

# Coupled cycling of metals with nitrogen and carbon in marine sediments

by

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## Abstract

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Jennifer S. Karolewski

Submitted to the MIT-WHOI Joint Program in Oceanography and Applied Ocean Science and Engineering on May 3<sup>rd</sup> 2024, in Partial Fulfilment of the Requirements for the Degree of Doctor of Philosophy

Cross element processes are complex and often understudied components within biogeochemical cycles. In this thesis, I use stable isotopes of carbon, nitrogen, and oxygen as the primary tools to interrogate these complex reactions. First, I report abiotic oxidation of nitrite to nitrate by manganese(III)-pyrophosphate. This reaction can occur even in the absence of oxygen, unlike biological nitrite oxidation. Reaction rates were measured at a range of environmentally relevant pH values (5-8) with the reaction proceeding more quickly at lower pH. Reaction order was second order with respect to manganese(III) and first order with respect to nitrous acid. No reversibility of reaction was observed upon addition of isotopically distinct nitrate. An inverse kinetic isotope effect of  $+19.9 \pm 0.7\%$  was calculated, which was comparable in magnitude and direction to that of biological nitrite oxidation. In natural waters, such as estuaries, this reaction could potentially play an important role in the nitrogen cycle. Next, I report an abiotic reaction between hydroxylamine and manganese(III)-pyrophosphate which forms nitrous oxide, nitrite, and likely dinitrogen gas. In artificial seawater (pH = 8), this reaction proceeds rapidly, with the ratio of products highly dependent on the reactant ratio. Nitrous oxide site preference (SP) of  $+35.5 \pm 0.6\%$  was observed, consistent with the isotopic signatures of several marine nitrifying organisms. This suggests that “leakage” of intermediate hydroxylamine from nitrifier cells could potentially react with manganese(III) in a mixed biotic-abiotic process without previously being noticed. Finally, I performed experiments using carbon-13 labelling to measure rates of anaerobic oxidation of methane (AOM) in cold seep sediments collected at Cascadia Margin. Four forms of oxidized manganese and four forms of oxidized iron were added to treatments in order to evaluate how these altered rates of AOM. In contrast to previous work, addition of metals did not overall increase rates of AOM above those of an unamended control and some treatments in fact reduced it. However, energy yields from microbes using metal as an electron acceptor are higher per mole of methane reduced than that of using sulfate so even with these lower rates, energy yields would have exceeded those of controls. Additionally, doubling times for the archaea performing AOM are long enough that the microbial community may not have been able to adapt on the timescale of the experiment. Overall, the results of this thesis illuminate the need for further study of abiotic and coupled cycling reactions when considering biogeochemical cycles.

Thesis Supervisor: Dr. Scott D. Wankel

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## 1. Introduction

Biogeochemistry involves the study of biological, geological, chemical, and physical processes and reactions that govern the distribution and cycling of elements in the environment. Among biogeochemists, it is common to discuss cycling in the context of a single element, such as the carbon or nitrogen cycle. Chapters 2 and 3 focus on the nitrogen cycle which I will briefly review here. Nitrogen is an essential element for life and often acts as a limiting nutrient within the ocean (Moore et al. 2013). Human impacts on the nitrogen cycle are substantial; the amount of artificially fixed nitrogen produced for fertilizers and other industrial applications is equivalent or greater than the amount fixed biologically per year (Galloway et al. 2004). Within the marine environment, nitrogen cycling reactions can be divided into those that occur in oxic and anoxic regions of the ocean (Figure 1). In surface waters, dinitrogen gas is fixed into ammonium or organic matter ( $\text{N}_2 \rightarrow \text{NH}_4^+$ ) primarily by photoautotrophs such as *Trichodesmium* (Tang et al. 2019). Also occurring in oxic regions is nitrification ( $\text{NH}_4^+ \rightarrow \text{NO}_2^- \rightarrow \text{NO}_3^-$ ) which will be discussed further below. In anoxic regions, denitrification ( $\text{NO}_3^- \rightarrow \text{NO}_2^- \rightarrow \text{NO} \rightarrow \text{N}_2\text{O} \rightarrow \text{N}_2$ ) is performed primarily by heterotrophs which use fixed nitrogen as an electron acceptor (Devol 2015). Dissimilatory reduction of nitrate to ammonium (DNRA;  $\text{NO}_3^- \rightarrow \text{NO}_2^- \rightarrow \text{NH}_4^+$ ) is performed by a similar nutritional class of microbes (chemoorganoheterotrophs) but does not result in the loss of fixed nitrogen from the system (Gruber 2008). Finally, anammox ( $\text{NH}_4^+ + \text{NO}_2^- \rightarrow \text{N}_2$ ) is performed by chemoautotrophs as an energy source and also results in the loss of fixed nitrogen (Kuenen 2008). Chapter 4 focuses on a specific portion of the carbon cycle, namely that of methane. Methane is the most abundant organic molecule on Earth and acts as a supply of energy to both humans and microbes (Whiticar 2020). Additionally, methane is a potent greenhouse gas that is the second most impactful to the climate after  $\text{CO}_2$  (Whiticar 2020). Methane is biologically produced in aquatic systems through methanogenesis which primarily occurs through the hydrogenotrophic pathway (from hydrogen and carbon dioxide) or the acetoclastic pathway (from breaking down acetate) (Whiticar 2020). Once formed methane can then be consumed through aerobic methanotrophy or anaerobic oxidation of methane (AOM) which will be discussed further below (Guerrero-Cruz et al. 2021). Aerobic methanotrophy is performed by bacteria which use methane as their sole source of carbon and energy and tend to accumulate the surface of sediments (Fenibo et al. 2023)

While it may be easier to limit biogeochemical studies to primarily one element, nature does not restrict itself in the same way and thus this approach omits important cross-element reactions. Coupled cycling can take many forms in the environment. Microbes can use redox-active species in order to gain energy (dissimilatory) and/or acquire biomass (assimilatory) (Kappler et al. 2021). Dissimilatory pathways can also be divided in anaerobic respiration, wherein oxidized forms of nitrogen, metals, sulfur, etc. are used as electron acceptors to break down organic matter, and chemolithotrophy, wherein inorganic redox reactions are used to directly harvest energy (Burgin et al. 2011). Chapter 4 of this thesis focuses on one such biological coupled cycling process: anaerobic oxidation of methane (AOM) which transforms methane ( $\text{CH}_4$ ) to carbon dioxide ( $\text{CO}_2$ ). This reaction serves as a pathway for microbes to acquire energy and also as a source of carbon. Generally, this process is thought to be most commonly tied to sulfate reduction (sulfate-AOM) performed by consortia of anaerobic methanotrophic archaea (ANME) and sulfate-reducing bacteria (SRB); though, oxidized metals such as iron (Fe(III)) and manganese (Mn(IV)) have also been linked to AOM (metal-AOM) (Beal et al. 2009; Boetius et al. 2000; Nauhaus et al. 2002; Sivan et al. 2011). In Chapter 4, I discuss a study of AOM in marine sediments, wherein the potential for oxidized forms of iron and manganese to oxidize methane to carbon dioxide is explored.

Abiotic reactions can also play an important role in coupled cycling. It has been demonstrated that many of the reactions in the conventional biotic view of the nitrogen cycling can also be performed abiotically, often by redox active metals such as iron and manganese (Figure 2, Doane 2017; Zhu-Barker et al. 2015). For instance, “chemodenitrification” has linked the iron and nitrogen cycles (Buchwald et al. 2016; Grabb et al. 2017; Jones et al. 2015). The most important nitrogen cycle reaction in this thesis is the process of nitrification. Nitrification is generally written as  $\text{NH}_3$  (ammonia)  $\rightarrow$   $\text{NO}_2^-$  (nitrite)  $\rightarrow$   $\text{NO}_3^-$  (nitrate) and can thus be divided into the steps of ammonia oxidation and nitrite oxidation (Ward 2008). Conventional views of nitrification suggest that these steps are performed in sequence to gain energy by obligately aerobic microbes, including ammonia-oxidizing archaea (AOA), ammonia-oxidizing bacteria (AOB), nitrite-oxidizing bacteria (NOB), and more recently discovered comammox bacteria which are capable of oxidizing both ammonia and nitrite (Könneke et al. 2005; Kowalchuk and Stephen 2001; Van Kessel et al. 2015; Watson et al. 1981). In Chapters 2 and 3, I make a detailed examination of abiotic nitrification

reactions between nitrogen and manganese species (Figure 3). In Chapter 2, I explore an alternative mechanism for nitrite oxidation which is both abiotic and agnostic to the presence of oxygen. Nitrification is also known to produce nitrous oxide ( $\text{N}_2\text{O}$ ) as a side product through a process that is still not well understood but may involve the reactive intermediate hydroxylamine ( $\text{NH}_2\text{OH}$ ). In Chapter 3, I investigate a second potential abiotic reaction mechanism that can transform  $\text{NH}_2\text{OH}$  to  $\text{N}_2\text{O}$  under environmental conditions. Coupled cycling may also play an important role in mixed abiotic-biotic reactions; for instance, leakage of a reactive intermediate such as hydroxylamine from an ammonia-oxidizing bacterial or archaeal cell may promote reaction with dissolved metals ions present outside the cell (Kits et al. 2019; Kozłowski et al. 2016; Liu et al. 2017; Soler-Jofra et al. 2021). In Chapter 3, I discuss one of these potential reactions: the abiotic reaction of manganese with biologically produced hydroxylamine.

When attempting to study these complex, multi-element processes, stable isotopes can provide a crucial tool. Within both carbon and nitrogen cycling, natural abundance stable isotopes have been used to help disentangle co-occurring processes (Casciotti 2016; Wagner and Herrle 2014). Additions of enriched isotope tracers have also been utilized to measure rates of reaction. In this thesis I use stable isotopes of nitrogen ( $^{15}\text{N}$ ,  $^{14}\text{N}$ ), oxygen ( $^{18}\text{O}$ ,  $^{16}\text{O}$ ), and carbon ( $^{13}\text{C}$ ,  $^{12}\text{C}$ ) to track reaction pathways, measure reaction rates, and calculate isotope effects. The goal of this thesis is to use stable isotopes as a tool to probe coupled cycling reactions between the trace metals iron and manganese and the nutrients carbon and nitrogen. This thesis consists of three data chapters. Chapters 2 and 3 focus on abiotic interactions between manganese (III) and nitrogen species nitrite and hydroxylamine, respectively. I establish that these reactions can occur under environmentally relevant conditions and that their isotopic signatures are similar or even identical to those of the corresponding biological reaction. I also use stable isotopes in these chapters to measure rates of reaction and evaluate potential back-reactions or further reaction of products, to better understand reaction mechanisms. Chapter 4 is a study of anaerobic oxidation of methane (AOM) in the presence of manganese, iron, and sulfur. Using  $^{13}\text{C}$  labeled methane as a tracer, I establish that the addition of oxidized metals to cold-seep sediments does not universally increase rates of AOM and may actually be inhibitory under some conditions. Finally, I conclude with Chapter 5, wherein I summarize the relevance and major findings of this thesis as well as briefly discuss future directions for study for each chapter.

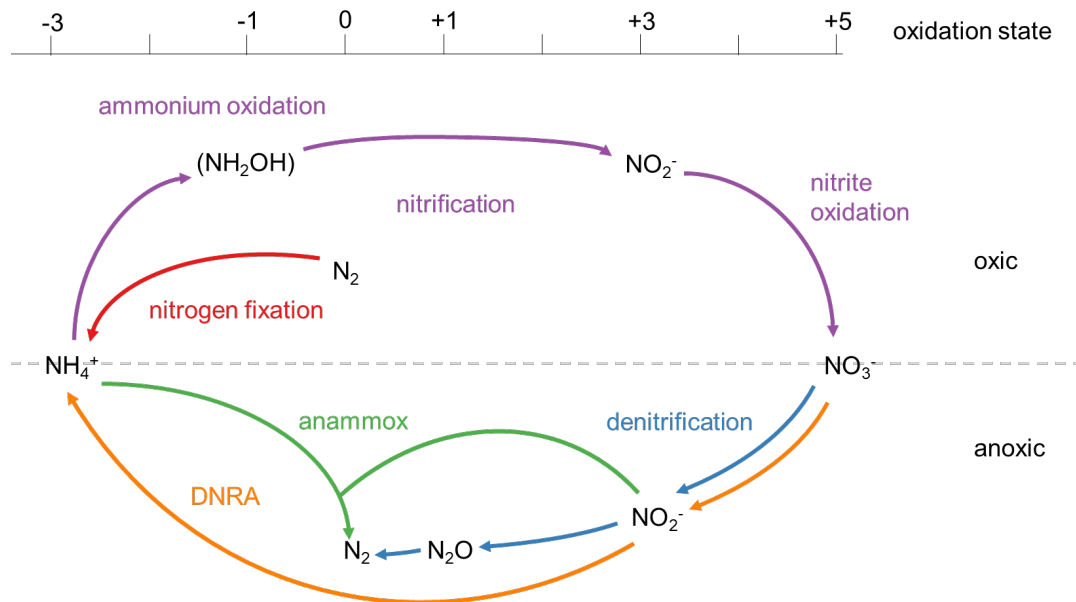
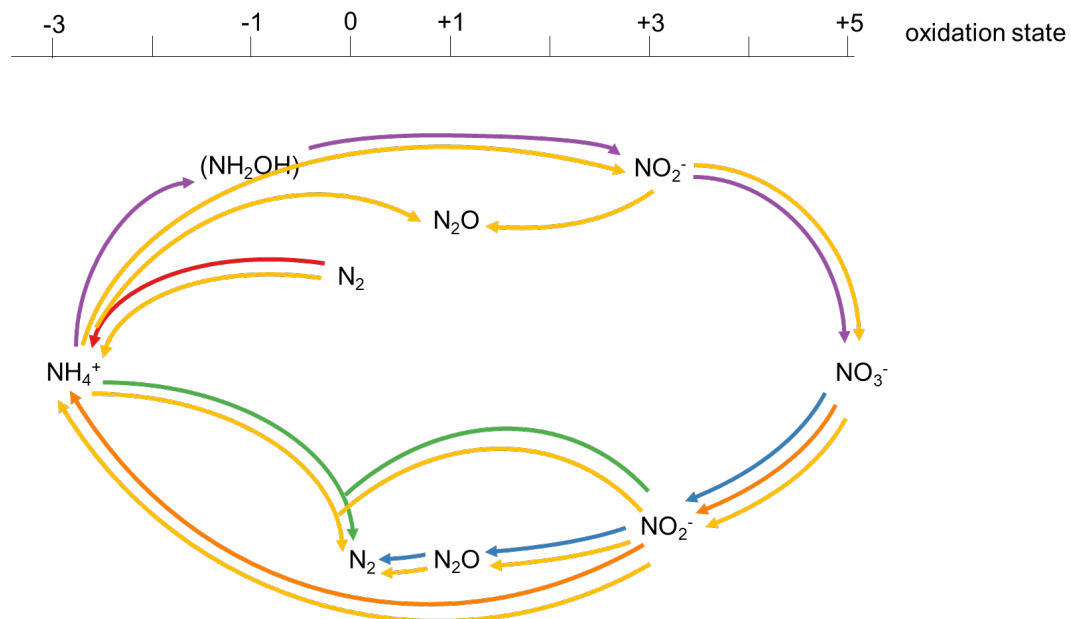


Figure 1: Major microbially driven processes and chemical species in the marine nitrogen cycle plotted against oxidation state of N. Processes above the dashed line occur in oxic environments and processes below occur in anoxic environments. DNRA = Dissimilatory Nitrate Reduction to Ammonium



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Figure 2: Major microbially driven processes and chemical species in the marine nitrogen cycle plotted against oxidation state of N (red, orange, green, blue, and purple arrows) alongside a selection of abiotic process (yellow arrows). Adapted from Doane 2017.

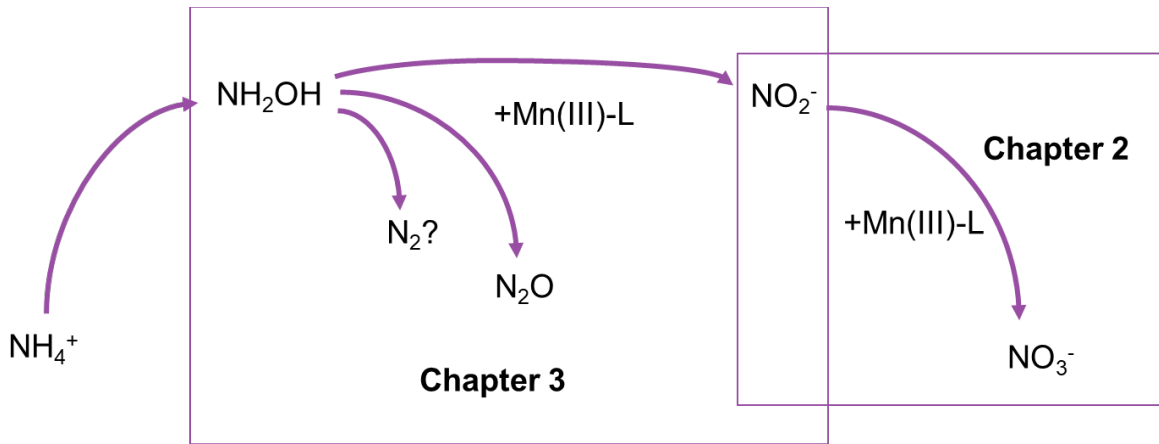


Figure 3: Conceptual diagram showing the abiotic reactions discussed in chapters 2 and 3.

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## 2. An isotopic study of abiotic nitrite oxidation by ligand-bound manganese (III)

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### **Abstract**

Redox transformations of nitrogen (N) play a critical role in determining its speciation and biological availability, thus defining the magnitude and extent of productivity in many ecosystems. A range of important nitrogen transformations often co-occur in regions hosting redox-active elements, including sulfur, iron and manganese (Mn), especially along sharp redox gradients within aquatic sediments. This proximity produces conditions under which multi-element interactions and coupled cycling are thermodynamically favored. While previous work has reported anoxic nitrification linked to the presence of manganese (Mn) oxides in sediments, a clear connection between the cycling of Mn and N has remained elusive. Soluble Mn(III), which is stabilized via ligand-complexation, has recently been shown to represent the dominant dissolved Mn species in many environments. Here, we examined the reactivity of ligand-stabilized Mn(III) with nitrite, using natural abundance stable nitrogen and oxygen isotopes to explore reaction dynamics under a range of conditions. Oxidation of nitrite to nitrate by Mn(III)-pyrophosphate proceeded abiotically under both oxygen replete and nitrogen-purged conditions. Kinetics and isotope systematics of this reaction were measured over a range of pH (5 to 8), with reaction rates decreasing with increasing pH. Under all treatments, an inverse kinetic isotope effect of  $-19.9 \pm 0.7\%$  was observed for N, remarkably similar with previously documented fractionation by nitrite-oxidizing organisms. Experiments using  $^{18}\text{O}$ -labeled water confirmed that the source of the additional oxygen atom was from water. These findings suggest that nitrite oxidation in environments hosting abundant ligand-bound Mn(III), including porewaters, estuaries and coastal waters, may be facilitated in part by abiotic reactions with Mn, even under functionally anoxic conditions.

## 2.1 Introduction

As a primary nutrient for sustaining life, the processes governing the transformations of nitrogen (N) have long been a topic of interest. The N cycle is also intricately linked with the cycling of other important elements in aquatic environments, including carbon, oxygen, phosphorous, sulfur, iron, and manganese (Mn) (Gruber and Galloway, 2008; Burgin et al., 2011; Melton et al., 2014). While the cycling of nitrogen has traditionally been attributed to microbially-mediated transformations, recent studies have highlighted abiotic processes as likely important and understudied aspects of nitrogen cycling under some conditions (Zhu-Barker et al., 2015; Heil et al., 2016; Doane, 2017; Cavazos et al., 2018; Stanton et al., 2018).

Redox interactions between Mn and N in sediments have been the focus of previous studies, however, their importance in global cycling is still poorly understood (Zhu-Barker et al., 2015; Doane, 2017). For example, Luther et al. (1997) showed in laboratory and field studies that reactions between ammonia (NH<sub>3</sub>) and Mn(III,IV) (oxy)(hydr)oxides (hereinafter Mn oxides) in sediments could act to “short circuit” the nitrogen cycle by providing a direct pathway to the formation of dinitrogen gas ( $2\text{NH}_3 + 3\text{MnO}_2 + 6\text{H}^+ \rightarrow 3\text{Mn}^{2+} + \text{N}_2 + 6\text{H}_2\text{O}$ ). Subsequent work also found indirect evidence for anoxic nitrification coupled to reduction of Mn oxides to Mn(II) (Hulth et al., 1999; Anschutz et al., 2000). In contrast, however, targeted studies using incubations amended with <sup>15</sup>NH<sub>4</sub><sup>+</sup> failed to find conclusive evidence that reactions between ammonia and manganese were occurring in a Mn oxide rich continental basin sediment (Thamdrup and Dalsgaard, 2000). More recent field studies have suggested that the specific geochemical conditions, including the concentration and age of the Mn oxides, are key factors controlling the efficacy of Mn oxide catalyzed anaerobic nitrification (Bartlett et al., 2007; Bartlett et al., 2008), or that reactions may only occur in presence of colloidal Mn oxides or more reactive Mn(III) species (Luther and Popp, 2002; Lin and Taillefert, 2014).

While many biogeochemical models of Mn in sediments include only soluble Mn(II) and solid Mn(III,IV) oxides, soluble Mn(III) can be stabilized via complexation by ligands and has been recently shown to represent the dominant dissolved Mn species in many environments (Madison et al., 2013; Oldham et al., 2015). With a reduction potential close to that of molecular oxygen (Luther et al., 1997; Luther III, 2010), Mn(III)-ligand (Mn(III)-L) complexes have the capacity to

be potent and important environmental oxidants. For instance, Mn(III)-L complexes can directly oxidize carbon, ferrous iron, and sulfide (Kostka et al., 1995). Ultimately, the extent to which Mn(III)-L complexes interact with other redox-active elements and molecules will depend on the specific ligand and subsequent strength of Mn(III) complexation. While the composition of Mn(III) ligands in natural systems is presently unknown, a diversity of ligand compositions and complex strengths has been predicted, ranging from weaker ligands such as pyrophosphate to complex humics with strong ligand moieties (Yakushev et al., 2009; Oldham et al., 2015; Oldham et al., 2017a).

The role of Mn(III) in Mn-N redox interactions is a potentially important component in the biogeochemical cycles of both elements that has not been fully addressed by previous studies (Luther et al., 1997; Luther et al., 2018). One major challenge to studying coupled cycling reactions is determining the importance of a single process from a range of potential biotic and abiotic reactions occurring in the environment. Stable isotope studies of nitrogen and oxygen have proven to be powerful tools in decoupling complex processes in the nitrogen cycle across a range of environments and contexts (Kendall et al., 2007; Casciotti, 2016). The abundance ratio of the two stable isotopes of N ( $^{14}\text{N}$  and  $^{15}\text{N}$ ) as well as O ( $^{16}\text{O}$  and  $^{18}\text{O}$ ) can vary as the result of isotope fractionation during processes including enzymatic or chemical reactions. As specific reactions may yield unique isotopic fractionation patterns, measurements of isotope ratios can be used to disentangle complex processes in the environment (Granger and Wankel, 2016). Hence, a focus of this study is to characterize the isotopic fractionation of specific reactions in order to identify abiotic, anoxic nitrite oxidation by ligand-stabilized Mn(III). Here we hypothesize that Mn(III) is a viable and environmentally relevant oxidant of nitrite ( $\text{NO}_2^-$ ) in aquatic systems. We present a series of experiments describing one such potentially important reaction between Mn(III) and  $\text{NO}_2^-$  and provide the first examination of the stable N and O isotope dynamics captured by the reaction.

## **2.2 Methods**

### *2.2.1 Experimental Overview*

Aspects of the reaction between Mn(III) and  $\text{NO}_2^-$  were targeted through a variety of experimental approaches. Specifically, experiments were conducted to evaluate 1) the influence of reactant concentrations and pH on the reaction kinetic expression, 2) the kinetic nitrogen isotope effect of

NO<sub>2</sub><sup>-</sup> oxidation by measurement of reactant and product isotopic compositions over reaction progress, 3) the influence of dissolved O<sub>2</sub> on reaction rates by varying solution and headspace composition, 4) the possible role of chemically catalyzed equilibrium (or back-reaction) between NO<sub>2</sub><sup>-</sup> and reaction products (by use of NO<sub>3</sub><sup>-</sup> with an elevated δ<sup>15</sup>N), and 5) the source of O atoms in reaction product NO<sub>3</sub><sup>-</sup> (by use of <sup>18</sup>O-labeled water).

### *2.2.2 Preparation of solutions*

Manganese(III)-pyrophosphate (Mn(III)-PP) solutions were prepared as previously described (Madison et al., 2011). A 5 mM solution of sodium pyrophosphate was prepared in de-oxygenated milliQ water and the pH adjusted to 7.0 using 6M hydrochloric acid (HCl). Manganese(III)-acetate salt (0.91 mM) was added to form a clear pink Mn(III)-PP solution (approximately 1 mM) which was subsequently filtered (0.45 μm) to remove any incidental particulate Mn oxides formed via disproportionation. The pH of Mn(III)-PP was adjusted by addition of 6M HCl before filter sterilization (0.2 μm). Additional solutions of Mn(III)-PP were prepared in <sup>18</sup>O-labeled water. Solid Mn oxides in the form of buserite were prepared as described previously (Mandernack et al., 1995). Sodium nitrite and sodium nitrate solutions (10 mM) were prepared in milliQ water and sterilized by autoclaving. Solutions of <sup>18</sup>O-labeled nitrite were prepared by equilibrating solutions of autoclaved nitrite in <sup>18</sup>O-labeled water in a 50°C oven for 7 days (Buchwald and Casciotti, 2013). All experiments were initiated in 160 mL serum bottles by the addition of 1 mL of 10 mM nitrite to 100 mL of ~1 mM Mn(III)-PP in excess pyrophosphate, giving a starting nitrite concentration of ~100 μM. Subsamples were collected over time by removing 3 mL of solution with a sterile syringe and replacing the headspace with air or N<sub>2</sub> gas depending on the experimental treatment. The presence of Mn(III)-PP complex was found to interfere with nitrite and nitrate concentration measurements and was thus removed prior to analysis by precipitation of all Mn as Mn oxides by the addition of 10 μL of 6M NaOH, followed by filtration of Mn precipitate (0.2 μm) and neutralization by addition of HCl.

### *2.2.3 Chemical speciation*

Concentrations of nitrate plus nitrite were measured using chemiluminescent NO<sub>x</sub> detection (Teledyne, T200) after reduction in hot acidic vanadyl sulfate solution (Braman and Hendrix, 1989). Nitrite concentrations were monitored using Griess reagent (Pai et al., 1990), and nitrate

concentration estimated by difference. Samples were diluted 10-fold with milliQ water to a final volume of 3 mL, treated with 60  $\mu$ L sulfanilamide (SAN) and 60  $\mu$ L *N*-(1-Naphthyl)ethylenediamine (NED) and measured for absorbance at 543 nm. Mn(III) concentrations were measured using the leucoberberlin blue method referenced to a standard curve of potassium permanganate and adjusted to account for the oxidation state offset (Krumbein and Altman, 1973; Jones et al., 2019).

#### 2.2.4 Isotopic measurements

Isotopic ratios ( $^{15}\text{N}/^{14}\text{N}$ ,  $^{18}\text{O}/^{16}\text{O}$ ) are reported using standard delta notation where  $\delta^{15}\text{N} = [(^{15}\text{R}_{\text{sample}}/^{15}\text{R}_{\text{N}_2\text{-ATM}})-1]*1000$ ] and  $^{15}\text{R} = ^{15}\text{N}/^{14}\text{N}$  and where  $\delta^{18}\text{O} = [(^{18}\text{R}_{\text{sample}}/^{18}\text{R}_{\text{VSMOW}})-1]*1000$ ] and  $^{18}\text{R} = ^{18}\text{O}/^{16}\text{O}$ . Isotopic composition of nitrite was measured after conversion of 20-30 nmol to nitrous oxide ( $\text{N}_2\text{O}$ ) using the azide method (McIlvin and Altabet, 2005) in 20 mL crimp-sealed headspace vials. Nitrate N and O isotopes were measured using the denitrifier method (Sigman et al., 2001; Casciotti et al., 2002) to convert samples to nitrous oxide after removal of nitrite by sulfamic acid addition (Granger and Sigman, 2009). The resulting  $\text{N}_2\text{O}$  was then purified and trapped on a modified TraceGas (IsoPrime, Inc.) purge and trap system coupled with a Gilson autosampler before isotopic analysis on an isotope ratio mass spectrometer (IRMS) (IsoPrime 100, Elementar Inc.). Isotope reference materials for nitrate (USGS 32, USGS 34, USGS 35) or nitrite (WILIS 10, WILIS 11 and WILIS 20) were run before and after samples at 3 different sizes to normalize reported isotope values and correct for variations in sample size and any instrument drift. Values of USGS 32, USGS 34, and USGS 35 are +180, -1.8, and +2.7‰ for  $\delta^{15}\text{N}$  and +25.4, -27.8, and +56.8‰ for  $\delta^{18}\text{O}$ , respectively (Brand et al., 2009). Inter-laboratory comparisons set the values of WILIS 10, WILIS 11, and WILIS 20 at -1.7, +57.1, and -7.8‰ for  $\delta^{15}\text{N}$  and +13.2, +8.6 and +47.6‰ for  $\delta^{18}\text{O}$  (Wankel et al., 2017). Typical reproducibility is  $\pm 0.2\%$  for both  $\delta^{15}\text{N}$  and  $\delta^{18}\text{O}$  using the azide method and  $\pm 0.2\%$  for  $\delta^{15}\text{N}$  and  $\pm 0.5\%$  for  $\delta^{18}\text{O}$  using the denitrifier method. Here we adopt the isotope notation convention wherein reactions resulting in products with a preference for lighter isotopes are indicated by a ‘normal’ isotope effect with a positive sign; thus, a negative sign indicates an inverse isotope effect.

## 2.3 Results

### 2.3.1 Concentrations of nitrite and nitrate

Nitrite (100  $\mu\text{M}$ ) was reacted with Mn(III)-PP ( $\sim 1$  mM) under a headspace of air over a period of 11 days at three pH treatments (pH = 5.0, 5.7, 6.5) with four replicates. Over the course of the experiment, nitrite concentrations were monitored and found to decrease to undetectable levels ( $< 1$   $\mu\text{M}$ ) by the end of the experiment, with higher pH treatments reacting more slowly (Figure 1a). At the conclusion of the experiment, concentrations of nitrate produced were 1:1 with nitrite consumed (not shown). Parallel controls without pyrophosphate or Mn(III)-PP showed no loss of nitrite during the experiment.

### 2.3.2 Isotopic fractionation

Nitrite  $\delta^{15}\text{N}$  values universally decreased from their starting value ( $-2.3\text{‰}$ ) during the course of the reaction in relation with the proportion of nitrite consumed. Oxygen isotope ratios showed no statistical difference between starting and ending values. Calculation of the N isotope effect of nitrite oxidation by Mn(III)-PP ( $^{15}\epsilon_{\text{NO}_{2\text{ox}},\text{MnIII}}$ ) assuming closed-system Rayleigh dynamics (Mariotti et al., 1981) yielded  $^{15}\epsilon_{\text{NO}_{2\text{ox}},\text{MnIII}}$  values of  $-19.1 \pm 0.5\text{‰}$  for pH = 5.0 ( $r^2 = 0.997$ ) and  $^{15}\epsilon_{\text{NO}_{2\text{ox}},\text{MnIII}} = -18.2 \pm 0.4\text{‰}$  for pH = 5.7 ( $r^2 = 0.997$ ) in initial experiments. Nitrogen isotope effects were also calculated during a subset of reaction kinetics experiments described below and ranged from  $-19.2 \pm 0.4\text{‰}$  to  $-20.6 \pm 0.2\text{‰}$  (Figure 1b; Table 1).

### 2.3.3 Reaction kinetics

Two experiments were conducted in order to determine the reaction kinetics and order with respect to Mn(III)-PP and nitrite. The isolation method was used, in which initial concentration of one reagent was varied while other variables were held constant. Solutions of varying Mn(III)-PP concentration were prepared by v/v dilution of an approximately 1 mM solution with 5 mM pyrophosphate. All experiments were run with air as the headspace at pH = 5.0 (Table 1).

To determine the role of pH in the kinetics of reaction, incubations were conducted at pH = 5.0, 5.7, and 6.5. Solution pH was buffered by excess pyrophosphate with pH stability confirmed by measurement at the conclusion of the experiment. Solid oxides were added to minimize influence of Mn(III)-PP loss during the reaction (additional Mn(III)-PP complex will form in the presence

of excess Mn oxides and pyrophosphate ligand). An additional control with Mn oxides and no pyrophosphate ligand displayed no reactivity with nitrite.

Using the balanced reaction (Eq. 1), a general rate law (Eq. 2) was written to derive the rate of reaction. Concentrations in Eq. 2 represent the total concentration of each reactant. For simplicity of notation,  $[NO_2^-]$  also includes any nitrous acid ( $HNO_2$ ) present.  $NO_2^- + 2Mn(III)-PP + H_2O \rightarrow NO_3^- + 2Mn^{2+} + 2PP + 2H^+$  [1]

$$\frac{d[NO_3^-]}{dt} = k[Mn(III)PP]^a[NO_2^-]^b[H^+]^c \quad [2]$$

$$rate = \frac{d[NO_3^-]}{dt} = -2 \frac{d[Mn(III)PP]}{dt} = -\frac{d[NO_2^-]}{dt} \quad [3]$$

where  $a$ ,  $b$ ,  $c$  represent the order of the reaction with respect to Mn(III)-PP,  $NO_2^-$ , and  $H^+$ , respectively, and  $k$  is the rate constant. When  $[Mn(III)-PP]$  is varied while pH and  $[NO_2^-]$  held constant equation 2 simplifies to:

$$rate = k_{obs,1}[Mn(III)PP]^a \quad [4]$$

where

$$k_{obs,1} = k[NO_2^-]^b[H^+]^c \quad [5]$$

Using the instantaneous rate method equation 4 can be rewritten as:

$$\log(rate_{ins}) = \log(k_{obs,1}) + a \log([Mn(III)PP]_{in}) \quad [6]$$

where  $rate_{ins}$  is the instantaneous rate and  $[Mn(III)PP]_{in}$  is the initial concentration of Mn(III)-PP. Thus, the slope ( $a$ ) of  $\log([Mn(III)PP]_{in})$  vs.  $\log(rate_{ins})$  indicated a 2<sup>nd</sup> order reaction with respect to Mn(III)-PP ( $a = 1.95 \pm 0.1$ ; Figure 2a).

Similarly, when  $[NO_2^-]$  is varied and  $[Mn(III)-PP]$  is held constant equation 2 can be written as:

$$rate = k_{obs,2}[NO_2^-]^b \quad [7]$$

with

$$k_{obs,2} = k[Mn(III)PP]^a[H^+]^c \quad [8]$$

As above this can be expressed as:

$$\log(rate_{int}) = \log(k_{obs,2}) + b \log([NO_2^-]_{in}) \quad [9]$$

The slope ( $b$ ) of  $\log([NO_2^-]_{in})$  vs.  $\log(rate_{int})$  gave a value of  $1.03 \pm 0.04$ , indicating the reaction is 1<sup>st</sup> order with respect to  $NO_2^-$  (Figure 2b).

