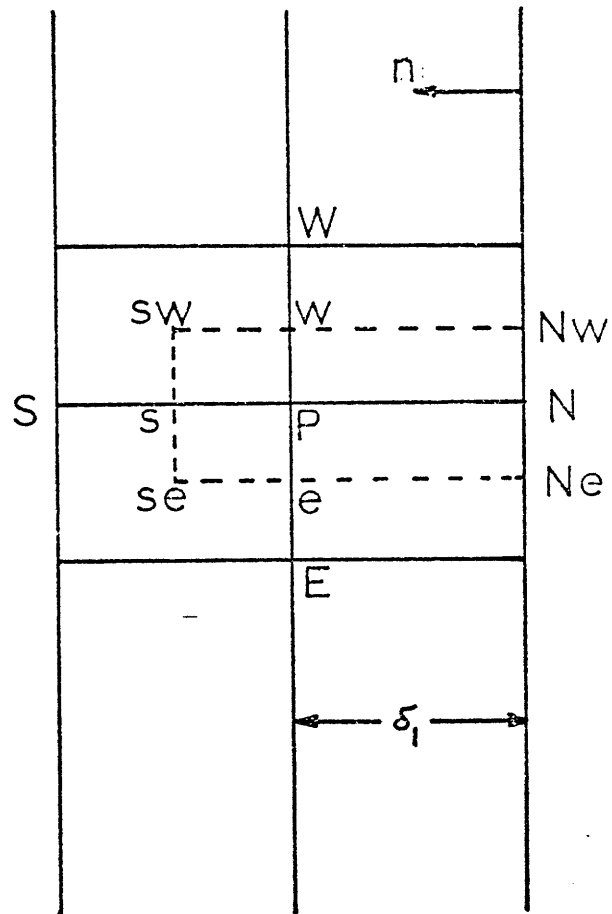
A brief treatment of wall function method for turbulence quantities (k and ϵ) and for heat transfer in the slag is given here. Fig. 4.6 shows the regions in the slag where wall function method has to be used. These regions which lie in the vicinity of various rigid walls are indicated by inclined lines and numbers 1, 2, 3, 4. Let us now illustrate the use of wall function approach with region 1 in Fig. 4.6. A portion of the grid in this region is shown in Fig. 4.7.

Let us assume that region 1 represents a constant shear layer with the value of shear stress being equal to τ_w . Let n represent distance from the wall, in the direction normal to the wall. Velocity distribution for this region can be written in terms of a "logarithmic law"⁵⁵

$$V_+ = \frac{1}{\kappa} \ln (E n^+) \quad (4.30)$$



4.6 Domains for wall function method.



4.7 Illustration for wall function approach.

where $\kappa =$ von Karman's constant $= 0.4$

$E =$ a function of wall roughness, approximately equal to 9 for a smooth wall

$V_+ = V/V_\tau =$ dimensionless velocity parallel to wall (z-direction for Fig. 4.7)

$V_\tau =$ friction velocity $= \tau_W / (\rho C_d^{1/4} k^{1/2})$

$n^+ = \frac{\rho n V_\tau}{\mu} = C_d^{1/4} \rho k^{1/2} n / \mu$

$=$ dimensionless distance from the wall.

For Eq. (4.30) to be valid, n^+ should be much larger than unity. For turbulent flow in a pipe, Pun and Spalding⁵⁵ suggest that $n^+ \geq 11.5$. Under these conditions, τ_W can be evaluated by using the following relationship⁵⁵,

$$\tau_W = \kappa C_d^{1/4} \rho V_p k_p^{1/2} / \ln [E \rho \delta_l k_p^{1/2} C_d^{1/4} / \mu] \quad (4.31)$$

The source term for the turbulence kinetic energy, S_k can be written as

$$S_k = G - D \quad (3.28)$$

$$= \tau_W \frac{\partial V}{\partial n} - \frac{C_d \rho^2 k^2}{\mu_t} \quad (4.32a)$$

$$= \tau_W \frac{\partial V}{\partial n} - \frac{C_d \rho^2 k^2}{\tau_W} \frac{\partial V}{\partial n} \quad (4.32b)$$

Near a wall, length scale of turbulence is proportional to distance from the wall and one can write ⁵⁵

$$\epsilon_p = C_d^{3/4} k_p^{3/2} / (\kappa \delta_1) \quad (4.33)$$

Let us now discuss wall function for the transfer of heat. By using the analogy between heat and momentum transfer, it can be shown ⁵⁶ that the local Nusselt number Nu_x can be given by a relationship of the following type*:

$$Nu_x = \frac{1/2 C_f' Re_x \sigma_\ell}{\sigma_t \{1 + \sqrt{1/2 C_f'} (\sigma_\ell / \sigma_t - 1) a\}} \quad (4.34)$$

where Re_x is the local Reynolds number

σ_ℓ is the Prandtl number of the fluid

σ_t is the turbulence Prandtl number

C_f' is the coefficient of skin friction defined as $1/2 C_f' = \tau_W / \rho V^2$

and 'a' is a parameter which makes an allowance for the transfer of heat through the viscous sublayer and depends on the ratio σ_ℓ / σ_t .

* Eq. (4.34) is valid in the absence of viscous dissipation or any other source of heat and for a constant wall temperature.

The final expression for the local flux of heat through the wall shown in Fig. 4.7 can be written as ⁵⁵:

$$-\frac{q_s}{\rho C_p V_p (T_p - T_N)} = \frac{\tau_w / \rho V_p^2}{\sigma_t \{1 + P \sqrt{\tau_w / \rho V_p^2}\}} \quad (4.36)$$

$$\text{with } P = 9 (\sigma_\ell / \sigma_t - 1) (\sigma_\ell / \sigma_t)^{-1/4} \quad (4.37)$$

The differential equation (4.6) is integrated over the area enclosed by the rectangle sw, se, Ne, Nw in Fig. 4.7. In the case of turbulence kinetic energy, diffusion through the wall is set equal to zero and source term is given by Eq. (4.32b). Dissipation rate of turbulence energy, ϵ_p is calculated by using Eq. (4.33). In the case of energy equation, heat flux through the wall is replaced by Eq. (4.36).

4.4 Solution Procedure

The governing differential equations and their boundary conditions have now been converted into a set of algebraic equations. These equations will now have to be solved by an iterative technique. The solution procedure used in this work is the Gauss-Seidel method and uses successive substitution as compared to the "block-methods" which use matrix inversion techniques. Among the point methods, the Gauss-Seidel method is known to yield rapid convergence and is efficient from the view point of

computer storage ³⁹. In the following subsections, the computational flowsheet will be provided together with a description of the computer program.

4.4.1 Flowsheet for computation

The equations for magnetic field intensity [Eqs. (4.1), (4.2)] are first solved to calculate the electromagnetic driving forces and the spatial distribution of the Joule heating rate. This involves using Eqs. (4.15) and (4.16) to update the values of $\hat{H}_{\theta R}$ and $\hat{H}_{\theta I}$ at the interior nodes and to use algebraic equivalent of boundary conditions to update the values at the boundary nodes. After convergence is obtained, the spatial distribution of current densities and the volumetric Joule heating rate are calculated using Eqs. (3.14 a,b) and (3.16). Next, the dependent variables for flow and heat transfer $\frac{\varepsilon}{r}$, ψ , k , ε , and T are taken up in the order indicated here. The procedure adopted can be summarized as follows:

(1) Each cycle of the iterative procedure is made up of IV subcycles where IV is the number of dependent variables.

(2) In each sub-cycle the domain of integration is scanned row by row and a single variable is updated. If the node being considered is an interior node, Eq. (4.8) is used; otherwise, the appropriate substitutional formula for the boundary node is used.

(3) When all of the sub-cycles have been completed, a new iteration cycle is commenced.

(4) The procedure is repeated until the changes in the values of the variables between successive iterations are less than a small specified quantity.

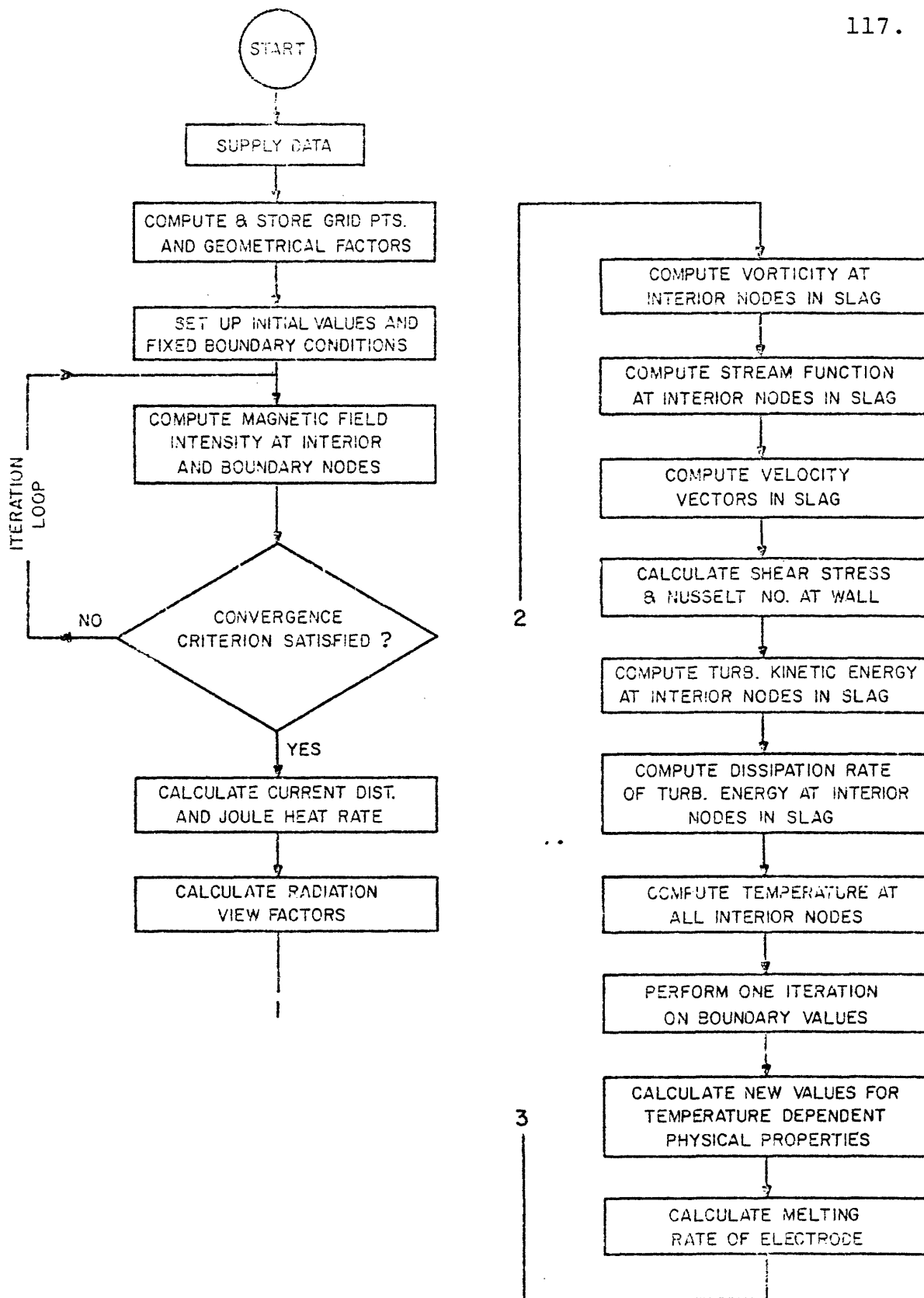
A simplified conceptual flow chart of the computational scheme is shown in Fig. 4.8.

4.4.2 Introduction to computer program

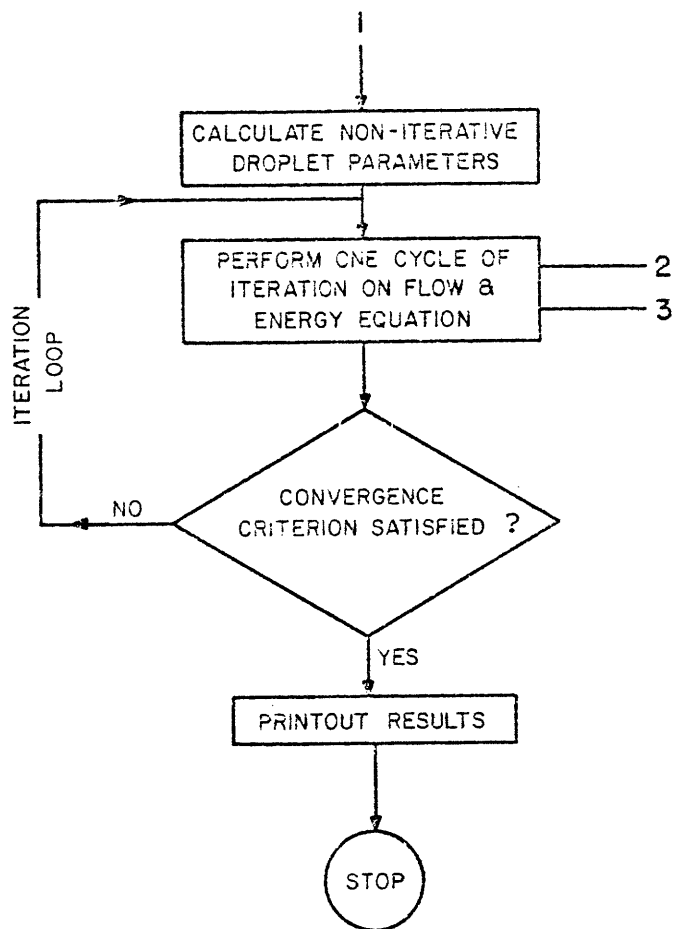
In this subsection a brief description of the computer program is given. The program was developed by following the outlines of the basic computer program published by Gosman et al ³⁹. However, extensive modifications and additions had to be made to tailor it for the present purposes. The program is subdivided into a number of subroutines, each one designed to perform a specific task. The listing of the computer program is given in Appendix E. The main features of this program are outlined in Table 4.2 which gives the names and the functions of various subroutines.

4.4.3 Stability and convergence problems

The search for a solution to the mathematical problem posed in Chapter III is based on the premise that the model describes the physics of the system adequately and that the set of differential equations together with



4.8 Simplified flow diagram for the computational scheme



4.8 Continued

Table 4.2 Description of the Computer Program

<u>Name</u>	<u>Function</u>
MAIN	Starts the computations and controls the iteration procedure for flow and heat transfer variables.
BLOCK DATA	Supplies reference values for physical properties, values for operating parameters and dimensions of the system as well as control indices for the program.
CORD	Calculates coordinates of the grid nodes as well as D_j of Eqs. (4.13), (4.14) and B_j' of Eq. (4.6).
INIT	Provides initial values for the dependent variables and computes those prescribed boundary conditions for which no iteration is required.
FIELD	Solves for magnetic field intensity. Computes the distribution of current density and Joule heat and total power usage.
VF DROP	Calculates radiation view factors and droplet parameters.

EQN Performs one cycle of iteration on the complete (both interior and boundary nodes) set of successive substitution equations by calling various subroutines. Also updates physical property values at the end of each iteration.

VORITY Computes vorticity at the interior nodes in slag.

STRFUN Computes stream function at the interior nodes in slag.

TURVAR Computes turbulence kinetic energy and the dissipation rate of turbulence energy at the interior nodes in slag.

TEMPR Computes temperature at all the interior nodes.

WALL Computes shear stress and Nusselt no. at rigid boundaries.

BOUND Computes dependent variables at those boundary nodes where iteration is required.

CONVEC Calculates A_j' of Eq. (4.6) and makes modifications for incorporating wall functions.

SORCE Calculates source term, $S_{\phi,p}$ of Eq. (4.6)

VELDIS Calculates velocity distribution in the slag.

VISCOS Calculates effective viscosity in the slag.

PROP Allows the use of temperature dependent thermo-
physical properties. Calculates the liquidus
and the solidus isotherms and the melting
rate of the electrode.

ADF Calculates first order derivative by the
three point quadratic approximation.

PRINT Prints out calculated results.

their boundary conditions constitute a complete and a well-posed problem. Even when these conditions are fulfilled it requires a great deal of numerical experimentation to ensure that the solution procedure converges to the "correct" solution. Another important aspect of the solution procedure is the speed of convergence, since the computation time has to be realistically limited. A discussion on the factors which may influence the convergence, accuracy and the economy of the procedure is given by Gosman et al ³⁹.

The computer program described earlier has evolved in stages and has involved considerable numerical experimentation. Following the practice in literature, the method of under-relaxation is used to reduce the chances of instability. If $\phi^{(N-1)}$ is the value of the variable calculated in the (N-1)th iteration and $\phi^{(N)}$ is the value which would be computed in the Nth iteration, then the value which is actually used in iteration N is computed from:

$$\phi = \alpha_{UR} \phi^{(N)} + (1 - \alpha_{UR}) \phi^{(N-1)} \quad (4.38)$$

where α_{UR} is called the under-relaxation parameter and is a number between 0 and 1. However, the rate of convergence of an iterative solution procedure can sometimes be

improved by over-relaxation³⁹. Mathematically, over-relaxation can be represented by an equation analogous to the above equation, i.e.,

$$\phi = \alpha_{OR} \phi^{(N)} + (1 - \alpha_{OR}) \phi^{(N-1)} \quad (4.39)$$

where α_{OR} , the over-relaxation parameter, lies between 1 and 2.

During numerical experimentation, the magnetic field equations were found to be very well behaved and over-relaxation was found to greatly enhance the rate of convergence. For the laboratory scale system discussed in the next chapter, $\alpha_{OR} = 1.5$ for $\hat{H}_{\theta R}$ and $\alpha_{OR} = 1.2$ for $\hat{H}_{\theta I}$ were found to give the optimum convergence rate.

In the case of other dependent variables ($\frac{\varepsilon}{r}$, ψ , k , ε , T), over-relaxation for the stream function and under-relaxation for the rest of the variables was found to be the best practice. The attempt to over-relax the vorticity equation lead to divergence.

To observe the convergence rate, two different criteria for convergence were employed. In one following Gosman et al³⁹, the maximum fractional change of ϕ in the field was dictated to be less than a prescribed value, i.e.;

$$[(\phi^{(N)} - \phi^{(N-1)})/\phi^{(N)}]_{\max} \leq \epsilon_1 \quad (4.40)$$

Usually ϵ_1 has been set in the range of 0.001 to 0.005.

It sometimes happens that when the value of a variable at a particular node is much smaller than the values at surrounding nodes, fluctuations, in the small value will occur which are unacceptable by the above criterion, even though the rest of the field has converged. In this case an alternative criterion used by some other authors^{32,35} was employed. This is given as

$$\frac{\sum |\phi^{(N)} - \phi^{(N-1)}|}{\sum |\phi^N|} \leq \epsilon_2 \quad (4.41)$$

where \sum means summation over all the interior nodes.

ϵ_2 has been set in the range 0.001 to 0.005.

The numerical solution was carried out on IBM 370 at MIT. Calculated results and discussions are given in the next chapter.

Nomenclature

$a_\phi, a_{1\phi}, b_\phi, c_\phi$	Coefficients in the general elliptic equation (4.6)
A'_j, B'_j	Coefficients in the general substitution formula, Eq. (4.8)
A_E, A_W, A_N, A_S	Coefficients in the convection terms of the general substitution formula, given by Eqs. (4.11a,b,c,d)
$A_{1E}, A_{1W}, A_{1N}, A_{1S}$	Coefficients accounting for the movement of interfaces, given by Eqs. (4.12a,b,c,d)
B_E, B_W, B_N, B_S	Coefficients in the diffusion terms of the general substitution formula, given by Eqs. (4.13a,b,c,d)
C_d	Dissipation rate constant
C'_f	Coefficient of skin friction
D_1, D_2	Terms in substitution formula for magnetic field intensity
D_N, D_S, D_E, D_W	Coefficients defined by Eqs. (4.21 a,b,c,d)
E	A function of wall roughness appearing in logarithmic law Eq. (4.30)

Nomenclature (cont'd)

$\hat{H}_\theta, \hat{H}_\theta $	Complex amplitude of magnetic field intensity in θ -direction, its magnitude
$\hat{H}_{\theta R}, \hat{H}_{\theta I}$	Real and imaginary parts of \hat{H}_θ
$\hat{J}_r, \hat{J}_r $	Complex amplitude of current density in r -direction, its magnitude
$\hat{J}_{rR}, \hat{J}_{rI}$	Real and imaginary parts of \hat{J}_r
$\hat{J}_z, \hat{J}_z $	Complex amplitude of current density in z -direction, its magnitude
$\hat{J}_{zR}, \hat{J}_{zI}$	Real and imaginary parts of \hat{J}_z
k	Kinetic energy (per unit mass) of turbulence
Nu_x	Local Nusselt number
n, n^+	Dimensional, dimensionless distance normal to wall
P	Defined by Eq. (4.37).
Re_x	Local Reynolds number

Nomenclature (cont'd)

r	Radial coordinate
S_1, S_2	Defined by Eqs. (4.19), (4.20)
S_ϕ	Source term in the general elliptic equation (4.6)
T	Temperature
V_+, V	Dimensionless, dimensional velocity parallel to wall
V_τ	Friction velocity
z	Axial coordinate
GREEK SYMBOLS	
α_{UR}, α_{OR}	Parameters for under and over relaxation
β_H	Phase angle of \hat{H}_θ
$\delta_1, \delta_2, \delta_3, \delta_4$	Domains for the wall function approach
ϵ	Dissipation rate of turbulence energy
ϵ_1, ϵ_2	Convergence parameters defined by Eqs. (4.40), (4.41)

Nomenclature (cont'd)

ϕ	General notation for dependent variables
ξ	Vorticity
ψ	Stream function
σ_λ, σ_t	Prandtl number, turbulence Prandtl number
τ_w	Shear stress at wall
κ	von Karman's constant

CHAPTER V

COMPUTED RESULTS AND DISCUSSION

The model developed in Chapter III is now used to make predictions on the flow and thermal characteristics in an ESR system. Computed results presented in this chapter show typical temperature and velocity distributions and pool profiles as well as the interdependence of key process parameters, with the power input, fill ratio, amount of slag used and the position of the electrode as the independent variables and the casting rate, pool depth, velocity and temperature fields as the dependent variables. Wherever possible these predictions will be compared with experimental measurements available in the literature ⁵⁷.

5.1 Description of the System Chosen for Computation

The experimental results, to which the predictions will be compared, are those reported by Mellberg⁵⁷ who studied the electroslag remelting of ball bearing steels in a laboratory scale system, using electrodes of 0.057 m diameter and a stationary water cooled copper mold of 0.1 m internal diameter. Remelting was done with alternating current and the mold was electrically insulated from the base plate. The electrode composition is given in Table 5.1 and the remelting parameters are given in Table 5.2.

Table 5.1 Composition of Electrodes Used by Mellberg

Components	C	Si	Mn	P	S	Cr	Al	O
Wt %	1.03	0.35	0.37	0.017	0.019	1.53	0.037	0.0025

Table 5.2 Remelting Parameters in Mellberg's Experiments

Ingot No.	Current, kA	Voltage V	Starting Slag Wt kg	Starting Slag Comp., Wt %				Casting rate cm/min
				CaF ₂	CaO	Al ₂ O ₃	SiO ₂	
15	1.7	34	1.5	68	1	29	1	1.23
17	1.55	30	1.5	68	1	29	1	1.03

5.2 Physical Properties and Parameters Used in Computation

The computer program described in Chapter IV and included in the thesis as Appendix E allows for the temperature dependence of physical properties (μ, C_p, ρ, K) appearing in the model. As described in Chapter III, in order to keep the equation for magnetic field intensity decoupled from the flow and heat transfer equations, the model uses average values for the electrical conductivities of slag and metal. However, in some of the calculations an approximate allowance has been made for the temperature dependence of electrical conductivity of slag. In the absence of specific information on the temperature dependence of properties for the system being modeled, it was decided to perform calculations with constant values for the properties.

Physical property values used in the computation are listed in Table 5.3. The liquidus temperature, the density and the viscosity of the slag were estimated from data reported in reference 40 and its electrical conductivity was estimated from compilations made by Hajduk and El Gammal⁵⁸. In the absence of better information, values for the specific heat, the thermal conductivity and the coefficient of volume expansion of the slag were taken the same as those used by Dilawari and Szekely¹⁵. The liquidus and the solidus temperature of the metal were given by Mellberg⁵⁷. Values for the other properties were taken from Dilawari and Szekely¹⁵ and from Elliott

and Maulvault¹¹. These values apply for pure iron or for intermediate carbon steels. The value for atomic thermal conductivity of molten metal was taken to be half of that for solid metal.

The dimensions of the system and the values for other parameters appearing in the model are shown in Table 5.4. The values for the constants C_1 , C_2 , C_d , σ_k , σ_ϵ of the $k - \epsilon$ model are those recommended by Launder and Spalding⁴⁶. These recommendations were made on the basis of extensive examination of free turbulent flows. However, one must be aware that these are not universal constants and may change in different situations. The value for the convective heat transfer coefficient between the electrode surface and the ambient was suggested to be $17.2 \text{ W}/(\text{m}^2\text{K})$ by Mendrykowski et al³. From experimental measurements, Maulvault⁷ calculated this to be in the range $19 - 32 \text{ W}/\text{m}^2 \text{ K}$. A value of $25 \text{ W}/\text{m}^2 \text{ K}$ was chosen for the present case. Values for heat transfer coefficients below the slag-metal interface were deduced from suggestions made by Elliott and Maulvault¹¹ and Ballantyne and Mitchell¹². As seen in Table 5.4, below the slag-metal interface, heat removal by cooling water is represented by three heat transfer coefficients. Instead of using discontinuous values for heat transfer coefficient, as has been done here, it will certainly be

Table 5.3 Physical Property Values Used

K_e	thermal conductivity of electrode, 31.39	}	$\frac{W}{mK}$
K_{sl}	thermal conductivity of slag, 10.46		
K_m	thermal conductivity of mushy zone, 31.39		
K_s	thermal conductivity of solid ingot, 31.39		
$K_{m,l}$	thermal conductivity of molten metal, 15.48		
ρ_e	density of electrode, 7.2×10^3	}	$\frac{kg}{m^3}$
ρ_{sl}	density of slag, 2.85×10^3		
ρ_l, ρ_m, ρ_s	density of liquid metal, mushy zone, solid ingot, 7.2×10^3		
$C_{p,e}$	specific heat of electrode, 502	}	$\frac{J}{kgK}$
$C_{p,sl}$	specific heat of slag, 837		
$C_{p,l}, C_{p,m}, C_{p,s}$	specific heat of liquid metal, mushy zone, solid ingot, 753		
$T_{l,m}$	liquidus temperature of metal, 1723 K		
$T_{s,m}$	solidus temperature of metal, 1523 K		
$T_{l,s}$	liquidus temperature of slag, 1650 K		

β	coefficient of cubical expansion of slag, $1 \times 10^{-4} \text{ K}^{-1}$
λ	latent heat of fusion of metal, 247 kJ/kg
σ_e, σ_m	electrical conductivity of electrode, metal, 7.14×10^5 mho/m
σ_{sl}	electrical conductivity of slag, 2.50×10^2 mho/m
ϵ_e	emissivity of electrode surface, 0.4
ϵ_s	emissivity of free slag surface, 0.6
γ	interfacial tension between molten slag and molten metal, 0.9 N/m
μ	viscosity of slag, 0.01 kg/m·s

Table 5.4 Numerical Values of Parameters Used In Computation

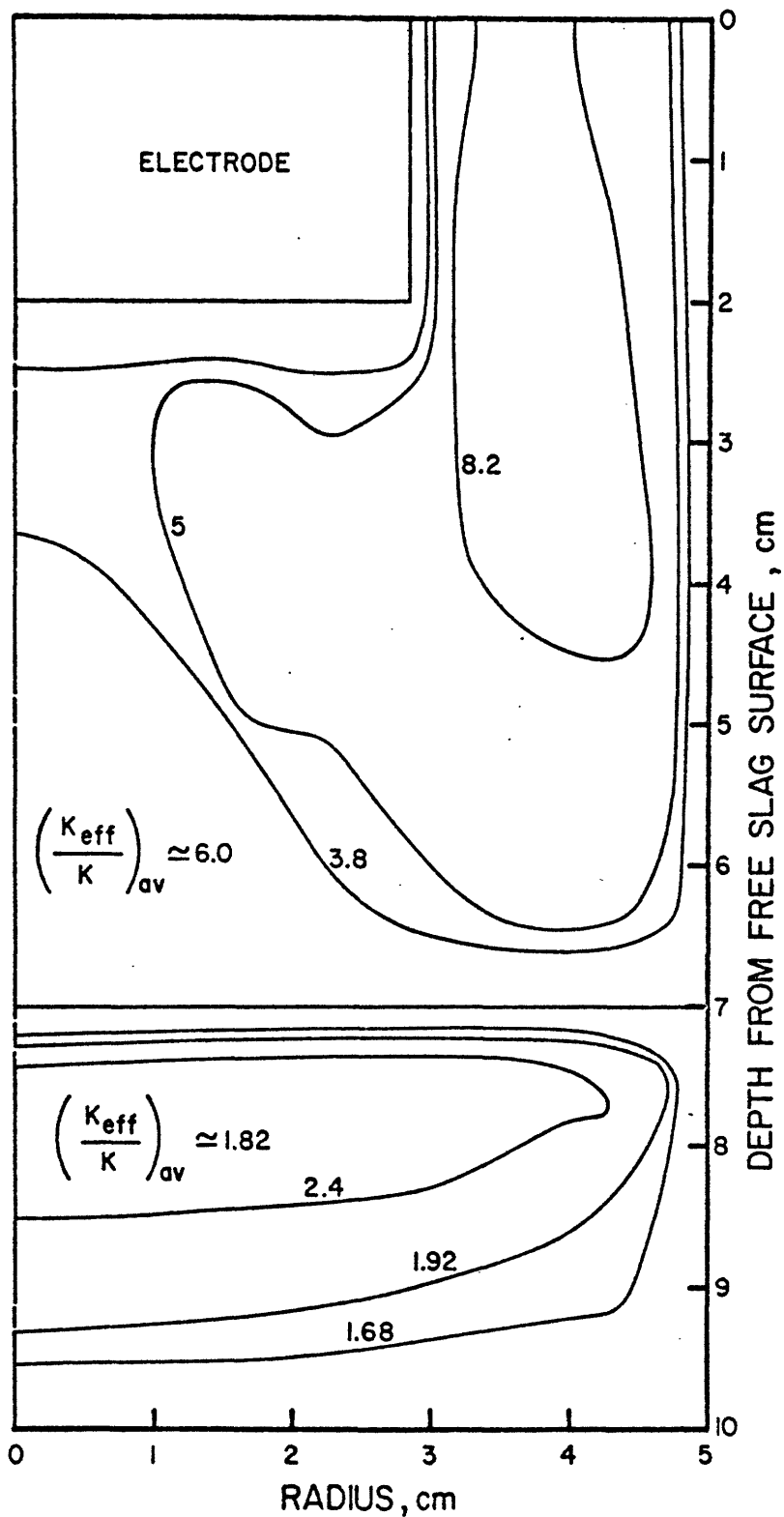
R_e	electrode radius, 0.0285 m	
R_m	mold inside radius, 0.05 m	
Z_1	free slag surface, 0.30 m	
Z_2	melting tip of electrode, 0.32 m	
Z_3	slag-metal interface, 0.37 m	
Z_6	lower boundary of the ingot, 0.73 m	
C_1	constant in $k - \epsilon$ model, 1.44	
C_2	constant in $k - \epsilon$ model, 1.92	
C_d	dissipation rate constant, 0.09	
σ_k	Prandtl number for k , 1.0	
σ_ϵ	Prandtl number for ϵ , 1.3	
μ_0	magnetic permeability, 1.26×10^{-6} Henry/m	
h_c	heat transfer coefficient between the electrode and the gas, 25.1	} $\frac{W}{m^2 K}$
$h_{w,1}$	heat transfer coefficient at the molten metal-mold interface, 272	

$h_{w,2}$	heat transfer coefficient at the mushy zone-mold interface, 272	} $\frac{W}{m^2 K}$
$h_{w,3}$	heat transfer coefficient at the ingot-mold interface, 188	
ω	angular frequency of current, 377 radians/s	
\bar{I}_0	total current (rms value), 1.4 - 2.5 kA	

more realistic to use heat transfer coefficient as a function of position if such information is available.

The evaluation of the parameter Λ which appears in Eq. (3.44) remains to be discussed. As seen from Eq. (3.44), $(1 + \Lambda)$ represents the ratio of effective and atomic thermal conductivities in the metal pool. In the present work an attempt has been made to link this parameter to operating conditions by evaluating it from the computed flow field in the slag. Calculations were carried out for turbulent fluid flow and heat transfer in both the slag and the metal pool for the conditions when the shape of the metal pool was assumed cylindrical and its size pre-determined. This approach is analogous to the one taken by Dilawari and Szekely¹⁵. A typical result on the computed ratios of effective and atomic thermal conductivities in both the slag and the metal pools is shown in Fig. 5.1. This figure represents computation for an operating current of 1.7 KA and for an assumed metal pool depth of 0.03 m. Calculations like these indicated that the average ratio of the effective and atomic thermal conductivities in the metal pool was about one third of the corresponding ratio for the slag pool, i.e.

$$\left(\frac{K_{\ell}}{K_{m\ell}}\right) = 1 + \Lambda \approx \frac{1}{3} \left(\frac{K_{eff}}{K_{avg}}\right) \quad (5.1)$$



5.1 Computed ratio of effective and atomic thermal conductivities in both slag and metal pools for operation with 1.7 kA (rms) and for an idealized metal pool shape and size.

where, as mentioned before, K_ℓ and $K_{m\ell}$ denote the effective and the atomic thermal conductivities of the metal pool whereas K_{eff} and K denote the corresponding quantities for the slag. An attempt such as Eq. (5.1) appears crude at best and it is entirely possible that the value of the coefficient in this equation would differ from the value of $1/3$ used in the present instance for different geometries and for much different current levels. Furthermore, according to the scheme chosen here, we only account for the mixing or dispersive action of turbulence in the metal pool, and the convective term in the equation for heat transport is still unaccounted for. These criticisms can not be taken care of unless the model is extended to calculate fluid flow in the metal pool. In the mean time, however, it does appear more reasonable to calculate the effective thermal conductivity in the metal pool from the model itself (albeit in an approximate manner) than selecting it to give a better agreement with the experimental measurements. For the results presented here, calculated values for Λ fell in the range $0.7 - 3.4$.

