

A MATHEMATICAL MODEL OF THE R-H VACUUM  
DEGASSING SYSTEM

by

Kazuro Shirabe

B. Eng. (Mechanical Engineering)  
Kyoto University (1972)

M. Eng. (Mechanical Engineering)  
Kyoto University (1974)

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Signature of Author Signature redacted  
Department of Materials Science  
and Engineering, May 8, 1981

Certified by Signature redacted  
Julian Szekely  
Thesis Supervisor

Accepted by Signature redacted  
Regis M. Pellox  
Chairman, Departmental Committee  
on Graduate Students

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KAZURO SHIRABE

Submitted to the Department of Materials Science  
and Engineering on May 8, 1981  
in partial fulfillment of the requirements for  
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### ABSTRACT

A mathematical model has been developed to describe the fluid flow field, the turbulence parameters and the rate at which oxide inclusion particles are removed by coalescence in an R-H Vacuum Degassing Unit.

The problem is stated through the turbulent Navier-Stokes equations, the  $k-\epsilon$  model for the turbulent viscosity and a coalescence mode.

The governing equations are solved numerically and a population balance model is being employed to represent the size distribution of the oxide particles.

The computed results indicate that the R-H unit is an excellent mixer and that the principal mechanism of the coalescence process is the adequate supply of the material contained in the ladle to the locations in the vicinity of the "down-leg" where the rate of turbulent energy dissipation is the greatest.

The computed results also show that the spatial distribution of particles of different size is quite uniform. Finally, the overall deoxidation rates predicted by the model appear to be in agreement with rates observed in industrial practice.

Thesis supervisor: Dr. Julian Szekely

Title: Professor of Materials Engineering

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## CHAPTER 1

### Introduction

In recent years there has been a growing interest in "clean steel" production because the oxide particles which are formed during deoxidizing process adversely affect the mechanical properties of the products. The studies on rate phenomena of deoxidation have been made by the many investigators. Theoretical considerations suggest that the factors influencing the growth and floatation of inclusions, i.e. deoxidation products, are complex, however the extent of inclusion growth by Brownian motion and Ostwald ripening is insignificant. On the basis of available experimental results, the rate of deoxidation is enhanced by the highly agitated melts in which the collision frequency is more rapid than in stagnant melts. The concept of the collision model in a turbulent field had been investigated by the researchers of meteorology or aerosol science. A simple application of this coagulation theories to the present problem seems to lead a reasonable agreement with experimental results.

The R-H vacuum degassing system has gained a widespread acceptance for decades due to its capacity of gaseous impurities removal and high mixing. At present the R-H treatment is employed not only to remove these impurities but also to gain the high mixing rate, i.e. to produce a strong turbulent field. The R-H unit makes it possible to achieve the rapid removal rate of oxide particles from the melt.

The purpose of this thesis is to make the attempt to simulate the deoxidation process in R-H unit by combining a turbulence theory and  $O_2$  particle coagulation theory.

The work to be described in this thesis represents the attempts toward a predictive model for flow and deoxidation characteristics of R-H de-

gassing process. The model for the oxide particle coalescence is employed in order to simulate the deoxidation process.

This thesis, is divided into six chapters.

In chapter 2 a literature survey is presented, which reviews the particle movement in turbulent flow, the particle population balance, the particle deposition theory, and the particle coalescence theory. The available turbulence model are also surveyed.

Chapter 3 gives the formulation of the mathematical model. After describing the R-H degassing unit and discussing the assumption made, the general form of the governing differential equations is given and the coefficients and the source term are represented.

In chapter 4 the numerical technique is outlined which was employed to solve the differential equations.

In Chapter 5 computed results on fluid field and particle distribution are discussed. The rate of deoxidation in R-H degasser is also treated here.

Finally, concluding remarks and some suggestions for future work are made in chapter 6.

## Chapter 2 LITERATURE SURVEY

In this chapter, the R-H degassing system is first described briefly. Next, the deoxidation mechanism is reviewed. In the later part of this chapter, the mathematical models for the coalescence frequency, the particle population balance, the turbulent flow and the particle deposition are described.

### 2.1 R-H Vacuum Degasser

The Ruhrstahl-Heraeus vacuum degassing process was originally developed in order to remove the gaseous impurities whose solubility in steel melts decrease under vacuum. This system has been useful for removing impurities like hydrogen and nitrogen which have an adverse effect on the mechanical properties of the final product. In addition the vacuum atmosphere accelerated the reaction between dissolved carbon and oxygen, so that some effects on decarburization may be expected. Another benefit of using the R-H system is that it allows a better yield of deoxidizers or other alloying additions because the tendency to oxidize is reduced under vacuum.

In the R-H degassing process, as shown in Fig. 2.1, two legs are immersed in a steel melt and an inert gas is injected into one leg (called the up-leg). The injected bubbles induced a buoyancy force which produces a recirculating flow through the vacuum vessel and ladle. This mixing effect is considerably larger than with argon stirring or other mixing arrangements [2-3]. Several reports were published to determine the recirculation rate in this system, mostly from laboratory scale models or industrial scale experiments [1,4]. An understanding of the recirculation rate is very important in order to obtain optimal gas flow rate and other operational parameters. Some extensive work has been done to define the state of mixing in R-H units and theoretical predictions regarding the time required for dispersion have been

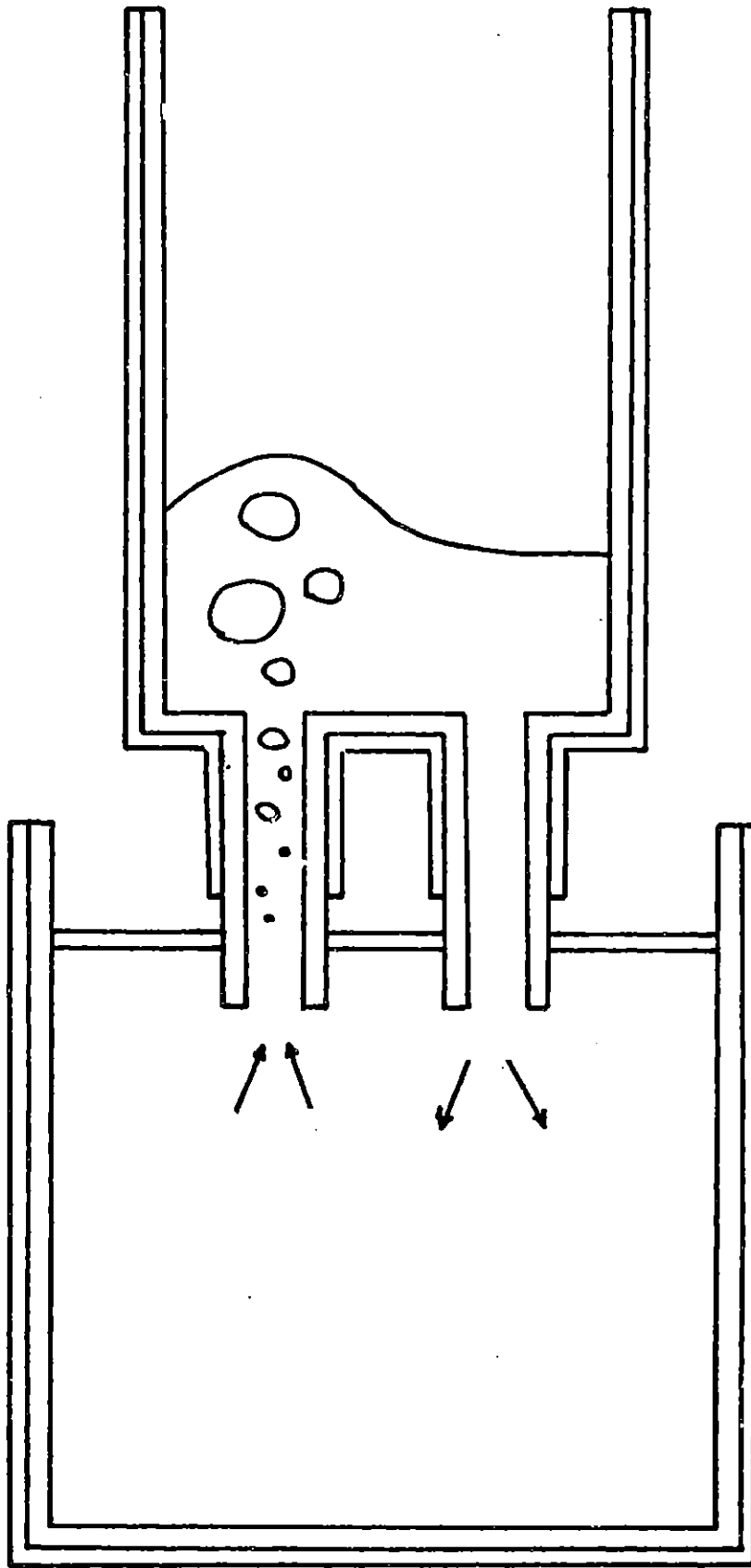


Fig. 2.1 Schematic diagram of the R-H degasser

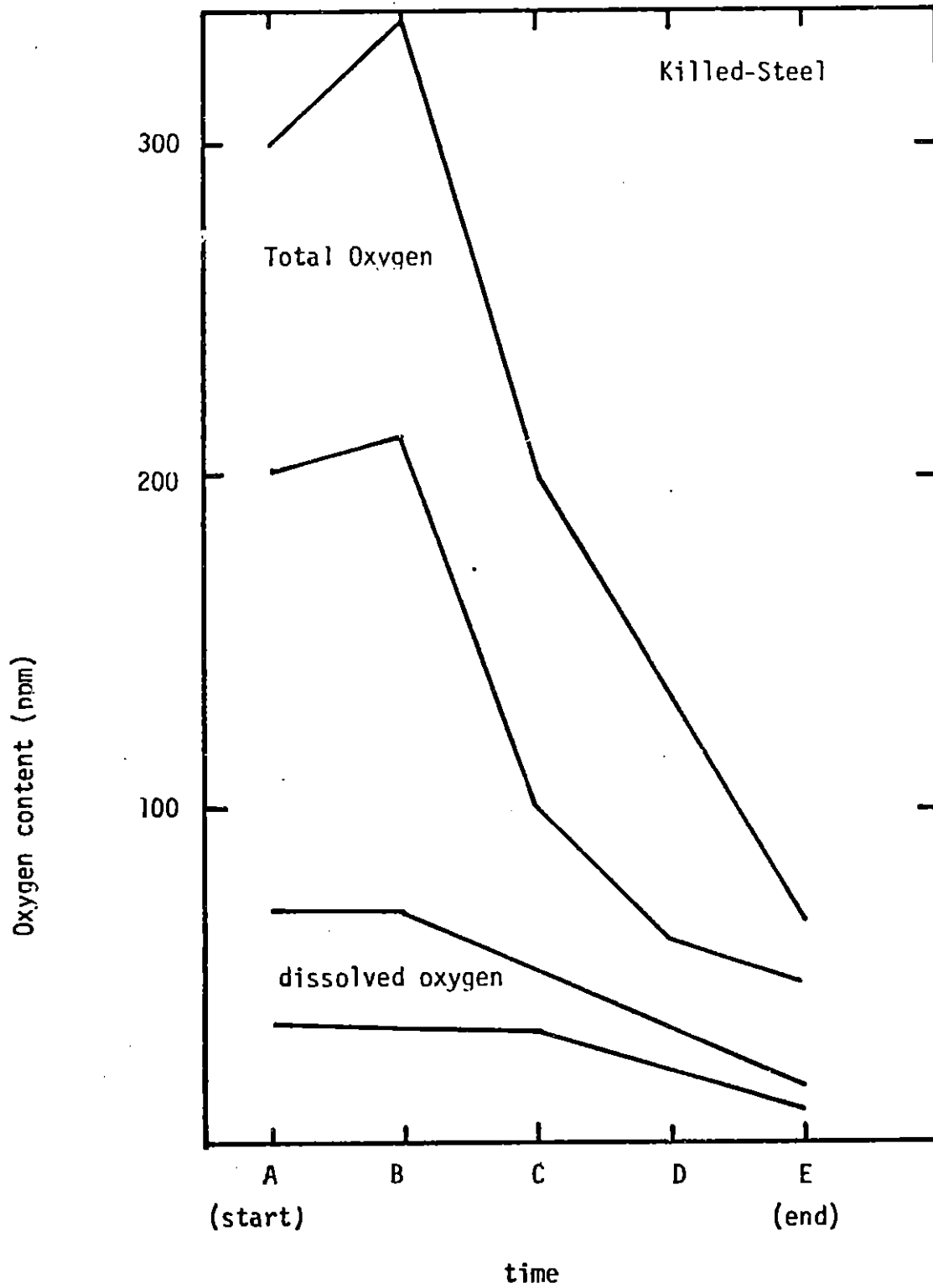


Fig. 2.2 Schematic representation of total oxygen and dissolved oxygen

made [1]. These predictions seem to be in good agreement with experimentally obtained time response curves.

This mixing capability gives another advantage to the R-H system in addition to the effective dispersion of additions: the coalescence and floatation of inclusions. The effect is not unique to this system, but common to the processes in which a steel melt is strongly agitated by forced convection (e.g. ASEA-SKF, [5] Argon stirred ladles, or TN-method). However, a few investigations have been done regarding the turbulent characteristics in R-H units and their effect on the removal of inclusions.

The decrease of inclusions is shown schematically in Fig. 2.2. Since various additions are made during treatment, it is difficult to deduce the effect of mixing on the rate of deoxidation. However, the total oxygen content increases slightly during the first stage and then decreases remarkably [54]. The value of the dissolved oxygen is constant at the initial step, but decreases gradually. The rate of reduction of total oxygen (most of which may be oxygen in the form of oxides) is much faster than that of dissolved oxygen.

## 2.2 Deoxidation Mechanism

A large number of articles have been published dealing with deoxidation [13-18]. According to Turkdogan [14], the deoxidation reaction may be separated into three steps: formation of critical nuclei of the deoxidation product; progress of deoxidation resulting in growth of the reaction products; and floatation from the melt.

As for the nucleation, Turkdogan [15] suggested that the number of nuclei formed at the time of addition of the deoxidizer is about  $10^8/\text{cm}^3$ . However, the time for nucleation is far less than 1 sec. [13] (for  $\text{SiO}_2$   $1 \times 10^{-6}$  sec).

Regarding the growth process, Turkdogan [14] suggested four major mechanisms: (a) Brownian motion, (b) Ostwald ripening, (c) diffusion, and (d) collision. Brownian motion is such a slow process that it would take 3 hours to reduce the oxidized particle density to  $10^7$  particles/ $\text{cm}^3$ . Ostwald ripening is the process for the system of dispersed particles of varying size and the smaller ones dissolve and the larger ones grow. The driving force is the interfacial energy. This process is also very slow [14, 16, 19]. Turkdogan also discussed the subject of diffusional growth [15]. The rate of oxidized particle removal by collisions was measured by several investigators [19, 20, 21]. A theoretical explanation of this problem was proposed by Lindborg et al. [19] who used the equations derived by Gunn [25] and by Saffman and Turner [26].



### 2.3 General Mechanism of Particle Movement in Turbulent Flow

In a turbulent dispersion a knowledge of relative motion of particles to surrounding fluid is of great importance for an understanding of the coagulation mechanism between particles, and the mass transfer from particles to fluid. The behavior of discrete particles in a turbulent fluid depends largely on the concentration of the particles and on their size relative to the scale of turbulence. The first extensive theoretical study was made by Tchen [6] on the motion of very small particles in a turbulent fluid. In Tchen's theory the following assumptions are made

- 1) The turbulence of the fluid is homogeneous and steady.
- 2) The domain of turbulence is infinite in extent.
- 3) The particle is spherical and so small that its motion relative to the ambient fluid follows Stokes' law of resistance.
- 4) The particle is small compared with the smallest wavelength presented in turbulence, i.e. with the Kolmogorov micro-scale  $\eta$ .
- 5) During the motion of the particle the neighborhood is by the same fluid.
- 6) Any external force acting on the particle originates from a potential field, such as gravity.

Assumption (4) seems to be valid for the present problem since the dissipation rate of turbulence in a ladle,  $\epsilon$ , is at most 100erg/g, thus the Kolmogorov micro scale length,  $\eta$ , is about 400 $\mu$ m. This length is much larger than the particle diameter being considered. Other assumptions may be valid for the present problem.

The basic equation extended by Tchen is as follows, [6-9];

$$\frac{\pi}{6} d_p^3 \rho_p \frac{dv_p}{dt} = \frac{\pi}{8} d_p^2 \rho_f C_d |v_f - v_p| (v_f - v_p) + \frac{\pi}{6} d_p^3 \rho_f \frac{dv_f}{dt} + \frac{1}{2} \frac{\pi}{6} d_p^3 \rho_f \left( \frac{dv_f}{dt} - \frac{dv_p}{dt} \right) + \frac{3}{2} d_p^3 \sqrt{\pi \rho_f u} \int_{t_0}^t dt' \frac{dv_f}{dt'} - \frac{dv_p}{dt} + F_e \quad (6)$$

(2.2.1)

where  $V_p$  and  $V_f$  are the turbulent velocities of fluid and particle,  $d_p$  the diameter of particle,  $C_d$  the drag coefficient in turbulent flow, and  $\rho$  and  $\rho_p$  the densities of fluid and particles. Each term means the following:

- (1) the force required to accelerate the particle,
- (2) drag force,
- (3) pressure gradient force,
- (4) added mass correction,
- (5) Basset term,
- (6) external force due to potential field.

When the potential force term is neglected equ. (2.2.1) can be rewritten as follows.

$$\frac{dV_p}{dt} + aV_p = aV_f + b \frac{dV_f}{dt} + c \int_{t_0}^t \frac{dV_f/dt' - dV_p/dt'}{\sqrt{t-t'}} dt' \quad (2.2.2)$$

where

$$a = \frac{36\mu}{(2\rho_p + \rho_f)d^2} \quad b = \frac{3\rho_f}{2\rho_p + \rho_f} \quad c = \frac{18}{(2\rho_p + \rho_f)d} \sqrt{\frac{\rho_f \mu}{\pi}}$$

Interesting results will be obtained if we assume that both  $V_p$  and  $V_f$  may be represented by a fourier integral [6].

$$V_f = \int_0^{\infty} d\omega (\alpha \cos \omega t + \beta \sin \omega t) \quad (2.2.3)$$

$$V_p = \int_0^{\infty} d\omega (\gamma \cos \omega t + \delta \sin \omega t) \quad (2.2.4)$$

Then the ratio between Lagrangian energy-spectrum functions for fluid and particles may be expressed as follows [6]

$$\frac{E_{pL}}{E_{fL}} = [1 + J_1(\omega)]^2 + J_2^2(\omega) \quad (2.2.5)$$

where

$$J_1(\omega) = \frac{\omega(\omega + c\sqrt{\pi\omega/2})(b-1)}{(a + c\sqrt{\pi\omega/2})^2 + (\omega + c\sqrt{\pi\omega/2})^2}$$

$$J_2(\omega) = \frac{\omega(a + c\sqrt{\pi\omega/2})(b-1)}{(a + c\sqrt{\pi\omega/2})^2 + (\omega + c\sqrt{\pi\omega/2})^2}$$

Assuming Pao's universal slope law (Fig. 2.3) for the spectrum distribution in the R-H units, we can obtain the energy spectrum distribution for the particle using equ. (2.2.5) (Fig. 2.4). For the present calculation a dissipation energy of  $\epsilon = 500 \text{ (erg/cm}^3\text{)}$  is used. There is only a slight difference between the energy spectrum of fluid and particles. On the other hand, Peskin [11-12] obtained the following relation between diffusivities of fluids and particles;

$$\frac{D_p}{D} = 1 - \frac{\lambda^2}{\lambda_E^2} \left( \frac{3K^2}{K+2} \right) + O\left(\frac{1}{\lambda_E^4}\right) \quad (2.2.6)$$

where  $K = (\sqrt{\pi}/i_8) \langle N_R \rangle \left( \frac{\rho}{\rho_p} \right) \left( \frac{2d}{\lambda} \right)$ . This result is shown in Fig. 2.5. Although we cannot obtain exact information about the Lagrangian or Eulerian microscale,  $K$  is far smaller than 1 for the case of deoxidized particles in a steel melt. Therefore, in the present computation the assumption of  $D_p/D \approx 1$  will be valid.

On the other hand, Kolmogorov assumed that the characteristics of turbulence could be determined by the parameters  $\nu$  and  $\epsilon$  at high Reynolds number. From a dimensional analysis, it follows that [6],

$$\text{for the length scale} \quad \eta = \left( \frac{\nu^3}{\epsilon} \right)^{\frac{1}{4}} \quad (2.2.7)$$

$$\text{for the velocity scale} \quad v = (\nu \epsilon)^{\frac{1}{4}} \quad (2.2.8)$$

Fig. 2.6 shows the Kolmogorov micro scale length  $\eta$  with respect to the turbulent kinetic energy  $\epsilon$ . Since  $\epsilon$  is now considered to be less than  $100 \text{ (cm}^2\text{/sec}^3\text{)}$ ,  $\eta$  is more than  $300\mu$ . As the particle being considered is less than  $20\mu\text{m}$ , the particle size is far smaller than  $\eta$ .

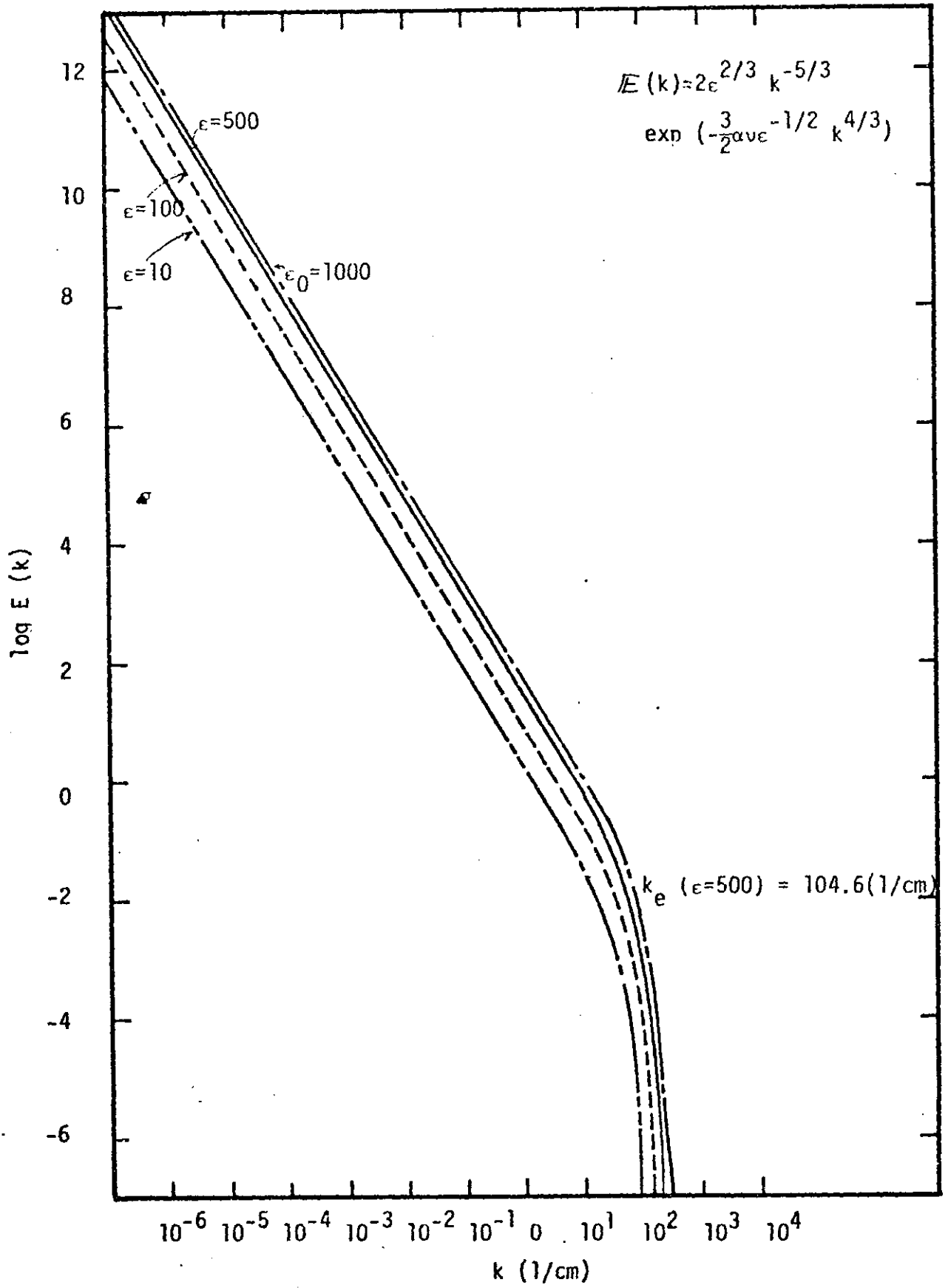


Fig. 2.3 Pao's universal slope law

$$\alpha = 1.5$$

$$\epsilon = 500 \text{ erg/cm}^3$$

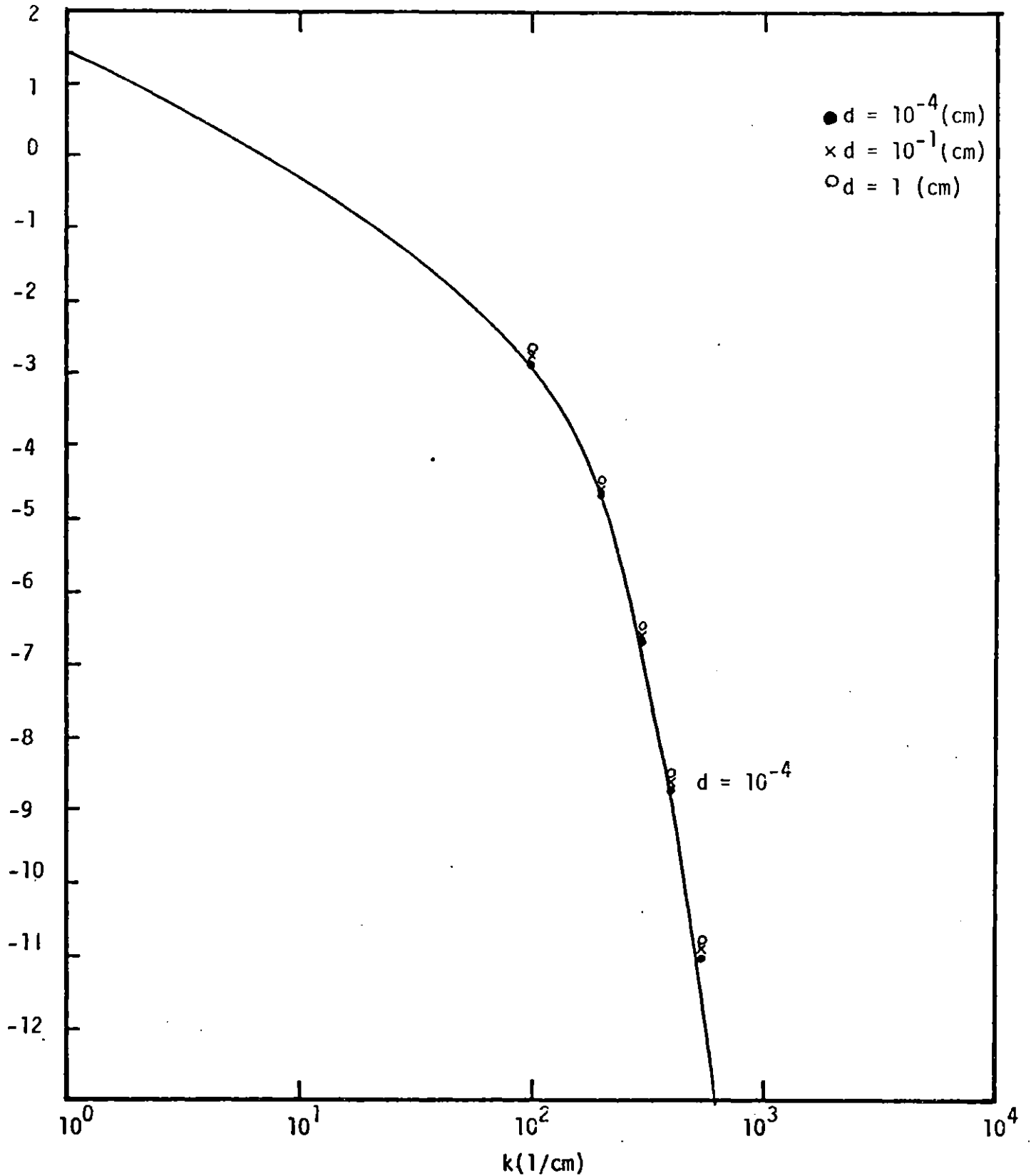


Fig. 2.4 Energy spectrum for fluid and particles

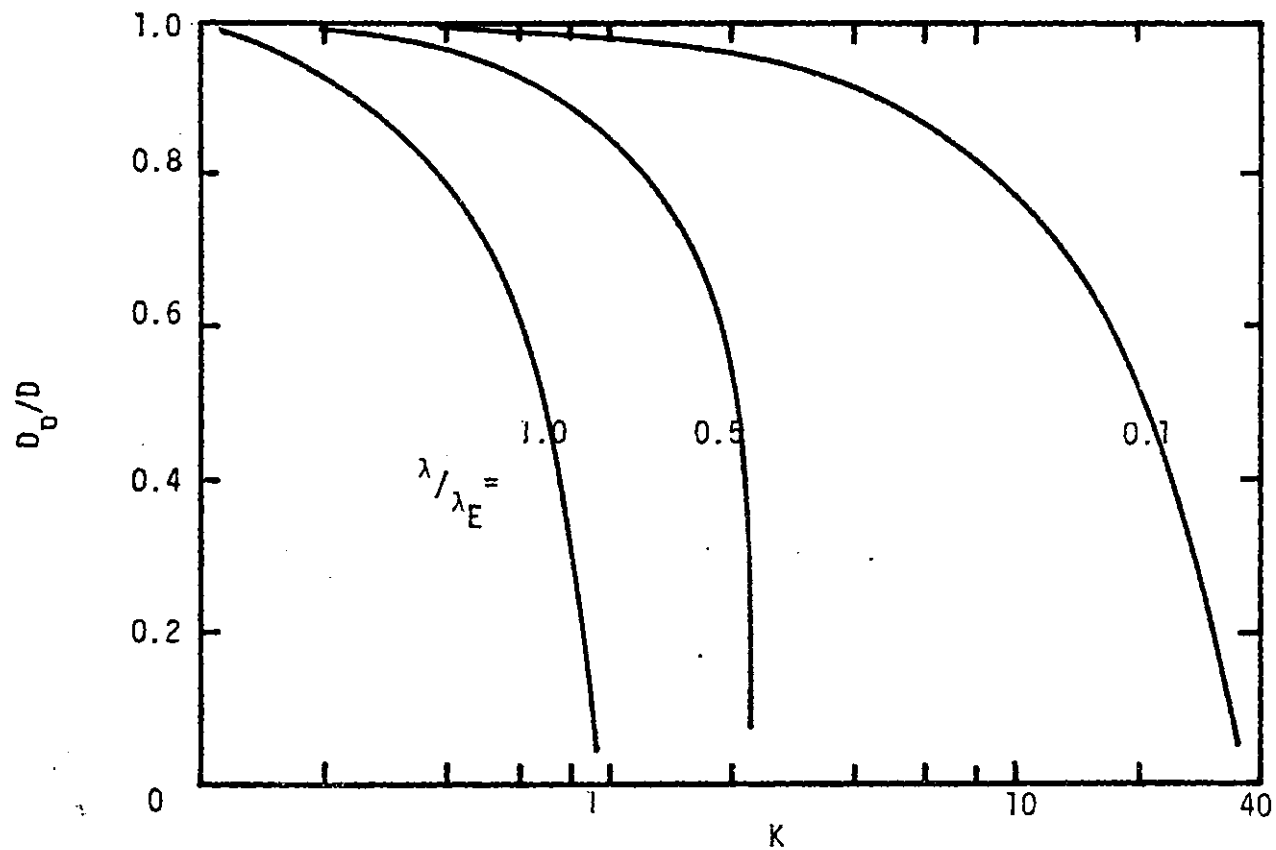
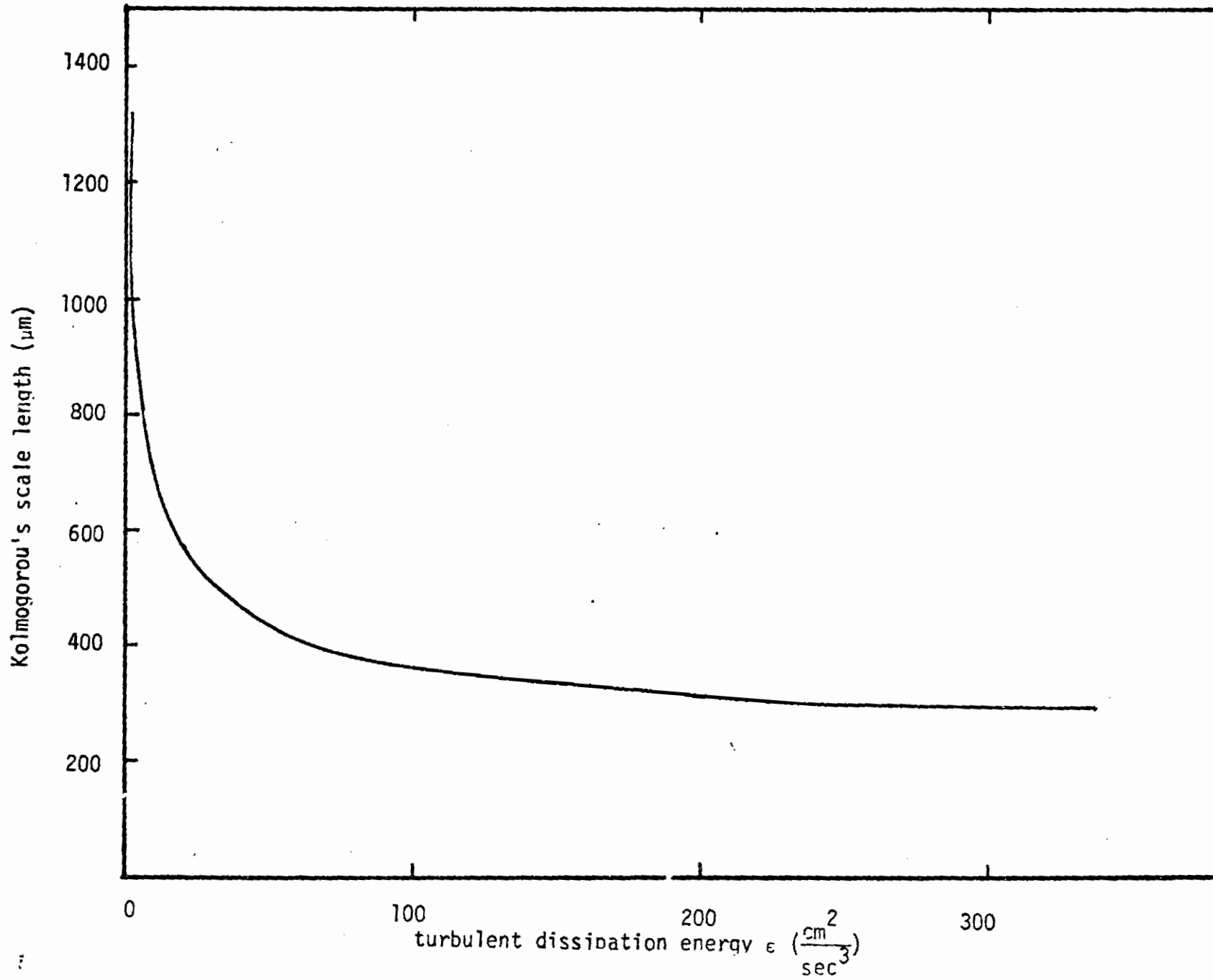


Fig. 2.5 Ratio of diffusivity of particle and turbulent flow (Soo) [12]

Fig. 2.6

Kolmogorov's scale length



## 2.4 General Expression for Particle Population Balance in Agitated Dispersions

A knowledge of the coalescence and the breakage of second phase particles within a turbulent fluid is important for an understanding of the chemical reactor with a dispersed phase system, and often, population balance concepts are employed to describe the dispersion [27-30]. This theory is often applied to the growth and the breakage of aerosol particles. Although the coalescence function depends largely on the nature of the particles, the general formulation developed by aerosol researchers is valuable for an understanding of the general structure of the problem.