To determine the role of pH, reactions were conducted in the presence of excess Mn oxides and pyrophosphate, to minimize any changes in the concentration of Mn(III)-PP. Thus assuming constant [Mn(III)-PP], kinetics appeared pseudo-first order with respect to nitrite and rate constants were calculated from the slope of time vs.  $\ln([NO_2^-])$  (Figure 2c). As above the rate expression was simplified:

$$rate = k_{obs,3}[H^+]^c \quad [10]$$

with

$$k_{obs,3} = k[Mn(III)PP]^a[NO_2^-]^b \quad [11]$$

Using the pseudo-first order rate constants derived as described above:

$$\log(rate) = \log(k_{obs,3}) + c \log([H^+]) \quad [12]$$

Equation 12 was solved for the slope  $c$ , indicating the reaction is 1<sup>st</sup> order with respect to concentration of protons (Figure 2d;  $c = 0.96 \pm 0.01$ ). The overall rate expression is thus:

$$\frac{d[NO_3^-]}{dt} = k[Mn(III)PP]^2[NO_2^-][H^+] \quad [13]$$

This rate expression can also be simplified as:

$$\frac{d[NO_3^-]}{dt} = k[Mn(III)PP]^2[HNO_2]K_a \quad [14]$$

Where  $K_a$  represents the acid dissociation constant of nitrous acid. Thus we conclude the reactant is  $HNO_2$ , rather than  $NO_2^-$ .

#### 2.3.4 Reaction rates

Based on observed changes in concentrations over time for experiments at pH = 5.0, 5.7, and 6.5 (starting  $NO_2^- = 100 \mu M$  and Mn(III)-PP = 1000  $\mu M$ , four replicates), nitrite reduction rates of  $518 \pm 16.8$ ,  $108 \pm 4.8$ , and  $21.6 \pm 2.4 \mu M d^{-1}$  were calculated, respectively (Table 2). Additional incubation experiments were performed with the same starting concentrations at pH 7 and 8 using isotopically labeled  $^{15}NO_2^-$  to determine the reaction rates at pH values relevant to the marine system (Ward, 2011; Beman et al., 2013). Unlabeled nitrite (9 mM),  $^{15}N$ -nitrite (1 mM), and unlabeled nitrate (4 mM) were pre-mixed and aliquotted into bottles as described above and then sampled over 3 months to track accumulation of  $^{15}N$  in the  $NO_3^-$  pool over time. Under these reaction conditions rates of nitrite oxidation by Mn(III)-PP at pH 7 and 8 were  $5.8 \pm 1.3$  and  $3.9 \pm 0.6 \mu M d^{-1}$ , respectively (Table 2).



### 2.3.5 Effect of dissolved oxygen

To determine the potential role of oxygen in the oxidation of nitrite to nitrate by Mn(III)-PP, two parallel incubations were conducted either with a headspace of laboratory air or after vigorously purging with N<sub>2</sub> gas for 15 minutes to substantially reduce the amount of dissolved oxygen. Experiments were run at pH 5 and sampled over 4 days. No significant difference in reaction rates was found between the oxic and N<sub>2</sub>-sparged treatments (Table 1, Figure 3). Similarly, the observed N isotope fractionation was unaltered by oxygen level ( $p = 0.28$ ).

### 2.3.6 Potential reversibility of reaction

To test the possibility of reaction reversibility, experiments were run with the addition of nitrate having an elevated  $\delta^{15}\text{N}$  value (USGS 32,  $\delta^{15}\text{N} = +180$ ). Two treatments contained an additional 10  $\mu\text{M}$  (10% of nitrite added) and 100  $\mu\text{M}$  (100% of nitrite added) nitrate at the beginning of each experiment at two pH values (pH = 5.0, 5.5). Sub-samples were collected over a period of 8 days. Again, no observed change in  $^{15}\epsilon_{\text{NO}_2\text{ox},\text{MnIII}}$  was noted among treatments receiving high  $\delta^{15}\text{N}\text{-NO}_3^-$  in comparison to previous experiments receiving no  $\text{NO}_3^-$  amendment (Table 1).

### 2.3.7 Source of additional oxygen atom

In order to determine the source of the additional oxygen atom in nitrate, an experiment using  $^{18}\text{O}$ -labeled water was performed. Two  $^{18}\text{O}$ -labeled water samples having  $\delta^{18}\text{O}$  values of approximately +18‰ and +40‰ were prepared by dilution from a stock solution ( $\sim+5000\text{‰}$ ), with an unlabeled water sample with  $\delta^{18}\text{O} \sim -5\text{‰}$  used as a third condition. As nitrite oxygen isotopes equilibrate with water quickly at the pH conditions of our experiments (Casciotti et al., 2007),  $^{18}\text{O}$ -labeled nitrite stock solutions were also prepared as described above in an aliquot of each labeled water sample. As the result of equilibrium isotope fractionation between  $\text{NO}_2^-$  and  $\text{H}_2\text{O}$ , fully equilibrated nitrite has a  $\delta^{18}\text{O}$  value  $\sim 14\text{‰}$  higher than its surrounding water (Casciotti et al., 2007; Buchwald and Casciotti, 2013). Average starting values of  $\delta^{18}\text{O}\text{-NO}_2^-$  were +11, +32, and +54‰ after equilibration with  $^{18}\text{O}$ -labeled water.

Five treatments ( $\delta^{18}\text{O}_{\text{water}} = -5\text{‰}$ , +18‰, +40‰ oxic,  $\delta^{18}\text{O} = -5\text{‰}$  N<sub>2</sub>-sparged, oxic no Mn control) were run at three pH conditions (pH = 5.0, 5.7, 6.5) and subsampled over 17 days. Samples of nitrite and nitrate were analyzed for  $\delta^{18}\text{O}$ . No differences in rates or  $\delta^{18}\text{O}$  values were found

between  $\delta^{18}\text{O}\text{-NO}_3^-$  produced under oxic or  $\text{N}_2$ -sparged conditions ( $p = 0.59$ ). The slope of  $\delta^{18}\text{O}\text{-H}_2\text{O}$  vs.  $\delta^{18}\text{O}\text{-NO}_3^-$  was very close to 1 under all three pH conditions, indicating water was the source of the third O-atom in nitrate (Figure 4; Table 3). Examination of the y-intercept of these data also allows calculation of the kinetic isotope effect associated with incorporation of the O atom from water ( $^{18}\epsilon_{\text{k,H}_2\text{O}}$ ), which was determined to be  $+20.3 \pm 1.5\text{‰}$ .

## 2.4 Discussion

Environmental transformations of nitrogen play a fundamental role in determining its fate as a nutrient and contaminant across ecosystems. While the framework for these processes is complex, it is widely understood that microbially driven reactions comprise the large majority of these transformations. Nevertheless, there also exists an array of abiotic transformations that may contribute to the complex framework of environmental nitrogen transformations under some conditions (Luther 2010; Zhu-Barker et al., 2015; Heil et al., 2016; Doane, 2017; Luther et al. 2018). Among these are redox reactions involving commonly abundant transition metals, especially Mn and Fe (Heil et al., 2015; Zhu-Barker et al., 2015; Buchwald et al., 2016; Doane, 2017; Grabb et al., 2017; Cavazos et al., 2018; Stanton et al., 2018). Here we demonstrate that ligand bound Mn(III) can serve as an important oxidant of nitrite, producing nitrate under environmentally relevant conditions and independent of molecular oxygen concentrations. We further present our stable isotopic interrogation of this process, shedding light on source O atoms and associated kinetic isotope effects, and discuss its possible relevance in environmental N cycling.

### 2.4.1 Mn(III) is an effective oxidant of $\text{NO}_2^-$ - with possible environmental relevance

Foremost, our results demonstrate that ligand bound Mn(III) is an effective oxidant of nitrite under the conditions evaluated including circumneutral pH and modestly elevated concentrations. While Mn is present in the environment in three oxidation states (II, III, and IV), most studies exploring the oxidative potential of oxidized Mn on the N cycle have only examined the reactivity of Mn oxide minerals, thus overlooking the possible influence of dissolved, oxidized Mn (Bartlett, 1981; Stone and Morgan, 1984; Nelson et al., 2002). Additionally, Mn oxide minerals may vary widely in structure, oxidation state and reactivity (Post, 1999). To the best of our knowledge, the potential relevance of Mn to nitrite oxidation has only been examined in two previous studies, both

involving solid-phase Mn oxides (Bartlett, 1981; Luther and Popp, 2002). Bartlett (1981) first observed abiotic oxidation of nitrite to nitrate in sterilized soils upon addition of Mn oxides, while Luther and Popp (Luther and Popp, 2002) more formally evaluated the kinetics of nitrite oxidation by colloidal Mn oxides. In contrast to these solid Mn oxide phases, ligand bound Mn(III) forms have recently been shown to comprise the majority of dissolved Mn across a range of aquatic systems (Kostka et al., 1995; Madison et al., 2011; Oldham et al., 2015; Oldham et al., 2017a). These Mn(III)-L complexes have been shown to easily pass through conventional filtration (0.2-0.45  $\mu\text{m}$ ) (Wilczak et al., 1993; Kostka et al., 1995; Luther and Popp, 2002) and ultrafiltration (0.02  $\mu\text{m}$ ) (Oldham et al., 2017a; Oldham et al., 2017b), suggesting that previous studies assuming that all dissolved Mn was present as Mn(II) may have overlooked an important and reactive fraction of soluble Mn. Indeed our experimental results demonstrate that Mn(III)-L complexes are viable oxidants of nitrite under conditions of environmental relevance.

#### 2.4.2 Reaction rate

Over the range of conditions we evaluated, observed rates of Mn(III)-L induced nitrite oxidation ranged from 3.9  $\mu\text{M d}^{-1}$  up to 518.4  $\mu\text{M d}^{-1}$  over pH values from 8.0 to 5.0, respectively (Table 2). While direct comparison with other studies of nitrite oxidation by bacterial cultures or in aqueous environments is not straightforward, to a first order, our observed rates are similar to those reported in a wide variety of studies. For example, recently reported rates of aerobic nitrite oxidation by axenic cultures of nitrite-oxidizing *Nitrobacter* and *Nitrospira* bacteria yielded half saturation constants ( $K_m$ ) of 49 to 544  $\mu\text{M}$  and 9 to 27  $\mu\text{M}$ , and  $V_{\text{max}}$  values of 64 to 164 and 18 to 48  $\mu\text{mol mg protein}^{-1} \text{ hr}^{-1}$ , respectively (Nowka et al., 2015). Under our experimental conditions (all other factors being equal), a nitrite-oxidizer cell density corresponding to hypothetical protein concentration of 100  $\mu\text{g/L}$ , would yield initial nitrite oxidation rates of 17 to 500  $\mu\text{M d}^{-1}$  – similar in magnitude to the initial Mn(III)-L induced rates we observed at pH 5.0 and 5.7 of 518  $\mu\text{M d}^{-1}$  and 108  $\mu\text{M d}^{-1}$ , respectively.

Rates of nitrite oxidation in aqueous environments, of course, are much lower than those observed in bacterial cultures or lab experiments and are therefore commonly measured by addition of  $^{15}\text{NO}_2^-$  and measured accumulation of  $^{15}\text{NO}_3^-$  with time (Ward, 2011). In particular, much effort has focused on characterization of nitrite oxidation rates in oxygen deficient hotspots of nitrogen

transformation in the global ocean – yielding values ranging from 0 to ~600 nM d<sup>-1</sup> (Ward et al., 1989; Lupschultz et al., 1990; Beman et al., 2013; Peng et al., 2015; Bristow et al., 2016; Sun et al., 2017). Other studied environments include coastal environments, open ocean, estuaries, and coral reefs, also typically exhibit rates ranging from ~0 up to several hundred nM d<sup>-1</sup> (Dore and Karl, 1996; Bianchi et al., 1997; Heiss and Fulweiler, 2016). While microbial nitrite oxidation is generally considered to be an aerobic process, under oxygen-restricted conditions, the anaerobic oxidation of ammonium (anammox) is also known to oxidize NO<sub>2</sub><sup>-</sup> to NO<sub>3</sub><sup>-</sup> at stoichiometry of ~0.19 moles of NO<sub>3</sub><sup>-</sup> produced per mole of NH<sub>4</sub><sup>+</sup> oxidized (Jetten et al., 1999; Strous et al., 2006; Kartal et al., 2011). Extrapolating from measured anammox rates in oceanic oxygen deficient zones (ODZs) and groundwaters suggests that environmental anammox based nitrite oxidation rates may range from <1 nM d<sup>-1</sup> up to 70 nM d<sup>-1</sup> (Kuypers et al., 2003; Dalsgaard et al., 2005; Lam et al., 2007; Moore et al., 2011).

Turning to the only previously reported rates of Mn induced nitrite oxidation, Luther and Popp (2002) reported a rate constant (k) of 493 M<sup>-1</sup> min<sup>-1</sup> at pH = 5.00 for reaction of NO<sub>2</sub><sup>-</sup> with “polymeric” (colloidal) Mn oxides. Thus, relative to rates we observe in our experiment, at [MnO<sub>2</sub>] = 1 mM and [NO<sub>2</sub><sup>-</sup>] = 100 μM, the predicted rate of NO<sub>3</sub><sup>-</sup> formation would be several orders of magnitude greater than rates we observed. Nevertheless, Mn oxides, including colloids, will be considerably lower than 1 mM in most environments, and could be less reactive due to surface adsorbates and/or co-precipitates. Further, Mn(III)-L and Mn oxides are oftentimes decoupled spatially. For instance, along redoxclines in stratified systems, Mn(III)-L span a wide redox gradient, while Mn oxides have a distinct peak in their distribution along the gradient (Trouwborst et al., 2006; Yakushev et al., 2007; Yakushev et al., 2009; Dijkstra et al., 2018). In any regards, predicted rates of nitrite oxidation by Mn(III)-L are similar in magnitude to biological rates described above. For example, under conditions that might typify porewaters close to an estuarine sediment-water interface (pH 6.5, [NO<sub>2</sub><sup>-</sup>] = 10 μM, [Mn(III)-PP] = 80 μM) an estimate of 14 nM d<sup>-1</sup> would be feasible (Madison et al., 2013). This result suggests that abiotic nitrite oxidation by Mn(III)-L complexes may be competitive with corresponding microbial processes, particularly at pH < 7 (Table 4). When taken together with the previously demonstrated potential for Mn oxides to also oxidize nitrite, Mn may therefore represent an important and currently underappreciated oxidant of nitrite within some ecosystems.

### 2.4.3 Stable isotope dynamics

Nitrite does not readily accumulate in most aquatic environments, with concentrations rarely reported above more than a few  $\mu\text{M}$ . Nevertheless, as with other reactive intermediates, its low concentrations reflect its high reactivity and fluxes involving nitrite can be high. As a consequence of these low ambient levels, nitrite has only recently been interrogated by stable isotope analyses. As both a reductive and oxidative intermediate of several transformation processes, the nitrogen and oxygen isotope dynamics of nitrite are often complex and reflect multiple processes (Casciotti et al., 2011; Buchwald and Casciotti, 2013; Casciotti, 2016; Buchwald et al., 2018). Thus, there still remains much to be learned from gaining an improved understanding of the systematics that govern its natural isotopic composition across environments in particular those with strong redox variations.

Our experiments yielded a number of insights that shed light on the nature of the reaction examined. First, abiotic nitrite oxidation by Mn(III)-PP yielded an average inverse nitrogen isotope effect ( $^{15}\epsilon_{\text{NO}_2\text{ox},\text{MnIII}}$ ) of  $-19.9 \pm 0.7\text{‰}$  across all experiments. No significant differences in this N isotope effect were observed between experiments, indicating that both pH ( $p = 0.59$ ) and  $\text{O}_2$  ( $p = 0.28$ ) did not influence N isotopic fractionation. While inverse isotope effects are not commonly observed, it is notable that biological nitrite oxidation has also been shown to exhibit this same dynamic. In a study of *Nitrococcus mobilis*, Casciotti (2009) first demonstrated this isotope behavior, suggesting that the lower zero point energy for the transition state of the  $^{14}\text{N}$  isotopologue over the  $^{15}\text{N}$  isotopologue for the N-O bond forming reaction favored the net transition of  $^{15}\text{N}$  into the product pool – thereby yielding a unique  $^{15}\text{N}$  depletion of the reactant nitrite pool over the course of the reaction. A similar dynamic has been demonstrated with anaerobic  $\text{NO}_2^-$  oxidation by anammox bacteria (Brunner et al., 2013; Kobayashi et al., 2019). This inverse isotope effect has since been invoked to explain large differences in  $\delta^{15}\text{N}$  of  $\text{NO}_2^-$  and  $\text{NO}_3^-$  in oxygen deficient zones of the oceans (up to  $\sim 40\text{‰}$ ) (Casciotti and McIlvin, 2007; Gaye et al., 2013; Bourbonnais et al., 2015; Peters et al., 2018), and in ocean sediment porewaters reported as high as  $54\text{‰}$  (Buchwald et al., 2018). Thus, the nitrogen isotope signature imparted by abiotic Mn-catalyzed oxidation of  $\text{NO}_2^-$  to  $\text{NO}_3^-$  appears similar in direction and magnitude to biological nitrite oxidation. Our study falls within the range of reported biological isotope effects for nitrite

oxidation (-12.8‰ to -45.3‰) (Casciotti, 2009; Kobayashi et al., 2019) with differences in magnitude likely resulting from differences in bond strengths in transition states.

Second, our results also indicate no significant variation in the observed values of  $^{15}\epsilon_{\text{NO}_{2\text{ox}},\text{MnIII}}$ , despite substantial differences in reaction rates among experimental conditions. Additionally, our evaluation of whether the unique inverse isotope effect might be explained by chemically catalyzed isotopic equilibrium between  $\text{NO}_2^-$  and  $\text{NO}_3^-$  confirmed that no backwards isotopic transfer occurred during the reaction. Had any sort of nitrogen isotope equilibrium occurred during the reaction, in-growth of  $^{15}\text{N}$  from labeled  $\text{NO}_3^-$  (added prior to experimental initiation) back into the reactant nitrite pool would have impacted the observed kinetic isotope effect. As such, our results suggest that the reaction proceeds in a single, irreversible step.

Third, no changes in reaction rate ( $p = 0.74$ ) or  $^{15}\epsilon_{\text{NO}_{2\text{ox}},\text{MnIII}}$  ( $p = 0.28$ ) were observed whether the reaction occurred under oxygen-saturated or oxygen-depleted ( $\text{N}_2$ -sparged) conditions, illustrating that the oxidation of nitrite to nitrate by Mn(III)-pyrophosphate is effectively agnostic to oxygen and occurs under hypoxic conditions. A similar observation was also previously reported during soil incubations of soils and synthetic Mn oxides, in which no differences in reaction extent or stoichiometry were observed between vessels open to air and those purged with  $\text{N}_2$  or  $\text{CO}_2$  (Bartlett, 1981).

The  $\delta^{18}\text{O}$  of the product nitrate derives from both reactant nitrite and the addition of a third O atom. Our experiments conducted in  $^{18}\text{O}$ -labeled water reveal the origin of this O atom – clearly deriving from water. By pre-equilibrating reactant  $\text{NO}_2^-$  with waters having different  $\delta^{18}\text{O}$  compositions, we observed a near 1:1 relationship between the experimental waters and the newly added oxygen (Figure 4). Luther and Popp (2002) postulated that this additional O atom might derive from Mn oxide, due to balancing of loss of two protons in the reaction. Although the formation of Mn oxide particles was not observed in our study, transient formation of Mn oxides via Mn(III) disproportionation is possible. However, if Mn-bound oxygen (or even  $\text{O}_2$ ) had been the source of the third oxygen atom, then the regression of  $\delta^{18}\text{O}_{\text{H}_2\text{O}}$  vs.  $\delta^{18}\text{O}_{\text{NO}_3}$  (Figure 4) would yield a slope of  $\sim 0.66$ , as the contribution of the third additional O atom would have the same  $\delta^{18}\text{O}$  value in all treatments (while the other two atoms from  $\text{NO}_2^-$  were in equilibrium with water). In all cases, the

near 1:1 slope unequivocally reflects incorporation of O atoms from water during formation of nitrate.

In contrast to the behavior of N isotopes in this system, nitrite O isotopes quickly equilibrate with the ambient water oxygen isotopes at the pH of our experiments (Casciotti et al., 2007; Buchwald and Casciotti, 2013). Resulting from this rapid oxygen isotope equilibration of  $\text{NO}_2^-$  with ambient  $\text{H}_2\text{O}$  at our experimental pH conditions, no differences between starting and ending  $\delta^{18}\text{O}$  of  $\text{NO}_2^-$  were observed. This complete oxygen isotope equilibration between nitrite and water allows us to determine the isotope effect associated with the incorporation of hydration shell water-oxygen into nitrate. Following derivations by Buchwald and Casciotti (2010), we calculate an overall kinetic isotope effect for incorporation of O from water  $^{18}\epsilon_{k,\text{H}_2\text{O}} = +20.3 \pm 1.5\%$ . As with the inverse N isotope effect, the isotope effect associated with incorporation of an O atom from water during Mn(III)-induced nitrite oxidation to nitrate is also analogous to the comparable isotope effect observed in nitrite oxidizing bacteria of +12.8 to +18.2‰ (Buchwald and Casciotti, 2010; Hollocher, 1984). Thus, abiotic  $\text{NO}_2^-$  oxidation by Mn(III) could conceivably operate in parallel to biological nitrite oxidation with no impact on the expected isotope dynamics of reactant  $\text{NO}_2^-$  or product  $\text{NO}_3^-$ .

#### *2.4.4 Coupling of Mn and N cycling in the environment*

Despite the favorable thermodynamic conditions for reactions coupling Mn and N transformations, and the commonly overlapping zonation of Mn and N species in redox transition regimes, direct evidence for the occurrence of these reactions in the environment remains limited. Coupled redox reactions between N and Mn species have been proposed by a number of previous studies using a range of approaches (Luther et al., 1997; Hulth et al., 1999; Anschutz et al., 2000; Thamdrup and Dalsgaard, 2000; Luther and Popp, 2002; Mortimer et al., 2004; Lin and Taillefert, 2014; Aigle et al., 2017). Notably, Luther and colleagues (Luther et al., 1997; Luther 2010; Luther et al., 2018) highlighted the thermodynamic favorability of reactions between Mn and N over a range of environmentally relevant conditions. Indeed, these thermodynamically favorable reactions have justified the search for microbial mediation of coupled Mn/N reactions. Studies of soils, freshwater lakes, marine sediments and even wastewater treatment operations have variably reported either the presence or absence of evidence for redox interactions of Mn and N (Dhakar and Burdige,

1996; Luther et al., 1997; Hulth et al., 1999; Anschutz et al., 2000; Thamdrup and Dalsgaard, 2000; Mortimer et al., 2002; Bartlett et al., 2007; Taillefert, 2014; Fernandes et al., 2015; Heil et al., 2015; Lin and Swathi et al., 2017). Nevertheless, while the apparent energetic yields of many Mn/N redox couples would appear to easily support microbial metabolisms, little evidence exists implicating any direct involvement in support of metabolic energy conservation.

Our data provide some intriguing insight into possible environmental links, specifically that soluble Mn(III)-ligands may readily oxidize  $\text{NO}_2^-$  to  $\text{NO}_3^-$  – an abiotic analog of the second step in bacterial nitrification – without the notable requirement of molecular oxygen. Indeed, several studies have concluded that so-called ‘anoxic nitrification’ may be important in marine and estuarine sediments (Luther et al., 1997; Hulth et al., 1999; Anschutz et al., 2000; Mortimer et al., 2002; Mortimer et al., 2004; Bartlett et al., 2008), with at least one study providing evidence for Mn-linked abiotic nitrification in soils (Bartlett, 1981). If important, anoxic nitrification could provide an important link and N loss term without a requirement of molecular oxygen. Most N loss (as  $\text{N}_2$ ) in soils and aquatic sediments is attributed to denitrification or anaerobic ammonium oxidation (anammox), both proceeding under low  $\text{O}_2$  conditions and requiring oxidized forms of N as electron acceptors (e.g.,  $\text{NO}_3^-$  or  $\text{NO}_2^-$ ). In general, production and delivery of these electron acceptors is linked to the activity of aerobic nitrifying organisms. Hence, a process by which N is oxidized in the absence of molecular oxygen could represent an important shunt in the N cycle.

A number of previous studies have highlighted the apparent occurrence of oxidative nitrogen cycling under anoxic conditions – with associated implications for involvement of Mn (Luther et al., 1997; Lin and Taillefert, 2014). For example, several studies examining highly resolved porewater profiles noted accumulation of  $\text{NO}_3^-$  at depths below what would be expected from diffusion alone, speculating that Mn oxides must play a role as environmental oxidant of reduced N in the absence of dissolved oxygen (Anschutz et al., 2000; Mortimer et al., 2004; Hulth et al., 2005; Bartlett et al., 2008). Other studies have used experimental amendments in sediment incubations of marine sediments – specifically, looking for responses of systemic nitrogen cycling to increased availability of Mn oxides – mostly focused on reactivity of solid phase Mn (III/IV) oxides (Bartlett et al., 2007; Lin and Taillefert, 2014). Accumulation of  $\text{NO}_3^-$  and/or  $\text{NO}_2^-$  has been reported from anoxic lab incubations of Mn-rich surface sediments and sediments amended with



various Mn oxides (Hulth et al., 1999; Bartlett et al., 2007). While it was suggested that differences in Mn mineral structure (e.g., phase, defects, composition, see Luther et al., 2018) could underlie variability among different environmental systems in results, it is unclear whether products of Mn reduction, which could include Mn(III)-ligand bound forms, may have played a role in the observed dynamics.

Interestingly, evidence for the oxidative ‘recycling’ of  $\text{NO}_2^-$  back to  $\text{NO}_3^-$  in low oxygen systems has been mounting, in both marine and terrestrial systems (Casciotti, 2016; Granger and Wankel, 2016). In low oxygen marine systems, including oxygen deficient zones (ODZs) and porewaters, nitrate N and O isotope data have consistently required substantial re-oxidative fluxes of  $\text{NO}_2^-$  to  $\text{NO}_3^-$ , albeit under low  $\text{O}_2$  conditions (Sigman et al., 2005; Casciotti and McIlvin, 2007; Gaye et al., 2013; Buchwald et al., 2018). The mechanism of this apparently large back-flux has remained enigmatic. Intriguingly,  $^{15}\text{N}$ -label rate measurements of nitrite oxidation in these systems have also indicated nitrite oxidation under very low  $\text{O}_2$  (Füssel et al., 2012; Beman et al., 2013; Sun et al., 2017; Babbín et al., in press), although some preservation approaches may induce potential artifacts (Ostrom et al., 2016). In parallel to these observational studies, multi-process multi-isotope modeling studies have also consistently concluded that substantial conversion of  $\text{NO}_2^-$  to  $\text{NO}_3^-$  under anoxic conditions is needed to explain dynamics observed in redox transition zones of ODZs, marine porewaters and groundwater (Casciotti, 2016; Granger and Wankel, 2016; Buchwald et al., 2018;). While our data cannot directly implicate the occurrence of abiotic N transformations in the environment, it is intriguing to consider the possible role of Mn(III)-L in driving some of this purported  $\text{NO}_2^-$  oxidation under low oxygen conditions. In freshwater systems, where pH is often  $<7$  and levels of dissolved metals are elevated, a possible role for Mn-based  $\text{NO}_2^-$  oxidation seems particularly feasible. In the absence of  $\text{O}_2$ , this mechanism provides an abiotic avenue for active  $\text{NO}_2^-$  reoxidation – promoting coupled biotic/abiotic cycling between  $\text{NO}_3^-$  and  $\text{NO}_2^-$  as suggested by modeling studies (Granger and Wankel, 2016). Reports of anoxic nitrification in soils and sediments may also reflect such a unique biotic/abiotic coupling. In comparison, marine redox transition zones exhibit higher pH and lower levels of dissolved metals (Landing and Bruland, 1987; Lewis and Landing, 1991; Lewis and Luther, 2000; Nameroff et al., 2002; Moffett et al., 2007; Kondo and Moffett, 2015). Under these conditions, oxidation of  $\text{NO}_2^-$  by Mn(III)-L is likely to be much slower. Speciation of Mn (including Mn(III)) in oxygen deficient

zones (ODZs) has not been widely examined, with only a few studies examining coincident N cycling features. Notably, Mn(III) was implicated as a controlling factor in fluxes of phosphorus within the redoxcline of the Black Sea through formation of Mn(III)-pyrophosphate complexes with proposed concentrations of ca. 50 nM within the suboxic zone (Dijkstra et al., 2018). Additionally Trouwborst et al. (2006) reported Mn(III)-L concentrations in the Black Sea up to 5  $\mu$ M. Interestingly, reported maxima in dissolved Mn in the Arabian Sea ODZ were always highly correlated with secondary nitrite maxima (Lewis and Luther, 2000) – a zone coinciding with active  $\text{NO}_2^-$  turnover in the absence of oxygen (Füssel et al., 2012; Beman et al., 2013; Sun et al., 2017). Future examination of such interactions seems duly warranted.

## 2.5 Summary

We demonstrate that a Mn(III)-L complex can facilitate abiotic  $\text{NO}_2^-$  oxidation under a wide range of environment conditions relevant to freshwater, marine, and sedimentary environments. We characterized the kinetics and N- and O- stable isotope systematics of Mn(III)-PP reaction with nitrite. The overall reaction is second order with respect to Mn(III)-PP, and first order with respect to both nitrite and  $\text{H}^+$ . An inverse nitrogen isotope effect of  $-19.9 \pm 0.7\%$  was observed between the product nitrate and the reactant nitrite. While inverse isotope effects such as the one we measured here are not common in kinetically-controlled reactions, it is similar in direction and magnitude to its biological analog in nitrification. The overall similarity in reaction rates and stable isotope effects of nitrite oxidation by Mn(III)-L complexes and by biologically-mediated nitrification demands further consideration of the relative importance of abiotic processes involving Mn(III)-L complexes in local nitrogen cycling.

Intriguingly, Mn(III)-PP oxidation of  $\text{NO}_2^-$  is insensitive to oxygen concentration, raising the possibility of an abiotic analog to nitrification under oxygen-poor conditions. Although Mn has long been implicated as an important player in suboxic and anoxic redox transformations, the consideration of Mn(III)-L complexes offers an additional avenue of inquiry that provides a greater mechanistic understanding for N-redox cycling in functionally anoxic environments and environments in which redox gradients facilitate interactions between Mn- and N- species of intermediate valence. Although Mn(III)-L complexes are widespread in natural waters, there is very little known about the diversity of Mn-binding ligands, including their composition, origin,

and binding strength. These are all critical factors in ultimately determining the environmental conditions under which Mn(III)-L complexes facilitate N redox reactions. In any case, interactions between Mn(III)-L complexes and nitrite are a potentially critical missing link in understanding local nitrogen budgets, the ultimate fate of these two important electron acceptors, and the energetic limits of life in the absence of oxygen.

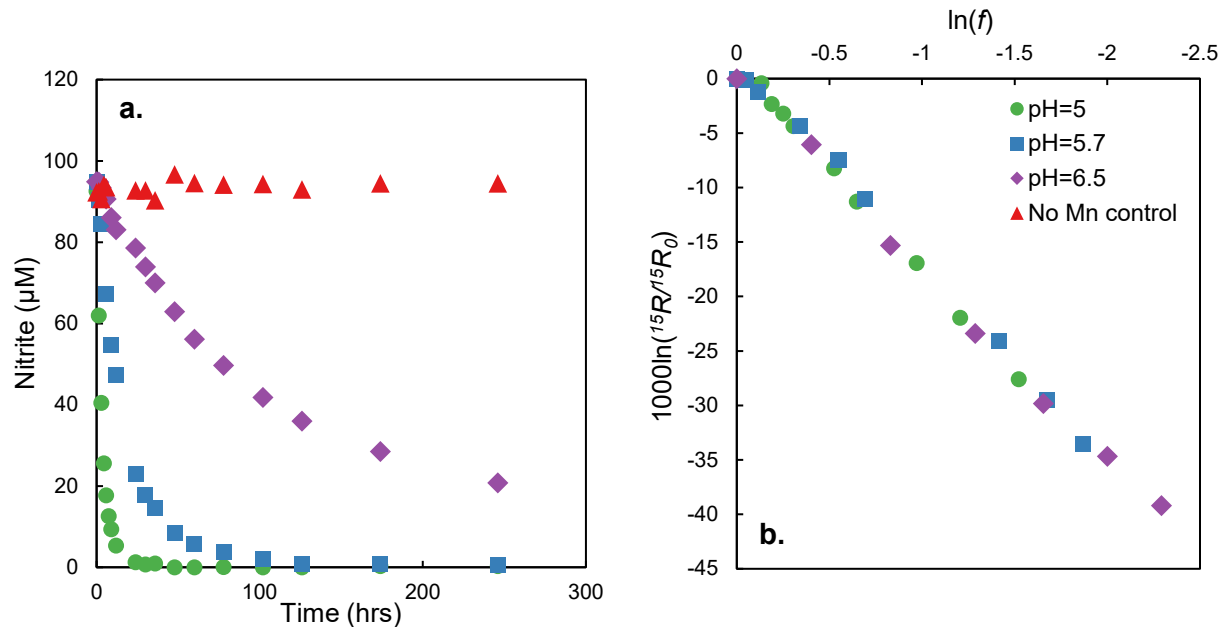


Figure 1. Nitrite concentration (a.) and closed-system Rayleigh distillation of  $\delta^{15}\text{N-NO}_2^-$  (b.) over the course of a timeseries experiment. Data points represent the average of four replicates with standard deviations smaller than the points. Higher pH treatments reacted more slowly and no measureable change in nitrite was observed in a no Mn addition control. Slope of  $\ln([\text{NO}_2^-])$  vs.  $\ln(^{15}R)$  was used to calculate  $^{15}\epsilon_{\text{NXR,MnIII}}$ , but are plotted here as  $\ln(f)$  vs.  $1000\ln(^{15}R/^{15}R_0)$ .