5.3 Computational Details

The numerical scheme outlined in Chapter IV was used to solve the governing equations. Fig. 5.2 shows the grid which is typical of those used in the calculations presented in this chapter. As shown in this figure,

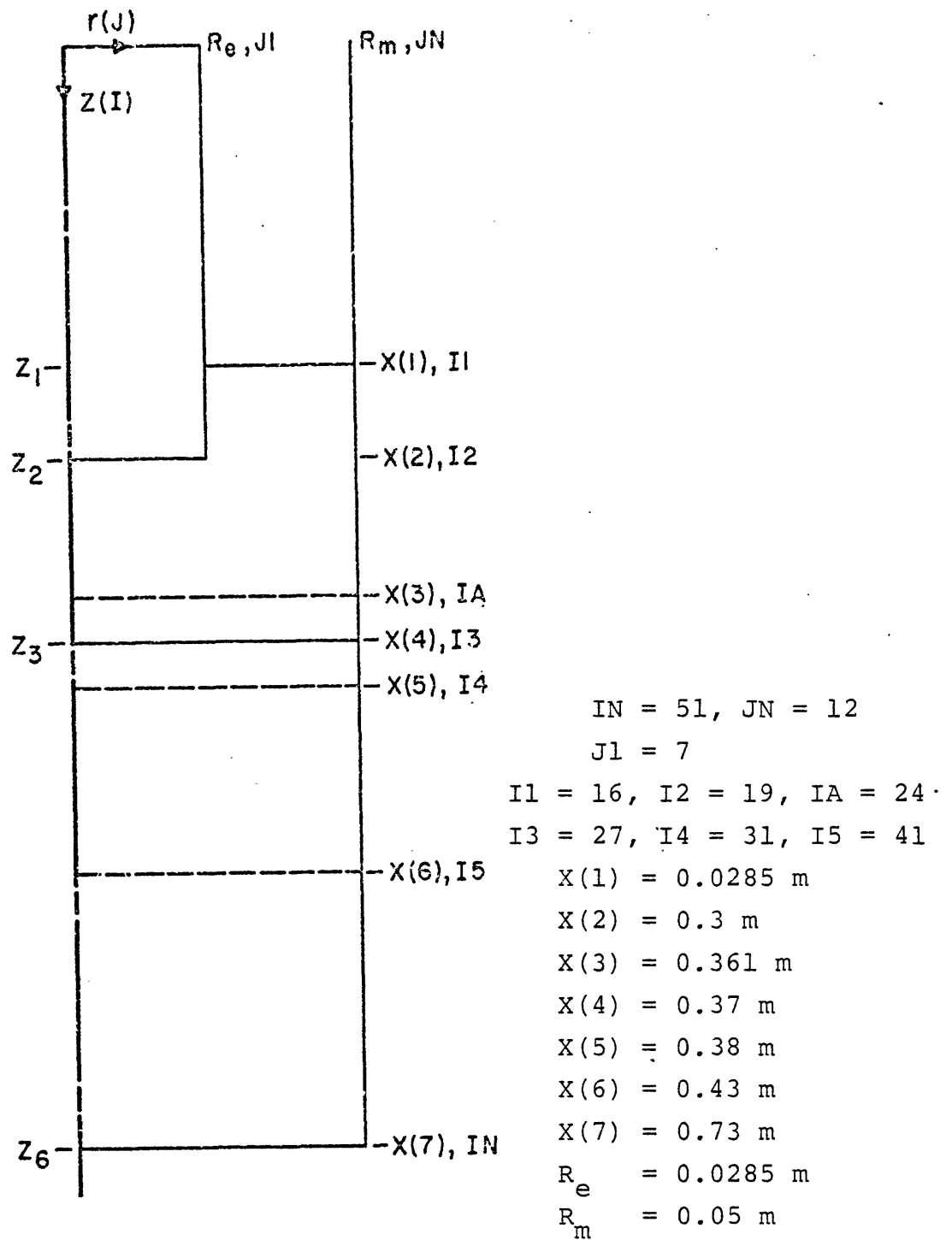


Fig. 5.2 Details on the grid configuration.

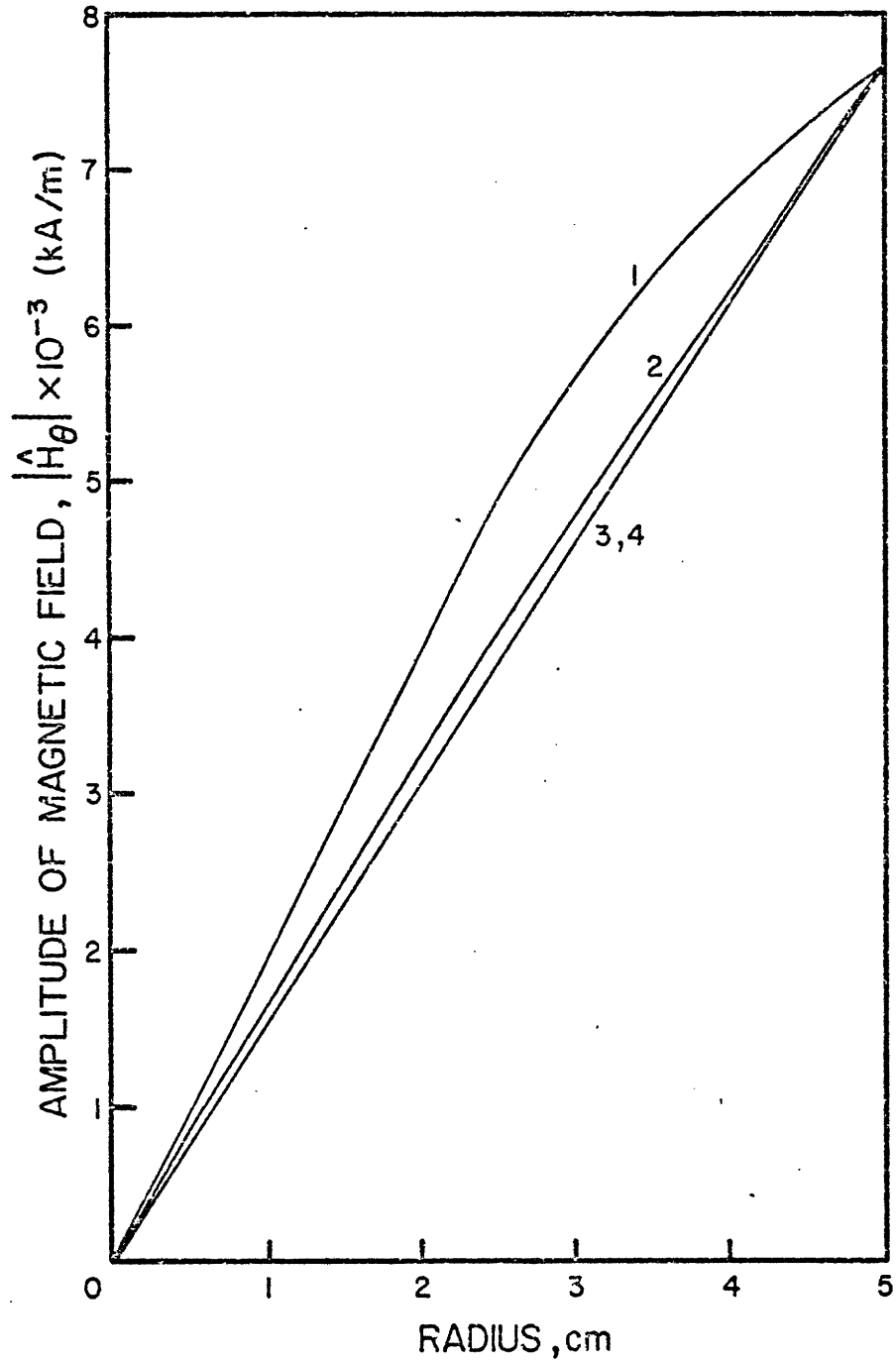
there are 51 I-lines (z-direction) and 12 J-lines (r-direction). While the spacing between the J-lines was kept the same in all the computations reported here, spacing between the I-lines was adjusted for various cases to concentrate nodes in the critical areas. The computations were carried out using the IBM 370 digital computer at MIT; the time interval involved in the computation was in the range of 100-200 seconds.

5.4 Results and Discussions

A selection of computed results on the electromagnetic aspect of the process is first presented and then results for the flow and thermal aspects are given. In the following discussions ingots 15 and 17 refer to operations with 1.7 kA and 1.55 kA (both rms values) respectively.

5.4.1 Computed results on electromagnetic parameters

Fig. 5.3 shows the radial distribution of the magnetic field intensity in the slag and in the metal calculated at different axial positions and for an operating current of 1.7 kA (rms). Curves 1 and 2 refer to calculations for the slag at vertical positions, 0.016 m and 0.044 m below the electrode respectively. Curves 3 and 4 refer to calculations for the metal at positions, 0.045 m and 0.22 m below the slag-metal interface

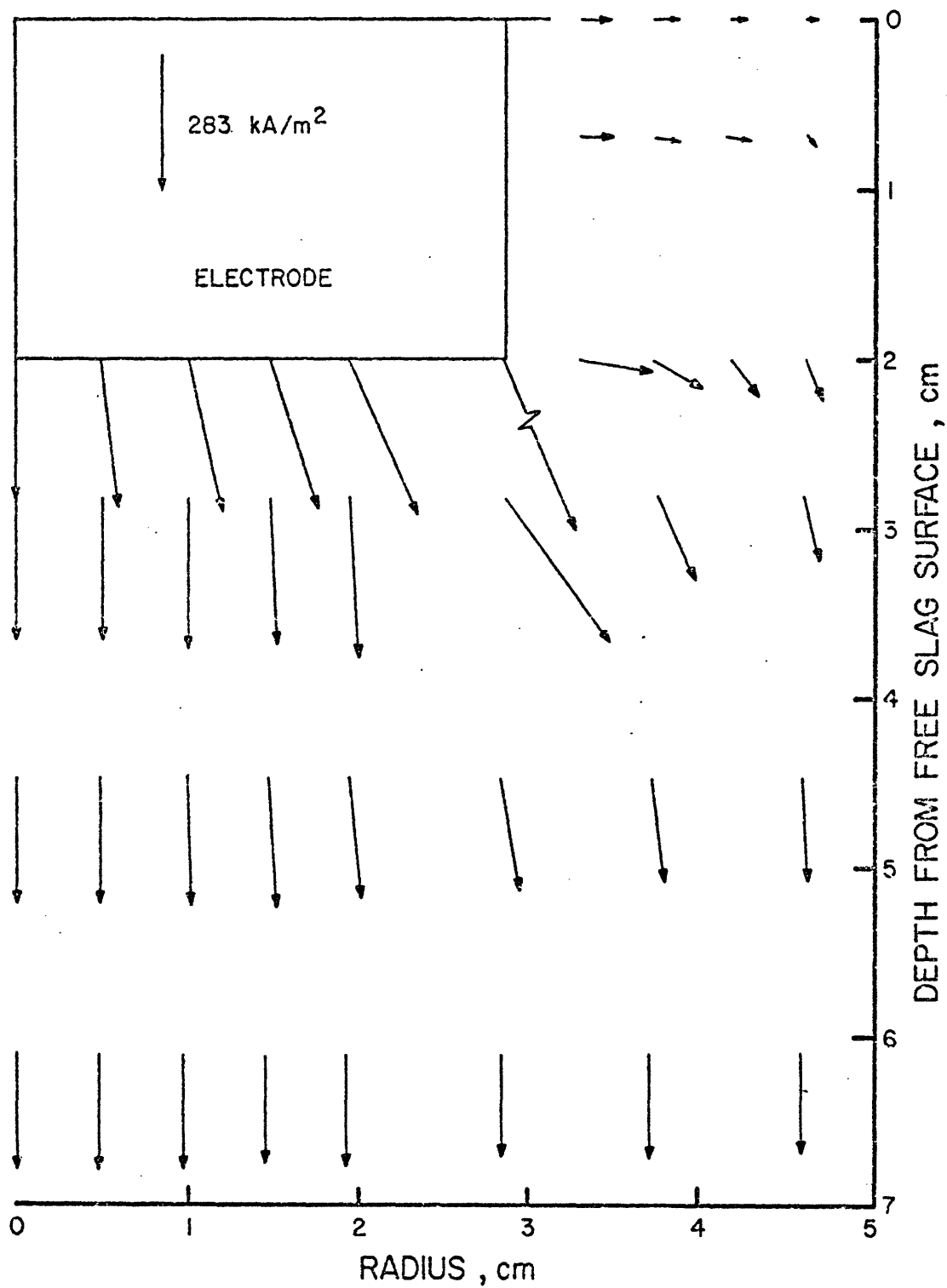


5.3 Computed magnetic field intensity for operation with 1.7 kA (rms).

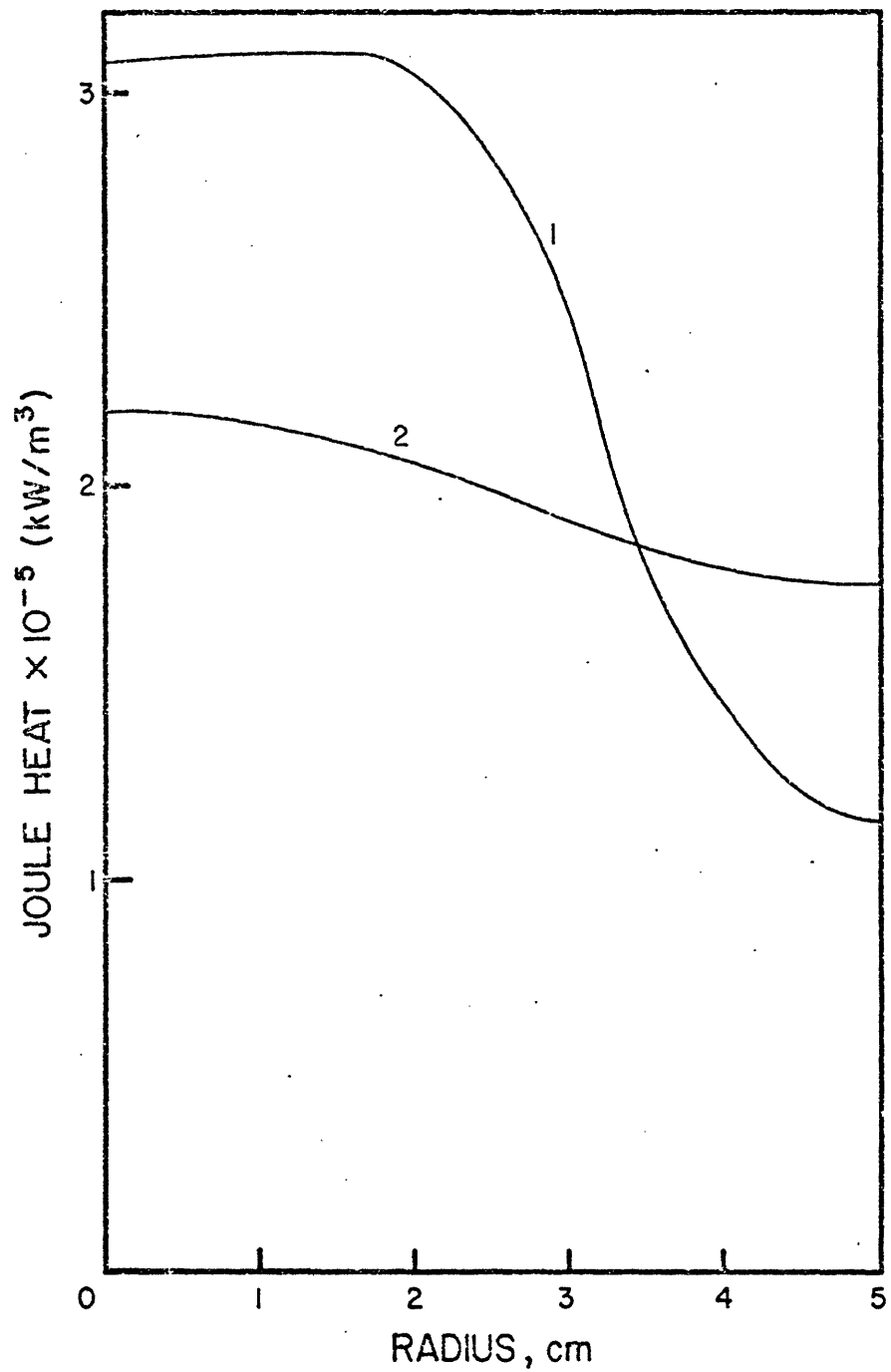
- 1 1.6 cm below electrode
- 2 4.4 cm below electrode
- 3 4.5 cm below the slag-metal interface
- 4 22 cm below the slag-metal interface

respectively. As seen in this figure, the radial distribution of the magnetic field intensity in the metal is linear and the distributions at the two locations are identical. This implies that the current in the radial direction is negligible and that the axial component of the current is distributed uniformly across the cross section (with a density of 216 kA/m^2). In the slag, as can be inferred from curves 1 and 2, the radial component of current is finite and becomes small as the slag-metal interface is approached. This is readily seen in Fig. 5.4 which shows the current density vectors (length of a vector represents the rms value of current density) in the slag. The current path diverges in the vicinity of the electrode-slag interface but it becomes almost parallel as the slag-metal interface approaches.

Fig. 5.5 shows the radial distribution of volumetric Joule heat generation rate in the slag for the same two axial positions as in Fig. 5.3 (i.e. 0.016 m and 0.044 m below the electrode). In the vicinity of the slag-electrode interface, heat generation rate is quite high and the distribution is non-uniform. As is to be expected from the discussions given in connection with previous figures, the radial distribution of heat generation rate becomes uniform when the distance from the slag-electrode interface increases. The heat generation rates



5.4 Computed current density vectors in slag for operation with 1.7 kA (rms).



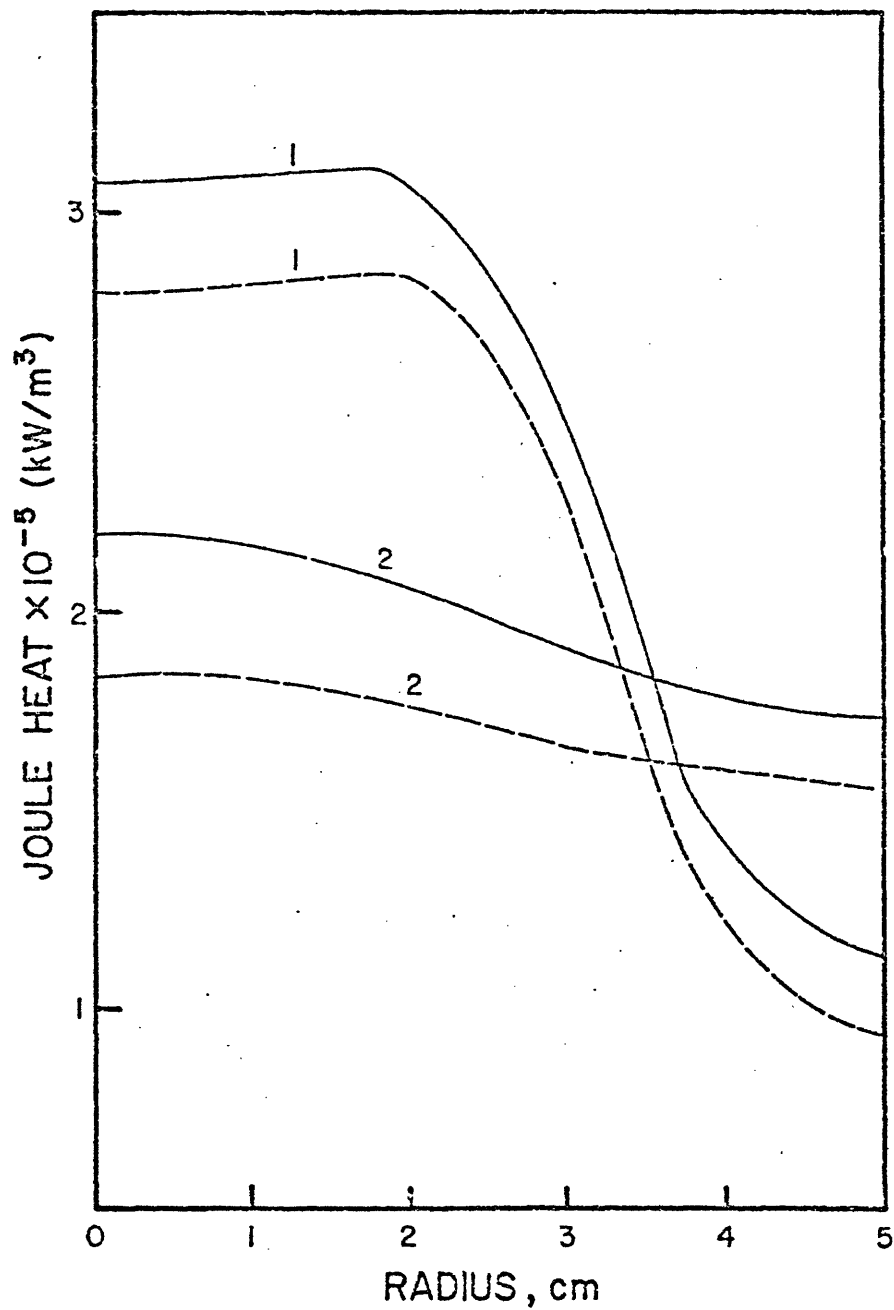
5.5 Computed radial distribution of volumetric heat generation rate in slag for operation with 1.7 kA.

- 1 1.6 cm below electrode
- 2 4.4 cm below electrode

are completely uniform in the ingot (65.45 kW/m^3) and in the upper portions of the electrode (621.6 kW/m^3).

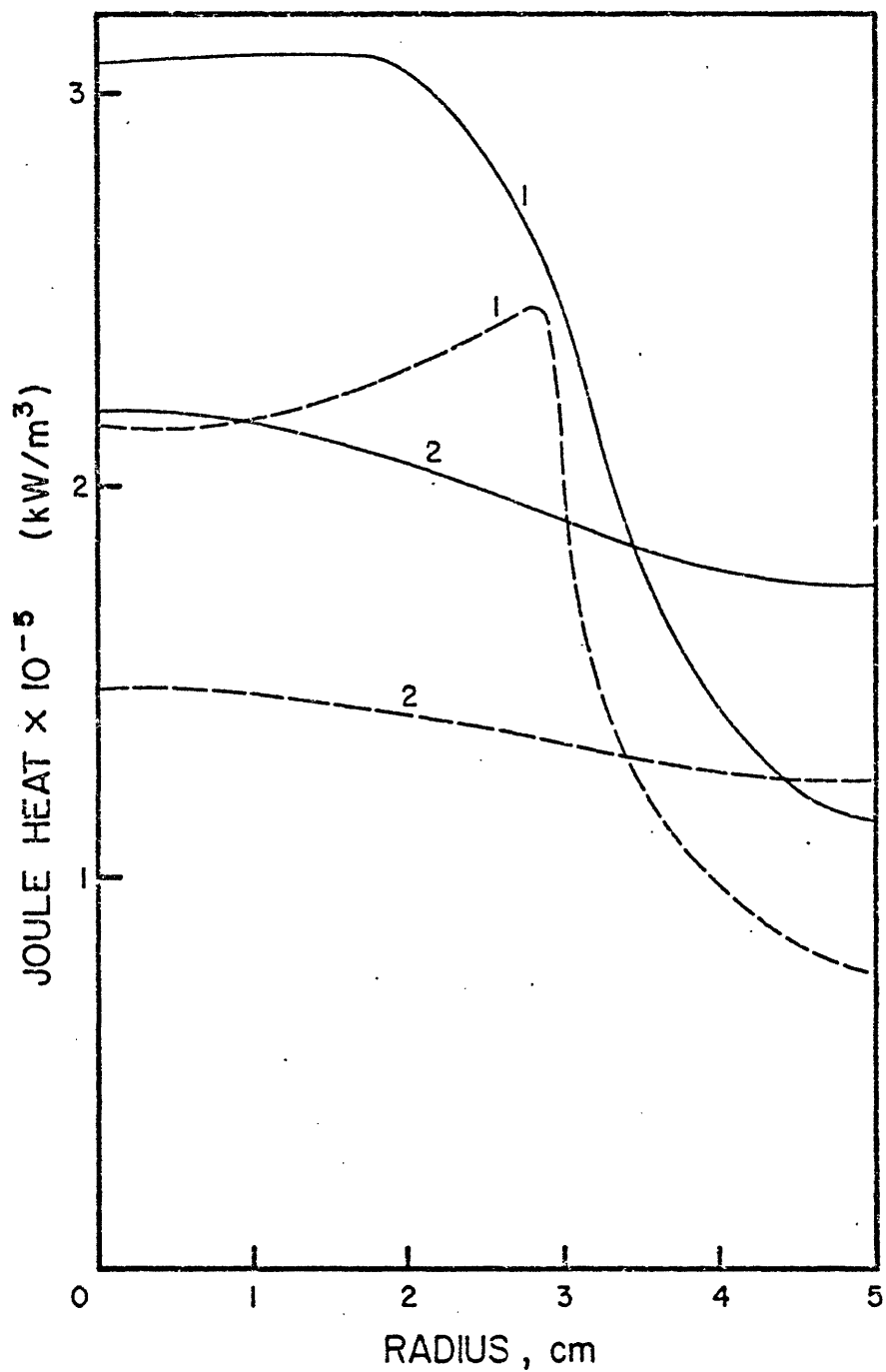
Fig. 5.6 shows the effect of electrode penetration depth in the slag. Here the solid lines represent calculations already shown in Fig. 5.5 whereas the broken lines denote calculations where the electrode protrudes 0.01 m into the slag (as compared to 0.02 m for the previous case). The total amount of slag used (1.5 kg) and the power input (73 kW) were the same in both the cases. Curves 1 and 2 in this figure have the same meanings as in Fig. 5.5. As seen here, the case with a lower electrode penetration depth has a lower volumetric heat generation rate in the bulk portion of the slag. This is to be expected since the volume of slag below the electrode is larger in this case. The different heat generation patterns in the two cases will lead to different temperature distributions in the slag. This will be examined subsequently.

Fig. 5.7 shows the effect of the amount of slag used on the heat generation rate in the slag. Once again the solid lines represent the results already described in Fig. 5.5 whereas the broken lines represent calculations for a higher amount of slag (1.9 kg vs 1.5 kg for the former case). The electrode penetration depth (0.02 m) and the input power (73 kW) were the same in both the



5.6 The effect of electrode penetration depth on heat generation rate in slag.

- depth of penetration of electrode 2 cm, power 73 kW
- depth of penetration of electrode 1 cm, power 73 kW
- 1 1.6 cm below electrode
- 2 4.4 cm below electrode

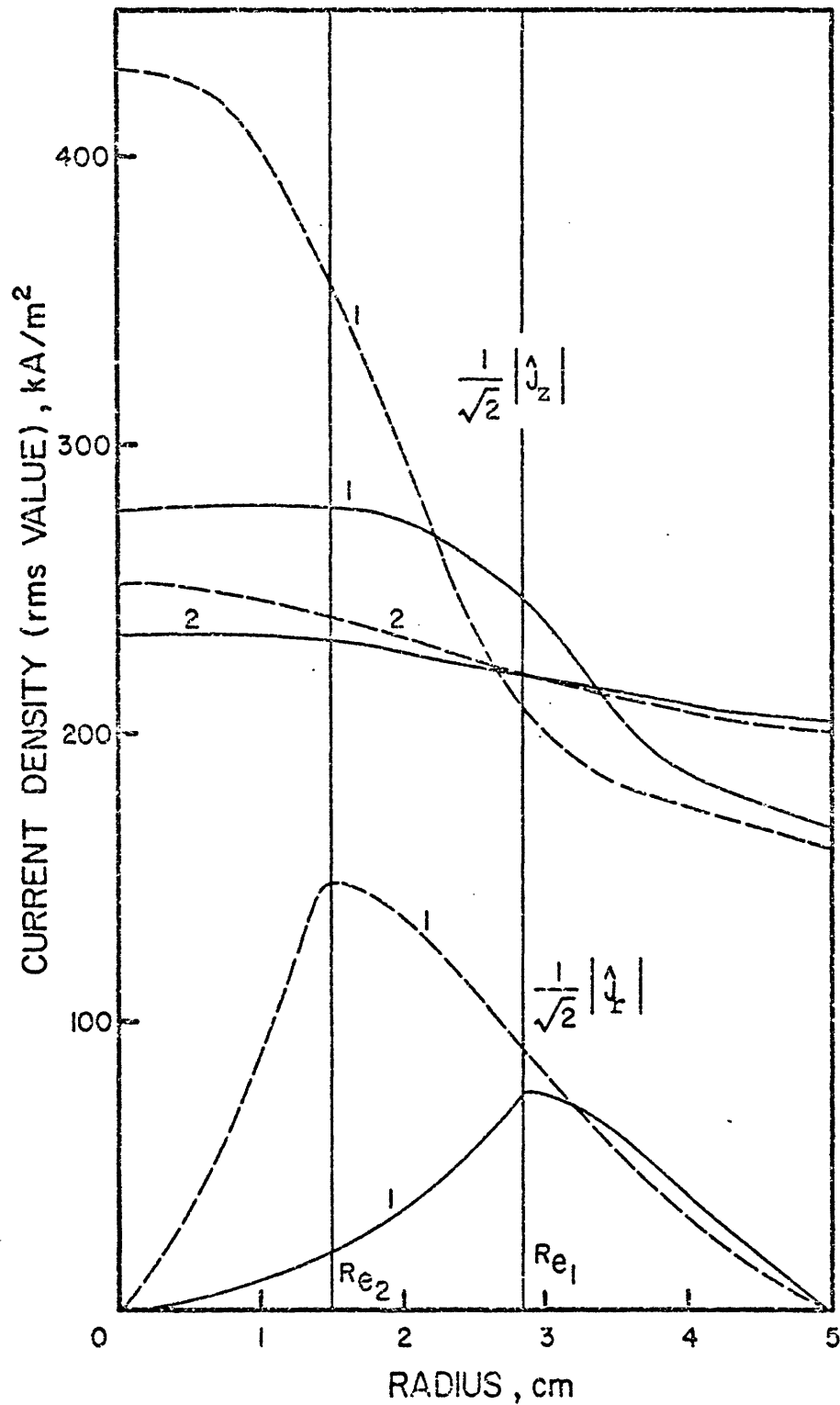


5.7 The effect of the amount of slag used on the heat generation rate in slag.

- amount of slag 1.5 kg
- - - amount of slag 1.9 kg
- 1 1.6 cm below electrode
- 2 4.4 cm below electrode

cases. As seen here, the larger volume of slag in the second case gives rise to a lower volumetric heat generation rate in the slag. Based on a uniform current distribution over the entire cross section of slag, the volumetric heat generation rate is $1.32 \times 10^5 \text{ kW/m}^3$ for operation with 1.9 kg of slag as compared to $1.87 \times 10^5 \text{ kW/m}^3$ for the other case. For both the lower electrode penetration depth and the larger amount of slag used, the resistance of the system was found to increase in accordance with the operating experience⁶².

Fig. 5.8 shows the effect of fill ratio (cross sectional area of electrode/c.s.area of mold) on current distribution in the slag. The solid lines denote calculations for an electrode radius of 0.0285 m (Re_1) whereas the broken lines represent calculations for an electrode radius of 0.015 m (Re_2). The mold radius in both the cases is 0.05 m and the total current in each case is 1.7 kA. As in the case of previous figures, 1 and 2 denote vertical positions 0.016 m and 0.044 m below the electrode-slag interface. In the vicinity of the electrode and directly below it, there is an appreciable difference in the current density in the two cases with the lower fill ratio case having a much larger current density. The difference narrows as the radius increases. From the discussions given in section 3.7.2, we expect that a larger



5.8 The effect of fill ratio on current distribution in the slag.

--- fill ratio = 0.09 1 1.6 cm below electrode
 — fill ratio = 0.325 2 4.4 cm below electrode

current density will give rise to increased velocity in the slag. This effect of the fill ratio will be examined subsequently. As the slag-metal interface is approached, the current density tends to be uniform and the difference in the two cases becomes small. Another effect of the reduced fill ratio is that the "effective cross section" for the passage of the current decreases, thereby increasing the electrical resistance of the system and the heat generation rate. Thus the total power input for the case with 0.015 m electrode radius (fill ratio = 0.09) is calculated to be 94 kW as compared to 73 kW for the case with 0.0285 m electrode radius (fill ratio = 0.32). The experimental observation of this effect is reported in the literature ^{61, 62}.

Before closing this subsection, it should be noted that the computed current distribution and the heat generation pattern, and consequently fluid flow and temperature distribution, will depend on the assumed shape of the electrode tip and on the assumptions made regarding the boundary conditions (e.g. insulating slag skin on the inside wall of the mold, the presence of a solidified slag crust on the submerged vertical wall of the electrode). As mentioned in Chapter III, the model developed in this work assumes a flat melting tip for the electrode and an insulating slag skin on the interior surface of the mold. The latter assumption is in accord with observations made

in literature ^{40,41}. The assumption of a flat melting tip is made for computational convenience and ideally the shape of the electrode tip should be calculated using the mathematical model itself. However, this refinement to the model can only be accomplished if a more realistic understanding is developed of the melting process. This will require both experimental and analytical work.

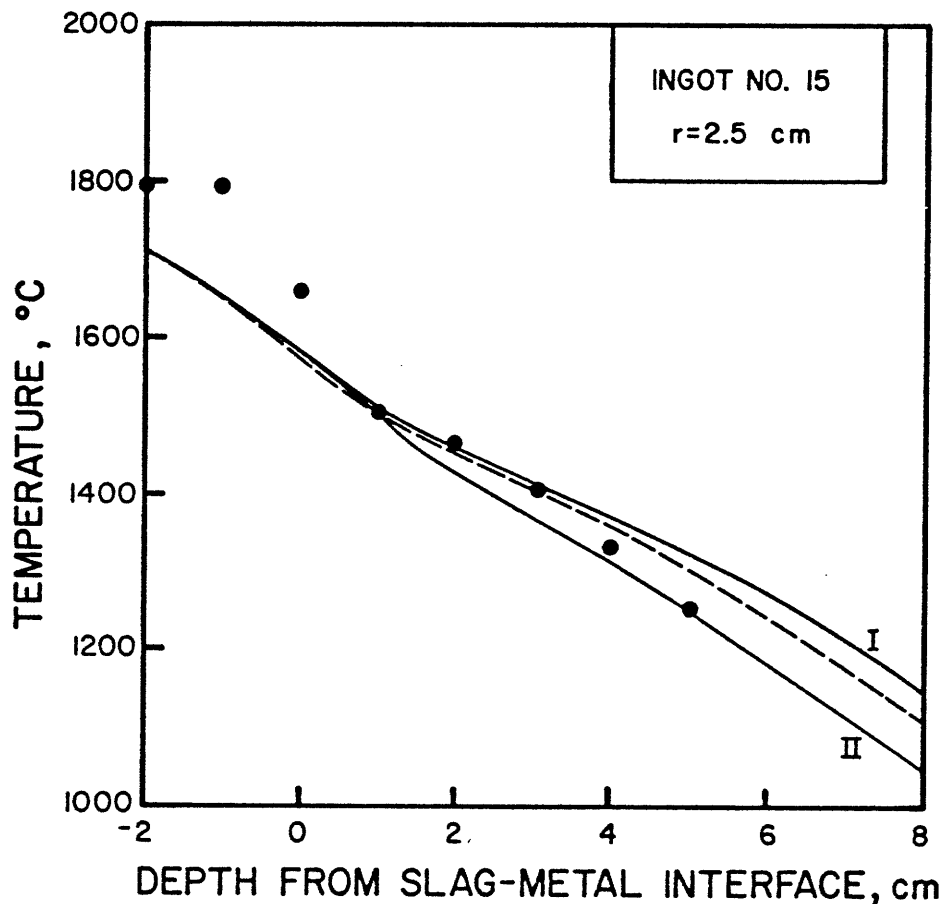
The effect of a solidified slag crust on the submerged, curved surface of the electrode will be analogous to the effect of a reduced fill ratio since the effective c.s.area for current will decrease. Then, from discussions given in connection with Fig. 5.8, for the same total current, power requirement will be higher for this case and the current distribution will be less uniform. From the preceding discussions, the presence of a solidified slag crust on the electrode will be expected to increase the velocity in the slag. These observations are confirmed by calculations reported by Dilawari and Szekely ^{14,59}.