We may define a number density  $f(\xi, t)$  of particles in the phase space [27] such that

$$\int(\xi, t) d\xi = \text{the number of particles in the system}$$

at time  $t$  with phase coordinate in the range  $\xi_1 \pm 1/2d\xi$ ,  $\xi_2 \pm 1/2d\xi_2$  and introduce the function  $h(\xi, t)$  to represent the net rate of addition of new particles into the system.

$$h(\xi, t) \cdot |d\xi| = \text{the net number of particles introduced into the system per unit time at time } t \text{ with phase coordinate in the range } \xi_1 \pm 1/2d\xi_1 \quad \xi_2 \pm 1/2d\xi_2$$

We may consider a small element in the field in order to obtain the convective mass transfer formulation [27].

$$\frac{\partial f}{\partial t} + \sum_i \frac{\partial \{u_i(\xi, t) \cdot f\}}{\partial \xi_i} = h(\xi_i, t) \quad (2.4.1)$$

Separating the phase coordinate from the external coordinate, we obtain [27]

$$\frac{\partial f}{\partial t} + \sum_i \frac{\partial (u_i f)}{\partial x_i} + \sum_j \frac{\partial \{G_j(c, \theta, r) \cdot f\}}{\partial \eta_j} = B(c, \theta, r) \quad (2.4.2)$$



where  $\beta$  is a nucleation function and  $G_j$  is a growth function which depends on the concentration  $C$ , the temperature  $\theta$ , and the dimension of the newly nucleated particles. When the coagulation effect causes only a change in particle distribution (in other words when the nucleation and the diffusional growth can be ignored), the discussion presented above will differ. In this case, we must assume that only two-particle collisions occur in the field. Since no particles are produced by nucleation or diffusional growth, total mass (or total volume) or particles must be conserved at any time.

Then,

$$\frac{dm}{dt} = 0 \quad (2.4.3)$$

The number density  $f(x, m, t)$  or particles in the space can be described as

$$\frac{\partial f}{\partial t} + \frac{\partial \{v(x, t) f\}}{\partial x} = h(x, m, t) \quad (2.4.4)$$

Here, particle nucleation under the influence of the chemical environment is ignored. Usually agglomeration at  $x, t$  between particles of mass  $m_1$  and  $m_2$  is proportional to the product of the number densities  $f(x, m_1, t), f(x, m_2, t)$ . The proportionality factor is  $a(x, t)$ . Since mass is conserved during a collision, the number of newly produced particles is [27] [23]

$$\frac{1}{2} a(x, t) \int f(x, m-m', t) f(x, m', t) dm' \quad (2.4.5)$$

where the integration extends over all possible values of  $m'$ . Similarly, the number of particles which disappear by coalescence at  $x, t$  is [2]

$$a(x, t) f(x, m, t) \int f(x, m', t) dm' \quad (2.4.6)$$

Then equ. (2.4.2) may be written in explicit form as

$$\begin{aligned} \frac{\partial f(x, m, t)}{\partial t} + \frac{\partial \{v(x, t) f(x, m, t)\}}{\partial x} \\ = a(x, t) \left[ \frac{1}{2} \int f(x, m-m', t) f(x, m', t) dm' \right. \\ \left. - \int f(x, m, t) \int f(x, m', t) dm' \right] \quad (2.4.7) \end{aligned}$$

When the effect of breakage of particles can no longer be ignored, equ. (2.4.7) may be expressed as C.A. Coulaloglou et al. [28] suggested, as

$$\begin{aligned} \frac{\partial f(x, m, t)}{\partial t} - \frac{\partial \{v(x, t) f(x, m, t)\}}{\partial x} \\ = a(x, t) \left[ \frac{1}{2} \int f(x, m-m', t) f(x, m', t) dm' - f(x, m, t) \int f(x, m', t) dm' \right] \\ + \int b(m', m) f(x, m', t) dm - b(m', m) f(x, m', t) \end{aligned} \quad (2.4.8)$$

where  $b(m', m)$  is the distribution function of daughter particles produced from breakage of mass  $m'$  particles. The generalized form for the mass population balance can be summarized in Table 2.1. Equ. (2.4.8) coincides with the expression employed by U. Lindborg and K. Torsell [23] except for the convection terms.

As mentioned above, the difficulty in calculating the population balance is in the mass balance. One of the earliest expressions of particle coalescence was made by Smoluchowski [31].

$$\begin{aligned} \frac{dn_1}{dt} &= -\alpha_{11} n_1^2 - \alpha_{12} n_1 n_2 - \alpha_{13} n_1 n_3 - \dots \\ \frac{dn_2}{dt} &= \frac{1}{2} \alpha_{11} n_1^2 - \alpha_{12} n_1 n_2 - \alpha_{22} n_2^2 - \alpha_{23} n_2 n_3 - \dots \\ \frac{dn_3}{dt} &= \alpha_{12} n_1 n_2 - \alpha_{13} n_1 n_3 - \alpha_{24} n_2 n_3 - \alpha_{33} n_3^2 - \dots \\ \frac{dn_4}{dt} &= \alpha_{13} n_1 n_3 + \frac{1}{2} \alpha_{22} n_2^2 - \alpha_{14} n_1 n_4 - \alpha_{24} n_2 n_4 - \dots \end{aligned} \quad (2.4.9)$$

However, simple this expression is, it contains a weakpoint hardly acceptable from the view point of mass balance.

Table 2.1 Expression for particle population balance

$$\frac{\partial f}{\partial t} + \sum_{i=1}^3 \frac{\partial (V_i f)}{\partial x_i} + G = B(C, \theta, r) + \alpha(x, m, t) + \beta(x, m, t)$$

J; Number density of particles

G; Growth by diffusion

B; Nucleation

$\alpha$ ; Coagulation of particles

$\beta$ ; Breakage of particles

$$G = \sum_j \frac{\partial \{G_j(C, \theta, r) f\}}{\partial r_j}$$

$$\alpha(x, m, t) = A(x, t) \left[ \frac{1}{2} \int f(x, m - m', t) f(x, m', t) dm' - f(x, m, t) \int f(x, m', t) dm' \right]$$

$$\beta(x, m, t) = \int b(m', m) f(x, m', t) dm' - b(m', m) f(x, m', t)$$

## 2.5 The Mechanism of Small Particle Coagulation in a Turbulent Flow

In the previous section, the generalized expression for particle population balance was discussed. Another important issue for the analysis of particle coagulation is an estimation of collision frequency in turbulent flow. Most of the studies on this subject were done in relation to meteorology or aerosol behavior. The most instructive studies on the collision frequency in turbulent streams were performed by P.G. Saffman and J.S. Turner.

- 1) Collision between particles moving with fluid. (by Saffman and J.S. Turner [26]).

Assuming that the mean concentrations of two sizes of particles in a given population be  $n_1$  and  $n_2$  per unit volume, and that their radii be  $r_1$  and  $r_2$  respectively, then the mean flux of fluid into a sphere of radius  $R = r_1 + r_2$  surrounding one particle is

$$-\int_{w_r} w_r ds \quad (2.5.1)$$

where  $w_r$  is the radial component of the relative velocity. The collision rate is

$$-n_1 n_2 \int_{w_r < 0} w_r ds \quad (2.5.2)$$

now, assuming that

$$-\int_{w_r} w_r ds = \frac{1}{2} \int |w_r| ds = 2\pi R^2 |\overline{w_x}| \quad (2.5.3)$$

then,

$$|\overline{w_x}| = R \left| \overline{\partial u / \partial x} \right|, \quad \overline{(\partial u / \partial x)^2} = \epsilon / 15\nu$$

and we obtain

$$\begin{aligned} N &= n_1 n_2 (2\pi R^2 |\overline{w_x}|) \\ &= n_1 n_2 2\pi R^3 \left| \frac{\partial u}{\partial x} \right| \\ &= n_1 n_2 (r_1 + r_2)^3 \left( \frac{8\pi\epsilon}{15\nu} \right)^{\frac{1}{2}} \\ &= 2.3 (r_1 + r_2)^3 n_1 n_2 \left( \frac{\epsilon}{\nu} \right)^{\frac{1}{2}} \end{aligned} \quad (2.5.4)$$

2) Collision between particles in relative motion with fluid [26].

A more sophisticated analysis was also made by P.G. Saffman and J.S. Turner for particles in motion relative to the surrounding fluid. In this case, the analysis of collision frequency is rather complicated. The collision frequency is derived from encounter probability which depends on the relative velocities between the particles and the fluid surrounding them. The final representation for the collision frequency can be written as

$$N = 2(2\pi)^{\frac{1}{2}} R^2 n_1 n_2 \left[ \left(1 - \frac{\rho_p}{\rho}\right)^2 (\tau_1 - \tau_2) \left(\frac{D\bar{u}}{Dt}\right)^2 + \frac{1}{3} \left(1 - \frac{\rho_p}{\rho}\right) (\tau_1 - \tau_2)^2 g^2 + \frac{1}{9} R^2 \frac{\epsilon}{\nu} \right]^{\frac{1}{2}} \quad (2.5.5)$$

where  $\rho_p$ , the density of particles

$\rho$ , the density of fluid

$\epsilon$ , the turbulent dissipation energy

When the density of particles can be considered to be equal to the density of the fluid, (i.e.  $\rho = \rho_p$ ) the first two terms disappear and equ. (2.5.5) gives

$$N = 1.67 R^2 n_1 n_2 \left(\frac{\epsilon}{\nu}\right)^{\frac{1}{2}} \quad (2.5.6)$$

Further, in the case when there is no turbulence (i.e. collision by buoyancy force) Equ. (2.5.5) leads to

$$N = \pi R^2 n_1 n_2 g \left(1 - \frac{\rho_p}{\rho}\right) (\tau_1 - \tau_2) \quad (2.5.7)$$

As shown later this expression is similar to the representation given by Lindborg and Torsell [19].

Equ. (2.5.6) is used for the calculation of particle coalescence

3) Levich's collision theory [32].

Levich proposed two types of collision; (1) gradient collision, (2) turbulent collision. For the gradient collision of two particles with radii  $r_1$  and  $r_2$ , the total number of encounters is represented by

$$N_{grad} = \frac{32}{3} n_0^2 \Gamma R^3 = \frac{4}{3} g_{grad} v (r_1 + r_2)^3 n_1 n_2 \quad (2.5.8')$$

where  $\Gamma$  is the velocity gradient in the fluid. This is essentially similar to Saffman's first case (e.g. equ. (2.5.4)) except for the coefficient.

On the other hand, Levich derived the expression for turbulent collisions as follows:

$$N_{turb} = 12\pi\beta \sqrt{\frac{\epsilon}{\nu}} R^3 n_0^2 \quad (2.5.9)$$

This expression is also similar to Saffman's representation except for the coefficient.

#### 4) Collision model by U. Lindborg and K. Torsell [19].

U. Lindborg and K. Torsell derived a collision model based on both Stokes' collision and gradient collision theory.

Their Stokes collision model comes from equ. (2.5.7). The Stokes' force can be written in an explicit form as

$$\tau = \frac{2r^2(p-p_0)}{9\mu} \quad (2.5.10)$$

substituting this into equ. (2.5.7) gives

$$\begin{aligned} N &= \pi R^3 n_1 n_2 g \left(1 - \frac{\rho_0}{\rho}\right) \frac{2(p-p_0)}{2\mu} |r_1^2 - r_2^2| \\ &= k |r_1^2 - r_2^2| (r_1 + r_2)^2 n_1 n_2 \\ &= k |r_1 - r_2| (r_1 + r_2)^3 n_1 n_2 \end{aligned} \quad (2.5.11)$$

where  $k$  is 7.2 for  $\text{SiO}_2$  particles in steel melt according to Lindborg and Torsell.

For the gradient collision model, Levich expressed the velocity gradient in explicit parameters as;

$$\begin{aligned} g_{grad} v &= \frac{v_e^{\frac{3}{2}}}{\nu^{\frac{1}{2}} l^{\frac{1}{2}}} && \text{for the interior of the bath} \\ g_{grad} v &= \frac{5v_e}{l} && \text{for the boundary layer} \end{aligned} \quad (2.5.12)$$

Finally, adding both terms, Lindborg obtained the following for gradient collision

$$N = \frac{4}{3} (r_1 + r_2)^3 \left( \frac{5\nu_e}{l} + \frac{9\nu_e^{\frac{3}{2}}}{l^{\frac{3}{2}}} \right)$$

A summary of the coagulation models in turbulent flow is listed in Table 2.2.

Table 2.2 Models of particles coalescence

Saffman and Turner (moving with air)	$N = n_1 n_2 (R_1 + R_2)^3 \sqrt{\frac{8\pi^2 \epsilon}{15\nu}} = 1.3 n_1 n_2 (R_1 + R_2)^3$ $\times \sqrt{\frac{\epsilon}{\nu}}$
Saffman and Turner (moving relatively)	$N = 2(2\pi)^{1/2} R^2 n_1 n_2 \left[ \left(1 - \frac{\rho}{\rho_0}\right)^2 (\tau_1 - \tau_2)^2 \left(\frac{DU}{dt}\right)^2 \right. \\ \left. + \frac{1}{3} \left(1 - \frac{\rho}{\rho_0}\right)^2 (\tau_1 - \tau_2)^2 g^2 + \frac{1}{9} R^2 \frac{\epsilon}{\nu} \right]^{1/2}$ <p>when the first two terms are zero</p> $N = \frac{2}{3} R^3 n_1 n_2 \left(\frac{2\pi\epsilon}{\nu}\right)^{1/2}$ $= 1.67 R^3 n_1 n_2 \left(\frac{\epsilon}{\nu}\right)^{1/2}$
Levich (Brownian)	$N = 8\pi Da n_0^2$
Levich (Turbulence)	$N = 12\pi\beta R^3 n_0^2 \sqrt{\frac{\epsilon_0}{\nu}}$
Lindborg and Torsell (stokes')	$N = 7.2  r_1 - r_2  (r_1 + r_2)^3 n_1 n_2$
Lindborg and Torsell (Turbulence)	$N = \frac{4}{3} (r_1 + r_2)^3 \left( \frac{5V_\ell}{\ell} + \frac{V_\ell^{3/2}}{\nu^{1/2} \ell^{1/2}} \right) n_1 n_2$
Scaninject	$N = 1.3 (R_1 + R_2)^3 n_1 n_2 \sqrt{\frac{\epsilon}{15\nu}}$



## 2.6 The Mechanism of Small Particle Deposition from Turbulent Flow to a Wall

As shown in the previous section, particle motion in turbulent streams may be described by equ. (2.2.1). However, the movement of particles in the laminar boundary layer is determined mainly by the lift force induced in viscous shear flow. Saffman [33] derived the lift force as follows:

$$F_L = \frac{K\mu\bar{U}a^2}{\nu^{\frac{1}{2}}} \left[ \frac{du}{dy} \right]^{\frac{1}{2}} \quad (2.6.1)$$

where  $\bar{U}$  is difference between the velocity of the particle and the fluid,  $du/dy$  is the velocity gradient in the shear flow and  $K$  is taken as 81.2.

In addition, a Stokes' force acts on the sphere in an opposite direction to the direction of motion.

$$F_S = 6\pi\mu d_p \bar{V} \quad (2.6.2)$$

where  $d_p$  is the particle radius

$\bar{V}$  is the relative velocity of the particle.

All of the forces acting on a particle in a laminar boundary layer are represented schematically in Fig. 2.7. P.O. Rouhianan and T. W. Stachiewicz [34] proposed a simple governing equation for the particle motion in the boundary layer

$$-3\pi\mu d_p (u_p - u_f) - \frac{\pi}{6} d_p^3 (\rho_p - \rho_f) g - \frac{\pi}{6} \rho_p d_p^3 \frac{du_p}{dt} \quad (2.6.3)$$

$$-3\pi\mu d_p v_p - \frac{K\mu (u_p - u_f)}{4} \left( \frac{du}{dy} \right)^{\frac{1}{2}} \frac{d\rho_p}{\nu^{\frac{1}{2}}} - \frac{\pi}{6} \rho_p d_p^3 \frac{dv_p}{dt} \quad (2.6.4)$$

where subscripts p and f denote particle and fluid, respectively. These equations can be regarded as a force balance on the particle in the direction of x and y. The second term of equ. (2.6.4) is the shear lift term posed by Saffman [33].

The velocity distribution along the flat wall can be described by Karman's linear approximation. At the nearest region to the wall, which is

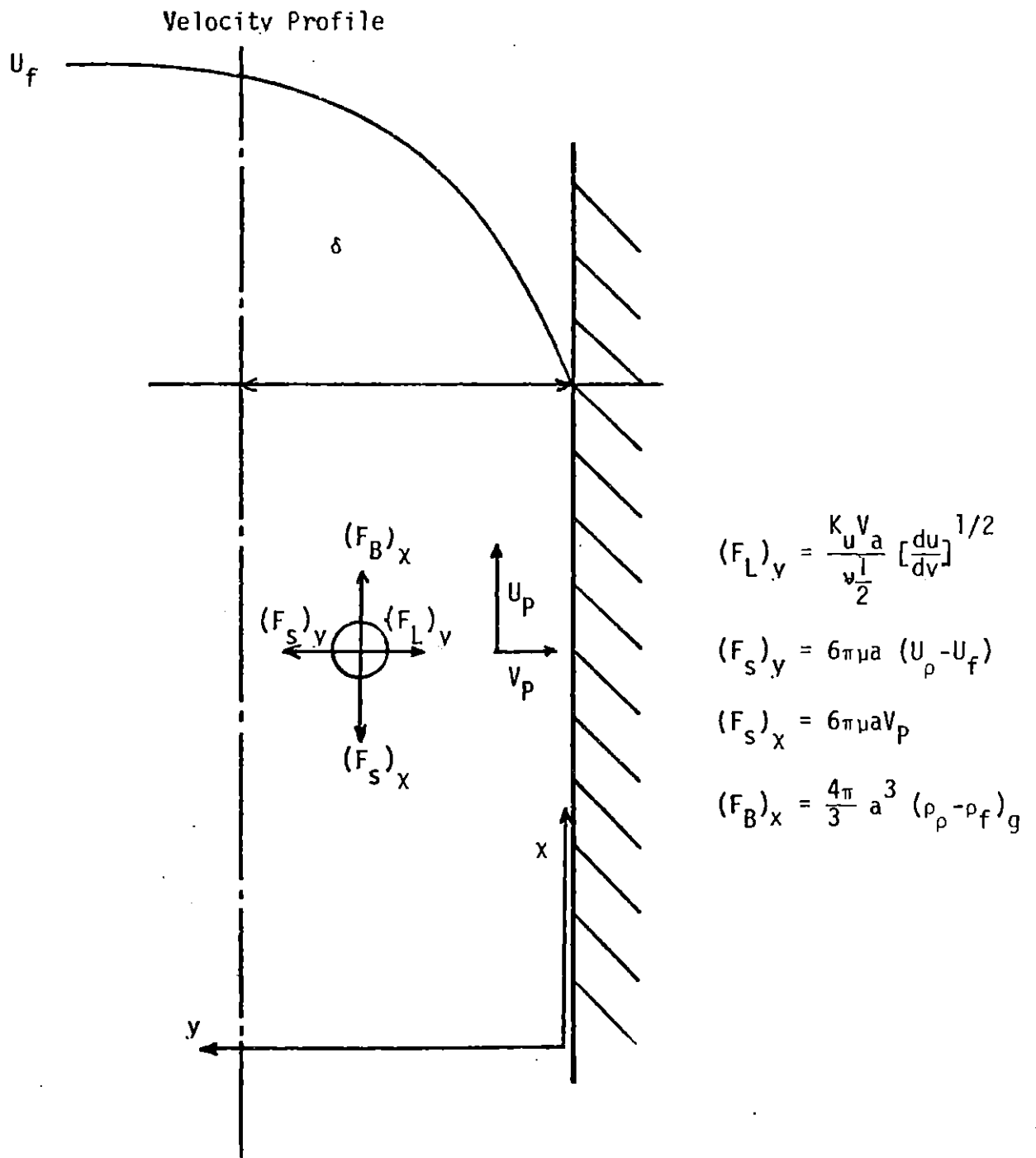


Fig. 2.7 Schematic representation of forces acting on a particle in a boundary layer

expressed as

$$v^+ = y^+ \quad 0 < y^+ < 5 \quad (2.6.5)$$

, so that

$$\frac{v}{\sqrt{\tau_0/\rho}} = \frac{y}{\nu} \sqrt{\frac{\tau_0}{\rho}}$$

then

$$u = \frac{y}{\nu} \frac{\tau_0}{\rho} = \frac{y^2}{\nu} V \frac{f}{2}$$

and

$$\frac{\partial u}{\partial y} = \frac{V^2 f}{\nu 2}$$

where  $f$  is the friction factor

$V$  is the fluid velocity at the edge of the sublayer.

Then, if we assume a value for the  $y$ -direction, velocity at the edge of sublayer, we can solve equations (2.6.3) and (2.6.4) and find the trajectory of a particle. Although P.O. Rouhianinen et al. [34] considered only the case of an air-solid particle system, it could be extended to the general concept of a particle deposition system.

On the other hand, mass-transfer coefficient approaches were made by S.K. Friedlander et al. [35] and J.T. Davis [38]. The advantage of this approach is that mass-transfer coefficient type description is convenient for the over-all computation of particle concentration in the vessel.

Generally speaking, the kinematic viscosity near the wall can be calculated, by taking

$$\nu_F = \tilde{v}_y' l = \tilde{v}_y' c y$$

on the other hand,

$$\tilde{v}_y' = \eta v_0 \quad \text{at } y = \delta_1$$

then

$$\begin{aligned}\tilde{v}_y' &= - \int (\partial \tilde{v}_z / \partial x) dx \\ &= \gamma^2 \tau v_0 / \delta_1^2 \\ &= C \gamma^3 \tau v_0 / \delta_1^2\end{aligned}\quad (2.6.8)$$

therefore

$$v_{E/\nu} = C \gamma_+^3 (17/25) \quad (2.6.9)$$

A reasonable fit with experimentally determined velocity distributions of velocity near the wall is obtained of  $c_1/25 = \frac{1}{250}$ .

Davis [38] suggest that at the turbulent core equ. (2.6.9) can be written as

$$v_{E/\nu} = (\gamma^+ / 8.9)^3 \quad (2.6.10)$$

Lin et al. [39] suggests

$$v_{E/\nu} = (\gamma^+ / 14.5)^3 \quad (2.6.11)$$

for the particles used in the present calculation the rate of transfer can be expressed as

$$j = -D_E \partial \bar{c} / \partial y \quad (2.6.12)$$

Combining (2.6.10) and (2.6.12) and assuming the Reynolds analogy at  $y^+ > 0$ , Davies [38] obtained the mass transfer correlation.

$$\frac{R}{V} = \frac{\frac{j}{2}}{1 + \sqrt{\frac{I}{2}} \left[ \frac{353}{S^{+2}} - 19 \right]} \quad (2.6.13)$$

On the other hand, Friedlander et al. [35] obtained the following form:

$$\frac{R}{V} = \frac{\frac{j}{2}}{1 + \sqrt{\frac{I}{2}} \left( \frac{1523}{S^{+2}} - 50.6 \right)} \quad (2.6.14)$$

where

$$S^+ = \frac{m \tilde{v}_y'}{3\pi \mu d_p} \frac{V_0}{\nu}$$

Then, as Davies mentioned in his book [38], the rate-determining factor

in the case of the deposition of large aerosol particles is the distance from the surface at which their fluctuation momentum can just carry them through the viscous layer.

A simple expression for particle deposition to the wall was proposed by Levich [32]. He analysed the coagulation of two particles caused by the velocity gradient induced by these particles. In the case of particles, the total number of collisions is expressed by

$$N_{\text{grad}} = \frac{32}{3} n_0 \Gamma a^3 \quad (2.6.15)$$

where

$$a = r_1 + r_2$$

$$\Gamma = \frac{2v_x}{\partial y}$$

Engh and Lindskog [21] applied Levich's theory to the deposition of oxidize particles on a wall. They also used the mass diffusivity proposed by Davis [38]

$$D_E = \frac{0.29 \times 10^{-2} v_0^3 \gamma^3}{\nu^2} \quad (2.6.16)$$

Combining equ. (2.6.16) and (2.6.12) using  $v_0$  which is calculated from Kolomogrov's law he obtained

$$N_a = v_i(c_a) S C_a \quad (2.6.17)$$

where

$S$  is wall surface area and

$$v_i(c_a) = \frac{0.29 \times 10^{-2} E_0 \nu a^2}{\nu^2 \rho_0 S}$$

The problem in calculating the deposition rate using Levich's method is that the particle size is independent of the rate of deposition. This assumption may be valid when we treat the deposition behavior of particles having a wide range of particle size.

Another model of particle deposition was presented by Linder [22] [24]

in his modeling work of oxidized particle removal from a stirred vessel

$$\frac{\partial n_p}{\partial t} = A.R. \cdot 0.01 \frac{\tau_0}{\rho \nu} n_{op} \quad (2.6.18)$$

This expression may be regarded as a simplified form of equ. (2.6.15) (2.6.18) and is independent of the particle size.

All the models of particle deposition from a turbulent flow are listed in Table 2.3.

Table 2.3 The description for particle deposition to the wall

Friedlander and Johnston	$\frac{k}{V_{av}} = \frac{f/2}{1 + \sqrt{\frac{f}{2} \left( \frac{1525}{S_+^2} - 50.6 \right)}}$
J.T. Davies	$\frac{k}{V_m} = \frac{f/2}{1 + \sqrt{\frac{f}{2} \left( \frac{353}{S_+^2} - 19 \right)}}$
Engh and Lindskog	$N_a = V_i(a) S Ca$ $V_i(a) = \frac{0.29 \times 10^{-2} \epsilon_0 Va^2}{v^2 \rho_0 S}$
Sten Linder	$\frac{\partial n_p}{\partial t} = A_i R \cdot 0.01 \frac{\tau_0}{\rho \nu} n_{op}$ $= A_i R \cdot 0.01 \frac{v^2}{\nu} \frac{f}{2} n_{op}$

## 2.7 Turbulence Modeling

The equations describing turbulent fluid flow are now presented. Although turbulence phenomena have been studied by many researchers and applied to simple types of flow, it cannot be said that a general expression for turbulence phenomena has been perfected. Still, some modeling methods are very useful and powerful for predicting these phenomena. Additionally, these techniques may provide an effective means of studying systems which are difficult to investigate experimentally, such as industrial scale reactor.

A turbulence model may be obtained by using the Boussinesq assumption [40].

$$-\rho \overline{u_i' u_j'} = \mu_T \left( \frac{\partial \overline{u_i}}{\partial x_j} + \frac{\partial \overline{u_j}}{\partial x_i} \right) - \frac{2}{3} \left( \mu_T \frac{\partial \overline{u_k}}{\partial x_k} + \bar{p} k \right) \delta_{ij} \quad (2.7.1)$$

Cartesian tensor notation is utilized in this expression. Boussinesq's assumption seems to be valid under several experimental circumstances. In analogy with the coefficient of viscosity in Stokes' law, Boussinesq introduced the concept of mixing coefficient

$$\tau_T = -\rho \overline{u'v'} = A_T \frac{\partial \bar{u}}{\partial y} \quad (2.7.2)$$

In this equation, the turbulent shear stress is related to the rate of mean strain through an apparent turbulent viscosity.

This assumption cannot be used for calculation unless a relation between  $A$  and  $\tau$  is given.

Based on the number of additional differential equations which are necessary in order to determine the turbulent characteristics, the turbulence models may be clarified into four categories based on the number of additional differential equations required to determine the turbulence characteristics [41-43]

- 1) zero-equation models,



- 2) one-equation models,
- 3) two-equation models,
- 4) multi-equation models.

1) Zero equation models

One of the simplest turbulence models was proposed by L. Prandtl;

$$\mu_T = \bar{\rho} l^2 \left| \frac{\partial \bar{u}}{\partial y} \right| \quad (2.7.3)$$

where  $l$  a mixing length. This hypothesis is derived from an analogy to the kinetic theory to gases.

With reasonable accuracy,  $l \left| \frac{\partial \bar{u}}{\partial y} \right|$  can be considered to be a characteristic velocity  $V_T$ . Then  $\mu_T$  can be interpreted to be

$$\mu_T = \rho V_T l \quad (2.7.4)$$

A typical mixing length distribution is given by van Driest [45]. He assumed that the amplitude of the motion diminishes from the wall according to the factor  $[\exp(-y/A)]$ , and that the factor  $[1 - \exp(-y/A)]$  must be applied to the fluid oscillation to obtain the damping effect of the wall, then

$$l_m = \kappa y \left[ 1 - \exp\left(-\frac{y \tau_s^{1/2} \rho^{1/2}}{A \mu}\right) \right] \quad (2.7.5)$$

where  $A$  is the damping const,  $A = 26$

2) One-equation models

"One equation models" are models which need the solution of one additional partial differential equation in order to evaluate the Reynolds stress and mass flux term.

Considering Prandtl's mixing length model mentioned earlier,  $\mu_T$ , may be expressed as  $\mu_T = \rho V_T l$ . Prandtl and Kolmogorov suggested that  $V_T$  was proportional to the square root of turbulent kinetic energy,  $k = \frac{1}{2} \overline{u' u'} = (\overline{u'^2} + \overline{v'^2} + \overline{w'^2})/2$  and that  $\mu_t$  could be expressed as

$$\mu_T = C_k \bar{\rho} \sqrt{k} l \quad (2.7.6)$$

The general transport equation for turbulent kinetic energy is [6]

$$\begin{aligned} \frac{Dk}{Dt} = \frac{\partial}{\partial x_i} u_i \left( \frac{\rho}{\rho} + k \right) - \overline{u_i u_j'} \frac{\partial \bar{u}_i}{\partial x_i} + \nu \frac{\partial}{\partial x_i} \mu_j \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \\ - \nu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \frac{\partial u_i}{\partial x_i} \end{aligned} \quad (2.7.7)$$

Assuming incompressibility and homogeneous turbulence, equ. (2.7.7) reduces to

$$\rho \frac{Dk}{Dt} = - \frac{\partial}{\partial y} (\rho \overline{v'k'} + \overline{v'p'}) - \rho \overline{u'v'} \frac{\partial u}{\partial y} - \mu \sum \left( \frac{\partial u_i}{\partial x_i} \right)^2 \quad (2.7.8)$$

convective flux = diffusion + production - dissipation

The above exact transport equation can be modeled as [41]

$$\rho \frac{Dk}{Dt} = \frac{\partial}{\partial y} \left( \frac{\mu_T}{\sigma_k} \frac{\partial k}{\partial y} \right) + \mu_T \left( \frac{\partial u}{\partial y} \right)^2 - C_D \frac{\rho k^{3/2}}{l} \quad (2.7.9)$$

### 3) Two equation models

In the one equation model,  $\mu_T$  depends only on  $k$ , which is characterized as independent of the "flow history".

One of the most frequently used two-equation models is the model of Jones and Launder.

In this model  $\epsilon$  is assumed to be related to other model parameters by  $\epsilon = Ck^{3/2}/l_\epsilon$  where  $l_\epsilon$  is referred to as the dissipation length and  $C$  is constant. Then the turbulent viscosity is

$$\mu_T = C_\mu \bar{\rho} k^2 / \epsilon = C' \rho k^{1/2} l_\epsilon \quad (2.7.10)$$

At high Reynolds number, the transport equation for  $\epsilon$  may be expressed as;

$$\rho \frac{D\epsilon}{Dt} = \frac{\partial}{\partial x_k} \left[ \frac{\mu_T}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial x_k} \right] + \frac{C_\mu l_\epsilon}{\rho} \left( \frac{\partial u_i}{\partial x_k} + \frac{\partial u_k}{\partial x_i} \right) \frac{\partial u_i}{\partial x_k} - C_2 \frac{\epsilon^2}{k} \quad (2.7.11)$$

For two dimensional incompressible flow

$$\rho \frac{DE}{Dt} = \frac{\partial}{\partial y} \left( \frac{\mu_T}{\sigma_\epsilon} \frac{\partial E}{\partial y} \right) - \frac{C_1 \mu_T E}{k} \left( \frac{\partial u}{\partial y} \right)^2 - \frac{C_2 \rho E^2}{k} \quad (2.7.12)$$

where typical values of the model constants are [44] [41]

$C_u$	$C_1$	$C_2$	$\sigma_k$	$\sigma_\epsilon$	$\sigma_T$
0.09	1.44	1.92	1.2	1.3	0.9

#### 4) Multi-equation models

The multi-equation models need more variables than  $k$  and  $\epsilon$ . For additional transport parameters, shear stress, normal stress, or higher correlations are used. An overall discussion of this subject is given in the book by Launder and Spalding [41].

## 2.8 Numerical Methods

Several numerical methods have been proposed to compute fluid flow phenomena. The finite-difference method is the most popular and advanced one. Using several kinds of finite-difference scheme and pressure correction equations, powerful numerical procedures have been developed by the researchers at Imperial College.

Initially, they developed the stream function-vorticity program and this has been copied and applied to fundamental and practical engineering problems. However, it has become apparent that the  $\omega$ - $\phi$  method is unsuitable for advanced flow problems. One weak-point of this method is its incapability to calculate a fluid flow field which has a pressure gradient.

A few years later a new program was developed by Pun and Spalding [46]. In stead of vorticity-stream function, "primitive-variables" such as velocities and pressure are used in this program. Additionally, this simplicity makes it possible to develop more sophisticated programs such as three-dimensional flow or mass transfer including chemical reactions.

### Chapter 3 FORMULATION OF MATHEMATICAL MODEL

In this chapter, a mathematical model is developed to describe flow and particle coagulation phenomena in R-H degassing system. A short description of the R-H degassing system is presented first and then the formulation of the mathematical model is discussed.

#### 3.1 Description of the R-H Degassing System

A R-H degasser, consists of two parts, a ladle and a vacuum vessel. After it is set under the vacuum vessel the ladle is lifted so as to immerse the twin legs of the vacuum vessel. Then the vacuum vessel is evacuated down to  $\sim 1$  mmHg. Due to atmospheric pressure the level of the molten steel is raised about 1.3m above the surface of the ladle. Inert gas is injected into one leg (called the up-leg) and a recirculating flow through the vacuum vessel and ladle occurs as a result of the apparent difference of density between the up-leg and down-leg side. When the molten steel is exposed to the vacuum atmosphere, the gaseous impurities are released from the melt as a result of the decrease of solubility.