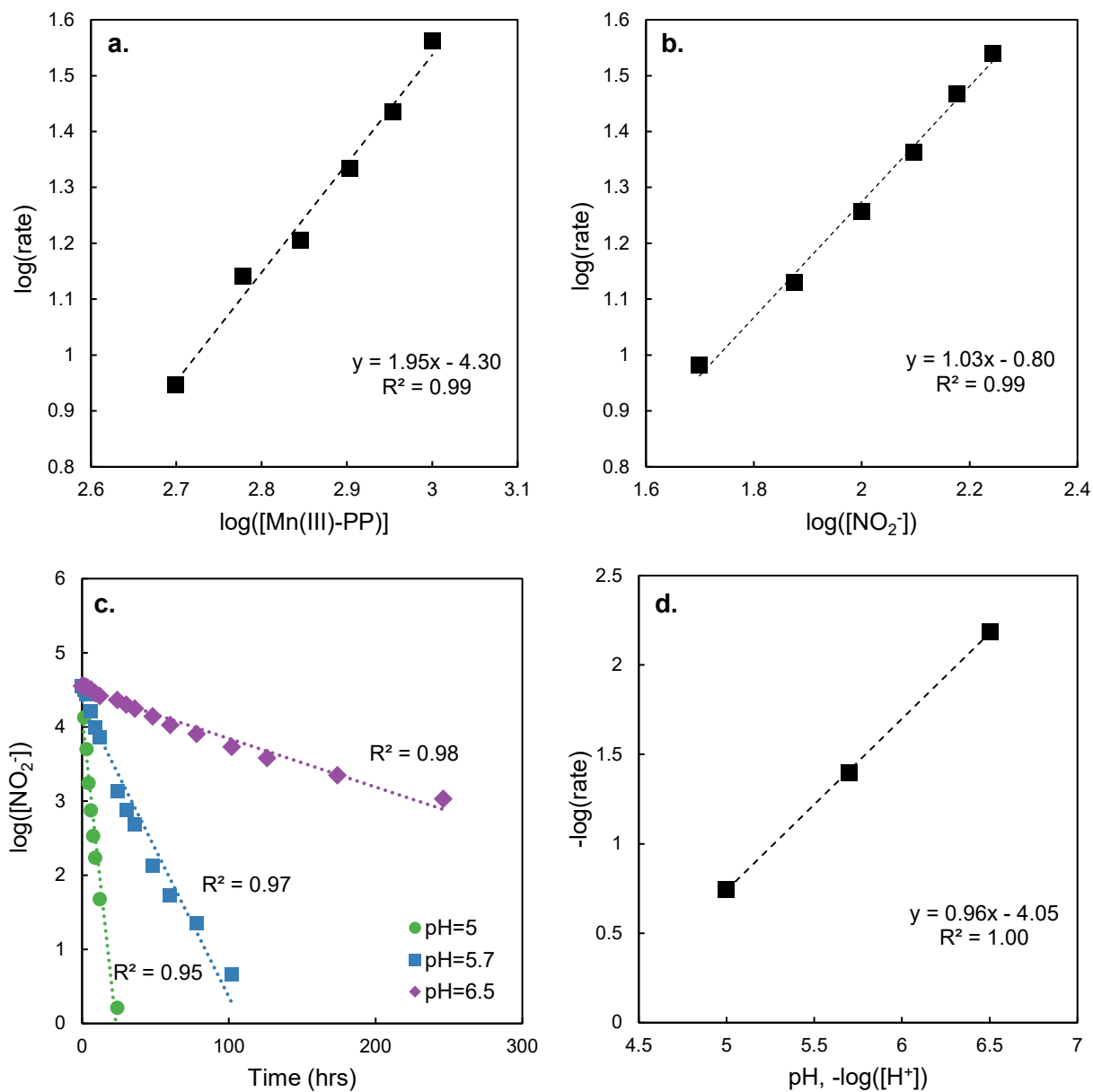


Figure 2. Log(rate) vs.  $\log([\text{Mn(III)-PP}])$  (a.),  $\log([\text{NO}_2^-])$  (b.), and  $-\log([\text{H}^+])$  (d.). Slope of linear regression represents the order of reaction with respect to that reactant, thus the reaction is second order in Mn(III)-PP and first order in  $\text{NO}_2^-$  and  $\text{H}^+$ .

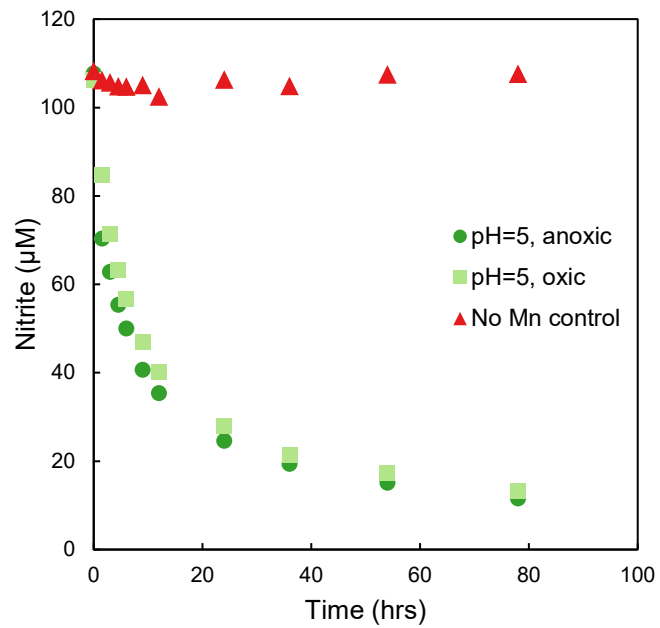


Figure 3. Time course of nitrite concentration at pH=5. No significant difference in rate was observed between air and N<sub>2</sub>-purged headspace treatments. A control treatment with no Mn addition showed no significant decrease in nitrite.

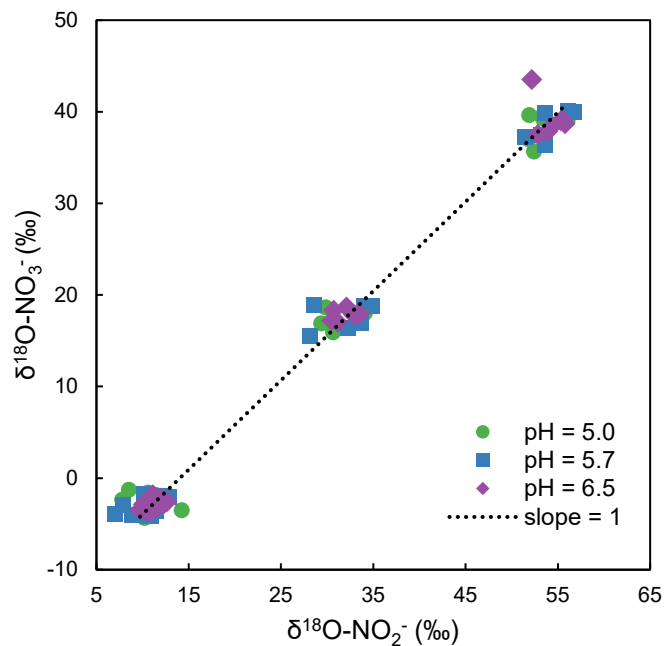


Figure 4.  $\delta^{18}\text{O-NO}_3^-$  produced from  $\text{NO}_2^-$  equilibrated with different  $^{18}\text{O}$ -labeled  $\text{H}_2\text{O}$  samples. Slopes of best-fit lines were indistinguishable from a 1:1 line for all three pH treatments. Intercepts of the linear regressions were used to calculate  $^{18}\epsilon_{k,\text{H}_2\text{O}}$ , as shown in Table 3.

Table 1: Summary of isotope effects for nitrite oxidation by Mn(III)-PP ( $^{15}\epsilon_{\text{NXR, Mn(III)}}$ ).

pH	Mn(III)-PP ( $\mu\text{M}$ )	$\text{NO}_2^-$ ( $\mu\text{M}$ )	Headspace	$^{15}\text{NO}_3^-$ ( $\mu\text{M}$ )	$^{15}\epsilon_{\text{NXR, Mn(III)}}$ ( $\text{\textperthousand}$ )		
5.0	1000	100	Air	–	–19.1	$\pm$	0.5
5.7	1000	100	Air	–	–18.2	$\pm$	0.4
5.0	1000	100	Air	–	–20.3	$\pm$	0.3
5.0	900	100	Air	–	–20.2	$\pm$	0.3
5.0	800	100	Air	–	–19.9	$\pm$	0.3
5.0	700	100	Air	–	–20.1	$\pm$	0.4
5.0	600	100	Air	–	–20.1	$\pm$	0.4
5.0	500	100	Air	–	–19.6	$\pm$	0.5
5.0	1000	50	Air	–	–19.8	$\pm$	0.3
5.0	1000	75	Air	–	–20.6	$\pm$	0.2
5.0	1000	100	Air	–	–19.6	$\pm$	0.5
5.0	1000	125	Air	–	–19.9	$\pm$	0.2
5.0	1000	150	Air	–	–20.2	$\pm$	0.2
5.0	1000	175	Air	–	–19.9	$\pm$	0.2
5.0	1000	100	N <sub>2</sub> -purged	–	–19.8	$\pm$	0.3
5.0	1000	100	Air	–	–20.1	$\pm$	0.1
5.0	1000	100	Air	10	–19.6	$\pm$	0.6
5.0	1000	100	Air	100	–19.4	$\pm$	0.3
5.7	1000	100	Air	10	–19.2	$\pm$	0.4
5.7	1000	100	Air	100	–20.5	$\pm$	0.2

Table 2: Rates of nitrite oxidation and rate constants, pH = 5.0–8.0.

pH	Nitrite oxidation rate			Rate constant ( $k_{\text{pH}}$ )		
	$\mu\text{M d}^{-1}$			$\mu\text{M}^{-2} \text{hr}^{-1}$		
5.0	518.4	$\pm$	16.8	2.16E–07	$\pm$	7.00E–09
5.7	108	$\pm$	4.8	4.50E–08	$\pm$	2.00E–09
6.5	21.6	$\pm$	2.4	9.00E–09	$\pm$	1.00E–09
7.0	5.8	$\pm$	1.3	2.40E–11	$\pm$	5.38E–10
8.0	3.9	$\pm$	0.6	1.62E–11	$\pm$	2.33E–10

Table 3: Results from  $^{18}\text{O}$ -labeled water experiments.

pH	$\delta^{18}\text{O}\text{-H}_2\text{O}$ ( $\text{\textperthousand}$ )	Headspace	Slope $\delta^{18}\text{O}$ ( $\text{NO}_2^-$ vs $\text{NO}_3^-$ )	Intercept $^{18}\epsilon_{\text{k,H}_2\text{O}}$ ( $\text{\textperthousand}$ )
5.0	–5	Air	$0.95 \pm 0.03$ ( $r^2 = 0.988$ )	$+20.5 \pm 0.8$
5.0	18	Air		
5.0	40	Air		
5.0	–5	N <sub>2</sub> -purged		
5.7	–5	Air	$0.94 \pm 0.02$ ( $r^2 = 0.991$ )	$+20.2 \pm 0.8$
5.7	18	Air		
5.7	40	Air		
5.7	–5	N <sub>2</sub> -purged		
6.5	–5	Air	$0.97 \pm 0.03$ ( $r^2 = 0.992$ )	$+22.5 \pm 0.4$
6.5	18	Air		
6.5	40	Air		
6.5	–5	N <sub>2</sub> -purged		



Table 4: Theoretical rates of nitrite oxidation under environmentally relevant conditions.

pH	[Mn(III)PP] μM	[NO <sub>2</sub> <sup>-</sup> ] μM	Oxidation Rate nM d <sup>-1</sup>
6.0	10	10	0.6
6.0	50	10	14.2
6.0	100	10	56.9
6.5	10	10	0.2
6.5	50	10	5.4
6.5	100	10	21.6
7.0	10	10	5.8E-04
7.0	50	10	1.4E-02
7.0	100	10	5.8E-02

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### 3. Abiotic production of nitrous oxide from hydroxylamine and ligand-bound manganese(III)

#### Abstract

Nitrous oxide ( $\text{N}_2\text{O}$ ) is a potent greenhouse gas whose main source in the ocean has historically been attributed to biological reactions. Here, we report the abiotic reaction of a biologically derived nitrogen cycle intermediate hydroxylamine ( $\text{NH}_2\text{OH}$ ) with manganese(III)-pyrophosphate ( $\text{Mn(III)-PP}$ ) which rapidly produces  $\text{N}_2\text{O}$  under environmental conditions. The concentration of  $\text{N}_2\text{O}$  formed following the addition of hydroxylamine ( $10 \mu\text{M}$ ) to solutions of  $[\text{Mn(III)-PP}] = 5 - 80 \mu\text{M}$  was quantified. At lower concentrations of  $\text{Mn(III)-PP}$ , a small amount of nitrite ( $\text{NO}_2^-$ ) was formed in addition to  $\text{N}_2\text{O}$ . Approximately 30-60% of the product remained uncharacterized but is posited to be  $\text{N}_2$ . The formation of  $\text{N}_2\text{O}$  was found not to be a result from back reaction of product  $\text{NO}_2^-$  with reactant  $\text{NH}_2\text{OH}$ ; in other words, it was not due to the combination of two different nitrogen species or “hybrid” formation. During all experiments, the  $\text{N}_2\text{O}$  site preference (SP) of  $+35.5 \pm 0.6\%$  was consistent, and identical to those of  $\text{N}_2\text{O}$  produced by marine nitrifying microorganisms. As  $\text{NH}_2\text{OH}$  is known to leak from nitrifying cells, this suggests that abiotic oxidation of hydroxylamine may be occurring unnoticed in the environment or could be a source of  $\text{N}_2\text{O}$  emissions previously attributed solely to biological nitrification reactions.

#### 3.1 Introduction

Nitrous oxide ( $\text{N}_2\text{O}$ ) is a greenhouse gas with 300 times the warming potential of  $\text{CO}_2$  over its 100-year lifetime in the atmosphere (Myhre et al. 2014; Prather et al. 2012). Additionally,  $\text{N}_2\text{O}$  is implicated in the destruction of stratospheric ozone and has been predicted to be the dominant ozone-depleting substance of the 21st century (Ravishankara et al. 2009). Nitrous oxide concentrations in the atmosphere have been increasing since the industrial revolution and this increase has begun to accelerate (Park et al. 2012; Thompson et al. 2019). The majority of  $\text{N}_2\text{O}$  flux to the atmosphere originates from terrestrial sources with an estimated ~20% coming from the ocean (Ji et al. 2018).

Traditionally  $\text{N}_2\text{O}$  production in the environment has been attributed to biological processes such as nitrification and denitrification (Freing et al. 2012). In contrast to denitrification, in which  $\text{N}_2\text{O}$

is an obligate intermediate, nitrification ( $\text{NH}_3 \rightarrow \text{NO}_2^- \rightarrow \text{NO}_3^-$ ) produces  $\text{N}_2\text{O}$  as a by-product through multiple poorly understood pathways (Soler-Jofra et al. 2021). Generally, the first step of nitrification is performed by either ammonia-oxidizing archaea (AOA) or ammonia-oxidizing bacteria (AOB), while only nitrite-oxidizing bacteria (NOB) have been found to complete the second step of nitrification (Ward 2008). Microbes capable of performing complete nitrification (comammox) have also been found in the environment (Daims et al. 2015; van Kessel et al. 2015). While there remain open questions as to the exact process by which  $\text{N}_2\text{O}$  is produced during nitrification, hydroxylamine ( $\text{NH}_2\text{OH}$ ) has been found to be a biologically produced intermediate of AOA, AOB, and comammox bacteria (Lee 1952, Liu et al. 2017a, Vajjala et al. 2013) and may be a substrate used to enzymatically produce  $\text{N}_2\text{O}$  in AOB (Caranto et al. 2016).

In recent years, increasing evidence has emerged implicating abiotic processes in  $\text{N}_2\text{O}$  production (Doane 2017; Zhu-Barker et al. 2015). Manganese (Mn) in the form of Mn(III,IV) (oxy)(hydr)oxides (hereinafter Mn oxides) has also been linked to production of  $\text{N}_2\text{O}$  both in laboratory experiments (Toyoda et al. 2005; Cavazos et al. 2018) and in soils (Bremner et al. 1980; Duan et al. 2020; Heil et al. 2015a; Liu et al. 2017b; Liu et al. 2019; Rue et al. 2018). While many of these studies assume Mn is in the form of either soluble Mn(II) or solid Mn oxides, in recent years soluble Mn(III) has been shown to be stabilized by ligands and may in fact represent the dominant Mn species in some environments (Madison et al. 2013; Oldham et al. 2015). Manganese (III) ligand complexes (Mn(III)-L) have been previously shown to oxidize iron (II) and sulfide (Kostka et al. 1995) as well as nitrite (Karolewski et al. 2021). Due to the recent appreciation of their abundance in the environment, however, their reactivity remains widely understudied. In this study, we use manganese(III)-pyrophosphate (Mn(III)-PP) as a model Mn(III) compound due to its stability under a wide variety environmental conditions and similar binding affinity when compared to Mn(III) ligands found in natural waters (Qian et al. 2019).

The potential for mixed biotic/abiotic reactions to produce  $\text{N}_2\text{O}$  has also received increased attention. Of particular note are reports that  $\text{N}_2\text{O}$  production from nitrification in culture studies may in fact be an abiotic reaction between biological intermediates such as  $\text{NH}_2\text{OH}$  and oxidized metals present in media (Kits et al. 2019; Kozlowski et al. 2016; Liu et al. 2017a). In light of the complex mix of linked processes known to produce  $\text{N}_2\text{O}$  in the environment, isotopes of nitrogen

( $^{14}\text{N}$ ,  $^{15}\text{N}$ ) and oxygen ( $^{16}\text{O}$ ,  $^{18}\text{O}$ ) have been successfully utilized to help disentangle different processes as both biotic and abiotic reactions can impart distinct isotopic signatures (Baggs 2008; Casciotti 2016; Ostrom and Ostrom 2017; Yu et al. 2008). Stable isotope labeling studies have also revealed a “hybrid” mechanism for  $\text{N}_2\text{O}$  formation by AOA, wherein one N is derived from  $\text{NO}_2^-$  and the other from  $\text{NH}_3$  (in the form of the intermediate  $\text{NH}_2\text{OH}$ ) (Kozlowski et al. 2016; Steiglmeier et al. 2014; Trimmer et al. 2016). Due to the asymmetry of the nitrous oxide molecule (N-N-O), an additional parameter known as site preference (SP) can be calculated using the intramolecular distribution of  $^{15}\text{N}$  (Yoshida and Toyoda 2000). Site preference of  $\text{N}_2\text{O}$  is a particularly powerful tool for tracing potential pathways as it is thought to be independent of substrate composition and reaction progress (Toyoda et al. 2002).

In this thesis chapter we report production of  $\text{N}_2\text{O}$  from an abiotic reaction between hydroxylamine and Mn(III)-PP. Additionally, we characterize the ratio of multiple products produced at a range of different concentrations of Mn(III)-PP and explore  $\text{N}_2\text{O}$  site preference values in the context of other abiotic reactions and culture experiments involving AOA, AOB, and comammox bacteria. Finally, we examine the potential for further reaction of the nitrogen species produced.

## **3.2 Methods**

### *3.2.1 Reagent preparation*

Manganese(III)-pyrophosphate (Mn(III)-PP) was prepared following Madison et al. (2011). Sodium pyrophosphate (5 mM) was dissolved in nitrogen-purged milliQ water and the pH adjusted to 8.0 using 6M hydrochloric acid. Manganese(III)-acetate (final concentration 1 mM) was then added, forming a clear pink solution of Mn(III)-PP (~1 mM). After allowing the solution to rest overnight, it was subsequently 0.2  $\mu\text{m}$  filtered to remove any particulate Mn. Fresh solutions of Mn(III)-PP were prepared monthly. Due to its instability in solution, hydroxylamine solutions were prepared fresh daily from hydroxylamine hydrochloride salt in DI water. Calcium and magnesium-free artificial seawater (ASW) was prepared according to Lyman and Fleming (1940).

### *3.2.2 Isotopic analyses*

Nitrous oxide was purified using a custom purge-and-trap system coupled with a PAL autosampler (McIlvin and Casciotti 2010, Weigand et al. 2016). Gas was then analyzed using an isotope ratio

mass spectrometer (IRMS) (Delta V Plus, Thermo Scientific). A suite of N<sub>2</sub>O gases of known isotopic values were run as standards, including B6, 94321, and S2 (Mohn et al. 2014). Isotope data were corrected using the pyisotopomer software package to calculate size corrections, scrambling coefficients, and isotopomer abundances (Kelly et al. 2023). Concentrations were calculated by comparing the areas of sample N<sub>2</sub>O peaks to areas produced by running standards of known concentration. Isotopic ratios of nitrogen ( $^{15}\text{R} = ^{15}\text{N}/^{14}\text{N}$ ) and oxygen ( $^{18}\text{R} = ^{18}\text{O}/^{16}\text{O}$ ) are reported using the standard delta notation where  $\delta^{15}\text{N} = [(^{15}\text{R}_{\text{sample}}/^{15}\text{R}_{\text{N}_2\text{-ATM}}) - 1] * 1000$  and  $\delta^{18}\text{O} = [(^{18}\text{R}_{\text{sample}}/^{18}\text{R}_{\text{VSMOW}}) - 1] * 1000$ , quantified by measurement of masses 44, 45 and 46. Site preference was calculated by taking the difference in  $\delta^{15}\text{N}$  between the outer ( $\delta^{15}\text{N-N}_2\text{O}^\alpha$ ) and inner ( $\delta^{15}\text{N-N}_2\text{O}^\beta$ ) position nitrogen atoms of N<sub>2</sub>O, quantified by simultaneous measurement of the abundance of mass 31 and 30 in the NO fragment. Reproducibility was generally  $\pm 0.1\%$ ,  $\pm 0.2\%$ , and  $\pm 0.7\%$  for  $\delta^{15}\text{N-N}_2\text{O}$ ,  $\delta^{18}\text{O-N}_2\text{O}$ , and SP, respectively.

Nitrite (NO<sub>2</sub><sup>-</sup>) analyses were performed by conversion to N<sub>2</sub>O using the azide method (McIlvin and Altabet 2005). Briefly, a 50/50 mixture of sodium azide (2 M) and acetic acid (1.7 M) was prepared and purged with N<sub>2</sub> gas. 0.1 mL was added to each vial and allowed to react for 30 minutes before neutralizing with sodium hydroxide (0.1 mL, 6 M). To correct for internal drift and sample size, RSIL-N23, N7373 and N10219 were run as standards on the IRMS alongside samples (Casciotti et al. 2007). Concentration and isotopic analyses of hydroxylamine were completed by conversion to N<sub>2</sub>O using a modified version of the method outlined in Liu et al. 2014. Sulfamic acid (0.5 mL, 5% w/v in water) was added to each bottle to remove any nitrite present, which is known to cause interference. Immediately after, iron(III) chloride (1 mL, 25 mM) was added to convert all hydroxylamine present to N<sub>2</sub>O. The resulting gas was then analyzed on the IRMS as described above. Standards were prepared from solutions of hydroxylamine added to 5 mL of ASW. The denitrifier method was used to determine concentration and isotopic composition of nitrate (Sigman et al. 2001). USGS32, USGS34, and USGS35 (Böhlke et al., 2003) were used as nitrate standards. Approximate precision of nitrite and nitrate measurements was  $\pm 0.1\%$ ,  $\pm 0.2\%$ ,  $\pm 0.2\%$ , and  $\pm 0.3\%$  for  $\delta^{15}\text{N-NO}_2^-$ ,  $\delta^{18}\text{O-NO}_2^-$ ,  $\delta^{15}\text{N-NO}_3^-$ , and  $\delta^{18}\text{O-NO}_3^-$ , respectively.

### 3.2.3 Gibbs free energy calculations

Gibbs free energy calculations were carried out for potential products  $N_2$ ,  $N_2O$ ,  $NO$ ,  $NO_2^-$ , and  $NO_3^-$  using  $\Delta G_f^0$  values from the literature or derived from equilibrium dissociation constants (Luther et al. 2015; Stumm and Morgan 1996; Zhu-Barker et al. 2015). For each reaction  $\Delta G_{exp}$  was calculated using experimental concentrations of reagents ( $[Mn(III)-PP] = 2.5 \mu M$ ,  $[Mn^{2+}] = 2.5 \mu M$ ,  $[PP] = 2.5 \mu M$ ,  $[NH_2OH] = 5 \mu M$ ,  $[N_2O] = 2.5 \mu M$ ,  $[NO] = 5 \mu M$ ,  $[NO_2^-] = 5 \mu M$ ,  $[NO_3^-] = 5 \mu M$ ,  $pH = 8$ ,  $1 \text{ atm } N_2$ ,  $T = 25^\circ C$ ). A range of environmental conditions were also used to generate  $\Delta G_{min}$  and  $\Delta G_{max}$  values ( $[Mn(III)-PP] = 30 - 70 \text{ nM}$ ,  $[Mn^{2+}] = 30 - 70 \text{ nM}$ ,  $[PP] = 100 - 900 \mu M$ ,  $[NH_2OH] = 5 - 20 \text{ nM}$ ,  $[N_2O] = 10 - 200 \text{ nM}$ ,  $[NO] = 50 - 250 \text{ pM}$ ,  $[NO_2^-] = 0.1 - 10 \mu M$ ,  $[NO_3^-] = 1 - 50 \mu M$ ,  $pH = 5 - 8$ ,  $1 \text{ atm } N_2$ ,  $T = 10 - 30^\circ C$ ) (Oldham et al. 2017b; Schweiger et al. 2007; Sundareshwar et al. 2001; Tian et al. 2020).

### 3.2.4 Experimental set-up

Quadruplicate vials of ASW (5 mL in 20 mL Restek crimp-sealed headspace vials with butyl stoppers) were prepared with varying amounts of Mn(III)-PP (5 to 80  $\mu M$ ) and then vigorously purged with  $N_2$  gas for 15 minutes to remove any  $N_2O$ . Hydroxylamine (50  $\mu L$ , 1 mM; final concentration 10  $\mu M$ ) was added to each vial and then allowed to react for 24 hours. As controls, additional vials were prepared containing no  $NH_2OH$  or no Mn(III)-PP. All vials were then analyzed on the IRMS for  $N_2O$ . Half of the vials were subsequently treated with azide to convert any product  $NO_2^-$  to  $N_2O$  and the remaining half with sulfamic acid and  $FeCl_3$  to convert any remaining  $NH_2OH$  to  $N_2O$ . Both sets of headspace vials were then run a second time on the IRMS. Finally, the samples measured for  $NH_2OH$  were returned to neutral pH and injected directly into denitrifier vials to convert any product  $NO_3^-$  present to  $N_2O$  and analyzed on the IRMS. Due to the rapid nature of the reaction (hours), it was assumed that no significant biological activity occurred during experiments. Statistical differences were evaluated using paired t-tests.

## 3.3 Results

### 3.3.1 Concentrations of nitrogen species

Nitrous oxide concentrations were  $1.2 \pm 0.1 \mu M$  at Mn(III)-PP = 5  $\mu M$  and increased rapidly before reaching a maximum of  $3.4 \pm 0.3 \mu M$  at Mn(III)-PP = 30  $\mu M$  (Figure 4). At higher values of Mn(III)-PP,  $N_2O$  concentrations decreased towards a value of  $1.9 \pm 0.2 \mu M$  at the highest addition

of Mn(III)-PP (80  $\mu\text{M}$ ) . Between 5 and 20  $\mu\text{M}$  Mn(III)-PP,  $\text{NO}_2^-$  concentrations were  $1 \pm 0.1 \mu\text{M}$ , but then decreased to zero at 40  $\mu\text{M}$  Mn(III)-PP and were similarly undetectable at higher values of Mn(III)-PP (Figure 5). Concentrations of the remaining hydroxylamine were  $2.2 \pm 0.4 \mu\text{M}$  at Mn(III)-PP = 5  $\mu\text{M}$  and decreased rapidly to near zero by Mn(III)-PP = 15  $\mu\text{M}$  (Figure 6). Controls with no added Mn(III)-PP had  $5.6 \pm 0.9 \mu\text{M}$  of  $\text{NH}_2\text{OH}$  remaining,  $0.23 \pm 0.5 \mu\text{M}$   $\text{N}_2\text{O}$ , and  $1.0 \pm 0.01 \mu\text{M}$   $\text{NO}_2^-$ . Controls with no added  $\text{NH}_2\text{OH}$  had no detectable  $\text{N}_2\text{O}$  or  $\text{NH}_2\text{OH}$  and  $\text{NO}_2^-$  concentrations that were comparable to that of reagent blanks ( $<0.1 \mu\text{M}$ ). Due to trace amounts of  $\text{NO}_3^-$  contamination in the ASW matrix,  $\text{NO}_3^-$  concentration measurements had a large blank ( $\sim 2 \mu\text{M}$ ). No samples or controls had concentrations detectable above the blank. Between 28 and 60% of N added remained unaccounted for (Figure 3).

### 3.3.2 Isotopes of nitrogen species

Isotopes of  $\text{N}_2\text{O}$ ,  $\text{NO}_2^-$ ,  $\text{NH}_2\text{OH}$ , and  $\text{NO}_3^-$  were measured by IRMS as described above. As Mn(III)-PP increased from 5 to 80  $\mu\text{M}$ ,  $\delta^{15}\text{N}_{\text{bulk}}\text{-N}_2\text{O}$  values decreased from  $-6.2 \pm 0.5\text{‰}$  to  $-12.6 \pm 0.2\text{‰}$  and  $\delta^{18}\text{O}\text{-N}_2\text{O}$  values increased from  $+36.2 \pm 0.3\text{‰}$  to  $+44.1 \pm 0.2\text{‰}$  (Figure 4). Site preference values were identical within measurement precision across all Mn(III)-PP treatments with an overall average value of  $+35.2 \pm 0.7\text{‰}$ .  $\delta^{15}\text{N}\text{-NO}_2^-$  values were approximately -25 to -26‰ for Mn(III)-PP additions between 0 and 20  $\mu\text{M}$ . For Mn(III)-PP treatments 25 to 40  $\mu\text{M}$ ,  $\delta^{15}\text{N}\text{-NO}_2^-$  increased before stabilizing at -7 to -8‰ for treatments 40 - 80  $\mu\text{M}$ .  $\delta^{18}\text{O}\text{-NO}_2^-$  increased slightly from  $+20.9 \pm 0.4\text{‰}$  to  $+23.1 \pm 0.2\text{‰}$  between Mn(III)-PP = 5 to 30  $\mu\text{M}$  before decreasing to  $+13.9 \pm 0.4\text{‰}$  at Mn(III)-PP = 80  $\mu\text{M}$  (Figure 5).  $\text{NH}_2\text{OH}$  increased in  $\delta^{15}\text{N}$  from  $-25 \pm 2\text{‰}$  to  $-5.7 \pm 0.6\text{‰}$  between 5 and 80  $\mu\text{M}$  of Mn(III)-PP added (Figure 6). Controls with no added Mn(III)-PP had  $\delta^{15}\text{N}_{\text{bulk}}\text{-N}_2\text{O} = -8.9 \pm 0.6\text{‰}$ ,  $\delta^{18}\text{O}\text{-N}_2\text{O} = +35.4 \pm 0.8\text{‰}$ ,  $\text{SP} = +37.2 \pm 0.7\text{‰}$ ,  $\delta^{15}\text{N}\text{-NO}_2^- = -25 \pm 3\text{‰}$ ,  $\delta^{18}\text{O}\text{-NO}_2^- = +14 \pm 8\text{‰}$ ,  $\delta^{15}\text{N}\text{-NH}_2\text{OH} = -15 \pm 1\text{‰}$ , and  $\delta^{18}\text{O}\text{-NH}_2\text{OH} = +46 \pm 2\text{‰}$ . No significant differences in  $\delta^{15}\text{N}\text{-NO}_3^-$  or  $\delta^{18}\text{O}\text{-NO}_3^-$  were found compared to the blank in any of the samples or controls.

### 3.3.3 Potential reaction of nitrite and hydroxylamine

In order to investigate whether further reaction occurred between product nitrite and reactant hydroxylamine,  $\text{NO}_2^-$  with a distinctly low isotopic signature ( $\delta^{15}\text{N} = -79.6\text{‰}$ , 4  $\mu\text{M}$ ) was added at the beginning of an additional 24 hr experiment in addition to  $\text{NH}_2\text{OH}$  (10  $\mu\text{M}$ ). Concentrations

and isotopes of nitrogen species were measured as described above. Relative to experiments without added nitrite, no significant differences were detected in either the concentration ( $p = 0.21$ ),  $\delta^{15}\text{N}_{\text{bulk}}$  ( $p = 0.39$ ), or SP ( $p = 0.13$ ) of  $\text{N}_2\text{O}$  produced. Differences in hydroxylamine concentrations also remained unchanged relative to the control ( $p = 0.31$ ).

### 3.3.4 Timeseries

To assess reaction kinetics, multiple reaction vials were prepared as described above and immediately sampled in sequence using the autosampler of the IRMS to generate a timeseries of  $\text{N}_2\text{O}$  production (Figure 7). The time between samples was 10 minutes. Three concentrations of Mn(III)-PP were used: 10, 30, and 50  $\mu\text{M}$ . In the timeseries where Mn(III)-PP = 10  $\mu\text{M}$ ,  $\text{N}_2\text{O}$  concentrations rose rapidly to  $1.34 \pm 0.06 \mu\text{M}$  and remained stable after 50 minutes.  $\delta^{15}\text{N}_{\text{bulk}}-\text{N}_2\text{O}$  fell slightly from  $-2.0\text{‰}$  to  $-3.0\text{‰}$  while  $\delta^{18}\text{O}-\text{N}_2\text{O}$  was constant at  $+34.5 \pm 0.2\text{‰}$ . The site preference had no significant change through the timeseries and averaged  $+35.8 \pm 0.4\text{‰}$  across 18 samples. In the Mn(III)-PP = 30  $\mu\text{M}$  treatment, the concentration of  $\text{N}_2\text{O}$  similarly rose rapidly to  $\sim 3 \mu\text{M}$  in the first 70 minutes and then increased slowly to  $3.25 \pm 0.03 \mu\text{M}$  by the end of the experiment (9.5 hrs). Similarly, the site preference was constant at  $+35.3 \pm 0.5\text{‰}$  ( $n=19$ ).  $\delta^{15}\text{N}_{\text{bulk}}-\text{N}_2\text{O}$  fell from  $-7.0\text{‰}$  to  $-12.1\text{‰}$  while  $\delta^{18}\text{O}-\text{N}_2\text{O}$  rose from  $+36.7\text{‰}$  to  $+40.8\text{‰}$  (Figure 7). When Mn(III)-PP was increased to 50  $\mu\text{M}$ ,  $\text{N}_2\text{O}$  concentration remained fairly constant at  $1.0 \pm 0.2 \mu\text{M}$  throughout the timeseries with SP =  $+36.3 \pm 0.3\text{‰}$  ( $n=8$ ). There was no clear trend in  $\delta^{15}\text{N}_{\text{bulk}}-\text{N}_2\text{O}$  or  $\delta^{18}\text{O}-\text{N}_2\text{O}$  which were  $-16 \pm 1\text{‰}$  and  $+49 \pm 2\text{‰}$  respectively.

### 3.3.5 Gibbs free energy calculations

Results of Gibbs free energy calculations are listed in Table 1 and ranged from  $-477$  to  $-832$  kJ/mol at experimental conditions and  $-374$  to  $-802$  kJ/mol at environmental conditions. All values were negative, indicating favorable forward reactions.

## 3.4 Discussion

Our data demonstrate that hydroxylamine ( $\text{NH}_2\text{OH}$ ) and Mn(III)-PP react rapidly in artificial seawater to form nitrite ( $\text{NO}_2^-$ ), nitrous oxide ( $\text{N}_2\text{O}$ ), and a third product, presumed to be dinitrogen gas ( $\text{N}_2$ ). Nitrous oxide is formed from two hydroxylamine molecules and is not the product of nitrite reacting with hydroxylamine, nor does nitrous oxide continue reacting to dinitrogen. The

proportion of these products varies based on the starting stoichiometry of the two reactants, with the maximum amount of N<sub>2</sub>O formed at 3:1 Mn(III)-PP:NH<sub>2</sub>OH. This N<sub>2</sub>O has an isotopic site preference signature identical to that of N<sub>2</sub>O produced by nitrifying organisms including AOA, AOB, and comammox bacteria; therefore leakage of NH<sub>2</sub>OH from cells in the environment could theoretically be oxidized by Mn(III)-L compounds producing N<sub>2</sub>O through an as yet unnoticed mixed biotic-abiotic process (Kits et al. 2019).

### 3.4.1 Isotopic signature of N<sub>2</sub>O

Stable isotopes of N<sub>2</sub>O can be used to provide information about its abiotic and/or biotic sources. Of particular interest to this study is the intramolecular site preference (SP), calculated as the difference in  $\delta^{15}\text{N}$  between the central N ( $\delta^{15}\text{N}_\alpha\text{-N}_2\text{O}$ ) and the outer N ( $\delta^{15}\text{N}_\beta\text{-N}_2\text{O}$ ) (Yoshida and Toyoda 2000). Site preference is a particularly powerful tool as it is thought to arise independent of the isotopic composition of the substrate and reaction progress, thus providing a consistent “fingerprint” for a given process (Toyoda et al. 2002).