5.4.2 Computed results on fluid flow and heat transfer

Results will now be presented for the temperature and velocity distributions in the system. Computed results on the temperature distribution will be compared with the limited measurements available.

It is noted that most of the calculations were carried out using a constant electrical conductivity of the slag. In some calculations, however, an allowance has been made for the temperature dependence of the electrical conductivity of the slag. The modifications required to the governing equations in order to accomplish this are discussed in Appendix D.

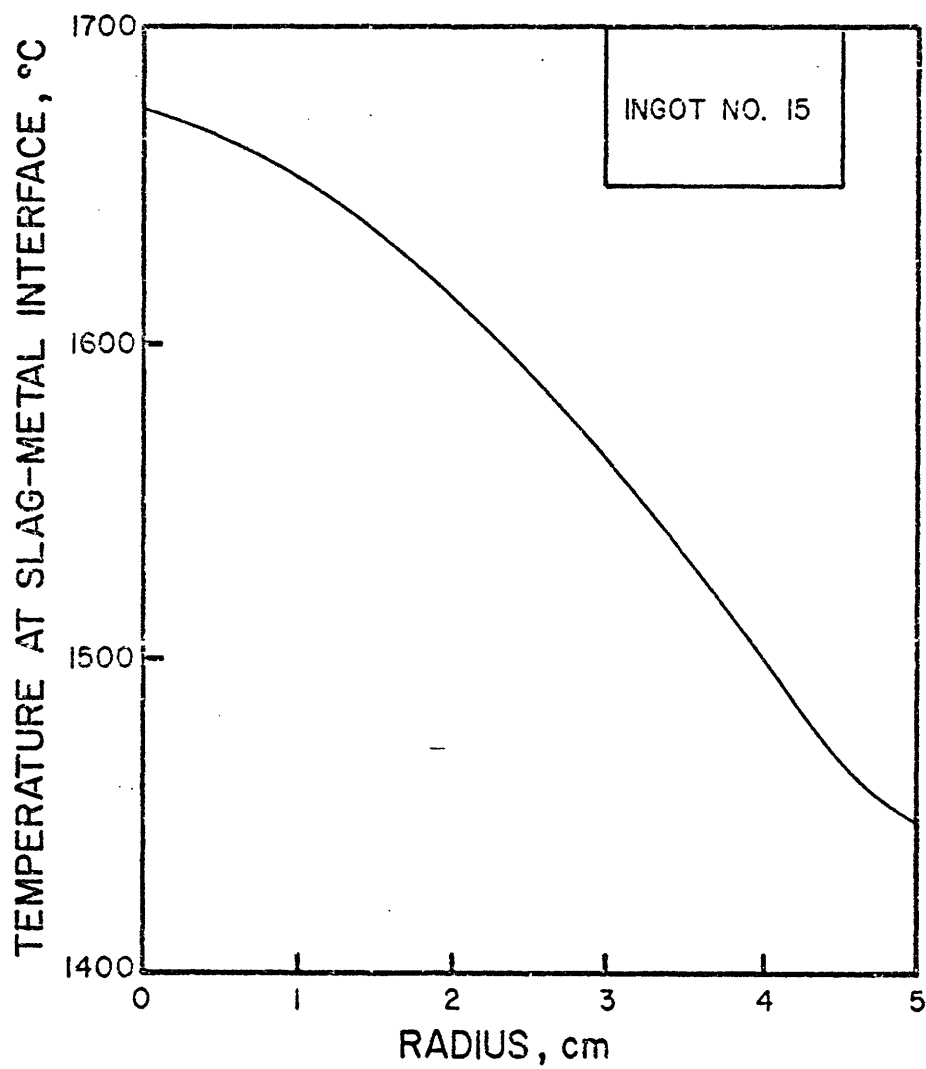
Fig. 5.9 shows a comparison between the experimentally measured axial temperature profile at a radial position $r = 0.025$ m and those predicted from the model. The discrete data points denote measurements, the broken line denotes predictions for the condition where the experimentally measured casting rate was used as an input to the model. The two solid lines denote predictions for the condition when the casting rate was computed from the model; curve I refers to calculations using a uniform electrical conductivity in the slag while curve II refers to calculations using a temperature dependent electrical conductivity in the slag. As discussed in Appendix D, temperature dependence of the electrical conductivity used in the calculations was deduced from experimental measurements reported by Mitchell and Cameron⁶⁰. Power input in both the cases is kept the same (73 kW). It is seen that measurements correspond to a steeper axial temperature gradient in the vicinity of slag-metal interface than that



- 5.9 Computed and measured axial temperature profiles for ingot 15 (rms current = 1.7 kA) at $r = 2.5$ cm;
- casting rate (V_c) calculated from the model
 - I uniform electrical conductivity in slag
 - II temperature dependent electrical conductivity in slag
 - experimentally measured value of V_c (0.74 m/hr) used as an input to the model
 - measured values from Mellberg ⁵⁷

exhibited by the calculated results. This, as pointed out by Melberg, may partly be due to inaccuracies involved in experimentally defining the zero position. In general, all three curves shown in Fig. 5.9 provide a reasonable representation of the data points below the slag-metal interface. Curve II provides a somewhat better agreement with measurements primarily because in this case, calculated casting rate (0.7 m/hr) and effective thermal conductivity in the metal pool (27 W/mK) are lower than the corresponding values for case I (casting rate = 0.76 m/hr, effective thermal conductivity in metal pool = 30 W/mK).

One important derived quantity in these calculations is the radial temperature distribution at the slag-metal interface. Since there is not much difference in the three cases cited in Fig. 5.9, only the distribution for case I is discussed. This is shown in Fig. 5.10. As seen here there is quite an appreciable radial variation in the temperature (about 225°C in the present case). It is noted that several authors, when modelling pool profiles and the temperature fields in the ingot, used the temperature at the slag-metal interface as an arbitrarily adjustable boundary condition. The choice of this boundary condition may be critical, because this represents the coupling between the heat source in the slag and the heat transfer processes that take place within the ingot.



5.10 Computed temperature distribution at the slag-metal interface for ingot 15.

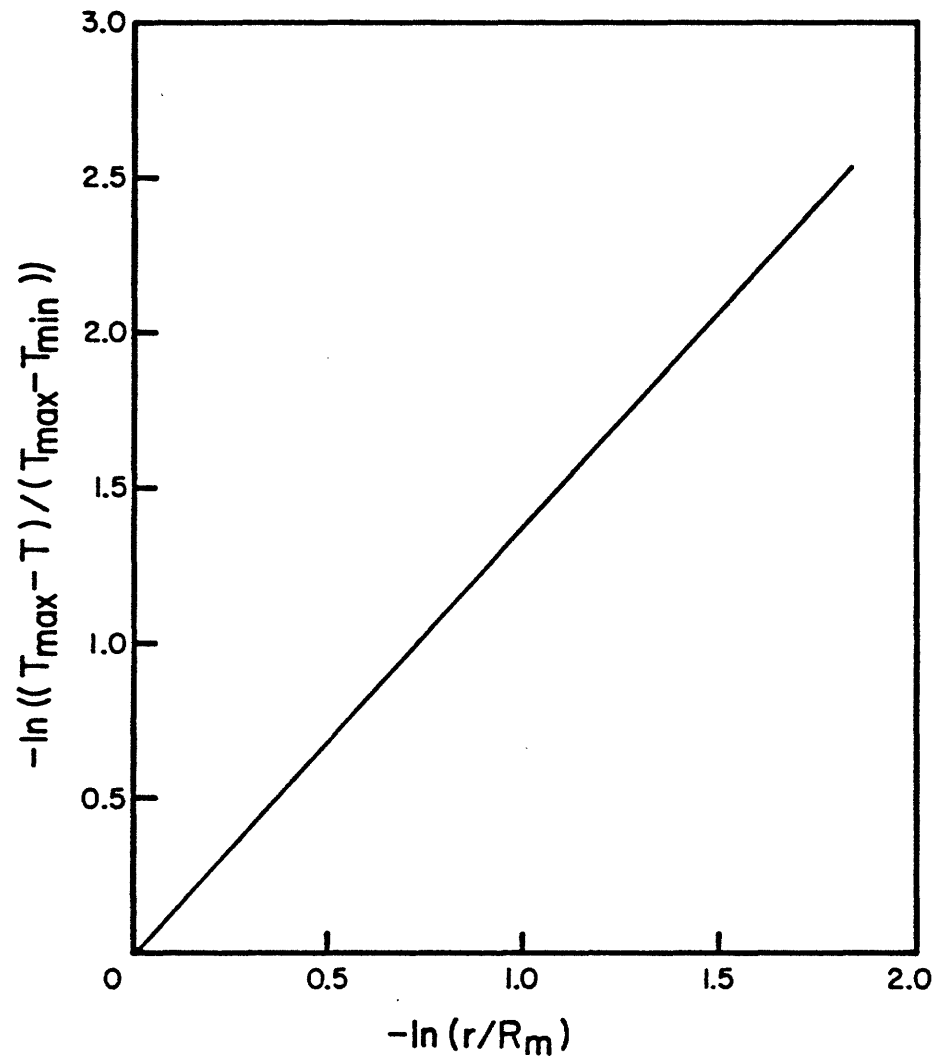
Fig. 5.11 shows an alternative way of expressing the radial distribution of temperature at the slag-metal interface. Here, $\ln\left(\frac{T_{\max} - T}{T_{\max} - T_{\min}}\right)$ is shown plotted against $\ln\left(\frac{r}{R_m}\right)$ where T_{\max} and T_{\min} are the maximum (1675°C) and the minimum (1450°C) temperatures respectively and R_m is the radius of the mold. From this figure, it can be shown that

$$\frac{T_{\max} - T}{T_{\max} - T_{\min}} \approx \left(\frac{r}{R_m}\right)^{1.375} \quad (5.2)$$

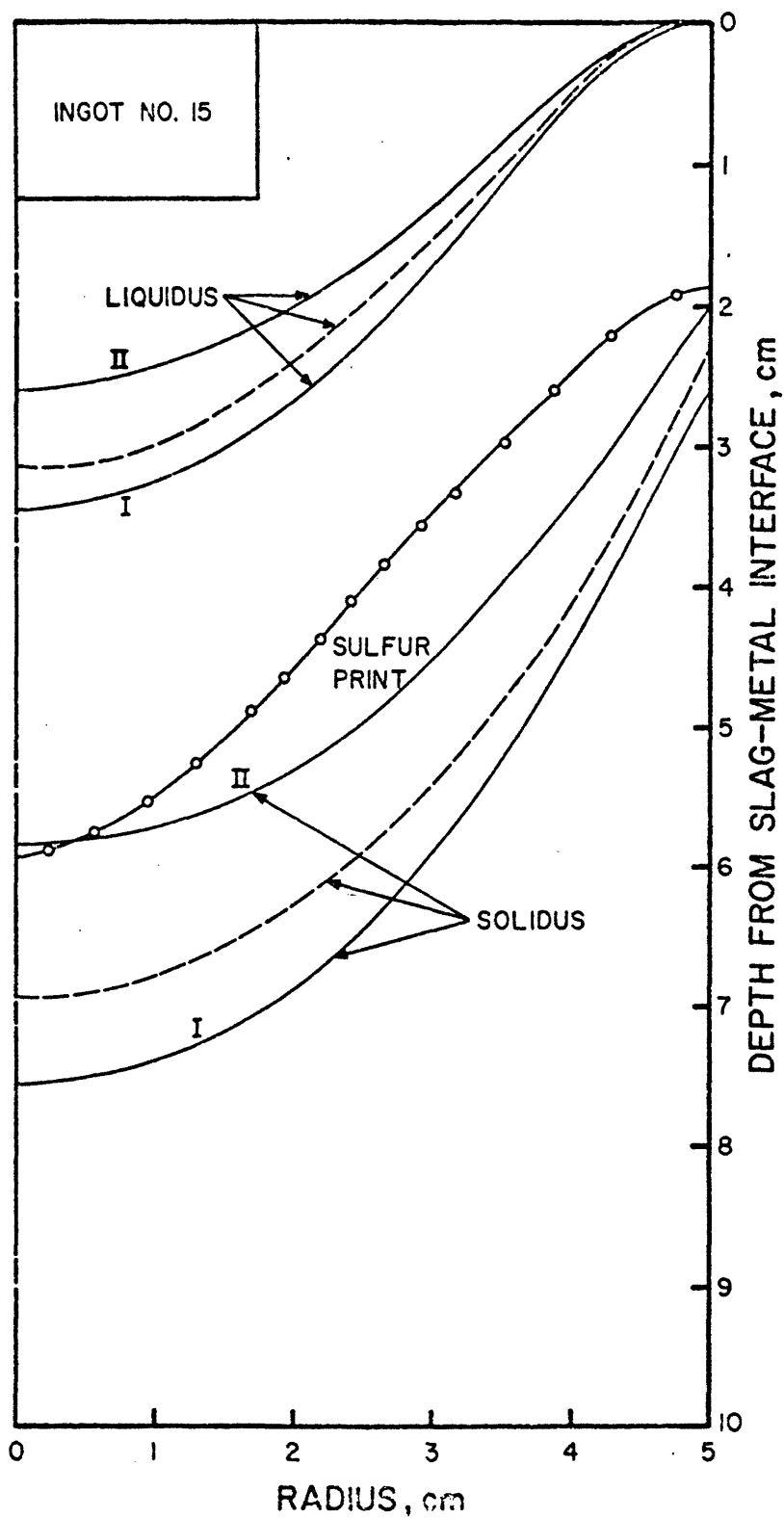
This type of relationship has been used by other authors to specify temperature distribution at the top of the ingot.

Fig. 5.12 shows the computed solidus and liquidus isotherms for the three cases that were represented in the previously given Fig. 5.9. Also shown, for the sake of comparison is a sulfur print reported by Mellberg, for corresponding operating conditions. It is seen that the sulfur print falls between the solidus and the liquidus curves, as one would expect. As before, curve II which represents computation with a temperature dependent electrical conductivity in the slag gives a closer agreement with the experimental measurements.

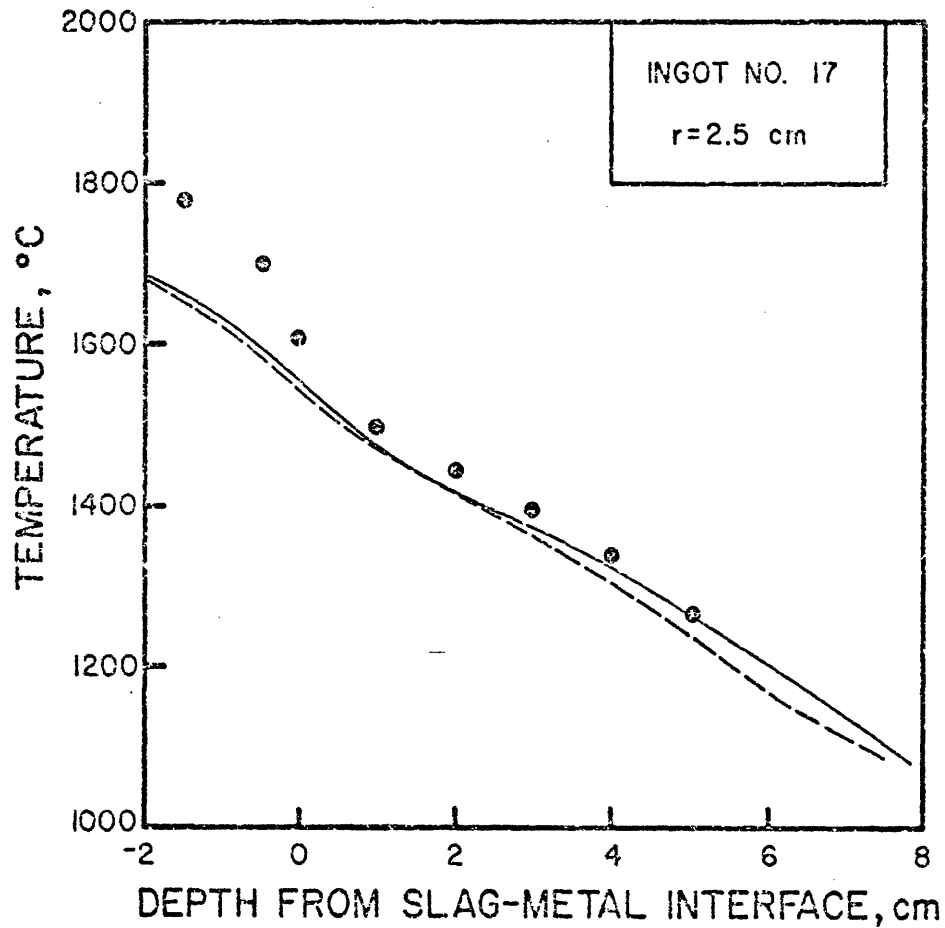
Fig. 5.13 shows a comparison between the experimentally measured and the theoretically predicted temperature profiles, for an ingot produced with a 1.55 kA current, at



5.11 Results from Fig. 5.10 expressed in an alternative way.



5.12 Computed liquidus and solidus isotherms for ingot 15.
 -0- sulfur print from Mellberg⁵⁷, rest of legends
 same as in Fig. 5.9.

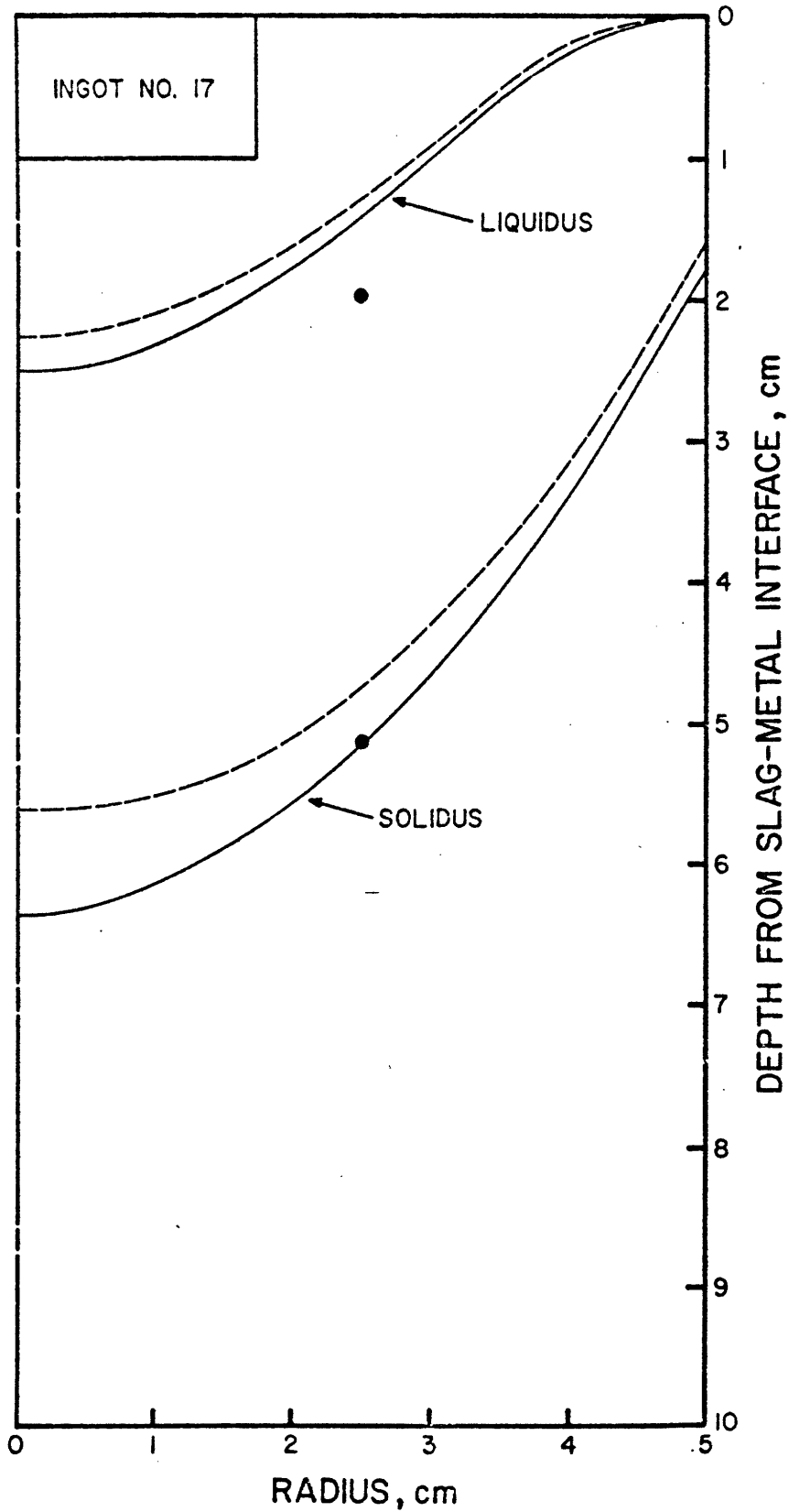


5.13 Computed and measured axial temperature profiles for ingot 17.

- casting rate (V_c) calculated from the model
- experimentally measured value of V_c (0.62 m/hr) used as an input to the model
- measured values from Mellberg⁵⁷

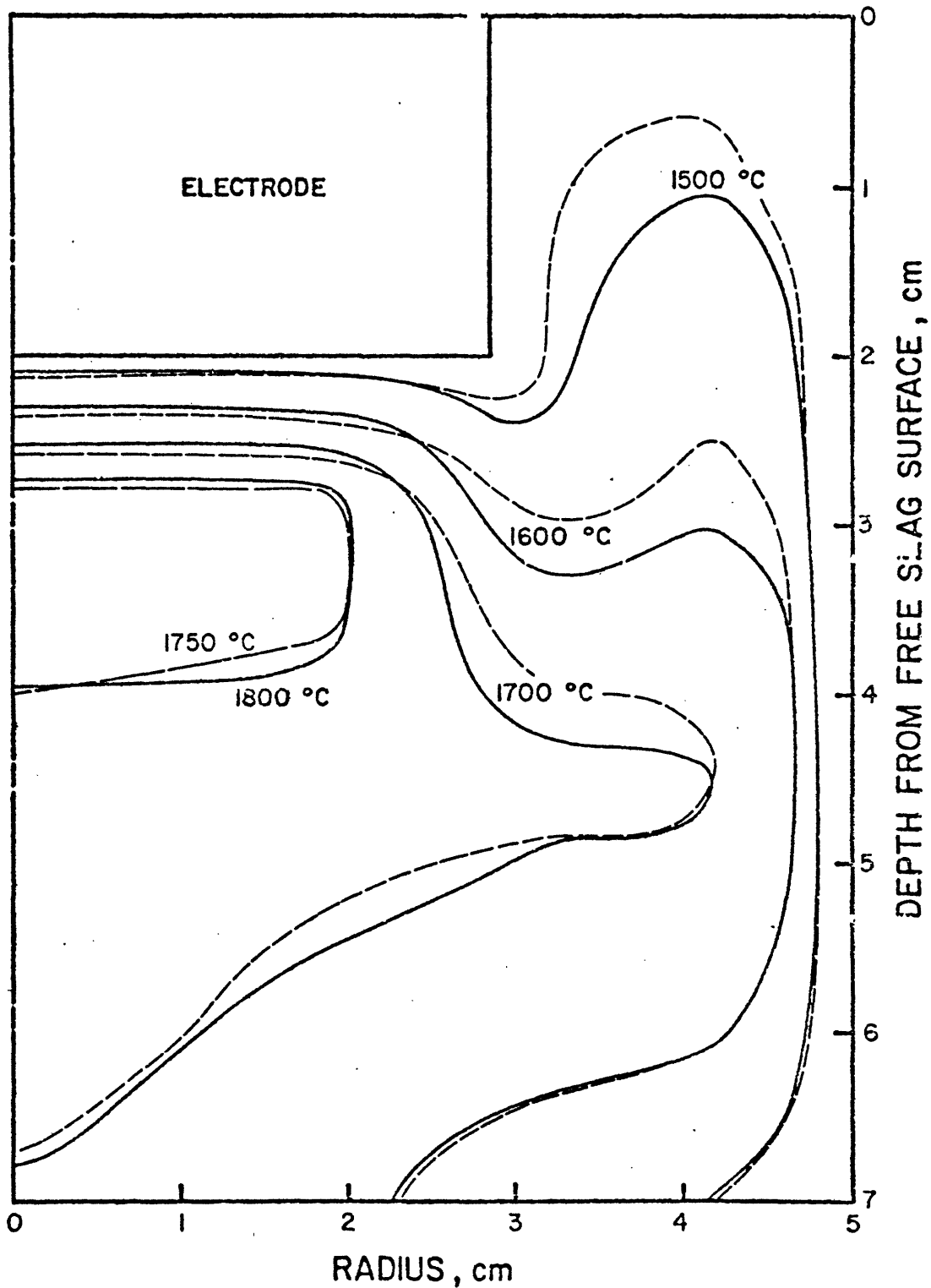
the mid-radius position. Here again the solid line represents the predictions for a condition, when the casting rate was computed, while the broken line corresponds to predictions, where the experimentally determined casting rate was used as an input for the model. It is seen once again that there is reasonably good agreement between the measurements and the predictions below the slag-metal interface. The computed liquidus and solidus isotherms for these two cases are shown in Fig. 5.14. Also given for the purpose of comparison are some of the measured locations of the isotherms. It is seen that the solidus and the liquidus lines predicted by the two techniques are comparable, and that there is a somewhat better agreement between measurements and predictions for the case in which the casting rate is calculated from the model (0.64 m/hr vs. measured value of 0.62 m/hr).

Fig. 5.15 shows the computed isotherms in the slag for ingot 15. The solid lines represent calculations with a uniform electrical conductivity of the slag while the broken lines represent calculations with a temperature dependent electrical conductivity. As seen here, the latter case gives a lower maximum temperature (1787 °C vs. 1832 °C for the former case) with a little more uniform distribution. This is as expected since the electrical conductivity of the slag increases with temperature. It is seen that the



5.14 Computed liquidus and solidus isotherms for ingot 17.

Legends same as in Fig. 5.13.



5.15. Computed isotherms in slag for ingot 15.

- uniform electrical conductivity in slag
- temperature dependent electrical conductivity in slag

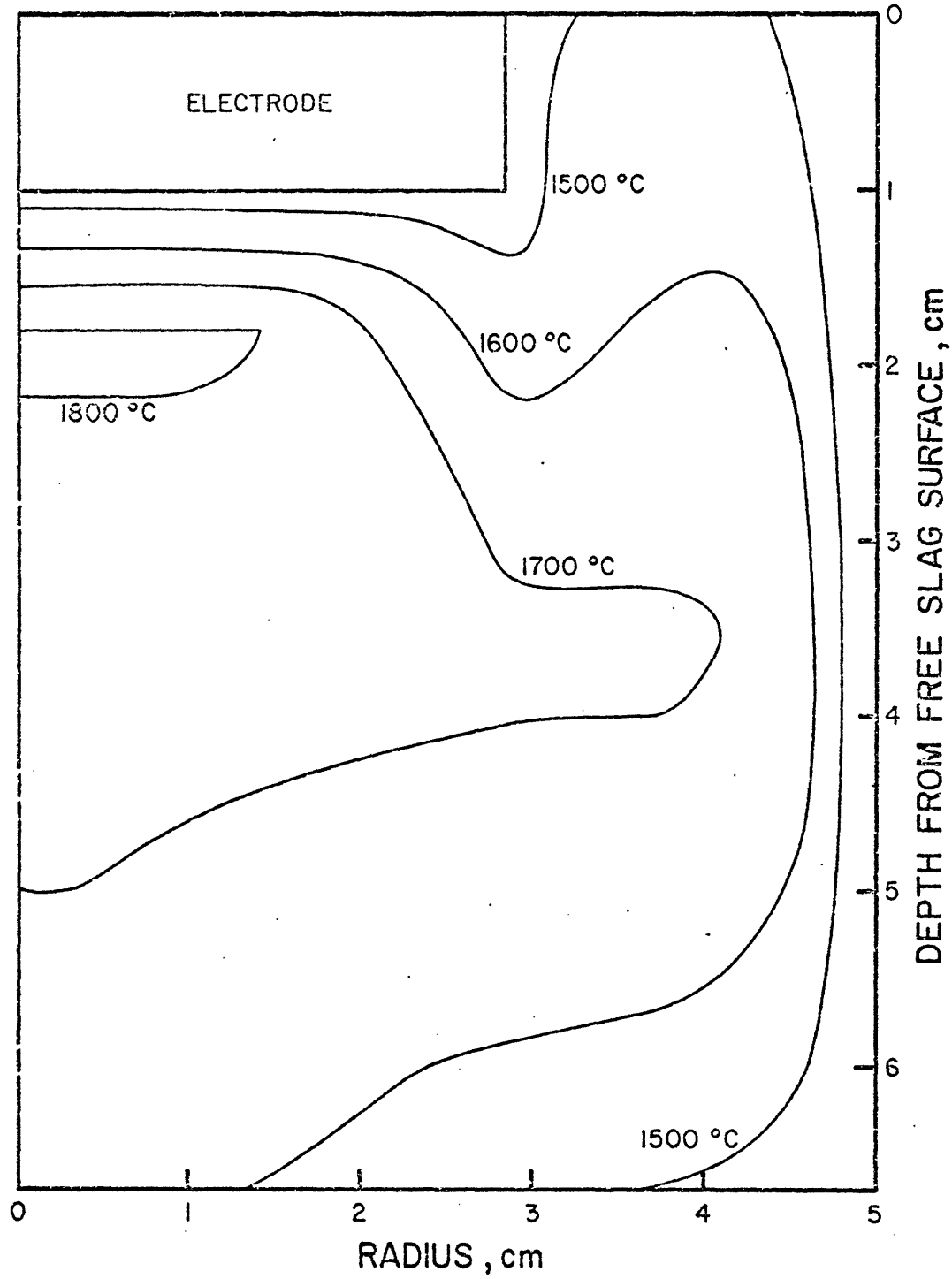
hottest region of the system is in the central portion, close to the electrode, but not in the immediate vicinity of the electrode.

It has to be stressed that at the surface of the electrode the temperature in the slag must equal the melting point of the electrode material, hence the positive axial temperature gradient in the immediate vicinity of the electrode. This positive axial temperature gradient is also consistent with the physical requirement that thermal energy has to be transferred from the slag to the electrode.

It should be noted that the temperature profiles depicted in Fig. 5.15 result from the combined effect of Joule heating and the convective fluid flow field in the slag phase. If convection had been neglected, one would have obtained unrealistically high temperatures in the vicinity of the electrode surface. An important effect of this convection, readily seen in Fig. 5.15, is the quite uniform temperature field in the central core of the slag; indeed, most of the temperature gradients appear to be confined to the vicinity of the wall.

This knowledge of the temperature field is of course quite important, if we wish to represent chemical reactions between the droplets and the slag, that may be temperature dependent.

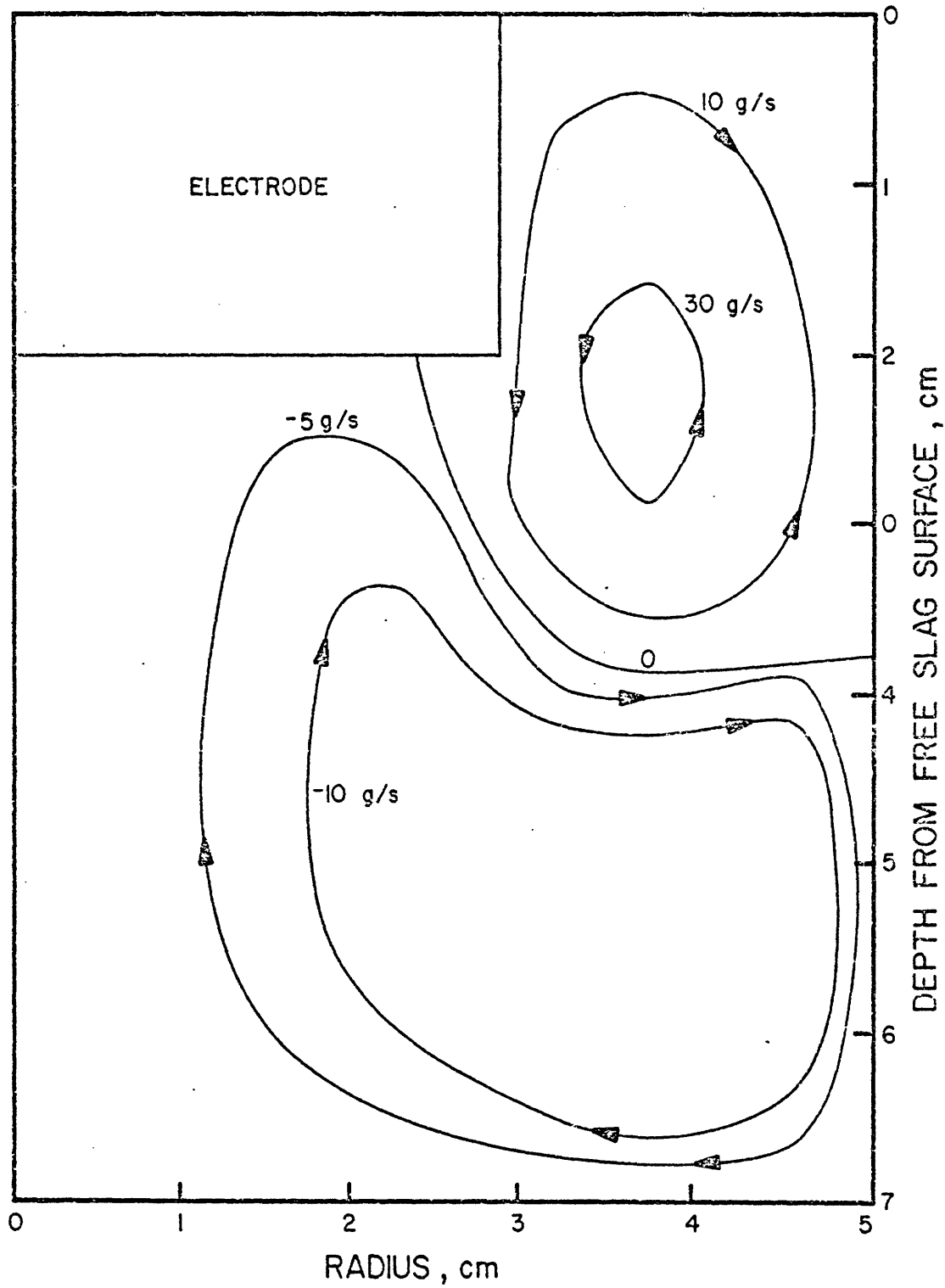
Fig. 5.16 shows the effect of electrode penetration depth in the slag on the isotherms in the slag. The isotherms shown here are computed for an electrode penetration depth of 0.01 m. The amount of slag used (1.5 kg), the input power (73 kW) and the value used for the effective thermal conductivity in the metal pool (30 W/mK) are the same as in the case of Fig. 5.15. Comparing Figures 5.15 and 5.16 reveals that the temperatures in the bulk portion of the slag below the electrode are somewhat reduced when a lower electrode penetration depth is used (maximum temperature 1807 °C vs. 1832 °C for the other case). This is to be expected from the discussions given in connection with Fig. 5.6 where it was shown that a lower penetration depth resulted in a lower volumetric heat generation rate in the bulk portion of the slag. Also the casting rate is now reduced (0.61 m/hr vs. 0.76 m/hr for the other case). As is to be expected from the discussion given in connection with Fig. 5.9, the agreement with measured temperatures below the slag-metal interface was somewhat better. However, the temperature profiles in the ingot are not shown here, for the sake of brevity. Although the immersion depth of the electrode appears to have an important effect on the casting rate and hence on the position of liquidus and solidus isotherms, its effect on the temperature and velocity in



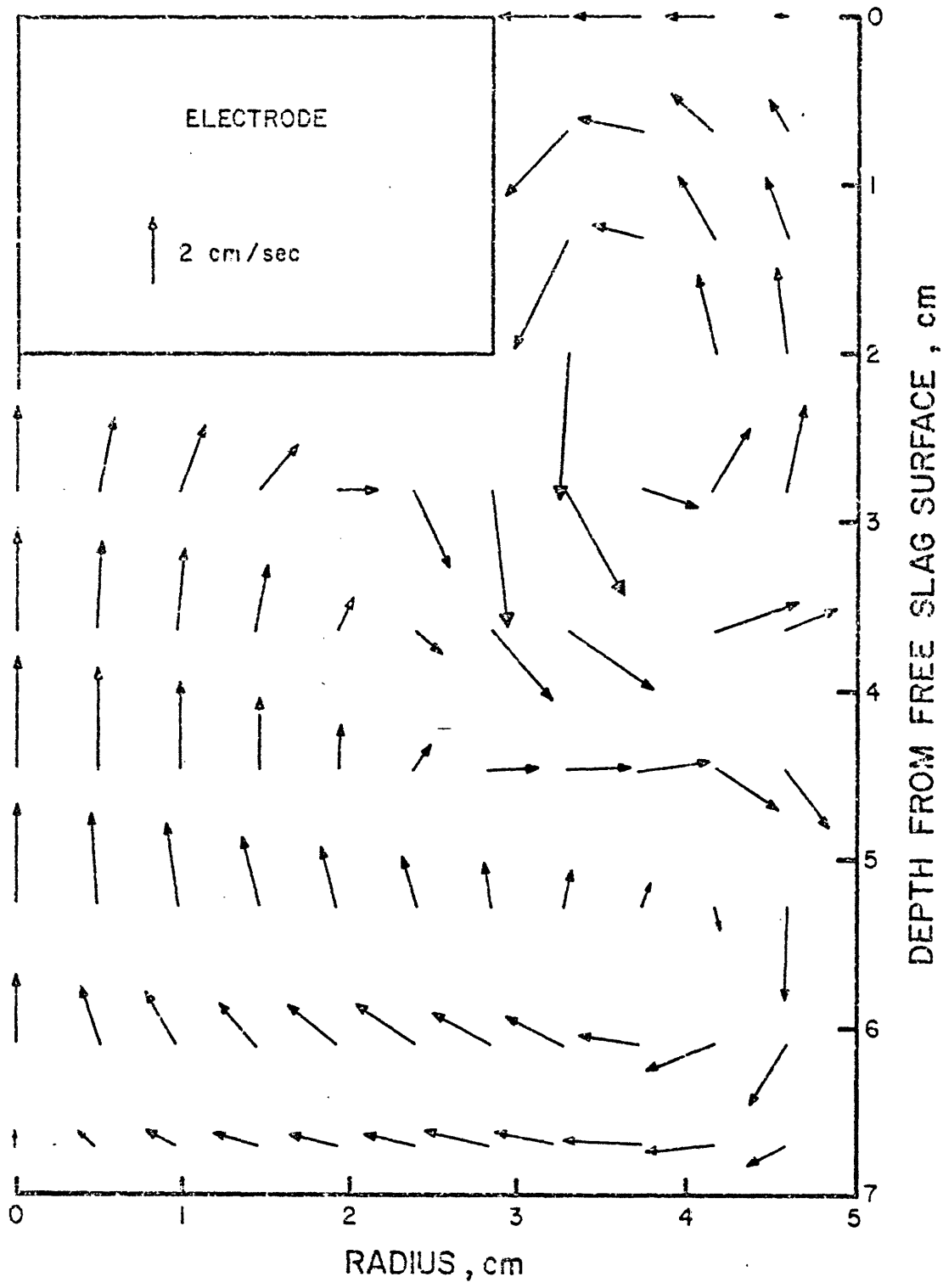
5.16 The effect of electrode penetration depth on temperature distribution in the slag.

the slag is less significant from the global viewpoint. Also, it should be noted that in practice, the immersion depth of the electrode is determined by the process itself. However, this aspect of the ESR process is yet to be modelled.