### 3.2 Assumptions Made in the Model

The physical model of the R-H vacuum process and appropriate coordinate system is shown in Fig. (3.1). The present model is limited to the fluid flow and particle coagulation in the ladle.

The assumptions made about the fluid flow field are as follows:

- 1) Two-dimensional coordinates may be applied to the flow and particle coagulation model.
- 2) Since the flow soon becomes steady state, time independent differential equation may be applied to the calculation of fluid field parameters.
- 3) The existence of slag on the surface may be neglected, therefore for the boundary condition of the top surface a free surface condition is applied.
- 4) It is assumed that neither the up-leg nor the down-leg is actually immersed in the molten metal.
- 5) The vertical velocities of the metal through the two legs are deduced from experimentally determined values.

The assumptions made to represent particle coagulation are as follows:

- 1) Although the particle coagulation system is assumed to be transient, the steady state flow field parameters may be used.
- 2) In the present computation, particle sizes are classified into ten Classes (i.e.  $2\mu\text{m}$  to  $20\mu\text{m}$ , every  $2\mu\text{m}$ ).
- 3) The initial particle distribution is calculated from some reports which measured precise particle distributions.
- 4) The initial particle distribution is uniform in each class.
- 5) The wall function for particle deposition is derived from equation (2.6.14) which was proposed by Fridlander and Johnston [35].

6) It is assumed that particle growth is caused only by coagulation as a result of the extremely low rate of diffusional growth and nucleation. Also, it is assumed that the bulk concentration of oxygen or oxidizer is so small that it does not affect the particle growth. (This assumption will be discussed the later in this chapter).

### 3.3 Governing Equations for Flow Phenomena in the Ladle

The equations describing fluid flow and mass transfer phenomena are now presented. Turbulent motion and mass transfer in the system are represented by the time-smoothed equation of motion and mass. The general transport equation in a two dimensional coordinated system can be written as:

$$\frac{\partial(\rho\phi)}{\partial t} + \underbrace{\frac{\partial}{\partial x}(\rho u\phi) + \frac{\partial}{\partial y}(\rho v\phi)}_{\text{convective term}} - \underbrace{\frac{\partial}{\partial x}(\Gamma_{\phi} \frac{\partial\phi}{\partial x}) - \frac{\partial}{\partial y}(\Gamma_{\phi} \frac{\partial\phi}{\partial y})}_{\text{diffusion term}} = \underbrace{S_{\phi}}_{\text{source term}} \quad (3.3.1)$$

where

$x, y$	are the coordinates,
$u$	is the x-direction component of the velocity vector,
$v$	is the y-direction component of the velocity vector,
$\rho$	is the density of the fluid,
$\phi$	is the general variable and takes the value of 1 for the continuity equation,
$\Gamma_{\phi}$	is the diffusion coefficient for the variables,
$S_{\phi}$	is the source term for the variable
$\phi$	can stand for a variety of differential

quantities, such as the mass fraction of a chemical species, the enthalpy or the temperature, a velocity component, the turbulent kinetic energy, or the turbulent dissipation energy. Additionally an appropriate meaning will have to be given to the diffusion coefficient  $\Gamma_{\phi}$  and the source term  $S_{\phi}$ .

#### 3.3.1 Fluid Flow Equations

##### 1) Equation of Continuity

If a value of unity is assigned to the general variable  $\phi$  and zero is assigned to the source term  $S_{\phi}$ , eq.: (3.3.1) leads to the continuity equations.

$$\frac{\partial}{\partial x}(\rho u) + \frac{\partial}{\partial y}(\rho v) = 0 \quad (3.3.2)$$



## 2) Equation of Motion

The general variable  $\phi$  stands for the velocity component  $u$  or  $v$ . In this case, the diffusion coefficients  $\Gamma_u$  and  $\Gamma_v$  are equal to the effective viscosity  $\mu_{\text{eff}}$  which is the sum of the molecular viscosity  $\mu$  and the turbulent viscosity  $\mu_t$ ,

$$\mu_{\text{eff}} = \mu + \mu_t \quad (3.3.3)$$

The source terms  $S_u$  and  $S_v$  contain terms associated with viscosity, pressure gradient, and velocity gradient.

The source term  $S_u$  for the momentum equation in X-direction is [46]:

$$S_u = -\frac{\partial p}{\partial x} + \frac{\partial}{\partial x} \left( \mu_{\text{eff}} \frac{\partial u}{\partial x} \right) + \frac{\partial}{\partial y} \left( \mu_{\text{eff}} \frac{\partial v}{\partial y} \right) - \rho g_x \quad (3.3.4)$$

where  $p$  is the time-smoothed static pressure

$\mu_{\text{eff}}$  is the effective viscosity

$g_x$  is the X-directional gravity coefficient

The sum of the static pressure gradient and gravitational force can be cancelled out. However, a pressure difference caused by the velocity field may occur. This pressure, called "pressure correction", is discussed in a later section [46, 47]. In the present case, isothermality is assumed so that the density is constant over the entire field.

Similarly, the source term  $S_v$  for the momentum equation in y-direction is represented as

$$S_v = -\frac{\partial p}{\partial y} + \frac{\partial}{\partial x} \left( \mu_{\text{eff}} \frac{\partial v}{\partial x} \right) + \frac{\partial}{\partial y} \left( \mu_{\text{eff}} \frac{\partial v}{\partial y} \right) \quad (3.3.5)$$

## 3) Transport Equation for Turbulent Properties

The concept of effective viscosity invented by Bousinesq was discussed in the previous section. The effective viscosity is the sum of a molecular viscosity and a turbulent viscosity. Although the molecular viscosity is a characteristic value of the fluid, the turbulent viscosity depends on the fluid motion and on the flow "history". In the present work a two-equation

known as k- $\epsilon$  model is used,

where  $k = \frac{1}{2} \sqrt{u'^2 + v'^2 + w'^2}$ , is the kinetic energy to turbulence

$\epsilon$  = rate of dissipation of k per unit mass.

In this model the turbulent viscosity is related to k and  $\epsilon$  by

$$\mu_t = C_D \rho k^2 / \epsilon$$

where  $C_D$  is a constant.  $\epsilon$  may also be expressed as

$$\epsilon = k^{3/2} / l$$

where  $l$  is a characteristic length scale of turbulence. Although this model contains some "vagueness", several comparisons between calculation and experiment seem to support its validity. Additionally these equations contain several constants which must be determined experimentally, but, as Spalding [44] mentioned, these constants vary little from one situation to another, so that they can be regarded to a certain extent as "universal". This simplicity makes the calculation of turbulence fields much easier, and especially in the engineering field, this model gives attractive insight into industrial scale reactor problems.

Transport Equations for k

The general variable  $\phi$  stands for the kinetic energy of turbulence k.

The differential transport equation can be written as:

$$\frac{\partial}{\partial x} (\rho u k) - \frac{\partial}{\partial y} (\rho v k) - \frac{\partial}{\partial x} (\Gamma_k \frac{\partial k}{\partial x}) - \frac{\partial}{\partial y} (\Gamma_k \frac{\partial k}{\partial y}) = S_k \quad (3.3.8)$$

where

$$S_k = G - D$$

The generation term;

$$G = \mu_t \left[ 2 \left\{ \left( \frac{\partial u}{\partial x} \right)^2 + \left( \frac{\partial v}{\partial y} \right)^2 \right\} + \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)^2 \right] \quad (3.3.9)$$

dissipation term

$$D = \rho \epsilon$$

and turbulent viscosity

$$\mu_t = \mu_{eff} - \mu_{lam} = c \rho k^2 / \epsilon \Rightarrow \mu_{lam}$$

The diffusion coefficient for turbulent energy  $\Gamma_k$  is supposed to be a property of the turbulence similar in magnitude to the effective viscosity

$$\Gamma_k = \frac{\mu_{eff}}{\sigma_k} \quad (3.3.10)$$

where  $\sigma_k$  is turbulent Prandtl number for the kinetic energy.

#### Transport Equation for $\epsilon$

The general variable  $\phi$  stands for the turbulent dissipation  $\epsilon$ . The differential transport equation can be written as

$$\frac{\partial}{\partial x} (\rho u \epsilon) + \frac{\partial}{\partial y} (\rho v \epsilon) + \frac{\partial}{\partial x} (\Gamma_\epsilon \frac{\partial \epsilon}{\partial x}) - \frac{\partial}{\partial y} (\Gamma_\epsilon \frac{\partial \epsilon}{\partial y}) = S_\epsilon \quad (3.3.11)$$

where

$$S_\epsilon = c_1 \frac{\epsilon}{k} G - c_2 \rho \frac{\epsilon^2}{k}$$

and  $G$  is a generation term which is mentioned above, and  $\Gamma_\epsilon$  is a diffusivity for turbulent dissipation energy described as

$$\Gamma_\epsilon = \frac{\mu_{eff}}{\sigma_\epsilon} \quad (3.3.12)$$

$\sigma_\epsilon$  is the Prandtl Number for turbulent dissipation energy. Prandtl numbers for both  $k$  and  $\epsilon$  are regarded to be in the vicinity of unity.

### 3.4 Boundary Conditions

In this section, the boundary conditions used for the fluid flow field are presented. The schematic boundary surfaces are shown in Fig. 3.1.

Boundary conditions for the present problem are classified into three categories, wall, free surface, and given velocity (i.e. up-leg and down-leg) boundaries. With reference to Fig. 3.1 the boundary conditions are as follows:

1) At  $x=0$ ,  $0 < y < y_1$ ,  $y_2 < y < y_3$ ,  $y_4 < y < y_5$  (at free surface)

$$u = \frac{\partial v}{\partial y} = 0 \quad (3.4.1)$$

$$\frac{\partial k}{\partial y} = \frac{\partial \epsilon}{\partial y} = 0 \quad (3.4.2)$$

2) At  $x=0$ ,  $y_1 < y < y_2$   $y_3 < y < y_4$  (at given velocity boundary)

$$u = U_{inlet} \quad (\text{at } y_1 < y < y_2), \quad u = -U_{inlet} \quad (\text{at } y_3 < y < y_4)$$

$$v = 0 \quad (3.4.3)$$

$$k = 0.05 \times [U_{inlet}]^2 \quad (3.4.4)$$

$$\epsilon = C_p k^{3/2} / (0.03 R_0) \quad (3.4.5)$$

$$(3.4.6)$$

where  $R_0$  is the radius of the up-leg or down-leg.

3) At  $y=0$  or  $y=y_5$ ,  $0 < x < x_5$  (at wall)

The "no-slip" condition is applied to the velocity at the wall

$$u = v = 0 \quad (3.4.7)$$

$$k = \epsilon = 0 \quad (3.4.8)$$

At a wall, boundary conditions called "wall-functions" must be included since the transport equations for several fluid dynamic characteristics are derived only for high Reynolds number flows. Close to the solid wall and some other interfaces, there are regions where the local Reynolds number of turbulence ( $\equiv R^{\frac{1}{2}} l / \nu$ , where  $l = R^{\frac{3}{2}} / \nu$ ) is so small that viscous effects

predominate over turbulent ones. The wall functions may be regarded as expressions for the momentum, energy and, mass transfer coefficients in the boundary layer. Therefore, the most appropriate wall-function to the situation should be chosen.

Fig. 3.1 shows the region where "wall-function" should be used. Fig. 3.2 describes the grid spacing along the wall. Now, the shear stress along the wall is uniform from wall to adjacent grid line. Then  $\tau_w$  may be regarded as a boundary condition for the u and v equations, and enters the generation term for the near-wall k. In the neighbourhood of the wall we can assume proportionality between mixing length and wall distance, so that

$$l = \kappa y \quad (3.4.9)$$

where  $\kappa$  denotes a dimensionless constant which must be deduced from experiment. On the other hand, according to Prandtl's assumption the turbulent shear stress becomes

$$\tau = \rho \kappa^2 y^2 \left( \frac{\partial u}{\partial y} \right)^2 \quad (3.4.10)$$

Introducing the friction velocity

$$u_0^* = \sqrt{\frac{\tau_w}{\rho}} \quad (3.4.11)$$

where  $\tau_w$  is the shear stress at the wall we obtain

$$u_0^* = \kappa y^2 \left( \frac{du}{dy} \right)^2 \quad (3.4.12)$$

Integrating equ. (3.4.12), we obtain

$$u = \frac{u_0^{*2}}{\kappa} \ln y + C \quad (3.4.13)$$

Because we assumed  $\tau = \text{constant}$ , equ. (3.4.13) is only valid in the neighborhood of the wall. Again, introducing the dimensionless distance from the wall,  $y^+ = y u_0^* / \nu$  we then modify equ. (3.4.13) to the following form

$$\frac{u}{u_0^*} = \frac{1}{\kappa} \ln y^+ + D_1 \quad (3.4.14)$$

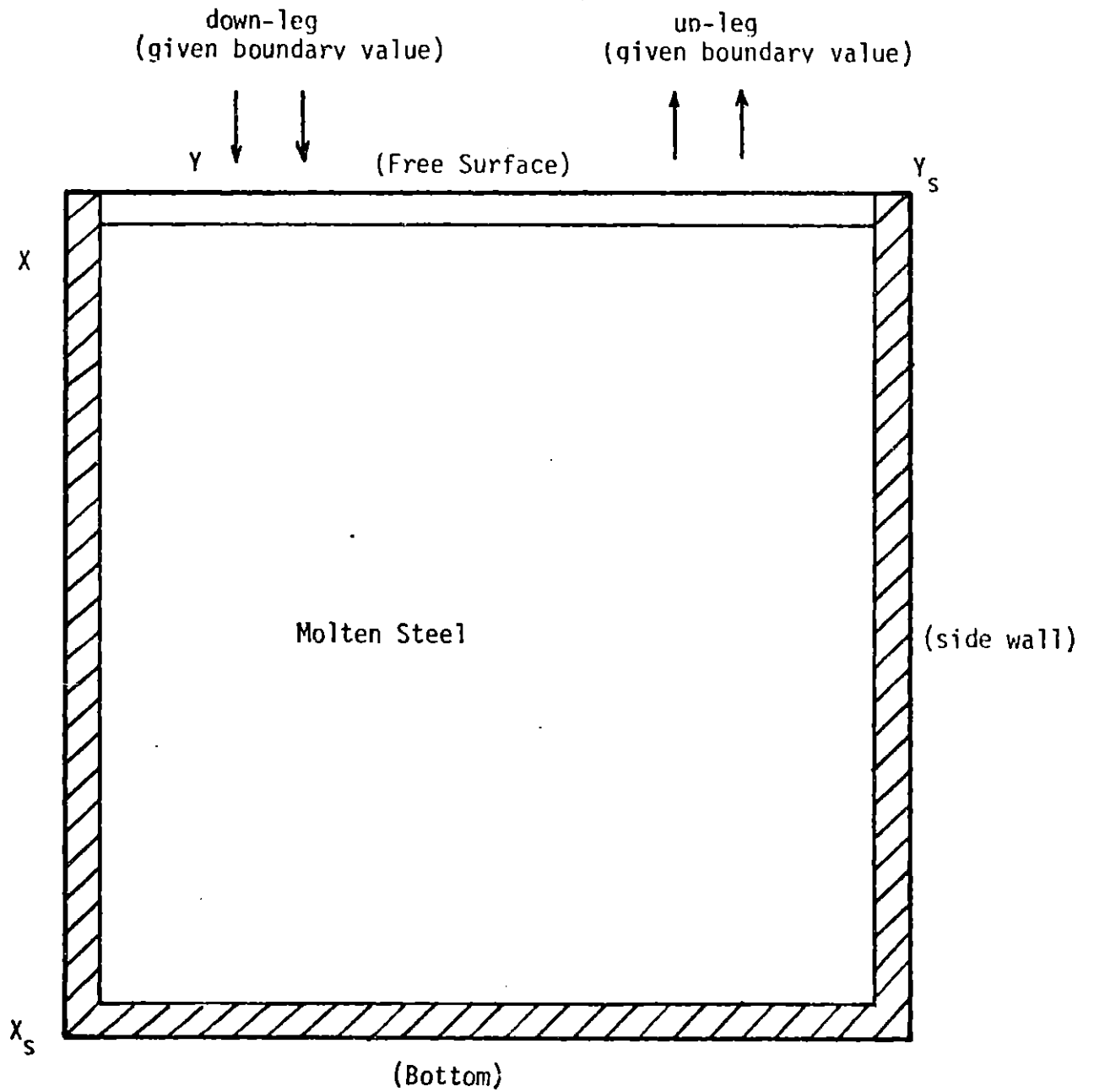


Fig. 3.1 Regions (hatched) for wall function

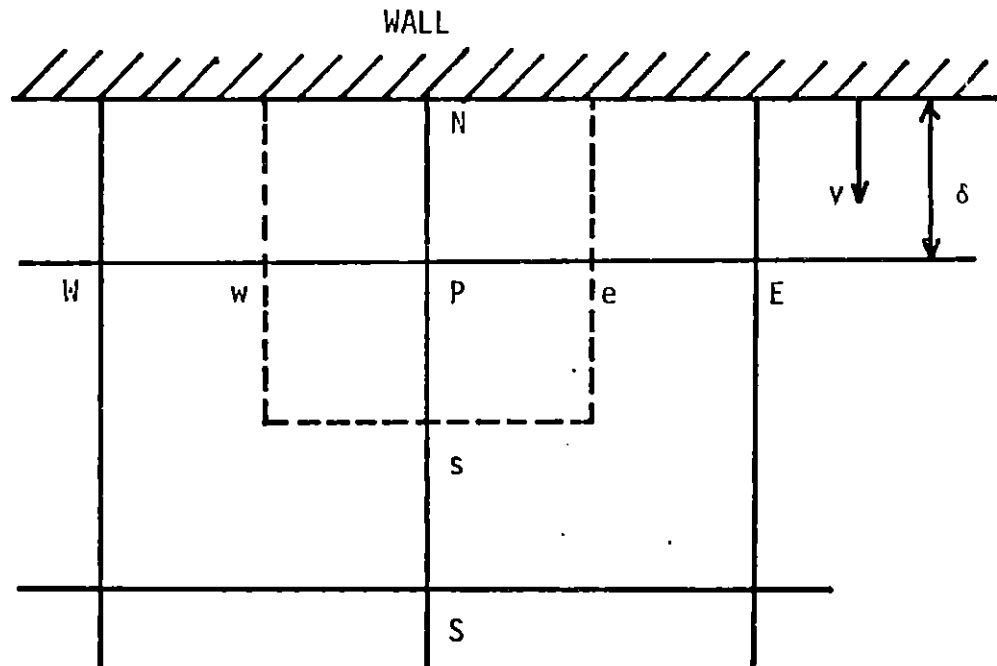


Fig. 3.2 Grid spacing near walls

where  $k$  and  $D_1$  are constants which may be determined experimentally, so that

$$A_1 = \frac{1}{k} = 2.5 \qquad D_1 = -\frac{1}{k} \ln \beta \qquad (3.4.15)$$

$\beta$  is determined as 0.111 from the experimental results by Nikuradse. Finally, we obtain the velocity distribution in the wall region as

$$u^+ = \frac{1}{k} \ln (E y^+) \qquad (3.4.16)$$

where  $E$  is 9.0.

Equ. (3.4.16) is only valid in the near wall region (i.e.  $y^+ < 11.5$ ). Usually the near wall grid point,  $P$ , is sufficiently remote from the wall grid point,  $w$ , that the turbulent effects at  $P$  totally overwhelm the viscous effects. Spalding proposed the following equation for the momentum flux:

$$\frac{\bar{U}_p}{(\tau/\rho)_w} C_{\mu}^{\frac{1}{4}} k_p^{\frac{1}{5}} = \frac{1}{k} \ln \left[ E y_p \frac{(C_{\mu}^{\frac{1}{4}} k_p)^{\frac{1}{5}}}{\nu} \right] \qquad (3.4.17)$$

here  $\bar{U}_p$ ,  $\tau_w$  and  $y_p$  are respectively the time average velocity of the fluid at point  $p$  along the wall, the shear stress on the wall, and the distance of point  $p$  from the wall. This relationship is used as the boundary condition for the velocity.



### 3.5 General Equations for Particle Transfer and Coagulation

The general equations describing particle transfer and coagulation are now presented. These equations are represented by the time-smoothed equation of mass transfer (particle transfer). The differential equations for particle coalescence are given for each class of size. In the present calculation sizes are classified into ten groups. It is assumed that when the particles grown to the maximum size they float up, so that the concentration of particles larger than the maximum size has no effect on the coagulation behavior of the particles.

Generally the number density  $f(x, m, t)$  of particles satisfies the following equation.

$$\begin{aligned} \frac{\partial J}{\partial t} + \frac{\partial}{\partial x}(uJ) + \frac{\partial}{\partial y}(vJ) - \frac{\partial}{\partial x}(\Gamma_f \frac{\partial J}{\partial x}) - \frac{\partial}{\partial y}(\Gamma_f \frac{\partial J}{\partial y}) + G \\ = B(c, \theta, r) + \alpha(x, m, t) + \beta(x, m, t) \end{aligned} \quad (3.5.1)$$

Where  $G$  is the growth by diffusion

$\alpha(x, m, t)$  is the coagulation of particles

$B(x, m, t)$  is the rate of nucleation

$\beta(x, m, t)$  is the breakage of particles

$C$  is bulk concentration of chemical species

$\theta$  is temperature

$\Gamma_f$  is diffusion coefficient for particles.

Now, it is assumed that the growth rates by diffusion and nucleation are ignored and also, the rate of breakage is too small to be considered. Then equ. (3.5.1) can be reduced to

$$\frac{\partial J}{\partial t} + \frac{\partial}{\partial x}(uJ) + \frac{\partial}{\partial y}(vJ) - \frac{\partial}{\partial x}(\Gamma_f \frac{\partial J}{\partial x}) - \frac{\partial}{\partial y}(\Gamma_f \frac{\partial J}{\partial y}) = \alpha(x, m, t) \quad (3.5.2)$$

here  $\alpha(x, m, t)$  maybe defined as

$$\alpha(x, m, t) = \frac{1}{2} \int a(x, m, t) f(x, m-m', t) f(x, m', t) dm' - f(x, m, t) \int a(x, m, t) f(x, m', t) dm' \quad (3.5.3)$$

where  $\alpha(m, x, t)$  is the rate of collision. Equ. (3.5.3) is an integro-differential equation in particle number density  $f(x, m, t)$ , and it is difficult to solve explicitly. In order to solve this equation using finite difference methods, it is necessary to establish the discretized equation for each group of particle sizes.

Defining the particle concentration for the  $i$ th group of size,  $C_i$ , equ. (3.5.2) becomes

$$\frac{\partial(\rho C_i)}{\partial t} + \frac{\partial(\rho u C_i)}{\partial x} + \frac{\partial(\rho v C_i)}{\partial y} - \frac{\partial}{\partial x} \left( \Gamma_{c,i} \frac{\partial C_i}{\partial x} \right) - \frac{\partial}{\partial y} \left( \Gamma_{c,i} \frac{\partial C_i}{\partial y} \right) = S_{c,i} \quad (3.5.4)$$

$(i=1, \dots, 10)$

where  $\Gamma_{c,i}$  is diffusion coefficient of particles of the  $i$ th size group.

Strictly speaking,  $\Gamma_{c,i}$  depends on the particle size, but, as mentioned in Chapter 2, the dependence of particle diffusivity on size is so small that in the present computation it may be ignored.

Thus

$$\Gamma_c = \frac{\mu_{eff}}{\sigma_c}$$

Here  $\sigma_c$  is turbulent Prandtl number for particle diffusivity. This value varies as shown in Fig. 2.5. In the present work a value of 1.0 was employed.

The modeling of the source term is one of the most essential points in this work. The first problem which we will consider is whether two particles colliding at steel making temperatures will rapidly form a single sphere. This effect may depend on the surface energy. Generally, studies performed on silica inclusions show that when two particles collide they usually sinter or coalesce together rapidly to form a single larger sphere [51]. On the other hand, it is reported that primary inclusions other than silica may or may not coalesce after they collide and stick, and that large interconnected

clusters form [51].

The various schematic coalescence models are shown in Fig. 3.3. Case I shows that collided particles become a single sphere and Case II shows that they only stick and form clusters. Case III shows the intermediate case between I and II. Although the resultant particles in these three cases have the same volume, the characteristic diameter may differ, so that the behavior in turbulent flow may differ. Smolchowski's model, discussed in Chapter 2, represents Case II (e.g. clustering). However, if we employ the coagulation derived from Case II, mass conservation is violated. Since the main purpose of this work is to simulate the deoxygenation process, this error may not be allowed. Therefore, we employed the assumptions as follows:

- 1) collided particles immediately form a single sphere
- 2) only two particles are involved in the collision

Fig. 3.4 - 3.6 show the collided particle sizes in Case I, II and III respectively. In Case II, approximately half of the collided particles grow to a diameter of more than  $20\mu\text{m}$ , which is now considered to be a critical size after the first collision. Therefore, if the coagulation model, Case II, is employed, the rate of particle growth by collision will be much faster than that predicted by the Case I model. However, when collided particles do not form a spherical particle, the Case II or Case III models, represent a better description of the turbulent flow agglomeration process than Case I.

Since present calculations assume the formation of spherical particles after collision, Case I is employed for the coagulation model. The problem is how to treat the source terms so that the mass continuity among each class of size is conserved. For example, when particles of  $12\mu\text{m}$  and  $14\mu\text{m}$  diameter collide with each other a particle of  $16.471\mu\text{m}$  diameter is formed. This particle is located between the  $16\mu\text{m}$  diameter class and  $18\mu\text{m}$  diameter

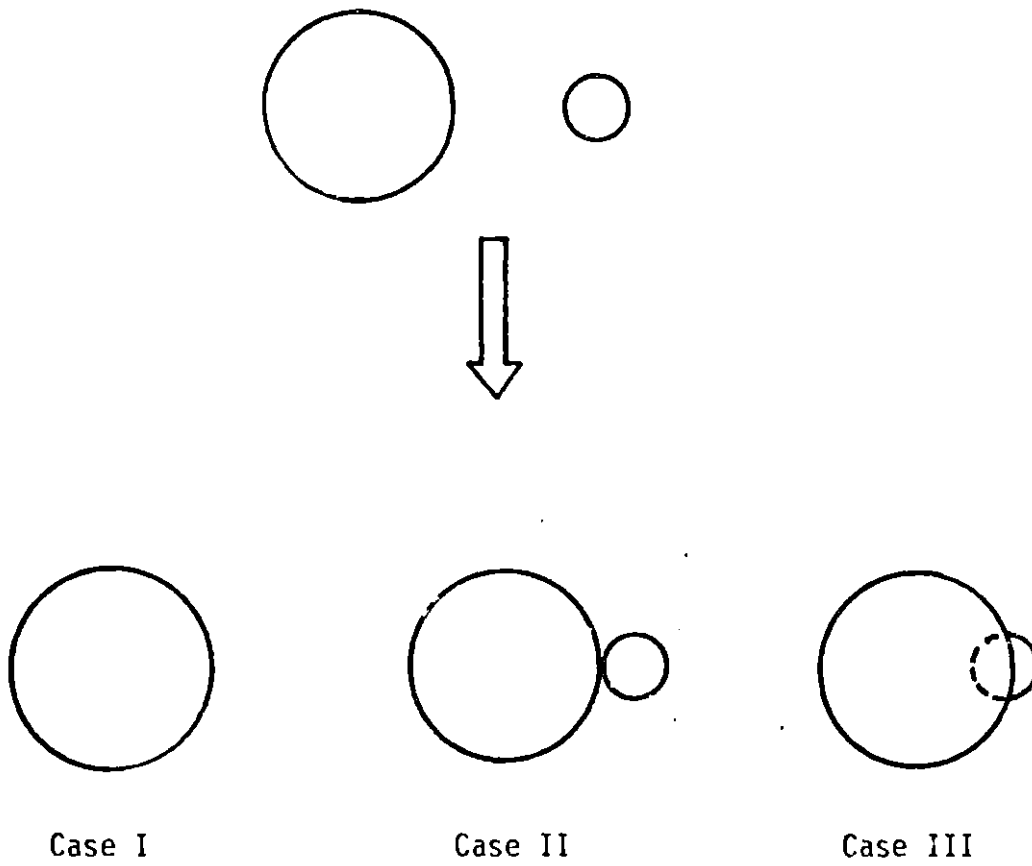
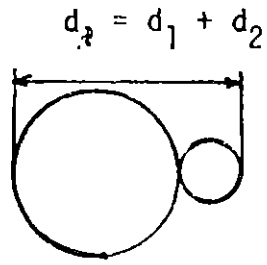


Fig. 3.3 Schematic coalescence models

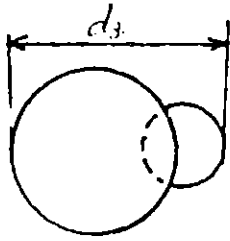
	2	4	6	8	10	12	14	16	18	20
2	2.520	4.160	6.070	8.040	10.027	12.018	14.014	16.010	18.008	20.007
4		5.04	6.542	8.320	10.209	12.146	14.108	16.083	18.066	20.053
6			7.560	8.996	10.674	12.451	14.358	16.276	18.219	20.178
8				10.079	11.478	13.084	14.822	16.641	18.512	20.418
10					12.599	13.973	15.528	17.208	18.975	20.801
12						15.119	16.475	17.992	19.608	21.347
14							17.639	18.982	20.469	22.066
16								21.492	21.492	22.955
18									22.679	24.005
20										25.198

Fig. 3.4 Coalesced particle size for Case I



	2	4	6	8	10	12	14	16	18	20
2	4	6	8	10	12	14	16	18	20	22
4		8	10	12	14	16	18	20	22	24
6			12	14	16	18	20	22	24	26
8				16	18	20	22	24	26	28
10					20	22	24	26	28	30
12						24	26	28	30	32
14							28	30	32	34
16								32	34	36
18									36	38
20										40

Fig. 3.5 Coalesced particle size for Case II



$$d_3 = \frac{(d_1 + d_2) + d_1}{2}$$

	2	4	6	8	10	12	14	16	18	20
2	3	5	7	9	11	13	15	17	19	21
3		6	8	10	12	14	16	18	20	22
6			9	11	13	15	17	19	21	23
8				12	14	16	18	20	22	24
10					15	17	19	21	23	25
12						18	20	22	24	26
14							21	23	25	27
16								24	26	28
18									27	29
20										30

Fig. 3.6 Coalesced particle size for Case III

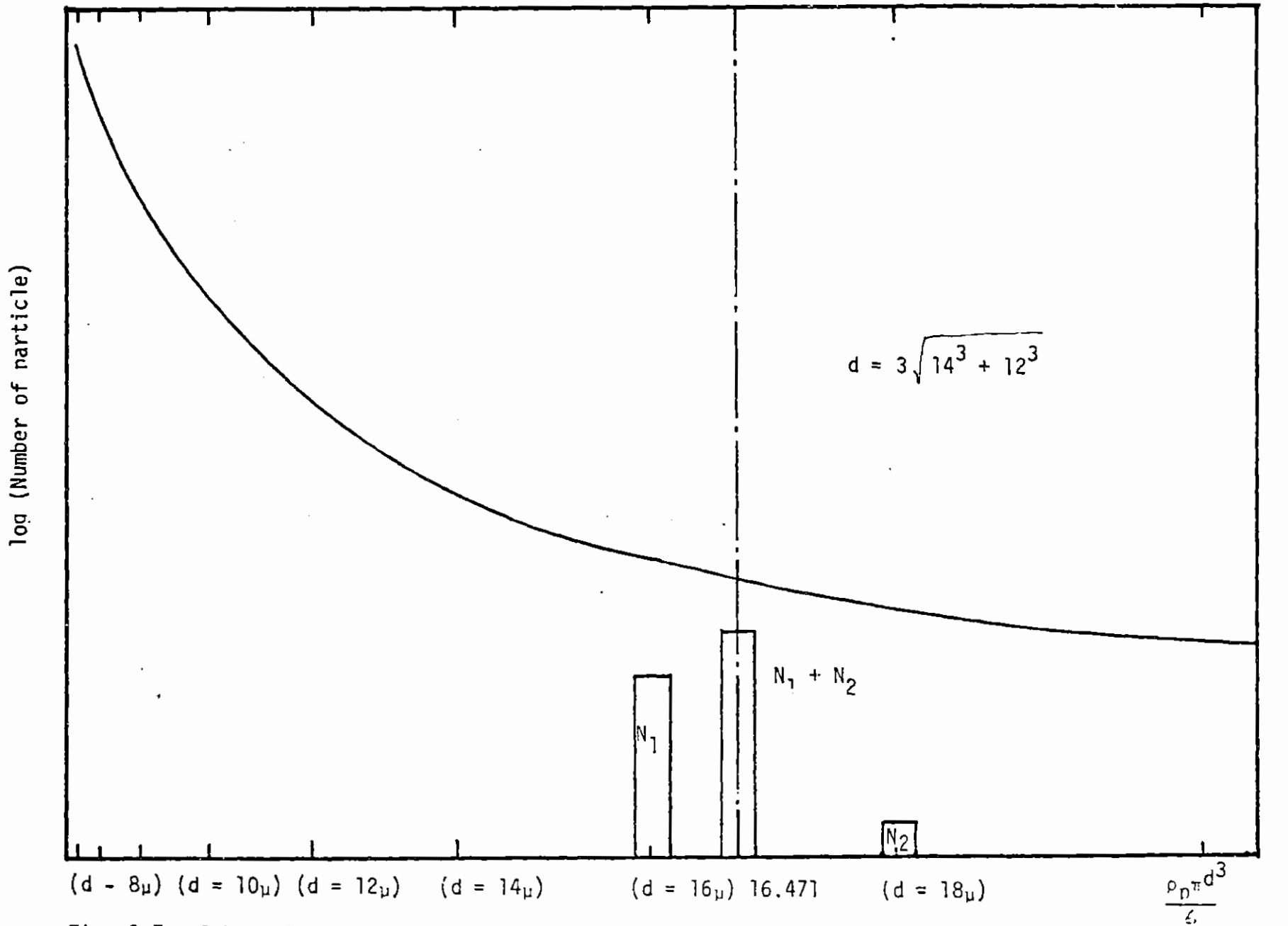


Fig. 3.7 Schematic representation of particle distribution



(um)

$d_1 \backslash d_2$	2	4	6	8	10	12	14	16	18	20
2	2.5998	4.1601	6.0731	8.0423	10.0114	12.0154	14.0132	16.0100	18.0077	20.0061
	4.0162	4.0764	6.0930	8.0933	10.0951	12.0973	14.0972	16.0978	18.0976	20.0973
	2.0552	6.0121	8.0107	10.0113	12.0101	14.0007	16.0005	18.0004	20.0003	22.0002
4		5.0596	6.5420	8.3202	10.2057	12.1061	14.1076	16.0525	18.0651	20.0526
		4.0571	6.0733	8.0869	10.0972	12.0937	14.0928	16.0963	18.0970	20.0976
		6.0620	8.0211	10.0131	12.0098	14.0069	16.0047	18.0036	20.0029	22.0025
6			7.5594	8.9757	10.6734	12.4502	14.3577	16.2760	18.2190	20.1775
			6.0274	8.0557	10.0734	12.0788	14.0824	16.0878	18.0906	20.0915
			8.0796	10.0645	12.0491	14.0215	16.0096	18.0122	20.0092	22.0083
8				10.0791	11.4773	13.0559	14.8212	16.6402	18.5115	20.4173
				10.0907	10.0276	12.0492	14.0625	16.0753	18.0976	20.0809
				12.0186	12.0701	14.0523	16.0383	18.0167	20.0359	22.0191
10					12.5957	13.9724	15.5274	17.2080	18.9745	20.8002
					12.0734	12.0016	14.0266	16.0422	18.0596	20.0627
					14.0061	14.0954	16.0734	18.0573	20.0416	22.0377
12						15.1186	16.4249	17.9712	19.6258	21.0652
						14.0276	16.0736	18.0009	19.0003	21.0970
						16.0504	18.0114	19.0973	20.0776	22.0027
14							17.0384	18.7819	20.4633	22.0652
							16.0184	18.0533	20.0788	22.0970
							18.0506	20.0417	22.0173	24.0027
16								20.1581	21.4919	22.9865
								20.0925	20.0222	22.0540
								22.0022	22.0727	24.0433
18									22.6771	24.0031
									22.0806	24.0972
									24.0377	26.0028
20										25.9776
										26.0405
										26.0575

Fig. 3.8 Collided particle size and the weighting factor for source terms

class (Fig. 3.7). Here the number of particles formed by collision can be calculated from equ. (2.5.6). The calculated number of collided particles may be between the discretized class. The size of collided particles is listed in the upper row in Fig. 3.8. This collided number is divided into each class so as to be inversely proportional to the mass scale. In this way, the sum of mass before collision become equal to that after collision. The coefficient of the weighting function is shown in the middle and the lower row of Fig. 3.8.