In this study, we measured consistent SP values of  $+35.5 \pm 0.6\text{‰}$  across all experiments ( $n = 97$ ), which are similar to values reported for other abiotic reactions of NH<sub>2</sub>OH. Toyoda et al. (2005) reported a SP =  $+29.5 \pm 1.1\text{‰}$  for the reaction of NH<sub>2</sub>OH with MnO<sub>2</sub>. While the exact reactants are unclear, Wunderlin et al. (2013) measured a SP of  $+30.3 \pm 0.2\text{‰}$  when combining NH<sub>2</sub>OH with tap water. Heil et al. (2014) performed experiments combining NH<sub>2</sub>OH with NO<sub>2</sub><sup>-</sup>, Fe<sup>3+</sup>, and Cu<sup>2+</sup> at a variety of concentrations and pH conditions and found a SP =  $+33.9\text{‰}$  to  $+35.6\text{‰}$  across all treatments. Studies that document abiotic N<sub>2</sub>O production from other N species have noted more variation in SP, such as Buchwald et al. (2016) who measured SP from 0.4‰ to +26.0‰ and Jones et al. (2015) who measured SP from +10‰ to +22‰ in studies of “chemodenitrification” of NO<sub>2</sub><sup>-</sup> by soluble Fe<sup>2+</sup> and Fe<sup>3+</sup> containing minerals. Grabb et al. (2017) observed a more consistent SP value of  $+26.5\text{‰} \pm 0.8\text{‰}$  emerging from reaction between NO<sub>2</sub><sup>-</sup> and the Fe(II)-Fe(III) oxyhydroxide phase green rust. Generally, the SP values measured in our experiments were consistent with those measured by Heil et al. (2014) and 4 - 5‰ higher than those measured by Toyoda et al. (2005) and Wunderlin et al. (2013).



Interestingly, the SP value reported here is also broadly consistent with several studies of N<sub>2</sub>O production from AOA and AOB (Duan et al. 2017). For instance, Sutka et al. (2006) reported SP values between +32.5‰ and +35.6‰ when providing NH<sub>2</sub>OH to several strains of AOB. Frame and Casciotti (2010) calculated a SP value of +36.3 ± 2.4‰ for N<sub>2</sub>O produced from NH<sub>2</sub>OH by AOB *Nitrosomonas marina*. Yamazaki et al. (2014) isolated the hydroxylamine oxidoreductase (HAO) enzyme from two species of AOB and measured SP values of +36.3 ± 2.3‰ during *in vitro* incubations with hydroxylamine. Enrichments of marine AOA produced N<sub>2</sub>O with SP values of +30.3 ± 2.4‰ (Santoro et al. 2011). Recently discovered comammox bacterium *Nitrospira inopinata* produced N<sub>2</sub>O with SP values of +34.2 ± 1.4‰ through a process the authors hypothesized to be mixed biotic/abiotic (Kits et al. 2019).

Taken together, these similarities in SP are suggestive of a common mechanism of N<sub>2</sub>O production. In abiotic reactions this is often presumed to be *cis*-hyponitrous acid (HO-<sup>14</sup>N=<sup>15</sup>N-OH) with the kinetic isotope effect leading to preferential breaking of the <sup>14</sup>N-O bond and thus enriching the central N (δ<sup>15</sup>N<sub>α</sub>-N<sub>2</sub>O) leading to a positive site preference (Heil et al. 2014). In AOB it is hypothesized that the HAO enzyme either acts on a similar symmetric intermediate or that it binds two NH<sub>2</sub>OH molecules in sequence, with a kinetic preference for binding <sup>14</sup>N-NH<sub>2</sub>OH over <sup>15</sup>N-NH<sub>2</sub>OH leading to cleavage of the <sup>14</sup>N-O bond (Duan et al. 2017; Schreiber et al. 2012). Caranto et al. (2016) reported that the cytochrome P460 enzyme from the AOB *Nitrosomonas europaea*, although not well understood, is capable of direct stoichiometric formation of N<sub>2</sub>O from NH<sub>2</sub>OH under anoxic conditions and posited a similar sequential binding mechanism. We hypothesize that the reaction mechanism for N<sub>2</sub>O production from NH<sub>2</sub>OH and Mn(III)-PP acts through creation of a symmetric intermediate thus leading to a positive site preference due to kinetic preference for breaking the <sup>14</sup>N-O bond. The similarities in SP between this study and several biological studies also suggests that this reaction could be occurring in the environment unnoticed due to the assumption that high SP values are indicative of nitrification, although further study will need to be undertaken to validate this.

### 3.4.2 N<sub>2</sub>O production is not “hybrid”

There are several potential pathways that are capable of transforming hydroxylamine into nitrous oxide: 1. oxidation of NH<sub>2</sub>OH by Fe(III), 2. oxidation of NH<sub>2</sub>OH by O<sub>2</sub> (autoxidation), 3.

disproportionation of  $\text{NH}_2\text{OH}$ , and 4. reaction of  $\text{NH}_2\text{OH}$  with  $\text{HNO}_2$  (Schreiber et al. 2012). Of these, pathways 1 and 2 can be excluded here as there was no Fe(III) present in the matrix and  $\text{O}_2$  was removed during the sparging process. Disproportionation of  $\text{NH}_2\text{OH}$  generally proceeds very slowly at  $\text{pH} = 8$  and is discussed further in 4.4.3 (Bonner et al. 1978). By contrast, reaction of  $\text{NH}_2\text{OH}$  with  $\text{HNO}_2$  is known to proceed rapidly and therefore  $\text{NO}_2^-$  (in equilibrium with  $\text{HNO}_2$ ) formed during biotic or abiotic oxidative pathways could potentially further react with  $\text{NH}_2\text{OH}$  and contribute to production of “hybrid”  $\text{N}_2\text{O}$  from two different N-bearing precursor molecules (Döring and Gehlen 1961).

Hybrid  $\text{N}_2\text{O}$  production from  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  has been reported in the literature, often linked to abiotic reactions with trace metals. Terada et al. (2017) performed experiments using an enrichment of AOB and isotopic labeling which showed ~50% of  $\text{N}_2\text{O}$  production was due to abiotic reaction of  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  ( $\text{pH} = 7.8$ ). However, there was no abiotic production of  $\text{N}_2\text{O}$  when similar experiments were performed in water, indicating the synthetic wastewater matrix (containing trace metals Fe, Mn, Cu, Zn, Ni) catalyzed the reaction. Terada et al. (2017) performed further experiments and concluded that Fe(III) was not involved. Harper et al. (2015), using the same media recipe and pH condition, concluded that Cu(II) catalyzed the formation of  $\text{N}_2\text{O}$  from  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$ . When mimicking reaction conditions found in wastewater treatment plants, Soler-Jofra et al. (2016) found a strong correlation between lower pH and faster rates of abiotic reaction of  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  which they attributed to increasing proportion of  $\text{HNO}_2$ . At the pH treatment closest to that of our study ( $\text{pH} = 7.6$ ) they measured a rate of  $1.4 \mu\text{M/hr}$   $\text{NH}_2\text{OH}$  consumption ( $0.7 \mu\text{M/hr}$   $\text{N}_2\text{O}$  production) upon addition of  $3.9 \text{ mM}$   $\text{NO}_2^-$  to  $21.4 \mu\text{M}$  to  $\text{NH}_2\text{OH}$ . The authors concluded trace metals present in the growth media (Fe, Zn, Co, Mn, Cu, Mo, and Ni) could be responsible for accelerating the rate of reaction (Soler-Jofra et al. 2016). Soler-Jofra et al. (2018) reported comparable levels of  $\text{N}_2\text{O}$  production from AOB *Nitrosomonas europaea* cultures ( $\text{pH} = 7.5$ ) and abiotic controls in which  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  were added to uninoculated media, concluding that observed  $\text{N}_2\text{O}$  production from their culture experiments was due to abiotic reaction between nitrous acid ( $\text{HNO}_2$ ) and  $\text{NH}_2\text{OH}$  potentially also involving metals (Cu, Fe, Mn, Mo, Zn, Co) from the AOB culture media.

Other studies have concluded that the abiotic reaction between  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  may represent a more minor source of  $\text{N}_2\text{O}$  compared to biotic  $\text{N}_2\text{O}$  production. Su et al. (2019a) measured the rate of abiotic reaction of  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  in the presence Fe(II) and Fe(III). Between pH 6 and pH 8, the reaction rate fell from 150 nmol/hr to 18 nmol/hr  $\text{N}_2\text{O}$  production, respectively, again indicating that  $\text{HNO}_2$  concentration controls the formation of  $\text{N}_2\text{O}$ . Overall these abiotic reaction rates were 1-5 orders of magnitude lower than those measured overall in the reactor, accounting for 0.025% to 2.6% of total  $\text{N}_2\text{O}$  production.

In order to investigate the potential for further reaction of product  $\text{NO}_2^-$  with reactant  $\text{NH}_2\text{OH}$ , we performed an experiment in which isotopically distinct  $\text{NO}_2^-$  ( $\delta^{15}\text{N} = -79.6\text{‰}$ ) was added at the beginning of the experiment. If this  $\text{NO}_2^-$  were involved in reactions with  $\text{NH}_2\text{OH}$ , this low  $\delta^{15}\text{N}$  signal would appear in the  $\text{N}_2\text{O}$  pool. If the rate of reaction was high enough, the overall concentration of  $\text{N}_2\text{O}$  would also rise above those documented in the parallel experiment without amended  $\text{NO}_2^-$ . In contrast, we saw no statistically significant difference in either the  $[\text{N}_2\text{O}]$  or  $\delta^{15}\text{N}_{\text{bulk-N}_2\text{O}}$  and thus no evidence of hybrid  $\text{N}_2\text{O}$  production between  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$ . However, it is possible the rate of reaction was too slow to measure with the low concentrations of  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  used, and the short timescale of the experiment compared to those previously described. Using the reaction rates calculated by Su et al. 2019b and comparable reaction conditions to my experiments (pH = 8,  $[\text{NO}_2^-] = 1 \mu\text{M}$ ,  $[\text{NH}_2\text{OH}] = 10 \mu\text{M}$ ) we calculate a rate of  $\text{N}_2\text{O}$  formation on the order of  $10^{-13} \text{ M/hr}$  which results in only 0.01 nM over 24 hours. If we assume no significant fractionation occurs, an addition of 0.01 nM of  $\text{N}_2\text{O}$  with  $\delta^{15}\text{N} \cong -40\text{‰}$  results in changes to the overall  $\delta^{15}\text{N}_{\text{bulk-N}_2\text{O}}$  of  $<0.1\text{‰}$ . Therefore, hybrid  $\text{N}_2\text{O}$  formation can be excluded, as it would be so minor as to be insignificant under the reaction conditions studied here.

### 3.4.3 Towards the closing of nitrogen mass balance

In this study, we simultaneously quantified changes in concentrations of reaction products  $\text{N}_2\text{O}$ ,  $\text{NO}_2^-$ , and  $\text{NO}_3^-$  together with the evolving reactant pool of  $\text{NH}_2\text{OH}$  remaining. However, there remained 30-60% of N unaccounted for when performing a mass balance of the overall reaction. In this section, we discuss potential other products that could account for this “missing” N.

First, we will consider the possibility of further reaction of products  $[\text{N}_2\text{O}]$  and  $[\text{NO}_2^-]$ . As described above, further reaction of  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$  to  $\text{N}_2\text{O}$  must be insignificant under the reaction conditions studied. However, other further reactions must also be considered. For instance,  $\text{NO}_2^-$  has been found to react to  $\text{NO}_3^-$  in the presence of Mn(III)-PP, although the reaction is relatively slow at  $\text{pH} = 8$  (Karolewski et al. 2021). Using the reaction conditions of these experiments ( $\text{pH} = 8$ ,  $[\text{NO}_2^-] = 1 \mu\text{M}$ ,  $[\text{Mn(III)-PP}] = 80 \mu\text{M}$ ) we calculate a rate of  $\text{NO}_3^-$  formation on the order of  $10^{-17} \text{ M/hr}$  which results in negligible  $\text{NO}_3^-$  formation over 24 hours. Even in environments with lower pH this reaction is unlikely to substantially affect  $[\text{NO}_2^-]$ ; for instance, at  $\text{pH} = 5$ , 4 nM/day could be removed which is  $<1\%$  of  $\text{NO}_2^-$  produced. These calculations are also supported by the measurements of  $[\text{NO}_3^-]$  which were undetectable above the blank. Nitrous oxide could also theoretically react with  $\text{Mn}^{2+}$  to form  $\text{N}_2$  and  $\text{MnO}_2$  (ie.  $\text{N}_2\text{O} + \text{Mn}^{2+} + \text{H}_2\text{O} \rightarrow \text{N}_2 + \text{MnO}_2 + 2\text{H}^+$ ) (Cavazos et al. 2018). Notably, however, if  $\text{N}_2\text{O}$  were being both produced and consumed, each process would impart an isotopic signature onto the overall SP of  $\text{N}_2\text{O}$ . However, the SP of  $\text{N}_2\text{O}$  was identical within precision throughout all experiments and did not vary with  $[\text{N}_2\text{O}]$ ,  $[\text{Mn(III)-PP}]$  added, fraction of missing N, or time elapsed during time series experiments. Thus, it is unlikely that there are multiple processes impacting SP of  $\text{N}_2\text{O}$  and further reaction of  $\text{N}_2\text{O}$  can also be ruled out.

In order to assess the thermodynamic viability of various products from the direct redox reaction of Mn(III)-PP and  $\text{NH}_2\text{OH}$ , we calculated the Gibbs free energy of reaction for production of  $\text{N}_2$ ,  $\text{N}_2\text{O}$ ,  $\text{NO}$ ,  $\text{NO}_2^-$ , and  $\text{NO}_3^-$  at both standard state conditions ( $\Delta G^\circ$ ) and relevant reaction conditions ( $\Delta G$ ). For all reactions, the  $\Delta G^\circ$  and  $\Delta G$  were both negative, indicating energetic favorability. As  $[\text{N}_2\text{O}]$ ,  $[\text{NO}_2^-]$ , and  $[\text{NO}_3^-]$  were already quantified during the experimental process, only  $\text{N}_2$  and  $\text{NO}$  remain as viable candidates. Nitric oxide ( $\text{NO}$ ) is a highly reactive free radical unlikely to persist in solution with other redox-active species. Thus, it seems most parsimonious that  $\text{N}_2$  is the likely identity of the missing N, if the reaction is a simple reduction-oxidation. Interestingly, the number of Mn(III)-PP equivalents needed to produce each product did not seem to predict products observed (Table 1; Figure 3). For instance, the production of  $\text{NO}_2^-$  requires 4 Mn(III)-PP molecules per  $\text{NH}_2\text{OH}$  while the production of  $\text{N}_2\text{O}$  requires only 2 Mn(III)-PP molecules per  $\text{NH}_2\text{OH}$ . However, at the lower ratios of Mn(III)-PP to  $\text{NH}_2\text{OH}$ ,  $\text{NO}_2^-$  was formed while at higher ratios

N<sub>2</sub>O was formed. Thus, we were unable to use the stoichiometry of balanced reactions to predict the identity of the missing N.

Because N<sub>2</sub> gas was used to purge vials during these experiments it was not possible to directly measure any production of N<sub>2</sub>. However, within the literature similar reactions have been documented. Dinitrogen gas was predicted as a product (along with N<sub>2</sub>O) when hydroxylamine was oxidized by manganese(III)-bis(salicylalimine) (Salem 1995). Additionally, Mn(II/III) was posited to be the active site of the DnfA enzyme which converts NH<sub>2</sub>OH to N<sub>2</sub> in dirammox heterotrophic bacteria (Hou et al. 2022). If N<sub>2</sub> is in fact the only missing N species, 65-100% of NH<sub>2</sub>OH added would be transformed into non-fixed nitrogen species, therefore potentially removing NH<sub>2</sub>OH from aquatic systems under the tested conditions. If all missing N is produced through disproportionation of NH<sub>2</sub>OH this value is still 52 - 87% (see below). Currently, most models of N cycling assume the biological processes denitrification and anammox are the primary loss terms of fixed N although other studies have shown production of N<sub>2</sub> from trace metals (Doane 2017; Luther et al. 1997; Moraghan and Buresh 1977).

Disproportionation reactions could also account for some of the missing N, likely also producing N<sub>2</sub>. As previously discussed, disproportionation of NH<sub>2</sub>OH generally proceeds slowly at pH = 8. However, it has been shown to be catalyzed by Fe(II) and Fe(III) compounds (Allusetti et al. 2004; Bari et al. 2010). Disproportionation can proceed as  $4\text{NH}_2\text{OH} \rightarrow \text{N}_2\text{O} + 2\text{NH}_3 + 3\text{H}_2\text{O}$  or  $3\text{NH}_2\text{OH} \rightarrow \text{NH}_3 + \text{N}_2 + 3\text{H}_2\text{O}$  (Cisneros et al. 2003). If all N<sub>2</sub>O formation at [Mn(III)-PP] = 30 μM was due to this disproportionation reaction, ~6.7 μM NH<sub>3</sub> would be formed in addition to the 3.4 μM N<sub>2</sub>O (6.7 μM N). However, only 10 μM of N (as NH<sub>2</sub>OH) was added at the beginning of the experiment and therefore cannot account for 6.7 μM NH<sub>3</sub> + 6.7 μM N-N<sub>2</sub>O = 13.4 μM. Similar results are found for all but the lowest (5 μM) and the highest (80 μM) treatments which suggests disproportionation producing N<sub>2</sub>O could only account for a fraction of the N<sub>2</sub>O produced. As the site preference remained consistent across experiments, multiple pathways of N<sub>2</sub>O formation are also unlikely and therefore disproportionation producing N<sub>2</sub>O is likely insignificant. However, disproportionation producing N<sub>2</sub> could account for some or all of the missing N fraction. In this scenario, one-third of the missing N would be in the form of NH<sub>3</sub> and the remaining two-thirds as

N<sub>2</sub>. As previously discussed, neither NH<sub>3</sub> nor N<sub>2</sub> concentrations were measured during these experiments so this possibility cannot be fully ruled out.

When examining the ratios of products in Figure 3, it does appear that there may be a shift in dynamics located at around 30 – 35 μM [Mn(III)-PP] where NO<sub>2</sub><sup>-</sup> is no longer formed, N<sub>2</sub>O begins to decrease, and the fraction of missing N correspondingly increases. It is possible this shift corresponds to disproportionation giving way to redox reactions with Mn(III)-PP as the ratio of Mn(III)-PP to NH<sub>2</sub>OH increases. In this scenario, 2/3 of the missing N would be N<sub>2</sub> at [Mn(III)-PP] < 30 μM and all of the missing N would be N<sub>2</sub> at [Mn(III)-PP] > 30 μM. However, as discussed above, higher ratios of Mn(III)-PP to NH<sub>2</sub>OH did not seem to correlate with the formation of more oxidized products, so it is difficult to determine if this visual trend in product ratio is in fact significant.

#### *3.4.4 Potential environmental relevance*

While this study did not directly measure rates in the environment, production of N<sub>2</sub>O has been correlated with soil Mn content in several previous studies (Heil et al. 2015b; Xu et al. 2022). Due to the relatively recent discovery of Mn(III)-L, no studies measuring N<sub>2</sub>O production from NH<sub>2</sub>OH have measured Mn(III) directly, although many methods used to quantify Mn would also include Mn(III)-L. For instance, Bremner et al. (1980) added NH<sub>2</sub>OH to a suite of sterilized soils containing oxidized Mn and the majority of N was transformed to N<sub>2</sub>O with minor amounts of N<sub>2</sub> production. Other studies similarly found total Mn content in soils was correlated with rapid N<sub>2</sub>O production from addition of NH<sub>2</sub>OH (Heil et al. 2015a; Liu et al. 2017b; Liu et al. 2019). Site preference values of N<sub>2</sub>O produced ranged from +31.4 ± 3.6‰ to +35‰, comparable to the value reported here (+35.5 ± 0.6‰) (Duan et al. 2020; Heil et al. 2015a).

Several studies have also directly studied the impact of solid Mn oxides (MnO<sub>2</sub>) on N<sub>2</sub>O production. Cavazos et al. (2018) performed laboratory experiments that showed rapid production of N<sub>2</sub>O from reaction of the phylломanganate birnessite and NH<sub>2</sub>OH under environmental conditions. Similarly, Rue et al. (2018) reacted NH<sub>2</sub>OH with pyrolusite and poorly crystalline MnO<sub>2</sub>(s) and found 82-86% transformed to N<sub>2</sub>O. Taken together, these studies suggest oxidized mineral forms of Mn also play an important role in transforming NH<sub>2</sub>OH to N<sub>2</sub>O.

Although  $\text{NH}_2\text{OH}$  has been known to accumulate in cultures of AOB, AOA, and comammox bacteria,  $\text{NH}_2\text{OH}$  rarely accumulates to measurable levels in the environment due to its instability and reactivity (Soler-Jofra et al. 2021). However, concentrations up to  $\sim 250$  nM have been measured in coastal seawater with high nitrification activity (Zhu-Barker et al. 2015). Additionally, rapid rates of reaction can prevent the buildup of  $\text{NH}_2\text{OH}$ , but do not preclude high rates of consumption. Due to the relatively recent discovery of the abundance of Mn(III)-L compounds in the environment, measurements are somewhat sparse (Madison et al. 2013; Oldham et al. 2015). Jones et al. (2020) reported a peak of up to 0.5 - 1 nM of Mn(III)-L at the base of the euphotic zone in oxygenated waters of the Northwest Atlantic, coincident with the peak in nitrification rates often observed at this depth (Ward 2008). Oldham et al. (2017a) found a similar peak at the base of the euphotic zone of 0.2 - 0.4  $\mu\text{M}$  Mn(III)-L in both fully oxygenated waters and above anoxic sediments in profiles from St. Lawrence Estuary. Within sediment porewaters, up to 80  $\mu\text{M}$  Mn(III)-L was reported by Madison et al. (2013) with maxima close to the oxic-suboxic interface where nitrification in sediments is similarly high (Ward 2008). While we are not aware of any studies simultaneously measuring  $\text{NH}_2\text{OH}$  and Mn(III)-L concentrations in the environment, these papers suggest several locations where  $\text{NH}_2\text{OH}$  formation and “leakage” by nitrifiers could overlap with regions high in Mn(III)-L. Comparing measurements from two similar estuarine sites with seasonal anoxia,  $\text{NH}_2\text{OH}$  was measured as 5 - 20 nM and Mn(III)-L was 30 - 70 nM (Oldham et al. 2017b; Schweiger et al. 2007). The ratios of Mn(III)-L: $\text{NH}_2\text{OH}$  would be between 1.5 to 14 which are of similar stoichiometric ratios as those used in this study (0.5 to 8). However, both studies note high degrees of temporal variability on the scale of hours to days as is to be expected from highly reactive species. Despite this variability,  $\Delta G$  values calculated at environmental concentrations consistently remained negative, indicating theoretical thermodynamic favorability (Table 1).

The ratio of products observed was highly dependent on the starting stoichiometry, with a peak in  $\text{N}_2\text{O}$  production at  $[\text{Mn(III)-L}] = 30$   $\mu\text{M}$  or a ratio of 3:1 Mn(III)-PP: $\text{NH}_2\text{OH}$ . At lower ratios of Mn(III)-PP, the products have a greater fraction of  $\text{NO}_2^-$  and missing N (presumed to be primarily  $\text{N}_2$ ). At higher ratios, the fraction of  $\text{N}_2\text{O}$  decreases while the presumed  $\text{N}_2$  rises. Thus, in environments higher in Mn(III)-L compounds with fewer nitrifiers releasing  $\text{NH}_2\text{OH}$ , such as in nearly anoxic porewaters, it is more likely that all N undergoing this reaction will be lost as non-

fixed N in the form of  $\text{N}_2\text{O}$  and  $\text{N}_2$ . At ratios between 1.5 and 6 Mn(III)-PP: $\text{NH}_2\text{OH}$ , half or more of the N added will be converted to  $\text{N}_2\text{O}$ . In locations such as open ocean oxygen deficient zones (ODZs), with high  $\text{NH}_2\text{OH}$  and generally lower trace metal contents, relatively more  $\text{NO}_2^-$  could be formed and continue in the nitrification pathway or subsequently be denitrified. If  $\text{NH}_3$  is also being formed through a disproportionation pathway, it could also be “recycled” back into nitrification. Further study will be necessary to determine if this reaction is occurring in the environment and to if so, to what degree.

### 3.5 Conclusion

Here, we have shown that Mn(III)-PP can abiotically oxidize  $\text{NH}_2\text{OH}$  primarily to  $\text{N}_2\text{O}$ , with  $\text{NO}_2^-$  as a secondary product when the ratio of Mn(III)-PP to  $\text{NH}_2\text{OH}$  was less than 4 to 1. Dinitrogen gas and potentially ammonia were presumed to be the remaining percentage of the products, although neither was measured directly. The isotope dynamics of  $^{15}\text{N}$  and  $^{18}\text{O}$  were characterized for both the known products and the reactant. Isotopically distinct  $\text{NO}_2^-$  was used to demonstrate that the formation pathway of  $\text{N}_2\text{O}$  was not a hybrid process between  $\text{NO}_2^-$  and  $\text{NH}_2\text{OH}$ . The site preference of  $\text{N}_2\text{O}$  formed was highly consistent at  $+35.5 \pm 0.6\%$  regardless of reactant ratio or reaction progress, indicating  $\text{N}_2\text{O}$  was likely formed through a symmetric intermediate and through only one production pathway with no further consumption occurring. This SP value is also very close to those reported in multiple studies of AOA, AOB, and comammox bacteria. Although this reaction has yet to be documented in the environment, the similarity in SP values suggests that previous measurements of environmental  $\text{N}_2\text{O}$  could have included abiotic oxidation of  $\text{NH}_2\text{OH}$  by Mn(III)-L while attributing its signature to solely biological nitrification processes. This study supports the hypothesis that abiotic and mixed biotic/abiotic processes potentially could contribute significantly to  $\text{N}_2\text{O}$  emissions and suggests that Mn(III)-L compounds could play an important role in greenhouse gas emissions.



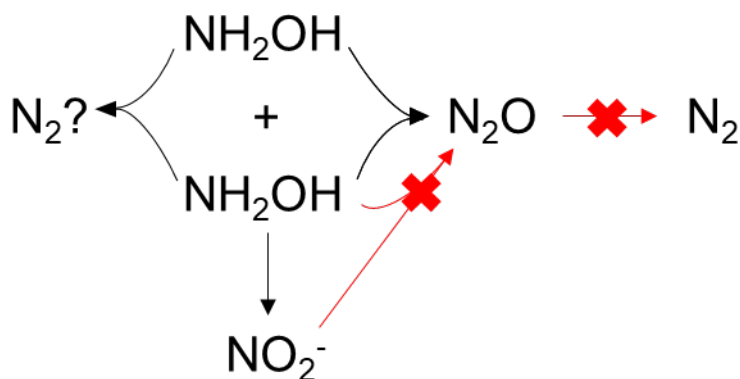


Figure 1: Conceptual diagram illustrating the major reactions occurring in this chapter. Hydroxylamine reacts with Mn(III) pyrophosphate to form nitrous oxide, nitrite, and potentially dinitrogen gas. Two potential reactions were also ruled out during this study, namely “hybrid” formation of nitrous oxide from nitrite and hydroxylamine and reduction of nitrous oxide to dinitrogen by  $\text{Mn}^{2+}$ .

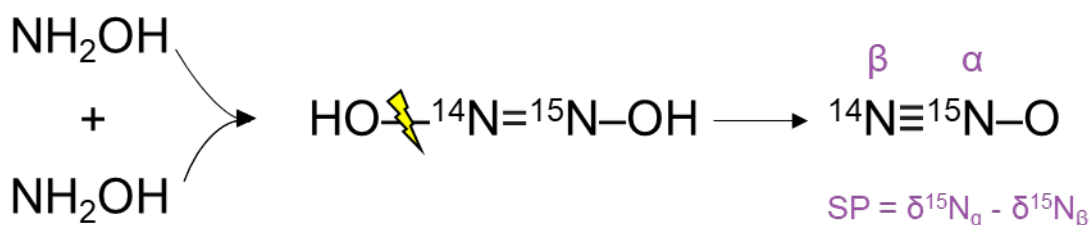


Figure 2: Reaction between two hydroxylamine atoms forms a symmetric intermediate *cis*-hyponitrous acid. Preferential breaking of the  $^{14}\text{N}-\text{O}$  bond and enriches the central N ( $\delta^{15}\text{N}_\alpha$ ) compared to the outer N ( $\delta^{15}\text{N}_\beta$ ) leading to a positive site preference.

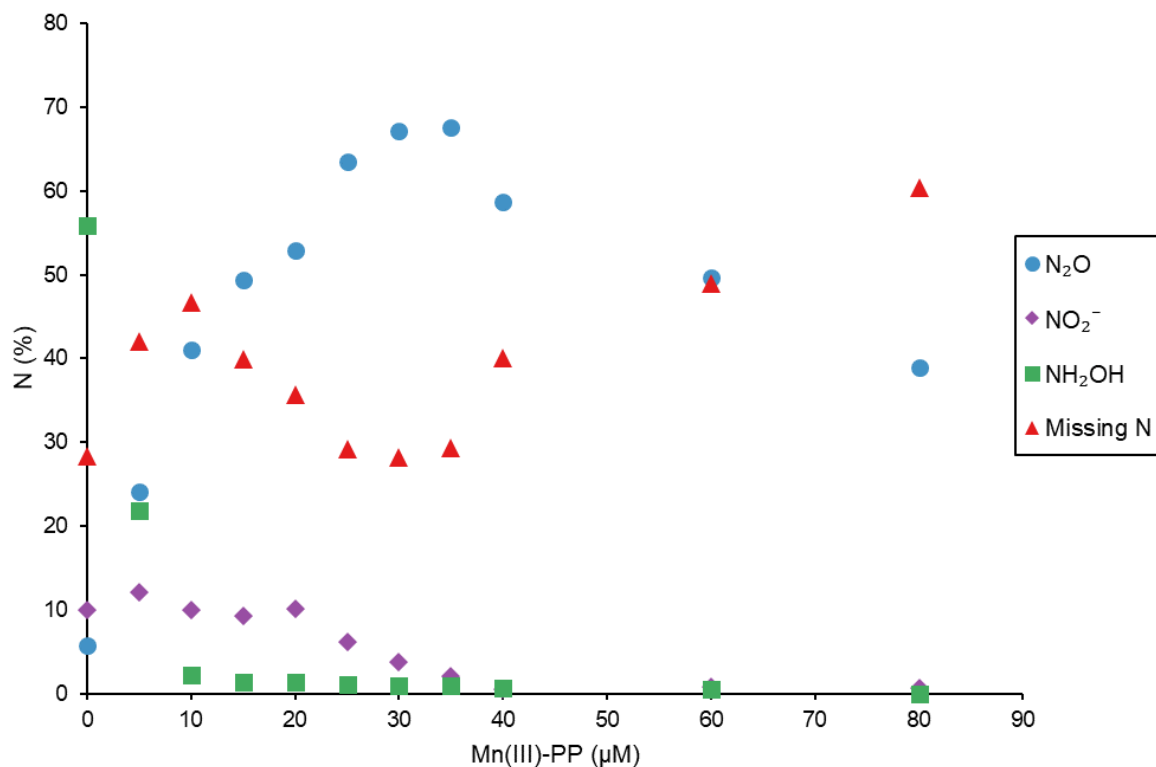


Figure 3: Remaining NH<sub>2</sub>OH and produced NO<sub>2</sub><sup>-</sup>, N<sub>2</sub>O, and missing product (presumed to be N<sub>2</sub>) after 24 hrs. of reaction vs. starting Mn(III)-PP (μM). Values are reported in % of N added.

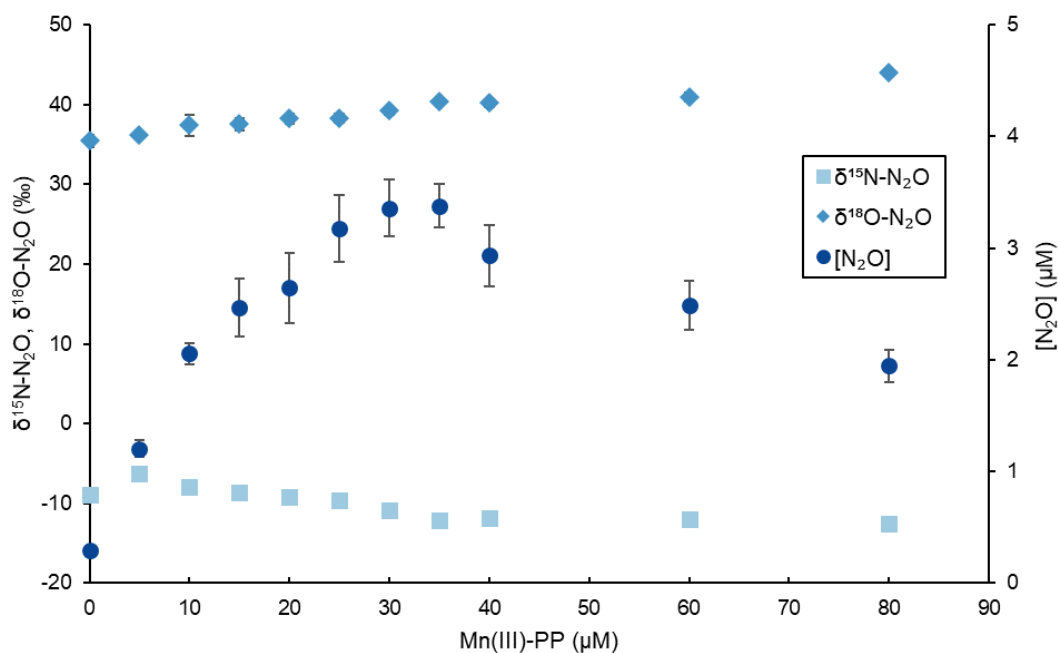


Figure 4: N<sub>2</sub>O produced (μM), δ<sup>15</sup>N-N<sub>2</sub>O, and δ<sup>18</sup>O-N<sub>2</sub>O after 24 hrs. of reaction vs. starting Mn(III)-PP (μM). Starting NH<sub>2</sub>OH was 10 μM and had an initial δ<sup>15</sup>N of -4‰. Error bars represent the standard deviation of measurements (n = 4).