In the next few figures, calculated results on the flow and turbulent mixing in the slag are discussed. Fig. 5.17 shows the calculated stream lines in the slag for ingot 15. Computed velocity vectors in the slag are presented in Fig. 5.18. It follows from the discussions given in Chapter III that there are two principal forces that drive fluid motion in the slag -- the electromagnetic force field which in the present case would tend to generate an anti-clockwise circulation pattern and the buoyancy force field, which would tend to generate a clockwise circulation pattern in the bulk of the slag. It is seen in Figs. 5.17 and 5.18 that for the case considered, buoyancy forces tend to dominate in the bulk of the slag, producing a clockwise circulation pattern. The anti-clockwise circulation pattern in the annular space between the electrode and the mold results from the combined effects of buoyancy and electromagnetic forces (if buoyancy forces alone acted in the region one would obtain two circulating loops, as caused by a hotter fluid being located between the two cold surfaces, viz the electrode and



5.17 Computed streamline pattern in slag for ingot 15.



5.18 Computed velocity vectors in slag for operation with 1.7 kA and for a fill ratio of 0.325.

the mold wall). The absolute magnitude of the velocities calculated for the system, viz 0 - 5 cm/s are comparable to computed values reported in earlier papers describing fluid flow in ESR process ¹³⁻¹⁵.

The circulation is an important characteristic of ESR systems and it would be desirable to define the conditions under which either the electromagnetic or the buoyancy forces dominate the flow field. By dimensional arguments it may be shown that the following group may be used to define the nature of the circulation:

$$\phi = \frac{\mu_0 \bar{I}_0^2 (1 - \frac{A_e}{A_m})}{4\pi A_e L \rho \beta g \Delta T} \quad (5.3)$$

where A_e and A_m are the cross sectional areas of the electrode and the mold respectively, L is the depth of the slag below the electrode, and \bar{I}_0 is the rms value of the total current.

The higher the value of ϕ the stronger is the domination of the electromagnetic forces. Thus the relative importance of electromagnetic stirring is increased by increasing the current, decreasing the fill ratio and decreasing the slag depth below the electrode.

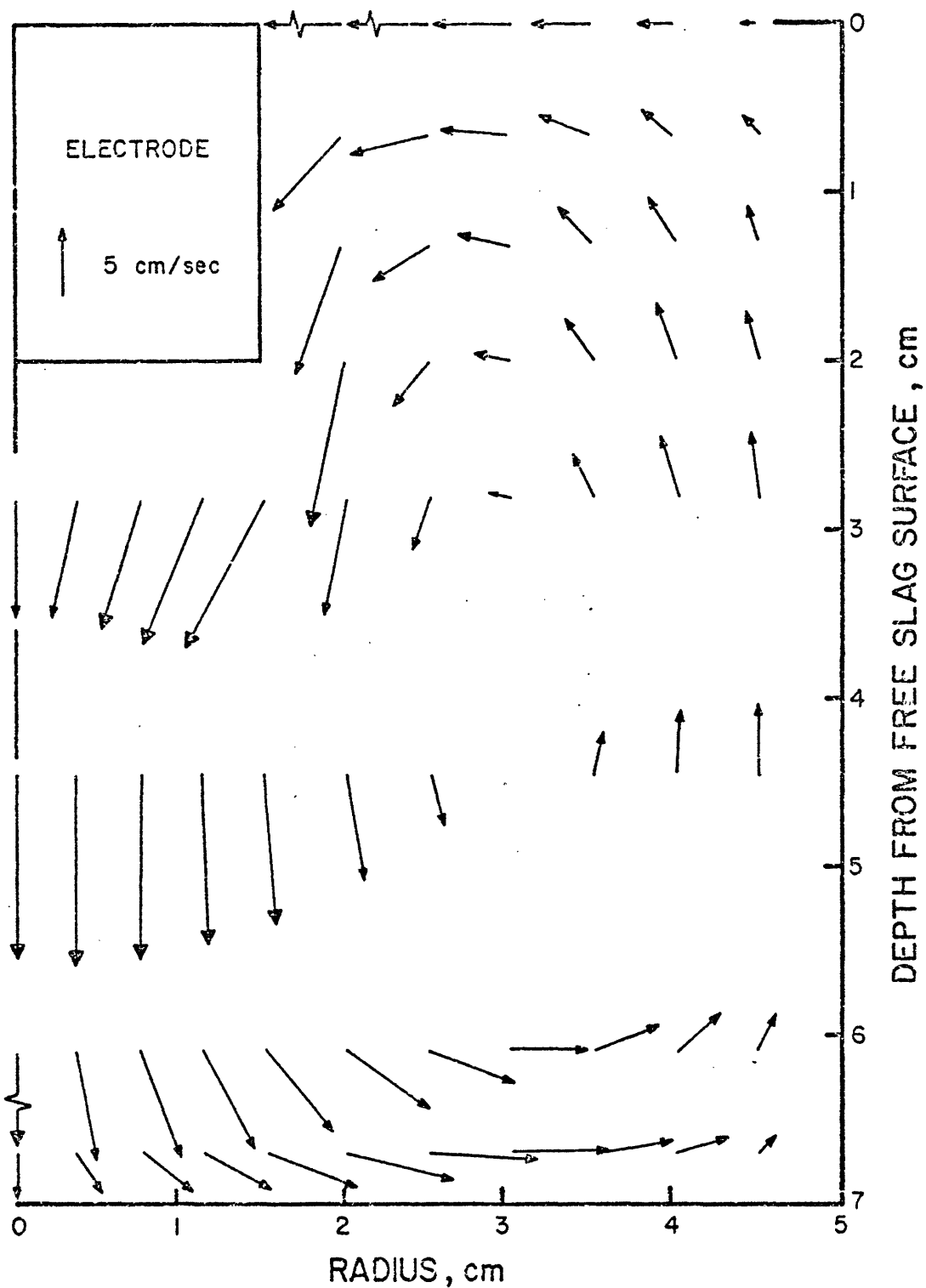
These findings seem reasonable on physical grounds, because a diverging current field will produce a stronger $J \times B$ force. Extreme examples of this have been found in electroslag welding, using wire electrodes.

Figure 5.19 shows the velocity field computed for an identical current to Fig. 5.18 but for a greatly reduced fill ratio (0.09 as opposed to 0.32 in the previous case). It is clearly seen that under these conditions the flow is now dominated by electromagnetic forces. Also as expected from discussions given in connection with Fig. 5.8, the magnitude of the velocity increases when the fill ratio is decreased.

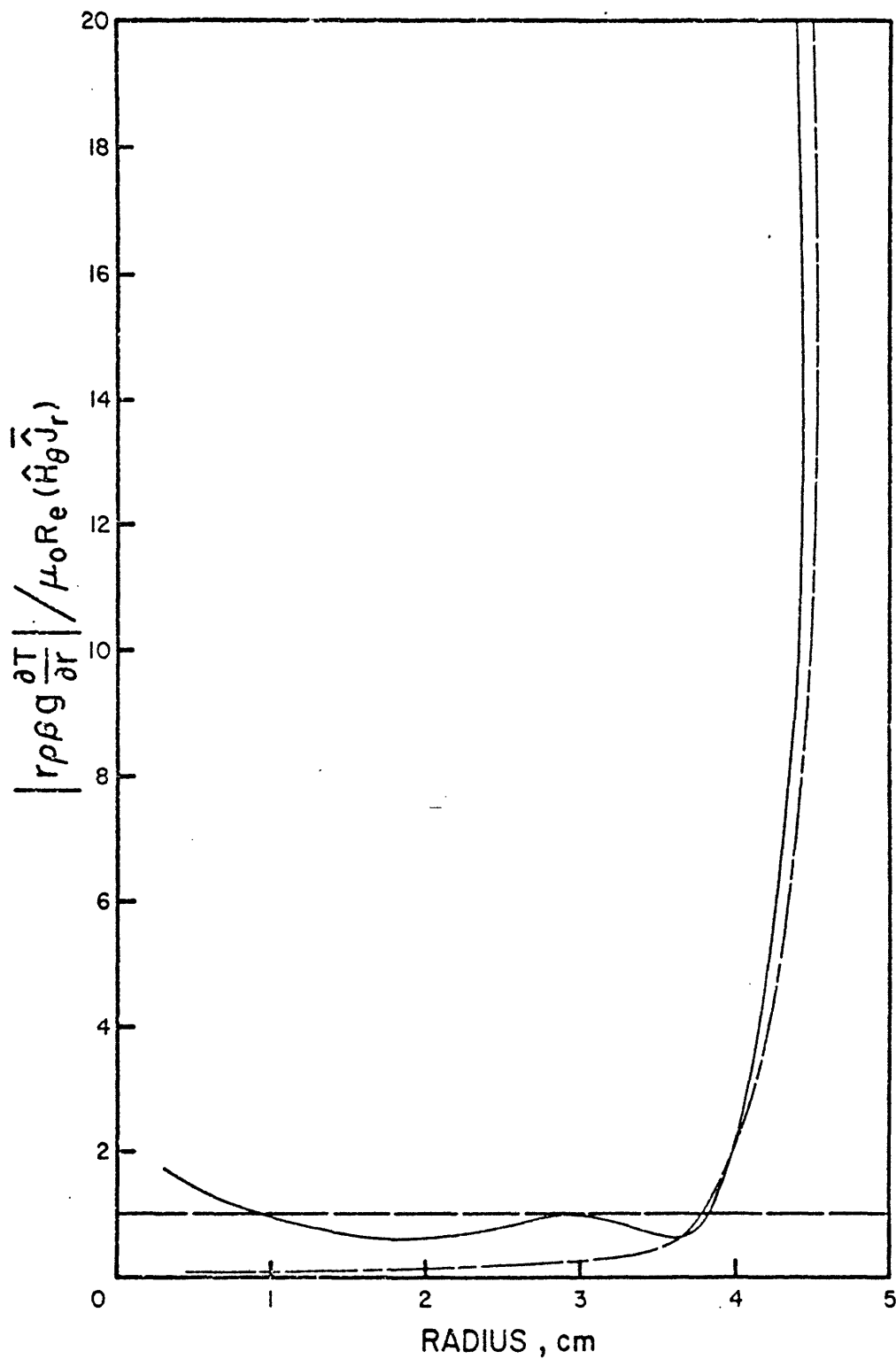
Fig. 5.20 shows the radial distribution of the ratio of buoyancy/electromagnetic contributions to vorticity, some 0.02 m below the electrode, computed for the cases that have been given in Figs. 5.18 and 5.19.

It is seen that buoyancy forces dominate in the vicinity of the walls because of the very steep radial temperature gradients. However, the curve drawn with the broken line, depicting the behavior of the system shown in Fig. 5.19 clearly indicates that the electromagnetic forces dominate in the central core for that case.

Fig. 5.21 shows the computed values for the turbulence kinetic energy in the slag for ingot 15. The maximum value for this parameter occurs in the annular space between the electrode and the mold and this value

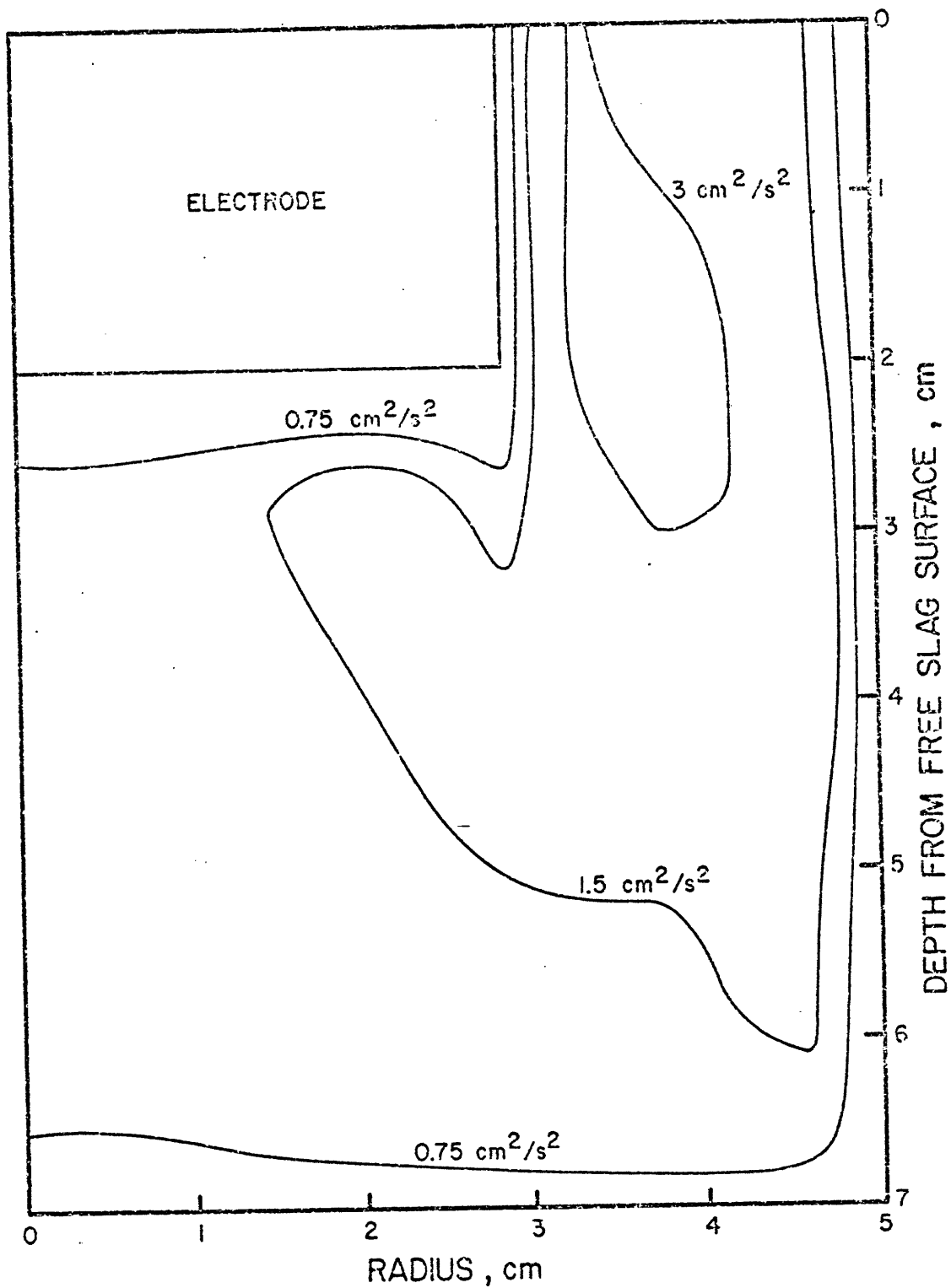


5.19 Computed velocity vectors in slag for operation with 1.7 kA and for a fill ratio of 0.09.



5.20 Radial distribution of buoyancy/electromagnetic contributions to vorticity, 2 cm below the electrode.

— 1.7 kA, $A_e/A_m = 0.325$, ϕ [Eq.(5.3)] = 1.75
 --- 1.7 kA, $A_e/A_m = 0.09$, ϕ [Eq.(5.3)] = 15

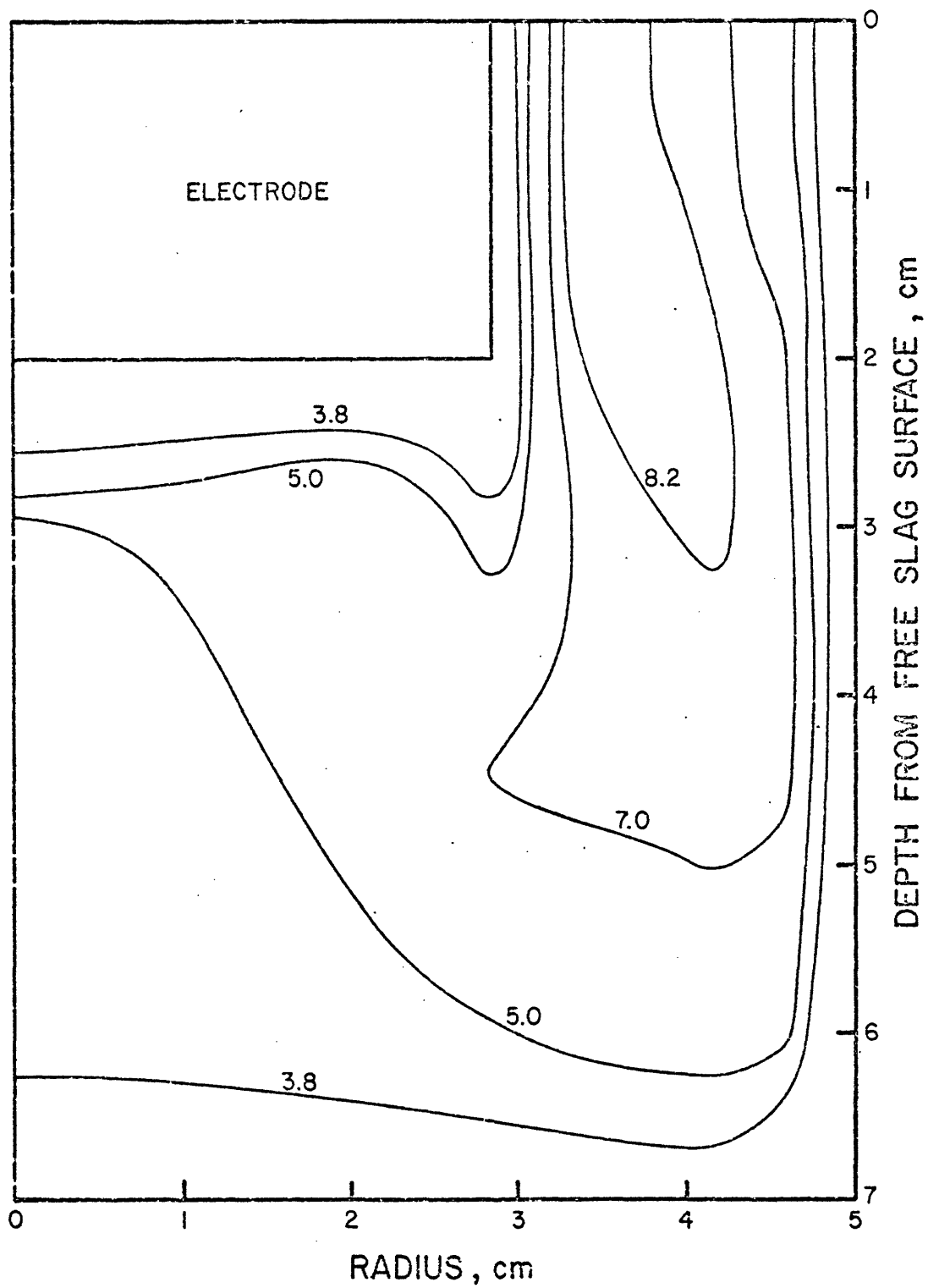


5.21 Computed distribution of turbulence kinetic energy in the slag for ingot 15.

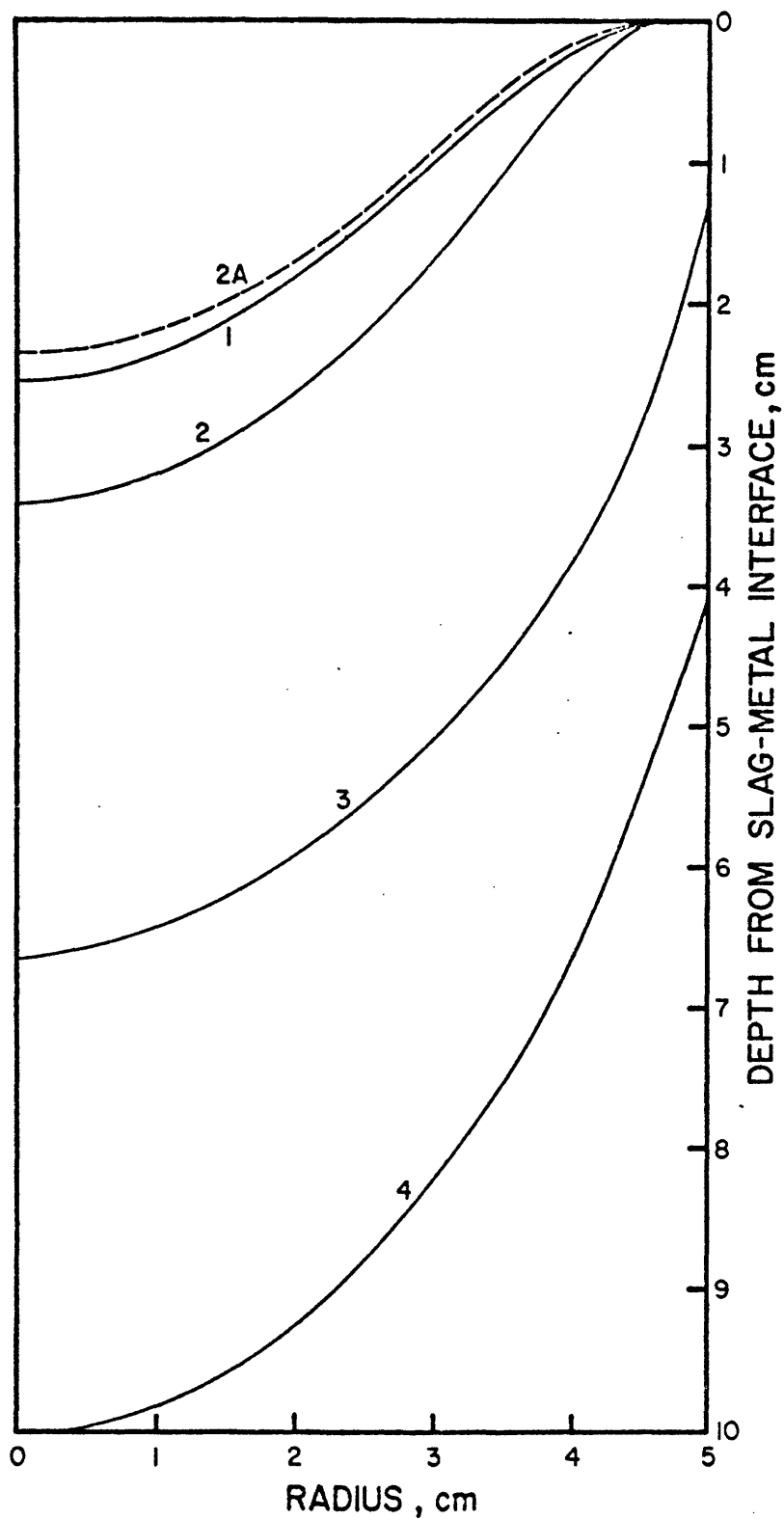
is about 25% of the maximum kinetic energy of the mean motion.

Fig. 5.22 shows a plot of the ratio: effective thermal conductivity/atomic thermal conductivity in the slag for ingot 15. It is seen that the strong convective field does indeed produce turbulent conditions, corresponding to an appreciable enhancement of the effective thermal conductivity. As in the case of Fig. 5.21, the regions of the maximum effective conductivity correspond to the zones where the circulation has its maximum intensity -- a behavior that is consistent with physical reasoning.

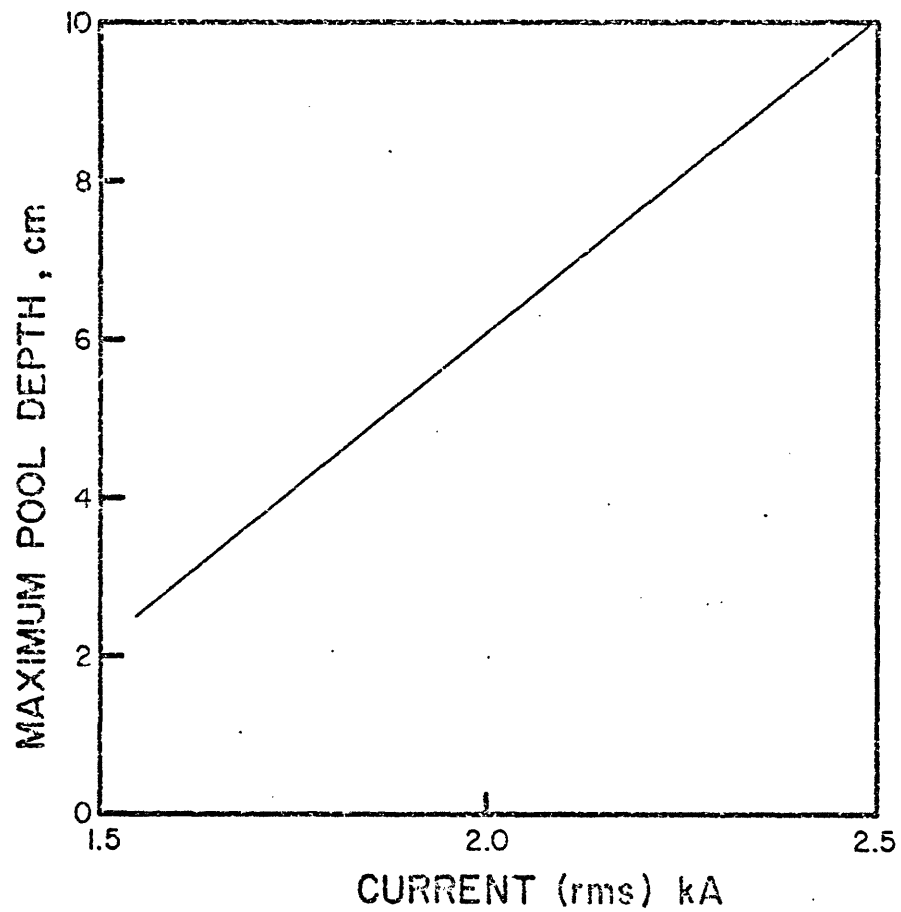
The role of the current in determining the shape and the depth of the metal pool is examined in Figs. 5.23 and 5.24. Fig. 5.23 shows computed pool profiles for different current levels. The curves, drawn with the solid line, show that the higher the current, the deeper the pool profile. This finding has been established experimentally a long time ago; however, this is the first time that these experimental findings have been predicated from first principles. The curve drawn with the broken line (2A) depicts the computed pool profile



5.22 Computed contours of the ratio effective thermal conductivity/atomic thermal conductivity in the slag for ingot 15.



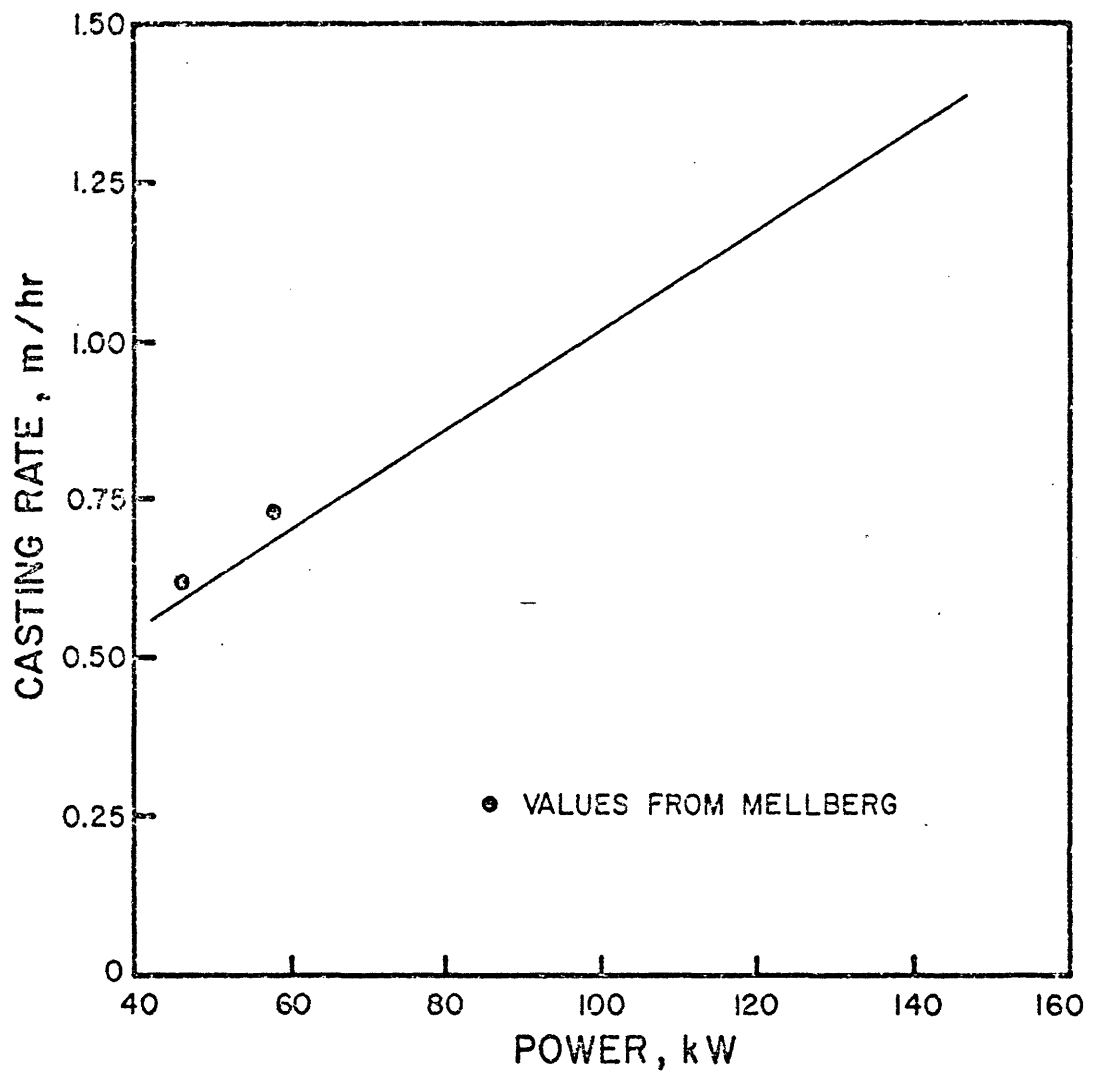
5.23 Computed metal pool depths for different currents.
 1. 1.55 kA, 2. 1.7 kA, 3. 2.0 kA, 4. 2.5 kA
 In all these cases amount of slag = 1.5 kg.
 2A. Same power as 2 (73 kW), amount of slag = 1.9 kg.



5.24 Variation of maximum pool depth with current.

for identical conditions of power to that given by (2) but for a greater amount of slag present (1.9 kg for the case 2A vs. 1.5 for the case 2). Heat loss from the slag to the mold wall for the case 2A was 30% higher than that for the case 2. This resulted in a smaller pool depth. Fig. 5.24 shows a plot of the computed maximum pool depth against the current used. Over the range examined the relationship is found to be linear. Fig. 5.25 shows a comparison between the theoretically predicted casting rates, as a function of power and the values reported experimentally by Mellberg⁵⁷. It is seen that the agreement is not unreasonable. The predicted relationship between the casting rate and the power is linear. This again is consistent with operating experience⁶².

