

Tuesday, October 18<sup>th</sup>, 2005, 9:30 – 11:00 a.m.

OPEN BOOK

QUIZ #1 SOLUTIONS

1.5 HOURS

**Problem 1 (45%) – Two-unit nuclear plant with single containment building**

- i) The containment building is the control volume of choice.

The energy equation is:

$$\frac{\partial E}{\partial t} = \dot{m}_{ws} h_{ws} \quad \Rightarrow \quad E_2 - E_1 = h_{ws} \int_{t_1}^{t_2} \dot{m}_{ws} dt = h_{ws} 0.2M_{ws} \quad (1)$$

where E is the total energy of the control volume, and  $0.2M_{ws}$  is the mass of water flown into the containment building. Expanding the energy terms on the left-hand side of Eq. (1), one gets:

$$(0.2M_{ws} + M_{wsp})u_{w2}(T_2, P_{w2}) + M_a u_{a2} - M_{wsp} u_{wsp} - M_a u_{a1} = h_{ws} 0.2M_{ws} \quad (2)$$

where superheated steam conditions were assumed in the containment at  $t_2$ . Equation (2) can be re-written as follows:

$$(0.2M_{ws} + M_{wsp})u_{w2}(T_2, P_{w2}) + M_a c_{va}(T_2 - T_1) = M_{wsp} u_{wsp} + h_{ws} 0.2M_{ws} \quad (3)$$

The equation to calculate the mass of air in the containment building (with zero initial humidity) is:

$$M_a = \frac{P_1 V_{a1}}{R_a T_1} \quad (4)$$

The total control volume is:

$$V_c = V_{a1} + \frac{M_{wsp}}{\rho_{wsp}} \quad (5)$$

The equation for the water volume at  $t_2$  is:

$$V_c = (0.2M_{ws} + M_{wsp})v_{w2}(T_2, P_{w2}) \quad (6)$$

Finally, the equation to calculate the containment pressure at  $t_2$  is:

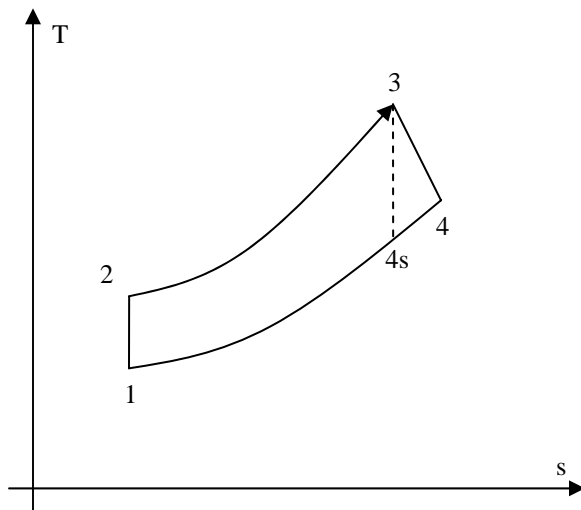
$$P_2 = P_{w2} + P_{a2} = P_{w2} + \frac{M_a R_a T_2}{V_c} \quad (7)$$

Equations (3) through (7) constitute a system of 5 equations in the 5 unknowns  $T_2$ ,  $P_{w2}$ ,  $M_a$ ,  $V_c$  and  $P_2$ .

- ii) Advantages of the single-containment approach include lower capital cost and greater ease of access and inspection. The disadvantages include reduced redundancy (failure of the containment building would result in a leak path for two reactors instead of one), and possibly larger plant footprint (depending on the building design).

### Problem 2 (55%) –Power cycle for a High Temperature Gas-Cooled Reactor

i)



ii) The net electric power of the plant,  $\dot{W}_{net}$ , is:

$$\begin{aligned} \dot{W}_{net} &= \dot{W}_T - \dot{W}_C = \dot{m} c_p [(T_3 - T_4) - (T_2 - T_1)] = \dot{m} c_p [\eta_T (T_3 - T_{4s}) - (T_2 - T_1)] = \\ &= \dot{m} c_p \left[ \eta_T T_3 \left( 1 - \frac{T_{4s}}{T_3} \right) - T_1 \left( \frac{T_2}{T_1} - 1 \right) \right] \end{aligned} \quad (8)$$

where  $\dot{m}$ ,  $c_p$ ,  $\eta_T$  and  $T_1$  are all given in the problem statement. The ratios  $T_{4s}/T_3$  and  $T_2/T_1$  can be readily calculated from the equation of the isentropic transformation for a perfect gas:

$$\frac{T_3}{T_{4s}} = \frac{T_2}{T_1} = \left( \frac{P_2}{P_1} \right)^{\frac{\gamma-1}{\gamma}} \approx 1.904 \quad (9)$$

Then  $T_2 = 1.904 \cdot T_1 \approx 710.2$  K.

$T_3$  can be calculated from the energy equation for the reactor:

$$\dot{Q}_0 = \dot{m}c_p(T_3 - T_2) \Rightarrow T_3 = T_2 + \frac{\dot{Q}_0}{\dot{m}c_p} \approx 1,017.9 \text{ K} \quad (10)$$

Substituting the numerical values into Eq. (8), one gets  $\dot{W}_{net} \approx 1,017 \text{ MW}$ .

iii) The energy equation for the fuel is:

$$\frac{\partial E}{\partial t} = \dot{Q} \Rightarrow E_2 - E_1 = \int_{t_1}^{t_2} \dot{Q} dt = \int_{60 \text{ min}}^{65 \text{ min}} 0.066 \dot{Q}_0 t^{-0.2} dt = 1.22 \times 10^{10} \text{ J} \quad (11)$$

where  $\dot{Q}$  is the decay power. The energy variation on the left-hand term of Eq. (11) can be rewritten in terms of the temperature rise,  $\Delta T_F$ , as follows:

$$E_2 - E_1 = M_F c_F \Delta T_F \quad (12)$$

where  $M_F$  is the fuel mass ( $4.405 \times 11,000 = 44,495 \text{ kg}$ ) and  $c_F$  is the fuel specific heat. Therefore the temperature rise is:

$$\Delta T_F = 1.22 \times 10^{10} / (44,495 \times 230) \approx 1,200 \text{ K} \quad (13)$$