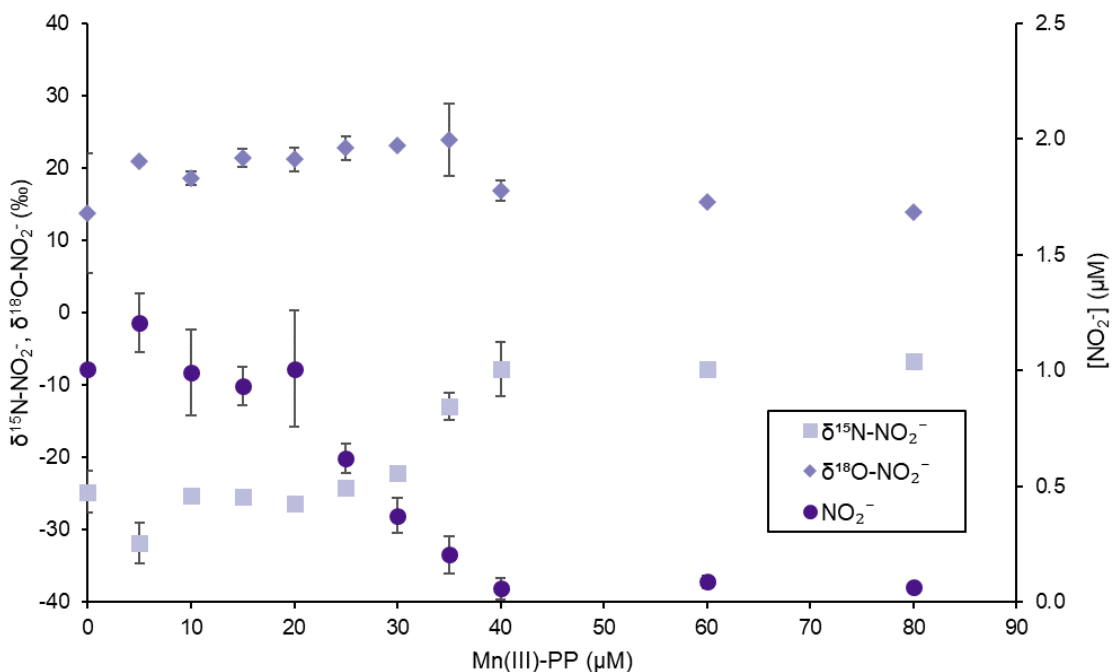


Figure 5:  $\text{NO}_2^-$  produced ( $\mu\text{M}$ ),  $\delta^{15}\text{N-NO}_2^-$ , and  $\delta^{18}\text{O-NO}_2^-$  after 24 hrs. of reaction vs. starting Mn(III)-PP ( $\mu\text{M}$ ). Starting  $\text{NH}_2\text{OH}$  was 10  $\mu\text{M}$  and had an initial  $\delta^{15}\text{N}$  of -4‰. Error bars represent the standard deviation of measurements ( $n = 2$ ).

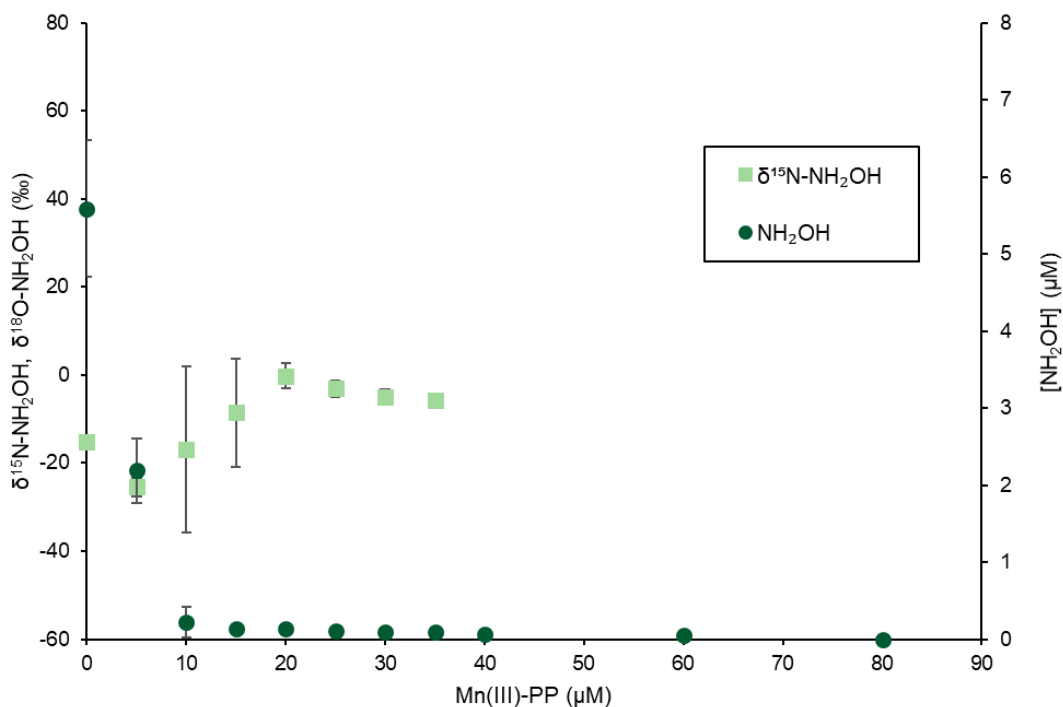


Figure 6:  $\text{NH}_2\text{OH}$  remaining ( $\mu\text{M}$ ) and  $\delta^{15}\text{N-NH}_2\text{OH}$  after 24 hrs. of reaction vs. starting Mn(III)-PP ( $\mu\text{M}$ ). Starting  $\text{NH}_2\text{OH}$  was 10  $\mu\text{M}$  and had an initial  $\delta^{15}\text{N}$  of -4‰. Error bars represent the standard deviation of measurements ( $n = 2$ ).

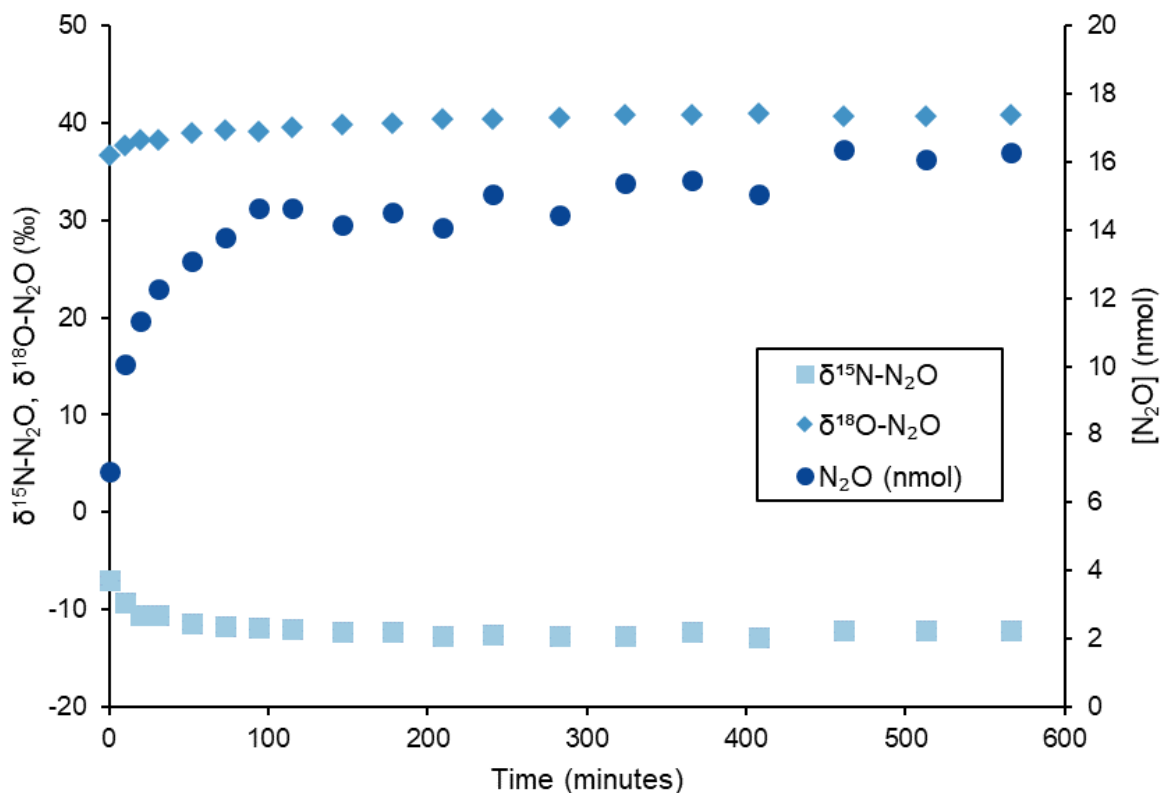


Figure 7:  $\text{N}_2\text{O}$  (nmol),  $\delta^{15}\text{N-N}_2\text{O}$ , and  $\delta^{18}\text{O-N}_2\text{O}$  vs. time in minutes for  $[\text{Mn(III)-PP}] = 30 \mu\text{M}$ . Starting  $\text{NH}_2\text{OH}$  was  $10 \mu\text{M}$  and had an initial  $\delta^{15}\text{N}$  of  $-4\text{‰}$ .

Balanced reaction	$\Delta G_{\text{exp}}$	$\Delta G_{\text{min}}$	$\Delta G_{\text{max}}$
$2\text{Mn(III)-PP} + 2\text{NH}_2\text{OH} \rightarrow 2\text{Mn}^{2+} + \text{N}_2 + 2\text{H}^+ + 2\text{H}_2\text{O} + 2\text{PP}$	-764	-728	-666
$4\text{Mn(III)-PP} + 2\text{NH}_2\text{OH} \rightarrow 4\text{Mn}^{2+} + \text{N}_2\text{O} + 4\text{H}^+ + \text{H}_2\text{O} + 4\text{PP}$	-832	-802	-671
$3\text{Mn(III)-PP} + \text{NH}_2\text{OH} \rightarrow 3\text{Mn}^{2+} + \text{NO} + 3\text{H}^+ + 3\text{PP}$	-477	-472	-374
$4\text{Mn(III)-PP} + \text{NH}_2\text{OH} + \text{H}_2\text{O} \rightarrow 4\text{Mn}^{2+} + \text{NO}_2^- + 5\text{H}^+ + 4\text{PP}$	-600	-563	-431
$6\text{Mn(III)-PP} + \text{NH}_2\text{OH} + 2\text{H}_2\text{O} \rightarrow 6\text{Mn}^{2+} + \text{NO}_3^- + 7\text{H}^+ + 6\text{PP}$	-820	-787	-575

Table 1: Gibbs free energy calculations for reaction conditions from this study ( $\Delta G_{\text{exp}}$ ) and for a variety of environmental conditions ( $\Delta G_{\text{min}}$  and  $\Delta G_{\text{max}}$ ). Experimental reaction conditions were  $[\text{Mn(III)-PP}] = 2.5 \mu\text{M}$ ,  $[\text{Mn}^{2+}] = 2.5 \mu\text{M}$ ,  $[\text{PP}] = 2.5 \mu\text{M}$ ,  $[\text{NH}_2\text{OH}] = 5 \mu\text{M}$ ,  $[\text{N}_2\text{O}] = 2.5 \mu\text{M}$ ,  $[\text{NO}] = 5 \mu\text{M}$ ,  $[\text{NO}_2^-] = 5 \mu\text{M}$ ,  $[\text{NO}_3^-] = 5 \mu\text{M}$ ,  $\text{pH} = 8$ ,  $1 \text{ atm N}_2$ ,  $T = 25^\circ\text{C}$  and the range of environmental reaction conditions were  $[\text{Mn(III)-PP}] = 30 - 70 \text{ nM}$ ,  $[\text{Mn}^{2+}] = 30 - 70 \text{ nM}$ ,  $[\text{PP}] = 100 - 900 \mu\text{M}$ ,  $[\text{NH}_2\text{OH}] = 5 - 20 \text{ nM}$ ,  $[\text{N}_2\text{O}] = 10 - 200 \text{ nM}$ ,  $[\text{NO}] = 50 - 250 \text{ pM}$ ,  $[\text{NO}_2^-] = 0.1 - 10 \mu\text{M}$ ,  $[\text{NO}_3^-] = 1 - 50 \mu\text{M}$ ,  $\text{pH} = 5 - 8$ ,  $1 \text{ atm N}_2$ ,  $T = 10 - 30^\circ\text{C}$ . All values are negative, indicating favorable reactions.

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## 4. Insights into metal-mediated methane oxidation in seep sediments of the Cascadia Margin

### **Abstract**

Anaerobic oxidation of methane (AOM) can be coupled to a variety of electron acceptors including manganese and iron; however, relatively little is understood about how various forms of oxidized metals may impact metal coupled AOM rates. In this chapter, we present a series of cold-seep sediment incubations from Cascadia Margin amended with a diverse range of oxidized manganese and iron species, including different mineral phases and soluble metal-ligand complexes. Rates of AOM were measured by tracking the incorporation of  $^{13}\text{C}$  from labeled methane into the DIC pool over the course of 8.5 months. Overall, rates were comparable to previous studies in similar environments, however, no oxidized metal addition consistently elevated rates of AOM. In fact, many metal species treatments lowered rates below that of the unamended control. We discuss possible explanations for this trend including that coupling of AOM to metal results in greater energy yields per mol of methane or that the microbial community was unable to adapt over the course of the experiment. Despite the overall lower rates of AOM, presumed metal-AOM did appear to occur at rates up to  $13 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$  in incubations containing little to no sulfate.

### **4.1 Introduction**

Methane ( $\text{CH}_4$ ) is a potent greenhouse gas with a projected 28-34 larger global warming potential than that of carbon dioxide ( $\text{CO}_2$ ) on a centennial time scale and is estimated to contribute to about 20% of present global warming (Myhre et al. 2014, Etminan et al. 2016). Despite its climatic relevance, estimates of oceanic contributions to the natural atmospheric methane budget remain limited (Weber et al. 2019). In marine environments, methane is primarily produced in anoxic sediments by methanogenesis. Up to 90% of this seafloor methane is then oxidized to  $\text{CO}_2$  through microbially mediated anaerobic oxidation of methane (AOM) (Knittel and Boetius 2009). Anaerobic oxidation of methane was initially found to proceed through coupling to sulfate reduction (sulfate-AOM) performed by consortia of anaerobic methanotrophic archaea (ANME) and sulfate-reducing bacteria (SRB) (Boetius et al. 2000; Nauhaus et al. 2002); though more recently, nitrate- and nitrite-dependent AOM have also been documented (Ettwig et al. 2010;

Haroon et al. 2013; Raghoebarsing et al. 2006), reflecting a wider range of possible metabolic couplings.

Metal-dependent AOM (metal-AOM) has also been demonstrated, wherein oxidized iron (Fe) or manganese (Mn), in the form of Fe(III) and Mn(IV), may serve as electron acceptors (Fe-AOM or Mn-AOM, respectively) (Beal et al. 2009; Egger et al. 2015; Riedinger et al. 2014; Rooze et al. 2016; Sivan et al. 2011). Generally, metal-AOM has been less studied compared to sulfate-AOM, so evaluation of its distribution and rates in the environment remains poorly constrained. In the marine environment, it has been primarily studied in sediments rich in methane such as those found near cold seeps (Beal et al. 2009) or in other areas with a high degree of spatial overlap between metals and methane (Egger et al. 2015; Riedinger et al. 2014; Segarra et al. 2013; Wankel et al. 2012). In freshwater environments, most reports of AOM have stemmed from studies of metal-rich lake sediments (Crowe et al. 2011; Mostovaya et al. 2021; Norði et al. 2013; Sivan et al. 2011; Torres et al. 2014).

Several studies have compared rates of AOM when incubations are supplemented with Fe(III) oxides (ferrihydrite) or Mn(III,IV) oxides (birnessite), with no clear trend when comparing relative rates, despite thermodynamic evidence that Mn-AOM may be favored under environmental conditions (Beal et al. 2009; Ettwig et al. 2016; Segarra et al. 2013). However, only a few experiments have compared rates of metal-AOM when incubated with different forms of oxidized iron (Ettwig et al. 2016; Li et al. 2021; Scheller et al. 2016) and, to our knowledge, none has compared different forms of Mn oxides. Thus, our study fills a gap in the literature by not only comparing between Fe-AOM and Mn-AOM rates, but also examining relative differences between different forms of oxidized manganese and iron, including soluble desferrioxamine B (DFOB) complexes. In other reactions that reduce iron and manganese, for instance those catalyzed by dissimilatory metal reducing bacteria (DMRB), the chemical form of the metal has been found to impact the reactivity, with poorly crystalline oxides more quickly reduced than crystalline ones, and soluble, ligand-bound species reacting even faster (Lovley et al. 2004; Nealson and Saffarini 1994; Weber et al. 2006). Additionally, higher surface area and reactive site concentrations have been shown to result in faster reactions rates (Roden and Zachara 1996). With manganese minerals, the degree of hydration has been shown to alter the ability to accept electrons and more hydrous

phases are also prone to interacting with soluble anions (Nealson et al. 2002). Therefore, we predicted that addition of different forms of oxidized metals may impact relative rates of AOM.

Here, we present the results from experiments designed to further examine the potential role of oxidized Fe and Mn in anaerobic methane oxidation rates near seafloor cold seeps, with a focus on comparing different minerals as well as soluble ligand bound forms. In addition to AOM rate measurements, we examine changes in Fe and  $\text{SO}_4^{2-}$  concentration over time.

## **4.2 Methods**

### *4.2.1 Study site description*

Sediments were collected at Cascadia Margin, a convergent accretionary margin stretching between the northern tip of Vancouver Island and Cape Mendocino, Northern California where the Juan de Fuca plate under-thrusts the North American plate (Figure 1a, Kulm et al. 1986). Due to the presence of abundant methane hydrates and methane gas trapped within organic-rich sediments, this region hosts numerous active bubble flares (Johnson et al. 2015). Over 3,500 bubble streams, clustered at 1,300 sites have been documented using multibeam sonar surveys along the US Cascadia Margin (Merle et al. 2021). During August and September of 2018, areas of interest for sampling were identified using multibeam surveys aboard R/V *Falkor* and then further examined using ROV *SuBastian* (Schmidt Ocean Institute “Hunting Bubbles” Cruise – FK180824).

### *4.2.2 Experimental setup*

#### **Sediment collection**

Sediments were collected from the vicinity of active methane seepage located along the Cascadia Margin off the coast of Oregon. Two different areas were included in this study: Hydrate Ridge (44.57° N, 125.15° W) and McArthur Canyon (45.85° N, 124.90° W) (Figure 1b). At each location, two sites were selected, one close to active bubble emission and one approximately 20 m away from any visible activity. Sediments were collected using pushcores inserted into selected areas using ROV *SuBastian*.

## Preparation of minerals

The following minerals were synthesized or purchased, in preparation for sediment amendment experiments. Solid manganese treatments included manganite,  $\delta$ -MnO<sub>2</sub>, and birnessite while solid iron treatments included oxide minerals ferrihydrite and goethite, as well as clay mineral nontronite.

Manganite (MnOOH) was synthesized following Larsen et al. (1998). A solution of MnSO<sub>4</sub> (0.06 M, 1000 mL) was continuously stirred while hydrogen peroxide (8.82 M, 20.4 mL) was added, followed by addition of ammonium (0.2 M, 300 mL). The mixture was then brought to a boil on a hotplate and allowed to react for 6 hours before decanting excess supernatant. The resulting material was then washed repeatedly with deionized water and stored suspended in clean deionized water.

$\delta$ -MnO<sub>2</sub> was prepared as described in Villalobos et al. (2003). Potassium permanganate (0.2 M, 1280 mL) was added to sodium hydroxide (0.5 mM, 1440 mL) while stirring. Manganese chloride (0.3 M, 1280 mL) was then added to the mixture over the course of 30 minutes forming a black precipitate. Supernatant was discarded after allowing the solids to settle over the course of several hours. To remove excess hydroxide and salts, the product was repeatedly centrifuged and washed with deionized water until the overlying solvent pH measured circumneutral.

Birnessite was synthesized following previously outlined methods as follows (Mandernack et al. 1995, Golden et al. 1987). Cold sodium hydroxide (6 M, 125 mL) was added to a stirring solution of manganese chloride (0.5 M, 125 mL) while sparging with oxygen using an air stone. The resulting black solution was transferred to an ice bath and sparged for an additional 4 hours. The product was then washed with deionized water until the overlying water pH was neutral, followed by freeze drying to produce a fine black powder.

Ferrihydrite (2-line) was prepared following Schwertmann and Cornell (2000). Potassium hydroxide (0.4 M, ~330 mL) was added slowly to a flask of Fe(NO<sub>3</sub>)<sub>3</sub> · 9H<sub>2</sub>O (0.2 M, 500 mL) while stirring until a stable pH of 7.5 was maintained. The product was washed thoroughly with deionized water to remove electrolytes.

Goethite was synthesized according to Schwertmann and Cornell 2000. Potassium hydroxide (5 M, 180 mL) was added to a flask of  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (1 M, 100 mL) while stirring vigorously. The resulting suspension was diluted with deionized water to a final volume of 2 L and held in a closed flask at 70°C for 60 hours, followed by washing to remove electrolytes.

Nontronite was purchased from the Clay Minerals Society (NAu-2) and has been extensively characterized by Keeling et al. (2000) (37.42%  $\text{Fe}_2\text{O}_3$ , 24.3% Fe)

### **Incubation initiation**

Immediately upon recovery, cores were sealed and refrigerated at 4° C until incubations were initiated. Cores were visually inspected and the top ~5-7 cm sliced and sieved using coarse wire mesh to remove any rocks, carbonates, and other debris. Multiple cores from the same sampling site were homogenized in plastic bags and 2.5 mL of sediment aliquoted into 25 mL Balch tubes. Nutrients (4.7 mM  $\text{NH}_4^+$ , 0.4 mM  $\text{PO}_4^{3-}$ , PRO99 metal mix, F/2 media vitamin mix) were added to autoclaved and  $\text{N}_2$ -purged sulfate-free artificial sea water (ASW) and 7.5 mL of the ASW mixture were added to each tube (Lyman & Fleming, 1940). Each treatment was then amended as follows: control (unamended), killed control (chloramphenicol), sulfate (10 mM), Mn(III)-DFOB and Fe(III)-DFOB (1 mM, DFOB=desferrioxamine B). No Mn(III)-DFOB or Fe(III)-DFOB treatments were performed at sites 1 and 2. Minerals (manganite, birnessite,  $\delta$ - $\text{MnO}_2$ , nontronite, ferrihydrite, goethite) were suspended in deionized water and added such that the final concentration of added Mn or Fe was 10 mM. All treatments were prepared in triplicate, such that three tubes could be sacrificed at each timepoint. Incubation tubes were then sealed with black butyl stoppers (Geo-microbial Technologies) and aluminum crimps. Oxygen/air was removed from the headspace by inserting a needle attached to a mechanical vacuum pump (Gast) and evacuating for 10 seconds.  $^{13}\text{C}$ -labeled methane (99%, ISOTECH) was added by injecting 1.5 mL by syringe. Unlabeled methane was then used to uniformly pressurize tubes to 29 PSI. As an initial timepoint, concentrations of iron, manganese, and sulfate as well as  $^{13}\text{C}$  content of DIC were measured on the starting slurry, as described below.

## Sampling

Incubations were stored upright in the dark at 4°C and sampled on days 35, 135, 189, and 259. Three replicate tubes per site and per treatment were sacrificed at each timepoint by venting, decrimping, and decanting overlying water for chemical and isotopic analyses as described below.

### 4.2.3 Chemical analyses

#### **<sup>13</sup>C-DIC measurements**

Methane oxidation rates were measured as the rate of <sup>13</sup>C accumulation in the DIC pool. Samples for <sup>13</sup>C-DIC were prepared by addition of 24 μL of 0.2 μm freshly filtered overlying water from incubations to 20 mL headspace vials, crimp-sealed with gray butyl septa. Each sample was prepared and analyzed in duplicate. Concentrated phosphoric acid (10 μL) was then added to each vial to convert all DIC into CO<sub>2</sub> for analysis. Standards were prepared by addition of sodium bicarbonate powder (3.4 mg, 40 μmol) to pre-evacuated Tedlar bags followed by dilution with N<sub>2</sub>-purged deionized water (400 mL) to produce 100 μM stock solutions. Two such stocks were produced, one using unlabeled bicarbonate and one using <sup>13</sup>C-labeled bicarbonate (99%, Cambridge Isotope Laboratories). Stock solutions were mixed gravimetrically through injection by Hamilton syringe into pre-weighed and crimp sealed 20 mL headspace vials (Restek) to produce standards varying from 0 to 9% <sup>13</sup>C. Phosphoric acid was added as described above. All standards were prepared in triplicate and showed excellent agreement between measured and predicted values ( $r^2 \geq 0.99$ ). To allow for removal of any air blank from empty vials, vials containing no added bicarbonate were run alongside standards. The resulting CO<sub>2</sub> was then purified and trapped on a modified TraceGas (IsoPrime, Inc.) purge and trap system coupled with a Gilson autosampler before isotopic analysis on an isotope ratio mass spectrometer (IRMS) (IsoPrime 100, Elementar Inc.). Comparison of replicate samples showed typical reproducibility of ±10‰ for less enriched samples (ie. 100-200‰) and ±50‰ for highly enriched samples (ie. 500-600‰). Corrections were applied to account for any air present in the headspace of the vial. Incubation replicates were averaged, and moles of methane oxidized were calculated using Equation 1. This calculation assumes no net removal of DIC occurs and that methane is the only additional source of DIC (i.e., there is no degradation of organic matter or dissolution of carbonates). Methane oxidized vs. time was plotted and a best fit line was calculated using linear regression, where the slope is the rate of



AOM. Error was estimated by calculating the same regression with data points adjusted plus and minus one standard deviation from the mean for each data point.

### **Sulfate concentrations**

Sulfate concentrations were measured using the barium chloride method (Vacu-vials kit, CHEMtrics). Overlying water was 0.2  $\mu\text{m}$  filtered and diluted as necessary, before the addition of acid and barium chloride to the sample. The resulting turbidity due to the formation of suspended barium sulfate crystals was measured by absorbance at 420 nm. Expected accuracy was  $\pm 15\%$  error at 75.0 ppm,  $\pm 20\%$  error at 25.0 ppm, and  $\pm 30\%$  at 10.0 ppm.

### **Iron concentrations**

All iron concentration measurements were made using the ferrozine method (Viollier et al. 2000). Immediately after collection of overlying water, samples for dissolved iron were 0.2  $\mu\text{m}$  filtered and 9  $\mu\text{L}$  of 10% v/v HCl was added to 700  $\mu\text{L}$  of filtered sample to stabilize the solution. To measure dissolved iron (II) (dFe(II)), acidified samples were then aliquoted (230  $\mu\text{L}$ ) into three wells of a 96 well plate and 12  $\mu\text{L}$  of 6 M ammonium acetate and 12  $\mu\text{L}$  of 0.01 M ferrozine were added to each well. After 1 hour, absorbance at 562 nm was measured on a microplate reader. For total dissolved iron (dFe(T)) measurements, 6  $\mu\text{L}$  of 1.4 M hydroxylamine was added to each well following dFe(II) measurement and allowed to react for 2 hours. Dissolved Fe(III) was calculated by difference.

For total iron (dissolved + particulate) measurements, 9  $\mu\text{L}$  of 10% v/v HCl was added to 700  $\mu\text{L}$  of unfiltered overlying water and allowed to digest overnight. Sample was aliquoted (230  $\mu\text{L}$ ) into three replicate wells and 12  $\mu\text{L}$  6 M ammonium acetate, 12  $\mu\text{L}$  0.01 M ferrozine, and 6  $\mu\text{L}$  1.4 M hydroxylamine were added to each well. Color was allowed to develop 1 hour before measuring absorbance. Measurement of pyritic iron samples was conducted by overnight treatment with 66  $\mu\text{L}$  of 10% v/v  $\text{HNO}_3$  per 700  $\mu\text{L}$  of unfiltered sample. Reagent additions and measurements were conducted as described above.

During the initial and final timepoint (t4), digests of the sediment were also performed by diluting sediment slurry 1:10 with deionized water and adding 10% v/v HCl as described for total iron

measurements above. Samples were then filtered and measured as described for dFe(II) and dFe(T). Sediment pyritic iron was also measured as described above.

Standard curves were prepared daily from stock solutions of ferrous sulfate ( $\text{FeSO}_4$ ). Precision between replicates was generally better than  $0.5 \mu\text{M}$ . Both Mn(III)-DFOB and Fe(III)-DFOB additions visibly altered the color of the samples, causing interference with absorption measurements. As such, absorbance of samples from these treatments was measured prior to addition of ferrozine, to allow for a background subtraction from final absorption measurements at 562 nm.

### Gibbs free energy calculations

Gibbs free energy of formation values at 1 bar and  $25^\circ \text{C}$  were taken from literature (Bellotti et al 2021; Stumm and Morgan 1996; Viellard 2000). Reaction with nontronite was assumed to reduce Fe(III) to Fe(II) without significant disturbance of the mineral structure, as has been demonstrated in microbial studies (Zhao et al. 2015). The following conditions were used for *in-situ*  $\Delta G$  calculations:  $[\text{CH}_4] = 1.5 \text{ mM}$ ,  $[\text{HCO}_3^-] = 11 \text{ mM}$ ,  $[\text{SO}_4^{2-}] = 10 \text{ mM}$ ,  $[\text{HS}^-] = 2 \text{ mM}$ ,  $[\text{Fe(III)-DFOB}] = [\text{Mn(III)-DFOB}] = 1 \text{ mM}$ ,  $[\text{Fe}^{2+}] = [\text{Mn}^{2+}] = 1 \mu\text{M}$ ,  $[\text{H}^+] = 10^{-8} \text{ M}$ , temperature =  $4^\circ \text{C}$ . Concentrations are taken either from the known amount added to incubations ( $\text{CH}_4$ ,  $\text{HCO}_3^-$ ,  $\text{SO}_4^{2-}$ , Fe(III)-DFOB, Mn(III)-DFOB), average of measurement performed on starting slurry ( $\text{Fe}^{2+}$ ), or literature values from the site ( $\text{HS}^-$ ,  $\text{Mn}^{2+}$ ,  $\text{H}^+$ ) (Luff and Wallman 2003).

## 4.3 Results

### 4.3.1 Methane oxidation rates

Site 1 was located close to an active bubble plume and carbonate mound at Hydrate Ridge (temperature:  $4.2^\circ \text{C}$ , depth: 797 m, salinity: 34.3). Methane oxidation rate in the control sediments was  $3.7 \pm 0.7 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$  (Figure 2a, Figure 3a, Table 1). No treatments significantly increased rates of AOM. However, both manganite and  $\delta\text{-MnO}_2$  additions significantly lowered rates of AOM compared to the control as did the killed control treatment ( $p < 0.05$ ).

Site 2 was also at Hydrate Ridge and close to Site 1 but was positioned 20 m away from any visible features of seep activity at a sediment-water interface free from carbonate structures, mats, or macrofauna (temperature:  $4.3^\circ \text{C}$ , depth: 787 m, salinity: 34.3). Overall compared to Site 1, Site 2

had slightly lower rates of AOM (Figure 2b, Figure 3b, Table 1). The control treatment had an AOM rate of  $2.7 \pm 0.2 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ . Addition of sulfate was the only treatment to show significant increases above the control ( $3.6 \pm 0.5 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ ) ( $p < 0.05$ ). As at Site 1, rates in manganite and  $\delta\text{-MnO}_2$  treatments were both significantly lower than the control. Nontronite and killed control treatments also had noticeable declines in measured AOM rate relative to the control.

Site 3 was located near a dark microbial mat and active bubble flares at McArthur Canyon (temperature:  $4.0^\circ \text{C}$ , depth: 832 m, salinity: 34.4). Of all the sites examined in this study, Site 3 had the highest overall rates of AOM (Figure 2c, Figure 3c, Table 1). In many treatments,  $\delta^{13}\text{C-DIC}$  values did not increase between t3 and t4 and thus rates for these treatments were calculated using data only up to t3. The unamended control had a rate of  $17.8 \pm 1.0 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ , nearly 5 times higher than Site 1 at Hydrate Ridge, which was also located near an area of active bubbling. Similar to Site 2, the addition of sulfate showed a significant increase in AOM rate. All four Mn treatments (manganite, birnessite,  $\delta\text{-MnO}_2$ , and Mn(III)-DFOB) had markedly lower rates compared to the control. Two iron treatments (ferrihydrite and goethite) and the killed control also had significantly lower rates of AOM.

Site 4 at McArthur Canyon was close to Site 3, but positioned 20 m away from cold seep features (temperature:  $4.0^\circ \text{C}$ , depth: 833 m, salinity: 34.3). Rates at this site were close in magnitude to those observed at Site 1 and Site 2, and much lower than Site 3 (Figure 2d, Figure 3d, Table 1). The control treatment exhibited an AOM rate of  $3.4 \pm 0.5 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ . No treatments had higher rates than the control. Three out of four Mn treatments, and all of the solid Mn oxide mineral additions, (manganite, birnessite, and  $\delta\text{-MnO}_2$ ) had significantly lower rates of AOM compared to the unamended control. Goethite and the killed control also showed depressed AOM rates.

Among the four study sites, there were several notable trends in measured AOM rates. In both sets of geographically paired sites (Sites 1+2, Sites 3+4), the site closer to the active cold seep had higher rates of AOM overall. Addition of sulfate caused significant increases in AOM at Sites 2 and 3. Across all study sites, no oxidized metal addition significantly increased rates of AOM above those of the unamended control treatment. However, both manganite and  $\delta\text{-MnO}_2$

consistently yielded significant reductions in methane oxidation rates. There was variability across the sites as to which other Mn or Fe treatments were found to depress rates of AOM.

#### *4.3.2 Sulfate concentrations*

Sulfate concentrations were measured in the starting slurries, at t2 (control and sulfate treatments only), and t4 (all treatments) (Table 2, Figure 4). Sites 1-3 had sulfate concentrations 1-2 mM in the starting slurry, while Site 4 started at 4 mM. Site 2 and Site 4 had higher concentrations of sulfate than their corresponding near-seep sites (Site 1 and Site 3, respectively). By t2, control treatments saw large decreases in sulfate concentrations with sites 1-3  $\leq 0.5$  mM and Site 4 measuring 2.3 mM. In the sulfate treatment at Site 3, sulfate concentration was nearly zero at t2. At the conclusion of the experiment, all sites and treatments were  $\leq 0.4$  mM. Site 3 had the lowest concentrations of sulfate overall, followed by Site 1. Excluding treatments with solid manganese mineral additions, the site closer to active seeps within geographically paired sites had lower sulfate concentrations ( $p < 0.05$ ).

#### *4.3.3 Iron concentrations*

Dissolved iron concentrations in the incubation water (dissolved Fe(II), dissolved Fe(III), total Fe, pyritic Fe) were measured in the starting slurries and at t1, t2, and t4 (Table 3-9, Figure 5-8). Overall, iron concentrations were consistently much lower at Site 3 (maximum  $\leq 30$   $\mu\text{M}$ ) compared to the other sites (maximum  $\geq 100$   $\mu\text{M}$ ).

At Site 1, 2, and 4, control, sulfate, and birnessite treatments generally displayed increases in [dFe(II)] between t1 and t2, then decreases between t2 and t4. Concentrations of dFe(II) at the t2 maximum were comparable in control and sulfate treatments (averages: 122  $\mu\text{M}$ , 132  $\mu\text{M}$  respectively), but lower in birnessite treatments (average: 72  $\mu\text{M}$ ). At Site 2, these treatments also had increases in particulate Fe (total Fe - dFe) concentrations between t2 and t4. Pyritic iron concentrations also increased in the control and sulfate treatments. At Site 3, relatively few changes were observed among these treatments and most iron concentrations were close to zero, though a small increase in dFe(II) was observed in the sulfate treatment at t2 (8  $\mu\text{M}$ ).

Generally stable, near zero iron concentrations were observed in the water among the killed, manganite, and  $\delta$ -MnO<sub>2</sub> treatments. At Site 1, a steady increase in [dFe(II)] was noted in the killed treatment. In the manganite treatment at Site 2 and Site 4, an increase in [dFe(II)] and small increase in [dFe(III)] occurred between t2 and t4. At Site 3, dFe(II) and particulate Fe concentrations rose between t2 and t4 in the  $\delta$ -MnO<sub>2</sub> treatment.