Values for the parameters associated with a metal droplet are shown in Table 5.5. The superheat given this table is for operation with 1.7 kA (i.e. ingot 15). As seen here, the residence time of the droplet in the slag is very small. The average velocity of a droplet (0.28 m/s) is substantially larger than the velocity of slag and therefore the assumption of a quiescent slag made in calculating droplet para-



5.25 Variation of casting rate with power
• measured values from Mellberg⁵⁷.

Table 5.5 Values for Droplet Parameters

Parameter	Values
diameter, d_d	1.3 cm
residence time, τ	0.18 s
average velocity, U_{av}	28 cm/s
superheat, $(T_f - T_{m,e})$	72 °C

meters (Section 3.5.4B) is reasonable.

This concludes the discussions of the computed results. The results presented in this chapter were selected to illustrate the predictive capability of the model developed in this work, and to investigate the interdependence of key process parameters. Concluding remarks are made in the next chapter.

CHAPTER VI

CONCLUSIONS AND SUGGESTIONS FOR FURTHER WORK

In this chapter concluding remarks are made and some suggestions are made for further work in mathematical modelling of ESR process.

6.1 Conclusions

In the work reported in this thesis a mathematical model has been developed to describe electromagnetic field, fluid flow, heat transfer and solidification phenomena in ESR systems. The model involved the simultaneous statement of Maxwell's equations, equations for turbulent flow and the differential thermal energy balance equations. These equations were first written in vectorial forms so that some general conclusions could be drawn regarding the behavior of ESR systems. Then the equations were presented in the cylindrical coordinate system with axial symmetry. The limitations of the model are inherent in the assumptions made in developing the model. While these assumptions are detailed in Section 3.3, some of the principal shortcomings of the model in its present form are as follows:

- (1) Fluid flow equations are solved in the slag only. Motion in the metal pool is accounted for by using an effective thermal conductivity. However, as discussed in section 5.2, an attempt is made to deduce this parameter in the model itself.

(2) The model assumes a predetermined shape (flat) for the melting tip of the electrode and a known electrode penetration depth in the slag. Ideally these parameters should be calculated using the mathematical model. However, this refinement can be made only if a more realistic understanding is developed of the melting process.

(3) A constant value is used for the electrical conductivity of the slag. In some of the calculations presented in Chapter 5, an approximate allowance has been made for the temperature dependence of this parameter.

(4) Effects associated with chemical and electrochemical reactions are not considered.

On the positive side, the model accomplishes the following:

(1) It allows for turbulent flow in slag as caused by both electromagnetic and natural convection forces.

(2) It accounts for the spatial distribution of heat generation rate, the transport of heat by the metal droplets falling through the slag and for the movements of the ingot and the electrode.

(3) By integrating transport processes taking place in different portions of an ESR system, the model allows predictive relationships to be developed among key process parameters.

The governing differential equations developed in Chapter III were solved using a numerical

technique outlined in Chapter IV to provide current distribution, velocity and temperature profiles for a laboratory scale system used by Mellberg⁵⁷. In general the theoretical predictions for the temperature profiles and for the pool profiles were found to be in reasonable agreement with the experimental measurements, thereby indicating experimental support for the model.

The predictive capacity which is inherent in this model enables one to develop theoretical relationships predicting the interdependence of the key process parameters. For example, it has been possible to relate the heat generation pattern, the temperature and the velocity fields, the melting rate and the pool profiles to the operating power and current and to the geometry of the system.

The principal findings may be summarized as follows:

(1) The temperature at the slag-metal interface was found to be strongly spatially dependent. As seen from the work reported by Kreyenberg and Schwerdtfeger¹⁶, the computed temperature and velocity distributions in the slag are strongly affected by the assumed temperature distribution at this interface and therefore it should be computed by the model rather than being specified arbitrarily.

(2) It was found that for a fixed geometry, the higher the current, the deeper was the pool profile; this

mode of operation also resulted in a faster casting rate. Over the range of parameters used in the computation, the relationship between maximum pool depth and the current and the relationship between casting rate and power were found to be linear.

(3) A deeper slag bath results in a larger heat loss through the mold wall. Thus for the same input power, a larger amount of slag gives rise to a lower pool depth.

(4) The depth of penetration of the electrode was found to have some effect on the slag temperature; more specifically the lower the penetration, the lower the slag temperature in the bulk and hence the lower the casting rate. However as mentioned before, in practice the electrode penetration is a factor that is determined by the process itself and this aspect of the problem is yet to be modelled.

(5) The model enables us to distinguish between the role buoyancy forces and electromagnetic forces play in driving the flow in the slag phase. It was found that the higher the current and the smaller the fill ratio, the more important was the role of electromagnetic forces. It has to be stressed, however, that in general, both these forces could play an important role in determining the flow field.

(6) The temperature distribution in the slag was found to be quite uniform with strong gradients in the vicinity of solid walls.

(7) The use of a temperature dependent electrical conductivity for slag gave a reduced maximum temperature in the slag and a somewhat more uniform temperature distribution. This resulted in a lower amount of heat being transported to the electrode and thus in a reduced casting rate.

(8) The ratio of effective/atomic thermal conductivity in the metal pool, computed according to suggestion outlined in section 5.2 was found to lie in the range of 1.7 to 4.5. This is consistent with values deduced from experimental works ⁶.

In closing, it is worthwhile to comment briefly on the principal differences and similarities between the present work and the earlier work reported by Dilawari and Szekely ¹³⁻¹⁵. As mentioned in Chapter II, in the earlier work, the electromagnetic field, the fluid flow field and the temperature field were represented for an ESR system for a predetermined and idealized pool shape and size. Heat transfer phenomena in the mushy zone and in the ingot were ignored. While many of the transport equations and the boundary conditions used in the present work are identical to those used in the earlier work, the advances made in the present work are as follows:

(1) The shape and the size of the molten metal pool is no longer specified but calculated by solving heat transfer equations in the mushy zone and in the ingot. The present work allows for the incorporation of solidification models to represent the release of latent heat in the mushy zone.

(2) The model allows for the first time for a comparison to be made between the measured and the predicted pool profiles and temperature fields in the ingot.

(3) A more up-to-date model is used to represent the turbulent viscosity and the turbulent thermal conductivity in the slag. The model allows for special treatment of flow and heat transfer phenomena in the near wall regions.

6.2 Suggestions for Further Work

From the point of view of mathematical modelling, ESR process represents a fascinating, if complex, group of problems. The model described in this work was an attempt at grouping together the salient features of current distribution, fluid flow and heat transfer phenomena so that the model could be used to investigate the interdependence of key process parameters. A few suggestions are given here for some further work in the area of modelling of ESR process. The suggestions given here are limited to mathematical modelling but it should be

recognized that physical modelling is a vast and extremely important area and that there is a need for a strong interaction between the two.

6.2.1 Suggestions for short term plans

These include the following:

(1) In the work reported in this thesis, limited measurements on a laboratory scale system were used. It would be desirable to have some measurements, specially on temperature distribution in the slag, available for a large scale system so as to be able to test the predictions of the model for this system.

(2) The model, in its present form, uses an effective thermal conductivity to account for convective heat transfer in the metal pool. The model can be extended to calculate flow in the metal pool. To achieve this it will be advantageous to employ a numerical scheme of the type used by Elliott and Maulvault¹¹ below the slag-metal interface.

(3) An attempt can be made to use the information on velocity and temperature distribution generated by the model in developing a kinetic model.

6.2.2 Suggestions for long term plans

These include the following:

(1) There is a strong need for both experimental and analytical work in order to develop a realistic under-

standing of melting phenomena at the slag-electrode interface.

(2) The model developed in this work can be extended to calculate fluid flow in the mushy zone so that it can be used to calculate macrosegregation in the ingot.

(3) Some preliminary calculations can be made for multiple electrode configurations. The modelling of multiple electrode system represents a major additional difficulty, because under these conditions axial symmetry is no longer observed.

(4) An approach similar to the one described in this thesis can be used to model the electroslag casting process.

APPENDIX A

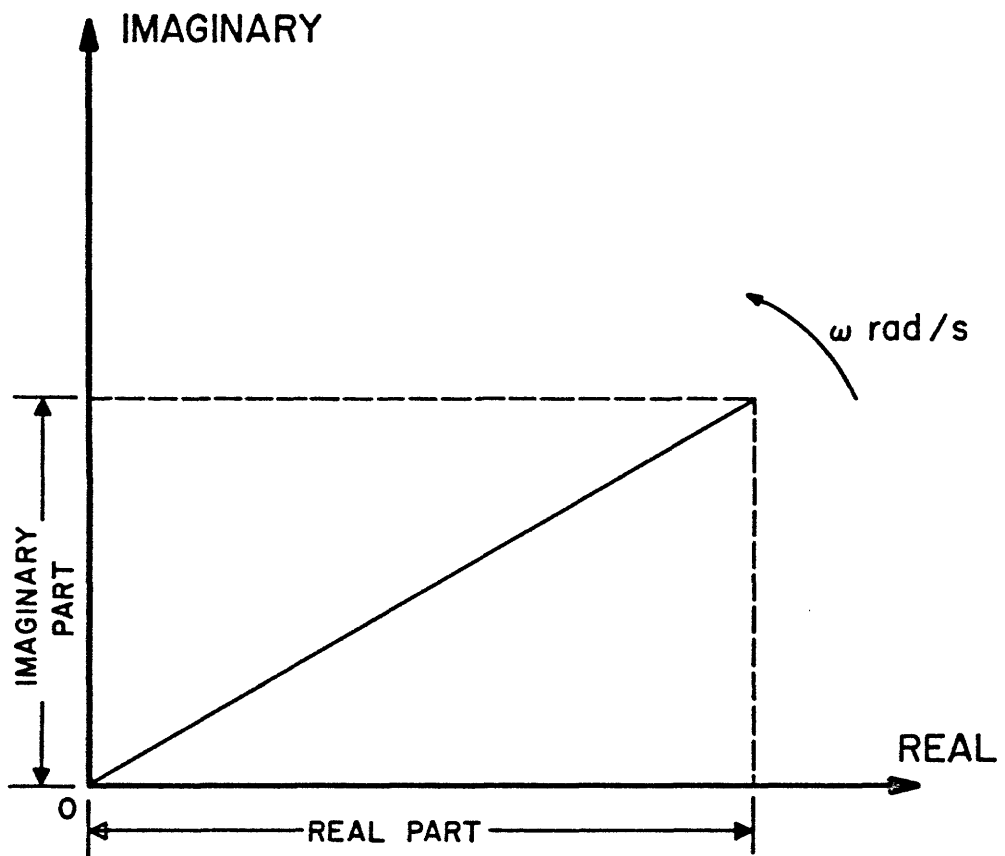
A BRIEF NOTE ON PHASOR NOTATION

In dealing with sinusoidally time-varying quantities it is convenient to use phasor approach. A phasor is a complex number which can be represented graphically as shown in Fig. A 1. The length of the line is equal to the magnitude of the complex number and the angle that the line makes with the positive real axis is the angle of the complex number. For example when the functional form is cosinusoidal, i.e. $A \cos (\omega t + \phi)$, the magnitude of the phasor is equal to the magnitude A of the cosinusoidal function and the angle of the phasor is equal to the phase angle ϕ of the function for $t = 0$. The real part of the phasor is $A \cos\phi$ which is the value of the function at $t = 0$. As seen from Fig. A.1, if the phasor is rotated about the origin in the counter-clockwise direction at the rate of ω rad/s, the time variation of its projection on the real axis describes the time variation of the cosinusoidal function. Using the terminology adopted in Chapters III and IV, a cosinusoidal function f can be represented, in phasor notation, as

$$f = \operatorname{Re} [\hat{A} e^{j\omega t}] \quad (\text{A.1})$$

where
$$\hat{A} = |A| e^{j\phi} \quad (\text{A.2})$$

$$|A| = \text{magnitude of the phasor at } t = 0.$$



A.1 Graphical representation of a phasor.

Similar considerations hold when dealing with sinusoidally time-varying vectors.

To illustrate the application of phasor concept, let us derive the expression for time average electromagnetic body force component F_z [i.e. Eq. (3.15b)]. From Eq. (3.10), the instantaneous value of this quantity can be written, in phasor notation, as

$$F_z' = \mu_0 \operatorname{Re}(\hat{H}_\theta e^{j\omega t}) \times \operatorname{Re}(\hat{J}_r e^{j\omega t}) \quad (\text{A.3})$$

$$= \mu_0 |\hat{H}_\theta| \cos(\omega t + \phi_1) \times |\hat{J}_r| \cos(\omega t + \phi_2)$$

$$= \mu_0 |\hat{H}_\theta| |\hat{J}_r| [\cos(\omega t + \phi_1) \cos(\omega t + \phi_2)]$$

$$= \frac{1}{2} \mu_0 |\hat{H}_\theta| |\hat{J}_r| [\cos(2\omega t + \phi_1 + \phi_2) \quad \text{I}$$

$$+ \cos(\phi_1 - \phi_2)] \quad (\text{A.4})$$

II

The time-average value can be found as follows:

$$F_z = \frac{1}{T} \int_0^T F_z' dt \quad (\text{A.5})$$

where T is the period.

The time-average value of the first term in Eq. (A.4) is equal to zero, thus

$$\begin{aligned}
F_z &= \frac{1}{2} \mu_0 |\hat{H}_\theta| |\hat{J}_r| \cos(\phi_1 - \phi_2) \\
&= \frac{1}{2} \mu_0 \operatorname{Re} [|\hat{H}_\theta| |\hat{J}_r| e^{j(\phi_1 - \phi_2)}] \\
F_z &= \frac{1}{2} \mu_0 \operatorname{Re} [|\hat{H}_\theta| e^{j\phi_1} \cdot |\hat{J}_r| e^{-j\phi_2}] \\
&= \frac{1}{2} \mu_0 \operatorname{Re} (\hat{H}_\theta \hat{J}_r^*) \qquad (3.15b)
\end{aligned}$$

where \hat{J}_r^* is the complex conjugate of \hat{J}_r .

Following a similar approach, expressions can be derived for other time-averaged parameters such as F_r [Eq. (3.15a)], Q_j [Eq. (3.16)], etc.

APPENDIX B

BOUNDARY CONDITIONS ON VORTICITY

In this appendix, expressions will be derived for vorticity at the axis of symmetry and at the walls.

B.1 Vorticity at the Axis of Symmetry ³⁹

Form Eq. (3.23b) in the text,

$$\bar{V}_z = \frac{1}{\rho r} \frac{\partial \psi}{\partial r}$$

It follows that in order for \bar{V}_z to be finite at $r = 0$, $\frac{\partial \psi}{\partial r}$ must tend to zero at the same rate as r near the axis.

It follows that in the immediate vicinity of the axis, the $\psi \sim r$ distribution is parabolic. Furthermore, because of symmetry the second term in the $\psi \sim r$ expansion should be the fourth power one; thus:

$$\psi - \psi_0 \approx ar^2 + br^4 \quad (\text{B.1})$$

where ψ_0 is the stream function at the axis and a and b are constants for a fixed z .

Using the definition of vorticity [Eq. (3.22)], the symmetry condition $\bar{V}_r = 0$ at the $r = 0$ and Eq. (B.1) we can write

$$\xi = - \frac{8br}{\rho} \quad (\text{B.2})$$

Thus $\xi = 0$ at $r = 0$, $\frac{\xi}{r}$ on the other hand is finite.

If 1 and 2 denote the nodes which are once and twice removed from the node 0 on the symmetry axis, we can evaluate b from

$$\begin{aligned}\psi_1 - \psi_0 &= ar_1^2 + br_1^4 \\ \psi_2 - \psi_0 &= ar_2^2 + br_2^4\end{aligned}\quad (\text{B.3a,b})$$

Then Eq. (B.2) gives;

$$\left(\frac{\xi}{r}\right)_0 = \frac{8}{\rho} \left[\frac{\psi_0 - \psi_2}{r_2^2} + \frac{\psi_1 - \psi_0}{r_1^2} \right] / (r_2^2 - r_1^2) \quad (\text{3.89b})$$

B.2. Vorticity at a Wall ⁵³

Let us illustrate the calculation of wall vorticity w.r.t slag-electrode interface. As seen in Fig. B.1, 0 is a node on the wall and 1 is the adjacent node in the z -direction. Using Taylor series expansion, the value of stream function at node 1, ψ_1 can be expressed as

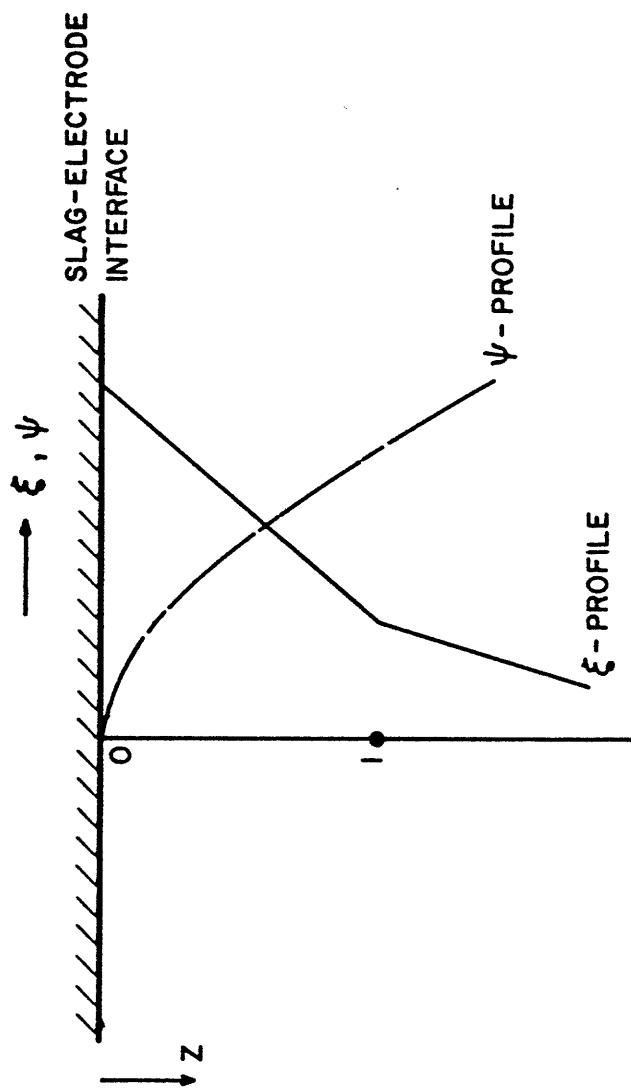
$$\psi_1 = \psi_0 + \frac{\partial \psi}{\partial z} \Big|_0 \Delta + \frac{1}{2} \frac{\partial^2 \psi}{\partial z^2} \Big|_0 \Delta^2 + \frac{1}{6} \frac{\partial^3 \psi}{\partial z^3} \Big|_0 \Delta^3 + O(\Delta^4) \quad (\text{B.4})$$

$$\text{where } \Delta = z_1 - z_0 \quad (\text{B.5})$$

From Eq. (3.23a)

$$\frac{\partial \psi}{\partial z} \Big|_0 = -\rho r \bar{V}_r \Big|_0 = 0 \quad (\text{B.6})$$

(no slip condition)



B.1 Evaluation of wall vorticity.

$$\text{and } \frac{\partial^2 \psi}{\partial z^2} \Big|_0 = -\rho r \frac{\partial \bar{V}_r}{\partial z} \Big|_0 \quad (\text{B.7})$$

From Eq. (3.22)

$$\begin{aligned} \xi \Big|_0 &= \frac{\partial \bar{V}_r}{\partial z} \Big|_0 - \frac{\partial \bar{V}_z}{\partial r} \Big|_0 \\ &= -\frac{1}{\rho r} \frac{\partial^2 \psi}{\partial z^2} \Big|_0 \end{aligned} \quad (\text{B.8})$$

Thus from Eq. (B.8) we can write

$$\frac{\partial^2 \psi}{\partial z^2} \Big|_0 = -\rho r \xi \Big|_0 \quad (\text{B.9})$$

$$\text{and } \frac{\partial^3 \psi}{\partial z^3} \Big|_0 = -\rho r \frac{\partial \xi}{\partial z} \Big|_0 \quad (\text{B.10})$$

Using Eqs. (B.6), (B.9) and (B.10) in Eq. (B.4) gives

$$\psi_1 = \psi_0 - \rho r \left[\frac{1}{2} \xi_0 + \frac{1}{6} \frac{\partial \xi}{\partial z} \Big|_0 \Delta \right] \Delta^2 \quad (\text{B.11})$$

If as shown in Fig. B.1, ξ is taken as varying linearly with z in the vicinity of the wall,

$$\frac{\partial \xi}{\partial z} \Big|_0 \Delta = (\xi_1 - \xi_0) \quad (\text{B.12})$$

Solving for ξ_0 from Eq. (B.11) then gives,

$$\left(\frac{\xi}{r} \right)_0 = \frac{3(\psi_0 - \psi_1)}{\rho r^2 (z_1 - z_0)^2} - \frac{1}{2} \left(\frac{\xi}{r} \right)_1 \quad (\text{3.91c})$$

Following an identical approach, expression for vorticity at the slag-metal interface can be derived. For the vertical surfaces, (i.e. $r = R_e$, $Z_1 \leq z \leq Z_2$ and $r = R_m$, $Z_1 \leq z \leq Z_3$), a similar approach is used but instead of assuming a linearly varying vorticity, the vorticity transport equation is used to give an expression for the normal gradient of vorticity at the wall.

APPENDIX C

CALCULATION OF RADIATION VIEW FACTORS

In this appendix, radiation view factors appearing in Eqs. (3.97) and (3.99) are calculated using the compilation made by Leunberger and Person⁵⁴ for finite coaxial cylinders. Fig. C.1 shows a schematic representation of the system for calculating view factors. Symbols s , e , m and t represent free surface of the slag, outer surface of the electrode, inner surface of the mold and top (open) surface respectively.

View factors are calculated with the aid of "view factor algebra" which relies on the reciprocity rule and on the fact that radiation is conserved. According to Leunberg and Person⁵⁴

$$F_{es}(z) = \frac{1}{2\pi} \left[\cos^{-1} \frac{A_2}{A_1} - \frac{x}{R_e} \left\{ \frac{A_3}{\sqrt{A_3^2 - 4R_e^2 R_m^2}} \right. \right. \\ \left. \left. \cos^{-1} \frac{A_2}{A_1} \frac{R_e}{R_m} - \cos^{-1} \frac{R_e}{R_m} \right\} \right] \quad (C.1)$$

where

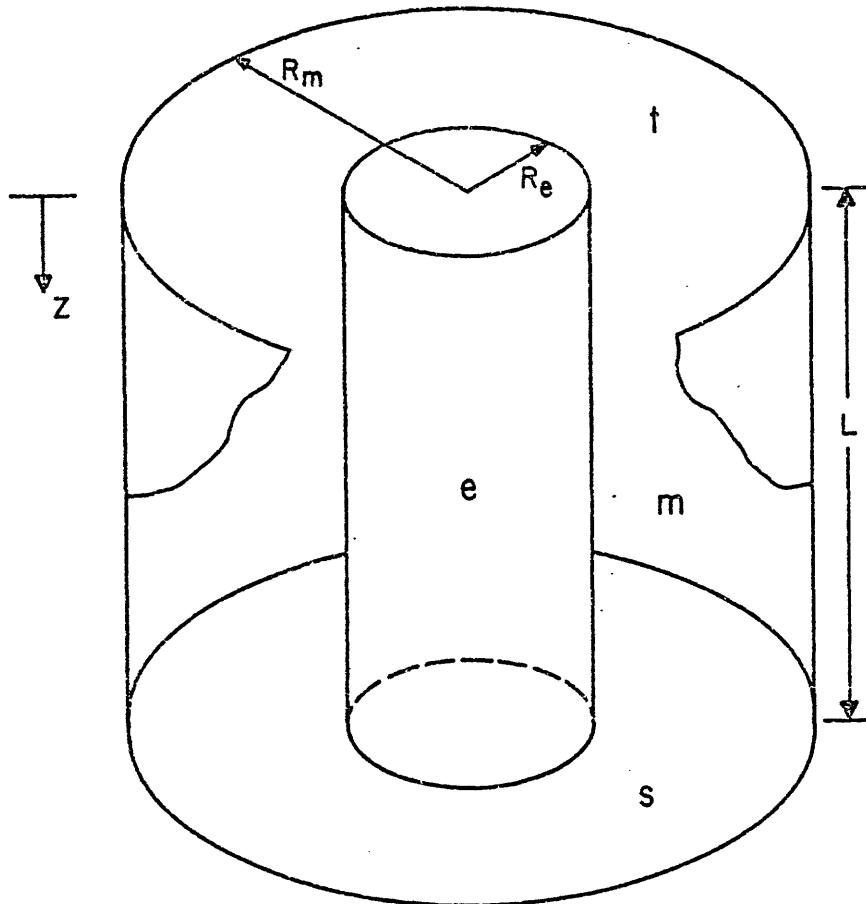
$$A_1 = x^2 + R_m^2 - R_e^2$$

$$A_2 = x^2 - R_m^2 + R_e^2$$

$$A_3 = x^2 + R_m^2 + R_e^2$$

$$x = L - z$$

(C.2, 3, 4, 5)



C.1 Schematic representation of the system for calculating view factors.

The view factor $F_{et}(z)$ can be evaluated by using Eq. (C.1) with $x = z$. Then $F_{em}(z)$ can be calculated using,

$$F_{em}(z) = 1 - F_{es}(z) - F_{et}(z) \quad (C.6)$$

Let us now consider the evaluation of F'_{sm} and F'_{se} . First we note that,

$$F'_{ms} + F'_{mm} + F'_{mt} + F'_{me} = 1 \quad (C.7)$$

where ' indicates that the view factors are w.r.t. the entire surface.

$$F'_{ms} = F'_{mt} \quad (C.8)$$

$$\text{Thus, } F'_{ms} = \frac{1}{2} (1 - F'_{mm} - F'_{me}) \quad (C.9)$$

Again, from reference 54,

$$F'_{me} = \frac{R_e}{R_m} \left\{ 1 - \frac{1}{\pi} \cos^{-1} \frac{A_5}{A_4} - \frac{1}{A_6} \left[A_7 \cos^{-1} \frac{R_e}{R_m} \frac{A_5}{A_4} + A_5 \sin^{-1} \frac{R_e}{R_m} - \frac{\pi}{2} A_4 \right] \right\} \quad (C.10)$$

where

$$\begin{aligned} A_4 &= L^2 + R_m^2 - R_e^2 \\ A_5 &= L^2 - R_m^2 + R_e^2 \\ A_6 &= 2R_m R_e \\ A_7 &= \sqrt{(L^2 + R_m^2 + R_e^2)^2 - 4R_e^2 R_m^2} \end{aligned} \quad (C.11, 12, 13, 14)$$

and

$$F'_{mm} = 1 - \frac{R_e}{R_m} + \frac{1}{\pi} \left\{ 2 \frac{R_e}{R_m} \tan^{-1} A_{11} - \frac{L}{2R_m} [A_8 \sin^{-1} A_9 - \sin^{-1} A_{10} + \frac{\pi}{2} (A_8 - 1)] \right\} \quad (C.15)$$

where

$$A_{11} = \frac{2 \sqrt{R_m^2 - R_e^2}}{L}$$

$$A_8 = \frac{\sqrt{4R^2 + L^2}}{L}$$

$$A_9 = \frac{A_{11}^2 + A_{10}}{A_{11}^2 + 1}$$

$$A_{10} = 1 - 2 \left(\frac{R_e}{R_m} \right)^2 \quad (C.16,17,18,19)$$

Thus after calculating F'_{me} from Eq. (C.10) and F'_{mm} from Eq. (C.15), we can calculate F'_{ms} from Eq. (C.9).

Then, from reciprocity rule,

$$F'_{sm} = \frac{2R_m L}{R_m^2 - R_e^2} F'_{ms} \quad (C.20)$$

similarly noting that ⁵⁴

$$F'_{st} = 1 - \frac{L}{R_m^2 - R_e^2} [R_e - R_m (F'_{mm} + 2F'_{me} - 1)] \quad (C.21)$$

and that $F'_{se} + F'_{sm} + F'_{st} = 1$

we can calculate

$$F'_{se} = 1 - F'_{sm} - F'_{st} \quad (\text{C.22})$$

APPENDIX D

USE OF TEMPERATURE DEPENDENT ELECTRICAL CONDUCTIVITY IN
THE SLAG

The magnetohydrodynamic form of Maxwell's equation (for low magnetic Reynolds no.) can be written as:

$$\mu_0 \frac{\partial \mathbf{H}}{\partial t} = - [\nabla \times \left(\frac{\nabla \times \mathbf{H}}{\sigma} \right)] \quad (\text{D.1})$$

In cylindrical coordinate and for axial symmetry ($H_r = H_z = \frac{\partial}{\partial \theta} = 0$), Eq.(D.1) can be written as follows:

$$\mu_0 \frac{\partial H_\theta}{\partial t} = \frac{\partial}{\partial z} \left[- \frac{1}{\sigma} \frac{\partial H_\theta}{\partial z} \right] + \frac{\partial}{\partial r} \left[- \frac{1}{\sigma} \frac{1}{r} \frac{\partial}{\partial r} (r H_\theta) \right] \quad (\text{D.2})$$

Expanding the terms in Eq.(D.2) gives:

$$\begin{aligned} \sigma \mu_0 \frac{\partial H_\theta}{\partial t} = & \left[\frac{\partial^2 H_\theta}{\partial z^2} + \frac{\partial}{\partial r} \left(- \frac{1}{r} \frac{\partial}{\partial r} (r H_\theta) \right) \right] - \\ & \left[\frac{\partial H_\theta}{\partial z} \frac{\partial \ln \sigma}{\partial z} + \frac{1}{r} \frac{\partial}{\partial r} (r H_\theta) \frac{\partial \ln \sigma}{\partial r} \right] \end{aligned} \quad (\text{D.3})$$

For the calculations reported in the text, the second term on the r.h.s. of Eq. (D.3) has been neglected. However, in some of the calculations the temperature dependence of σ , appearing on the l.h.s of Eq.(D.3) has been accounted for. The basic approach in these latter calculations involved:

(1) Solution of field equations for a specified temperature distribution in slag

(2) Values for electromagnetic force and Joule heat rate generated in step 1 was then used to solve flow and temperature equations.

(3) Temperature field generated in step 2 was used to calculate the new distribution of σ in slag.

Steps 1 to 3 were repeated until the temperature fields in slag calculated in two consecutive iterations agreed within a specified limit. It is to be noted that each of steps 1 and 2 is iterative in addition to the overall process being iterative.

The temperature dependence of electrical conductivity was deduced from data published by Mitchell and Cameron⁶⁰ on 70% CaF_2 , 30% Al_2O_3 slags. Their data in the range 1500 °C - 1700 °C, can be represented by the following equation:

$$\ln \sigma = \frac{-9888}{T} + 10.467$$

where σ is in $\text{ohm}^{-1}\text{m}^{-1}$ and T is in °K.

APPENDIX E
THE COMPUTER PROGRAM

The computer program used for the solution of the governing differential equations is presented in this Appendix. A brief introduction to the program and the functions of various subroutines have already been given in Chapter IV. The computer program given here incorporates wall function approach for turbulence quantities and for temperature. However, the computed results reported in the thesis did not utilize this feature.

E.1 List of Fortran Symbols

<u>Symbol</u>	<u>Meaning</u>
A(I,J,K)	The dependent variables for flow and temperature equations and V_z , V_r , μ_t , μ_{eff} , K , ρ , C_p .
B(I,J,K)	Variables for electromagnetic field.
AE, AW, AN, AS	A_j' of Eq. (4.8)
ANAME (6, 12)	An alphameric array containing the names of variables for flow and temperature equations.

ASYMBL	An alphameric array containing the names of residuals as defined by Eq. (4.40).
AKEFF	Effective thermal conductivity in metal pool.
APP	$a_{\phi,p}$ of Eq (4.11 a,b,c,d)
BNAME (6,10)	An alphameric array containing the names of variables for electromagnetic field.
BE(I), BW(I), BN(J), BS(J)	B_j' of Eq. (4.8)
BPP	$b_{\phi,p}$ of Eq. (4.8)
BBE, BBW, BBN, BBS	The group of terms $c_{\phi,j} (b_{\phi,j} + b_{\phi,p}) B_j'$ in Eq. (4.8).
BETA	Coefficient of volume expansion (β).
C1, C2, C3, CD	Constants in the turbulence model.
CC,CP	The convergence criteria for flow and temperature equations, magnetic field equations.
CU	Total current (maximum value), kA

CAPPA	Von Karman's constant (κ)
D	S in Eq. (3.75)
D1, D2, DN, DS	Parameters in Eqs. (4.15) and (4.16).
E	The wall roughness factor, E in Eq. (4.30)
ES, EE, EM	Emissivities of slag surface (ϵ_s) of electrode (ϵ_e) and of mold (ϵ_m)
FES, FEM, FSM, FSE	Radiation view factors F_{es} , F_{em} , F'_{sm} , F'_{se}
FR	Geometric factors to account for the fact that control volumes for integration in near wall regions are different from those in the interior of the domain.
GAMA	Interfacial tension between molten metal and slag (γ).
HC	Heat transfer coefficient between electrode and gas
HW	Overall heat transfer coefficients at interfaces defined by Eq. (3.104).

HCD	$\pi R_e^2 V_{me} \rho_e C_{P,d}$ in Eq. (3.76)
HL	Heat of fusion
I	Index for constant - z grid lines
IE	The number of differential equations (for flow and heat transfer) to be solved.
I1, I2, I3, I4, I5, IA, J1	Indices defined in Fig. 5.2
IN	The total number of constant z grid lines
IP	The number of successive iterations for which print-out is to be produced
IV	The number of variables whose values are to be printed out.
J	Index for constant-r lines.
JN	The total number of constant-r lines.
K	The index which denotes the dependent variable in question.

MIT		The maximum number of iterations for magnetic field equations
MPRINT		The number of iterations between print-out cycles for magnetic field variables.
NEP	Indices for flow and heat tr. variables	Dissipation rate of turbulence energy
NF		Stream function
NK		Turbulence energy
NMT		Turbulent viscosity
NMU		Effective viscosity
NRO		Density
NSP		Specific heat
NT		Temperature
NTC		Thermal conductivity
NVI		Velocity in z-direction
NV2		Velocity in r-direction
NW		Vorticity (ξ/r)

NHR	Indices for electromagnetic field variables	Real part of magnetic field intensity
NHI		Imaginary part of magnetic field intensity
NH		Magnetic field intensity
NJRR		Real part of current density in r-direction
NJRI		Imaginary part of current den- sity in r-direction
NJR		Current density in r-direction
NJZR		Real part of current density in z-direction
NJZI		Imaginary part of current density in z-direction
NJZ		Current density in z-direction
NJJ		Joule heat ($\text{kCal/m}^3\text{s}$)
NMAX	The maximum number of iterations for flow and heat transfer equations.	