The final representation of the source terms is shown in Table 3.1 in an explicit form.

Table 3.1 Governing Equation for Particle Coalescence

$$\frac{\partial n_i}{\partial t} + \frac{\partial}{\partial x} (u n_i) + \frac{\partial}{\partial y} (v n_i) - \frac{\partial}{\partial x} \left( E \frac{\partial n_i}{\partial x} \right) - \frac{\partial}{\partial y} \left( E \frac{\partial n_i}{\partial y} \right) = S_{\phi, i}$$

$$(i = 1, \dots, 10)$$

$$S_{\phi, i} = S_{u, i} + S_{p, i}, \quad n_i \quad E = \frac{\nu_{\text{eff}}}{\rho \sigma_{c, i}}$$

$$n = 1$$

$$S_{u, 1} = 0.0$$

$$S_{p, 2} = -0.1428 \alpha_{1, 1} n_1 - \sum_{j=2}^{10} \alpha_{1, j} n_j$$

$$n = 2$$

$$S_{u, 2} = 0.1428 \times \frac{1}{2} n_1^2$$

$$S_{p, 2} = -0.0526 \times \alpha_{2, 1} \times n_1 - 0.4216 \times \frac{1}{2} \alpha_{22} n_2 - \sum_{j=3}^{10} \alpha_{2, j} n_j$$

$$n = 3$$

$$S_{u, 3} = 0.0526 \alpha_{2, 1} n_1 n_2 + 0.4210 \frac{\alpha_{22}}{2} \times n_2 n_2$$

$$S_{p, 3} = -0.027 \alpha_{13} n_1 - 0.2162 \alpha_{23} n_2 - 0.7293 \alpha_{33} n_3 - \sum_{j=4}^{10} \alpha_{3, j} n_j$$

$$n = 4$$

$$S_{u, 4} = 0.027 \alpha_{31} n_3 n_1 + 0.2162 \alpha_{23} n_3 n_2 + 0.7296 \frac{\alpha_{33}}{2} n_3^2$$

$$S_{p, 4} = -0.0163 \alpha_{14} n_1 - 0.1311 \alpha_{24} n_2 - 0.4425 \alpha_{3, 4} n_3 - \sum_{j=4}^{10} \alpha_{j4} n_j$$

Table 3.1 (cont'd)

n = 5

$$S_{u,5} = 0.0163 \alpha_{41} n_1 n_4 + 0.1311 \alpha_{42} n_2 n_4 + 0.4425 \alpha_{43} n_4 n_3 \\ + 0.9671 \frac{\alpha_{44}}{2} n_4 n_4$$

$$S_{p,5} = -0.0109 \alpha_{51} n_1 - 0.0878 \alpha_{25} n_2 - 0.2966 \alpha_{35} n_3 - 0.7031 \alpha_{45} n_4 \\ - \sum_{j=5}^{10} \alpha_{5j} n_j$$

n = 6

$$S_{u,6} = 0.0329 \alpha_{44} \frac{n_4^2}{2} + 0.0109 \alpha_{51} n_5 n_1 + 0.0878 \alpha_{52} n_2 n_5 \\ 0.2966 \alpha_{35} n_3 n_5 + 0.7031 \alpha_{45} n_4 n_5 + 0.7324 \frac{n_5^2}{2}$$

$$S_{p,6} = 0.0077 \alpha_{61} n_1 - 0.0629 \alpha_{62} n_2 - 0.2125 \alpha_{63} n_3 - 0.5038 \alpha_{64} n_4 \\ - 0.9840 \alpha_{65} n_5 - \sum_{j=6}^{10} \alpha_{6j} n_j$$

n = 7

$$S_{u,7} = 0.2676 \alpha_{55} \frac{n_5^2}{2} + 0.0077 \alpha_{61} n_6 n_1 + 0.0629 \alpha_{62} n_6 n_2 \\ 0.2125 \alpha_{63} n_6 n_3 + 0.5038 \alpha_{64} n_6 n_4 + 0.9840 n_6 n_5 + 0.4736 \alpha_{66} \frac{n_6^2}{2}$$

$$S_{p,7} = -0.0058 \alpha_{17} n_1 - 0.0472 \alpha_{27} n_2 - 0.1596 \alpha_{37} n_3 - 0.3785 \alpha_{47} n_4 \\ - 0.7394 \alpha_{57} n_5 - 0.7836 \alpha_{67} n_6 - \sum_{j=7}^{10} \alpha_{7j} n_j$$

TABLE 3.1 (cont'd)

n = 8

$$S_{u,8} = 0.5264 \alpha_{66} \frac{n_6^2}{2} + 0.0058 \alpha_{17} n_1 n_7 + 0.0472 \alpha_{27} n_2 n_7 + 0.1592 \alpha_{37} n_3 n_7 \\ + 0.3785 \alpha_{47} n_4 n_7 + 0.7394 \alpha_{57} n_5 n_7 + \alpha_{67} n_6 n_7 + 0.1984 \alpha_{77} \frac{n_7^2}{2}$$

$$S_{p,8} = - 0.0044 \alpha_{81} n_1 - 0.0367 \alpha_{82} n_2 - 0.1242 \alpha_{83} n_3 - 0.2947 \alpha_{84} n_4$$

$$- 0.5758 \alpha_{85} n_5 - 0.9951 \alpha_{86} n_6 - \sum_{j=7}^{10} \alpha_{7j} n_j$$

n = 9

$$S_{u,9} = 0.2164 \alpha_{76} n_6 n_7 + 0.8016 \alpha_{77} \frac{n_7^2}{2} + 0.0044 \alpha_{81} n_8 n_1 + 0.0367 \alpha_{82} n_8 n_2$$

$$+ 0.1242 \alpha_{83} n_8 n_3 + 0.2947 \alpha_{84} n_8 n_4 + 0.5758 \alpha_{85} n_8 n_5$$

$$+ 0.9951 \alpha_{86} n_8 n_6 + 0.5252 \alpha_{87} n_8 n_7$$

$$S_{p,9} = - 0.0035 \alpha_{91} n_1 - 0.0293 \alpha_{92} n_2 - 0.0994 \alpha_{93} n_3 - 0.2359 \alpha_{94} n_4$$

$$- 0.4610 \alpha_{95} n_5 - 0.17967 \alpha_{96} n_6 - \sum_{j=7}^{10} \alpha_{9j} n_j$$

n = 10

$$S_{u,10} = 0.4647 \alpha_{87} n_8 n_7 + 0.9278 \alpha_{88} \frac{n_8^2}{2} + 0.0035 \alpha_{91} n_9 n_1$$

$$+ 0.0293 \alpha_{92} n_9 n_2 + 0.0994 \alpha_{93} n_9 n_3 + 0.2359 \alpha_{94} n_9 n_4$$

$$+ 0.4610 \alpha_{95} n_9 n_5 + 0.7967 \alpha_{96} n_9 n_6 + 0.7828 \alpha_{97} n_9 n_7$$

$$+ 0.2722 \alpha_{98} n_9 n_8$$

$$S_{p,10} = - 0.0027 \alpha_{10,1} n_1 - 0.0239 \alpha_{10,2} n_2 - 0.0813 \alpha_{10,3} n_3$$

$$- 0.1931 \alpha_{10,4} n_4 - 0.3773 \alpha_{10,5} n_5 - \sum_{j=6}^{10} \alpha_{10,j} n_j$$

### 3.6 Boundary Conditions for Particle Coagulation Equation

Referring to Fig. 3.1 once more, the boundary conditions for the particle coagulation equation are written as follows:

$$1) \text{ at } x=0 \text{ and } 0 < y < y_1, y_2 < y < y_3, y_4 < y < y_5 \text{ (at free surface)}$$

$$\frac{\partial C_i}{\partial y} = 0 \quad (i=1,10) \quad (3.6.1)$$

$$2) \text{ at } x=0 \text{ and } y_1 < y < y_2, y_3 < y < y_4 \text{ (at the up- and down leg)}$$

$$C_i(\text{up-leg}) = C_i(\text{down-leg})$$

$$(i=1,10) \quad (3.6.2)$$

$$3) \text{ at } y=0 \text{ or } y=y_5 \text{ and } 0 < x < x_s \text{ (at the wall)}$$

By using the mass transfer coefficient expression of Friedlander, the particle flux,  $q$ , from the fluid to the wall can be expressed as;

$$\frac{q}{V_p(C_N - C_p)} = \frac{\frac{f}{2}}{1 + \sqrt{\frac{f}{2}} \left( \frac{1.525}{S^{+2}} - 50.6 \right)}$$

$$= \frac{\tau_w / \rho V_p^2}{1 + \sqrt{\frac{\tau_w}{\rho V_p^2}} \left( \frac{1.525}{S^{+2}} - 50.6 \right)} \quad (3.6.3)$$

$C_n$ ; the particle density at the node N

$C_p$ ; the particle density at the wall (=0)

$f$ ; the friction coefficient

$S^+$ ; non dimensional stopping length (equ. 2.6.14)

$\tau_w$ ; the shear stress on the wall

## Chapter 4 Numerical Technique in Computation

In this chapter we shall present an outline of the numerical technique used for solving the differential equations developed in the preceding chapter.

### 4.1 Derivation of Finite-Difference Equations

In this section the reduction of finite-difference equations both for fluid flow and particle coagulation is discussed. The finite difference equations can be obtained by discretizing the general elliptic partial differential equations.

#### 4.1.1 Derivation of the Finite-Difference Equation

The derivation of the finite-difference equation for a general elliptic, partial differential equations is summarized.

The general two dimensional elliptic differential equation (Steady State) has the following form

$$\frac{\partial}{\partial x}(\rho u \phi) + \frac{\partial}{\partial y}(\rho v \phi) - \frac{\partial}{\partial x}(\Gamma_{\phi} \frac{\partial \phi}{\partial x}) - \frac{\partial}{\partial y}(\Gamma_{\phi} \frac{\partial \phi}{\partial y}) = S_{\phi} \quad (4.1.1)$$

convective term
diffusive term
source term

This partial differential equation can be written as follows:

$$\frac{\partial \phi_1}{\partial x} + \frac{\partial \phi_2}{\partial y} = S_{\phi} \quad (4.1.2)$$

where

$$\phi_1 = (\rho u \phi) - \Gamma_{\phi} \frac{\partial \phi}{\partial x}$$

$$\phi_2 = (\rho v \phi) - \Gamma_{\phi} \frac{\partial \phi}{\partial y}$$

Usually in a convective flow the diffusion term is negligible, while for a quiescent liquid the convective term is small in comparison to the diffusion term. The "central-difference scheme" leads to numerical instabilities when applied to strongly convective flows. In order to compensate for this, several algorithms have been suggested by Patankar [46]. These are 1) the upwind scheme, 2) the exponential scheme, 3) the Hybrid scheme, and 4) the

power-law scheme. Here we shall consider a steady one-dimensional convection and diffusion equation with no source term:

$$\rho u \phi - \Gamma_{\phi} \frac{\partial \phi}{\partial x} = 0 \quad (4.1.3)$$

This equation can be solved exactly when  $\Gamma_{\phi}$  is a constant and with the following boundary conditions:

$$\text{at } x=0 \quad \phi = \phi_0$$

$$\text{at } x=L \quad \phi = \phi_L$$

The solution is

$$\frac{\phi - \phi_0}{\phi_L - \phi_0} = \frac{\exp(P_e x/L) - 1}{\exp(P_e) - 1} \quad (4.1.4)$$

where  $P_e$  is a Peclet number defined by:

$$P_e = \frac{\rho u L}{\Gamma_{\phi}} \quad (4.1.5)$$

The Peclet number is the ratio of the strength of convection to diffusion. The characteristic of equation (4.1.4) is shown in Fig. 4.1. When  $P_e$  is very large, the value of  $\phi$  in the domain is influenced by the upstream value of  $\phi$ . Fig. 4.2 shows part of the orthogonal grid with a typical node P and the surrounding nodes E, W, N and S. The exact solution of the one dimensional convection diffusion equation may be written as a finite-difference equation as follows:

$$F_e \left( \phi_p - \frac{\phi_p - \phi_E}{\exp(P_e) - 1} \right) - F_w \left( \phi_w + \frac{\phi_w - \phi_p}{\exp(P_e) - 1} \right) = 0 \quad (4.1.6)$$

This finite-difference form can be transformed into a standard form:

$$a_p \phi_p = a_E \phi_E + a_w \phi_w \quad (4.1.7)$$

where

$$a_E = \frac{F_e}{\exp(F_e/D_e) - 1} \quad (4.1.8)$$

$$a_w = \frac{F_w \exp(F_w/D_w)}{\exp(F_w/D_w) - 1} \quad (4.1.9)$$



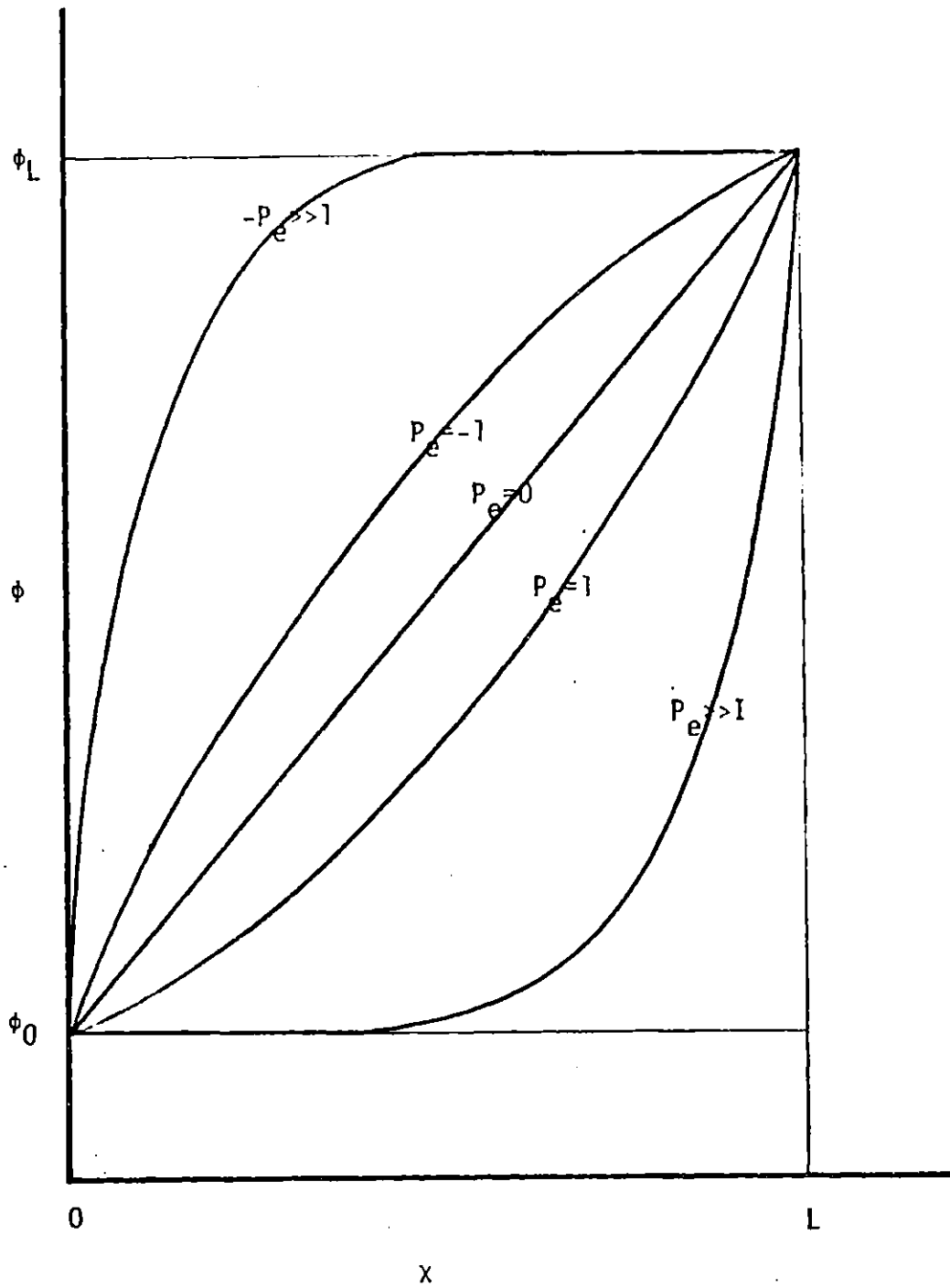


Fig. 4.1 Exact solution for the one dimensional convection-diffusion problem

and

$$F = \rho u \quad D = \bar{\Gamma} \phi / \delta x$$

This is called the exponential scheme. Although this scheme is theoretically exact, it requires a large amount of computation time, and is therefore not practicable. The simplest approximation of the exact finite-difference scheme is the so called "upwind scheme". When  $F_e$  (and also  $F_w$ ) is larger than zero

$$a_E = \frac{F_E}{(1 + F_E/D_E) - 1} = D_E \quad (4.1.10)$$

$$a_W = \frac{F_W (1 + F_W/D_W)}{(1 + F_W/D_W) - 1} = D_W + F_W \quad (4.1.11)$$

On the other hand, when  $F_e$  (and  $F_w$ ) is smaller than zero

$$a_E = \frac{F_E \exp(-F_E/D_E)}{1 - \exp(-F_E/D_E)} = D_E - F_E \quad (4.1.12)$$

$$a_W = D_W \quad (4.1.13)$$

Equations (4.1.10) ~ (4.1.13) can be written in a more correct form as:

$$\begin{aligned} a_e &= D_e + \llbracket -F_e, 0 \rrbracket \\ a_w &= D_w + \llbracket F_w, 0 \rrbracket \end{aligned} \quad (4.1.14)$$

$$a_p = a_e + a_w + (F_e - F_w)$$

where  $\llbracket \quad \rrbracket$  denotes the largest of the arguments contained within it.

A more precise approximation of the exact solution was developed by Spalding.

From (4.1.12) it follows that

$$\frac{a_e}{D_e} = \frac{Pe}{\exp(Pe) - 1} \quad (4.1.15)$$

The variation of  $a_e/D_e$  with Peclet number is shown in Fig. 4.1. The hybrid scheme consists of three parts.

$$\text{for } Pe < -2 \quad \frac{a_e}{D_e} = -Pe \quad (4.1.16)$$

$$\text{for } -2 \leq Pe \leq 2 \quad \frac{a_e}{D_e} = 1 - \frac{Pe}{2}$$

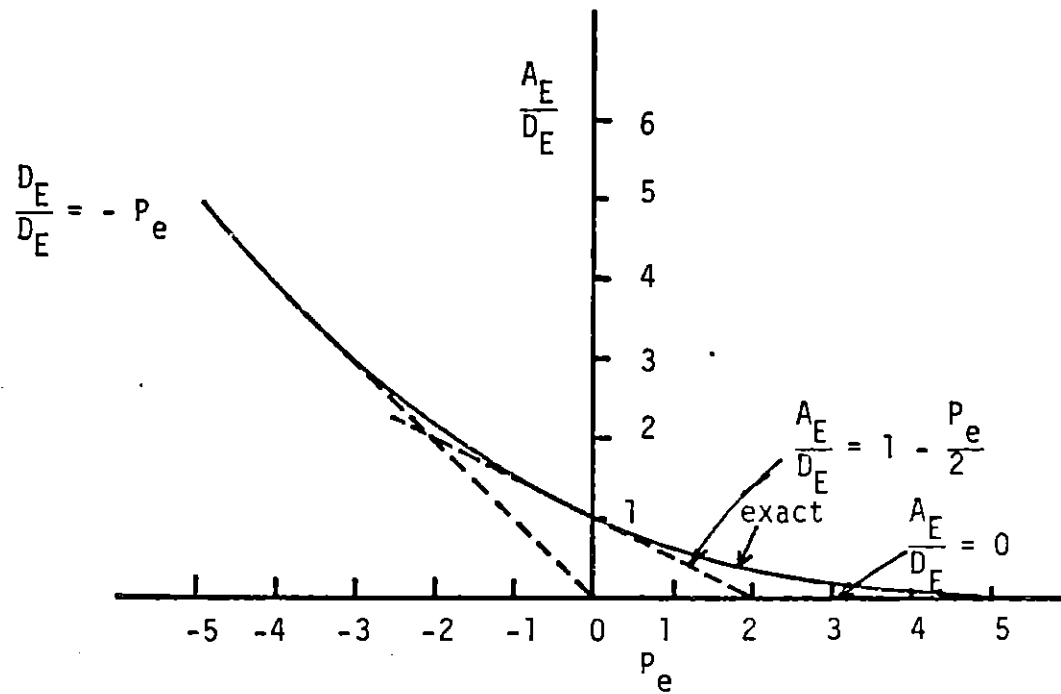


Fig. 4.2 Variation of the coefficient  $A_E$  with Peclet number

$$\text{for } P_e > 2 \quad \frac{a_e}{D_e} = 0$$

These three equations can be expressed in a more convenient form as

$$\begin{aligned} a_e &= \left[ -F_e, D_e - \frac{F_e}{2}, 0 \right] \\ a_w &= \left[ F_w, D_w + \frac{F_w}{2}, 0 \right] \\ a_p &= a_e + a_w + (F_x - F_w) \end{aligned} \quad (4.1.17)$$

We have discussed several schemes for the general one-dimensional elliptic partial differential equation. Similarly, the two-dimensional discretization equations can be written as

$$a_p \phi_p = a_e \phi_e + a_w \phi_w + a_n \phi_n + a_s \phi_s + b \quad (4.1.18)$$

where

$$\begin{aligned} a_e &= D_e A(|P_e|) + \left[ -F_e, 0 \right] \\ a_w &= D_w A(|P_w|) + \left[ F_w, 0 \right] \\ a_n &= D_n A(|P_n|) + \left[ -F_n, 0 \right] \\ a_s &= D_s A(|P_s|) + \left[ F_s, 0 \right] \\ b &= S_c \Delta x \Delta y \\ a_p &= a_e + a_w + a_n + a_s - S_p \Delta x \Delta y \end{aligned} \quad (4.1.19)$$

In this expression,  $A(|P_e|)$  depends the scheme used and is shown in Table

4.1.  $F_e$ ,  $F_w$ ,  $F_n$ , and  $F_s$  are the mass flow rates through the surfaces of the control volume.

$$\begin{aligned} F_e &= (\rho u)_e \Delta y \\ F_w &= (\rho u)_w \Delta y \\ F_n &= (\rho v)_n \Delta x \\ F_s &= (\rho v)_s \Delta x \end{aligned} \quad (4.1.20)$$

$D_e$ ,  $D_w$ ,  $D_n$ , and  $D_s$  are the diffusion conductances through the faces and are defined as follows:

$$\begin{aligned} D_e &= \frac{F_e \Delta y}{(\delta x)_e} \\ D_w &= \frac{F_w \Delta y}{(\delta x)_w} \\ D_n &= \frac{F_n \Delta x}{(\delta y)_n} \\ D_s &= \frac{F_s \Delta x}{(\delta y)_s} \end{aligned} \quad (4.1.21)$$

Table 4.1 The function  $A(|P|)$  for different schemes (by Patankar)

Scheme	Formulation for $A( P )$
Central difference	$1 - 0.5  P $
Upwind	1
Hybrid	$[0, 1 - 0.5  P ]$
Power law	$[0, (1 - 0.1  P )^5]$
Exponential	$ P  / [\exp( P ) - 1]$

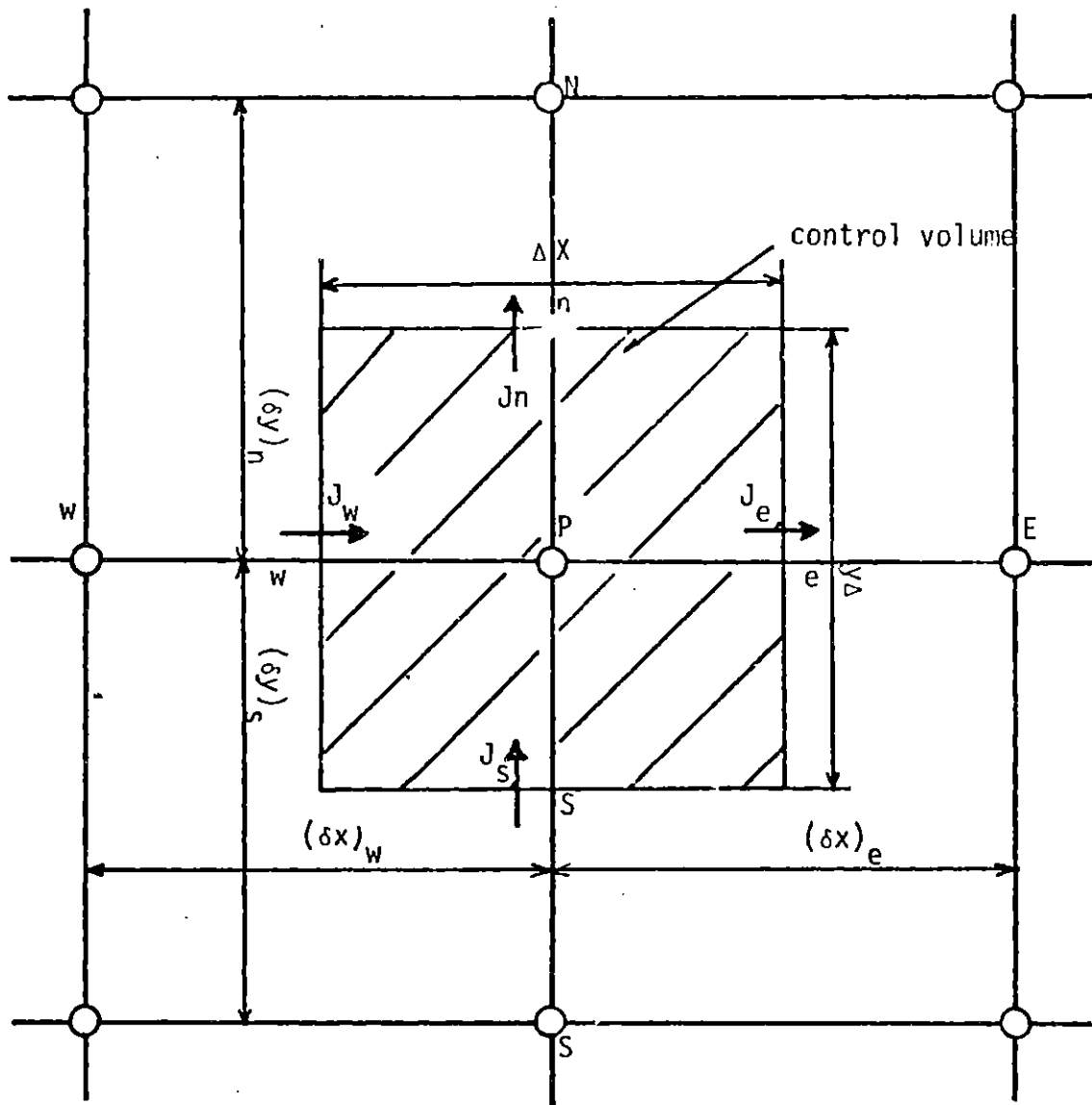


Fig. 4.2 Portion of the finite-difference grid

#### 4.1.2 Finite Difference Representation of the Transient Two-Dimensional Elliptic Equation

$$\frac{\partial}{\partial t}(\rho\phi) + \frac{\partial}{\partial x}(\rho u\phi) + \frac{\partial}{\partial y}(\rho v\phi) - \frac{\partial}{\partial x}\left(\Gamma_x \frac{\partial\phi}{\partial x}\right) - \frac{\partial}{\partial y}\left(\Gamma_y \frac{\partial\phi}{\partial y}\right) = S\phi \quad (4.1.22)$$

Generally we can deduce the finite-difference form for the transient two-dimensional elliptic partial differential equation by using a weighting factor  $\lambda$ . Equation (4.1.18) can be replaced by the finite-difference expression

$$\frac{\partial(\rho\phi)}{\partial t} + a_p\phi_p = \sum_{i=1, S, W, E} a_i\phi_i + b \quad (4.1.23)$$

where the subscript  $p$  denote the central point and the subscript  $i$  denotes its neighbors. In order to deduce the finite-difference expression for the transient partial differential equation,  $\partial(\rho\phi)/\partial t$  is replaced by  $\rho(\phi_p^{k+1} - \phi_p^k)/\Delta t$  and  $\phi_p$  and  $\phi_n$  are expressed as weighted mean concentrations as follows;

$$\begin{aligned} \rho(\phi_p^{k+1} - \phi_p^k) \Delta x \Delta y / \Delta t + \{ (1-\lambda)a_p^k \phi_p^k + \lambda a_p^{k+1} \phi_p^{k+1} \} \\ = \{ (1-\lambda) \sum a_i^k \phi_i^k + \lambda \sum a_i^{k+1} \phi_i^{k+1} \} \\ + \{ (1-\lambda)b^k + \lambda b^{k+1} \} \end{aligned} \quad (4.1.24)$$

where the superscript  $k$  or  $k+1$  denotes the number of the time step. In the present computation  $A_n$ ,  $A_s$ ,  $A_w$ , and  $A_e$  are independent of the time step, and the super script  $k$  or  $k+1$  can be dropped, while the terms  $A_p$  and  $b$  have different values for each time step. Then

$$a_p^k = a_e + a_w + a_n + a_s - S_p^k \Delta x \Delta y \quad (4.1.25)$$

$$b^k = S_c^k \Delta x \Delta y$$

Rearranging the equation (4.1.24), we obtain the final form for the finite-difference computation.

$$\begin{aligned} \left\{ \frac{\rho \Delta x \Delta y}{\Delta t} + \lambda a_p^{k+1} \right\} \phi_p^{k+1} \\ = \lambda \sum a_i \phi_i^{k+1} + \lambda b^{k+1} \\ + \left[ \frac{\rho \Delta x \Delta y}{\Delta t} \phi_p^k + (1-\lambda)a_p^k \phi_p^k + (1-\lambda) \sum a_i \phi_i^k + (1-\lambda)b^k \right] \end{aligned} \quad (4.1.25)$$

If  $\lambda = 1$ , equ. (4.1.25) becomes the implicit scheme. If  $\lambda = \frac{1}{2}$ , we obtain the Crank-Nicolson formula. On the other hand, if  $\lambda = 0$ , the explicit formula is obtained. In present calculations, the fully implicit scheme is employed

$$\left\{ \frac{\rho \Delta x \Delta y}{\Delta t} + a_p^{k+1} \right\} \phi_p^{k+1} = \sum_i a_i \phi_i^{k+1} + b^{k+1} + \frac{\rho \Delta x \Delta y}{\Delta t} \phi_p^k \quad (4.1.26)$$

and the final discretization equation can be written as

$$a_p \phi_p^{k+1} = a_e \phi_e^{k+1} + a_w \phi_w^{k+1} + a_n \phi_n^{k+1} + a_s \phi_s^{k+1} + b \quad (4.1.27)$$

where  $A_E$ ,  $A_W$ ,  $A_N$ , and  $A_S$  have the same form as obtained in equ. (4.1.17)

and

$$a_p^0 = \frac{\rho \Delta x \Delta y}{\Delta t}$$

$$b = S_c \Delta x \Delta y + a_p^0 \phi_p^k$$

(4.1.28)

$$a_p = a_e + a_w + a_n + a_s + a_p^0 - S_p \Delta x \Delta y$$



## 4.2 Solution Procedure

### 4.2.1 Tridiagonal Matrix Algorithm

The solution of the discretization equation formulated in the preceding chapter is obtained by the standard Gaussian-elimination method. Because of its simplicity, this algorithm is very useful.

The general form of the equations to be solved can be expressed as

$$a_i \phi_i = b_i \phi_{i+1} + c_i \phi_{i-1} + d_i \quad (4.2.1)$$

where  $i$  is the number of the grid point and points 1 and  $n$  denote the boundary point. In any boundary condition,  $T_n$  or  $(\frac{\partial T}{\partial x})_n$  is given, therefore  $c_1 = 0$  and  $b_n = 0$  could be set. This enables us to begin a "back-substitution" process in which  $\phi_{n-1}$  is determined by  $\phi_n$ , and  $\phi_{n-2}$  from  $\phi_{n-1}$ . The following form is obtained by elimination;

$$\phi_i = p_i \phi_{i+1} + q_i \quad (4.2.2)$$

and the coefficients  $p_i$  and  $q_i$  are given by

$$p_i = \frac{b_i}{a_i - c_i p_{i-1}} \quad (4.2.3)$$

$$q_i = \frac{d_i + c_i q_{i-1}}{a_i - c_i p_{i-1}}$$

The equation for  $i = 1$  is given as

$$p_1 = \frac{b_1}{a_1} \quad q_1 = \frac{d_1}{a_1} \quad (4.2.4)$$

For the time-dependent problem, more calculation is required, but this algorithm is also applicable. This procedure is performed in the program SOLVE. In effect, when solving nonlinear partial differential equations the coefficients cannot be determined explicitly, so that several iterations are required.

### 4.2.2 Pressure Correction Equation

The aim of the pressure correction equation is to modify the velocity components  $u$  and  $v$  so as to conserve the mass continuity in a control volume.

After the momentum equation is solved, the pressure correction equation, derived from the continuity equation, is applied

$$a_p p'_p = a_w p'_w + a_e p'_e + a_n p'_n + a_s p'_s + b \quad (4.2.5)$$

where

$$a_e = \rho_e d_e \Delta y$$

$$a_w = \rho_w d_w \Delta y$$

$$a_n = \rho_n d_n \Delta x$$

$$a_s = \rho_s d_s \Delta x$$

$$a_p = a_w + a_e + a_n + a_s$$

$$b = [(\rho u^*)_w - (\rho u^*)_e] \Delta y + [(\rho v^*)_s - (\rho v^*)_n] \Delta x$$

The correction to the velocity is made as follows:

$$u_e = u_e^* + d_e (p'_p - p'_e) \quad (4.2.6)$$

The correction formula in other directions can be derived similarly.