Ferrihydrite and goethite treatments generally behaved similarly at Site 2, with an increase in pyritic iron concentration between t1 and t2 followed by a decrease between t2 and t4. Additionally, particulate iron and dFe(III) concentrations rose between t2 and t4. Similar dynamics in pyritic iron concentration were observed at Site 1 and Site 4; however, increases in particulate iron and dFe(III) concentrations were only observed in the ferrihydrite treatment. At Sites 1, 2, and 4, nontronite treatments had similar pyritic iron dynamics as ferrihydrite and goethite treatments with generally lower maxima at t2 (averages: 52  $\mu$ M, 116  $\mu$ M, 82  $\mu$ M respectively). Particulate iron concentrations also increased between t1 and t2 and either decreased or remained constant between t2 and t4. At Site 3, iron concentrations for the goethite treatment remained close to zero and only small changes were observed in the nontronite treatment.

At Site 3, both the Mn(III)-DFOB and Fe(III)-DFOB treatments remained close to zero for all iron measurements. At Site 4, concentrations of dFe(II), dFe(III), and particulate Fe rose between t1 and t2 and then fell between t2 and t4 in the Mn(III)-DFOB treatment. Similarly to other oxidized iron treatments, the Fe(III)-DFOB treatment had a peak in pyritic iron concentration at t2 while dFe(III) and particulate iron concentration rose between t2 and t4 at Site 4.

To complement the iron measurements from the incubation waters, sediment digests (total Fe(II) and total Fe(III)) were also performed at the conclusion of the experiments (t4). Across all sites and treatments, no Fe(III) was detectable. Total Fe(II) concentration between sites and treatments varied between ~600 and 1000  $\mu$ M. All iron treatments had statistically significantly higher total Fe(II) concentrations compared to control treatments at all sites ( $p < 0.05$ ). No significant differences were found between total Fe(II) concentrations in kill or any manganese treatments compared to the control treatment.

## 4.4 Discussion

Rates of AOM were overall comparable to those of previous studies; however, in contrast to prior work, addition of oxidized iron or manganese did not increase measured rates of AOM above those from unamended controls. Two manganese treatments, in fact, caused rates to decrease at all four sites, which we hypothesize may be due to competition from heterotrophs. This divergence in results may also be due to other studies “pre-aging” sediments to entirely remove sulfate which may have allowed the slow growing ANME organisms to shift to metal-AOM based metabolisms prior the initiation of those experiments (Beal et al. 2009). We hypothesize the microbial community may have oxidized less methane overall in some metal treatments as metal-AOM results in higher theoretical energy yields per mole of methane. Finally, we infer the presence of metal-AOM at a site with low sulfate which suggests metal-AOM may occur under certain environmental conditions.

### 4.4.1 Comparison to previously reported rates of AOM

The marine sediments of the Cascadia Margin hosted substantial rates of AOM in our incubations. In environments of this type, AOM is thought to occur primarily in the sulfate-methane transition zone (SMTZ), a region found in anoxic sediments where the diffusion of sulfate downward and methane upward in the sediment overlap (Barnes and Goldberg 1976; Martens and Berner 1974; Reeburgh 2007). The depth of the SMTZ below the sediment-water interface varies widely (mm to >200 m) depending on several geochemical parameters including the input of organic matter and the rate of diffusion compared to factors controlling the microbially regulated rates of consumption of sulfate and methane (Knittel and Boetius 2009). Rates of sulfate-AOM in the environment have been found to vary across several orders of magnitude from several  $\mu\text{mol cm}^{-3} \text{ day}^{-1}$  in cold seeps with surface methane hydrates to  $<1 \text{ nmol cm}^{-3} \text{ day}^{-1}$  in anoxic marine water columns. Substrate availability and oxygen concentration are believed to be the primary factors controlling the wide range of rates, with other environmental parameters such as pH, salinity, pressure, and temperature playing smaller roles (Knittel and Boetius 2009).

In contrast to expectations, the addition of oxidized forms of Fe and Mn did not universally increase rates of AOM. Generally, rates of metal-AOM in the environment have been reported from  $1\text{-}60 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ , although isolating metal-AOM rates from concurrently occurring

sulfate-AOM has not always been possible (Table 12; Norði et al. 2013). Laboratory experiments have provided additional insights into estimating rates of metal-AOM and have varied from a few nmol to tens of  $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$  (Table 13; Beal et al. 2009; Ettwig et al. 2016; Li et al. 2021; Segarra et al. 2013; Scheller et al. 2016). Several studies have also compared rates when treated with different forms of iron oxides. Scheller et al. (2016) incubated seep sediments from Santa Monica Basin with either Fe(III)-citrate, Fe(III)-EDTA, or Fe(III)-NTA. Fe(III)-citrate showed the highest rates of Fe-AOM, followed by Fe(III)-EDTA, and finally Fe(III)-NTA, suggesting the strength of the ligand may play a role in the observed reactivity and rate of metal-coupled AOM (Scheller et al. 2016). Solubility and surface area were also suggested to play an important role in determining metal-AOM rates in culture experiments conducted by Ettwig et al. (2016). Compared to nano-particulate ferrihydrite, soluble Fe(III)-citrate had approximately 13 times faster rates of Fe-AOM per g of protein  $\text{day}^{-1}$  (Ettwig et al. 2016). Li et al. (2021) compared different solid iron oxides (magnetite, goethite, and ferrihydrite) with goethite displaying the highest rates, followed by ferrihydrite, and magnetite; however, all rates were roughly comparable and the researchers cautioned that recycling of dissolved Fe(II) back to Fe(III) by putative iron oxidizer *Chlorobium* bacterium present at high relative abundance could confound their results.

Compared to literature rates, our results from oxidized metal treatments (Table 1, 0.8 - 18  $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ ) are similar in magnitude to other metal-addition incubations using natural aquatic sediments (Table 13, 0 - 14  $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ ) (Beal et al. 2009; Egger et al. 2015; Segarra et al. 2013; Sivan et al. 2011). Indeed, the rates measured in our incubations were most comparable to those of Beal et al. 2009, which also used sediments collected from marine methane seeps. However, in several of these studies, the addition of oxidized metals caused rates of AOM to increase above those of unamended control treatments, while our study did not observe any metal treatment consistently increasing rates of AOM. Instead, no individual oxidized metal treatment elevated rates of AOM above that of the live control. In all four incubations, manganite and  $\delta\text{-MnO}_2$  amendments resulted in significantly depressed rates of AOM compared to control treatments ( $p < 0.05$ ). Similarly lowered rates of AOM were observed in rice paddy soil and lake sediments upon addition of  $\delta\text{-MnO}_2$  and in North Sea sediments upon addition of birnessite (Aromokeye et al. 2020; Kumaraswamy et al. 2001; Vigderovich et al. 2022). We speculate that our lowered rates of AOM may have been due to preferential organoclastic Mn reduction compared

to Mn-AOM. This could lower rates of AOM below that of the control if the heterotroph community stimulated by addition of manganite and  $\delta$ -MnO<sub>2</sub> were able to outcompete ANME for a limiting nutrient required by both groups. Alternatively, the release of unlabeled CO<sub>2</sub> from natural organic material could depress the  $\delta^{13}\text{C}$ -CO<sub>2</sub> signal. We further discuss additional potential explanations for these results below. As in other studies, the addition of sulfate increased rates of AOM significantly, but only at Site 2 and 3 ( $p < 0.05$ , Beal et al. 2009; Segarra et al. 2013). Site 1 and Site 4 also had higher concentrations of sulfate at t2 compared to Site 2 and Site 3, potentially suggesting overall slower rates of sulfate-AOM (Figure 4).

#### 4.4.2 Community energy yields

In order to compare the relative reactivities of the oxidized metals used in our incubation experiments, we calculated both  $\Delta G^0$  (at standard state conditions) and  $\Delta G$  (at *in-situ* conditions) (Table 10). Notably, the *in-situ*  $\Delta G$  of AOM coupled to goethite reduction was positive, indicating it would be thermodynamically unfavorable under the reaction conditions of this experiment.

Examination of Gibbs free energy yields for AOM coupled to different electron acceptors also reveals that microbes could potentially generate the same energy yield while oxidizing fewer moles of methane coupled to oxidized metal compared to sulfate (Segarra et al. 2013). For instance, using calculated *in-situ*  $\Delta G$  values, oxidation of the same amount of methane yields 7 times more energy when coupled to reduction of birnessite compared to reduction of sulfate. At Site 3, we observe a rate of  $33 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$  for the sulfate treatment and  $9.4 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$  for birnessite. If we consider the energy yields, sulfate-AOM at this rate yields only  $1.64 \text{ J cm}^{-3} \text{ yr}^{-1}$  compared to  $3.53 \text{ J cm}^{-3} \text{ yr}^{-1}$  for birnessite-AOM (Figure 9, Table 11). In fact, we find equivalent or larger theoretical energy yields in all oxidized metal treatments across all sites compared to calculated theoretical energy yields for sulfate. This approach assumes microbes are only utilizing the added electron acceptor (i.e., no sulfate-AOM occurs in the birnessite treatment) and that solid minerals do not need to be broken down to be used; however, it illustrates the large potential gain in energy yield using oxidized metals compared to sulfate. If we instead assume the community need only produce the same energy yield as observed in the sulfate treatment, it is possible to calculate the minimum fraction of the AOM rate measured in the study that must be metal-AOM (Equation 2,3, Figure 10). Following from this, it is evident in most treatments that even a relatively modest



fraction of metal-AOM (on average ~15%) could provide the community with equivalent energy yield to that of our added sulfate treatment. These two approaches suggest potential minima and maxima for the predicted energy yields from our treatments.

Microbes performing AOM (ANME) are known to double extremely slowly (1.5 - 8 months) and thus the community may not have been able to expand rapidly when offered increased access to substrates over the course of the experiment (8.5 months) (Nauhaus et al. 2007; Zhang et al. 2011). Reports on similar incubation approaches have “aged” sediments for 12 months to eliminate residual sulfate and thereby allowed the microbial community to slowly adapt to sulfate-free conditions, thus possibly priming them for metal-AOM (Beal et al. 2009). Additionally, many questions remain as to the exact mechanisms of electron transfer between methane and solid metal oxides (Liang et al. 2019; Dang et al. 2021; Zhang et al. 2021). If ANME are in fact participating in direct interspecies electron transfer (DIET) as some researchers suggest, this could also be impeded by our incubation set-up. Li et al. (2021) found that additions of iron oxides (magnetite, goethite, and ferrihydrite) to a bioreactor containing an enrichment *Ca. “M. ferrireducens”* appreciably lowered Fe-AOM rates for >100 days and suggested that this may be due to disruption of archaeal-Fe oxide particle aggregates necessary for DIET (Li et al. 2021).

#### 4.4.3 Inferring metal-AOM from other elements

Using the sulfate concentration data collected, we calculated overall sulfate removal rates and compared them to the AOM rates. Assuming a 1:1 stoichiometry of  $\text{SO}_4^{2-}$  to  $\text{CH}_4$ , even if all sulfate present went towards sulfate-AOM there was insufficient sulfate present to support measured methane consumption rates in nearly all treatments at site 3, including the control, all Mn treatments excluding  $\delta\text{-MnO}_2$ , and all four Fe treatments. This indicates that metal-AOM must have been occurring in these treatments, even though their overall rates were not higher than the control or sulfate treatments. Inferred metal-AOM rates from Mn and Fe addition treatments varied from 5 - 13  $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ . As no additional Mn or Fe was added to the control, oxidized metals already present in the sediment at Site 3 could have been responsible for this posited metal-AOM which accounted for ~40% of its overall AOM rate (13  $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ ). Site 3 had the lowest starting  $[\text{SO}_4^{2-}]$  of the four sites and thus its native microbial community may have been

better able to adapt to using metals in the place of sulfate or have already been performing metal-AOM *in-situ* prior to the initiation of the experiment.

It is difficult to fully close mass balance for iron as only the overlying water was measured at the majority of the timepoints. There was an intermediate accumulation of dFe(II) at t2 in several treatments including control, sulfate, and birnessite treatments from all four sites up to 163  $\mu\text{M}$  (1.2  $\mu\text{mol}$  total). Assuming this release of  $\text{Fe}^{2+}$  was related to Fe-AOM, this would only account for 0.2  $\mu\text{mol}$  of  $\text{CH}_4$  oxidized. This example illustrates that while rates of metal-AOM may not be as high as those of sulfate-AOM, these reactions could still significantly impact other biogeochemical cycles. The relative stoichiometry (8:1 for Fe/ $\text{CH}_4$ , 4:1 for Mn/ $\text{CH}_4$ ) of metal-AOM reactions causes them to potentially be more impactful to metal cycling than carbon. Further, iron(II) can be removed from solution by reaction with sulfide to form authigenic iron sulfide minerals such as mackinawite. However, due to the constraints imposed by the method of Fe measurement used we were unable to directly measure their formation within the sediments and thus estimates of Fe-AOM solely from Fe measurements were unfeasible. Speciation of Mn in solution was not performed.

#### **4.5 Conclusion**

As the climate changes, it grows ever more urgent to understand the processes controlling the emissions of greenhouse gases such as methane. Other studies have suggested metal-AOM may be responsible for a portion of the removal of seafloor methane, thereby preventing its release to the atmosphere; however, the rates and mechanisms by which this process occurs are still poorly understood. In this study, we measured the rates of AOM from cold-seep sediments collected from four sites along the Cascadia Margin incubated with a diverse array of potentially environmentally relevant oxidized iron and manganese species. While we did not observe any consistently elevated rates of AOM due to these additions, many oxidized metal treatments in fact decreased rates of AOM below that of an unamended control, including manganite and  $\delta\text{-MnO}_2$  which lowered rates in all four incubations. We hypothesize this finding could have been related to increased energy yields to the microbial community related to coupling AOM to metal. Additionally, ANME are known to grow particularly slowly so they may not have been able to take full advantage of an increase in substrate on the timescale of the experiment. Finally, manganite and  $\delta\text{-MnO}_2$  may have

stimulated heterotrophs which competed for nutrients with ANME. Nevertheless, in the site with the lowest recorded sulfate, rates of up to  $13 \mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$  of inferred metal-AOM were observed, suggesting its role in marine sediments is non-negligible. Further study will be necessary to continue to expand our understanding of how and why different forms of oxidized iron and manganese impact rates of AOM in the environment.

$$^{12}\text{CH}_4 + ^{13}\text{CH}_4 = \left(1 + \frac{(1 + F_{13}^*)}{F_{13}^*}\right) \frac{F_{13} \text{ } ^{12}\text{DIC} + F_{13} \text{ } ^{13}\text{DIC} + ^{13}\text{DIC}}{1 - F_{13} \left(1 + \frac{(1 - F_{13}^*)}{F_{13}^*}\right)}$$

$$F_{13}^* = \frac{^{13}\text{CH}_4^*}{^{12}\text{CH}_4^* + ^{13}\text{CH}_4^*}$$

$$F_{13} = \frac{^{13}\text{DIC} + ^{13}\text{CH}_4}{^{12}\text{DIC} + ^{13}\text{DIC} + ^{12}\text{CH}_4 + ^{13}\text{CH}_4}$$

$^{12}\text{CH}_4$  = moles of  $^{12}\text{C}$ -methane oxidized

$^{13}\text{CH}_4$  = moles of  $^{13}\text{C}$ -methane oxidized

$^{12}\text{CH}_4^*$  = moles of  $^{12}\text{C}$ -methane at  $t_0$

$^{13}\text{CH}_4^*$  = moles of  $^{13}\text{C}$ -methane at  $t_0$

$^{12}\text{DIC}$  = moles of  $^{12}\text{C}$ -DIC at  $t_0$

$^{13}\text{DIC}$  = moles of  $^{13}\text{C}$ -DIC at  $t_0$

Equation 1: Formula to calculate overall moles of methane oxidized using  $F_{13}$  = the isotopic composition of total DIC measured on IRMS at a given time. For this experiment,  $F_{13}^* = 0.06044$ ,  $^{12}\text{DIC} = 2354 \mu\text{mol}$ ,  $^{13}\text{DIC} = 26.2 \mu\text{mol}$

AOM rate = Sulfate-AOM rate + Metal-AOM rate

Energy yield = Sulfate-AOM energy yield + Metal-AOM energy yield

$$= \Delta G_{\text{SO}_4}(\text{Sulfate-AOM rate}) + \Delta G_{\text{Metal}}(\text{Metal-AOM rate})$$

Equations 2, 3: Calculations used to produce Figure 5. AOM rate = measured by  $\delta^{13}\text{C}$ , Energy yield = energy yield from the sulfate treatment at a given site.

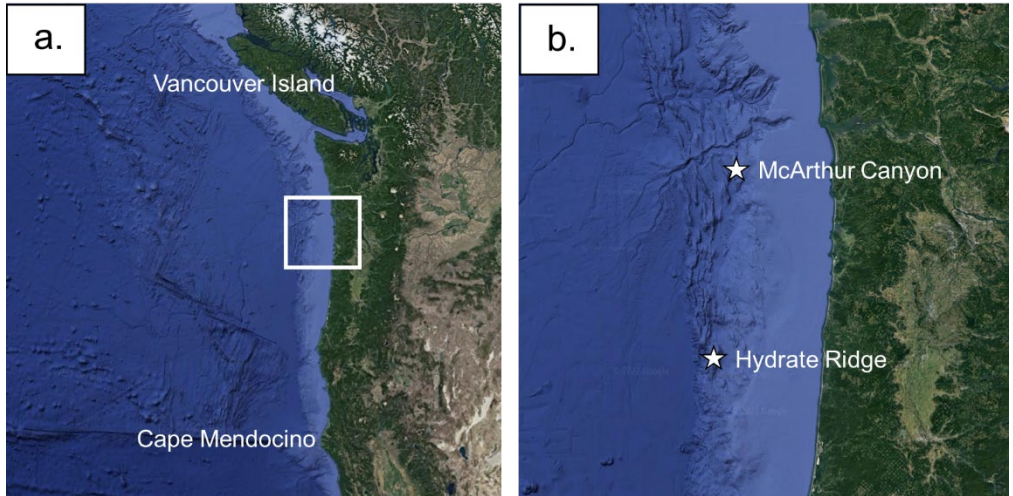


Figure 1: a. Satellite image of the west coast of the United States and Canada showing the full range of the Cascadia Margin, white box is magnified in b. Satellite image of the coast of Oregon with two major study areas marked.

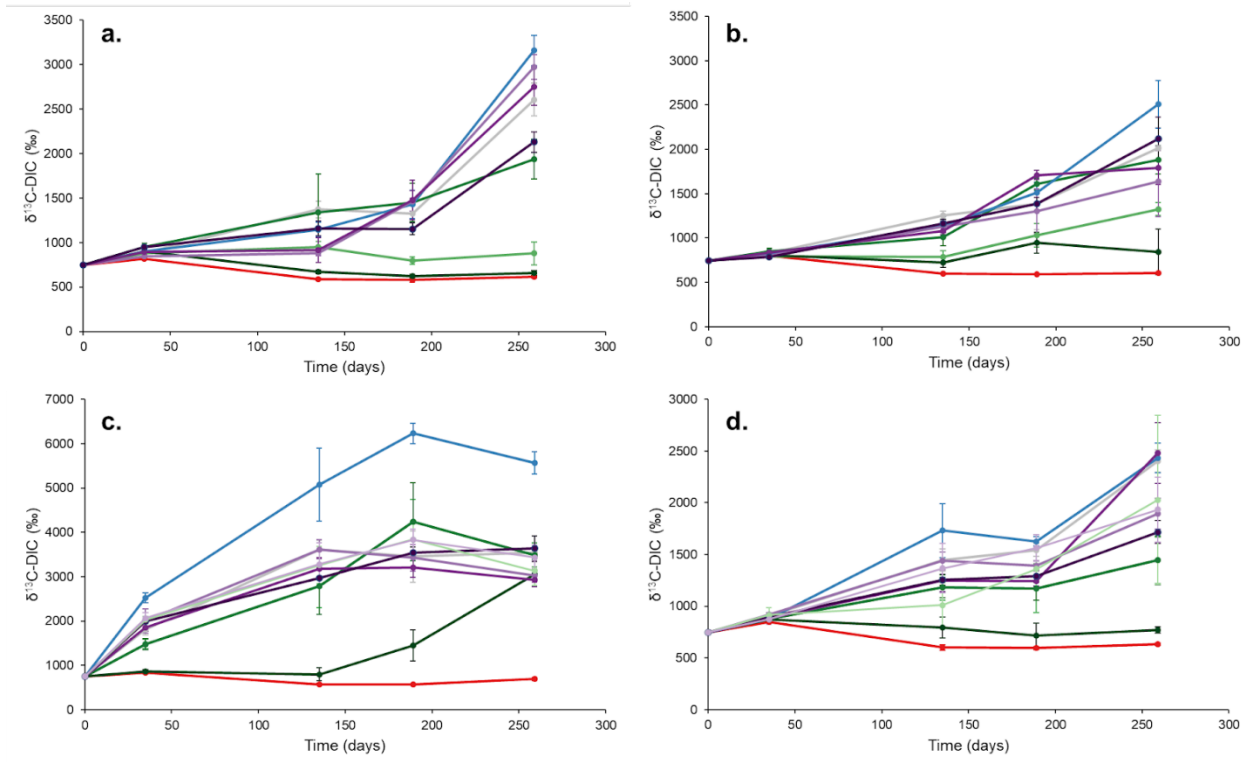


Figure 2:  $\delta^{13}\text{C-DIC}$  (‰) vs. time (days) from all four incubations a. Site 1: Hydrate Ridge, near bubbles, b. Site 2: Hydrate Ridge, 20m from bubbles, c. Site 3: McArthur Canyon, microbial mat, d. Site 4: McArthur Canyon, 20m from bubbles. Oxidized Mn additions are colored in green and oxidized Fe additions are colored in purple (full color key below). No Mn(III)-DFOB or Fe(III)-DFOB treatments were conducted at Site 1 or Site 2. Error bars represent the standard deviation between three replicate tubes, measured in duplicate.

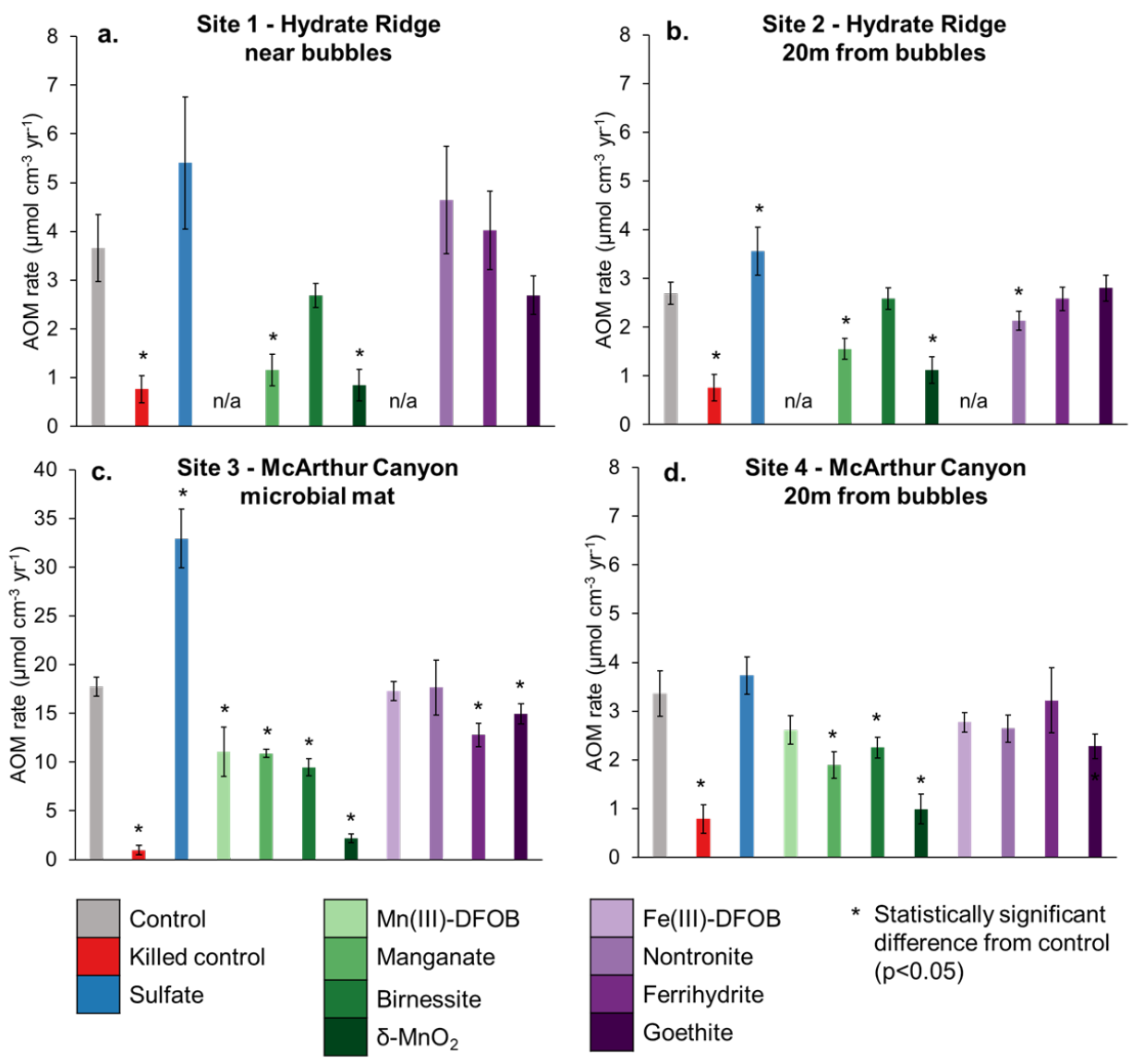


Figure 3: Rates of AOM ( $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ ) from all four incubations. Oxidized Mn additions are colored green and oxidized Fe additions are colored purple. No Mn(III)-DFOB or Fe(III)-DFOB treatments were conducted at Site 1 or Site 2. Bars marked with a \* have a statistically significant difference from the control treatment ( $p < 0.05$ ). Error bars represent the standard deviation between three replicate tubes.

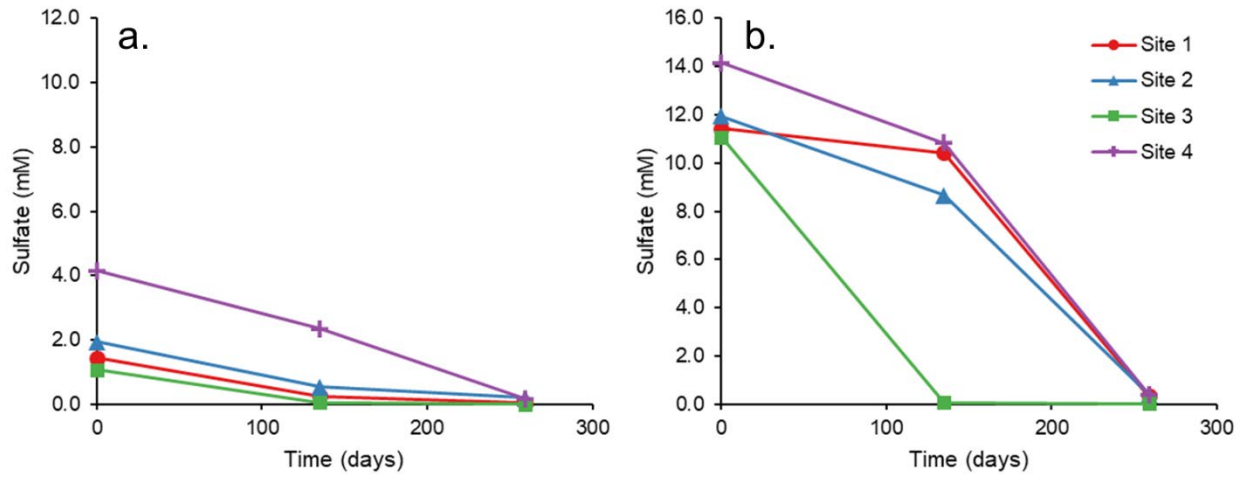


Figure 4: Sulfate concentrations (mM) vs. time (days) for the starting slurry ( $t_0$ ) and a. Control treatments ( $t_2$  and  $t_4$ ), b. Sulfate treatments ( $t_2$  and  $t_4$ ).  $t_0$  for sulfate treatments is calculated by adding the control values to the amount added (10mM).

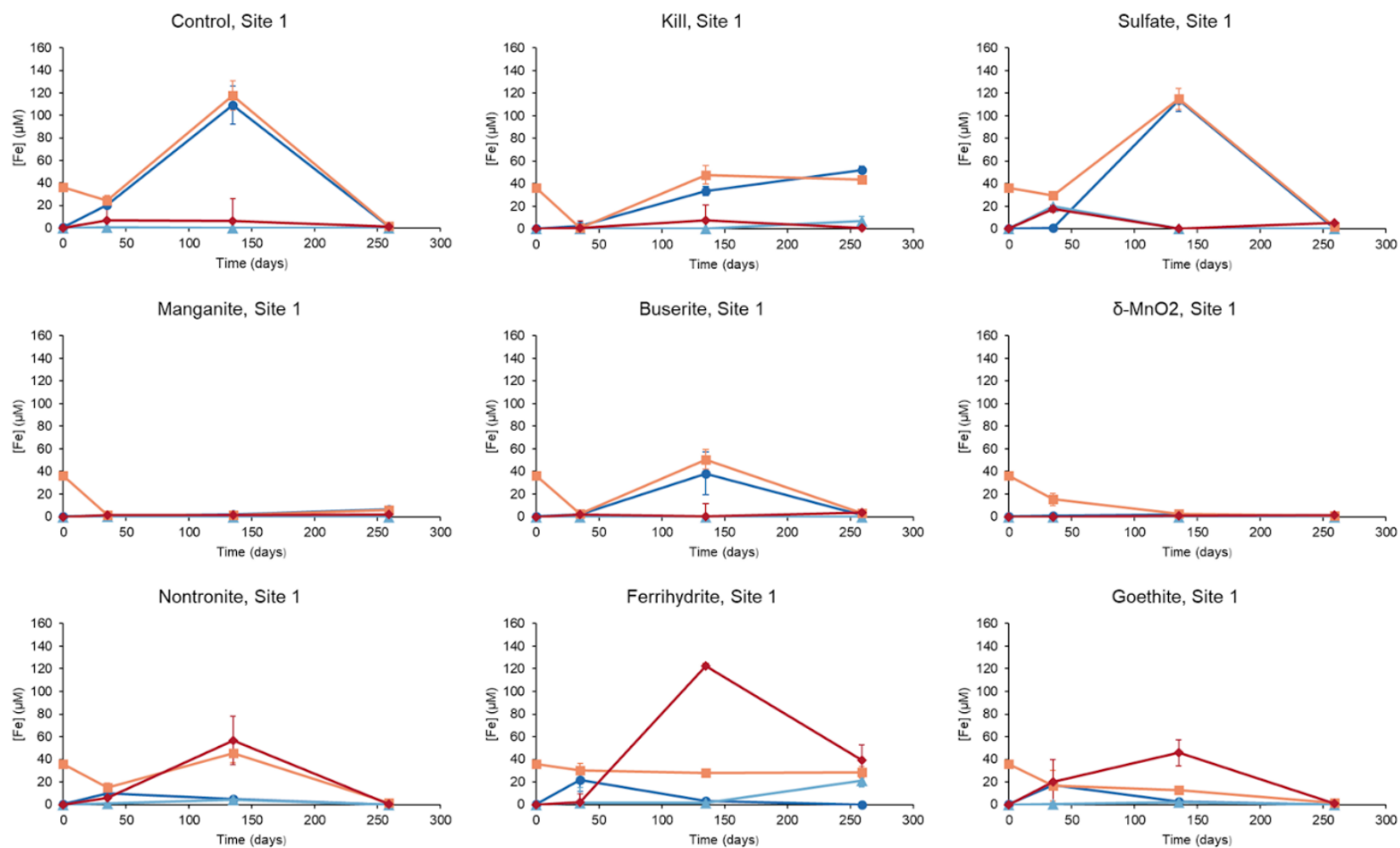


Figure 5: Site 1 iron concentrations from incubation liquid only. Dark blue: dFe(II), light blue: dFe(III), orange: total Fe (unfiltered), red: pyritic iron



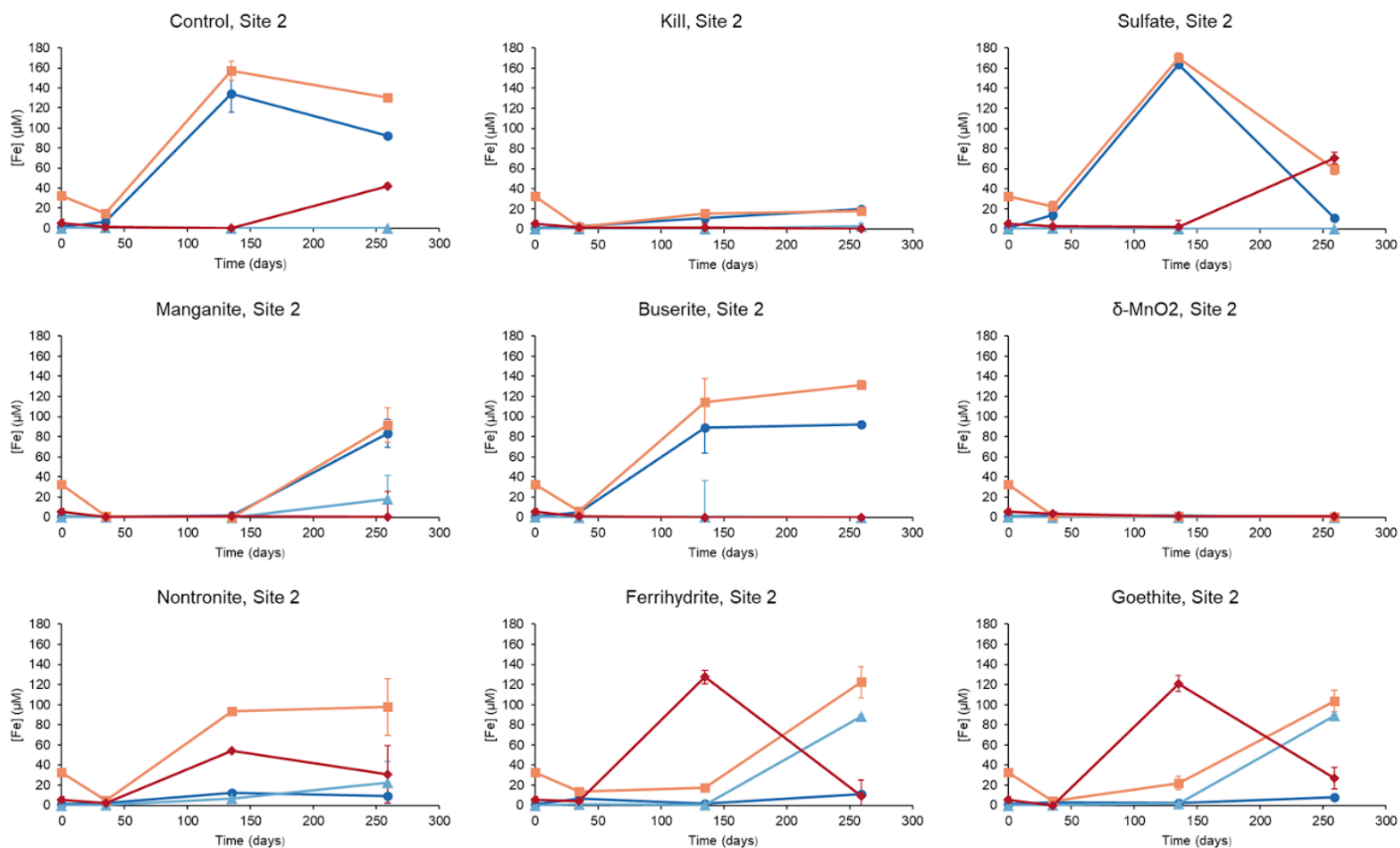


Figure 6: Site 2 iron concentrations from incubation liquid only. Dark blue: dFe(II), light blue: dFe(III), orange: total Fe (unfiltered), red: pyritic iron