NPRINT	The number of iterations between print out cycles for flow and heat tr. variables
P	Magnetic permeability, μ_0 .
PR(K)	The Prandtl or Schmidt numbers.
QS	Q_S of Eq (3.76)
R(J)	r
RE, RM	Radius of electrode (R_e), radius of mold (R_m)
RES	The maximum residual $(1 - \phi_p^N / \phi_p^{N-1})_{\max}$ for all of the ϕ equations.
ROREF(5)	Reference densities for various media.
RP(K)	Relaxation parameters for flow and temperature equations.
RS	The residual at a particular node.
RSDU(K)	The maximum value of RS for each ϕ equation.
SB	10^{12} x Stefan-Boltzmann constant ($\text{kCal/m}^2\text{sK}^4$)

S(4)	Electrical conductivities of electrode, slag, molten metal, ingot.
SN1, SN2, SN3, SN4	Local heat transfer coefficients in regions defined in Fig. 4.6.
SOURCE	$S_{\phi,p}$ of Eq. (4.8).
SPREF(5)	Reference specific heats
TLM, TSM, TLS, TA, TM, TW TF, TB	$T_{\ell,m}$, $T_{s,m}$, $T_{\ell,s}$, T_a , T_m , T_w T_f , T_B in Eq. (3.74).
TCREF(5)	Reference thermal conductivities.
TAUW1, TAUW2, TAUW3, TAUW4	Shear stress values in regions defined in Fig. 4.6.
TAU	Residence time of a droplet.
UP	Velocity parallel to a wall.
VOLT	Voltage.
VE	Melting rate of electrode.
VC	Casting rate.
W	Relaxation parameters for magnetic field equations.

X(7)	Defined in Fig. 5.2.
X1(I)	z-coordinate of the grid nodes.
X2(J)	r-coordinate of the grid nodes.
YL(J)	Position of liquidus isotherm.
YS(J)	Position of solidus isotherm.
ZMUREF	Reference value for viscosity.


```

COMMON/CDVAR/A(71,15,12)
COMMON/CNAME/ANAME(6,12),ASYMBL(10),BNAME(6,10)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CCRIT/NWI,NWJ,NFI,NFJ,GOSA,TOTA
COMMON/CITER/NMAX,NPRINT,NITER,IP,IE,IV,CC
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CFLD/B(71,15,10),LF,CU
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CDROP/TAU,HCD,D,QS,QM
COMMON/CAVM/AVM(20)
COMMON/CLS/YL(15),YS(15)
INM=IN-1
JNM=JN-1
C** READ ALPHAMEIC INFORMATION FOR HEADINGS AND TITLES
      LEAD(5,200)ANAME,ASYMBL,BNAME
C** COMPUTE AND PRINT COORDINATES
      CALL CORD
      WRITE(6,12) I1,I2,I3,I4,J1
      WRITE(6,101) (X1(I),I=1,IN)
      WRITE(6,102) (X2(J),J=1,JN)
C** INITIALIZE
      CALL INIT
C *** FEAD INFORMATION FROM PREVIOUS CALCULATIONS
      DO 21 K=1,5
      DC 21 J=1,JN
21 FEAD(4,14) (B(I,J,K),I=1,IN)
      DO 22 K=1,5
      DO 22 J=1,JN
22 READ(4,14) (A(I,J,K),I=1,IN)
      DC 25 J=1,JN
25 READ(4,18) YL(J),YS(J)
14 FORMAT(/,7(1PE10.3))
18 FORMAT(2(F10.4))
C *** PERFORM ELECTRO MAGNETIC FIELD CALCULATIONS

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SAR00010
SAR00020
SAR00030
SAR00040
SAR00050
SAR00060
SAR00070
SAR00080
SAR00090
SAR00100
SAR00110
SAR00120
SAR00130
SAR00140
SAR00150
SAR00160
SAR00170
SAR00180
SAR00190
SAR00200
SAR00210
SAR00220
SAR00230
SAR00240
SAR00250
SAR00260
SAR00270
SAR00280
SAR00290
SAR00300
SAR00310
SAR00320
SAR00330
SAR00340
SAR00350
SAR00360

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SAR00370
SAR00380
SAR00390
SAR00400
SAR00410
SAR00420
SAR00430
SAR00440
SAR00450
SAR00460
SAR00470
SAR00480
SAR00490
SAR00500
SAR00510
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SAR00560
SAR00570
SAR00580
SAR00590
SAR00600
SAR00610
SAR00620
SAR00630
SAR00640
SAR00650
SAR00660
SAR00670
SAR00680
SAR00690
SAR00700
SAR00710
SAR00720
PAGE 2

CALL FIELD
IF (LF EQ 2) GO TO 30
C*** PERFORM FLUID FLOW CALCULATIONS
C *** INITIAL GUESS FOR PROPERTIES
CALL PROP(1)
CALL VFDROP
NITER=0
1 CONTINUE
NITER=NITER+1
C*** CAUSE ONE CYCLE OF ITERATION TO BE PERFORMED
CALL EQN
C*** TEST IF PRINTOUT TO BE PRODUCED
IF ((NITER+NPRINT-IP)/NPRINT NE. NITER/NPRINT) GO TO 10
CALL PKINT(1,IV,1)
WRITE(6,103) (ASYMBL(K),K=1,10)
WRITE(6,104) NITER, (RSDU(K),K=1,IE), (SAN(K),K=1,IE), NWJ,NWI,NFJ,NFI,SAR00520
SAR00530
10 CONTINUE
C** TEST IF MAXIUM NUMBER OF ITERATONS PERFORMED
IF(NITER.EQ NMAX) GO TO 8
FES=0
DO 7 K=1,IE
IF (ABS(RES) LT ABS (RSDU(K))) RES=RSDU (K)
RSDU(K)=0.
7 CONTINUE
SANWF=0.
DO 3 K=1,IE
IF (ABS (SANWF) .LT. ABS (SAN (K))) SANWF=SAN (K)
SAN (K) =0
3 CONTINUE
C*** TEST IF CONVERGENCE CRITERION SATISFIED
IF (ABS (SANWF) .GT..006) GO TO 1
WRITE(6,105) NITER
CALL PRINT(1,8,1)
WRITE(6,225)
CALL PRINT(9,10,2)
GO TO 9

```

```

8 WRITE(6,106) NITER
CALL PRINT(5,7,1)
9 CONTINUE
30 CONTINUE
STOP
12 FORMAT(/,4H I1=,I2,4H I2=,I2,4H I3=,I2,4H I4=,I2,4H J1=,I2)
101 FCRMAT(25HODISTANCES IN DIRECTION-1/(1H 4E25.8))
102 FCRMAT(25HODISTANCES IN DIRECTION-2/(1H 4E25.8))
103 FCRMAT(36HOMAXIMUM RESIDUAL FOR EACH VARIABLE://
16HONITER,10(3X,A6), 3X, 16H NWJ NWI NFJ NFI//)
104 FCRMAT(1H0 I3,3X,10(F9.4), 5X,I2,3(I4))
106 FCRMAT(32H0THE PROCESS DID NOT CONVERGE IN, I5, 13H ITERATIONS)
105 FCRMAT(32H0THE PROCESS CONVERGED IN, I5, 13H ITERATIONS)
200 FCRMAT( 6A6)
225 FCRMAT(/,50H DEIVING FORCES ARE FIRST ELECTROMAG THEN BUOYANCY)
END
SAR00730
SAR00740
SAR00750
SAR00760
SAR00770
SAR00780
SAR00790
SAR00800
SAR00810
SAR00820
SAR00830
SAR00840
SAR00850
SAR00860
SAR00870
SAR00880

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BLOCK DATA
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CDIM/X(7),RE,RM
COMMON/CITER/NMAX,NPRINT,NITER,IP,IE,IV,CC
COMMON/CCONT/C1,C2,C3,CD
COMMON/CRLEX/RP(10),RSDU(10),SAN(10)
COMMON/CEMP/WF,P,S(4)
COMMON/CHJ/NHR,NHI,NH,NJEP,NJRI,NJR,NJZR,NJZI,NJZ,NJJ
COMMON/FRLAX/W(2),SUM(2),SUM1(2)
COMMON/FITER/MIT,MPRINT,CP
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SB,HL
COMMON/CTEMP/TLM,TSM,TLS,TA,TM,TW
COMMON/CTRL/VE,VC
COMMON/CHEAT/HC,HW(4)
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CVF/FES(21),FEM(21),FSM,FSE
COMMON/CDROP/TAU,HCD,D,QS,QM
COMMON/CTAUW/TAUW1(20),TAUW2(15),TAUW3(21),TAUW4(10),CAPPA,E
COMMON/CFLD/B(71,15,10),LF,CU
C ** PROGRAM AND PRINT OUT CONTROL DATA
DATA NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,IE,IV/1,2,3,4,6,7,5,8,9,5,5/
1,NMAX,NPRINT,IP,CC/600,200,1,0.005/
2,RP/0.1,1.2,0.5,0.5,0.5,5*1.0/
3,NTC,NSP,NMT/10,11,12/
DATA RSDU,SAN/10*0.0,10*0.0/
DATA NHR,NHI,NH,NJRR,NJRI,NJR,NJZR,NJZI,NJZ,NJJ/1,2,6,3,4,
17,9,10,8,5/
1,W,SUM,SUM1/1 50,1.20,2*0.0,2*0 0/
2,MIT,MPRINT,CP/400,200,0.005/
C*** PHYSICAL DATA
DATA ROREF/7 2E+03,2.8E+03,7.2E+03,7.2E+03,7.2E+03/
1,ZMUREF/1.0E-02,6.0E-03/
2,PR/1 0,1 0,1 0,1.3,6*1 0/
3,TCREF/7.5E-03,2.500E-03,3.7E-03,7.5E-03,7.5E-03/
SAR00890
SAR00900
SAR00910
SAR00920
SAR00930
SAR00940
SAR00950
SAR00960
SAR00970
SAR00980
SAR00990
SAF01000
SAR01010
SAR01020
SAR01030
SAR01040
SAR01050
SAR01060
SAR01070
SAR01080
SAR01090
SAR01100
SAR01110
SAR01120
SAR01130
SAR01140
SAR01150
SAR01160
SAR01170
SAR01180
SAR01190
SAR01200
SAR01210
SAR01220
SAR01230
SAR01240

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4, SPEEF, HL/0.12, 0.20, 0.18, 0.18, 0.18, 0.18, 59.0/
 5, TLM, TSM, TLS, TA, TM, TW/1723.0, 1523.0, 1650.0, 323.0, 323.0, 330.0/
 6, ES, EE, EM, SB/0.60, 0.40, 1.00, 13.70/
 7, BETA/1.0E-04, 1.0E-03/
 8, VE, VC, HC/6 31E-04, 2.05E-04, 6.0E-03/
 9, GAMA/0.9/
 1, HW/1 50E-01, 6.50E-02, 6.50E-02, 4.5E-02/
 2, CAPPA, E/0.40, 9.0/
 DATA C1, C2, C3, CD/1.44, 1.92, 1.0, 0.09/
 DATA WF, P/3.77E+02, 1.26E-06/
 1, S/7 14E+05, 2.5E+02, 7.14E+05, 7 14E+05/
 2, CU/2.404/
 GRID DATA
 DATA IN, JN/51, 12/
 1, X/0.3, 0.32, 0.36, 1.0, 370, 0.38, 0, 450, 0.730/
 2, KE, RM/0.0285, 0.05/
 3, I1, I2, IA, I3, I4, I5, J1/16, 19, 24, 27, 31, 41, 7/
 4, IMIN/7*2, 5*17/
 5, IMAX/12*50/
 END

C***

SAR01250
 SAR01260
 SAR01270
 SAR01280
 SAR01290
 SAR01300
 SAR01310
 SAR01320
 SAR01330
 SAR01340
 SAR01350
 SAR01360
 SAR01370
 SAR01380
 SAR01390
 SAR01400
 SAR01410
 SAR01420
 SAR01430
 SAR01440

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SUBROUTINE CORD
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CDIM/X(7),RE,RM
COMMON/CB/BE(71),BW(71),BN(15),BS(15)
COMMON/CEMP/WF,P,S(4)
COMMON/CGEOM/FR(4)
COMMON/CX/D1(71,15),D2(71,15),DN(15),DS(15)
X1(1)=0.0
X2(1)=0.0
I(1)=X2(1)
DZ1=X(1)/FLOAT(I1-1)
DZ2=(X(2)-X(1))/FLOAT(I2-I1)
DZ3=(X(3)-X(2))/FLOAT(IA-I2)
DZ4=(X(4)-X(3))/FLOAT(I3-IA)
DZ5=(X(5)-X(4))/FLOAT(I4-I3)
DZ6=(X(6)-X(5))/FLOAT(I5-I4)
DZ7=(X(7)-X(6))/FLOAT(IN-I5)
DR1=RE/FLOAT(J1-1)
DR2=(RM-RE)/FLOAT(JN-J1)
DO 10 I=2,IN
IF(I.LE.I1) DX1=DZ1
IF(I.GT.I1.AND.I.LE.I2) DX1=DZ2
IF(I.GT.I2.AND.I.LE.IA) DX1=DZ3
IF(I.GT.IA.AND.I.LE.I3) DX1=DZ4
IF(I.GT.I3.AND.I.LE.I4) DX1=DZ5
IF(I.GT.I4.AND.I.LE.I5) DX1=DZ6
IF(I.GT.I5.AND.I.LE.IN) DX1=DZ7
10 X1(I)=X1(I-1)+DX1
DO 50 J=2,JN
DX2=DR1
IF(J.GT.J1.AND.J.LE.JN) DX2=DR2
X2(J)=X2(J-1)+DX2
R(J)=X2(J)
50 CONTINUE
C ** CALCULATE BE,BW,BN,BS,DN,DS,D1,D2

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SAR01450
SAR01460
SAR01470
SAR01480
SAR01490
SAR01500
SAR01510
SAR01520
SAR01530
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SAR01560
SAR01570
SAR01580
SAR01590
SAR01600
SAR01610
SAR01620
SAR01630
SAR01640
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SAR01660
SAR01670
SAR01680
SAR01690
SAR01700
SAR01710
SAR01720
SAR01730
SAR01740
SAR01750
SAR01760
SAR01770
SAR01780
SAR01790
SAR01800

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DO 20 J=2,JNM
IL=IMIN(J)
IH=IMAX(J)
DC 20 I=IL,IH
DX1=1./ (X1(I+1)-X1(I-1))
BW(I)=DX1/(X1(I)-X1(I-1))
BE(I)=DX1/(X1(I+1)-X1(I))
DX2=1.0/(X2(J+1)-X2(J-1))
A1=DX2/(X2(J+1)-X2(J))
DN(J)=2./ (R(J+1)+R(J))*A1
BN(J)=(1.+R(J+1)/R(J))*0.5*A1
A2=DX2/(X2(J)-X2(J-1))
DS(J)=2./ (R(J-1)+R(J))*A2
BS(J)=(1.+R(J-1)/R(J))*0.5*A2
D1(I,J)=R(J)*(DN(J)+DS(J))+BE(I)+BW(I)
S1=S(2)
IF(I.LE.I2.AND.J.LE.J1) S1=S(1)
IF(I.GT.I3) S1=S(1)
D2(I,J)=0.5*WF*P*S1
DD=D1(I,J)**2+D2(I,J)**2
D1(I,J)=D1(I,J)/DD
D2(I,J)=D2(I,J)/DD
DN(J)=R(J+1)*DN(J)
DS(J)=R(J-1)*DS(J)
20 CONTINUE
FR(1)=2.- (X2(JNM)-X2(JNM-1))/(X2(JN)-X2(JNM-1))
FR(2)=2.- (X1(I2+2)-X1(I2+1))/(X1(I2+2)-X1(I2))
FR(3)=2.- (X1(I3-1)-X1(I3-2))/(X1(I3)-X1(I3-2))
FR(4)=2.- (X2(J1+2)-X2(J1+1))/(X2(J1+2)-X2(J1))
RETURN
END

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SAR01810
SAR01820
SAR01830
SAR01840
SAR01850
SAR01860
SAR01870
SAR01880
SAR01890
SAR01900
SAR01910
SAR01920
SAR01930
SAR01940
SAR01950
SAR01960
SAR01970
SAR01980
SAR01990
SAR02000
SAR02010
SAR02020
SAR02030
SAR02040
SAR02050
SAR02060
SAR02070
SAR02080
SAR02090
SAR02100
SAR02110

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SUBROUTINE INIT
COMMON/CFLD/B(71,15,10),LF,CU
COMMON/CHJ/NHR,NHI,NH,NJRR,NJRI,NJR,NJZR,NJZI,NJZ,NJJ
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CDIM/X(7),RE,RM
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CTEMP/TLM,TSM,ILS,TA,IM,TW
COMMON/CLS/YL(15),YS(15)
C*** SET VALUES IN STROE TO ZERO
DO 30 K=1,12
DO 30 J=1,JN
DO 30 I=1,IN
A(I,J,K)=0.0
IF(K.GT.10) GO TO 30
B(I,J,K)=0.0
30 CONTINUE
DO 31 J=1,J1
DO 31 I=1,I2
31 B(I,J,NHR)=CU*R(J)/(2.0*3.14*RE*RE)
C *** INITIAL GUESS FOR LIQUIDUS SOLIDUS ISOTHERMS
DO 32 J=1,JN
YL2=0.016*(RM-R(J))
YL(J)=0.00+SQRT(YL2)
YS2=0.0360*(RM-R(J))
YS(J)=0.015+SQRT(YS2)
32 CONTINUE
C *** INITIAL GUESS FOR TEMPERATURE
DO 50 J=1,JN
DO 50 I=1,I3
IF(J.GT.J1.AND.I.LT.I1) GO TO 50
A(I,J,NF)=1800.0
IF(J.LE.J1.AND.I.LE.I2) A(I,J,NT)=1500.0
50 CONTINUE
I31=I3+1

```

SAR02120
SAR02130
SAR02140
SAR02150
SAR02160
SAR02170
SAR02180
SAR02190
SAR02200
SAR02210
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SAR02230
SAR02240
SAR02250
SAR02260
SAR02270
SAR02280
SAR02290
SAR02300
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SAR02340
SAR02350
SAR02360
SAR02370
SAR02380
SAR02390
SAR02400
SAR02410
SAR02420
SAR02430
SAR02440
SAR02450
SAR02460
SAR02470


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DO 54 J=1, JN
DO 54 I=I31, IN
XSM=X1(I)-X1(I3)
IF(XSM.LE.YL(J)) A(I, J, NT)=1750.0
IF(XSM.GT.YL(J)).AND.XSM.LE.YS(J) A(I, J, NT)=1650.0
IF(XSM.GT.YS(J)) A(I, J, NT)=1500.0
54 CONTINUE
C*** FIXED BOUNDARY CONDITIONS
DO 11 I=11, IN
11 B(I, JN, NHR)=CU/(2.0*3.14*RM)
J12=J1+1
DO 12 J=J12, JN
12 B(I1, J, NHR)=CU/(2.0*3.14*R(J))
CONTINUE
DO 20 J=2, JNM
IL=I1+1
IF(J.LE.J1) IL=I2+1
IH=I3-1
DO 20 I=IL, IH
A(I, J, MK)=0.0001
A(I, J, NEP)=0.00001
20 CONTINUE
DO 14 J=1, J1
14 A(I2, J, NT)=TLM
DO 17 I=11, IH
17 A(I, JN, NT)=TLS
RETURN
END

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SAR02480
SAR02490
SAR02500
SAR02510
SAR02520
SAR02530
SAR02540
SAR02550
SAR02560
SAR02570
SAR02580
SAR02590
SAR02600
SAR02610
SAR02620
SAR02630
SAR02640
SAR02650
SAR02660
SAR02670
SAR02680
SAR02690
SAR02700
SAR02710
SAR02720
SAR02730
SAR02740
SAR02750

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SUBROUTINE FIELD
COMMON/CGRID/IN, INM, JN, JNM, I1, I2, I3, I4, I5, IA, J1
COMMON/CHJ/NHR, NHI, NH, NJRR, NJRI, NJR, NJZR, NJZI, NJZ, NJJ
COMMON/CFLD/B(71,15,10), LF, CU
COMMON/CEMP/WF, P, S(4)
COMMON/CB/BE(71), BW(71), BN(15), BS(15)
COMMON/CX/D1(71,15), D2(71,15), DN(15), DS(15)
COMMON/CCORD/IMIN(15), IMAX(15), XI(71), X2(15), R(15)
COMMON/FRLAX/W(2), SUM(2), SUM1(2)
COMMON/FITER/MIT, MPRINT, CP
COMMON/CAVM/AVM(20)
NIT=0
1 CONTINUE
C*** BOUNDARY I=1, J<J1
J11=J1-1
XQ=X1(2)-X1(1)
XR=X1(3)-X1(1)
BB=XR*XR/(XR*XR-XQ*XQ)
DO 10 K=NHR, NHI
DO 10 J=2, J11
Z=B(1, J, K)
B(1, J, K)=BB*B(2, J, K)+(1.-BB)*B(3, J, K)
SUM(K)=SUM(K)+ABS(Z-B(1, J, K))
SUM1(K)=SUM1(K)+ABS(B(1, J, K))
B(1, J, K)=Z+W(K)*(B(1, J, K)-Z)
INTERIOR POINTS
DO 11 J=2, JNM
IL=IMIN(J)
IF(J.EQ.J1) IL=I1+1
IH=IMAX(J)
DO 19 I=IL, IH
IF(J.EQ.J1.AND.I.LE.I2) GO TO 30
IF(I.EQ.I2.AND.J.LT.J1) GO TO 14
IF(I.EQ.I3) GO TO 14
R1=DN(J)*B(I, J+1, NHR)+DS(J)*B(I, J-1, NHR)
I+BE(I)*B(I+1, J, NHR)+BW(I)*B(I-1, J, NHR)
10
C***

```

SAR02760
SAR02770
SAR02780
SAR02790
SAR02800
SAR02810
SAR02820
SAR02830
SAR02840
SAR02850
SAR02860
SAR02870
SAR02880
SAR02890
SAR02900
SAR02910
SAR02920
SAR02930
SAR02940
SAR02950
SAR02960
SAR02970
SAR02980
SAR02990
SAR03000
SAR03010
SAR03020
SAR03030
SAR03040
SAR03050
SAR03060
SAR03070
SAR03080
SAR03090
SAR03100
SAR03110

```

R2=DN(J)*B(I,J+1,NHI)+DS(J)*B(I,J-1,NHI)
1+BE(I)*B(I+1,J,NHI)+BW(I)*B(I-1,J,NHI)
DO 17 K=NHR,NHI
Z=B(I,J,K)
IF(K.EQ.NHI) GO TO 15
S1=R1
S2=R2
GO TO 16
15 S1=R2
S2=-R1
16 B(I,J,K)=D1(I,J)*S1+D2(I,J)*S2
SUM(K)=SUM(K)+ABS(Z-B(I,J,K))
SUM1(K)=SUM1(K)+ABS(B(I,J,K))
17 B(I,J,K)=Z+W(K)*B(I,J,K)-Z
GO TO 111
C *** BOUNDARY J=J1,I1<I2
30 BB=(X2(J1)-X2(J1-1))/(X2(J1+1)-X2(J1))*S(1)/S(2)
DO 31 K=NHR,NHI
Z=B(I,J,K)
B(I,J,K)=R(J-1)*B(I,J-1,K)+R(J+1)*BB*B(I,J+1,K)
B(I,J,K)=B(I,J,K)/R(J)/(1.+BB)
SUM(K)=SUM(K)+ABS(Z-B(I,J,K))
SUM1(K)=SUM1(K)+ABS(B(I,J,K))
31 B(I,J,K)=Z+W(K)*B(I,J,K)-Z
GO TO 111
C*** BOUNDARY I=I3,OR I=I2
14 CON1=S(2)/S(3)
CON2=S(1)/S(2)
CON=CON1
IF(I.EQ.I2) CON=CON2
XQ=X1(I)-X1(I-1)
XR=X1(I+1)-X1(I)
DO 141 K=NHR,NHI
BB=1./(1.+XQ/XR*CON)
Z=B(I,J,K)
B(I,J,K)=BB*B(I-1,J,K)+(1.-BB)*B(I+1,J,K)

```

SAR03120
SAR03130
SAR03140
SAR03150
SAR03160
SAR03170
SAR03180
SAR03190
SAR03200
SAR03210
SAR03220
SAR03230
SAR03240
SAR03250
SAR03260
SAR03270
SAR03280
SAR03290
SAR03300
SAR03310
SAR03320
SAR03330
SAR03340
SAR03350
SAR03360
SAR03370
SAR03380
SAR03390
SAR03400
SAR03410
SAR03420
SAR03430
SAR03440
SAR03450
SAR03460
SAR03470

```

SUM(K)=SUM(K)+ABS(Z-B(I,J,K))
SUM1(K)=SUM1(K)+ABS(B(I,J,K))
141 B(I,J,K)=Z+W(K)*(B(I,J,K)-Z)
111 CONTINUE
19 CONTINUE
11 CONTINUE
C*** BOUNDARY I=IN
XQ=X1(IN)-X1(INM)
XR=X1(IN)-X1(INM-1)
BB=XR*XR/(XR*XR-XQ*XQ)
DO 151 K=NHR,NHI
DO 151 J=2,JNM
Z=B(IN,J,K)
B(IN,J,K)=BB*B(INM,J,K)+(1.-BB)*B(INM-1,J,K)
SUM(K)=SUM(K)+ABS(Z-B(IN,J,K))
151 SUM1(K)=SUM1(K)+ABS(B(IN,J,K))
C*** CHECK FOR CONVERGENCE
CF1=SUM(NHR)/SUM1(NHR)
CF2=SUM(NHI)/SUM1(NHI)
CFF=CF1
IF(CF1.LT.CF2) CFF=CF2
IF(CFF.LE.CP) GO TO 9
NIT=NIT+1
C*** CHECK FOR PRINT OUT
K1=NIT/MPRINT
K2=K1*MPRINT
IF(NIT.NE.K2) GO TO 5
CALL PRINT(1,2,2)
WRITE(6,104) NIT,CF1,CF2
104 FORMAT(/,6H NIT=,I4/,6H CF1=,E14.8,6H CF2=,E14.8/)
5 CONTINUE
C*** CHECK FOR MAX. NO. OF ITERATIONS
IF(NIT.LT.MIT) GO TO 1
WRITE(6,106) NIT
106 FORMAT(32H0THE FLD.EQN DID NOT CONVERGE IN,15,13H ITERATIONS)
LF=2

```

SAR03480
SAR03490
SAR03500
SAR03510
SAR03520
SAR03530
SAR03540
SAR03550
SAR03560
SAR03570
SAR03580
SAR03590
SAR03600
SAR03610
SAR03620
SAR03630
SAR03640
SAR03650
SAR03660
SAR03670
SAR03680
SAR03690
SAR03700
SAR03710
SAR03720
SAR03730
SAR03740
SAR03750
SAR03760
SAR03770
SAR03780
SAR03790
SAR03800
SAR03810
SAR03820
SAR03830

```

GO TO 20
CONTINUE
LF=1
DO 18 I=1, IN
DO 18 J=1, JN
18 B(I,J,NH)=SQRT(B(I,J,NHR)**2+B(I,J,NHI)**2)
DO 29 J=2, JNM
DO 191 I=1, IN
IF(I.LT.II.AND.J.GT.J1) GO TO 191
IF(I.EQ.II.AND.J.LT.J1) GO TO 193
IF(I.EQ.IN) GO TO 193
IF(J.EQ.JI.AND.I.LE.I1) GO TO 192
IF(I.EQ.II.AND.J.GT.J1) GO TO 196
DFW=(X1(I+1)-X1(I))*BW(I)
DBE=(X1(I)-X1(I-1))*BE(I)
B(I,J,NJRR)=DBE*(B(I,J,NHR)-B(I+1,J,NHR))
1+DFW*(B(I-1,J,NHR)-B(I,J,NHR))
B(I,J,NJRI)=DBE*(B(I,J,NHI)-B(I+1,J,NHI))
1+DFW*(B(I-1,J,NHI)-B(I,J,NHI))
193 DF=X2(J+1)-X2(J)
DB=X2(J)-X2(J-1)
B(I,J,NJZR)=(DB*DB*B(I,J+1,NHR)-DF*DF*B(I,J-1,NHR)
1+(DF*DF-DB*DB)*B(I,J,NHR))/(DB*DF*(DB+DF))+B(I,J,NHR)/R(J)
B(I,J,NJZI)=(DB*DB*B(I,J+1,NHI)-DF*DF*B(I,J-1,NHI)
1+(DF*DF-DB*DB)*B(I,J,NHI))/(DB*DF*(DB+DF))+B(I,J,NHI)/R(J)
GO TO 191
192 B(I,J,NJZR)=(B(I,J,NHR)-B(I,J-1,NHR))/(X2(J)-X2(J-1))
1+B(I,J,NHR)/R(J)
B(I,J,NJZI)=(B(I,J,NHI)-B(I,J-1,NHI))/(X2(J)-X2(J-1))
1+B(I,J,NHI)/R(J)
GO TO 191
C *** JR AT I=II
196 B(I,J,NJRR)=(B(I,J,NHR)-B(I+1,J,NHR))/(X1(I+1)-X1(I))
26 B(I,J,NJRI)=(B(I,J,NHI)-B(I+1,J,NHI))/(X1(I+1)-X1(I))
191 CONTINUE
29 CONTINUE

```

SAR0384C
SAR03850
SAR03860
SAR0387C
SAR03880
SAR03890
SAR03900
SAR03910
SAR03920
SAR03930
SAR03940
SAR03950
SAR03960
SAR0397C
SAR03980
SAR03990
SAR0400C
SAR04010
SAR04020
SAR0403C
SAR04040
SAR04050
SAR04060
SAR04070
SAR04080
SAR04090
SAR0410C
SAR04110
SAR04120
SAR0413C
SAR04140
SAR04150
SAR04160
SAR04170
SAR04180
SAR04190

```

C*** JZ AT THE CENTER
DO 21 I=1,IN
B(I,1,NJZR)=(B(I,2,NHR)-B(I,1,NHR))/(X2(2)-X2(1))*2.
21 B(I,1,NJZI)=(B(I,2,NHI)-B(I,1,NHI))/(X2(2)-X2(1))*2.
C*** JZ AT J=JN
DO 25 I=1,IN
B(I,JN,NJZR)=(B(I,JN,NHR)-B(I,JNM,NHR))/(X2(JN)-X2(JNM))
1+B(I,JN,NHR)/R(JN)
25 B(I,JN,NJZI)=(B(I,JN,NHI)-B(I,JNM,NHI))/(X2(JN)-X2(JNM))
1+B(I,JN,NHI)/R(JN)
DO 195 I=1,IN
DO 195 J=1,JN
B(I,J,NJZ)=SQRT(B(I,J,NJZR)**2+B(I,J,NJZI)**2)
195 B(I,J,NJR)=SQRT(B(I,J,NJRR)**2+B(I,J,NJRI)**2)
DO 115 I=1,IN
DO 115 J=1,JN
IF(J.GT.J1.AND.I.LT.I1) GO TO 115
S1=S(2)
IF(I.LE.I2.AND.J.LE.J1) S1=S(1)
IF(I.GT.I3) S1=S(3)
B(I,J,NJJ)=(B(I,J,NJRR)**2+B(I,J,NJRI)**2+B(I,J,NJZR)**2+B(I,J,
INJZI)**2)
B(I,J,NJJ)=119.531*B(I,J,NJJ)/S1
115 CONTINUE
C CALCULATE VOLTAGE
SUMI=0.
DO 200 I=11,I3
N=I-I1+1
JL=J1
IF(I.GE.I2) JL=1
SUMJ=0.
DO 201 J=JL,JNM
DX2=0.5*(X2(J+1)-X2(J))
201 SUMJ=SUMJ+(R(J+1)*B(I,J+1,NJJ)+R(J)*B(I,J,NJJ))*DX2
200 AVM(N)=SUMJ
N3=I3-I1

```

```

DO 203 N=1,N3
I=N+11-1
DZ=(X1(I+1)-X1(I))*0.5
203 SUMI=SUMI+(AVM(N)+AVM(N+1))*DZ
VOLT=6.286*4.185*SUMI/CU*1.414
WRITE(6,110) NIT
CALL PRINT(5,8,2)
WRITE(6,204) VOLT
110 FORMAT(32H0THE FIELD EQUATION CONVERGED IN,15,13H ITERATIONS)
204 FORMAT(/,9H VOLTAGE=,F10.3)
20 CONTINUE
RETURN
END
SAR04560
SAR04570
SAR04580
SAR04590
SAR04600
SAR04610
SAR04620
SAR04630
SAR04640
SAR04650
SAR04660
SAR04670
SAR04680

```

SAR04690
 SAR04700
 SAR04710
 SAR04720
 SAR04730
 SAR04740
 SAR04750
 SAR04760
 SAR04770
 SAR04780
 SAR04790
 SAR04800
 SAR04810
 SAR04820
 SAR04830
 SAR04840
 SAR04850
 SAR04860
 SAR04870
 SAR04880
 SAR04890
 SAR04900
 SAR04910
 SAR04920
 SAR04930
 SAR04940
 SAR04950
 SAR04960
 SAR04970
 SAR04980
 SAR04990
 SAR05000
 SAR05010
 SAR05020
 SAR05030
 SAR05040

```

SUBROUTINE VFDR0P
COMMON/CVFF/FES(21),FEM(21),FSM,FSE
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CPROP/RCREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CTRLV/VE,VC
COMMON/CDIM/X(7),RE,RM
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SB,HL
COMMON/CDROP/TAU,HCD,D,QS,QM
C *** CALCULATION OF VIEW FACTORS
RM2=RM*RM
RE2=RE*RE
XL=X1(I1)
DO 10 I=1,I1
Z=XL-X1(I)
A1=Z*Z+RM2-RE2
A2=Z*Z+RE2-RM2
A3=Z*Z+RM2+RE2
A4=A3/SQRT(A3*A3-4.0*RE2*RM2)
A4=A4*ARCOS(RE/RM*A2/A1)-ARCOS(RE/RM)
FES(I)=(ARCOS(A2/A1)-Z/RE*A4)*0.1591
Z=X1(I)
A1=Z*Z+RM2-RE2
A2=Z*Z+RE2-RM2
A3=Z*Z+RM2+RE2
A4=A3/SQRT(A3*A3-4.0*RE2*RM2)
A4=A4*ARCOS(RE/RM*A2/A1)-ARCOS(RE/RM)
FET=(ARCOS(A2/A1)-Z/RE*A4)*0.1591
FEM(I)=1.0-FES(I)-FET
10 CONTINUE
Z=XL
A1=Z*Z+RM2-RE2
A2=Z*Z+RE2-RM2
A3=Z*Z+RM2+RE2
A4=SQRT(A3*A3-4.0*RE2*RM2)
A4=A4*ARCOS(RE/RM*A2/A1)+A2*ARSIN(RE/RM)-1.5708*A1

```



```

A4=(ARCOS(A2/A1)-A4/(2.0*RE*Z))*0.31831
FME=RE/RM*(1.0-A4)
Z2=Z*Z
A1=4.0*(RM2-RE2)/Z2
A2=SQRT(A1)
A3=SQRT(4.0*RM2/Z2+1.0)
A4=ARSIN((A1+(1.0-2.0*RE2/RM2))/(1.0+A1))
A4=A3*A4-ARSIN(1.-2.*RE2/RM2)+1.5708*(A3-1.)
A4=2.*RE/RM*ATAN(A2)-0.5*Z/RM*A4
FMM=1.-RE/RM+0.31831*A4
FSM=RM*Z/(RM2-RE2)*(1.-FMM-FME)
FST=1.-Z/(RM2-RE2)*(RE-RM*(FMM+2.*FME-1.))
FSE=1.-FSM-FST
WRITE(6,4) (FES(I),I=1,II)
FORMAT(25HVIEW FACTORS FES(I) ARE/(1H 7E14.4))
4 WRITE(6,5) (FEM(I),I=1,II)
FORMAT(25HVIEW FACTORS FEM(I) ARE/(1H 7E14.4))
5 WRITE(6,8) FSM,FSE
FORMAT(/,10H FSM =,E14.4,10H FSE =,E14.4)
8 *** CALCULATION OF DROP PARAMETERS
RO=ROREF(2)
R02=RO*RO
DRO=ROREF(3)-RO
DP=2.8566*SQRT(GAMA/9.81/DRO)
VU=ZMUREF(1)
VU4=VU**4
PP=(GAMA**3)*R02/(9.81*DRO*VU4)
P1=PP**0.85
Y=1.3333*DP*DP*R02*GAMA*GAMA/VU4/P1
IF(Y.LT.70.0) GO TO 15
Z=(22.222*Y)**0.422
GO TO 16
15 Z=(0.75*Y)**0.784
16 RN=(Z-0.75)*(PP**0.15)
VDT=RN*VU/DP/RO
C ** CALCULATION OF RESIDENCE TIME

```

SAR05410
SAR05420
SAR05430
SAR05440
SAR05450
SAR05460
SAR05470
SAR05480
SAR05490
SAR05500
SAR05510
SAR05520
SAR05530
SAR05540
SAR05550
SAR05560
SAR05570
SAR05580
SAR05590
SAR05600