### 4.3 Flow Sheet and Computer Program for Computation

#### 4.3.1 Flow Field Calculation

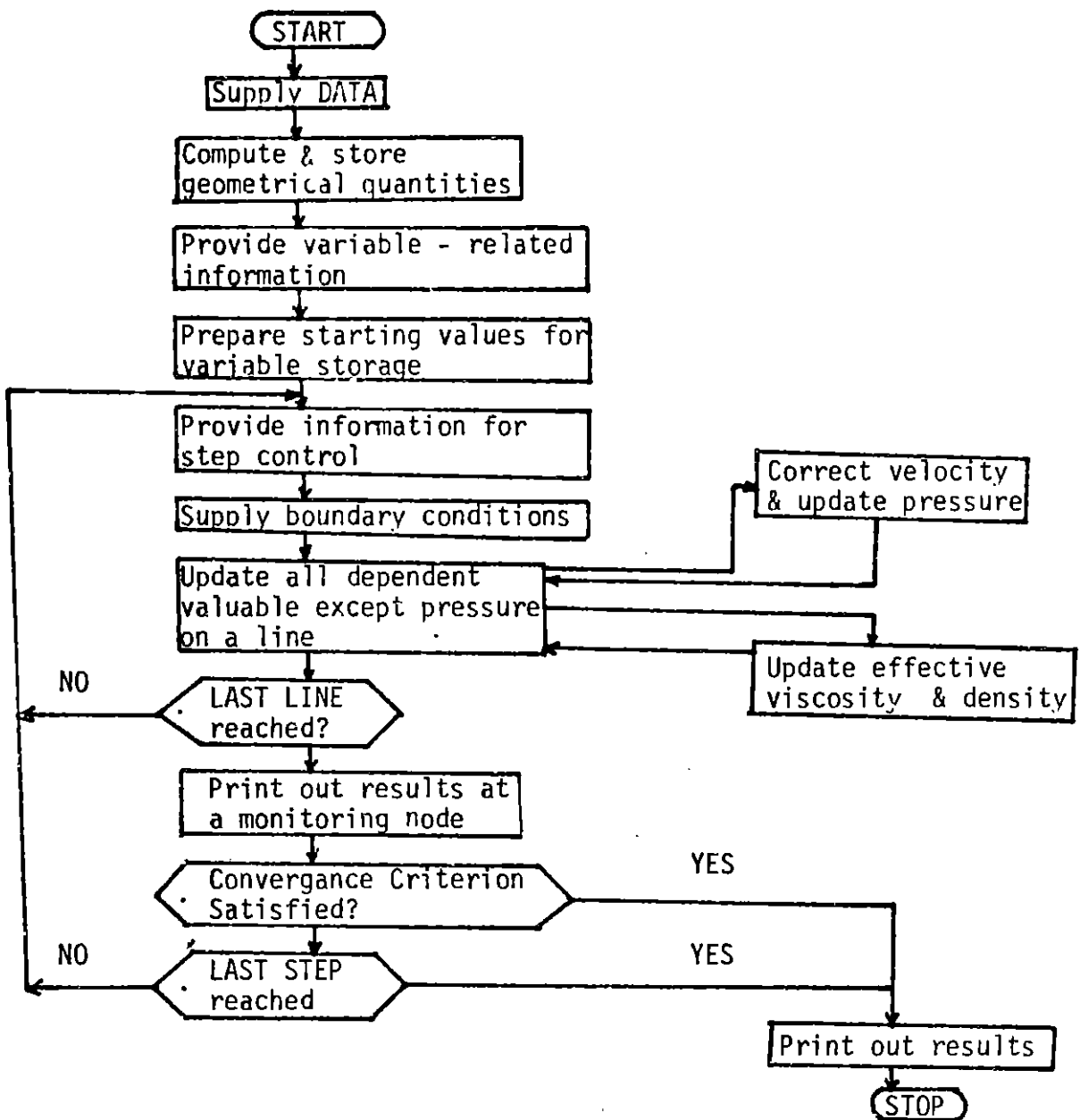
Fig. 4.3 shows a flow chart of the computation. In the present computation, the four dependent variables  $u$ ,  $v$ ,  $k$  and  $\epsilon$  are calculated, and updated in that order. The effective viscosity  $\mu_{\text{eff}}$  is an independent variable which is determined by  $k$  and  $\epsilon$ . Along one  $X$ -line, all of the four dependent variables are updated using the Gaussian-elimination algorithm. This is then repeated for the next  $X$ -line. In this way, a total of  $NX$  lines are updated. After each iteration is complete, the value of  $\mu_{\text{eff}}$  for each grid point is calculated, and  $u$  and  $v$  are corrected so as to observe mass continuity. The calculated value of effective viscosity is used for the next calculation. This procedure is continued until the residue and the difference of values between successive iterations are less than a specified value.

The program was initially developed by Pun and Spalding for turbulent pipe flow. The program can be divided into several subroutines the tasks of which are listed on Table 4.2. The listing of the program is given in Appendix A.

#### 4.3.2 Particle Coagulation Program

Fig. 4.4 shows a flow chart of the computation scheme. In the present work, particle sizes are divided into ten classes and transient partial differential equations are solved in each size group. A single iteration is performed for each dependent variable along successive  $X$ -lines. For the calculation of the source terms, the field values computed at the previous sweep are employed. After convergence is obtained at each time step, the calculation for the next time step is performed until the final time step is reached. The structure of this program is shown in Fig. 4.5. The structure

Fig. 4.3 Flow chart of the computational scheme



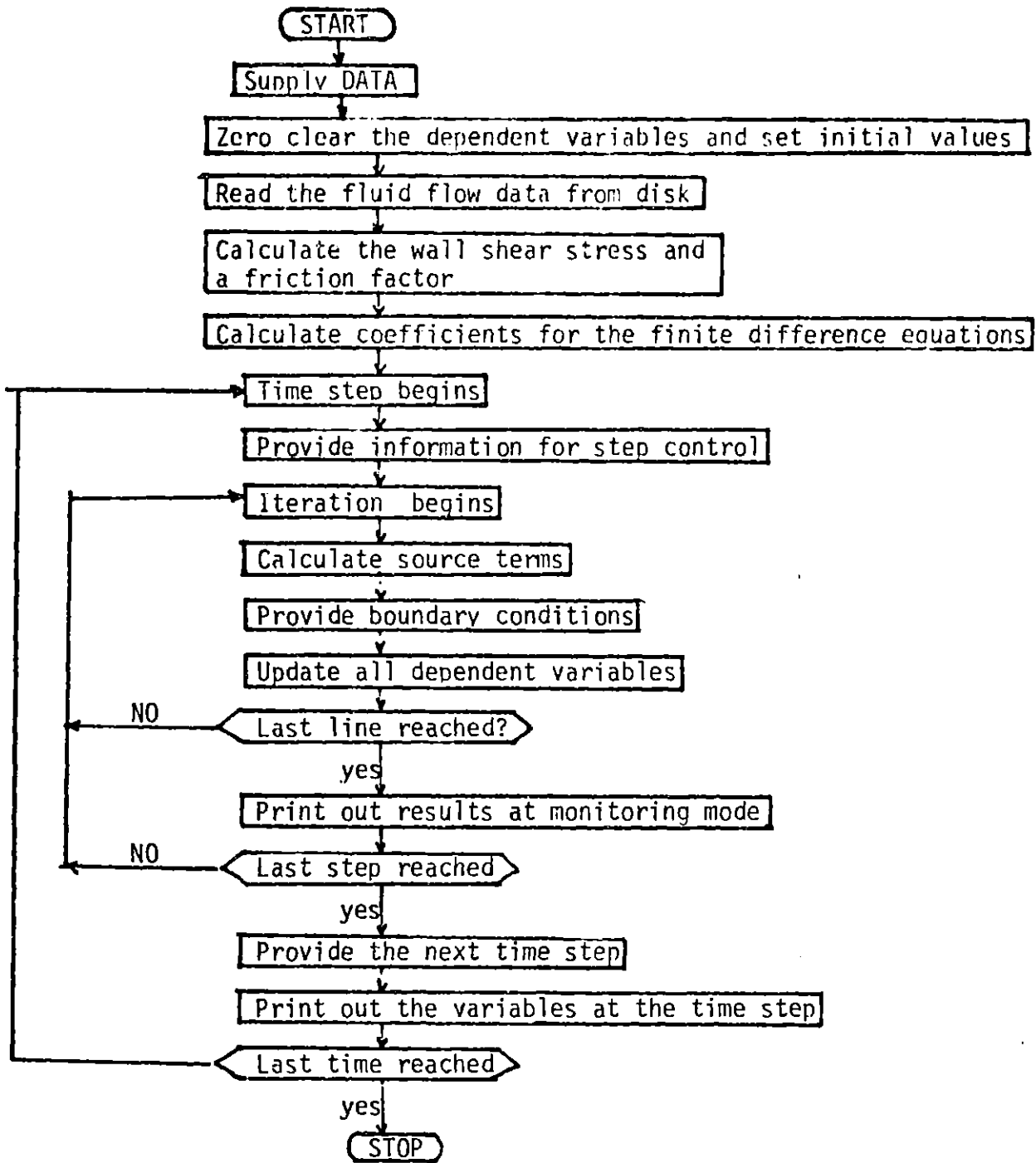


Fig. 4.4 Flow chart of the computational theme for particle coagulation

Table 4.2 Function of the Subroutines

<u>Name:</u>	<u>Function:</u>
MAIN	Starts the computations and controls the iteration procedure.
BLOCK DATA	Specifies numerical data and control indices for the problem.
OUTPUT	Organizes the bulk of the print-out results; divided into four parts by an entry statement.
OUTPH	Prints out headings like problem titles, size of the system, etc.
OUTPF	Prints out the field values of dependent variables.
OUTP1	Prints residual-source information and variable values at a monitoring mode.
OUTP2	Provides output of pipe flow characteristics
CONST	
CONST 2	Calculates quantities related to NX and NY.
CONST 3	Calculates all constants related to the variables.
CONST 5	Provides constants for starting preparations.
ADJUST	Performs various adjustments to the different variables in order to enhance the rate of convergence.
AVACON	Adjusts the mean pressure. This is not used in the present case.
CELCON	Applies the cell-wise continuity correction, through the use of pressure-correction values.
BOUND	Updates values on boundaries of the flow domain.
SOURCE	Supplies source terms $S_u$ and $S_p$ not provided in subroutine COEFF.
MODIFY	Makes all modifications to boundary conditions.
GEOM	Evaluates all geometrical quantities related to the grid.
COEFF	Calculates all coefficients of the finite-difference equations.
CELPHI	Provides cell-wall densities and viscosities for u-, v- and other cells.
SOLVE	Solves the finite-difference equations by means of the tri-diagonal matrix algorithm.

Table 4.2 Function of the Subroutines (cont'd)

<u>Name:</u>	<u>Function:</u>
PRINT	Prints variable-values in the two-dimensional field.
TEST	Prints information for program testing; consists of seven sections: TEST 11, TEST 12, TEST 13, TEST 21, TEST 22, TEST 23 and TEST 31.

itself is very similar to the fluid flow program except for the transient feature. The listing of program is given in Appendix B.



#### 4.4 Stability and Convergence

Two problems crucial to the successful solution of the coupled finite difference non linear equations are the stability and the rate of convergence. Instabilities are caused not only by the presence of round-off or other computation error, but also by large time steps. Stability analysis has been performed on several simple finite difference schemes. In general, however, it is not possible to extend this analysis to non linear coupled equations. As Patankar said in his book [47], there is no general guarantee that, for all non linearities and inter-linkages, we will obtain a convergent solution.

In order to avoid divergence in the iterative scheme, an underrelaxation technique is often employed. If  $\phi_{old}$  is the value of the variable calculated in the last iteration and  $\phi_{new}$  is the new value the use of a relaxation factor,  $\alpha$ , defined by

$$\phi = \alpha \phi_{new} + (1-\alpha) \phi_{old} \quad (4.4.1)$$

causes the dependent variables to respond more slowly to the change in other variables. A diffusion coefficient  $\Gamma$  can also be under-relaxed to reduce the influence of other variables. The present value of  $\Gamma$  is calculated from

$$\Gamma = \alpha \Gamma_{new} + (1-\alpha) \Gamma_{old} \quad (4.4.2)$$

The relaxation factor is required to be positive and less than 1. Other variables, for example the source term or the boundary value, may also be underrelaxed. The values of  $\alpha$  for each case need not to be the same. Therefore, it is very difficult to determine the optimum combination of the relaxation parameters for each variable and coefficient.

Convergence is checked by two different criteria. One of these is the residual  $RS_p$  which is calculated as follows;

$$RS_p = \phi_p (\sum_i a_i S_p) - (\sum_i a_i \phi_i + S_u) \quad (4.4.3)$$

where  $i = W, E, N, S$ . Just as before, the values of a variable on a line are updated and the algebraic sum of the residual sources on the line for the variable is calculated with the finite-difference coefficient available. The sum of the absolute value of the algebraic-source term on each line over the whole domain is required to be less than a prescribed small value, i.e.

$$\sum_i \left| \sum_j (RS_{i,j}) \right| < \epsilon_1 \quad (4.4.4)$$

where  $i$  and  $j$  express the lines over the whole domain and the nodes on a line respectively.

Another criterion is used in the present calculation. This alternative criterion has been used by some investigators [53].

$$\frac{\sum \left| \phi_{new} - \phi_{old} \right|}{\sum \left| \phi_{new} \right|} \leq \epsilon_2 \quad (4.4.5)$$

where  $\Sigma$  means summation over all the interior nodes. In the present numerical calculation for fluid flow, eqs. (4.4.4) and (4.4.5) are used.  $\epsilon_1$  was set to 0.001 and  $\epsilon_2$  to 0.005. In the calculation for particles coagulation, equ. (4.4.3) was used and  $\epsilon_2$  was set to 0.03.

## Chapter 5 Computed Results and Discussion

The model developed in Chapter 3 was used to predict the fluid flow and particle coagulation process in the R-H vacuum degasser. The calculated results of the flow field in the ladle were used for the prediction of coagulation rate.

### 5.1 Fluid Flow Calculation

#### 5.1.1 System, Physical Properties and Parameters

The system chosen for computation was the ladle of a 150 ton R-H degassing system. The ladle diameter,  $X_s$ , was 2.5m and its height,  $Y_s$ , was 2.5m. The values of the physical properties used for the computation are listed in Table 5.1. The values used in this computation are common in the literature. The values for the empirical constants  $C_1$ ,  $C_2$ ,  $C_D$ ,  $\sigma_k$  and  $\sigma_\epsilon$  of the k- $\epsilon$  model are those recommended by Launder and Spalding. This set of numerical values is adequate for many applications and a more extensive discussion is provided by the same authors.

#### 5.1.2 Computational Details

A 15 (X-direction) X 18 (Y-direction) finite difference grid as shown in Table 5.2. The nodes are spaced so as to be concentrated in the regions a wall or free surface. The relaxation factors and the direction of sweeps are shown in Table 5.3. The computation was carried out using the IBM370/168 digital computer at M.I.T. The compilation of the program required 25 sec. and a typical run required 180 sec.

#### 5.1.3 Computed Results and Discussion

Fig. 5.1 represents the computed velocity field in the 150 ton ladle for an inlet velocity of 72cm/s. It is seen that there are two regions of local recirculation; one near the surface and one in the vicinity of the left side wall. According to the calculation of Nakanishi, et al. [1] who

Table 5.1 Numerical value of parameters (fluid flow)

$X_s$	Height of a ladle	250 (cm)
$Y_s$	Diameter of a ladle	250 (cm)
$R$	Diameter of up- or down leg	35 (cm)
$\rho$	Density of molten steel	7.2 (g/cm <sup>3</sup> )
$\mu$	Viscosity of molten steel	0.06 (g/cm sec.)
$C_1$	Constant in k- $\epsilon$ model	1.44 (-)
$C_2$	Constant in k- $\epsilon$ model	1.92 (-)
$C_D$	Dissipation constant	0.09 (-)
$\sigma_k$	Effective Prantdl number for k	0.9 (-)
$\sigma_\epsilon$	Effective Prantdl number for $\epsilon$	1.0 (-)

Table 5.2 Details of the finite-difference grid

x (i)		y (i)	
x (1)	0	y (1)	0
	5.0		6.25
	25.0		21.25
	45.0		26.25
	65.0		53.75
	85.0		71.25
	105.0		88.75
	125.0		103.25
	145.0		117.75
x (10)	165.0	y (10)	132.25
	185.0		146.75
	205.0		161.25
	225.0		178.75
	245.0		196.25
x (15)	250.0		213.75
			228.75
			243.75
		y (18)	250.0

Table 5.3 Details of computation

NO of iteration	u	v	k	$\epsilon$	$\rho'$	$\mu$	Direction of sweep
1-100	0.3	0.6	0.5	0.5	0.6	0.5	single
100-720	0.3	0.6	0.7	0.7	0.6	0.5	single

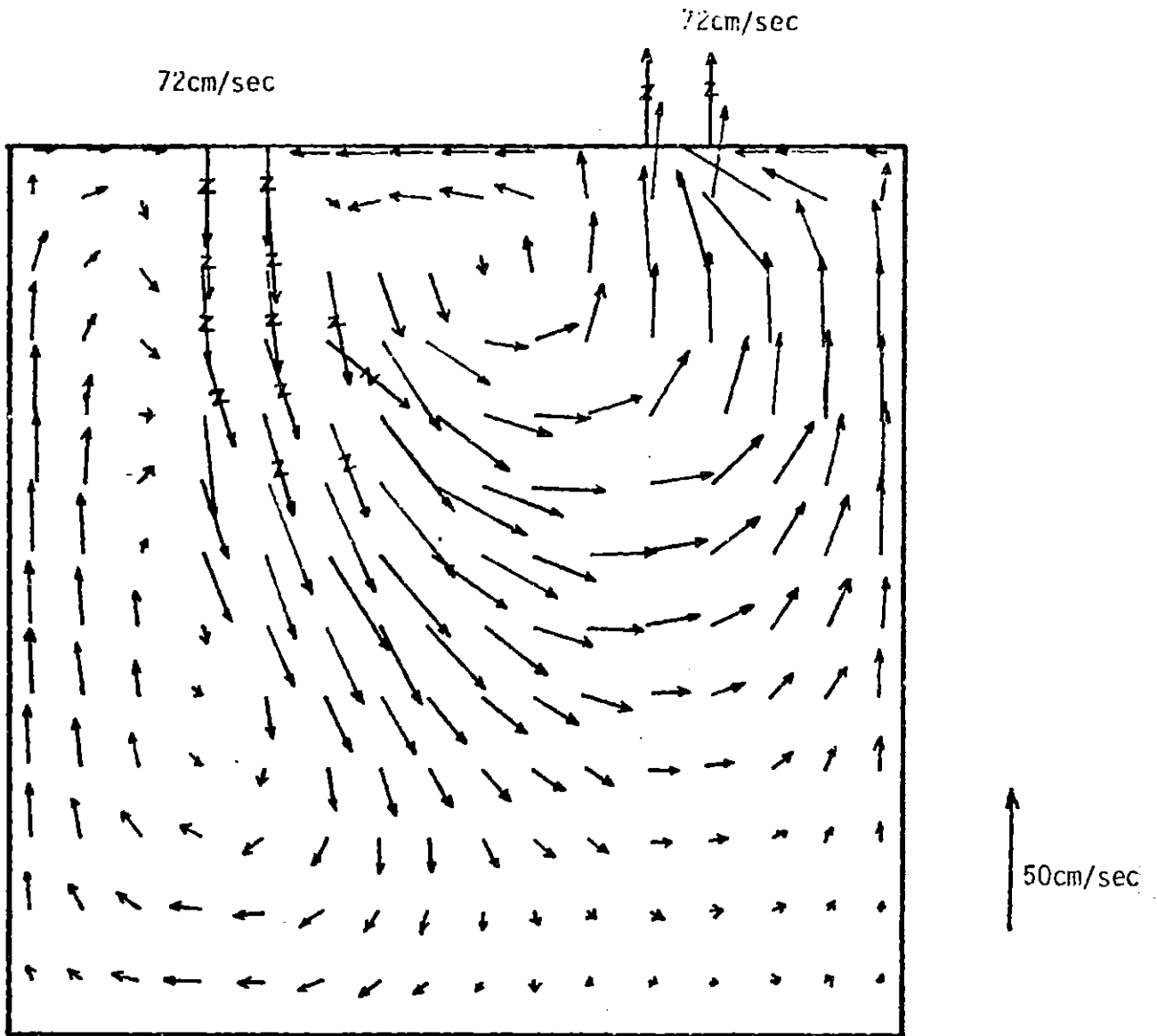


Fig. 5.1 Velocity field in the ladle of the R-H system (cm/sec).

used the vorticity-stream function program, there seem to be three local circulations. Since they assumed a free surface condition at the top of the ladle, there was no circulation between the two legs. Although a realistic boundary condition would be neither a solid surface condition nor a free surface condition (due to the existence of slag layer), it is apparent that there would be a local surface circulation when the solid surface condition weakened. The reason why the relatively large circulation occurs near the wall of down-leg side is not clear, but the high momentum of the flow in the down-leg seems to cause some "choking effect", which results in recirculation. At the bottom of the ladle, the metal velocities are much smaller (minimum 1.0 cm/s) but still non zero.

The computed spatial distribution of the turbulent kinetic energy,  $k$ , and the turbulent dissipation energy,  $\epsilon$ , are shown in Fig. 5.2 and Fig. 5.3, respectively. The two profiles are very similar, but the decrease in the dissipation energy towards the wall is much faster than that in the kinetic energy. The maximum value of both kinetic turbulent energy and the dissipation energy appear just under the down-leg. On the contrary, Nakanishi's calculation showed that the maximum value appears under the up-leg. This seems to come from a difference of the boundary conditions for the up-leg. In the present calculation, we used the same boundary conditions both for the discharge and the suction area but Nakanishi used the zero-gradient boundary condition which is valid only for the free-surface,

Fig. 5.4 shows the distribution of the eddy diffusivity. The eddy diffusivity also has the maximum value under the down-leg (72 cm/sec). Fig. 5.5 shows the distribution of the ratio of the effective viscosity to the molecular viscosity. The maximum value of this ratio is about 8000.



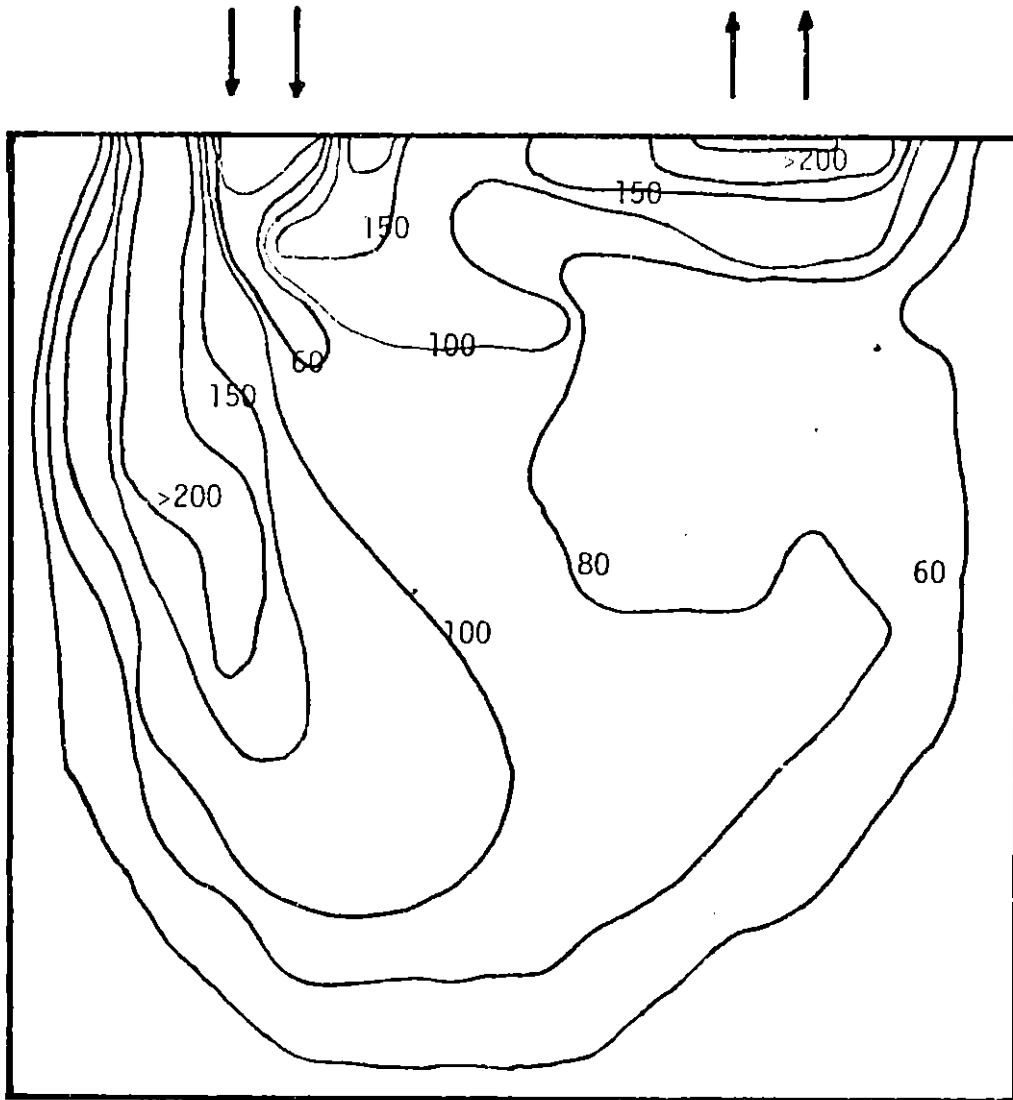


Fig. 5.2 Distribution of the kinetic energy  $k$  ( $\text{cm}^2/\text{sec}^2$ ).

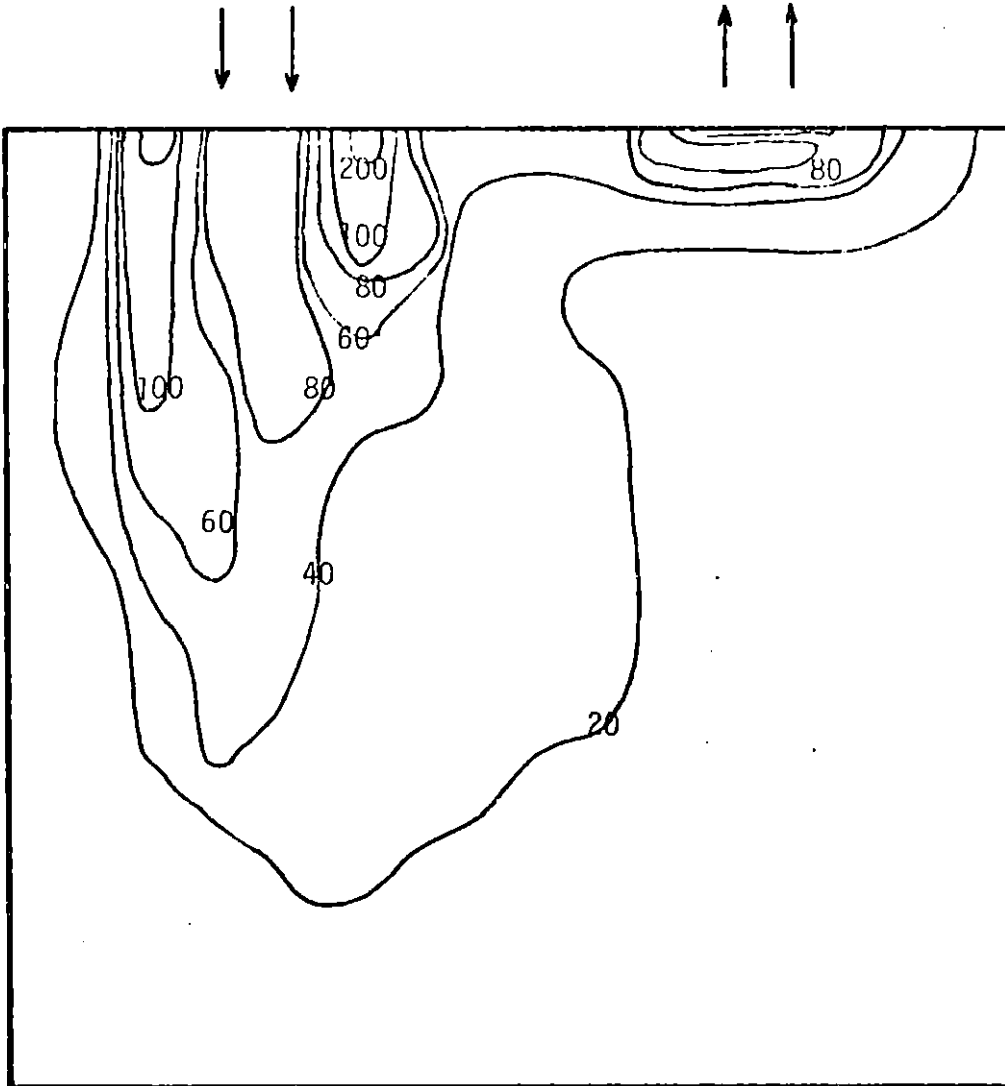


Fig. 5.3 Distribution of the turbulent dissipation energy  $\epsilon$  ( $\text{cm}^2/\text{sec}^3$ ).

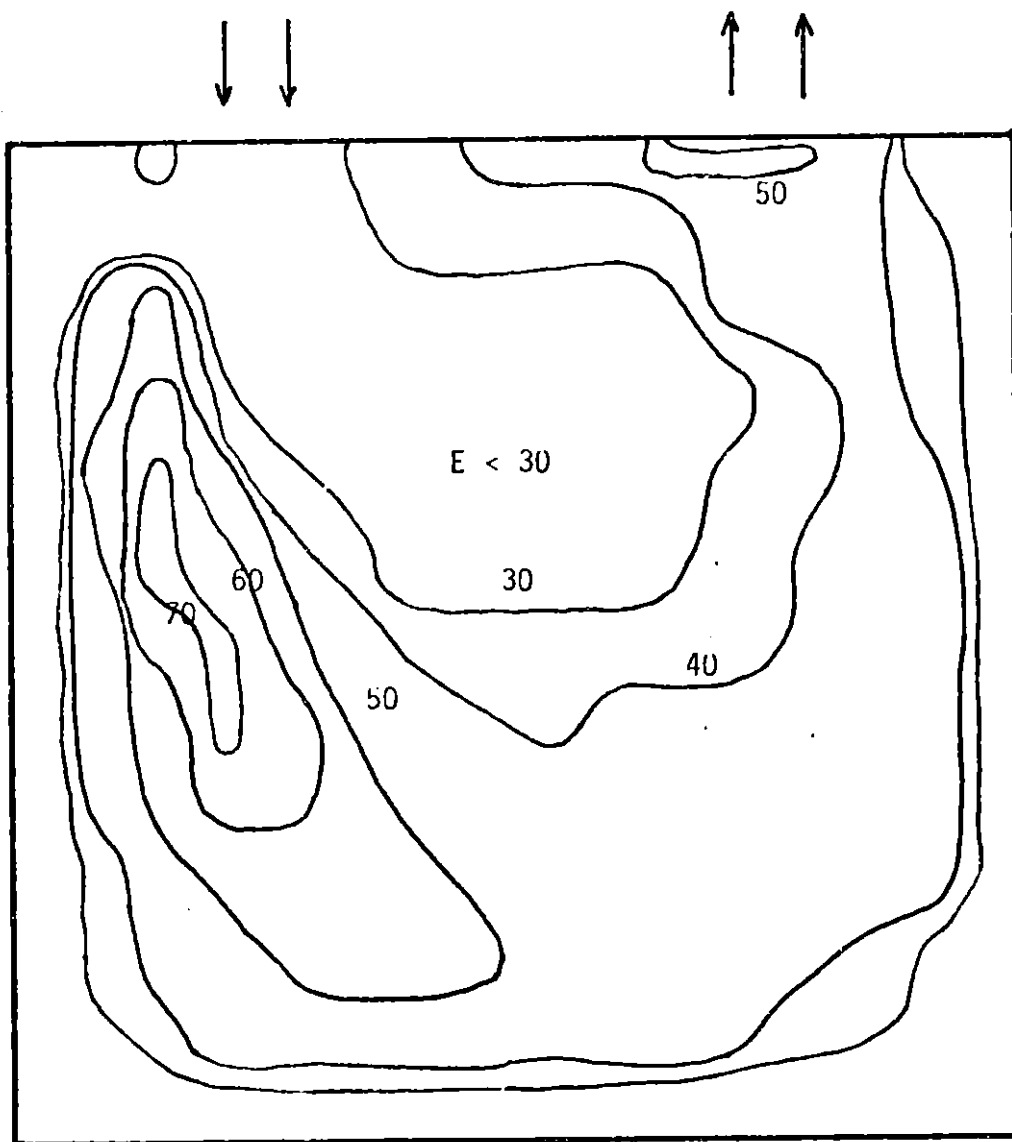


Fig. 5.4 Distribution of the eddy diffusivity  $E$  ( $\text{cm}^2/\text{sec}$ ).

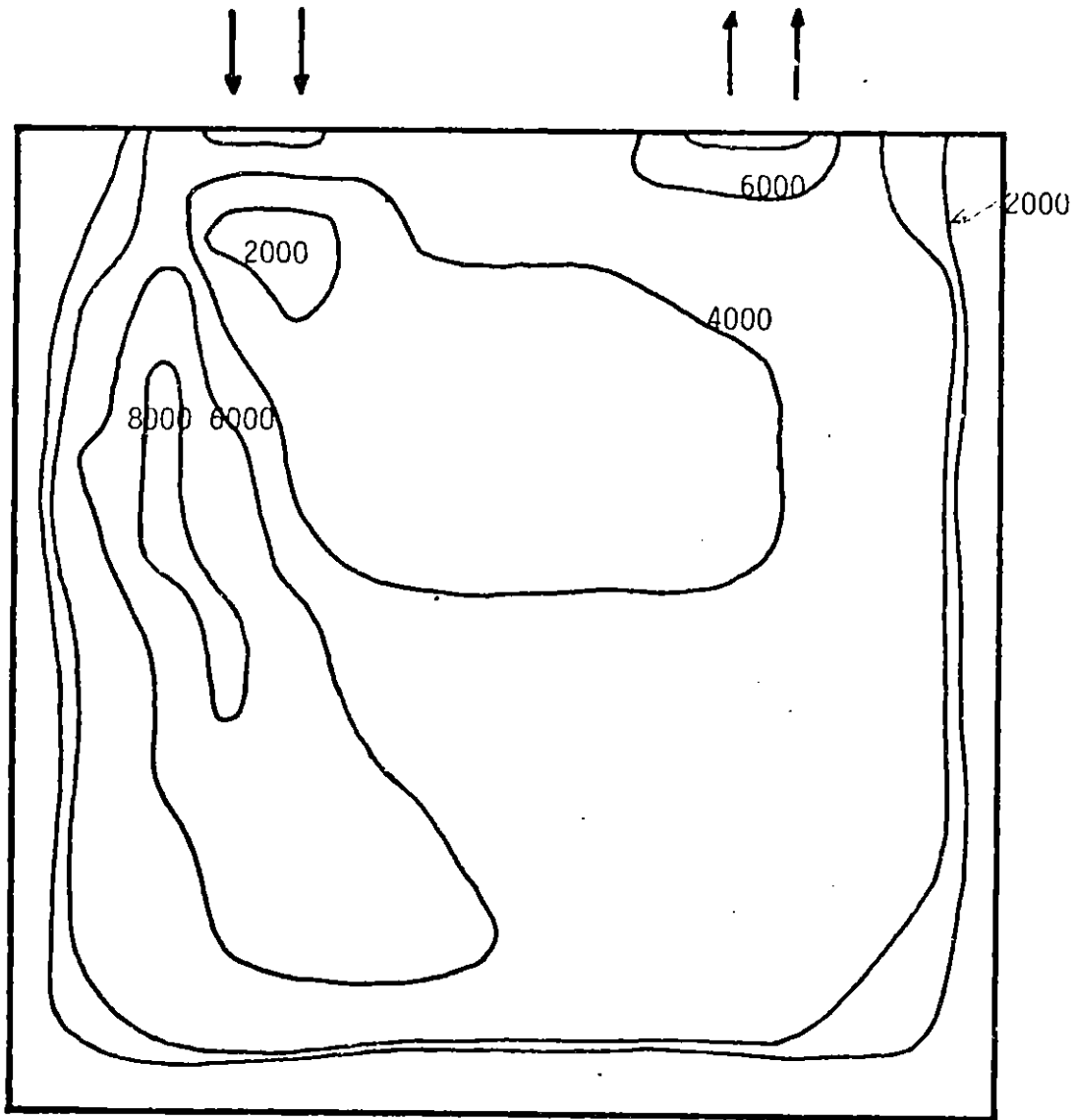


Fig. 5.5 Distribution of the ratio  $(\mu_{\text{eff}}/\mu)$

## 5.2 Particle Coalescence Calculation

### 5.2.1 Data used for the Calculation

In the present calculation, as mentioned in the previous chapter, the fluid flow data computed for the case of steady condition were used for the transient particle transport equation. All of the data computed in the F array, which is equivalent to nine dependent variables were stored on a disk after convergence was reached.

