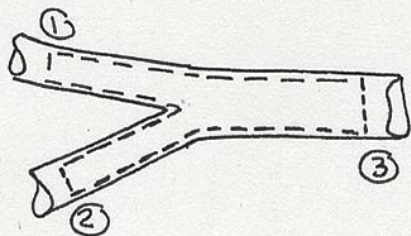


ANSWER 1.8

CHOOSE A CONTROL VOLUME (DASH) FAR ENOUGH AWAY FROM JUNCTURE SUCH THAT $\partial T / \partial n = 0$ AT EACH FLUX SURFACE.



$$(A) \frac{d}{dt} \int_{cv} C dV = - \int_{cs} C \vec{V} \cdot \vec{n} dA + \int_{cs} D_n \frac{\partial C}{\partial n} dA \pm S$$

THE CONCENTRATION OF HEAT ENERGY IS,

$$C [J m^{-3}] = \rho C_p T$$

FLUID DENSITY $[kg m^{-3}]$ SPECIFIC HEAT $[J kg^{-1} K^{-1}]$ TEMP $[^{\circ}K]$

$$C_p = 4200 J kg^{-1} K^{-1}$$

FOR WATER

FOR SIMPLICITY, ASSUME $\rho, c_p \neq f(T)$.

IF WE ASSUME STEADY STATE, THE FIRST TERM IN (A) IS ZERO,

BECAUSE WE POSITION SURFACES 1, 2, 3 WHERE $\frac{dT}{dn} = 0$,
THE DIFFUSIVE FLUX TERM IS ZERO.

BECAUSE THE PIPES ARE INSULATED, $S = 0$.

SO, FINALLY (A) BECOMES,

$$(B) \quad 0 = \rho c_p T_1 u_1 A_1 + \rho c_p T_2 u_2 A_2 - \rho c_p T_3 u_3 A_3$$

DROPPING ρc_p , AND SOLVING FOR T_3 ,

$$(C) \quad T_3 = \frac{u_1 A_1 T_1 + u_2 A_2 T_2}{u_3 A_3}$$

NOTE FROM STATEMENT $u_1 A_1 = u_2 A_2$

AND FROM FLUID MASS CONSERVATION $(u_1 A_1 + u_2 A_2) = u_3 A_3$

$$(D) \quad T_3 = \frac{u_1 A_1 (T_1 + T_2)}{2 u_1 A_1} = \frac{1}{2} (T_1 + T_2)$$

$$\therefore T_3 = 15^\circ\text{C} \quad [288^\circ\text{K}]$$