```
Z=X1(I3)-X1(I2)
A=DR0/(ROREF(3)+0.5*RO)*9.81
C=2.*A/VDT
AM=4.*EXP(C*Z/VDT)
TAU=AM-2.+SQRT(AM*AM-4.*AM)
TAU=ALOG(TAU*0.5)/C
VDA=Z/TAU
C *** CALCULATE D=6.HD/DP/RO/CPD AND HCD=F.MD.CPD
PRN=SPREF(2)*VU/TCREF(2)
RN=VDA*DP*RO/VU
SN=0.8*SQRT(RN)*(PRN**0.333)
HD=TCREF(2)*SN/DP
SPRF3=SPREF(3)
D =6.*HD/(DP*SPRF3*ROREF(3))
HCD=3.1416*SPRF3*RE2*VE*ROREF(3)
WRITE(6,17) DP,VDT,RN,HD,TAU,D,HCD
17 FORMAT(/,5H DP=,F12.5,/,5H VDT=,F12.4,/,5H RN=,F12.3,/,
15H HD=,F12.3,/,5H TAU=,F12.3,/,5H D=,F12.3,/,5H HCD=,F12.4)
RETURN
END
```

```

SUBROUTINE EQN
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CCRIT/NWI,NWJ,NFI,NFJ,GOSA,TOTA
COMMON/CITER/NMAX,NPRINT,NITER,IP,IE,IV,CC
C*** OBTAIN EFFECTIVE VISCOSITY
CALL VISCOS
C*** VORTICITY SUB-CYCLE
GOSA=0.0
TOTA=0.0
CALL VORITY
IF(GOSA.EQ.0.0.AND.TOTA.EQ.0.0) GO TO 10
SAN(NW)=GOSA/TOTA
GO TO 40
10 SAN(NW)=1.
40 CONTINUE
C*** STREAM FUNCTION SUB-CYCLE
GOSA=0.0
TOTA=0.0
CALL STRFUN
IF(GOSA.EQ.0.0.AND.TOTA.EQ.0.0) GO TO 20
SAN(NF)=GOSA/TOTA
GO TO 50
20 SAN(NF)=1.
50 CONTINUE
CALL VELDIS
CALL WALL
C*** SUB-CYCLE FOR TURBULENT VARIABLES
DO 41 K=NK,NEP
GOSA=0.0
TOTA=0.0
CALL TURVAR(K)
IF(GOSA.EQ.0.0.AND.TOTA.EQ.0.0) GO TO 30
SAN(K)=GOSA/TOTA
GO TO 41

```

```

SAR05610
SAR05620
SAR05630
SAR05640
SAR05650
SAR05660
SAR05670
SAR05680
SAR05690
SAR05700
SAR05710
SAR05720
SAR05730
SAR05740
SAR05750
SAR05760
SAR05770
SAR05780
SAR05790
SAR05800
SAR05810
SAR05820
SAR05830
SAR05840
SAR05850
SAR05860
SAR05870
SAR05880
SAR05890
SAR05900
SAR05910
SAR05920
SAR05930
SAR05940
SAR05950
SAR05960

```

```

30 SAN(K)=1.
41 CONTINUE
C *** TEMPERATURE SUB CYCLE
GOSA=0.0
TOTA=0.0
CALL TEMPR
IF(GOSA.EQ.0.0.AND.TOTA.EQ.0.0) GO TO 25
SAN(NT)=GOSA/TOTA
GO TO 26
25 SAN(NT)=1.
26 CONTINUE
C*** INITIATE ITERATION ON BOUNDARY NODES
CALL BOUND
C *** READJUST PROPERTIES AND ISOTHERMS
CALL PROP(2)
RETURN
END
SAR05970
SAR05980
SAR05990
SAR06000
SAR06010
SAR06020
SAR06030
SAR06040
SAR06050
SAR06060
SAR06070
SAR06080
SAR06090
SAR06100
SAR06110
SAR06120
SAR06130

```

```

SUBROUTINE VORTICITY
COMMON/CB/BE(71),BW(71),BN(15),BS(15)
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CCRIT/NWI,NWJ,NFI,NFJ,GOSA,TOTA
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,S0,HL
DO 11 J=2,JNM
  IL=I1+1
  IF(J.LE.J1) IL=I2+1
  IH=I3-1
  DO 11 I=IL,IH
    CALL SOURCE,I,J,NW)
    CALL CONVEC(AE,AW,AN,AS,I,J,NW)
    RSQ=R(J)*R(J)
    BBE=2.*RSQ*BE(I)
    BBW=2.*RSQ*BW(I)
    BBN=(R(J+1)*R(J+1)+RSQ)*BN(J)
    BBS=(R(J-1)*R(J-1)+RSQ)*BS(J)
  IMPLICIT VORTICITY CALCULATIONS
  TERM1=A(I+1,J,NW)
  TERM2=A(I-1,J,NW)
  TERM3=A(I,J-1,NW)
  TERM4=A(I,J+1,NW)
  TERM5=0.0
  IF(J.NE.JNM) GO TO 12
  DX2=X2(JN)-X2(JNM)
  DT=A(I,JNM,NT)-A(I,JN,NT)
  BT=BETA(1)
  BOU= 2.452*A(I,JN,NRO)*BT*DX2*DT/A(I,JNM,NMU)/R(JN)
  TERM4 =3.*(A(I,JN,NF)-A(I,JNM,NF))/DX2/DX2/RSQ /A(I,JN,NRO)
  TERM4=TERM4+BOU
  TERM5=0.5*(AN+A(I,J+1,NMU)*BBN)
GO TO 14

```

C

SAR06140
SAR06150
SAR06160
SAR0617C
SAR06180
SAR06190
SAR06200
SAR0621C
SAR06220
SAR06230
SAR06240
SAR06250
SAR06260
SAR0627C
SAK06280
SAR06290
SAR06300
SAR06310
SAR06320
SAR0633C
SAR06340
SAR06350
SAR06360
SAR06370
SAR06380
SAR06390
SAR0640C
SAR06410
SAR06420
SAR06430
SAR06440
SAR06450
SAR0646C
SAR06470
SAR06480
SAR06490

```

12 IF(I.NE.(I2+1)) GO TO 15
   IF(J.GT.J1) GO TO 15
   DX12=(X1(I2+1)-X1(I2))*#2
   TERM2 =3.*(A(I2,J,NF)-A(I2+1,J,NF))/DX12/RSQ/A(I2,J,NRO)
   TERM5=0.5*( AW+A(I-1,J,NMU)*BBW)
   GO TO 14

15 IF(J.NE.(J1+1)) GO TO 16
   IF(I.GT.I2) GO TO 16
   DX2=X2(J1+1)-X2(J1)
   DX22=DX2*DX2
   BT=BETA(I)
   DT=A(I,J1,NT)-A(I,J1+1,NT)
   BOU= 2.452*A(I,J1,NRO)*BT*DX2*DT/A(I,J1+1,NMU)/R(J1)
   TERM3 =3.*(A(I,J1,NF)-A(I,J1+1,NF))/DX22/RSQ/A(I,J1,NRO)
   TERM3=TERM3+BOU
   TERM5=0.5*(AS+A(I,J-1,NMU)*BBS)
   GO TO 14

16 IF(I.NE.(I3-1)) GO TO 14
   DX12=(X1(I3)-X1(I3-1))*#2
   TERM1 =3.*(A(I3,J,NF)-A(I3-1,J,NF))/DX12*RSQ*A(I3,J,NRO)
   TERM5=0.5*( AE+A(I+1,J,NMU)*BBE)
   GO TO 14

14 CONTINUE
   ANUM=(AE+A(I+1,J,NMU)*BBE)*TERM1
   1+(AW+A(I-1,J,NMU)*BBW)*TERM2
   2+(AS+A(I,J-1,NMU)*BBS)*TERM3
   3+(AN+A(I,J+1,NMU)*BBN)*TERM4
   ADNM=AE+AW+AN+AS+A(I,J,NMU)*(BBE+BBW+DBN+BBS)+TERMS
   IF(ADNM.EQ.0.) GO TO 4
   Z=A(I,J,NW)
   A(I,J,NW)=ANUM/ADNM
   IF(Z.EQ.0.0.AND.A(I,J,NW).EQ.0.0) GO TO 1
   RS=1.-Z/A(I,J,NW)
   GO TO 3
1 RS=0.
3 CONTINUE
GOSA=GOSA+ABS(Z-A(I,J,NW))

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SAR06500
SAR06510
SAR06520
SAR06530
SAR06540
SAR06550
SAR06560
SAR06570
SAR06580
SAR06590
SAR06600
SAR06610
SAR06620
SAR06630
SAR06640
SAR06650
SAR06660
SAR06670
SAR06680
SAR06690
SAR06700
SAR06710
SAR06720
SAR06730
SAR06740
SAR06750
SAR06760
SAR06770
SAR06780
SAR06790
SAR06800
SAR06810
SAR06820
SAR06830
SAR06840
SAR06850

```

    TOT A=TOT A+ABS(A(I,J,NW))
C*** UNDER- OR OVER-RELAX
    A(I,J,NW)=Z+RP(NW)*(A(I,J,NW)-Z)
C*** STORE MAXIMUM RESIDUAL
    IF(ABS(RS)-LE.ABS(RSDU(NW))) GO TO 4
    RSDU(NW)=RS
    NWJ=J
    NWI=I
    4 CONTINUE
    11 CONTINUE
    RETURN
    END

```

```

SAR0686C
SAR06870
SAR06880
SAR06890
SAR06900
SAR06910
SAR0692C
SAR06930
SAR06940
SAR06950
SAR0696C
SAR06970

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SUBROUTINE STRFUN
COMMON/CB/BE(71),BW(71),BN(15),BS(15)
COMMON/COVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CCRIT/NWI,NWJ,NFI,NFJ,GOSA,TOTA
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
DO 21 J=2,JNM
IL=I1+1
IF(J.LE.J1) IL=I2+1
IH=I3-1
DO 21 I=IL,IH
CALL SOURCE(SOURCE,I,J,NF)
RISQ=1./R(J)/R(J)
ROP=A(I,J,NRO)
BBE=4./(A(I+1,J,NRO)+ROP)*RISQ*BE(I)
BBW=4./(A(I-1,J,NRO)+ROP)*RISQ*BW(I)
BBN=16./(A(I,J+1,NRO)+ROP)/((R(J+1)+R(J))**2)*BN(J)
BBS=16./(A(I,J-1,NRO)+ROP)/((R(J-1)+R(J))**2)*BS(J)
ANUM=BBE*A(I+1,J,NF)+BBW*A(I-1,J,NF)+BBN*A(I,J+1,NF)
I+BBW*A(I,J-1,NF)+SOURCE
ADNM=BBE+BBW+BBN+BBS
IF(ADNM.EQ.0.) GO TO 5
Z=A(I,J,NF)
A(I,J,NF)=ANUM/ADNM
IF(Z.EQ.0.0.AND.A(I,J,NF).EQ.0.0) GO TO 8
RS=1.-Z/A(I,J,NF)
GO TO 6
8 RS=0.0
6 CONTINUE
GOSA=GOSA+ABS(Z-A(I,J,NF))
TOTA=TOTA+ABS(A(I,J,NF))
A(I,J,NF)=Z+RP(NF)*(A(I,J,NF)-Z)
IF(ABS(RS).LE.ABS(RSDU(NF))) GO TO 5
RSDU(NF)=RS

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SAR06980
SAR06990
SAR07000
SAR07010
SAR07020
SAR07030
SAR07040
SAR07050
SAR07060
SAR07070
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SAR07090
SAR07100
SAR07110
SAR07120
SAR07130
SAR07140
SAR07150
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SAR07260
SAR07270
SAR07280
SAR07290
SAR07300
SAR07310
SAR07320
SAR07330

SAR07340
SAR07350
SAR07360
SAR07370
SAR07380
SAR07390

NFJ=J
NFI=I
5 CONTINUE
21 CONTINUE
RETURN
END

```

SUBROUTINE TURVAR(K)
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CBB/BRE,BBW,BBN,BBS,BPP
COMMON/CSORSE/SOURCE,SPRIME
COMMON/CCRIT/NWI,NWJ,NFI,NFJ,GOSA,TOTA
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CB/BE(71),BW(71),BN(15),BS(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
DO 31 J=2, JNM
  IL=I1+1
  IF(J.LE.J1) IL=I2+1
  IH=I3-1
DO 31 I=IL, IH
  BPP=A(I,J,NMU)
  BBE=(A(I+1,J,NMU)+BPP)/PR(K)*BE(I)
  BBW=(A(I-1,J,NMU)+BPP)/PR(K)*BW(I)
  BBN=(A(I,J+1,NMU)+BPP)/PR(K)*BN(J)
  BBS=(A(I,J-1,NMU)+BPP)/PR(K)*BS(J)
  SPRIME=0.
CALL SOURCE(SOURCE,I,J,K)
CALL CONVEC(AE,AW,AN,AS,I,J,K)
ANUM=(AE+BDE)*A(I+1,J,K)+(AW+BBW)*A(I-1,J,K)+(AN+BBN)*A(I,J+1,K)
I+(AS+BBS)*A(I,J-1,K)+SOURCE
ADNM=AE+AW+AN+AS+BBE+BBW+BBN+BBS+SPRIME
IF(ADNM.EQ.0.) GO TO 6
Z=A(I,J,K)
A(I,J,K)=ANUM/ADNM
IF(Z.EQ.0.0.AND.A(I,J,K).EQ.0.0) GO TO 3
RS=1.-Z/A(I,J,K)
GO TO 5
3 RS=0.0
5 CONTINUE
GOSA=GOSA+ABS(Z-A(I,J,K))

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SAR07400
SAR0741C
SAR07420
SAR07430
SAR07440
SAR07450
SAR07460
SAR07470
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SAR07510
SAR07520
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SAR07560
SAR07570
SAR07580
SAR07590
SAR07600
SAR0761C
SAR07620
SAR07630
SAR07640
SAR07650
SAR07660
SAR0767C
SAR07680
SAR07690
SAR07700
SAR0771C
SAR07720
SAR07730
SAR0774C
SAR07750

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TOTL=TOTL+ABS(A(I,J,K))
A(I,J,K)=Z+RP(K)*(A(I,J,K)-Z)
IF(A(I,J,K)-LE.0.0) A(I,J,K)=0.0
IF(ABS(RS).LT.ABS(RSDU(K))) GO TO 6
RSDU(K)=RS
  6 CONTINUE
 31 CONTINUE
  RETURN
  END

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SAR07760
SAR07770
SAR07780
SAR07790
SAR07800
SAR07810
SAR07820
SAR07830
SAR07840

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SUBROUTINE TEMPR
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCRIT/NWI,NWJ,NFI,NFJ,GOSA,TOTA
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CB/BE(71),BW(71),BN(15),BS(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CAVI/TB
COMMON/CTRVL/VE,VC
COMMON/CDROP/TAU,HCD,D,QS,QM
COMMON/CLS/YL(15),YS(15)
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SB,HL
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CBB/BBE,BBW,BBN,BBS,BPP
COMMON/CSNW/SN1(20),SN2(15),SN3(21),SN4(10)
COMMON/CSORSE/SOURCE,SPRIME
COMMON/CTEMP/TLM,TSM,TLS,TA,TM,TW
COMMON/CFLD/B(71,15,10),LF,CU
COMMON/CHJ/NHR,NHI,NH,NJRR,NJRI,NJR,NJZR,NJZI,NJZ,NJJ
COMMON/CAVM/AVM(20)
C *** CALCULATE AVERAGE BULK TEMPERATURE OF SLAG, TB
J11=J1-1
DO 33 I=I2,I3
N=I-I2+1
SUMT=0.
DO 34 J=1,J11
DR=R(J+1)-R(J)
34 SUMT=SUMT+(R(J)*A(I,J,NT)+R(J+1)*A(I,J+1,NT))*DR
33 AVM(N)=SUMT/R(J1)/R(J1)
N3=I3-I2
SUMT=0.
DO 35 N=1,N3
I=N+I2-1
DZ=(X1(I+1)-X1(I))*0.5
35 SUMT=SUMT+(AVM(N)+AVM(N+1))*DZ

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SAR07850
SAR07860
SAR07870
SAR07880
SAR0789C
SAR07900
SAR07910
SAR0792C
SAR07930
SAR07940
SAR07950
SAR07960
SAR07970
SAR07980
SAR07990
SAR08000
SAR0801C
SAR08020
SAR08030
SAR08040
SAR0805C
SAR08060
SAR08070
SAR08080
SAR08090
SAR08100
SAR08110
SAR0812C
SAR08130
SAR08140
SAR08150
SAR08160
SAR08170
SAR08180
SAR0819C
SAR08200

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SAR08210
SAR08220
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SAR08380
SAR08390
SAR08400
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SAR08560

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PAGE 29

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TB=SUMT/(X1(I3)-X1(I2))
TF=TB-(TB-TLM)/EXP(D*TAU)
QS=HCD*(TF-TLM)
C *** CALCULATE VOLUME OF THE METAL POOL
SUMV=0.
DO 14 J=1,JNM
DX=R(J+1)-R(J)
SUMV=SUMV+(R(J)*YL(J)+R(J+1)*YL(J+1))*DX
14 CONTINUE
VOL=SUMV*3.14
QM=QS/VOL
DO 10 J=2,JNM
IL=2
IF(J.EQ.J1) IL=I2+1
IF(J.GT.J1) IL=I1+1
DO 11 I=IL,INM
IF(I.EQ.I2.AND.J.LE.J1) GO TO 11
IF(I.EQ.I3) GO TO 11
IF(J.GT.J1.AND.I.LE.I2) GO TO 20
IF(I.GT.I2.AND.I.LT.I3) GO TO 20
VV=VE
IF(I.GT.I3) VV=VC
AEW=VV/(X1(I+1)-X1(I-1))*A(I,J,NRO)*A(I,J,NSP)
BPP=A(I,J,NTC)
BBE=(A(I+1,J,NTC)+BPP)*BE(I)
BBW=(A(I-1,J,NTC)+BPP)*BW(I)
BBN=(A(I,J+1,NTC)+BPP)*BN(J)
DBS=(A(I,J-1,NTC)+BPP)*BS(J)
IF(I.LT.I3) GO TO 36
XSM=X1(I)-X1(I3)
IF(XSM.GT.YL(J).AND.XSM.LE.YS(J)) GO TO 31
SOURCE=QM
GO TO 32
31 SOURCE=ADF(I,J,I,NT)/(TLM-TSM)
SOURCE=-VC*HL*A(I,J,NRO)*SOURCE
GO TO 32

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```

36 SOURCE=0.
32 CONTINUE
   ANUM=BBE*A(I+1,J,NT)+BBW*A(I-1,J,NT)+BBN*A(I,J+1,NT)
   1+BBN*A(I,J-1,NT)+SOURCE+AEW*(A(I-1,J,NT)-A(I+1,J,NT))
   ADMN=BBE+BBW+BBN+BBS
   GO TO 21
20 CONTINUE
   CALL SOURCE(SOURCE,I,J,NT)
   BPP=A(I,J,NMT)*A(I,J,NSP)/PR(NT)+A(I,J,NTC)
   BBE=(A(I+1,J,NMT)*A(I+1,J,NSP)/PR(NT)+A(I+1,J,NTC)+BPP)*BE(I)
   BBW=(A(I-1,J,NMT)*A(I-1,J,NSP)/PR(NT)+A(I-1,J,NTC)+BPP)*BW(I)
   BBN=(A(I,J+1,NMT)*A(I,J+1,NSP)/PR(NT)+A(I,J+1,NTC)+BPP)*BN(J)
   BBS=(A(I,J-1,NMT)*A(I,J-1,NSP)/PR(NT)+A(I,J-1,NTC)+BPP)*BS(J)
   SPRIME=0.
   CALL CONVEC(AE,AW,AN,AS,I,J,NT)
   AEW= VC/(X1(I+1)-X1(I-1))*A(I,J,NRO)*A(I,J,NSP)
   AE=AE-AEW
   AW=AW+AEW
   K=NT
   ANUM=(AE+BBE)*A(I+1,J,K)+(AW+BBW)*A(I-1,J,K)+(AN+BBN)*A(I,J+1,K)
   1+(AS+BBS)*A(I,J-1,K)+SOURCE
   ADMN=AE+AW+AN+AS+BBE+BBW+BBN+BBS+SPRIME
21 CONTINUE
   IF(ADNM.EQ.0.) GO TO 11
   Z=A(I,J,NT)
   A(I,J,NT)=ANUM/ADNM
   IF(Z.EQ.0.0.AND.A(I,J,NT).EQ.0.0) GO TO 1
   RS=1.-Z/A(I,J,NT)
   GO TO 3
1 RS=0.
3 CONTINUE
   GOSA=GOSA+ABS(Z-A(I,J,NT))
   TOTA=TOTA+ABS(A(I,J,NT))
   A(I,J,NT)=Z+RP(NT)*(A(I,J,NT)-Z)
   IF(ABS(RS).LE.ABS(RSDU(NT))) GO TO 4
   RSDU(NT)=RS

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SAR08570
SAR08580
SAR08590
SAR08600
SAR08610
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SAR08680
SAR08690
SAR08700
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SAR08790
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SAR08820
SAR08830
SAR08840
SAR08850
SAR08860
SAR08870
SAR08880
SAR08890
SAR08900
SAR08910
SAR08920

4 CONTINUE
11 CONTINUE
10 CONTINUE
RETURN
END

SAR08930
SAR08940
SAR0895C
SAR08960
SAR08970

```

SUBROUTINE WALL
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SB,HL
COMMON/CCONT/C1,C2,C3,CD
COMMON/CTAUW/TAUW1(20),TAUW2(15),TAUW3(21),TAUW4(10),CAPPA,E
COMMON/CSNW/SN1(20),SN2(15),SN3(21),SN4(10)
A1=ROREF(2)*CD**0.25
PRL=SPREF(2)*ZMUREF(1)/TCREF(2)
RECPRT=1./PR(NT)
PRRAT=PRL*RECPRT
PJAY=9.*(PRRAT-1.)/(PRRAT**0.25)
***** AT J=JN,TAUWI , SNI
YP=X2(JN)-X2(JNM)
IL=I1+1
IH=I3-1
DO 1 I=IL,IH
N=I-IL+1
A2=A1*SQRT(A(I,JNM,NK))
YPP=YP*A2/ZMUREF(1)
UP=ABS(A(I,JNM,NV1))
IF(YPP.GT.11.5) GO TO 2
TAUWI(N)=ZMUREF(1)*UP/YP
GO TO 3
2 TAUWI(N)=CAPPA*UP*A2/ALOG(YPP*E)
3 FRIC=TAUWI(N)/(UP*UP*ROREF(2))
SNI(N)=FRIC*RECPRT/(1.+PJAY*SQRT(FRIC))
SNI(N)=SNI(N)*ROREF(2)*SPREF(2)*UP
***** AT I=I2+1,I<J<JI
YP=X1(I2+1)-X1(I2)
DO 4 J=2,JI
A2=A1*SQRT(A(I2+1,J,NK))
YPP=YP*A2/ZMUREF(1)

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SAR08980
SAR08990
SAR09000
SAR09010
SAR09020
SAR09030
SAR09040
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SAR0907C
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SAR09090
SAR09100
SAR09110
SAR09120
SAR09130
SAR0914C
SAR09150
SAR09160
SAR09170
SAR09180
SAR09190
SAR0920C
SAR09210
SAR09220
SAR09230
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SAR09250
SAR0926C
SAR09270
SAR09280
SAR09290
SAR09300
SAR09310
SAR09320
SAR0933C


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UP=ABS(A(I2+1,J,NV2))
IF(YPP.GT.11.5) GO TO 5
TAUW2(J)=ZMUREF(1)*UP/YP
GO TO 6
5 TAUW2(J)=CAPP*UP*A2/ALOG(YPP*E)
6 FRIC=TAUW2(J)/(UP*UP*ROREF(2))
SN2(J)=FRIC*RECPRT/(1.+PJAY*SQRT(FRIC))
SN2(J)=SN2(J)*ROREF(2)*SPREF(2)*UP
40 CONTINUE
4 CONTINUE
C ***
      AT I=I3-1,I<J<JN , TAUW3 , SN3
      YP=X1(I3)-X1(I3-1)
      DO 7 J=2,JNM
      A2=A1*SQRT(A(I3-1,J,NK))
      YPP=YP*A2/ZMUREF(1)
      UP=ABS(A(I3-1,J,NV2))
      IF(YPP.GT.11.5) GO TO 8
      TAUW3(J)=ZMUREF(1)*UP/YP
      GO TO 9
8 TAUW3(J)=CAPP*UP*A2/ALOG(YPP*E)
9 FRIC=TAUW3(J)/(UP*UP*ROREF(2))
SN3(J)=FRIC*RECPRT/(1.+PJAY*SQRT(FRIC))
SN3(J)=SN3(J)*ROREF(2)*SPREF(2)*UP
TCM=A(I3-1,J,NTC)
SN3(J)=TCM/(X1(I3)-X1(I3-1))
70 CONTINUE
7 CONTINUE
C ***
      AT J=J1+1,I1<I2
      IF(I1.EQ.I2) GO TO 15
      YP=X2(J1+1)-X2(J1)
      IL=I1+1
      I21=I2-1
      DO 10 I=IL,I2
      N=I-IL+1
      A2=A1*SQRT(A(I,J1+1,NK))
      YPP=YP*A2/ZMUREF(1)

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SAR09340
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SAR09680
SAR09690

SAR09700
SAR09710
SAR09720
SAR09730
SAR09740
SAR09750
SAR09760
SAR09770
SAR09780
SAR09790
SAR09800
SAR09810
SAR09820
SAR09830
SAR09840

```
UP=ABS(A(I,J1+1,NV1))
IF(YPP.GT.11.5) GO TO 11
TAUW4(N)=ZMUREF(1)*UP/YP
GO TO 12
11 TAUW4(N)=CAPP*A*UP*A2/ALOG(YPP*E)
12 FRIC=TAUW4(N)/(UP*UP*RREF(2))
SN4(N)=FRIC*RECPT/(1.+PJAY*SQRT(FRIC))
SN4(N)=SN4(N)*RREF(2)*SPREF(2)*UP
TCM=A(I,J1+1,NTC)
SN4(N)=TCM/(X2(J1+1)-X2(J1))
100 CONTINUE
10 CONTINUE
15 CONTINUE
RETURN
END
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SUBROUTINE BOUND
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CDROP/TAU,HCD,D,QS,QM
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CLS/YL(15),YS(15)
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SB,HL
COMMON/CSNW/SN1(20),SN2(15),SN3(21),SN4(10)
COMMON/CVF/FES(21),FEM(21),FSM,FSE
COMMON/CTEMP/TLM,TSM,TLS,TA,TM,TW
COMMON/CHEAT/HC,HW(4)
J11=J1-1
C ** AT I=1, J<J1
DO 50 J=1, J1
50 A(1,J,NT)=(4.*A(2,J,NT)-A(3,J,NT))/3.
C ** AT THE CENTER
R3SQ =R(3)*R(3)
R2SQ =R(2)*R(2)
BB =R3SQ / (R3SQ -R2SQ )
DO 41 I=2, INM
A(I,1,NT)=BB*A(I,2,NT)+(1.-BB)*A(I,3,NT)
IF(I.LT.I2.OR.I.GT.I3) GO TO 41
A(I,1,NW)=(A(I,1,NF)-A(I,3,NF))/R3SQ+(A(I,2,NF)-A(I,1,NF))/R2SQ
A(I,1,NW) =8.*A(I,1,NW) / A(I,1,NRO) / (R3SQ-R2SQ)
A(I,1,NK)=BB*A(I,2,NK)+(1.-BB)*A(I,3,NK)
A(I,1,NEP)=BB*A(I,2,NEP)+(1.-BB)*A(I,3,NEP)
41 CONTINUE
C** AT SIDE WALL
C **@ VORTICITY
DX2=X2(JN)-X2(JNM)
DO 42 I=11,I3
Z=A(I,JN,NW)
DT=A(I,JNM,NT)-A(I,JN,NT)

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SAR09850
SAR09860
SAR09870
SAR09880
SAR09890
SAR09900
SAR09910
SAR09920
SAR09930
SAR09940
SAR09950
SAR09960
SAR09970
SAR09980
SAR09990
SAR10000
SAR10010
SAR10020
SAR10030
SAR10040
SAR10050
SAR10060
SAR10070
SAR10080
SAR10090
SAR10100
SAR10110
SAR10120
SAR10130
SAR10140
SAR10150
SAR10160
SAR10170
SAR10180
SAR10190
SAR10200

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SAR10210
SAR10220
SAR10230
SAR10240
SAR10250
SAR1026C
SAR10270
SAR10280
SAR10290
SAR10300
SAR10310
SAR10320
SAR1033C
SAR10340
SAR10350
SAR10360
SAR1037C
SAR10380
SAR10390
SAR10400
SAR10410
SAR10420
SAR10430
SAR10440
SAR10450
SAR10460
SAR1047C
SAR10480
SAR10490
SAR10500
SAR10510
SAR10520
SAR10530
SAR10540
SAR10550
SAR1056C

```

```

BT=BETA(1)
BOU= 2.452*A(I,JN,NRO)*BT*DX2*DT/A(I,JNM,NMU)/R(JN)
A(I,JN,NW)=3.*(A(I,JN,NF)-A(I,JNM,NF))/DX2/DX2/R(JN)/A(I,JN,NRO)
A(I,JN,NW)=A(I,JN,NW)/R(JNM)-0.5*A(I,JNM,NW)+BOU
A(I,JN,NW)=Z+RP(NW)*(A(I,JN,NW)-Z)
42 CONTINUE
C *** TEMPERATURE
J=JN
DO 54 I=I3,INM
XSM=X1(I)-X1(I3)
IF(I.LT.I3) HTW=HW(1)
IF(I.GE.I3.AND.XSM.LE.YL(J)) HTW=HW(2)
IF(XSM.GT.YL(J).AND.XSM.LE.YS(J)) HTW=HW(3)
IF(XSM.GT.YS(J)) HTW=HW(4)
TT=TW
BB=(X2(JN)-X2(JNM))*HTW*2./A(I,JN,NTC)
A(I,JN,NT)=4.*A(I,JNM,NT)-A(I,JNM-1,NT)
54 A(I,JN,NT)=(A(I,JN,NT)+BB*TT)/(3.+BB)
IF(A(I3,JN,NT).LT.TLM) A(I3,JN,NT)=TLM
C*** AT FREE SURFACE
C *** FIRST CALCULATE THE AVERAGE SLAG TEMPERATURE(AT SURFACE)
SUMT=0.
DO 51 J=J1,JNM
DR=R(J+1)-R(J)
SUMT=SUMT+(R(J)*A(I1,J,NT)+R(J+1)*A(I1,J+1,NT))*DR
51 TSA=SUMT/(R(JN)*R(JN)-R(J1)*R(J1))
TSA=TSA*0.0010
C *** NOW CALCULATE AV. ELECTRODE SURFACE TEMPERATURE,TEA
SUMF=0.
I11=I1-1
DO 52 I=1,I11
DZ=(X1(I+1)-X1(I))*0.5
SUMT=SUMT+(A(I,J1,NT)+A(I+1,J1,NT))*DZ
52 TEA=SUMT/(X1(I1)-X1(1))*0.001
TMI=TM*0.001
XQ=X1(I1+1)-X1(I1)

```

```

SAR10570
SAR10580
SAR10590
SAR10600
SAR10610
SAR10620
SAR10630
SAR10640
SAR10650
SAR10660
SAR10670
SAR10680
SAR10690
SAR10700
SAR10710
SAR10720
SAR10730
SAR10740
SAR10750
SAR10760
SAR10770
SAR10780
SAR10790
SAR10800
SAR10810
SAR10820
SAR10830
SAR10840
SAR10850
SAR10860
SAR10870
SAR10880
SAR10890
SAR10900
SAR10910
SAR10920

```

XR=X1(I1+2)-X1(I1)
DB=XR*XR/(XR*XR-XC*XQ)
A2=TSA**4-FSM*EM*TM1**4-EE*FSE*TEA**4
J12=J1+1
DO 44 J=J12,JNM
AK=A(I1,J,NTC)+A(I1,J,NMT)*A(I1,J,NSP)/PR(NT)
A1=SB*ES*XQ/AK*2.
C *** NEGLECT CONVECTIVE TR. AT THE SLAG SURFACE
A3=0.
A(I1,J,NT)=4.*A(I1+1,J,NT)-A(I1+2,J,NT)-A1*A2+A3*TA
A(I1,J,NT)=A(I1,J,NT)/(3.+A3)
A(I1,J,NK)=BB*A(I1+1,J,NK)+(1.-BB)*A(I1+2,J,NK)
A(I1,J,NEP)=BB*A(I1+1,J,NEP)+(1.-BB)*A(I1+2,J,NEP)
44 CONTINUE
C *** AT SLAG-METAL INTERFACE Z=Z3 , ASSUMED TO BE A SOLID WALL
DX12=(X1(I3)-X1(I3-1))**2
DO 43 J=2,JNM
RSQ=R(J)*R(J)
A(I3,J,NW)=3.*A(I3,J,NF)-A(I3-1,J,NF)/(DX12*RSQ*ROREF(2))
1-0.5*A(I3-1,J,NW)
XF=X1(I3+1)-X1(I3)
TCM=A(I3,J,NTC)
BB=SN3(J)*XF/TCM
ANUM=A(I3+1,J,NT)+BB*A(I3-1,J,NT)
ADNM=1.+BB
Z=A(I3,J,NT)
A(I3,J,NT)=ANUM/ADNM
A(I3,J,NT)=Z+RP(NT)*(A(I3,J,NT)-Z)
43 CONTINUE
C *** AT I=I2,J<J1
DX12=(X1(I2+1)-X1(I2))**2
DO 40 J=2,J1
RSQ=R(J)*R(J)
A(I2,J,NW)=3.*A(I2,J,NF)-A(I2+1,J,NF)/(DX12/RSQ/A(I2,J,NRO))
A(I2,J,NW)=A(I2,J,NW)-0.5*A(I2+1,J,NW)
40 CONTINUE