The initial particle size distribution was taken from the available published and unpublished data. The initial distribution of particle size may depend on the process and the pretreatment method, but the distribution is assumed so as to represent the real situation as well as possible.

### 5.2.2 Computational Details

The finite difference grid used for the particle coagulation model was the same as that used for the fluid flow calculation. The important information of the details of the computation is listed in Table 5.4. The compilation time and the execution time of the program were about 25 sec. and 860 sec., respectively. In the present calculation the wall function for the particle coagulation was not calculated.

### 5.2.3 Computational Results and Discussions

Fig. 5.7 - Fig 5.11 represent the computed particle density distribution at nodes 50, 81, 112, 128, 176, 224. These grid points are chosen so as to monitor the dependence on the dissipation energy, the velocities and the wall effect. The location of these grid points are shown in Fig. 5.6. Although the particle density distributions seem to be similar, some significant characteristics are found. At every grid point the larger particles increase in number at the initial stage (at 10 sec.), but soon begin to decrease, and at the time  $t = 60$  sec. the number of particles of size  $d = 20\mu\text{m}$  becomes almost the same as the initial value. Since it is assumed that all

Table 5.4 The detail of computation for particle coagulation

Time (sec.)	Time interval	Prantle Number $\tau_{c,i}$	relaxation parameter $\alpha_{i,c}$	The number of iteration	sweep
0	10	1.0	1.0	5	single
10					
20	10	1.0	1.0	5	"
40	20	1.0	1.0	5	"
60	20	1.0	1.0	5	"
90	30	1.0	1.0	5	"
120	30	1.0	1.0	5	"
180	60	1.0	1.0	5	"
240	60	1.0	1.0	5	"
300	60	1.0	1.0	5	"
400	100	1.0	1.0	5	"
500	100	1.0	1.0	5	"

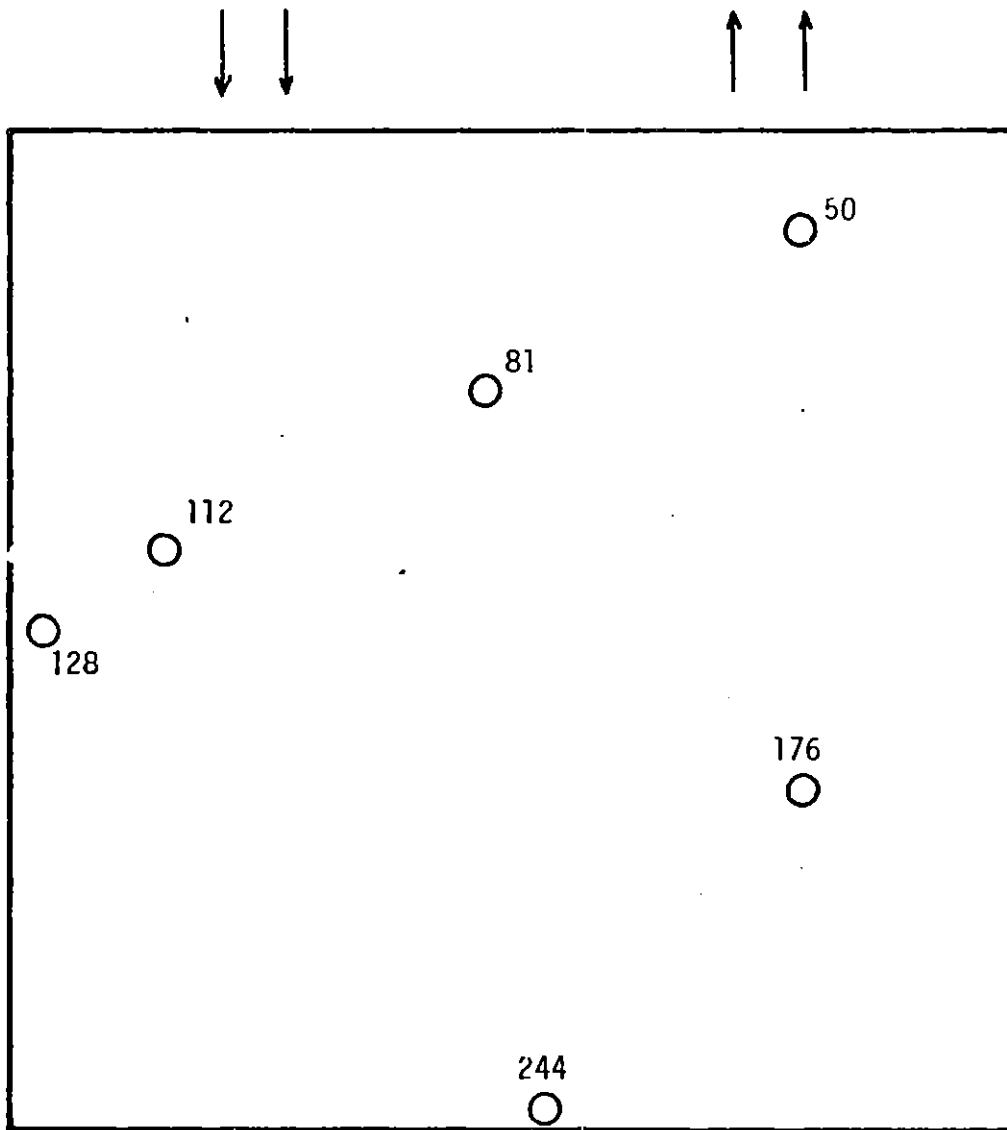


Fig. 5.6 The location of the grid points from which the plots were extracted

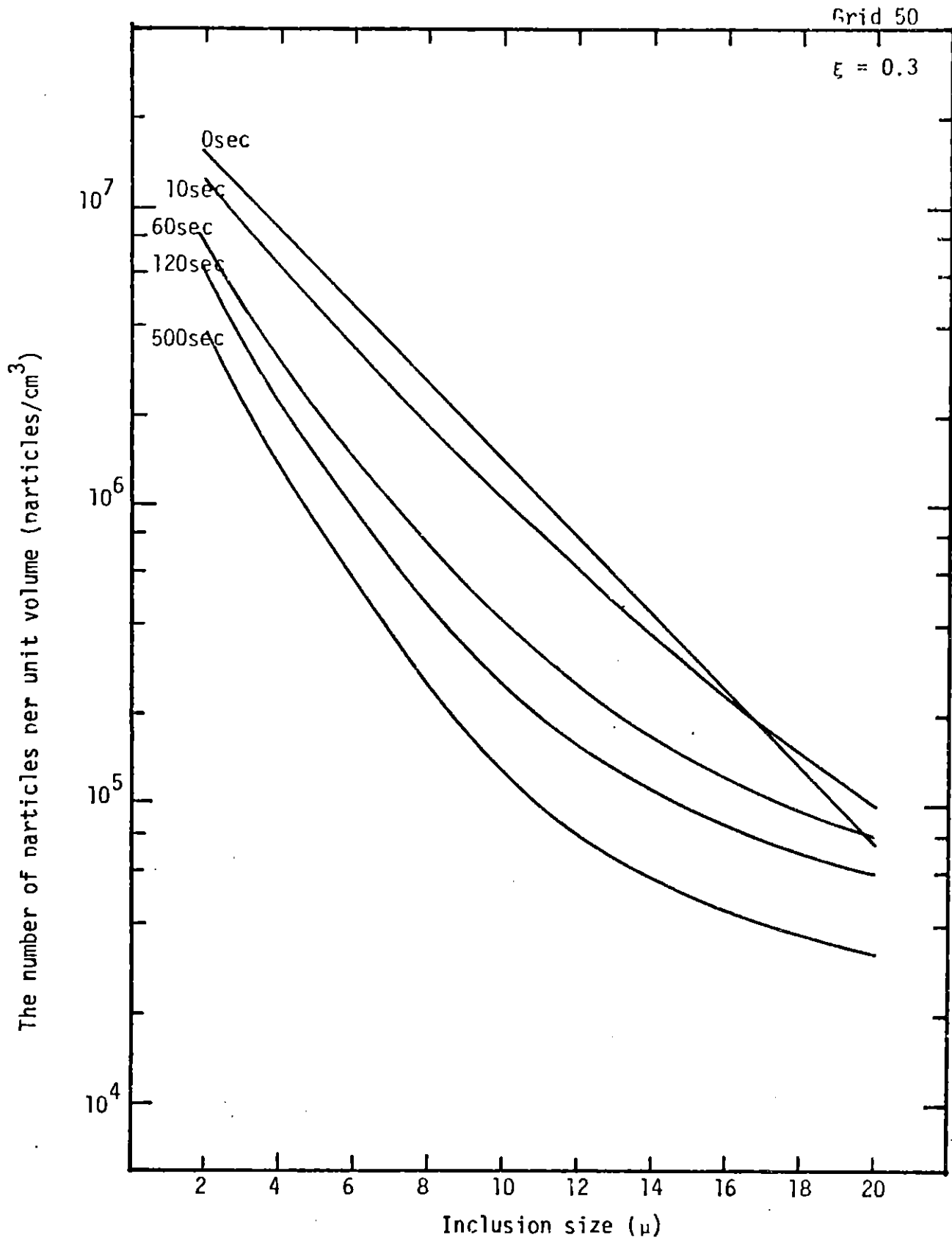


Fig. 5.7 Particle distribution (at grid 50)



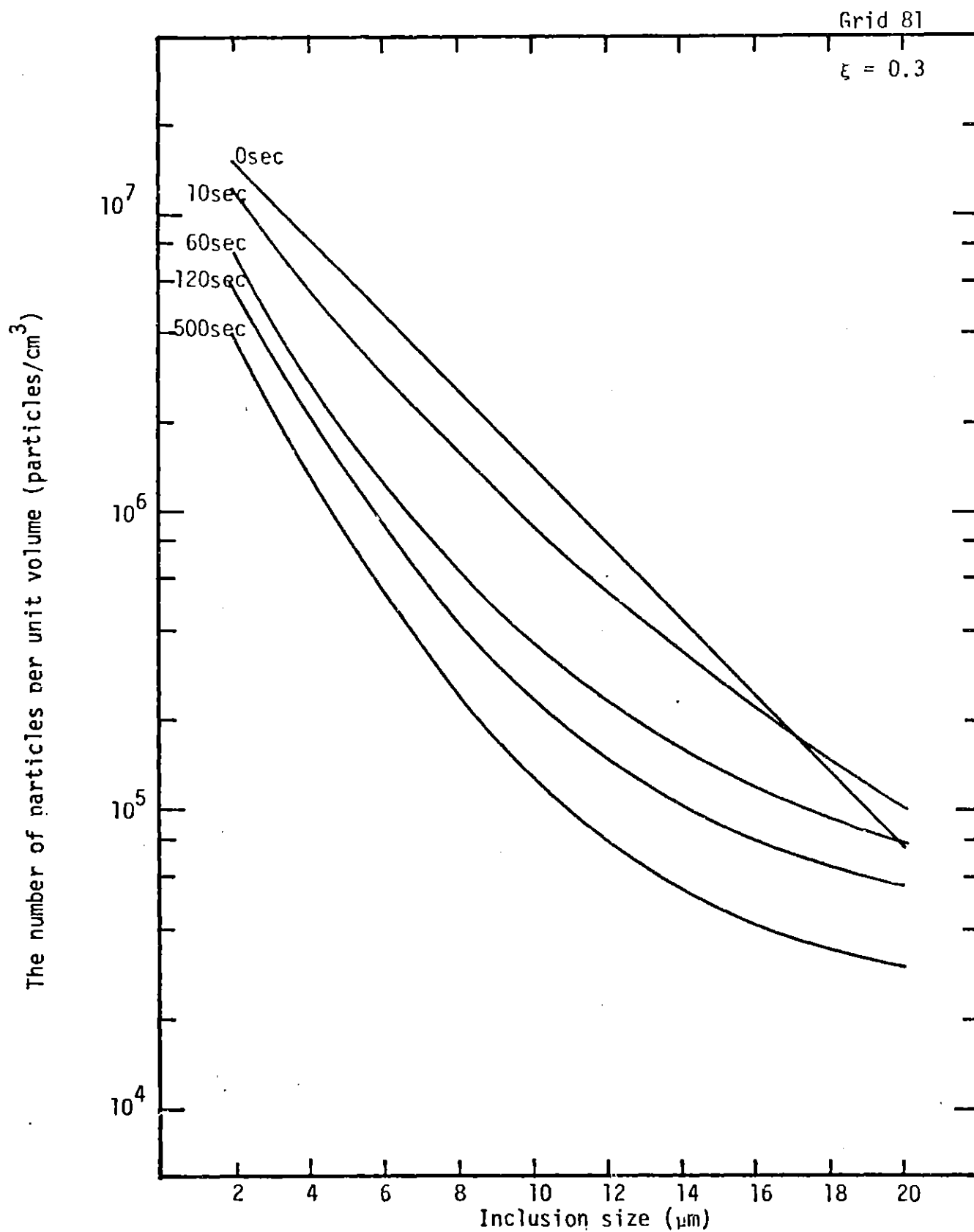


Fig. 5.8 Particle distribution (at grid 81)

Grid 112

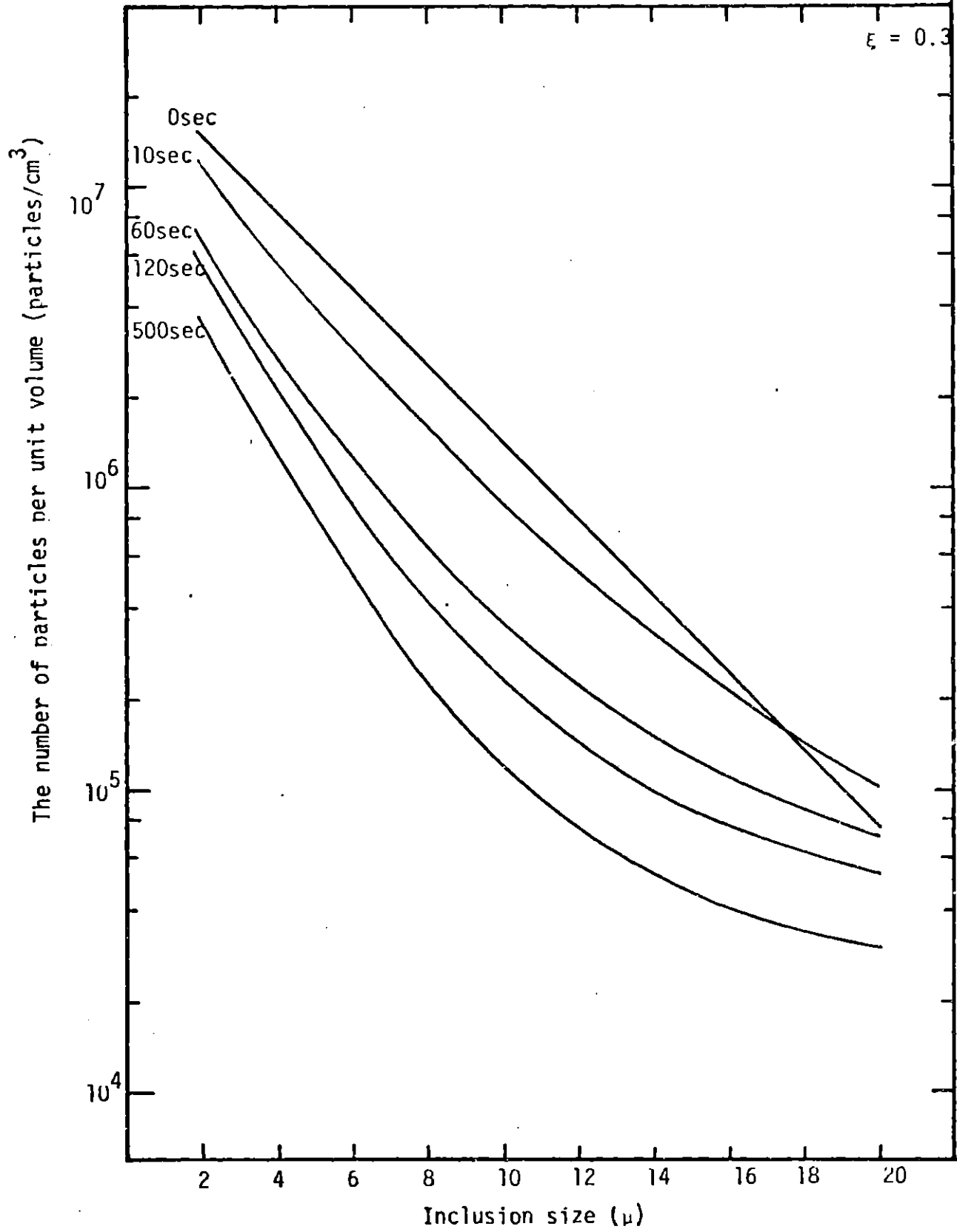
 $\epsilon = 0.3$ 

Fig. 5.9 Particle distribution (at grid 112)

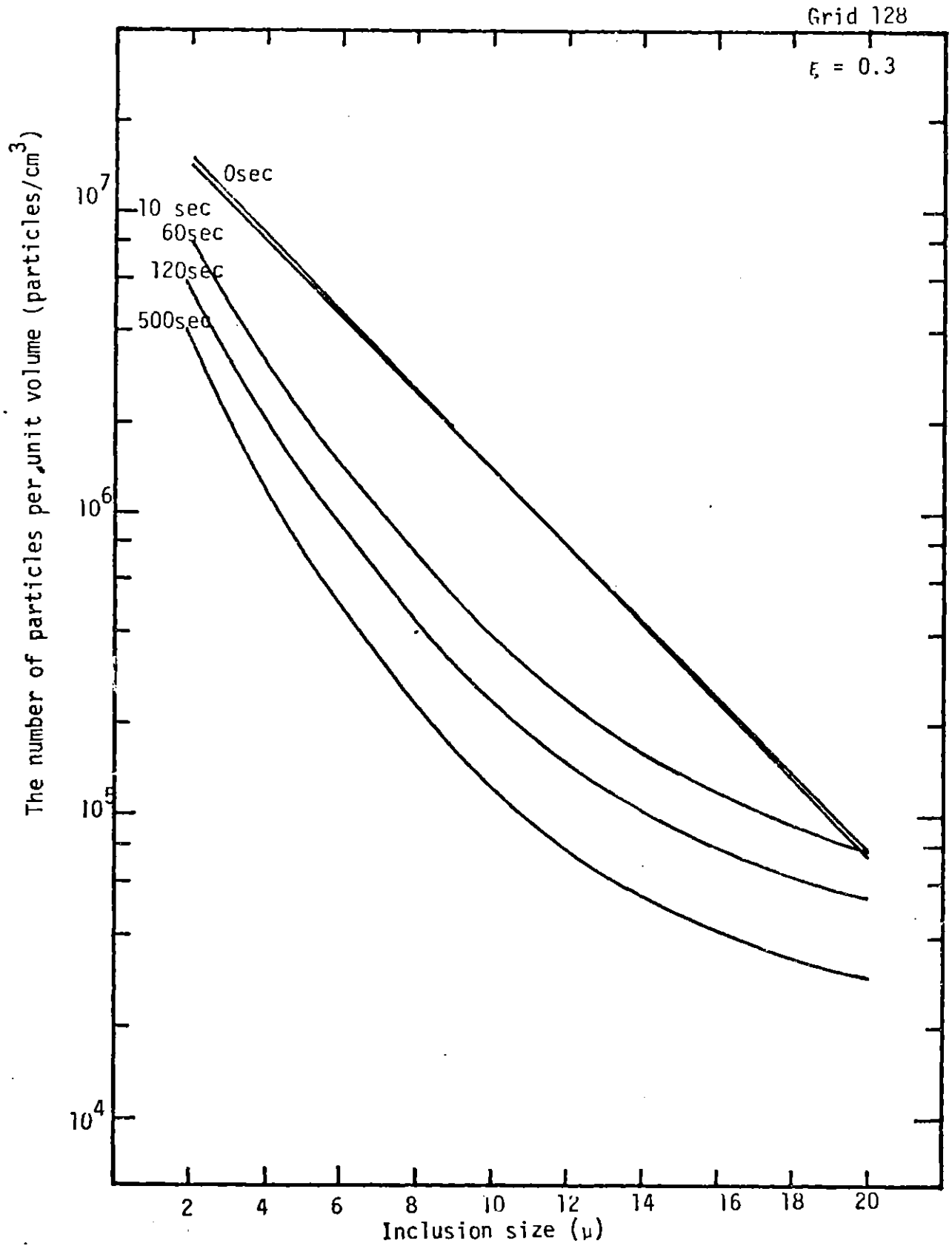


Fig. 10 Particle distribution (at grid 128)

Grid 176

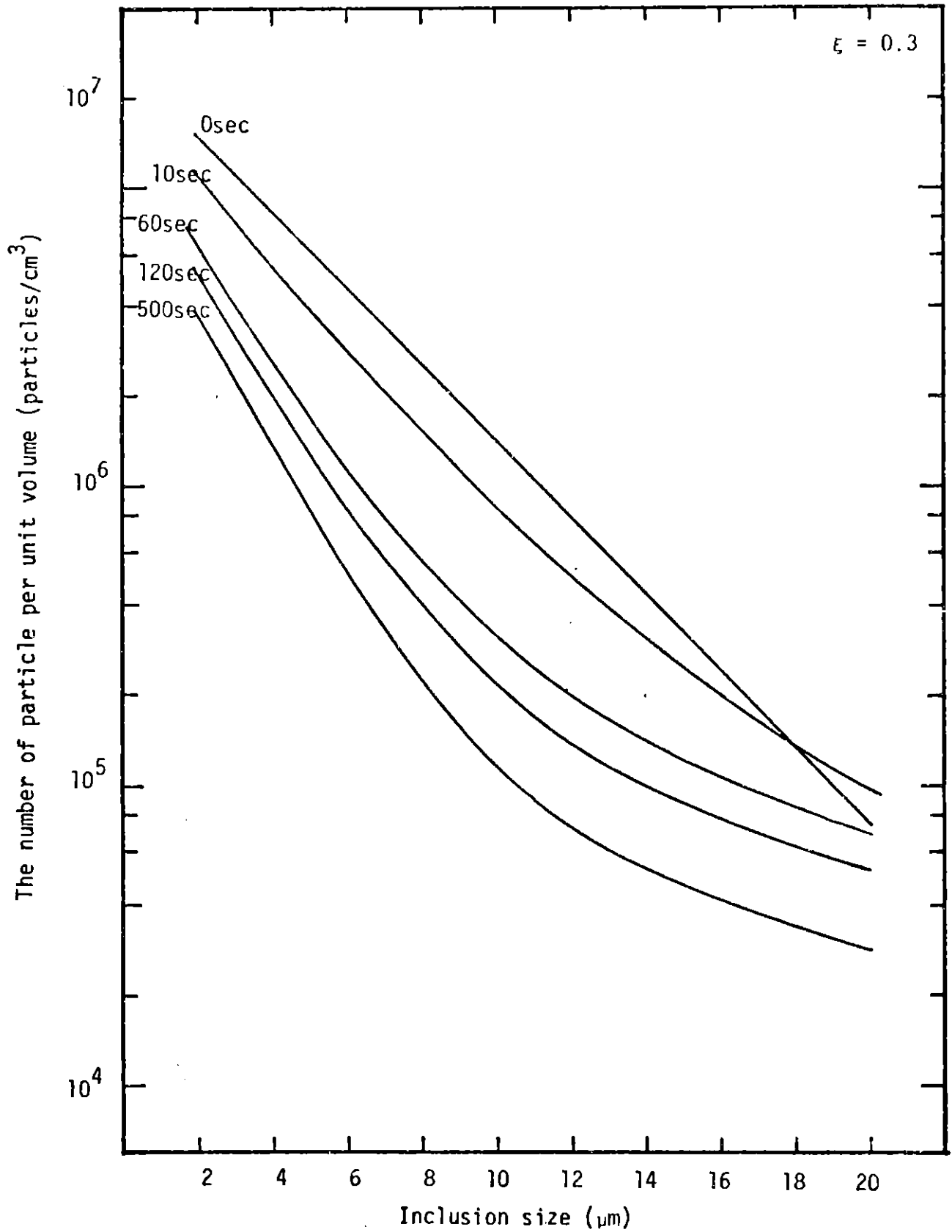


Fig. 5.11 Particle distribution (at grid 176)

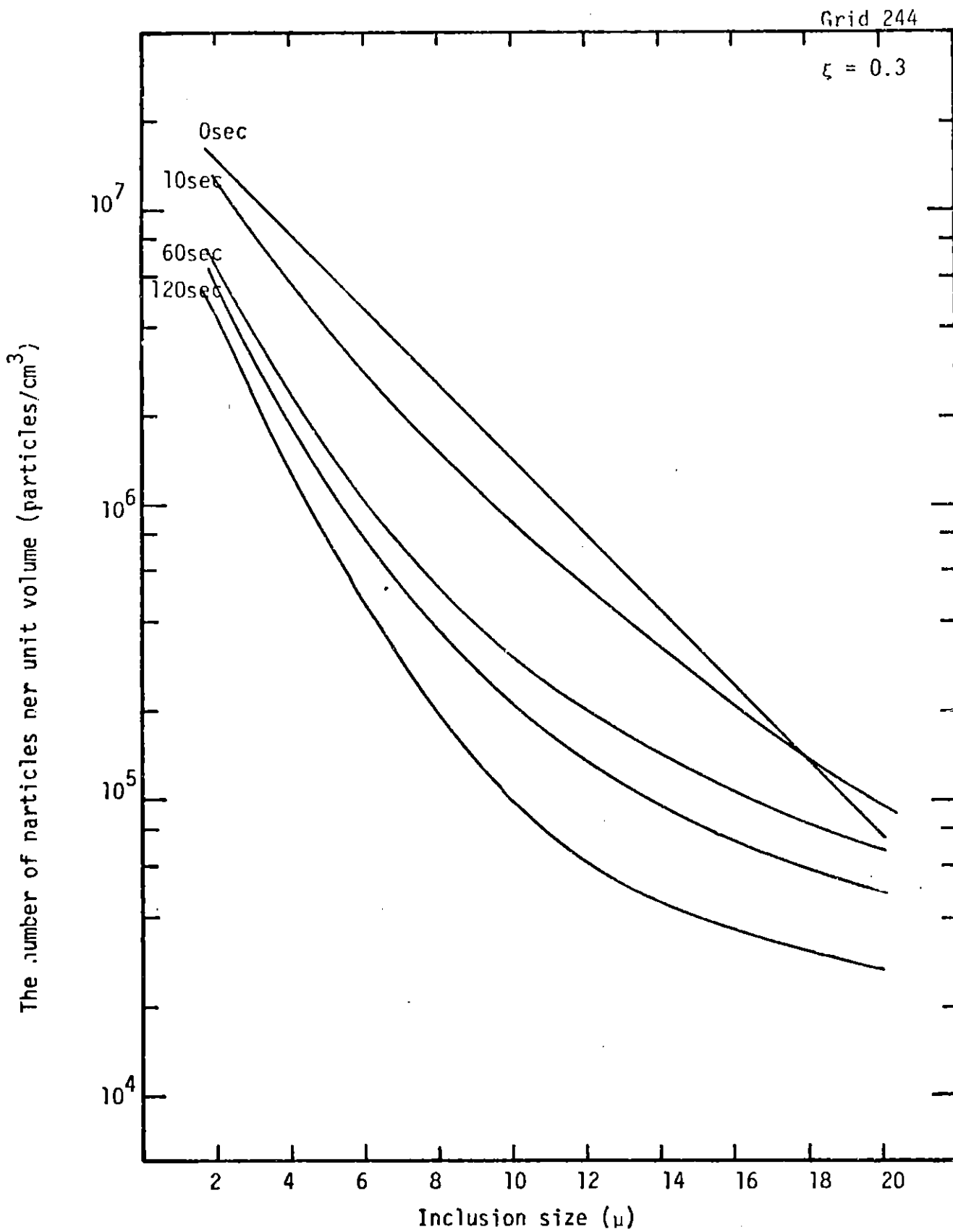


Fig. 5.12 Particles distribution (at grid 244)

the particles which have grown up to a size more than  $d_{crit}$  float up and are removed from the system, the coalescence behavior between larger particles is completely neglected. If a wider particle size range is taken, the increase in the number of larger particles would be more significant.

Another feature we can observe from these figures is that the rate of coagulation between intermediate size (i.e.  $6\mu\text{m} \sim 16\mu\text{m}$ ) particles is relatively high compared with that of smaller particles. This effect is also seen in the calculation of the mass scale (not in the number scale), but at  $t = 200$  sec. The volume fraction of inclusions per class decreases remarkably and this seems to be somewhat contradictory to the experimental results.

The calculated results of P.K. Iyenger and W.O. Philbrook [52] show that the particle distribution decreases in a parallel way in a naturally convected molten steel bath. This seems to come from the fact that they didn't consider the mass conservation but simply applied the Smolchowski's coagulation model. We also experienced the "parallel decrease in number scale" when the Smolchowski's coagulation theory was employed. In other words, their assumptions seem to lack the condition of  $\frac{dm}{dt} = 0$ .

Another calculation was also made by K. Nakanishi et al. [5]. Although they assumed the average turbulent dissipation energy, they obtained similar results to the present calculation. Their results also show that a high reduction rate of particle number appears in the medium size range.

The other feature which the computation results display is the local dependence of the particle reduction rate. At grid point 128 which is adjacent to the wall, the initial reduction rate of oxidized particles is very slow because the convective flow is intense there and the turbulent dissipation energy is very small. However, at time  $t = 60$  sec., the particle distribution seems not to be significantly different from that at other

grid points, because the strong convection makes the particle distribution uniform. At grid point 244 where either the flow velocity or the turbulent dissipation energy is small, the initial reduction rate of oxidized particle is not as small as at grid point 128.

Fig. 5.13 - Fig. 5.15 show the spatial distribution of particles of size 2, 10 and  $20\mu\text{m}$  respectively at time  $t = 120$  sec. The particle concentrations are relatively large near the down-leg and decreased towards the bottom of the ladle. As shown in previous section, the turbulent dissipation energy is very high just below the down-leg collide with each other rapidly and soon become larger. Another high particle concentration is seen at the bottom right hand side. In this region, either the turbulent dissipation energy of the fluid velocity is very low and therefore the coagulation rate is low.

Fig. 5.16 - Fig. 5.18 show the rate of reduction for a number of particles. For large particles ( $20\mu\text{m}$  radius), it increases about 20-30% at the very initial stage of deoxidation, but decreases again to around the initial value at time  $t = 60$  sec.

On the contrary, for small and medium sized ( $1\mu\text{m}$  and  $10\mu\text{m}$ ) particles the rate of reduction decreases at the beginning of deoxidation, and falls abruptly to a very low value. According to Lindborg et al. [19], three stages occur in the process of deoxidation. The first stage is the incubation period where there is a gradual growth of oxidized particles. The second stage is the period of rapid oxygen removal where the largest particles reach a certain size at which point they rapidly float out of the vessel. The final slow stage begins when the remaining large-sized particles are separated from the bath. In the present calculation, the first stage arises from the nature of the modeling. They assumed the 8 size

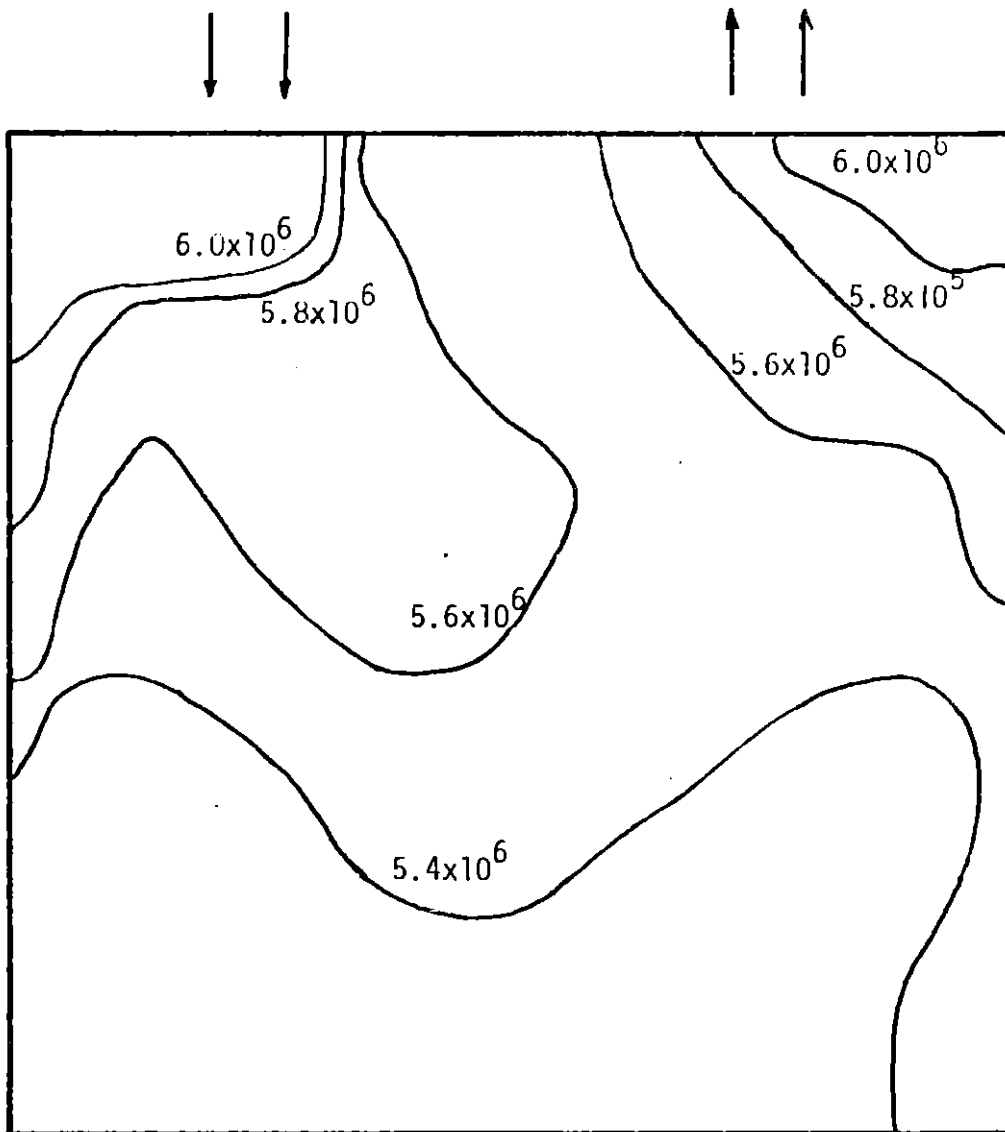


Fig. 5.13 Spatial distribution of the number of the oxidized particles at the time  $t = 120$  sec. ( $d_p = 1 \mu\text{m}$ ).