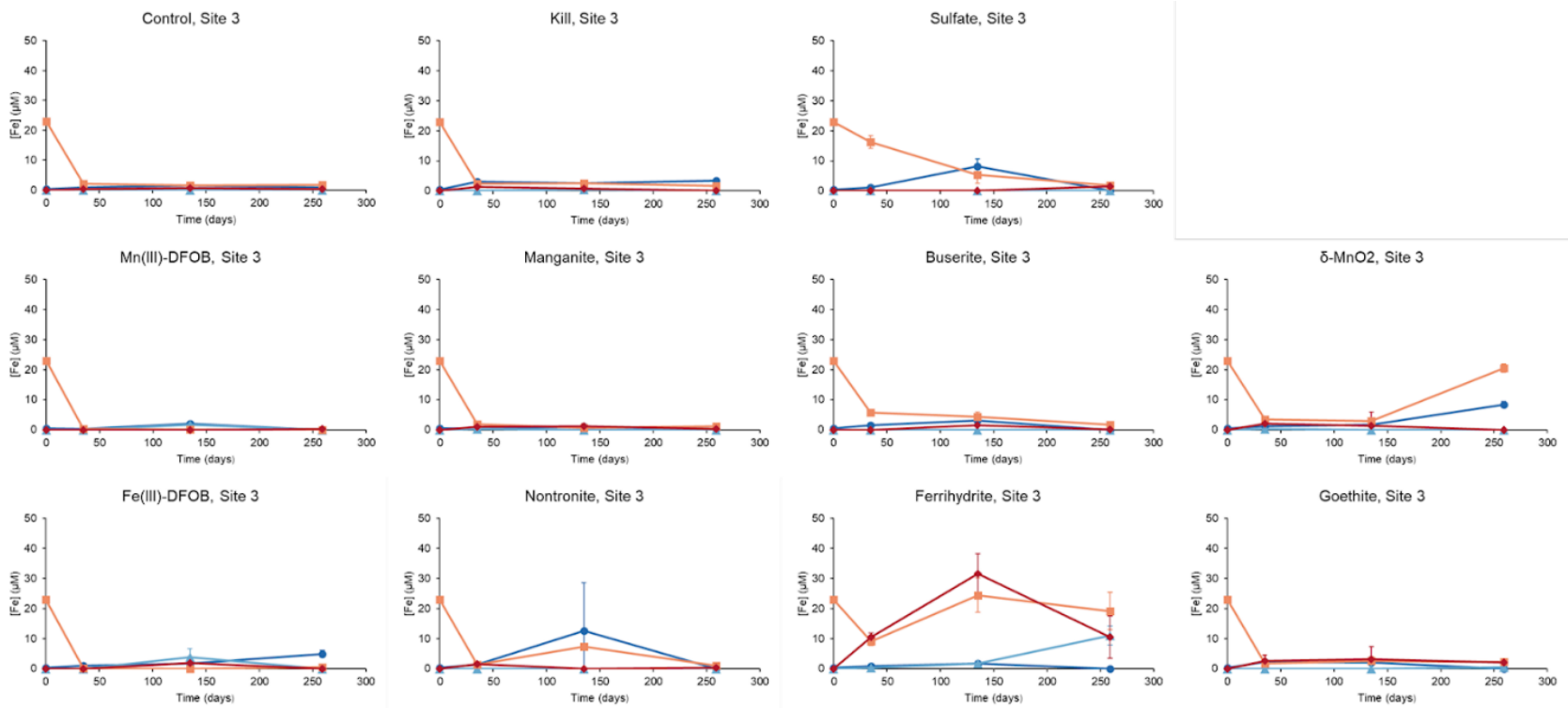


Figure 7: Site 3 iron concentrations from incubation liquid only. Dark blue: dFe(II), light blue: dFe(III), orange: total Fe (unfiltered), red: pyritic iron

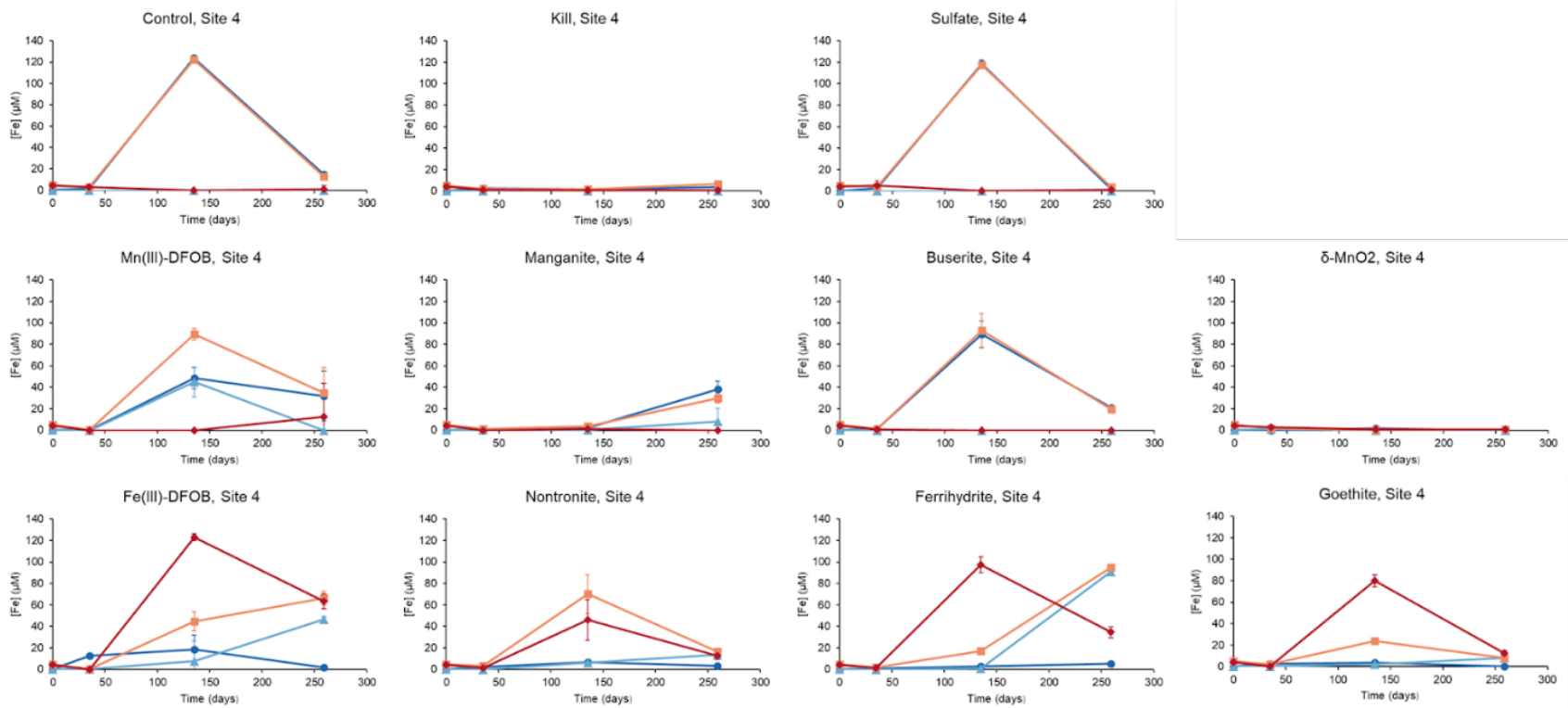


Figure 8: Site 4 iron concentrations from incubation liquid only. Dark blue: dFe(II), light blue: dFe(III), orange: total Fe (unfiltered), red: pyritic iron

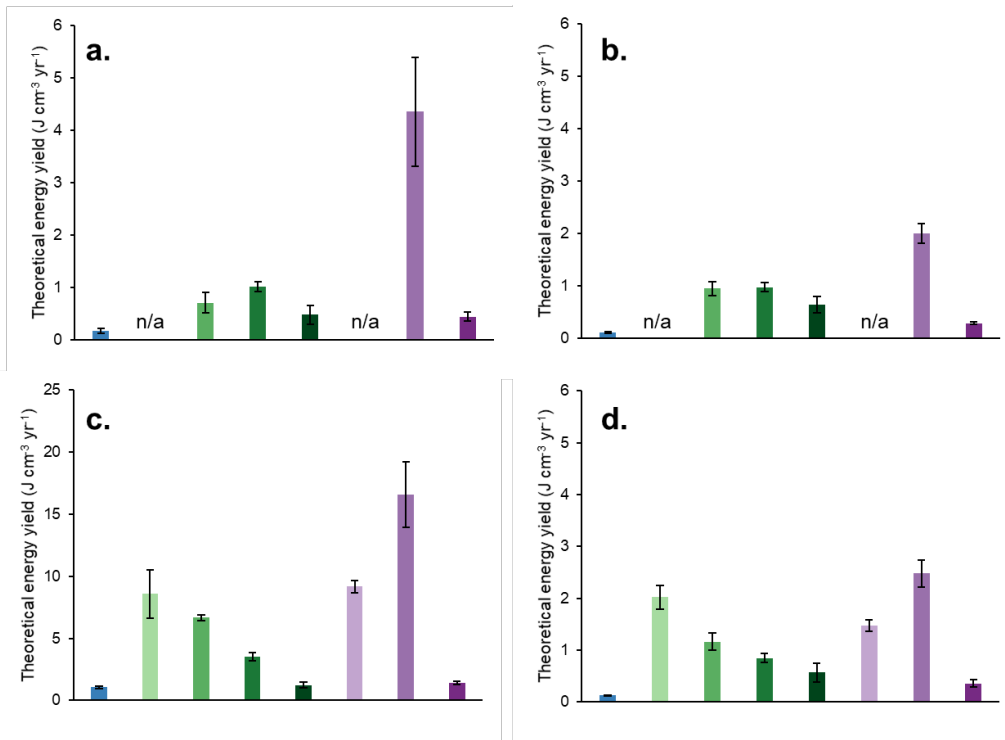


Figure 9: Theoretical energy yields assuming all measured AOM was due to the added electron acceptor.

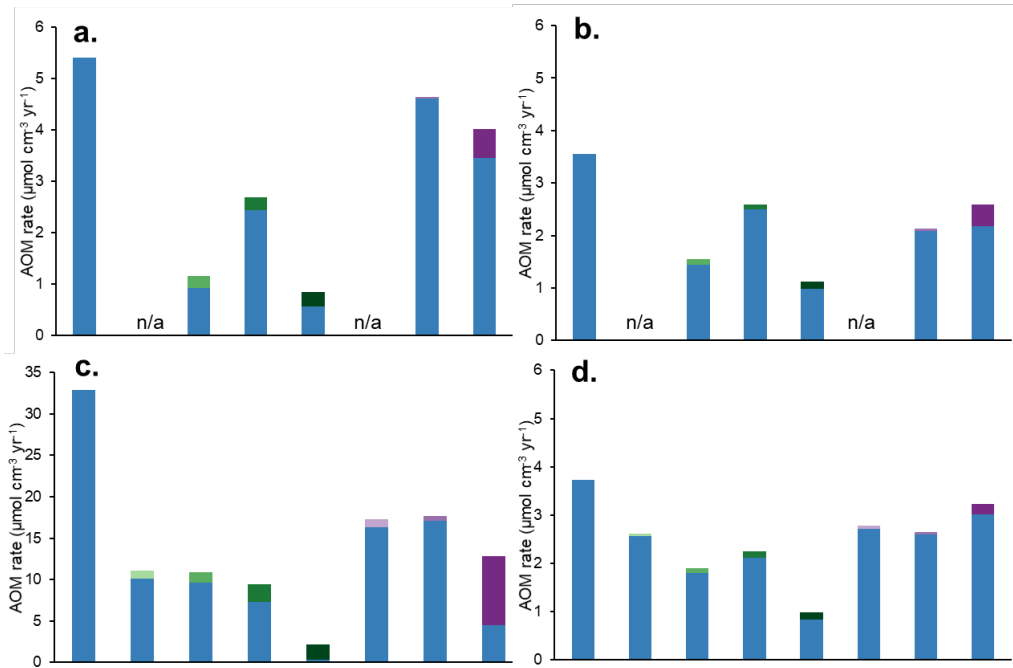


Figure 10: Total heights of bars represent the measured AOM rate at each site. Fractions are calculated such that total energy yield from the sum of sulfate-AOM and metal-AOM are equal in each bar.

Treatment	Site 1	Site 2	Site 3	Site 4
Control	3.7 ± 0.7	2.7 ± 0.2	17.8 ± 1.0	3.4 ± 0.5
Kill	0.8 ± 0.3	0.8 ± 0.3	1.0 ± 0.5	0.8 ± 0.3
Mn(III)-DFOB	n/a	n/a	11.1 ± 2.5	2.6 ± 0.3
Manganite	1.2 ± 0.3	1.6 ± 0.2	10.9 ± 0.4	1.9 ± 0.3
Birnessite	2.7 ± 0.3	2.6 ± 0.2	9.4 ± 0.9	2.3 ± 0.2
δ-MnO <sub>2</sub>	0.8 ± 0.3	1.1 ± 0.3	2.2 ± 0.4	1.0 ± 0.3
Sulfate	5.4 ± 1.4	3.6 ± 0.5	32.9 ± 2.3	3.7 ± 0.4
Fe(III)-DFOB	n/a	n/a	17.3 ± 0.9	2.8 ± 0.2
Nontronite	4.6 ± 1.1	2.1 ± 0.2	17.6 ± 2.8	2.6 ± 0.3
Ferrihydrite	4.0 ± 0.8	2.6 ± 0.2	12.8 ± 1.2	3.2 ± 0.7
Goethite	2.7 ± 0.4	2.8 ± 0.3	15.0 ± 1.0	2.3 ± 0.3

Table 1: Rates of AOM ( $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ ) from four incubation experiments treated with a variety of oxidized iron and manganese species, as well as sulfate and live/killed controls. Errors represent one standard deviation between three replicate tubes.

Timepoint	Treatment	Site 1	Site 2	Site 3	Site 4
t0	Starting slurry	1.44	1.95	1.06	4.15
t2	Control	0.26	0.54	0.05	2.34
	Sulfate	10.43	8.67	0.06	10.82
t4	Control	0.04	0.20	n.d.	0.16
	Kill	0.09	0.19	0.07	0.10
	Mn(III)-DFOB			0.01	0.18
	Manganite	0.24	0.23	0.01	0.26
	Buserite	0.16	0.17	0.02	0.10
	δ-MnO <sub>2</sub>	0.25	0.22	0.03	0.18
	Sulfate	0.34	0.40	0.03	0.41
	Fe(III)-DFOB			0.03	0.25
	Nontronite	0.11	0.24	0.01	0.22
	Ferrihydrite	0.09	0.19	0.02	0.19
Goethite	0.11	0.20	0.01	0.19	

Table 2: Sulfate concentrations (mM) from starting slurry and incubation timepoints. n.d. = below detection limit. Accuracy expectations are ±15% error at 0.78 mM, ±20% error at 0.26 mM, and ±30% at 0.10 mM.

	Timepoint	Control	Kill	Manganite	Buserite	$\delta$ -MnO <sub>2</sub>	Sulfate	Nontronite	Ferrihydrite	Goethite
dFe(II)	t0	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10	0.28 ± 0.10
	t1	20.58 ± 0.15	2.57 ± 0.15	0.63 ± 0.28	1.74 ± 0.47	1.13 ± 0.15	1.02 ± 0.09	9.80 ± 3.51	21.56 ± 9.70	17.40 ± 0.40
	t2	109.04 ± 17.08	33.46 ± 4.19	1.77 ± 0.69	38.22 ± 18.71	2.21 ± 0.59	113.96 ± 10.17	4.77 ± 0.68	3.08 ± 0.37	2.75 ± 0.56
	t4	0.94 ± 0.60	52.05 ± 3.10	6.65 ± 0.97	1.24 ± 0.16	n.d.	n.d.	n.d.	n.d.	n.d.
dFe(T)	t0	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07	0.28 ± 0.07
	t1	21.02 ± 0.32	2.52 ± 0.21	0.96 ± 0.25	1.48 ± 0.58	1.10 ± 0.17	20.94 ± 1.05	10.58 ± 3.21	23.04 ± 9.47	17.52 ± 1.09
	t2	108.68 ± 17.21	33.30 ± 4.10	1.66 ± 0.73	38.21 ± 18.64	1.88 ± 0.59	113.32 ± 10.31	8.92 ± 1.39	4.32 ± 0.19	4.74 ± 1.07
	t4	0.75 ± 0.60	59.26 ± 2.17	5.89 ± 1.30	0.86 ± 0.41	n.d.	n.d.	n.d.	21.01 ± 5.66	n.d.
dFe(III)	t0	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
	t1	0.43 ± 0.36	n.d.	0.33 ± 0.37	n.d.	n.d.	19.91 ± 1.06	0.78 ± 4.76	1.47 ± 13.55	0.12 ± 1.16
	t2	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	4.14 ± 1.55	1.24 ± 0.42	2.00 ± 1.21
	t4	n.d.	7.21 ± 3.78	n.d.	n.d.	n.d.	n.d.	n.d.	21.01 ± 5.68	n.d.
Fe(III)%	t0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
	t1	2.05	0.00	34.61	0.00	0.00	95.11	7.34	6.40	0.67
	t2	0.00	0.00	0.00	0.00	0.00	0.00	46.45	28.74	42.10
	t4	0.00	12.17	0.00	0.00	n/a	n/a	n/a	100.00	n/a
Total Fe	t0	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19	36.06 ± 0.19
	t1	24.50 ± 4.01	1.02 ± 0.02	1.44 ± 0.58	2.72 ± 0.16	15.22 ± 5.48	29.38 ± 1.32	15.14 ± 3.57	30.14 ± 6.18	16.86 ± 13.43
	t2	117.64 ± 13.13	47.62 ± 8.19	1.41 ± 1.10	50.61 ± 8.53	2.54 ± 1.51	114.88 ± 9.25	45.50 ± 8.71	28.06 ± 2.34	12.67 ± 0.72
	t4	1.46 ± 0.36	43.46 ± 2.93	5.65 ± 1.29	2.88 ± 0.29	0.87 ± 0.04	1.71 ± 0.13	1.75 ± 0.78	28.48 ± 4.83	1.54 ± 0.14
FeS	t0	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
	t1	6.70 ± 13.06	1.04 ± 5.89	1.66 ± 1.04	1.91 ± 1.29	n.d.	17.80 ± 2.71	6.11 ± 4.48	1.95 ± 7.27	19.82 ± 19.85
	t2	6.27 ± 19.67	7.43 ± 13.46	1.23 ± 1.39	0.10 ± 11.26	1.12 ± 1.99	n.d.	56.62 ± 21.62	122.52 ± 2.39	45.76 ± 11.47
	t4	1.08 ± 0.96	1.04 ± 5.89	2.24 ± 3.10	3.70 ± 0.88	1.56 ± 0.25	5.35 ± 0.58	0.58 ± 0.91	39.07 ± 13.60	0.86 ± 0.29
Digest Fe(II)	t4	648.15 ± 110.89	702.79 ± 19.07	812.03 ± 29.12	853.60 ± 22.06	780.79 ± 26.16	919.06 ± 9.64	928.62 ± 33.21	953.63 ± 23.95	957.58 ± 9.82
Digest Fe(T)	t4	628.73 ± 108.07	698.40 ± 20.45	806.70 ± 31.03	844.83 ± 21.29	731.72 ± 22.88	910.90 ± 10.28	920.65 ± 32.22	943.38 ± 21.83	943.81 ± 8.91
Digest Fe(III)	t4	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.

Table 3: Site 1 iron concentrations (μM). Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.

	Timepoint	Control	Kill	Manganite	Buserite	$\delta$ -MnO <sub>2</sub>	Sulfate	Nontronite	Ferrihydrite	Goethite
dFe(II)	t0	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05	0.97 ± 0.05
	t1	6.07 ± 1.02	2.52 ± 0.02	0.51 ± 0.10	4.68 ± 0.71	1.29 ± 0.38	14.49 ± 0.64	2.09 ± 0.65	6.94 ± 2.75	2.83 ± 0.66
	t2	134.53 ± 19.03	11.14 ± 0.98	1.91 ± 0.70	89.07 ± 25.60	1.63 ± 0.11	163.75 ± 3.28	12.59 ± 0.85	1.82 ± 0.37	2.32 ± 0.19
	t4	92.49 ± 0.54	20.15 ± 2.49	83.58 ± 13.94	92.30 ± 1.05	n.d.	11.14 ± 1.04	9.33 ± 0.21	10.90 ± 1.16	7.81 ± 0.73
dFe(T)	t0	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04	1.05 ± 0.04
	t1	6.60 ± 1.63	2.41 ± 0.04	0.90 ± 0.15	4.51 ± 0.75	1.28 ± 0.41	15.18 ± 0.97	2.43 ± 1.10	8.19 ± 2.84	3.08 ± 0.79
	t2	134.07 ± 18.95	10.95 ± 1.09	1.78 ± 0.70	89.36 ± 25.56	1.52 ± 0.06	162.90 ± 2.72	19.15 ± 0.27	2.53 ± 0.38	4.06 ± 0.59
	t4	91.64 ± 0.57	22.74 ± 1.24	101.82 ± 18.76	90.77 ± 1.52	n.d.	10.79 ± 1.36	31.74 ± 21.03	99.05 ± 1.34	97.15 ± 1.00
dFe(III)	t0	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06	0.08 ± 0.06
	t1	0.53 ± 1.93	n.d.	0.39 ± 0.18	n.d.	n.d.	0.68 ± 1.16	0.34 ± 1.28	1.25 ± 3.95	0.25 ± 1.03
	t2	n.d.	n.d.	n.d.	0.29 ± 36.17	n.d.	n.d.	6.56 ± 0.89	0.71 ± 0.53	1.74 ± 0.62
	t4	n.d.	2.58 ± 2.78	18.24 ± 23.37	n.d.	n.d.	n.d.	22.40 ± 21.03	88.15 ± 1.77	89.35 ± 1.23
Fe(III)%	t0	7.92	7.92	7.92	7.92	7.92	7.92	7.92	7.92	7.92
	t1	8.04	0.00	43.65	0.00	0.00	4.49	14.02	15.29	8.19
	t2	0.00	0.00	0.00	0.33	0.00	0.00	34.27	27.93	42.84
	t4	0.00	11.36	17.92	0.00	n/a	0.00	70.60	89.00	91.96
Total Fe	t0	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35	32.60 ± 2.35
	t1	14.63 ± 0.15	2.18 ± 0.06	1.20 ± 0.25	6.32 ± 0.76	1.37 ± 0.43	22.27 ± 5.08	4.55 ± 3.17	13.72 ± 2.46	4.04 ± 0.38
	t2	157.07 ± 9.52	15.72 ± 2.58	n.d.	114.17 ± 23.76	0.88 ± 1.03	170.29 ± 4.87	93.78 ± 1.79	17.45 ± 3.34	22.09 ± 6.68
	t4	130.25 ± 1.23	18.06 ± 1.83	91.54 ± 16.82	131.66 ± 3.91	0.64 ± 0.05	59.51 ± 5.65	97.63 ± 28.43	122.47 ± 15.69	103.54 ± 10.89
FeS	t0	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36	5.24 ± 3.36
	t1	0.90 ± 1.76	1.74 ± 1.90	0.54 ± 0.76	0.96 ± 1.15	3.61 ± 0.57	2.74 ± 6.31	2.27 ± 3.77	4.45 ± 4.93	n.d.
	t2	n.d.	1.52 ± 4.72	0.71 ± 0.18	n.d.	0.81 ± 1.09	2.39 ± 5.78	54.13 ± 1.82	127.57 ± 6.68	121.02 ± 8.01
	t4	42.12 ± 2.21	n.d.	0.38 ± 25.04	n.d.	1.26 ± 0.79	70.73 ± 5.69	31.00 ± 28.43	9.31 ± 15.72	26.95 ± 10.90
Digest Fe(II)	t4	813.57 ± 26.50	762.58 ± 23.19	868.48 ± 23.17	890.19 ± 17.61	835.31 ± 22.23	928.75 ± 44.75	947.52 ± 26.42	988.56 ± 19.03	1012.40 ± 29.95
Digest Fe(T)	t4	779.56 ± 30.48	759.37 ± 23.05	861.63 ± 24.26	882.57 ± 17.55	793.81 ± 20.85	920.46 ± 45.38	939.72 ± 24.54	980.15 ± 18.73	999.80 ± 30.88
Digest Fe(III)	t4	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.

Table 4: Site 2 iron concentrations (μM). Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.

	Timepoint	Control	Kill	Mn(III)-DFOB	Manganite	Buserite	$\delta$ -MnO <sub>2</sub>	Sulfate	Fe(III)-DFOB	Nontronite	Ferrihydrite	Goethite
dFe(II)	t0	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22	0.37 ± 0.22
	t1	0.89 ± 0.05	3.01 ± 0.07	0.20 ± 0.18	0.42 ± 0.07	1.45 ± 0.07	1.13 ± 0.07	1.10 ± 0.14	0.91 ± 0.04	1.31 ± 0.35	0.78 ± 0.12	2.25 ± 0.06
	t2	1.51 ± 0.36	2.45 ± 0.01	2.10 ± 0.21	1.03 ± 0.07	3.03 ± 0.12	1.72 ± 0.27	9.45 ± 1.61	1.63 ± 2.33	12.60 ± 16.01	1.73 ± 0.24	2.04 ± 0.97
	t4	0.89 ± 0.76	3.40 ± 0.60	n.d.	0.20 ± 0.15	n.d.	8.33 ± 1.09	n.d.	4.94 ± 1.21	n.d.	n.d.	n.d.
dFe(T)	t0	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03	0.18 ± 0.03
	t1	0.79 ± 0.07	2.90 ± 0.06	n.d.	0.77 ± 0.05	0.99 ± 0.22	1.37 ± 0.30	1.06 ± 0.15	0.45 ± 0.05	1.15 ± 0.43	1.00 ± 0.24	2.27 ± 0.09
	t2	1.36 ± 0.27	2.91 ± 1.12	3.77 ± 0.20	1.00 ± 0.04	3.00 ± 0.09	1.51 ± 0.31	8.08 ± 2.63	5.38 ± 1.84	11.92 ± 15.42	3.47 ± 0.90	1.54 ± 0.85
	t4	0.80 ± 0.80	2.17 ± 0.84	n.d.	n.d.	n.d.	6.84 ± 0.44	n.d.	3.55 ± 0.78	n.d.	10.98 ± 3.16	0.44 ± 0.30
dFe(III)	t0	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
	t1	n.d.	n.d.	n.d.	0.35 ± 0.09	n.d.	0.25 ± 0.31	n.d.	n.d.	n.d.	0.22 ± 0.27	0.02 ± 0.11
	t2	n.d.	0.46 ± 1.12	1.67 ± 0.29	n.d.	n.d.	n.d.	n.d.	3.74 ± 2.97	n.d.	1.73 ± 0.93	n.d.
	t4	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	10.98 ± 3.16	0.44 ± 0.43
Fe(III)%	t0	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
	t1	0.00	0.00	0.00	45.68	0.00	17.92	0.00	0.00	0.00	22.30	0.83
	t2	0.00	15.82	44.36	0.00	0.00	0.00	0.00	69.63	0.00	50.01	0.00
	t4	0.00	0.00	n/a	0.00	n/a	0.00	n/a	0.00	n/a	100.00	100.00
Total Fe	t0	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62	22.92 ± 0.62
	t1	2.18 ± 0.61	2.33 ± 0.06	0.26 ± 0.26	1.86 ± 0.13	5.68 ± 0.43	3.49 ± 0.82	16.21 ± 2.09	0.08 ± 0.02	1.39 ± 0.19	9.05 ± 1.43	1.66 ± 0.43
	t2	1.61 ± 0.16	2.60 ± 0.28	0.04 ± 0.01	0.57 ± 0.63	4.37 ± 1.58	2.84 ± 3.01	5.27 ± 2.67	n.d.	7.30 ± 0.64	24.47 ± 5.64	2.55 ± 1.41
	t4	1.68 ± 0.40	1.72 ± 0.18	n.d.	1.19 ± 0.25	1.61 ± 0.23	20.47 ± 1.41	1.90 ± 0.11	0.52 ± 0.02	1.06 ± 0.20	19.17 ± 6.30	2.31 ± 0.17
FeS	t0	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.
	t1	0.26 ± 0.83	1.29 ± 0.36	n.d.	1.05 ± 0.66	n.d.	2.03 ± 0.82	n.d.	n.d.	1.46 ± 0.56	10.46 ± 1.49	2.63 ± 1.82
	t2	0.66 ± 0.43	0.71 ± 0.31	n.d.	1.15 ± 0.89	1.45 ± 2.92	1.29 ± 4.64	n.d.	1.82 ± 0.95	n.d.	31.66 ± 6.64	3.19 ± 4.21
	t4	0.40 ± 0.47	n.d.	0.25 ± 0.18	0.28 ± 0.40	0.17 ± 0.67	n.d.	1.53 ± 0.49	n.d.	0.36 ± 0.28	10.51 ± 7.08	2.07 ± 0.44
Digest Fe(II)	t4	647.11 ± 19.25	619.30 ± 28.85	712.30 ± 25.72	760.74 ± 81.71	704.27 ± 34.35	731.95 ± 17.34	788.20 ± 9.29	845.94 ± 10.80	805.12 ± 44.19	889.71 ± 20.41	876.78 ± 37.48
Digest Fe(T)	t4	638.78 ± 25.14	614.95 ± 27.50	707.50 ± 24.88	752.92 ± 80.32	696.36 ± 33.44	709.16 ± 19.28	781.58 ± 9.42	834.61 ± 10.44	794.77 ± 45.44	877.78 ± 20.38	869.40 ± 35.66
Digest Fe(III)	t4	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.

Table 5: Site 3 iron concentrations (μM). Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.



	Timepoint	Control	Kill	Mn(III)-DFOB	Manganite	Buserite	$\delta$ -MnO <sub>2</sub>	Sulfate	Fe(III)-DFOB	Nontronite	Ferrihydrite	Goethite
dFe(II)	t0	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05	0.25 ± 0.05
	t1	1.26 ± 0.49	2.46 ± 0.06	0.21 ± 0.07	0.56 ± 0.34	1.06 ± 0.08	n.d.	2.62 ± 0.71	12.76 ± 1.22	2.49 ± 0.32	0.95 ± 0.10	2.66 ± 0.18
	t2	123.82 ± 1.91	1.56 ± 0.03	48.42 ± 9.87	2.19 ± 0.40	89.48 ± 12.44	1.59 ± 0.22	118.42 ± 3.70	18.41 ± 13.37	6.80 ± 0.37	2.64 ± 0.27	3.46 ± 0.82
	t4	14.86 ± 2.57	3.47 ± 0.67	31.92 ± 23.21	38.31 ± 7.26	20.79 ± 0.30	n.d.	1.86 ± 0.16	1.95 ± 1.01	3.37 ± 0.54	5.04 ± 0.63	n.d.
dFe(T)	t0	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21	0.36 ± 0.21
	t1	1.24 ± 0.55	2.38 ± 0.04	n.d.	0.90 ± 1.31	0.65 ± 0.06	1.31 ± 0.26	2.61 ± 0.84	12.85 ± 1.24	2.55 ± 0.47	0.97 ± 0.20	2.75 ± 0.22
	t2	123.47 ± 1.84	1.41 ± 0.13	93.34 ± 9.80	2.22 ± 0.46	89.36 ± 12.68	1.40 ± 0.8	115.45 ± 2.51	25.92 ± 13.65	13.07 ± 0.59	3.48 ± 0.64	5.79 ± 1.26
	t4	14.61 ± 2.52	2.84 ± 1.75	31.39 ± 23.81	46.56 ± 10.07	20.66 ± 0.19	n.d.	1.54 ± 0.29	48.78 ± 2.22	16.93 ± 2.83	96.23 ± 0.24	8.00 ± 1.02
dFe(III)	t0	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22	0.11 ± 0.22
	t1	n.d.	n.d.	n.d.	0.35 ± 0.46	n.d.	1.31 ± 0.27	n.d.	0.09 ± 1.75	0.06 ± 0.57	0.02 ± 0.23	0.10 ± 0.28
	t2	n.d.	n.d.	44.92 ± 13.91	0.03 ± 0.61	n.d.	n.d.	n.d.	7.51 ± 19.11	6.27 ± 0.70	0.84 ± 0.69	2.32 ± 1.51
	t4	n.d.	n.d.	n.d.	8.25 ± 12.42	n.d.	n.d.	n.d.	46.83 ± 2.44	13.56 ± 2.88	91.19 ± 0.68	8.00 ± 1.02
Fe(III)%	t0	30.29	30.29	30.29	30.29	30.29	30.29	30.29	30.29	30.29	30.29	30.29
	t1	0.00	0.00	0.00	38.21	0.00	100.00	0.00	0.67	2.43	1.58	3.48
	t2	0.00	0.00	48.12	1.22	0.00	0.00	0.00	28.96	47.95	24.20	40.17
	t4	0.00	0.00	0.00	17.72	0.00	n/a	0.00	96.01	80.10	94.77	100.00
Total Fe	t0	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65	4.98 ± 0.65
	t1	2.69 ± 1.59	1.94 ± 0.57	0.12 ± 0.08	1.28 ± 0.42	1.18 ± 0.11	1.85 ± 0.57	4.27 ± 1.29	0.34 ± 0.06	3.36 ± 0.74	1.69 ± 0.18	2.20 ± 0.89
	t2	122.21 ± 1.89	1.59 ± 0.54	89.50 ± 5.29	3.83 ± 2.05	92.68 ± 15.83	0.44 ± 0.69	117.21 ± 2.38	44.67 ± 8.69	70.05 ± 18.01	17.25 ± 0.75	23.58 ± 1.91
	t4	12.81 ± 2.09	6.38 ± 0.04	34.61 ± 23.93	30.03 ± 4.44	19.39 ± 1.00	0.61 ± 0.04	3.61 ± 1.01	66.35 ± 6.50	16.76 ± 2.33	94.78 ± 1.49	8.10 ± 0.45
FeS	t0	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72	4.17 ± 0.72
	t1	2.72 ± 2.04	0.95 ± 1.30	n.d.	n.d.	0.65 ± 0.72	2.57 ± 1.50	4.93 ± 4.57	n.d.	1.27 ± 0.92	1.10 ± 0.89	0.40 ± 0.95
	t2	n.d.	0.45 ± 0.63	n.d.	1.13 ± 2.20	n.d.	0.70 ± 0.79	n.d.	123.15 ± 3.22	45.92 ± 18.91	97.39 ± 7.36	79.80 ± 5.63
	t4	1.13 ± 3.16	0.87 ± 1.43	12.54 ± 31.30	n.d.	n.d.	0.72 ± 0.29	1.42 ± 1.05	63.41 ± 6.71	12.77 ± 3.69	34.60 ± 5.36	12.55 ± 2.49
Digest Fe(II)	t4	624.96 ± 41.14	592.50 ± 16.45	723.31 ± 36.96	681.46 ± 18.51	709.19 ± 29.05	655.89 ± 17.76	826.06 ± 6.90	838.13 ± 23.58	811.93 ± 8.02	853.39 ± 37.24	916.63 ± 14.13
Digest Fe(T)	t4	623.71 ± 38.60	601.89 ± 16.89	721.12 ± 34.66	678.80 ± 17.65	706.02 ± 28.82	642.42 ± 26.54	819.62 ± 7.26	831.36 ± 23.42	808.76 ± 8.50	848.19 ± 34.90	902.86 ± 15.98
Digest Fe(III)	t4	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.	n.d.