```

C *** AT THE CORNER I=I2,J=J1
      RSQ=R(J1)*R(J1)
      DXSS=(X2(J1+1)-X2(J1))*2+(X1(I2+1)-X1(I2))*2
      A(I2,J1,NW)=3.*(A(I2,J1,NF)-A(I2+1,J1+1,NF))/DXSS/RSQ/A(I2,J1,NRO)
      A(I2,J1,NH)=A(I2,J1,NW)-0.5*A(I2+1,J1+1,NW)
C *** TEMP. AT J=J1, 2<I<I1
      DX2=R(J1)-R(J11)
      DO 53 I=2,I11
      A1=HC*DX2*2./A(I,J1,NTC)
      A2=EE*SB*DX2*2./A(I,J1,NTC)
      Z=A(I,J1,NT)
      A4=ES*FES(I)*TSA**4
      A5=EM*FEM(I)*TMI**4
      A3=0.0001*A(I,J1,NT)
      DNM=3.+A1+A2*(A3**3)
      ANM=4.*A(I,J1,NT)-A(I,J11-1,NT)+A1*TA+A2*(A4+A5)
      A(I,J1,NT)=ANM/DNM
53   A(I,J1,NT)=Z+RP(NT)*(A(I,J1,NT)-Z)
C *** AT J=J1, I1<I<I2
      IF(I1.EQ.I2) GO TO 47
      DX2=X2(J1+1)-X2(J1)
      DX22=DX2*DX2
      I21=I2-1
      RSQ=R(J1)*R(J1+1)
      XB=X2(J1)-X2(J11)
      BT=BETA(I)
      DO 45 I=I1,I21
      TCM=A(I,J11,NTC)
      IF(I.EQ.I1) GO TO 48
      BB=SN4(I-I1)
      GC TO 49
48   BB=A(I,J1+1,NTC)/DX2
49   BB=BB*2.*XB/TCM
      A(I,J1,NT)=4.*A(I,J11,NT)-A(I,J11-1,NT)+BB*A(I,J1+1,NT)
      A(I,J1,NT)=A(I,J1,NT)/(3.+BB)
      Z=A(I,J1,NW)

```

```

DT=A(I,J1,NT)-A(I,J1+1,NT)
BOU= 2.452*A(I,J1,NRO)*BT*DX2*DT/A(I,J1+1,NMU)/R(J1)
A(I,J1,NW)=3.*(A(I,J1,NF)-A(I,J1+1,NF))/DX2/RSQ/A(I,J1,NRO)
A(I,J1,NW)=A(I,J1,NW)-0.5*A(I,J1+1,NW)+BOU
A(I,J1,NW)=Z+RP(NW)*(A(I,J1,NW)-Z)
45 CONTINUE
47 CONTINUE
C *** AT I=IN
XQ=X1(IN)-X1(INM)
XR=X1(IN)-X1(INM-1)
BB=XR*XR/(XR*XR-XQ*XQ)
DO 55 J=1,JN
55 A(IN,J,NT)=BB*A(INM,J,NT)+(1.-BB)*A(INM-1,J,NT)
RETURN
END
SAR11290
SAR11300
SAR11310
SAR1132C
SAR11330
SAR11340
SAR11350
SAR11360
SAR11370
SAR11380
SAR11390
SAR11400
SAR11410
SAR1142C
SAR11430

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```

SUBROUTINE CONVEC(AE,AW,AN,AS,I,J,K)
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
COMMON/CBB/BBE,BBW,BBN,BBS,BPP
COMMON/CSORSE/SOURCE,SPRIME
COMMON/CTAUW/TAUW1(20),TAUW2(15),TAUW3(21),TAUW4(10),CAPPA,E
COMMON/CCONT/C1,C2,C3,CD
COMMON/CSNW/SN1(20),SN2(15),SN3(21),SN4(10)
COMMON/CGEOM/FR(4)
C*****
C SUBROUTINE FOR CALCULATION OF AE,AW,AN,AS
C*****
C** CALCULATION MEAN MASS FLOW RATE AT FOUR TUBES OF THE TANK
DV=R(J)*(X1(I+1)-X1(I-1))*(X2(J+1)-X2(J-1))
GIPW=(A(I,J+1,NF)-A(I,J-1,NF)+A(I-1,J+1,NF)-A(I-1,J-1,NF))/DV
GIPE=(A(I,J+1,NF)-A(I,J-1,NF)+A(I+1,J+1,NF)-A(I+1,J-1,NF))/DV
G2PS=(A(I-1,J,NF)-A(I+1,J,NF)+A(I-1,J-1,NF)-A(I+1,J-1,NF))/DV
G2PN=(A(I-1,J,NF)-A(I+1,J,NF)+A(I-1,J+1,NF)-A(I+1,J+1,NF))/DV
C *** ACCOUNT FOR THE WALL FUNCTION
IF(K.EQ.NW.OR.K.EQ.NF) GO TO 10
IF(I.EQ.(I3-1).AND.K.EQ.NI) GO TO 10
IF(J.EQ.(J1+1).AND.K.EQ.NI) GO TO 10
IF(J.NE.JNM) GO TO 7
GIPE=- (A(I,J-1,NF)+A(I,J,NF)+A(I+1,J,NF)+A(I+1,J-1,NF))/DV
GIPW=- (A(I,J-1,NF)+A(I,J,NF)+A(I-1,J,NF)+A(I-1,J-1,NF))/DV
BBE=BDE*FR(1)
BBW=BBW*FR(1)
BBN=0.0
G2PN=0.
IF(K.NE.NK) GO TO 15
DX=X2(JN)-X2(JNM-1)
UA=ABS(A(I,JNM,NV1)+A(I,JNM-1,NV1))/DX
TAUW=TAUW1(I-1)

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SAR11440
SAR11450
SAR11460
SAR11470
SAR11480
SAR11490
SAR11500
SAR11510
SAR11520
SAR11530
SAR11540
SAR11550
SAR11560
SAR11570
SAR11580
SAR11590
SAR11600
SAR11610
SAR11620
SAR11630
SAR11640
SAR11650
SAR11660
SAR11670
SAR11680
SAR11690
SAR11700
SAR11710
SAR11720
SAR11730
SAR11740
SAR11750
SAR11760
SAR11770
SAR11780
SAR11790


```

15 GO TO 20
   IF(K.NE.NEP) GO TO 16
   YP=X2(JN)-X2(JNM)
   GO TO 21
16 B1=FR(1)
   B2=2.*R(J+1)/R(J)/(X2(J+1)-X2(J-1))
   SNW=SN1(I-1)
   TWALL=A(I,J+1,NT)
   GO TO 22
7   IF(I.NE.(I2+1)) GO TO 8
   IF(J.GT.J1) GO TO 8
   G2PN=-(A(I,J+1,NF)+A(I,J,NF)+A(I+1,J,NF)+A(I+1,J+1,NF))/DV
   G2PS=-(A(I,J-1,NF)+A(I,J,NF)+A(I+1,J,NF)+A(I+1,J-1,NF))/DV
   G1PW=0.
   BBN=BBN*FR(2)
   BBS=BBS*FR(2)
   BBW=0.0
   IF(K.NE.NK) GO TO 17
   DX=X1(I2+2)-X1(I2)
   UA=ABS(A(I2+1,J,NV2)+A(I2+2,J,NV2))/DX
   TAUW=TAUW2(J)
   GO TO 20
17 IF(K.NE.NEP) GO TO 18
   YP=X1(I)-X1(I-1)
   GO TO 21
18 B1=FR(2)
   B2=2./(X1(I+1)-X1(I-1))
   SNW=SN2(J)
   TWALL=A(I-1,J,NT)
   GO TO 22
8   IF(I.NE.(I3-1)) GO TO 9
   G2PN= (A(I,J+1,NF)+A(I,J,NF)+A(I-1,J,NF)+A(I-1,J+1,NF))/DV
   G2PS= (A(I,J-1,NF)+A(I,J,NF)+A(I-1,J,NF)+A(I-1,J-1,NF))/DV
   G1PE=0.
   BBE=0.0
   BBN=BBN*FR(3)

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SAR11800
SAR11810
SAR11820
SAR11830
SAR11840
SAR11850
SAR11860
SAR11870
SAR11880
SAR11890
SAR11900
SAR11910
SAR11920
SAR11930
SAR11940
SAR11950
SAR11960
SAR11970
SAR11980
SAR11990
SAR12000
SAR12010
SAR12020
SAR12030
SAR12040
SAR12050
SAR12060
SAR12070
SAR12080
SAR12090
SAR12100
SAR12110
SAR12120
SAR12130
SAR12140
SAR12150

```

BBS=BBS*FR(3)
IF(K.NE.NK) GO TO 25
DX=X1(I+1)-X1(I-1)
UA=ABS(A(I3-1,J,NV2)+A(I3-2,J,NV2))/DX
TAUW=TAUW3(J)
GO TO 20
25 IF(K.NE.NEP) GO TO 26
YP=X1(I+1)-X1(I)
GO TO 21
26 B1=FR(3)
B2=2./(X1(I+1)-X1(I-1))
SNW=SN3(J)
T WALL=A(I+1,J,NT)
GO TO 22
9 IF(J.NE.(J1+1)) GO TO 10
IF(I.GT.I2) GO TO 10
CIPE= (A(I,J+1,NF)+A(I,J,NF)+A(I+1,J,NF)+A(I+1,J+1,NF))/DV
GIPW= (A(I,J+1,NF)+A(I,J,NF)+A(I-1,J,NF)+A(I-1,J+1,NF))/DV
G2PS=0.
BBS=0.
BBE=BBE*FR(4)
BBW=BBW*FR(4)
IF(K.NE.NK) GO TO 27
DX=X2(J1+2)-X2(J1)
UA=ABS(A(I,J1+1,NV1)+A(I,J1+2,NV1))/DX
TAUW=TAUW4(I-I1)
GO TO 20
27 IF(K.NE.NEP) GO TO 28
YP=X2(J1+1)-X2(J1)
GO TO 21
28 B1=FR(4)
B2=2.*R(J-1)/R(J)/(X2(J+1)-X2(J-1))
SNW=SN4(I-I1)
T WALL=A(I,J-1,NT)
GO TO 22
20 SOURCE=UA*TAUW

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SAR12160
SAR1217C
SAR12180
SAR12190
SAR1220C
SAR12210
SAR12220
SAR1223C
SAR12240
SAR12250
SAR1226C
SAR12270
SAR12280
SAR12290
SAR1230C
SAR12310
SAR12320
SAR12330
SAR1234C
SAR12350
SAR1236C
SAR1237C
SAR12380
SAR12390
SAR12400
SAR12410
SAR12420
SAR12430
SAR12440
SAR12450
SAR1246C
SAR12470
SAR12480
SAR12490
SAR12500
SAR12510

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SPRIME=UA*CD*A(I,J,NRC)**2*A(I,J,NK)/TAUW
GO TO 10
21 SOURCE      =(CD**0.75)*(A(I,J,NK)**1.50)/CAPPA/YP
SPRIME=1.
AE=0.
AW=0.
AN=0.
AS=0.
BBE=0.
BBW=0.
BBN=0.
BBS=0.
GO TO 100
22 SOURCE=SOURCE*B1+B2*SNW*TWALL
SPRIME=SNW*B2
10 CONTINUE
C*** COMPUTE AE,AW,AN,AS
APP=1.
IF(K.EQ.NW) APP=R(J)*R(J)
IF(K.EQ.NT) APP=A(I,J,NSP)
AW=0.5*APP*(ABS(G1PW)+G1PW)
AE=0.5*APP*(ABS(G1PE)-G1PE)
AN=0.5*APP*(ABS(G2PN)-G2PN)
AS=0.5*APP*(ABS(G2PS)+G2PS)
100 CONTINUE
RETURN
END
SAR12520
SAR12530
SAR12540
SAR12550
SAR12560
SAR12570
SAR12580
SAR12590
SAR12600
SAR12610
SAR12620
SAR12630
SAR12640
SAR12650
SAR12660
SAR12670
SAR12680
SAR12690
SAR12700
SAR12710
SAR12720
SAR12730
SAR12740
SAR12750
SAR12760
SAR12770
SAR12780

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SUBROUTINE PRINT(NBEGIN,NTOTAL,LP)
COMMON/CNAME/ANAME(6,12),ASYMBL(10),BNAME(6,10)
COMMON/CDVAR/A(71,15,12)
COMMON/CFLD/B(71,15,10),LF,CU
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CAVT/TR
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRC,NTC,NSP,NMT
COMMON/CAK/AKEFF
COMMON/CLS/YL(15),YS(15)
COMMON/CTRVL/VE,VC
JX=JN/10
IF(JX.LT.1) JX=1
IX=IN/10
IF(IX.LT.1) IX=1
DO 10 K=NBEGIN,NTOTAL
IF(LP.EQ.2) GO TO 11
WRITE(6,100) (ANAME(L,K),L=1,6)
GO TO 12
11 WRITE(6,100) (BNAME(L,K),L=1,6)
12 CONTINUE
DO 2 L=1,JN,JX
J=JN+1-L
IS=26
IF(LP.EQ.2) GO TO 15
WRITE(6,103) (A(I,J,K),I=11,IS,1),J
GO TO 16
15 WRITE(6,103) (B(I,J,K),I=11,IS,1),J
16 CONTINUE
2 CONTINUE
IF(LP.EQ.1) GO TO 18
WRITE(6,104) (I,I=11,IS,1)
GO TO 10
18 WRITE(6,104) (I,I=11,IS,1)
10 CONTINUE
IF(LP.EQ.2) GO TO 20
WRITE(6,201)

```

SAR12790
SAR12800
SAR1281C
SAR12820
SAR12830
SAR1284C
SAR12850
SAR12860
SAR1287C
SAR12880
SAR12890
SAR12900
SAR1291C
SAR1292C
SAR12930
SAR12940
SAR1295C
SAR12960
SAR12970
SAR12980
SAR12990
SAR13000
SAR1301C
SAR1302C
SAR13030
SAR13040
SAR1305C
SAR13060
SAR13070
SAR13080
SAR13090
SAR13100
SAR1311C
SAR13120
SAR13130
SAR13140

```

DO 202 J=1,JI
202 WRITE(6,203) J,(A(I,J,NT),I=1,I1)
   WRITE(6,204)
   I31=IS+1
DO 205 J=1,JN
205 WRITE(6,203) J,(A(I,J,NT),I=I31,IN,1)
   WRITE(6,207) YL(J),YS(J)
20 WRITE(6,212) VE,TB,AKEFF
20 CONTINUE
   RETURN
100 FORMAT(1H130X,21HTHE DISTRIBUTION OF ,6A6/
126X,51H-----/
21H0110X,1HJ//)
103 FORMAT(1H0,3X,11(1PE10.3),3X,I2,/)
104 FORMAT(1H0//3H I,4X,10(12,8X),I2/4H ---)
201 FORMAT(/,32H TEMP. DISTRIBUTION IN ELECTRODE)
204 FORMAT(/,32H TEMP. DISTRIBUTION IN METAL)
203 FORMAT(/,10H J      =,I2,/,10(3X,F8.1))
207 FORMAT(/,4H YL=,F10.4,4H YS=,F10.4)
212 FORMAT(/,4H VE=,E12.4,4H TB=,F12.2,7H AKEFF=,E12.3)
   END
SAR13150
SAR13160
SAR1317C
SAR13180
SAR13190
SAR13200
SAR13210
SAR13220
SAR13230
SAR13240
SAR13250
SAR13260
SAR1327C
SAR13280
SAR13290
SAR13300
SAR13310
SAR13320
SAR13330
SAR13340
SAR13350

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SUBROUTINE SOURCE(SOURCE,I,J,K)
COMMON/CFLD/8(71,15,10),LF,CU
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCONT/C1,C2,C3,CD
COMMON/CTURB/GK(71,15)
COMMON/CTRLV/VE,VC
COMMON/CHJ/NHR,NHI,NH,NJRR,NJRI,NJR,NJZR,NJZI,NJZ,NJJ
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CEMP/WF,P,S(4)
COMMON/CDROP/TAU,HCD,D,QS,QM
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SB,HL
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CLS/YL(15),YS(15)
COMMON/CTEMP/TLM,TSM,ILS,IA,IM,TW
GO TO (1,2,3,4,5,6,6,6,6),K
SOURCE=0.0
RETURN
C *** FOR VORTICITY/R
1 SOURCE=B(I,J,NHR)*B(I,J,NJRR)+B(I,J,NHI)*B(I,J,NJRI)
SOURCE=(1.0E+06)*P*SOURCE
B(I,J,NJZR)=SOURCE
BT=BETA(1)
IF(I.GE.13) BT=BETA(2)
B1=ADF(I,J,2,NT)
B2=R(J)*A(I,J,NRO)*BT*.81*B1
B(I,J,NJZI)=B2
SOURCE=SOURCE+B2
RETURN
C*** FOR STREAM FUNCTION
2 SOURCE=A(I,J,NW)
RETURN
C*** FOR TURBULENCE ENERGY
3 CONTINUE
B1=ADF(I,J,1,NV1)
B2=ADF(I,J,2,NV2)

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SAR13360
SAR13370
SAR13380
SAR1339C
SAR13400
SAR13410
SAR13420
SAR1343C
SAR13440
SAR13450
SAR13460
SAR13470
SAR13480
SAR13490
SAR13500
SAR13510
SAR13520
SAR13530
SAR13540
SAR13550
SAR13560
SAR13570
SAR13580
SAR13590
SAR13600
SAR13610
SAR1362C
SAR13630
SAR13640
SAR13650
SAR13660
SAR13670
SAR13680
SAR13690
SAR13700
SAR13710

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B3=ADF(I,J,2,NV1)
B4=ADF(I,J,1,NV2)
B5=A(I,J,NV2)/R(J)
GK(I,J)=A(I,J,NMT) *(2.0*(B1**2+B2**2+B5**2)+(83+B4)**2)
DK=A(I,J,NRO)*A(I,J,NEP)
SOURCE=GK(I,J)-DK
RETURN
TURB.ENERGY DISSIPATION
C*** 4 CONTINUE
IF(A(I,J,NK).EQ.0.0) GO TO 100
TERM1=0.0
TERM2=C1*GK(I,J)*A(I,J,NEP)/A(I,J,NK)
TERM3=C2*A(I,J,NRO)*(A(I,J,NEP)**2)/A(I,J,NK)
SOURCE=TERM1+TERM2-TERM3
RETURN
100 SOURCE=0.0
RETURN
C *** SOURCE FOR TEMPERATURE
5 CONTINUE
IF(J.GT.J1) GO TO 8
Z=X1(I3)-X1(I2)
SOURCE=B(I,J,NJJ)-QS/(3.14*R(J1)*R(J1)*Z)
GO TO 9
8 SOURCE=B(I,J,NJJ)
9 CONTINUE
RETURN
END
SAR13720
SAR13730
SAR13740
SAR13750
SAR13760
SAR13770
SAR13780
SAR13790
SAR13800
SAR13810
SAR13820
SAR13830
SAR13840
SAR13850
SAR13860
SAR13870
SAR13880
SAR13890
SAR13900
SAR13910
SAR13920
SAR13930
SAR13940
SAR13950
SAR13960
SAR13970
SAR13980

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```

SUBROUTINE VELDIS
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
DO 50 J=2,JNM
  IL=I1+1
  IF(J.LE.J1) IL=I2+1
  IH=I3-1
DO 51 I=IL,IH
  A(I,J,NV1)=ADF(I,J,2,NF)/R(J)/A(I,J,NRO)
  A(I,J,NV2)=-ADF(I,J,1,NF)/R(J)/A(I,J,NRO)
51 CONTINUE
50 CONTINUE
  IL=I1+1
  IH=I3-1
DO 54 I=IL,IH
  A(I,1,NV1)=2.0*A(I,2,NF)/(R(2)*R(2))/A(I,1,NRO)
54 CONTINUE
  J12=J1+1
DO 40 J=J12,JNM
  A(I1,J,NV2)=-ADF(I1,J,1,NF)/R(J)/A(I1,J,NRO)
40 CONTINUE
RETURN
END
SAR1399C
SAR14000
SAR14010
SAR1402C
SAR14030
SAR14040
SAR1405C
SAR14060
SAR14070
SAR14080
SAR1409C
SAR14100
SAR14110
SAR1412C
SAR14130
SAR14140
SAR14150
SAR14160
SAR14170
SAR14180
SAR14190
SAR14200
SAR14210
SAR14220
SAR14230
SAR14240

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SUBROUTINE VISCOS
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,J1
COMMON/CRLAX/RP(10),RSDU(10),SAN(10)
COMMON/CCONT/C1,C2,C3,CD
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CCORD/IMIN(15),IMAX(15),XI(71),X2(15),R(15)
C*** CALCULATE TURBULENT VISCOSITY
I31=I3-1
DO 10 J=1,JNM
DO 11 I=1,I31
IF(J.LE.J1.AND.I.LE.I2) GO TO 12
IF(A(I,J,NEP).LE.0.0.(R.A(I,J,NK).LE.0.0) GO TO 20
A(I,J,NMT) =A(I,J,NRO)*CD*(A(I,J,NK)**2)/A(I,J,NEP)
GO TO 21
20 CONTINUE
A(I,J,NMT)=0.
21 CONTINUE
Z=A(I,J,NMU)
EMU=ZMUREF(1)
A(I,J,NMU)=EMU +A(I,J,NMT)
A(I,J,NMU)=Z+RP(NMU)*(A(I,J,NMU)-Z)
12 CONTINUE
11 CONTINUE
10 CONTINUE
RETURN
END
SAR14250
SAR14260
SAR14270
SAR14280
SAR14290
SAR14300
SAR14310
SAR14320
SAR14330
SAR14340
SAR14350
SAR14360
SAR14370
SAR14380
SAR14390
SAR14400
SAR14410
SAR14420
SAR14430
SAR14440
SAR14450
SAR14460
SAR14470
SAR14480
SAR14490
SAR14500
SAR14510
SAR14520

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SUBROUTINE PROP(L)
COMMON/CDVAR/A(71,15,12)
COMMON/CNUMB/NW,NF,NK,NEP,NV1,NV2,NT,NMU,NRO,NTC,NSP,NMT
COMMON/CPROP/ROREF(5),ZMUREF(2),PR(10),GAMA
COMMON/CLS/YL(15),YS(15)
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CTHERM/TCREF(5),SPREF(5),BETA(2),ES,EE,EM,SD,HL
COMMON/CAK/AKEFF
COMMON/CTEMP/TLM,TSM,TLS,TA,TM,TW
COMMON/CTRVL/VE,VC
COMMON/CDROP/TAU,HCD,D,QS,QM
COMMON/CSNW/SN1(20),SN2(15),SN3(21),SN4(10)
COMMON/CAVM/AVM(20)
COMMON/CFLD/B(71,15,10),LF,CU
COMMON/CHJ/NHR,NHI,NH,NJRR,NJRI,NJR,NJZR,NJZI,NJZ,NJJ
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
IF(L.EQ.2) GO TO 1
DO 2 I=1,I3
DO 2 J=1,JN
IF(I.LE.I2.AND.J.LE.J1) GO TO 3
A(I,J,NRO)=ROREF(2)
A(I,J,NMU)=ZMUREF(1)
A(I,J,NTC)=TCREF(2)
A(I,J,NSP)=SPREF(2)
GO TO 2
3 A(I,J,NRO)=ROREF(1)
A(I,J,NTC)=TCREF(1)
A(I,J,NSP)=SPREF(1)
A(I,J,NMU)=ZMUREF(1)
2 CONTINUE
AKEFF=TCREF(3)
1 CONTINUE
IF(L.EQ.1) GO TO 5
C *** REPOSITION THE ISOTHERMS
LIO=0
DO 10 J=1,JN

```

SAR14530
SAR1454C
SAR14550
SAR14560
SAR1457C
SAR14580
SAR14590
SAR1460C
SAR14610
SAR14620
SAR14630
SAR14640
SAR14650
SAR14660
SAR14670
SAR14680
SAR1469C
SAR14700
SAR14710
SAR14720
SAR14730
SAR1474C
SAR14750
SAR1476C
SAR14770
SAR14780
SAR1479C
SAR14800
SAR14810
SAR1482C
SAR1483C
SAR14840
SAR14850
SAR1486C
SAR14870
SAR14880

```

DO 11 I=I3,IN
IF(LIQ.EQ.1) GO TO 14
TL=A(I,J,NT)-TLM
TLA=ABS(TL)/TLM
IF(TLA.GT.0.0002) GO TO 12
YL(J)=X1(I)-X1(I3)
LIQ=1
GO TO 11
12 IF(TL.GT.0.) GO TO 11
DXT=(X1(I)-X1(I-1))/(A(I,J,NT)-A(I-1,J,NT))
YL(J)=X1(I-1)+DXT*(TLM-A(I-1,J,NT))-X1(I3)
LIQ=1
14 TS=A(I,J,NT)-TSM
TSA=ARS(TS)/TSM
IF(TSA.GT.0.0002) GO TO 15
YS(J)=X1(I)-X1(I3)
LIQ=0
GO TO 10
15 IF(TS.GT.0.) GO TO 16
DXT=(X1(I)-X1(I-1))/(A(I,J,NT)-A(I-1,J,NT))
YS(J)=X1(I-1)+DXT*(TSM-A(I-1,J,NT))-X1(I3)
LIQ=0
GO TO 10
16 LIQ=1
11 CONTINUE
10 CONTINUE
C RECALCULATE VE, VC
DR=R(2)-R(1)
DXF=X1(I2+1)-X1(I2)
DXH=X1(I2)-X1(I2-1)
A1=TCREF(1)/DXR*0.5
A3= 1./ (R(J1)*R(J1)*RREF(1)*HL)
XF=X1(I2+1)-X1(I2)
AVM(1)=0.
DO 60 J=2,J1
A4=A1*(4.*A(I2-1,J,NT)-3.*A(I2,J,NT)-A(I2-2,J,NT))

```

SAR14890
SAR14900
SAR14910
SAR14920
SAR14930
SAR14940
SAR14950
SAR14960
SAR14970
SAR14980
SAR14990
SAR15000
SAR15010
SAR15020
SAR15030
SAR15040
SAR15050
SAR15060
SAR15070
SAR15080
SAR15090
SAR15100
SAR15110
SAR15120
SAR15130
SAR15140
SAR15150
SAR15160
SAR15170
SAR15180
SAR15190
SAR15200
SAR15210
SAR15220
SAR15230
SAR15240

```

I+SN2(J)*(A(I2+1,J,NT))-A(I2,J,NT))
60  AVM(J)=R(J)*A4
    SUMV=0.
    J11=J1-1
    DO 61 J=1,J11
    DX2=X2(J+1)-X2(J)
61  SUMV=SUMV+(AVM(J)+AVM(J+1))*DX2
    Z=VE
    VE=A3*SUMV
    VC=VE*R(J1)*R(J1)/(R(JN)*R(JN))
    VC=VC*ROREF(1)/ROREF(5)
    HCD=HCD*VE/Z
C *** FIRST CALCULATE THE AVERAGE KEFF IN THE SLAG
    SUMI=0.
    DO 62 I=I1,I3
    N=I-I1+1
    JL=J1
    IF(I.GE.I2) JL=1
    SUMJ=0.
    DO 64 J=JL,JNM
    DX2=0.5*(X2(J+1)-X2(J))
64  SUMJ=SUMJ+(A(I,J,NMT)*R(J)+A(I,J+1,NMT)*R(J+1))*DX2
    RAV=(R(JN)+R(JL))*0.5
62  AVM(N)=SUMJ/(X2(JN)-X2(JL))/RAV
    N3=I3-I1
    DO 66 N=1,N3
    I=N+I1-1
    DZ=(X1(I+1)-X1(I))*0.5
66  SUMI=SUMI+(AVM(N)+AVM(N+1))*DZ
    AVMU=SUMI/(X1(I3)-X1(I1))
    AKEFF=AVMU*SPREF(2)/TCREF(2)+1.
    AKEFF=AKEFF*TCREF(3)*0.3333
    IF(AKEFF.LT.TCREF(3)) AKEFF=TCREF(3)
5  CONTINUE
    DO 4 J=1,JN
4  A(I3,J,NTC)=AKEFF

```

C *** ASSIGN THE PROPERTIES TO PROPER DOM AINS

```
I J1=I3+1
DO 54 J=1, JN
DO 54 I=I31, IN
XSM=X1(I)-X1(I3)
IF(XSM.GT.YL(J)) GO TO 55
A(I,J,NRO)=RORREF(3)
A(I,J,NTC)=AKEFF
A(I,J,NSP)=SPREF(3)
GO TO 54
55 IF(XSM.GT.YS(J)) GO TO 56
A(I,J,NRO)=RORREF(4)
A(I,J,NTC)=TCREF(4)
A(I,J,NSP)=SPREF(4)
GO TO 54
56 A(I,J,NRO)=RORREF(5)
A(I,J,NTC)=TCREF(5)
A(I,J,NSP)=SPREF(5)
54 CONTINUE
RETURN
END
```

SAR15610
SAR15620
SAR15630
SAR15640
SAR15650
SAR15660
SAR15670
SAR15680
SAR15690
SAR15700
SAR15710
SAR15720
SAR15730
SAR15740
SAR15750
SAR15760
SAR15770
SAR15780
SAR15790
SAR15800
SAR15810

```

FUNCTION ADF(I,J,LX,K)
COMMON/CDVAR/A(71,15,12)
COMMON/CCORD/IMIN(15),IMAX(15),X1(71),X2(15),R(15)
COMMON/CGRID/IN,INM,JN,JNM,I1,I2,I3,I4,I5,IA,JI
C FUNCTION FOR EVALUATION OF FIRST DERIVATIVES
M=1
PP=1.
IF(J.EQ.1) M=2
IF(J.EQ.JN) M=4
IF(I.EQ.I1) M=3
IF(I.EQ.IN) M=5
GO TO (1,2,3,4,5),M
C*** M=1, FOR POINTS NOT ON ANY OF THE BOUNDARIES
1 IF(LX.EQ.2) GO TO 11
PN=1.
BENQ=A(I+1,J,K)
BWSR=A(I-1,J,K)
BP=A(I,J,K)
XENQ=X1(I+1)-X1(I)
XWSR=X1(I)-X1(I-1)
GO TO 100
11 PN=1.
BENQ=A(I,J+1,K)
BWSR=A(I,J-1,K)
BP=A(I,J,K)
XENQ=X2(J+1)-X2(J)
XWSR=X2(J)-X2(J-1)
GO TO 100
C *** FOR POINTS ON THE SYMMETRY AXIS
2 IF(LX.EQ.1) GO TO 1
PN=-1.
BENQ=A(I,J+1,K)
BWSR=A(I,J+2,K)
BP=A(I,J,K)
XENQ=X2(J+1)-X2(J)
XWSR=X2(J+2)-X2(J)

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```

SAR1582C
SAR15830
SAR1584C
SAR1585C
SAR15860
SAR1587C
SAR15880
SAR15890
SAR15900
SAR15910
SAR1592C
SAR15930
SAR15940
SAR15950
SAR15960
SAR15970
SAR1598C
SAR1599C
SAR16000
SAR1601C
SAR16020
SAR16030
SAR16040
SAR1605C
SAR1606C
SAR16070
SAR1608C
SAR16090
SAR16100
SAR16110
SAR1612C
SAR16130
SAR16140
SAR1615C
SAR16160
SAR16170

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```

GO TO 100
C*** M=3, FOR POINTS ON THE BOUNDARY I=11
3 IF(LX.EQ.2) GO TO 11
PN=-1.
BENQ=A(I+1,J,K)
BWSR=A(I+2,J,K)
BP=A(I,J,K)
XENQ=X1(I+1)-X1(I)
XWSR=X1(I+2)-X1(I)
GO TO 100
C*** M=4, FOR POINTS ON THE BOUNDARY J=JN
4 IF(LX.EQ.1) GO TO 1
PN=-1.
PP=-1.
BENQ=A(I,J-1,K)
BWSR=A(I,J-2,K)
BP=A(I,J,K)
XENQ=X2(J)-X2(J-1)
XWSR=X2(J)-X2(J-2)
GO TO 100
C*** M=5, FOR POINTS ON THE BOUNDARY I=IN
5 IF(LX.EQ.2) GO TO 11
PN=-1.
PP=-1.
BENQ=A(I-1,J,K)
BWSR=A(I-2,J,K)
BP=A(I,J,K)
XENQ=X1(I)-X1(I-1)
XWSR=X1(I)-X1(I-2)
100 CONTINUE
ADF=((XENQ*XENQ-XWSR*XWSR)*BP+
1XWSR*XWSR*BENQ-XENQ*XENQ*BWSR)/(XENQ*XWSR*(PN*XENQ+XWSR))*PP
RETURN
END

```

```

SAR16180
SAR16190
SAR16200
SAR1621C
SAR1622C
SAR16230
SAR16240
SAR1625C
SAR16260
SAR16270
SAR1628C
SAR16290
SAR16300
SAR16310
SAR16320
SAR16330
SAR16340
SAR1635C
SAR16360
SAR16370
SAR16380
SAR16390
SAR16400
SAR16410
SAR16420
SAR16430
SAR16440
SAR16450
SAR16460
SAR16470
SAR16480
SAR16490
SAR16500
SAR16510

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VORTICITY
STREAM FUNCTION
TURBULENCE ENERGY
TURBULENCE DISSIPATION
TEMPERATURE
DIR.-1 VELOCITY
DIR.-2 VELOCITY
EFFECTIVE VISCOSITY
DENSITY
THERMAL CONDUCTIVITY
SPECIFIC HEAT
TURBULENT VISCOSITY
RSVDRTRSSTRMRSTENGRSDISRSTEMPSANVOR
SANSTMSANTKESANDSPSANTMP
RE MAGNETIC FLUX INTENSITY
IM MAGNETIC FLUX INTENSITY
RE CURRENT IN DIR.-R
IM CURRENT IN DIR.-R
JOULE HEAT
MAGNETIC FLUX INTENSITY
CURRENT IN DIR.-R
CURRENT IN DIR.-Z
RE CURRENT IN DIR.-Z
IM CURRENT IN DIR.-Z

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BIOGRAPHICAL NOTE

The author was born in Bihar, India on June 26, 1952. After finishing high school in Calcutta he attended Indian Institute of Technology, Kharagpur, from 1969 to 1974 and obtained the degree of Bachelor of Technology (Honours) in Chemical Engineering. During both high school and undergraduate years he received numerous awards for achievements in academics and extra-curricular activities. On completion of his undergraduate studies in 1974, Department of Chemical Engineering awarded him Professor S.K. Nandi Gold Medal for being the "best all rounder" Chemical Engineering student in the class of 1974, the Institute Silver Medal for securing first rank in B. Tech. examinations and an award for the Best Undergraduate Thesis.

In June 1974, the author married Saraswati Jha. In September 1974, he joined State University of New York at Buffalo and obtained the degree of Master of Science in Chemical Engineering in June 1976. His thesis work was on the effect of flow maldistribution on the performance of catalytic packed bed reactors. He joined the Department of Materials Science and Engineering at MIT in September 1976. In 1978, the department awarded him Falih N. Darmara Materials Achievement Award "in recognition of outstanding academic performance, excellent research work and extra curricular activities". The same year he received the

Annual Student Paper Award of the Eastern Iron and Steel Section of AIME for a paper "Optimization of Burden Size for a Blast Furnace".

As a research associate (Summers of 1976, 1977, 1978) at both SUNY at Buffalo and at MIT, the author has worked on a number of projects, both experimental and theoretical. He has worked on a broad range of problems as parts of various consulting assignments. Some of the assignments have involved heat transfer and fluid flow calculations in an electric furnace smelter, heat transfer calculations for recuperators using impinging jets, material and energy balance analysis for coal gasification and direct reduction processes, etc. He has also published papers in the areas of chemical reaction engineering, gas-solid reaction, and modelling of electroslag refining process.

The author is a student member of AIME and ASM. He is also a member of Sigma Xi.