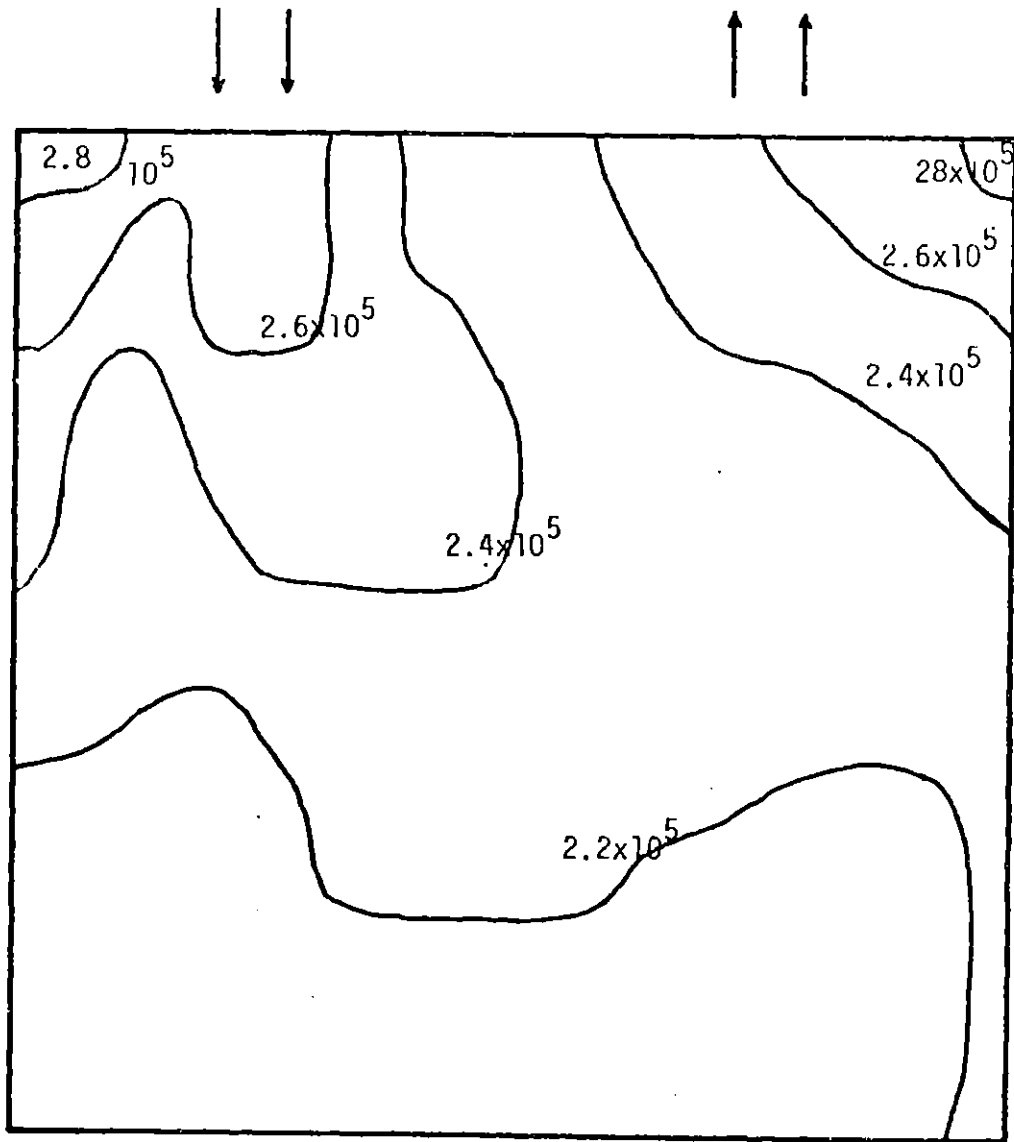


Fig. 5.14 Spatial distribution of the number of the oxidized particles at the time  $t = 120$  sec. ( $d_p = 10 \mu\text{m}$ )

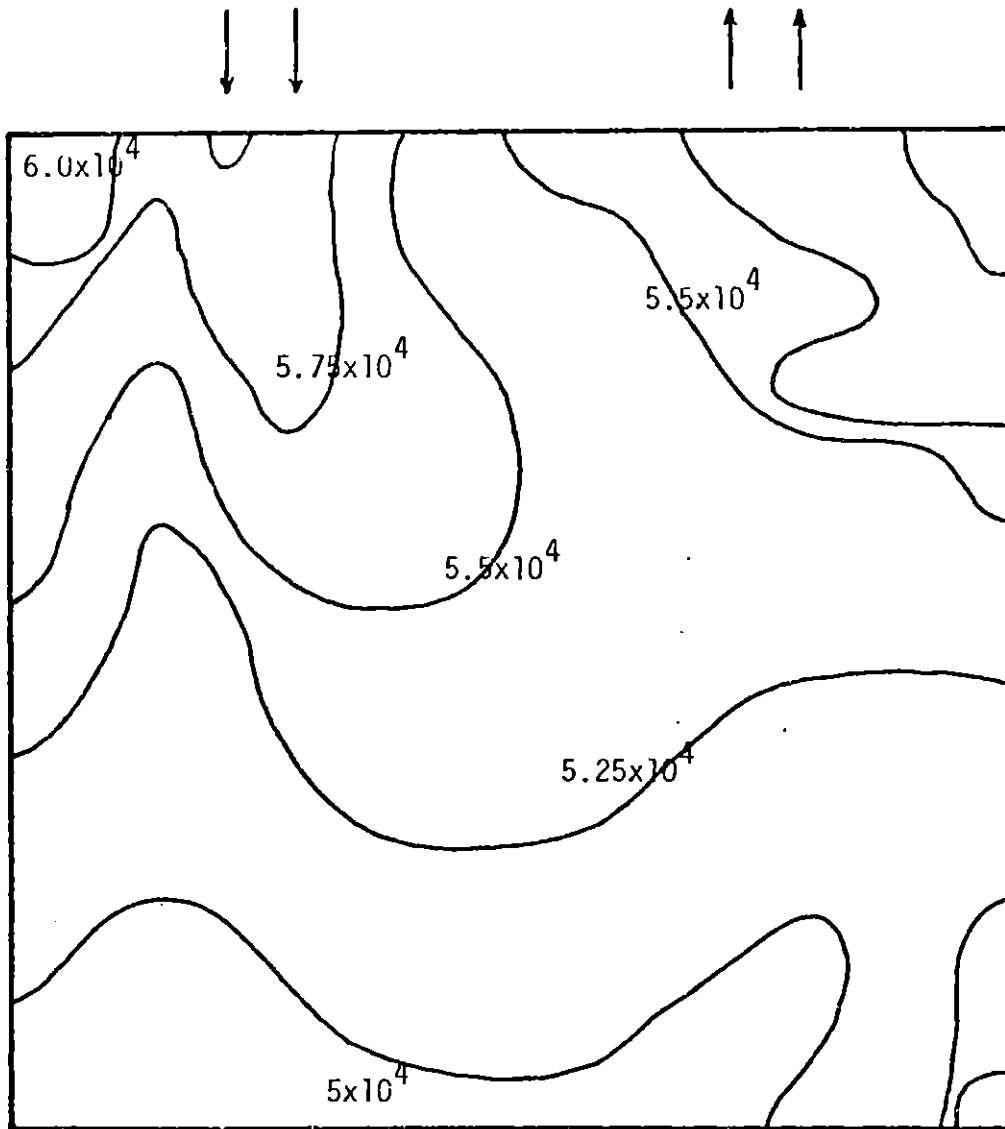


Fig. 5.15 Spatial distribution of the number of the oxidized particles at the time  $t = 120$  sec. ( $d_p = 20 \mu\text{m}$ ).

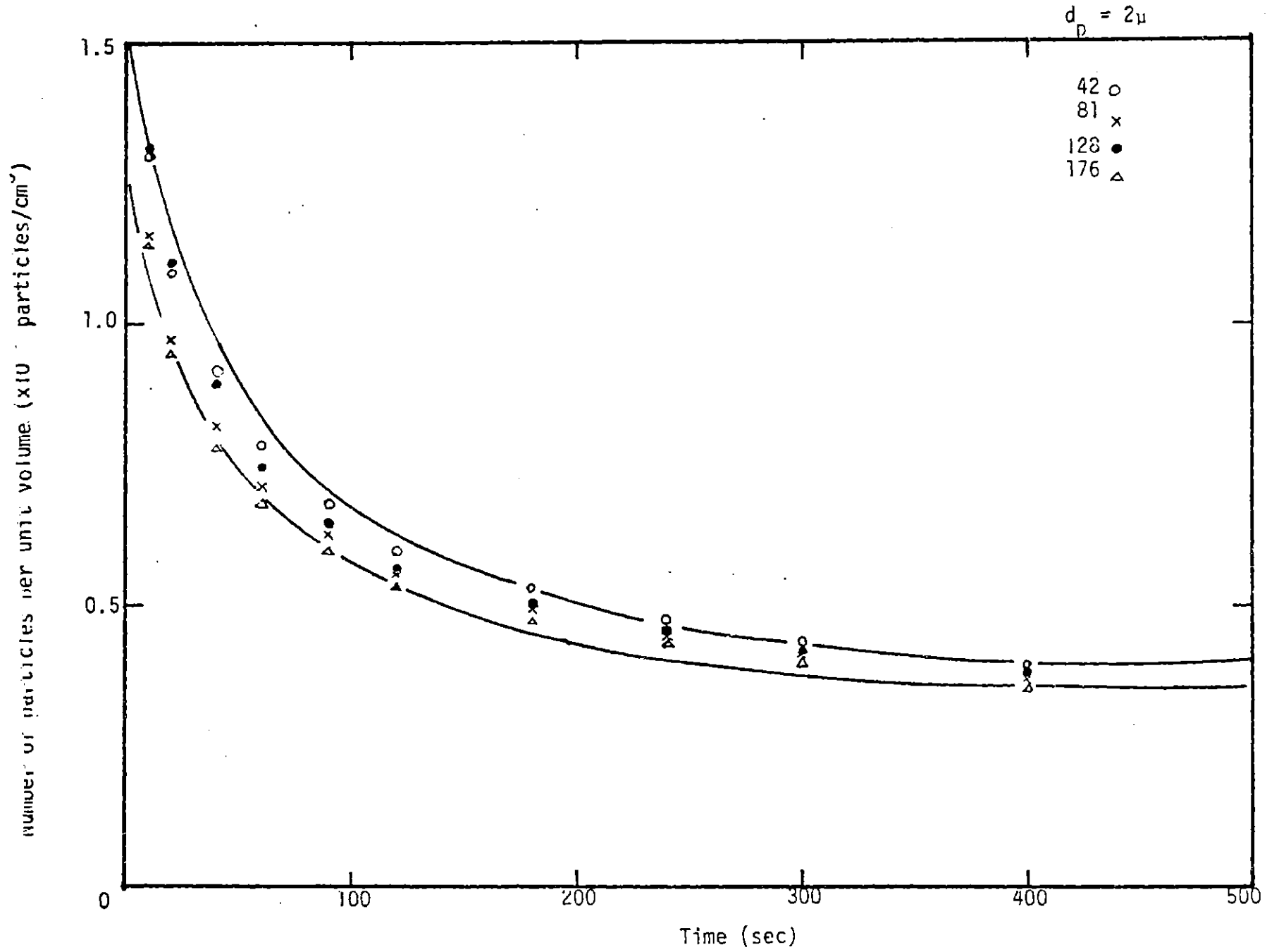


Fig. 5.16 The number of inclusions  $v_s$  time ( $d_p = 10\mu$ )

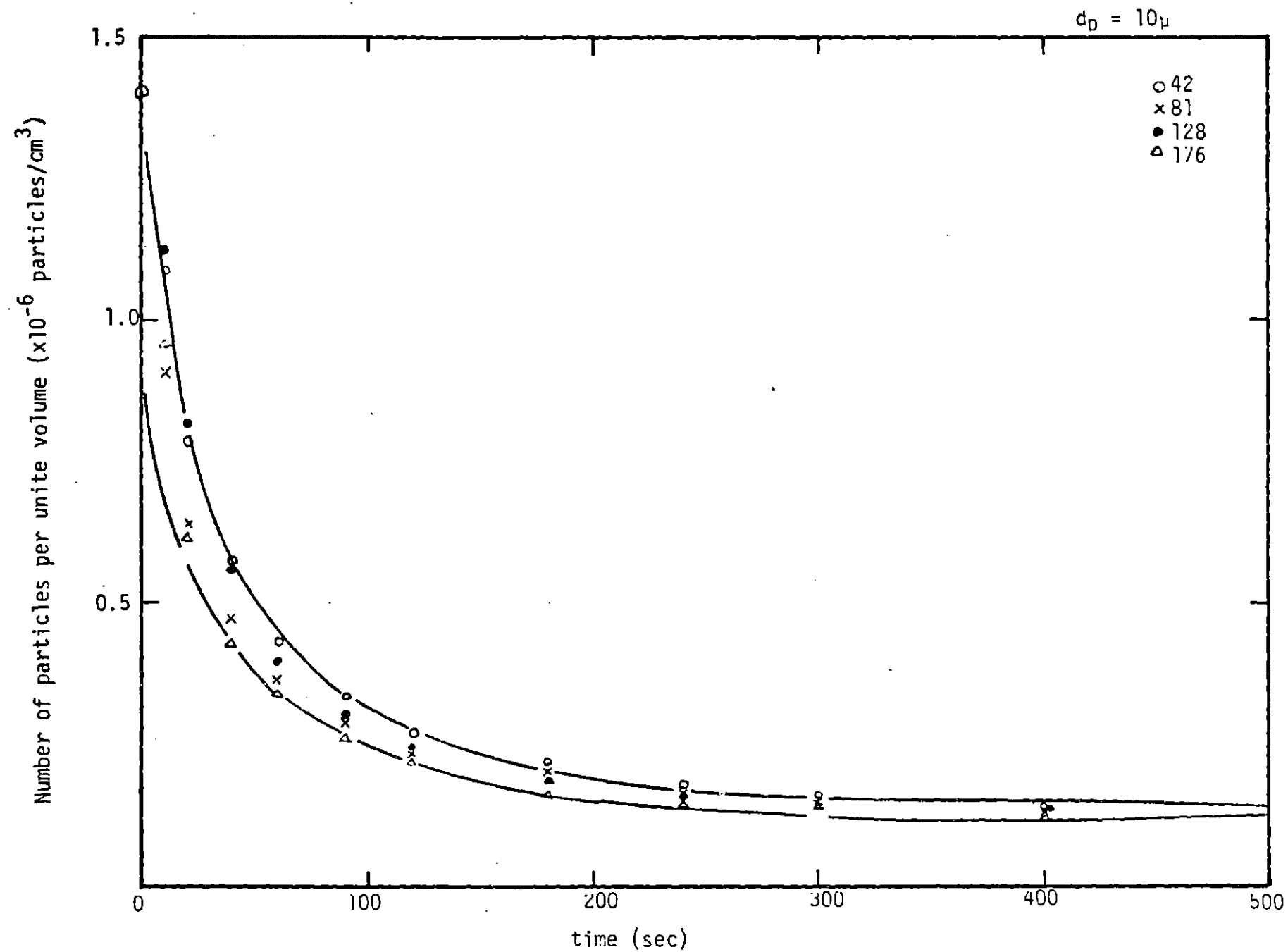


Fig. 5.17 The number of inclusions vs time ( $d_p = 10\mu\text{m}$ )

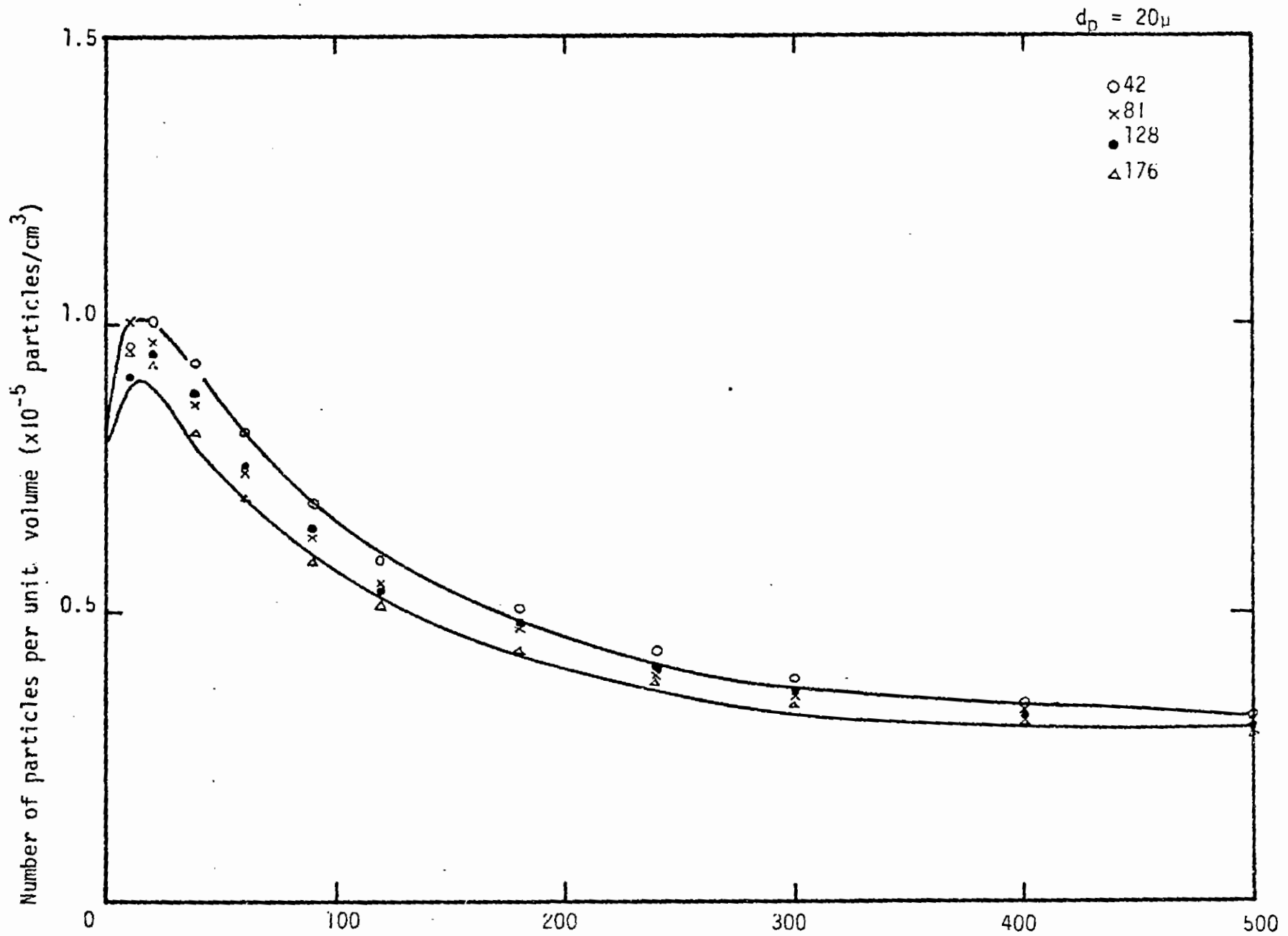


Fig. 5.18 The number of inclusions vs Time (sec) ( $d_p = 20\mu\text{m}$ )

classes from  $1\mu\text{m}$  to  $128\mu\text{m}$ , but initial particles have only sizes of 1, 2 and  $4\mu\text{m}$ , so that it takes several minutes for particles to reach the critical size, in their case  $32\mu\text{m}$ . On the contrary, in the present calculation the critical size of particles is considered to be  $20\mu\text{m}$  and the particles of size  $20\mu\text{m}$  exist from the beginning of the computation. This may be the reason why the first stage didn't appear. It is very difficult to determine the critical particle sizes at which particles are rapidly separated from the bath. However, it may be said that the first stage will appear if the initial particle size is far smaller than the critical size.

Fig. 5.19 shows the initial coalescence frequency

$$N = 1.67 \left(\frac{\mathcal{E}}{\nu}\right)^{\frac{1}{2}} (r_1 + r_2)^3 n_1 n_2$$

where  $\mathcal{E}$  is taken as  $40 \text{ erg/cm}^3$ . The highest collision rate occurs for  $6\mu\text{m}$  particles and is almost equivalent to the initial number of  $6\mu\text{m}$  particles. Since the collision rate is proportional to the product of particle concentration and the third power of the sum of their radii, the coagulation rate is extra ordinarily high at initial stage but soon falls to a small value. Therefore, if the large particles are assumed to exist, the initial rate of particle removal is very rapid.

Until now, the discussion has been made on the basis of particle population, but major experimental results are expressed in mass scale. As Nakanishi [5] said in his paper, there is the discrepancy between the oxygen content obtained by the counting method and the chemical analysis. However, it may be practically meaningful to convert present particle number scale to mass scale,

$$[\%O] = \frac{100\pi M O_y}{6 \Omega \rho_{Fe}} \int_0^{d_{\max}} d^3 f(d) d(d)$$

$$E = 40 (\text{m}^2/\text{m}^2)$$

$d_1$ $d_2$	2	4	6	8	10	12	14	16	18	20
2	$9256 \cdot 10^1$	$3126 \cdot 10^1$	$7425 \cdot 10^1$	$1426 \cdot 10^1$	$2670 \cdot 10^1$	$3761 \cdot 10^1$	$5926 \cdot 10^1$	$8435 \cdot 10^1$	$1.157 \cdot 10^2$	$1.54 \cdot 10^2$
	$2.053 \cdot 10^2$	$3983 \cdot 10^1$	$5220 \cdot 10^1$	$5120 \cdot 10^1$	$5.208 \cdot 10^1$	$4.762 \cdot 10^1$	$3910 \cdot 10^1$	$3.081 \cdot 10^1$	$2.256 \cdot 10^1$	$1.732 \cdot 10^1$
4		$7405 \cdot 10^1$	$1.444 \cdot 10^2$	$2.670 \cdot 10^1$	$3761 \cdot 10^1$	$5926 \cdot 10^1$	$8.625 \cdot 10^1$	$1.157 \cdot 10^2$	$1.54 \cdot 10^2$	$1991 \cdot 10^1$
		$5.350 \cdot 10^1$	$5.77 \cdot 10^1$	$5.46 \cdot 10^1$	$4.703 \cdot 10^1$	$4.125 \cdot 10^1$	$3.155 \cdot 10^1$	$2.360 \cdot 10^1$	$1.702 \cdot 10^1$	$1.275 \cdot 10^1$
6			$2.670 \cdot 10^1$	$3761 \cdot 10^1$	$5926 \cdot 10^1$	$8.625 \cdot 10^1$	$1.157 \cdot 10^2$	$1.540 \cdot 10^2$	$1.991 \cdot 10^2$	$2.562 \cdot 10^2$
			$5.521 \cdot 10^1$	$4.550 \cdot 10^1$	$3.595 \cdot 10^1$	$3.171 \cdot 10^1$	$2.315 \cdot 10^1$	$1.737 \cdot 10^1$	$1.222 \cdot 10^1$	$896 \cdot 10^1$
8				$5.926 \cdot 10^1$	$8.625 \cdot 10^1$	$1.157 \cdot 10^2$	$1.540 \cdot 10^2$	$1.991 \cdot 10^2$	$2.562 \cdot 10^2$	$3.175 \cdot 10^2$
				$4.065 \cdot 10^1$	$3.07 \cdot 10^1$	$2.467 \cdot 10^1$	$1.956 \cdot 10^1$	$1.468 \cdot 10^1$	$1.092 \cdot 10^1$	$819 \cdot 10^1$
10					$1.157 \cdot 10^2$	$1.540 \cdot 10^2$	$1.991 \cdot 10^2$	$2.562 \cdot 10^2$	$3.175 \cdot 10^2$	$3905 \cdot 10^1$
					$2.269 \cdot 10^1$	$1.735 \cdot 10^1$	$1.231 \cdot 10^1$	$856 \cdot 10^1$	$609 \cdot 10^1$	$410 \cdot 10^1$
12						$1.991 \cdot 10^2$	$2.562 \cdot 10^2$	$3.175 \cdot 10^2$	$3905 \cdot 10^1$	$4.751 \cdot 10^2$
						$1.018 \cdot 10^1$	$8945 \cdot 10^1$	$6.092 \cdot 10^1$	$4.011 \cdot 10^1$	$2.562 \cdot 10^1$
14							$3.175 \cdot 10^2$	$3905 \cdot 10^1$	$4.751 \cdot 10^2$	$5.854 \cdot 10^2$
							$6.146 \cdot 10^1$	$4.824 \cdot 10^1$	$3.71 \cdot 10^1$	$1.971 \cdot 10^1$
16								$4.751 \cdot 10^2$	$5.854 \cdot 10^2$	$6.745 \cdot 10^2$
								$2.73 \cdot 10^4$	$1.773 \cdot 10^4$	$1.115 \cdot 10^4$
18									$6.745 \cdot 10^2$	$7926 \cdot 10^1$
									$1.140 \cdot 10^4$	$7.23 \cdot 10^3$
20										$7.402 \cdot 10^3$
										$5.207 \cdot 10^3$

Fig. 5.19 Initial coalescence frequency

where,  $M_O$  is the atomic weight of oxygen,  $\rho_{Fe}$  is the density of the molten iron,  $\Omega$  is the molar volume of oxide particle and  $y$  is the stoicheometric number of oxygen in oxide.

Fig. 5.20 shows the rate of deoxidation in mass scale at the grid point 81 and Fig. 5.21 shows the spatial distribution of oxygen content in the form of oxide.

Fig. 5.22 shows the non-dimensional deoxidation rate.



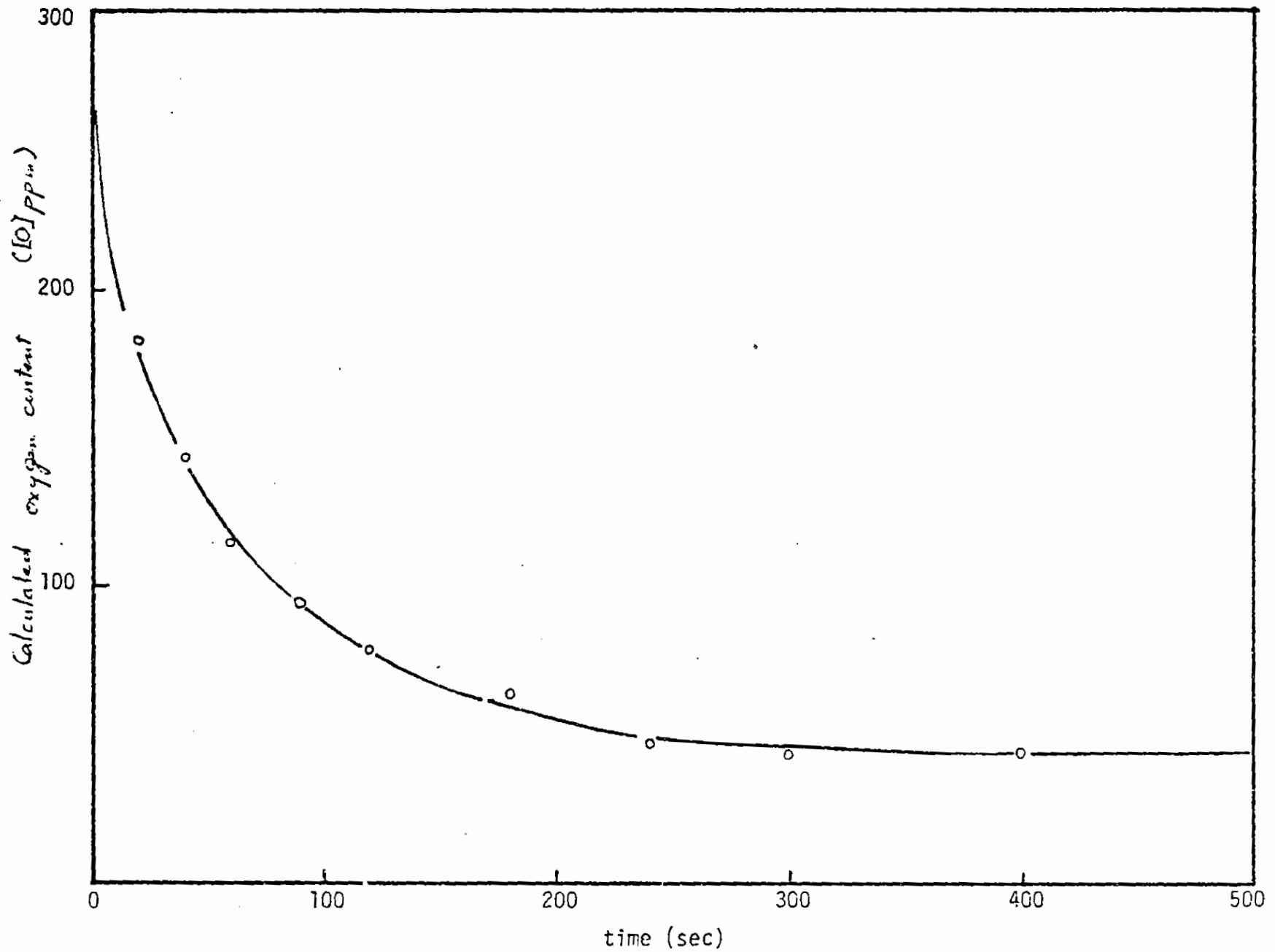


Fig. 5.20 The calculated total inclusion content vs time

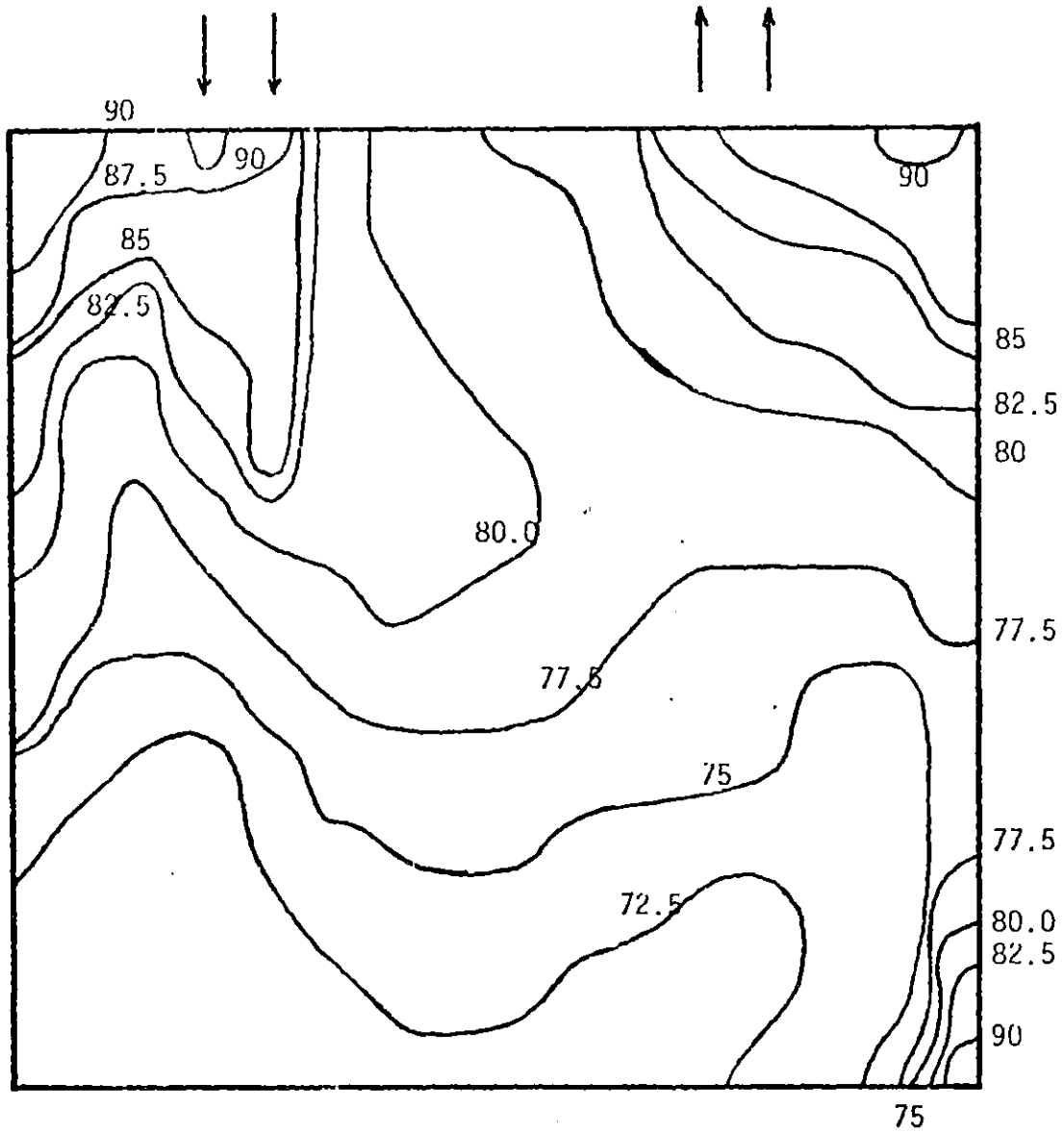


Fig. 5.21 Spatial distribution of oxygen content at the time  $t = 120$  sec. ( $[O]$  ppm).