Table 6: Site 4 iron concentrations (µM). Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.

Timepoint	Treatment	dFe(II)				dFe(III)				Fe(III) %			
		Site 1	Site 2	Site 3	Site 4	Site 1	Site 2	Site 3	Site 4	Site 1	Site 2	Site 3	Site 4
t0	Starting slurry	0.28 ± 0.10	0.97 ± 0.05	0.37 ± 0.22	0.25 ± 0.05	n.d.	0.08 ± 0.06	n.d.	0.11 ± 0.22	0.00	7.92	0.00	30.29
t1	Control	20.58 ± 0.15	6.07 ± 1.02	0.89 ± 0.05	1.26 ± 0.49	0.43 ± 0.36	0.53 ± 1.93	n.d.	n.d.	2.05	8.04	0.00	0.00
	Kill	2.57 ± 0.15	2.52 ± 0.02	3.01 ± 0.07	2.46 ± 0.06	n.d.	n.d.	n.d.	n.d.	0.00	0.00	0.00	0.00
	Mn(III)-DFOB			0.20 ± 0.18	0.21 ± 0.07			n.d.	n.d.			0.00	0.00
	Manganite	0.63 ± 0.28	0.51 ± 0.10	0.42 ± 0.07	0.56 ± 0.34	0.33 ± 0.37	0.39 ± 0.18	0.35 ± 0.09	0.35 ± 0.46	34.61	43.65	45.68	38.21
	Buserite	1.74 ± 0.47	4.68 ± 0.71	1.45 ± 0.07	1.06 ± 0.08	n.d.	n.d.	n.d.	n.d.	0.00	0.00	0.00	0.00
	δ-MnO <sub>2</sub>	1.13 ± 0.15	1.29 ± 0.38	1.13 ± 0.07	n.d.	n.d.	n.d.	0.25 ± 0.31	1.31 ± 0.27	0.00	0.00	17.92	100.00
	Sulfate	1.02 ± 0.09	14.49 ± 0.64	1.10 ± 0.14	2.62 ± 0.71	19.91 ± 1.06	0.68 ± 1.16	n.d.	n.d.	95.11	4.49	0.00	0.00
	Fe(III)-DFOB			0.91 ± 0.04	12.76 ± 1.22			n.d.	0.09 ± 1.75			0.00	0.67
	Nontronite	9.80 ± 3.51	2.09 ± 0.65	1.31 ± 0.35	2.49 ± 0.32	0.78 ± 4.76	0.34 ± 1.28	n.d.	0.06 ± 0.57	7.34	14.02	0.00	2.43
	Ferrihydrite	21.56 ± 9.70	6.94 ± 2.75	0.78 ± 0.12	0.95 ± 0.10	1.47 ± 13.55	1.25 ± 3.95	0.22 ± 0.27	0.02 ± 0.23	6.40	15.29	22.30	1.58
Goethite	17.40 ± 0.40	2.83 ± 0.66	2.25 ± 0.06	2.66 ± 0.18	0.12 ± 1.16	0.25 ± 1.03	0.02 ± 0.11	0.10 ± 0.28	0.67	8.19	0.83	3.48	
t2	Control	109.04 ± 17.08	134.53 ± 19.03	1.51 ± 0.36	123.82 ± 1.91	n.d.	n.d.	n.d.	n.d.	0.00	0.00	0.00	0.00
	Kill	33.46 ± 4.19	11.14 ± 0.98	2.45 ± 0.01	1.56 ± 0.03	n.d.	n.d.	0.46 ± 1.12	n.d.	0.00	0.00	15.82	0.00
	Mn(III)-DFOB			2.10 ± 0.21	48.42 ± 9.87			1.67 ± 0.29	44.92 ± 13.91			44.36	48.12
	Manganite	1.77 ± 0.69	1.91 ± 0.70	1.03 ± 0.07	2.19 ± 0.40	n.d.	n.d.	n.d.	0.03 ± 0.61	0.00	0.00	0.00	1.22
	Buserite	38.22 ± 18.71	89.07 ± 25.60	3.03 ± 0.12	89.48 ± 12.44	n.d.	0.29 ± 36.17	n.d.	n.d.	0.00	0.33	0.00	0.00
	δ-MnO <sub>2</sub>	2.21 ± 0.59	1.63 ± 0.11	1.72 ± 0.27	1.59 ± 0.22	n.d.	n.d.	n.d.	n.d.	0.00	0.00	0.00	0.00
	Sulfate	113.96 ± 10.17	163.75 ± 3.28	8.08 ± 2.63	118.42 ± 3.70	n.d.	n.d.	n.d.	n.d.	0.00	0.00	0.00	0.00
	Fe(III)-DFOB			1.63 ± 2.33	18.41 ± 13.37			3.74 ± 2.97	7.51 ± 19.11			69.63	28.96
	Nontronite	4.77 ± 0.68	12.59 ± 0.85	12.60 ± 16.01	6.80 ± 0.37	4.14 ± 1.55	6.56 ± 0.89	n.d.	6.27 ± 0.70	46.45	34.27	0.00	47.95
	Ferrihydrite	3.08 ± 0.37	1.82 ± 0.37	1.73 ± 0.24	2.64 ± 0.27	1.24 ± 0.42	0.71 ± 0.53	1.73 ± 0.93	0.84 ± 0.69	28.74	27.93	50.01	24.20
Goethite	2.75 ± 0.56	2.32 ± 0.19	2.04 ± 0.97	3.46 ± 0.82	2.00 ± 1.21	1.74 ± 0.62	n.d.	2.32 ± 1.51	42.10	42.84	0.00	40.17	
t4	Control	0.94 ± 0.60	92.49 ± 0.54	0.89 ± 0.76	14.86 ± 2.57	n.d.	n.d.	n.d.	n.d.	0.00	0.00	0.00	0.00
	Kill	52.05 ± 3.10	20.15 ± 2.49	3.40 ± 0.60	3.47 ± 0.67	7.21 ± 3.78	2.58 ± 2.78	n.d.	n.d.	12.17	11.36	0.00	0.00
	Mn(III)-DFOB			n.d.	31.92 ± 23.21			n.d.	n.d.			n/a	0.00
	Manganite	6.65 ± 0.97	83.58 ± 13.94	0.20 ± 0.15	38.31 ± 7.26	n.d.	18.24 ± 23.37	n.d.	8.25 ± 12.42	0.00	17.92	0.00	17.72
	Buserite	1.24 ± 0.16	92.30 ± 1.05	n.d.	20.79 ± 0.30	n.d.	n.d.	n.d.	n.d.	0.00	0.00	n/a	0.00
	δ-MnO <sub>2</sub>	n.d.	n.d.	8.33 ± 1.09	n.d.	n.d.	n.d.	n.d.	n.d.	n/a	n/a	0.00	n/a
	Sulfate	n.d.	11.14 ± 1.04	n.d.	1.86 ± 0.16	n.d.	n.d.	n.d.	n.d.	n/a	0.00	n/a	0.00
	Fe(III)-DFOB			4.94 ± 1.21	1.95 ± 1.01			n.d.	46.83 ± 2.44			0.00	96.01
	Nontronite	n.d.	9.33 ± 0.21	n.d.	3.37 ± 0.54	n.d.	22.40 ± 21.03	n.d.	13.56 ± 2.88	n/a	70.60	n/a	80.10
	Ferrihydrite	n.d.	10.90 ± 1.16	n.d.	5.04 ± 0.63	21.01 ± 5.68	88.15 ± 1.77	10.98 ± 3.16	91.19 ± 0.68	100.00	89.00	100.00	94.77
Goethite	n.d.	7.81 ± 0.73	n.d.	n.d.	n.d.	89.35 ± 1.23	0.44 ± 0.43	8.00 ± 1.02	n/a	91.96	100.00	100.00	

Table 7: Dissolved iron concentrations (μM) from all four sites. Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.

Timepoint	Treatment	Total Fe				FeS			
		Site 1	Site 2	Site 3	Site 4	Site 1	Site 2	Site 3	Site 4
t0	Starting slurry	36.06 ± 0.19	32.60 ± 2.35	22.92 ± 0.62	4.98 ± 0.65	n.d.	5.24 ± 3.36	n.d.	4.17 ± 0.72
t1	Control	24.50 ± 4.01	14.63 ± 0.15	2.18 ± 0.61	2.69 ± 1.59	6.70 ± 13.06	0.90 ± 1.76	0.26 ± 0.83	2.72 ± 2.04
	Kill	1.02 ± 0.02	2.18 ± 0.06	2.33 ± 0.06	1.94 ± 0.57	1.04 ± 5.89	1.74 ± 1.90	1.29 ± 0.36	0.95 ± 1.30
	Mn(III)-DFOB			0.26 ± 0.26	0.12 ± 0.08			n.d.	n.d.
	Manganite	1.44 ± 0.58	1.20 ± 0.25	1.86 ± 0.13	1.28 ± 0.42	1.66 ± 1.04	0.54 ± 0.76	1.05 ± 0.66	n.d.
	Buserite	2.72 ± 0.16	6.32 ± 0.76	5.68 ± 0.43	1.18 ± 0.11	1.91 ± 1.29	0.96 ± 1.15	n.d.	0.65 ± 0.72
	δ-MnO <sub>2</sub>	15.22 ± 5.48	1.37 ± 0.43	3.49 ± 0.82	1.85 ± 0.57	n.d.	3.61 ± 0.57	2.03 ± 0.82	2.57 ± 1.50
	Sulfate	29.38 ± 1.32	22.27 ± 5.08	16.21 ± 2.09	4.27 ± 1.29	17.80 ± 2.71	2.74 ± 6.31	n.d.	4.93 ± 4.57
	Fe(III)-DFOB			0.08 ± 0.02	0.34 ± 0.06			n.d.	n.d.
	Nontronite	15.14 ± 3.57	4.55 ± 3.17	1.39 ± 0.19	3.36 ± 0.74	6.11 ± 4.48	2.27 ± 3.77	1.46 ± 0.56	1.27 ± 0.92
	Ferrihydrite	30.14 ± 6.18	13.72 ± 2.46	9.05 ± 1.43	1.69 ± 0.18	1.95 ± 7.27	4.45 ± 4.93	10.46 ± 1.49	1.10 ± 0.89
Goethite	16.86 ± 13.43	4.04 ± 0.38	1.66 ± 0.43	2.20 ± 0.89	19.82 ± 19.85	n.d.	2.63 ± 1.82	0.40 ± 0.95	
t2	Control	117.64 ± 13.13	157.07 ± 9.52	1.61 ± 0.16	122.21 ± 1.89	6.27 ± 19.67	n.d.	0.66 ± 0.43	n.d.
	Kill	47.62 ± 8.19	15.72 ± 2.58	2.60 ± 0.28	1.59 ± 0.54	7.43 ± 13.46	1.52 ± 4.72	0.71 ± 0.31	0.45 ± 0.63
	Mn(III)-DFOB			0.04 ± 0.01	89.50 ± 5.29			n.d.	n.d.
	Manganite	1.41 ± 1.10	n.d.	0.57 ± 0.63	3.83 ± 2.05	1.23 ± 1.39	0.71 ± 0.18	1.15 ± 0.89	1.13 ± 2.20
	Buserite	50.61 ± 8.53	114.17 ± 23.76	4.37 ± 1.58	92.68 ± 15.83	0.10 ± 11.26	n.d.	1.45 ± 2.92	n.d.
	δ-MnO <sub>2</sub>	2.54 ± 1.51	0.88 ± 1.03	2.84 ± 3.01	0.44 ± 0.69	1.12 ± 1.99	0.81 ± 1.09	1.29 ± 4.64	0.70 ± 0.79
	Sulfate	114.88 ± 9.25	170.29 ± 4.87	5.27 ± 2.67	117.21 ± 2.38	n.d.	2.39 ± 5.78	n.d.	n.d.
	Fe(III)-DFOB			n.d.	44.67 ± 8.69			1.82 ± 0.95	123.15 ± 3.22
	Nontronite	45.50 ± 8.71	93.78 ± 1.79	7.30 ± 0.64	70.05 ± 18.01	56.62 ± 21.62	54.13 ± 1.82	n.d.	45.92 ± 18.91
	Ferrihydrite	28.06 ± 2.34	17.45 ± 3.34	24.47 ± 5.64	17.25 ± 0.75	122.52 ± 2.39	127.57 ± 6.68	31.66 ± 6.64	97.39 ± 7.36
Goethite	12.67 ± 0.72	22.09 ± 6.68	2.55 ± 1.41	23.58 ± 1.91	45.76 ± 11.47	121.02 ± 8.01	3.19 ± 4.21	79.80 ± 5.63	
t4	Control	1.46 ± 0.36	130.25 ± 1.23	1.68 ± 0.40	12.81 ± 2.09	1.08 ± 0.96	42.12 ± 2.21	0.40 ± 0.47	1.13 ± 3.16
	Kill	43.46 ± 2.93	18.06 ± 1.83	1.72 ± 0.18	6.38 ± 0.04	1.04 ± 5.89	n.d.	n.d.	0.87 ± 1.43
	Mn(III)-DFOB			n.d.	34.61 ± 23.93			0.25 ± 0.18	12.54 ± 31.30
	Manganite	5.65 ± 1.29	91.54 ± 16.82	1.19 ± 0.25	30.03 ± 4.44	2.24 ± 3.10	0.38 ± 25.04	0.28 ± 0.40	n.d.
	Buserite	2.88 ± 0.29	131.66 ± 3.91	1.61 ± 0.23	19.39 ± 1.00	3.70 ± 0.88	n.d.	0.17 ± 0.67	n.d.
	δ-MnO <sub>2</sub>	0.87 ± 0.04	0.64 ± 0.05	20.47 ± 1.41	0.61 ± 0.04	1.56 ± 0.25	1.26 ± 0.79	n.d.	0.72 ± 0.29
	Sulfate	1.71 ± 0.13	59.51 ± 5.65	1.90 ± 0.11	3.61 ± 1.01	5.35 ± 0.58	70.73 ± 5.69	1.53 ± 0.49	1.42 ± 1.05
	Fe(III)-DFOB			0.52 ± 0.02	66.35 ± 6.50			n.d.	63.41 ± 6.71
	Nontronite	1.75 ± 0.78	97.63 ± 28.43	1.06 ± 0.20	16.76 ± 2.33	0.58 ± 0.91	31.00 ± 28.43	0.36 ± 0.28	12.77 ± 3.69
	Ferrihydrite	28.48 ± 4.83	122.47 ± 15.69	19.17 ± 6.30	94.78 ± 1.49	39.07 ± 13.60	9.31 ± 15.72	10.51 ± 7.08	34.60 ± 5.36
Goethite	1.54 ± 0.14	103.54 ± 10.89	2.31 ± 0.17	8.10 ± 0.45	0.86 ± 0.29	26.95 ± 10.90	2.07 ± 0.44	12.55 ± 2.49	

Table 8: Particulate iron concentrations (µM) from all four sites. Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.

Treatment	Digest Fe(II)				Digest Fe(III)			
	Site 1	Site 2	Site 3	Site 4	Site 1	Site 2	Site 3	Site 4
Control	648.15 ± 110.89	813.57 ± 26.50	647.11 ± 19.25	624.96 ± 41.14	n.d.	n.d.	n.d.	n.d.
Kill	702.79 ± 19.07	762.58 ± 23.19	619.30 ± 28.85	592.50 ± 16.45	n.d.	n.d.	n.d.	n.d.
Mn(III)-DFOB			712.30 ± 25.72	723.31 ± 36.96			n.d.	n.d.
Manganite	812.03 ± 29.12	868.48 ± 23.17	760.74 ± 81.71	681.46 ± 18.51	n.d.	n.d.	n.d.	n.d.
Buserite	853.60 ± 22.06	890.19 ± 17.61	704.27 ± 34.35	709.19 ± 29.05	n.d.	n.d.	n.d.	n.d.
δ-MnO <sub>2</sub>	780.79 ± 26.16	835.31 ± 22.23	731.95 ± 17.34	655.89 ± 17.76	n.d.	n.d.	n.d.	n.d.
Sulfate	919.06 ± 9.64	928.75 ± 44.75	788.20 ± 9.29	826.06 ± 6.90	n.d.	n.d.	n.d.	n.d.
Fe(III)-DFOB			845.94 ± 10.80	838.13 ± 23.58			n.d.	n.d.
Nontronite	928.62 ± 33.21	947.52 ± 26.42	805.12 ± 44.19	811.93 ± 8.02	n.d.	n.d.	n.d.	n.d.
Ferrihydrite	953.63 ± 23.95	988.56 ± 19.03	889.71 ± 20.41	853.39 ± 37.24	n.d.	n.d.	n.d.	n.d.
Goethite	957.58 ± 9.82	1012.40 ± 29.95	876.78 ± 37.48	916.63 ± 14.13	n.d.	n.d.	n.d.	n.d.

Table 9: Iron digest concentrations (μM) from all four sites at the end of the experiment. Errors represent the standard deviations between three replicate incubation tubes measured in triplicate. n.d. = below detection limit.

Addition	Balanced reaction	Free energy (kJ mol CH <sub>4</sub> <sup>-1</sup> )	
		ΔG <sup>0</sup>	ΔG
Sulfate	CH <sub>4</sub> + SO <sub>4</sub> <sup>2-</sup> → HCO <sub>3</sub> <sup>-</sup> + HS <sup>-</sup> + H <sub>2</sub> O	-32.94	-32.06
Mn(III)-DFOB	CH <sub>4</sub> + 8Mn(III)-DFOB + 3H <sub>2</sub> O → HCO <sub>3</sub> <sup>-</sup> + 8Mn(II)-DFOB + 9H <sup>+</sup>	-650.96	-773.64
Manganite	CH <sub>4</sub> + 8MnOOH + 15H <sup>+</sup> → HCO <sub>3</sub> <sup>-</sup> + 8Mn <sup>2+</sup> + 13H <sub>2</sub> O	-998.15	-611.76
Birnessite	CH <sub>4</sub> + 4MnO <sub>2</sub> + 7H <sup>+</sup> → HCO <sub>3</sub> <sup>-</sup> + 4Mn <sup>2+</sup> + 5H <sub>2</sub> O	-550.31	-376.03
δ-MnO <sub>2</sub>	CH <sub>4</sub> + 4MnO <sub>2</sub> + 7H <sup>+</sup> → HCO <sub>3</sub> <sup>-</sup> + 4Mn <sup>2+</sup> + 5H <sub>2</sub> O	-790.31	-567.22
Fe(III)-DFOB	CH <sub>4</sub> + 8Fe(III)-DFOB + 3H <sub>2</sub> O → HCO <sub>3</sub> <sup>-</sup> + 8Fe(II)-DFOB + 9H <sup>+</sup>	-26.07	-530.55
Nontronite	CH <sub>4</sub> + 8Fe(III)-clay + 3H <sub>2</sub> O → HCO <sub>3</sub> <sup>-</sup> + 8Fe(II)-clay + 9H <sup>+</sup>	-560.87	-938.08
Ferrihydrite	CH <sub>4</sub> + 8Fe(OH) <sub>3</sub> + 15H <sup>+</sup> → HCO <sub>3</sub> <sup>-</sup> + 8Fe <sup>2+</sup> + 21H <sub>2</sub> O	-496.15	-109.76
Goethite	CH <sub>4</sub> + 8FeOOH + 15H <sup>+</sup> → HCO <sub>3</sub> <sup>-</sup> + 8Fe <sup>2+</sup> + 13H <sub>2</sub> O	-357.91	28.48

Table 10: Balanced reaction for AOM and Gibbs free energy calculations for the electron acceptors added in this study. Nontronite calculation assumes Fe<sup>3+</sup> was reduced in place without significantly disturbing the mineral structure.

Addition	Theoretical energy yield (J cm <sup>-3</sup> yr <sup>-1</sup> )			
	Site 1	Site 2	Site 3	Site 4
Sulfate	0.17 ± 0.04	0.11 ± 0.02	1.06 ± 0.07	0.12 ± 0.01
Mn(III)-DFOB			8.56 ± 1.96	2.02 ± 0.23
Manganite	0.71 ± 0.20	0.95 ± 0.13	6.65 ± 0.26	1.16 ± 0.17
Birnessite	1.01 ± 0.09	0.97 ± 0.08	3.35 ± 0.33	0.85 ± 0.08
δ-MnO <sub>2</sub>	0.48 ± 0.18	0.64 ± 0.16	1.24 ± 0.25	0.56 ± 0.17
Fe(III)-DFOB			9.17 ± 0.50	1.47 ± 0.11
Nontronite	4.35 ± 1.03	2.00 ± 0.19	16.55 ± 2.62	2.48 ± 0.26
Ferrihydrite	0.44 ± 0.09	0.28 ± 0.03	1.40 ± 0.13	0.35 ± 0.07
Goethite				

Table 11: Theoretical energy yields, assuming only the added electron acceptor is utilized for AOM.

Environment	Rate	Description	Reference
Marine	6 - 14 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Marine methane-seep sediments, Eel River Basin	Beal et al. 2009
	1.32 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Brackish coastal sediments, Bothnian Sea	Egger et al. 2015
	59 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Metalliferous hydrothermal sediments, Chowder Hill	Wankel et al. 2012
	n/a	Marine sediments, Argentine Basin	Riedinger et al. 2014
	n/a	Brackish coastal sediments, Georgia	Segarra et al. 2013
	1 - 33 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Marine methane-seep sediments, Cascadia Margin	<i>This study</i>
Freshwater	13 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$ *	Freshwater sediments from an iron-rich lake, Lake Øm	Norði et al. 2013
	1.3 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Freshwater sediments from a deep lake, Lake Kinneret	Sivan et al. 2011
	n/a	Crude oil-contaminated groundwater near Bemidji	Amos et al. 2012
	n/a	Sediments from a mud volcano, eastern Taiwan	Chang et al. 2012
	n/a	Fresh water from a deep ferruginous lake, Lake Matano	Crowe et al. 2011
	n/a	Freshwater sediments from an iron-rich lake, Lake Øm	Mostovaya et al. 2021
	n/a	Freshwater sediments, Lake Baikal	Torres et al. 2014

Table 12: Rates of metal-AOM measured in various environments (modified from He et al. 2018). Wankel et al. 2012 and Norði et al. 2013 rates are the maximum rates reported in these publications. \* includes sulfate-AOM

Metal oxide/complex	Sample	Rate	Reference
Ferrihydrite	Marine sediments, Eel River Basin	6 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Beal et al. 2009
	Enrichment from freshwater sediment, Australia	23 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Cai et al. 2018
	Coastal sediments, Bothnian Sea	1.3 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Egger et al. 2015
	Culture of nitrate-AOM	144 $\mu\text{mol CO}_2 \text{ g}_{(\text{protein})}^{-1} \text{ d}^{-1}$	Ettwig et al. 2016
	Co-culture of nitrate-AOM and <i>S. oneidensis</i> MR-1	29 $\mu\text{mol CH}_4 \text{ g}_{(\text{biomass})}^{-1} \text{ d}^{-1}$	Fu et al. 2016
	Culture of nitrate-AOM	0 $\mu\text{mol CH}_4 \text{ g}_{(\text{biomass})}^{-1} \text{ d}^{-1}$	Fu et al. 2016
	Culture from Cai et al. 2018	1.1 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Li et al. 2021
	Brackish salt marsh sediment, Georgia	1.4 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Segarra et al. 2013
	Freshwater tidal creek sediment, Georgia	4.6 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Segarra et al. 2013
	Marine methane-seep sediments, Cascadia Margin	3 - 13 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	<i>This study</i>
Goethite/iron oxyhydroxide	Marine sediments, Eel River Basin	0 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Beal et al. 2009
	Culture from Cai et al. 2018	464 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Li et al. 2021
	Freshwater sediments, Lake Kinneret	1.3 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Sivan et al. 2011
	Marine methane-seep sediments, Cascadia Margin	2 - 15 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	<i>This study</i>
Magnetite	Culture from Cai et al. 2018	330 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Li et al. 2021
Fe(III)-citrate	Culture of nitrate-AOM	1920 $\mu\text{mol CO}_2 \text{ g}_{(\text{protein})}^{-1} \text{ d}^{-1}$	Ettwig et al. 2016
	Culture of sulfate-AOM	290 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Scheller et al. 2016
	Enrichment from freshwater sediment, Zoibe wetland	1410 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Chen et al. 2022
Fe(III)-EDTA	Culture of sulfate-AOM	44 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Scheller et al. 2016
Fe(III)-NTA	Culture of sulfate-AOM	15 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Scheller et al. 2016
Bimessite	Marine sediments, Eel River Basin	14 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	Beal et al. 2009
	Culture of nitrate-AOM	504 $\mu\text{mol CO}_2 \text{ g}_{(\text{protein})}^{-1} \text{ d}^{-1}$	Ettwig et al. 2016
	Culture from Cai et al. 2018	16 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Leu et al. 2020
	Brackish salt marsh sediment, Georgia	0.88 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Segarra et al. 2013
	Freshwater tidal creek sediment, Georgia	1.3 $\mu\text{mol CH}_4 \text{ cm}^{-3} \text{ yr}^{-1}$	Segarra et al. 2013
	Marine methane-seep sediments, Cascadia Margin	2 - 9 $\mu\text{mol CO}_2 \text{ cm}^{-3} \text{ yr}^{-1}$	<i>This study</i>

Table 13: Rates of metal-AOM from laboratory experiments using a variety of metal oxides or metal-ligand complexes (modified from He et al. 2018).

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## 5. Conclusion

In nature, abiotic and biotic reactions are often intertwined and rarely involve only a single element. The restrictions of scientific study require us to simplify and disentangle these processes in order to perform experiments with clear parameters. However, there are risks to systematically oversimplifying experiments and models to include only biotic processes and/or only a single element. The work of this thesis demonstrates that coupled cycling reactions are worthy of greater attention and that their study may illuminate important processes occurring in nature. Here, I summarize the results of the three data chapters and provide suggestions for future steps.

In Chapter 2, I presented results of an isotopic study of the abiotic oxidation of nitrite to nitrate by manganese(III)-pyrophosphate (Mn(III)-PP). An inverse isotope effect of  $-19.9 \pm 0.7\text{‰}$  was measured between the  $\delta^{15}\text{N}$  of nitrite consumed and nitrate produced over a range of environmentally relevant pH values (5-8). Through the addition of mildly  $^{15}\text{N}$  enriched nitrate at the beginning of the reaction, I demonstrate that this inverse isotope effect is kinetic in nature and that no back-reaction occurs. These results are widely congruent with that of its biological analog during nitrification, which also has an inverse kinetic isotope effect of similar magnitude. Experiments in  $^{18}\text{O}$ -labeled water further showed that water is the source of the additional oxygen atom in nitrate associated with an isotope effect of  $+20.3 \pm 1.5\text{‰}$ , again comparable to that of nitrite-oxidizing organisms. Additionally, I showed that the reaction is second-order with respect to Mn(III)-PP and first order with respect to nitrous acid; thus the reaction rate falls with increasing pH. Finally, the reaction was found to be “agnostic” to oxygen; that is, the rate of reaction is unaffected by the presence or absence of oxygen, suggesting ligand bound Mn(III) could oxidize nitrite in the environment even under functionally anoxic conditions. While this study was undertaken in a laboratory environment, these results suggest that results of anoxic nitrification in the environment could in fact be due to abiotic reactions which do not necessarily require oxygen as biological nitrification does. The similarity in isotope effect magnitude and direction to the corresponding biotic reactions also suggests reactions between Mn(III)-L and nitrite would go unnoticed by conventional stable isotope approaches.

There remain several open questions from Chapter 2. Firstly, Mn(III)-L complexes have not been well characterized and are thought to contain complex mixtures of humic substances (Oldham et

al. 2015). While Mn(III)-PP is seen as a model ligand, it is unclear what proportion of natural Mn(III)-L complexes also react with nitrite, and if so, what their rates of reactions would be (Qian et al. 2019). Nitrite is also a reactive species involved in several biological nitrogen cycling processes, including nitrification, denitrification, and anammox (Gruber 2008). It is unclear if the rate of reaction of abiotic oxidation by Mn(III)-L could compete with these biotic reactions. While the results of Chapter 2 suggest reactions between Mn(III)-L and nitrite could occur in the environment, further studies would be necessary to determine if this reaction is occurring in nature and, if so, to what extent. Estuarine environments, which can experience high concentrations of both nitrite and Mn(III)-L would be a probable location to begin environmental investigations of the process (Madison et al. 2013; Oldham et al. 2017). Lakes containing ferromanganese nodules might also be likely locations to investigate the potential for this reaction. For instance, Second Connecticut Lake contains abundant ferromanganese nodules and has an average pH of 6.6, which are conditions which would theoretically favor this reaction (Asikainen and Werle 2007). Incubations could be conducted in these waters using  $^{15}\text{N}$ -labeled nitrite to measure rates of nitrite oxidation in filter-sterilized vs unfiltered water to separate abiotic and biotic nitrite oxidation. This approach yields “potential” rates since the addition of nitrite perturbs the system. Further experimentation in a variety of ecosystems would be necessary to determine the potential environmental relevance of this reaction. Overall, the results of this chapter open avenues for further exploration of “anoxic nitrification” in the environment and suggest that Mn(III)-L may play an important role in impacting the nitrogen cycle in natural waters of  $\text{pH} < 7$ .

In Chapter 3, I reported abiotic conversion of hydroxylamine to nitrous oxide by manganese(III)-PP (Mn(III)-PP) in artificial seawater. The site preference of the nitrous oxide was found to be  $+35.5 \pm 0.6\%$ , identical to that produced by ammonia-oxidizing organisms. In addition to nitrous oxide, nitrite and another product (presumed to be dinitrogen gas) were also formed. The proportion of products was found to vary with the starting ratio of reactants with a peak in nitrous oxide production at 3:1 Mn(III)-PP to hydroxylamine. The potential for “hybrid” production of  $\text{N}_2\text{O}$  (i.e., two N atoms having different precursor sources) was investigated through addition of isotopically distinct nitrite added at the beginning of the reaction; however, this signal was not found in the nitrous oxide, indicating no further reaction of nitrite to nitrous oxide. Additionally, further consumption of nitrous oxide was ruled out due to the consistent site preference throughout



reaction progress and starting reactant ratios. The results of this chapter suggest abiotic formation of nitrous oxide by manganese(III) could occur in nature but also be thus far unnoticed due to the congruence of the isotope effect with biotic reactions. This study supports others that have suggested nitrous oxide production from nitrifiers may be a largely mixed biotic-abiotic process.

In the future, in order to fully close nitrogen mass-balance in this reaction, nitrogen gas and/or ammonium production would need to be quantified. As dinitrogen was present in the headspace of the experiments presented, it was not possible to determine if it was a reaction product. Changing the inert gas used to purge from nitrogen to helium, for example, would allow for quantification of  $N_2$ . Ammonium concentration can be quantified through persulfate oxidation, although this method often results in a high blank (Knapp et al. 2005). Measurement of Mn(III)-PP concentration using the leucoberberlin blue before and after reaction with hydroxylamine would also allow for more discrete redox accounting, which could further help to identify the “missing N.” I also plan to perform future experiments in the presence of oxygen to determine if the reaction is able to proceed under oxic conditions. If the reaction produces  $N_2$  in the presence of oxygen, that would contrast with conventional understanding the  $N_2$  is generally produced by anammox and denitrification under anoxic conditions (Devol 2015). As in Chapter 2, a wider variety of Mn(III)-L complexes could also be tested to ensure natural Mn(III)-L is being emulated as closely as possible. Mn(IV) oxides have also been shown to react with  $NH_2OH$ , though to the best of my knowledge the isotopic composition of the resulting  $N_2O$  has not been characterized which could provide another interesting avenue of exploration (Cavazos et al. 2018). Further lab experiments could also investigate the potential of coupled biotic/abiotic reaction, by adding Mn(III)-L to cultures of AOA, AOB, and/or comammox bacteria and measure the resulting products (particularly  $N_2O$ ) compared to controls with no added Mn(III)-L. This study also highlights the importance of abiotic controls when performing culture experiments. It is essential to perform abiotic media controls not only with the reactant (in this case  $NH_3$ ), but also with any reactive intermediates that are formed by microbes (in this case  $NH_2OH$ ). Similar incubation studies in natural waters with high natural rates of nitrification, such as above the oxic/anoxic interface in oxygen deficient zones would help to establish the relevance of the reaction in the environment.

The results of both Chapter 2 and 3 shed light on abiotic coupled cycling reactions between Mn and N. However, they are by no means exhaustive studies and there remains much important work to be done in this area. Firstly, pyrophosphate is only one among many potential ligands that can complex Mn(III) which may have different degrees of reactivity. Relatively little is known at this time about the identities of the organics able to complex Mn(III) which means most studies are performed with model ligands such as pyrophosphate or DFOB. These studies both focused on Mn(III)-L complexes; however, Mn(III,IV)oxyhydroxides are also commonly found in the environment could potentially react with many nitrogen species. Natural manganese oxides exist in many different mineral forms with varying reactivities. These chapters have also highlighted some of the challenges associated with studying coupled cycling reactions; for instance, that the potential for redox reactions between Mn and N also can result in interferences in the methods used to measure their concentrations. This remains a primary area of concern when performing studies of this nature and requires extensive testing and the use of multiple types of controls.

In Chapter 4, I described experiments designed to measure rates of anaerobic oxidation of methane (AOM) in presence of a variety of electron acceptors including sulfate and a variety of oxidized forms of manganese and iron ranging from solid mineral phases to dissolved ligand-bound species. Cold-seep sediments were collected from the Cascadia Margin and incubated for 8.5 months using  $^{13}\text{C}$  to track the formation of carbon dioxide from methane. Generally, rates were comparable to those measured in other studies of cold-seep environments, however, in contrast to previous work AOM rates were not consistently elevated in the presence of additional oxidized iron and manganese. In fact, some metal treatments were found to depress rates of AOM below that of the unamended control treatment. It was hypothesized that these findings may be attributed to increased energy yields per mole of methane consumed compared to traditional sulfate-AOM and an inability of the slow-growing microbial community to adapt to the increase in new electron acceptors. While the result that metal additions depressed rates of AOM contrasted with previous work, I also did not age sediments before initiating the experiment as other studies did, thus slowly removing sulfate and allowing the community to adapt alongside. Generally, the results of my study suggest that microbes performing metal-AOM may not be able to take full advantage of a high input of oxidized metals without a period of adjustment.

Results of 16S rRNA extractions performed by collaborators will need to be incorporated into this study and may shed further light on any shifts in community composition. If community composition was not significantly altered between the initiation and end of the study, this would support the hypothesis that the microbial community was unable to quickly adapt to take advantage of provided oxidized metal sources. Furthermore, examination of the differences between treatments could lead to greater understanding of if community composition was altered depending on the particular mineral or complexed species added. Future studies could incorporate pre-aging of sediments or selection of locations already low in sulfate in order to maximize the ability to measure rates of metal-AOM. Additionally, new experiments would benefit from utilization of an IRMS prep system designed to process DIC samples which would minimize error in measurements.

Taken as a whole, this thesis illuminates both the complexity and necessity of studying coupled cycling reactions. While these experiments are often more difficult to perform than those that focus solely on one element, the insights gleaned from examining the interactions between multiple elements can be immensely rewarding.

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