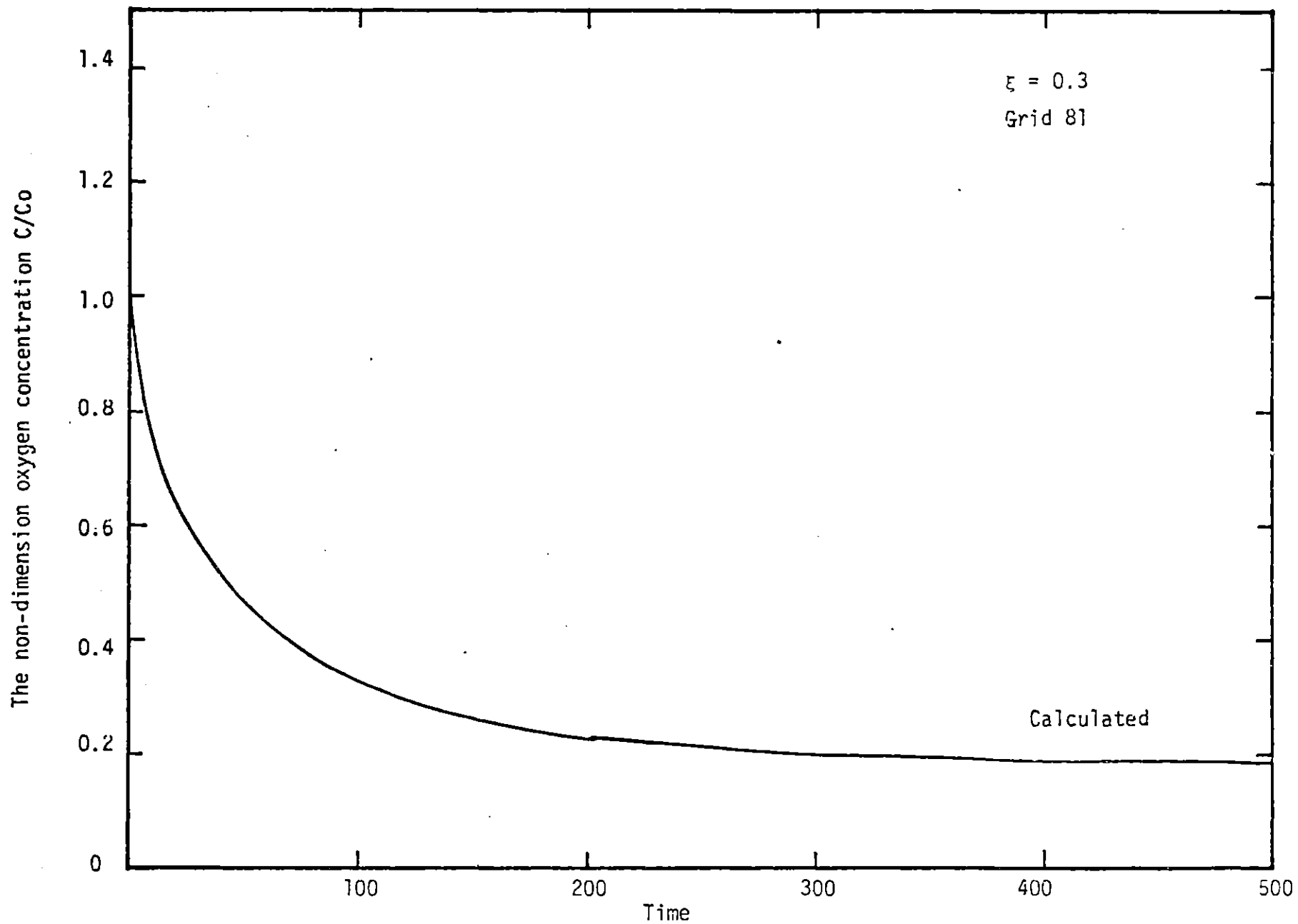


Fig. 5.22 The non-dimension oxvgen concentration vs time

## Chapter 6 Conclusions

Concluding remarks and some suggestions for future work are made in this chapter.

### 6.1 Conclusions

A mathematical model has been developed to describe fluid flow and oxidized particle coagulation phenomena in the R-H vacuum degassing system. The program consists of two parts: fluid flow program and particle coagulation program. Regarding the fluid flow calculation, the turbulent Navier-Stokes equations were solved by using a numerical technique developed by Pun and Spalding. The principal findings are succeeded as follows:

1. The computed results indicated that the metal moves quite rapidly in the upper part of the ladle, with maximum velocity - 60-70 cm/sec. In the lower part of the ladle the velocities are relatively small but still finite even at the bottom.
2. Two major local recirculating loops appear: one between the two legs and one near the wall of the down-leg side.
3. The metal velocity is quite fast in the vicinity of the vertical walls.
4. The turbulence characteristics, i.e., the kinetic energy of turbulence, the dissipation rate of the kinetic energy of turbulence and the effective viscosity are very large just below the dow leg which is consistent with the velocity field.
5. The effective diffusivity is high just under the dow leg with the maximum value  $70 \text{ cm}^2/\text{sec}$ , but the region of the low effective diffusivity appears between the two legs.

The particle coalescence calculations involved population balance models coupled to the previously computed velocity field. The following principal

results are:

1. The time-dependent particle distribution was obtained at each grid point in the ladle. Under the assumption presently used, the reduction rate of particles is rapid for the intermediate size particles because of the high probability to encounter other particles.

2. Regarding the spatial distribution of the particle, the high concentration appears in the vicinity of the dow-leg and the up-leg. The concentration tends to be lower at the lower portion of the ladle except at the corner of bottom and up-leg side wall.

3. The larger particles were found to increase at the very initial stage of the mixing. It is suggested that the larger particles play important role in the reduction of the smaller particles. Possibly the addition of larger particles would contribute to reduce the very small particle inclusions.

## 6.2 Suggestion for a further study

The present work represents a first attempt at combining population balance models with the representation of turbulent recirculating flows to model metal deoxidation kinetics. The results which have been presented indicate that this could be a very fruitful approach to a rather boarder class of problems. The following appear to be rather obvious extensions of the present study:

1. The model could be extended to represent the removal of oxide particles due to collision with the walls of the system.
2. The model could be extended to include a dynamic oxygen balance, which would allow for both the removal of oxygen due to the removal of the inclusions and the addition of oxygen to the system from the walls and or from the atmosphere.
3. The chemical factors which influence the collision efficiency could also be incorporated into the model and finally.
4. While the actual model development was undertaken within the framework of the R-H system, clearly identical consideration could be applied to other deoxidation systems, involving turbulent recirculation flow.

## NOMENCLATURE

$A_i$	Coefficients in the finite-difference equations ( $i = W, E, N, S$ )
$B$	Nucleation function in Table 2.1
$b$	Distribution function of daughter particles
$C_i$	Particle density
$C_D$	Dissipation constant
$C_d$	Drag coefficient
$C_1, C_2$	Constants in k- $\epsilon$ model
$d_p$	Partical diameter
$D$	Dissipation term for kinetic energy of turbulence
$D_a$	Brownian diffusional coefficient in Table 2.2
$D$	Diffusion coefficient
$D_i$	Diffusion conductance defined by Equ. (4.1.21)
$E$	Function of wall roughness in Equ. (3 4.16)
$E$	Energy-spectrum function
$f(\xi, t)$	Number density of particles at $\xi, t$
$f$	The friction factor
$F_i$	Mass flow rate defined by Equ. (4.1.20)
$F_L, F_S$	Forces acting on the sphere in Equations (2.6.1) and (2.6.2)
$G$	The function for diffusional growth
$h(x, m, t)$	Production term in Equ. (2.4.4)
$k$	Mass transfer coefficient for particles
$K$	Kinetic energy of turbulence
$\lambda$	Characteristic length scale of turbulence
$\lambda_\epsilon$	Dissipation length in Equ. (2.7.10)
$m$	Mass scale for number density function
$n_i$	Number of particles in $i$ -th class

$N_{grad}$	Rate of particle coalescence by velocity gradient collision
$N_{turb}$	Rate of particle coalescence by turbulent collision
$p$	Time-smoothed static pressure
$P_i, Q_i$	Coefficients for pressure correction
$P_e$	Peclet number
$r$	Radius of particles
$S^+$	Non-dimensional stopping length for a particle
$S_\phi$	Source term for variable $\phi$
$S_\phi$	$= S_u + S_p \phi_p$
$t$	Time
$u$	X-directional component of velocity
$V$	Y-directional component of velocity
$v$	Kolmogorov's velocity scale
$W_w$	Radial component of the relative velocity around a particle
$X_s$	Height of the ladle
$Y_s$	Diameter of a ladle
$y, y_+$	Dimensional and dimensionless distance from the wall
<u>Greek</u>	
$\alpha$	Relaxation factor
$\alpha_{ij}$	Coalescence function between i-th and j-th class
$\alpha(x, m, t)$	Coalescence function in Table 2.1
$\beta(x, m, t)$	Breakage function of particles in Table 2.1
$\Gamma$	Velocity gradient around a particle in Equ. (2.6.15)
$\Gamma_\phi$	Diffusion Coefficient for the general variable
$\epsilon$	Rate of dissipation of kinetic energy of turbulence
	von Karman's constant
$\lambda, \lambda_E$	Lagrangian or Eulerian microscale, respectively



$\nu$	Kinetic viscosity
$\rho$	Density
$\rho_f$	Density of fluid
$\rho_p$	Density of particles
$\tau_1, \tau_2$	Stokes' forces
$\tau_w, \tau_0$	Shear stress near the wall
$\mu, \mu_t$	Laminar and turbulent viscosity of fluid
$\mu_{eff}$	Effective viscosity
$\eta$	Kolmogorov's scale length
$\phi$	General variable ( - u, v, k, )
$\omega$	Angular frequency

## APPENDIX A

## THE COMPUTER PROGRAM FOR FLUID FLOW CALCULATION

BLOCK DATA	CAS00010
COMMON	CAS00020
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL	CAS00030
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)	CAS00040
2.RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)	CAS00050
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)	CAS00060
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)	CAS00070
3, EMUX(22), HCONE(22), HCONN(22), HCONW(22)	CAS00080
3, PHOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)	CAS00090
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPhi(22)	CAS00100
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)	CAS00110
4, PDxu(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)	CAS00120
5/DUPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)	CAS00130
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)	CAS00140
5, RSSUM(10), ITITLE(10)	CAS00150
COMMON	CAS00160
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT	CAS00170
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF	CAS00180
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO	CAS00190
6, JU, JV, JVP1, KINP1, KMPA, KRAD, KRROMJ, KTEST, LABPHI	CAS00200
6, LASTEP, LINEF, LINEL, NEO, NEOP1	CAS00210
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NODMA, NUMCOL	CAS00220
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV	CAS00230
6, NY, NYMAX, NYM1, NYM2, PI, RSCHK, RSMAX, TINY	CAS00240
COMMON/PROP/ EMUPEF, PRL(10), PRT(10), RHOREF	CAS00250
COMMON/D2D1/ ARSL(22,10), RSLINE(22,10)	CAS00260
COMMON/D2D2/ U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)	CAS00270
7, RHO(484), EMU(484)	CAS00280
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH	CAS00290
COMMON	CAS00300
9/TURB/ C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)	CAS00310
9, TAUTW2(22), YPUST1(22), YPUST2(22)	CAS00320
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW	CAS00330
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA	CAS00340
9, INLY1, INLY2, IOUT1, IOUT2, I1M1, I2P1, I3M1, I4P1	CAS00350
COMMON/ABC/AREAE	CAS00360
DIMENSION F(3755)	CAS00370
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)	CAS00380
EQUIVALENCE (HCONS(2), HCONN(1))	CAS00390
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))	CAS00400
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)	CAS00410
EQUIVALENCE (F(1), U(1))	CAS00420
DIMENSION A(22), B(22)	CAS00430
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))	CAS00440
CHAPTER 1 ----- GENERAL FLOW PARAMETERS	CAS00450
DATA GREAT, TINY, PI/1.E30, 1.E-30, 3.1415926/	CAS00460
DATA RPIPE, XPIPE, UINLET, HINLET, HWALL/	CAS00470
1 250., 250., 72., 0.0, 0.0/	CAS00480
DATA KTEST/0/	CAS00490
CHAPTER 2 ----- GRID	CAS00500
DATA NXMAX, NYMAX/22, 22/	CAS00510
DATA KRAD/1/	CAS00520
DATA FXSTEP/1.0/	CAS00530
CHAPTER 3 ----- VARIABLES	CAS00540
DATA JU, JV, JTKE, JTED, JH, JPP, JP, JRHO, JEMU, JLAST/	CAS00550

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1 1, 2, 3, 4, 5, 6, 7, 8, 9, 9/
DATA NEO/4/
DATA KSOLVE/4*1.0,1,1,0,1,0/
DATA KADSCR/2*0.2-1.6*0/
DATA KRS/4*1.0,1,4*0/
CHAPTER 4 ----- PROPERTY DATA
DATA RHOREF, EMUREF/7.2,0.06/
DATA PRL,PRT/12*1.,0.9,7-1.0/
CHAPTER 5 ----- STARTING PREPARATIONS
DATA IXPREF,IYPREF/2,2/
DATA KINPRI/0/
CHAPTER 6 ----- STEP CONTROL
CHAPTER 7 ----- BOUNDARY CONDITIONS
DATA C1,C2,CD,CAPPA,ECONST/
1 1.43,1.92,0.09,0.4,9.0/
DATA SQRTCD,CD25/ 0.3,0.54722/
DATA FACTKE,FACTED/0.005,0.03/
CHAPTER 8 ----- ADVANCE
DATA NTDMA/1/
CHAPTER 9 ----- COMPLETE
CHAPTER 10 ----- ADJUST
DATA KMPA/0/
CHAPTER 11 ----- PRINT
DATA NUMCOL/10/
CHAPTER 12 ----- DECIDE
DATA LATESTP/100/
END
C
MAIN PROGRAM
COMMON
1/CASE1/UIINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AH(22), AP(22), AS(22), AX(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUX(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)
3, VOLUME(22), CCNN(22), CONS(22), CONE(22), CONW(22), ESMPH1(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSGUM(10), TITL(10)
COMMON
6/DD/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IYPREF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LATESTP, LINEF, LINEL, NEO, NEQP1
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PRDP/EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(452), V(452), TKE(484), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(484)

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CAS00560
CAS00570
CAS00580
CAS00590
CAS00600
CAS00610
CAS00620
CAS00630
CAS00640
CAS00650
CAS00660
CAS00670
CAS00680
CAS00690
CAS00700
CAS00710
CAS00720
CAS00730
CAS00740
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CAS00950
CAS00960
CAS00970
CAS00980
CAS00990
CAS01000
CAS01010
CAS01020
CAS01030
CAS01040
CAS01050
CAS01060
CAS01070
CAS01080
CAS01090
CAS01100

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7 .INLY(10),IOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH          CAS01110
COMMON                                                       CAS01120
9/TURB/C1,C2,CD,SDORTCD,CD25,ECONST,CTAUTW,CYPTW,TAUTW1(22) CAS01130
9,TAUTW2(22),YPUST1(22),YPUST2(22)                         CAS01140
9,TAULW(22),XPUSLW(22),CTAULW,CXPLW                       CAS01150
9,GENK(22),FACTKE,FACTED,UTKE,UTED,CAPPA                 CAS01160
9,INLY1,INLY2,IOUT1,IOUT2,I1M1,I2P1,I3M1,I4P1           CAS01170
COMMON/ABC/AREAE                                           CAS01180
DIMENSION F(3766)                                          CAS01190
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22)           CAS01200
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1))         CAS01210
EQUIVALENCE (RHOS(2),RHON(1)), (AREAE,AREAW)             CAS01220
EQUIVALENCE (HCONS(2),HCONN(1))                          CAS01230
EQUIVALENCE (F(1),U(1))                                   CAS01240
DIMENSION A(22),B(22)                                      CAS01250
EQUIVALENCE(A(1),AN(1)),(S(1),AS(1))                     CAS01260
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1 1 CAS01270
CASE1..... LAMINAR, UNIFORM-PROPERTY, DEVELOPING FLOW IN A PIPE CAS01280
COMMENT..... ALL NUMERICAL DATA ARE PUT IN VIA BLOCK DATA CAS01290
READ(5,9860) KTEST                                         CAS01300
READ(5,9860) NX,NY                                         CAS01310
READ(5,9860) (X(I),I=1,NX)                                CAS01320
READ(5,9860) (Y(I),I=1,NY)                                CAS01330
READ(5,9860) (RELAX(I),I=1,10)                            CAS01340
READ(5,9860) NTDMA,LASTEP,KSWEEP,NOUPT1,ISTEP1           CAS01350
READ(5,9860) IPLRS,IPRINT                                  CAS01360
READ(5,9860) RSCHEK,CCHECK,RSFCHE,RSFC2                  CAS01370
READ(5,9870) TKEINP,TEDINP                                CAS01380
READ(5,9860) KIN,KOUT                                      CAS01390
READ(5,9860) (INLY(I),I=1,KIN)                            CAS01400
READ(5,9860) (IOUT(I),I=1,KOUT)                          CAS01410
READ(5,9860) RLEG                                          CAS01420
READ(5,9860) IXMON,IYMON                                   CAS01430
READ(5,9860) ISTCH                                         CAS01440
READ(5,9860) RELTKE,RELTED                                 CAS01450
9850 FORMAT (BF10.0)                                       CAS01460
9860 FORMAT (10I5)                                         CAS01470
9870 FORMAT (5E10.3)                                       CAS01480
ISTEP=0                                                    CAS01490
ILINE=0                                                    CAS01500
DO 9800 JPHI=1,JLAST                                       CAS01510
JGROUP(JPHI)=0                                             CAS01520
DO 9800 IX=1,NX                                             CAS01530
9800 RSLINE(IX,JPHI)=0.0                                    CAS01540
C ----- PRINT OUT HEADINGS                               CAS01550
RSEJM=0.0                                                  CAS01560
RSEJM1=0.0                                                 CAS01570
JRSF=0                                                     CAS01580
JRSF1=0                                                    CAS01590
CALL OUTPH                                                CAS01600
CHAPTER 2 2 2 2 2 GRID 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 CAS01610
C ----- QUANTITIES RELATED TO NX AND NY                 CAS01620
CALL CONST2                                               CAS01630
C ----- CALCULATE GRID QUANTITIES                       CAS01640
CALL GEOM                                                  CAS01650

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      I2=ILAST(JPHI)
      DO 51 I=11,I2
51     F(I)=0.0
50     CONTINUE
C----- PUT U=UINLET AND H=HINLET IN FIELD, EXCEPT AT WALL
      DO 5009 IX=2,NXM2
      DO 5009 IY=2,NYM1
      I=IY+NY*(IX-1)
5009  U(I)=1.0
      DO 5010 IX=2,NXM1
      DO 5010 IY=2,NYM2
      I=IY+(IX-1)*NYM1
5010  V(I)=1.0
      DO 5011 IX=1,NXM1
      DO 5011 IY=2,NYM1
      I=IY+(IX-1)*NY
      TKE(I)=SQRT(TKEIN)
      TED(I)=SQRT(TEDIN)
      EMU(I)=CD*RHO(I)*TKE(I)**2/TED(I)+EMUREF
5011  CONTINUE
      DO 5012 IY=INLY1,INLY2
      IX=2
      I=IY+NY
      IW=I-NY
5012  EMU(IW)=CD*RHO(IW)*TKEIN**2/TEDIN+EMUREF
      DO 5013 IY=IOUT1,IOUT2
      I=IY+NY
      IW=I-NY
5013  EMU(IW)=CD*RHO(IW)*TKEIN**2/TEDIN+EMUREF
C----- INITIALIZE TDMA-LINE STORAGE
      DO 555 IY=1,NXYP
555   P(IY)=0.0
      DO 501 IY=1,NY
      AN(IY)=0.0
      DV(IY)=0.0
      AS(IY)=0.0
      AE(IY)=0.0
      AW(IY)=0.0
      SU(IY)=0.0
      SP(IY)=0.0
      DU(IY)=0.0
      VOLUME(IY)=0.0
      PP(IY)=0.0
501   PHIOLD(IY)=0.0
C----- INITIALIZE Y-DIRECTION ARRAYS
      DO 502 IX=1,NX
      YPUST1(IX)=0.0
      YPUST2(IX)=0.0
      TAUTW1(IX)=0.0
502   TAUTW2(IX)=0.0
C----- INITIALIZE Y-DIRECTION ARRAYS
      DO 503 IY=1,NY
      TAULW(IY)=0.0
503   XPUSLW(IY)=0.0
C----- PRINT OUT STARTING VALUES

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CAS02210
CAS02220
CAS02230
CAS02240
CAS02250
CAS02260
CAS02270
CAS02280
CAS02290
CAS02300
CAS02310
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CAS02340
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CAS02550
CAS02560
CAS02570
CAS02580
CAS02590
CAS02600
CAS02610
CAS02620
CAS02630
CAS02640
CAS02650
CAS02660
CAS02670
CAS02680
CAS02690
CAS02700
CAS02710
CAS02720
CAS02730
CAS02740
CAS02750

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IF(KTEST.GT.0) CALL TEST 13	CAS02760
IF(KINPRI.GT.0) CALL OUTPF	CAS02770
GO TO 60	CAS02780
55 IF(ISTEP.GT.1) GO TO 65	CAS02790
CHAPTER 6 6 6 6 6 STEP CONTROL 6 6 6 6 6 6 6 6 6	CAS02800
60 CONTINUE	CAS02810
DO 69 JPHI=1,NEQ	CAS02820
69 RSSUM(JPHI)=0.0	CASC2830
RSSUM(JPP)=0.0	CAS02840
FLOWUP=FLOWIN	CAS02850
IF(ISTEP.GT.1) GO TO 64	CAS02860
IF(ILINE.GT.0) GO TO 65	CAS02870
C----- Y-DIRECTION TDMA TRAVERSES	CAS02880
62 LINEF=2	CAS02890
LINEL=NXM1	CAS02900
NODEF=2	CAS02910
NODEL=NYM1	CAS02920
C----- FOR BOTH X- AND Y-DIRECTION TRAVERSES	CAS02930
NODEF1=NODEF-1	CAS02940
NODEL1=NODEL-1	CAS02950
NODLP1=NODEL+1	CAS02960
64 ILINE=LINEF	CAS02970
C----- QUANTITIES RELATED TO IX VALUE OF TDMA LINE	CAS02980
65 CONTINUE	CAS02990
IX=ILINE	CAS03000
IXP1=IX+1	CAS03010
IX1NY=(IX-1)*NY	CAS03020
IX1NY1=(IX-1)*NYM1	CAS03030
IX2NY2=(IX-2)*NYM2	CAS03040
DO 66 JPHI=1,JLAST	CAS03050
66 IXNY(JPHI)=IX1NY	CAS03060
IXNY(JV)=IX1NY1	CAS03070
IXNY(JP)=IX2NY2-1	CAS03080
CHAPTER 7 7 7 7 7 BOUNDARY CONDITIONS 7 7 7 7 7 7 7 7	CAS03090
IF(ISTEP.LT.ISTCH) GO TO 70	CAS03100
RELAX(JTKE)=RELTKE	CAS03110
RELAX(JTED)=RELTED	CAS03120
70 CONTINUE	CAS03130
IF(ISTEP.GT.1) GO TO 799	CAS03140
C-----U V H ON THE LADLE WALL	CAS03150
IN=NY+IX1NY	CAS03160
INV=NY-1+IX1NY1	CAS03170
IS=1+IX1NY	CAS03180
ISV=1+IX1NY1	CAS03190
U(IN)=0.0	CAS03200
V(INV)=0.0	CAS03210
U(IS)=0.0	CAS03220
V(ISV)=0.0	CAS03230
IF(IX.NE.2) GO TO 75	CAS03240
DD 7001 I=1,I1M1	CAS03250
7001 U(I)=0.0	CAS03260
DD 7002 I=INLY1,INLY2	CAS03270
TKE(I)=TKEIN	CAS03280
TED(I)=TEDIN	CAS03290
7002 U(I)=UINLET	CAS03300



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7003 DO 7003 I=I2P1,I3M1
      U(I)=0.0
      DO 7004 I=IOUT1,IOUT2
        TKE(I)=TKEIN
        TED(I)=TEDIN
7004 U(I)=-UINLET
      DO 7005 I=I4P1,NY
7005 U(I)=0.0
      75 CONTINUE
      799 CONTINUE
C-----CALCULATE TAU AND Y+ FOR LADLE WALL LEFT
      I=2+IX1NY
      IE=I-NY
      UP=U(IE)+(U(I)-U(IE))*FUNODE(IX)
      ABSUP=ABS(UP)
      IF(IX.EQ.2.AND.ABSUP.LE.TINY) UP=TINY
      RSQRTK=RHO(I)*SQRT(TKE(I))
      YPUST1(IX)=RSQRTK-CYPTW
      IF(YPUST1(IX).GT.11.5) GO TO 701
      TAUTW1(IX)=CTAUTW*UP
      GO TO 710
701 TAUTW1(IX)=CAPPA*UP*RSQRTK*CD25/ALOG(ECONST*YPUST1(IX))
710 CONTINUE
C-----CALCULATE TAU AND Y+ FOR LADLE WALL- RIGHT
      I=NYM1+IX1NY
      IW=I-NY
      UP=U(IW)+(U(I)-U(IW))*FUNODE(IX)
      ABSUP=ABS(UP)
      IF(IX.EQ.2.AND.ABSUP.LE.TINY) UP=TINY
      RSQRTK=RHO(I)*SQRT(TKE(I))
      YPUST2(IX)=RSQRTK*CYPTW
      IF(YPUST2(IX).GT.11.5) GO TO 702
      TAUTW2(IX)=CTAUTW*UP
      GO TO 711
702 TAUTW2(IX)=CAPPA*UP*RSQRTK*CD25/ALOG(ECONST*YPUST2(IX))
711 CONTINUE
C CALCULATE TAU AND X+ FOR LADLE BOTTOM
      IF(IX.NE.NXM1) GO TO 720
      DO 721 IY=2,NYM1
        I=IY+IX1NY
        IV=IY+IX1NY
        ISV=IV-1
        VP=V(ISV)+(V(IV)-V(ISV))*FVNODE(IY)
        RSQRTK=RHO(I)*SQRT(TKE(I))
        XPUSLW(IY)=RSQRTK*CXPLW
        IF(XPUSLW(IY).GT.11.5) GO TO 722
        TAULW(IY)=CTAULW*VP
        GO TO 721
722 TAULW(IY)=CAPPA*VP*RSQRTK*CD25/ALOG(ECONST*XPUSLW(IY))
721 CONTINUE
720 CONTINUE
CHAPTER 6 8 8 8 8 ADVANCE 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8
80 CONTINUE
C----- PUT NTRAVS EQUAL TO NTDMA, OR TO OTHER VALUES TO GIVE
C MULTI-TRAVERSE ON SELECTED LINES

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CAS03310
CAS03320
CAS03330
CAS03340
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CAS03370
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CAS03400
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CAS03780
CAS03790
CAS03800
CAS03810
CAS03820
CAS03830
CAS03840
CAS03850

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      NTRAVS=NTCMA
C----- PUT GREAT INTO ARSL'S
      DO 85 J=1,NEQ
85   ARSL(IX,J)=GREAT
C - OUTER LOOP FOR CARRYING OUT A MAX. OF NTRAVS TRAVERSES ON LINE IX
      DO 1000 NT=1,NTRAVS
      KOUNT(IX)=NT
      RSMAX=0.
C - INNER LOOP FOR ALL VARIABLES (PLUS ONE FOR PREPARATIONS FOR TRANSFER
C TO NEXT LINE OR TO NEXT SWEEP OF FIELD)
      DO 1001 JPHI=1,NEQP1
      IF(JPHI.EQ.NEQP1) GO TO 960
      IF(KSOLVE(JPHI).EQ.0) GO TO 1001
      JG=JGROUP(JPHI)
      IF(JG.NE.5) GO TO B4
      IF(NT.EQ.NTRAVS) GO TO 81
      IF(RSMAX.GT.RSCHEK) GO TO 1001
84   IF(ARSL(IX,JPHI).LT.RSCHEK.AND.ARSL(IX,JPHI).GT.0.) GO TO 1001
81   IF(JPHI.NE.JU) GO TO 83
      IF(IX.EQ.NXM1) GO TO 1001
C----- UPDATE JPHI ON TDMA LINE
83   RSLINE(IX,JPHI)=0.0
      LABPHI=JPHI
      CALL COEFF(JPHI)
      CALL MODIFY(JPHI)
      IF(KTEST.GT.2) CALL TEST 31
      CALL SOLVE(JPHI)
      IF(JPHI.GE.JU) CALL BOUND(JPHI)
      RSLINE(IX,JPHI)=RSLINE(IX,JPHI)/RSREF(JPHI)
      ABSRS=ABS(RSLINE(IX,JPHI))
      ARSL(IX,JPHI)=ABSR5
      RSMAX=AMAX1(RSMAX,ABSR5)
      IF(KTEST.GT.1) CALL TEST 21
      GO TO (1010,1020,930,940,1001), JG
CHAPTER 9 9 9 9 9 COMPLETE 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9
930 CONTINUE
COMMENT INSERT INSTRUCTIONS HERE TO UPDATE RHO. ALSO CALL
COMMENT BOUND(RHO) IF APPROPRIATE
      GO TO 1011
940 CONTINUE
COMMENT INSERT INSTRUCTIONS HERE TO UPDATE EMU. ALSO CALL
COMMENT BOUND(EMU) IF APPROPRIATE
      DO 911 IY=NODEF,NODEL
      I=IY+IX*INY
      EMUNEW=(CD*RHO(I)+TKE(I))/(TED(I)+TINY)+TKE(I)+EMUREF
      EMU(I)=EMU(I)+(EMUNEW-EMU(I))*RELAX(JEMU)
911 CONTINUE
      CALL BOUND(JEMU)
      GO TO 1001
960 IF(NT.EQ.NTRAVS) GO TO 961
      IF(RSMAX.LE.RSCHEK) GO TO 961
      GO TO 1001
C----- PREPARATIONS FOR TRANSFER TO THE NEXT LINE OR TO
C THE NEXT SWEEP OF THE FIELD
C ----- SUM OF RESIDUAL-SOURCE VALUES ON LINE FOR EACH JPHI

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961 DO 962 J=1,JPP                                CAS04410
    IF(KSOLVE(J).EQ.0) GO TO 962                  CAS04420
    IF(J.EQ.JU.AND.IX.EQ.NXM1) GO TO 962         CAS04430
    RSSUM(J)=RSSUM(J)+ARSL(IX,J)                 CAS04440
962 CONTINUE                                     CAS04450
C----- CHECK IF LAST LINE OF FIELD REACHED    CAS04460
    IF(ILINE.EQ.LINEL) GO TO 963                 CAS04470
C----- PREPARE FOR MOVING TO NEXT LINE         CAS04480
COMMENT IF REQUIRED, CALCULATE FLOWUP FOR THE NEW LINE HERE. IN THE CAS04490
COMMENT PRESENT SET-UP FLOWUP HAS BEEN PUT EQUAL TO FLOWIN, AS   CAS04500
COMMENT PROBLEMS OF THE FIXED FLOW-RATE TYPE ASSUMED           CAS04510
    ILINE=ILINE+1                                CAS04520
    GO TO 55                                      CAS04530
C - PREPARE FOR BEGINNING THE NEXT SWEEP OF THE FIELD          CAS04540
C     MAX. RESIDUAL-SOURCE VALUE IN FIELD FOR CONVERGENCE CHECK CAS04550
963 RSMAX=0.0                                     CAS04560
    DO 964 J=1,JPP                                CAS04570
964 RSVAX=AMAX1(RSMAX,RSSUM(J))                  CAS04580
C     ADJUST P'S TO GIVE ZERO AT REF. LOCATION                CAS04590
    PIPREF=P(IPREF)                              CAS04600
    DO 965 IP=1,NXYP                              CAS04610
965 P(IP)=P(IP)-PIPREF                          CAS04620
    GO TO 110                                     CAS04630
CHAPTER 10 10 10 10 ADJUST 10 10 10 10 10 10 10 10 10 10 CAS04640
C----- ADJUSTMENT AFTER UPDATING U'S           CAS04650
1010 IF(KSOLVE(JRHO).EQ.0) GO TO 1011           CAS04660
    CALL BOUND(JU)                                CAS04670
    GO TO 1001                                    CAS04680
C----- OVERALL CONTINUITY CORRECTION          CAS04690
1011 IF(KMPA.NE.0) CALL DVACDN                  CAS04700
    CALL BOUND(JU)                                CAS04710
    IF(KTEST.GT.1) CALL TEST 22                  CAS04720
    GO TO 1001                                    CAS04730
C----- ADJUSTMENT AFTER UPDATING V'S         CAS04740
1020 IF(KSOLVE(JPP).NE.0) GO TO 1021           CAS04750
    CALL BOUND(JV)                                CAS04760
    GO TO 1001                                    CAS04770
C----- CELL-WISE CONTINUITY CORRECTION       CAS04780
1021 RSLINE(IX,JPP)=0.0                         CAS04790
    CALL COEFF(JPP)                              CAS04800
    CALL MODIFY(JPP)                             CAS04810
    LABPHI=JPP                                   CAS04820
    IF(KTEST.GT.2) CALL TEST 31                  CAS04830
    CALL SOLVE(JPP)                              CAS04840
    RSLINE(IX,JPP)=RSLINE(IX,JPP)/RSREF(JPP)    CAS04850
    ARSL(IX,JPP)=ABS(RSLINE(IX,JPP))            CAS04860
    CALL CELCON                                  CAS04870
    IF(KTEST.GT.1) CALL TEST 23                  CAS04880
    CALL BOUND(JV)                              CAS04890
    GO TO 1001                                    CAS04900
C----- END OF INNER J-LOOP                   CAS04910
1001 CONTINUE                                   CAS04920
C----- END OF OUTER NTRAVS LOOP              CAS04930
1000 CONTINUE                                   CAS04940
CHAPTER 11 11 11 11 PRINT 11 11 11 11 11 11 11 11 11 11 CAS04950

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110 CONTINUE CAS04960
C----- PRINT OUT RESIDUAL SOURCES AND VARIABLE VALUES CAS04970
C AT MONITORING LOCATION (IXMON,IYMON) CAS04980
IF(MOD(ISTEP,NOUTP1).EQ.0) CALL OUTP1 CAS04990
C----- PRINT OUT OF FIELD VALUES CAS05000
IF(RSMAX.LE.CCHECK) GO TO 115 CAS05010
IF(ISTEP.LT.0) GO TO 115 CAS05020
114 IF(MOD(ISTEP,IPRINT).NE.0.OR.ISTEP.EQ.0) GO TO 112 CAS05030
115 CALL OUTPF CAS05040
GO TO 120 CAS05050
112 IF(ISTEP.EQ.LASTEP) CALL OUTPF CAS05060
CHAPTER 12 12 12 12 DECIDE 12 12 12 12 12 12 12 12 12 CAS05070
C----- CONVERGENCE CHECK CAS05080
120 IF(RSMAX.LE.CCHECK) GO TO 1299 CAS05090
C----- CHECK IF LAST STEP IS REACHED CAS05100
IF(ISTEP.GE.LASTEP) GO TO 129 CAS05110
128 ISTEP=ISTEP+1 CAS05120
GO TO 60 CAS05130
129 CALL OUTP2 CAS05140
1299 WRITE(9,1300) NX,NY CAS05150
WRITE(9,1301) (X(I),I=1,NX) CAS05160
WRITE(9,1301) (Y(I),I=1,NY) CAS05170
WRITE(9,1301) (F(I),I=1,3766) CAS05180
1300 FORMAT(214) CAS05190
1301 FORMAT(5E13.5) CAS05200
END CAS05210
SUBROUTINE OUTPUT CAS05220
COMMON CAS05230
1/CASE1/UIINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL CAS05240
2/ENY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22) CAS05250
2,PSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22) CAS05260
3/DNYDNX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22) CAS05270
3,DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22) CAS05280
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22) CAS05290
3,PHIOLD(22), RHOE(22), RHDN(22), RHOW(22), SP(22), SU(22) CAS05300
3,VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22) CAS05310
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22) CAS05320
4,RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22) CAS05330
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10) CAS05340
5,JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10) CAS05350
5,SSUM(10), ITITLE(10) CAS05360
COMMON CAS05370
6/D0/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT CAS05380
6,ISTEP, IX, IXINY, IXINY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF CAS05390
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO CAS05400
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI CAS05410
6, LASTEP, LINEF, LINEL, NEQ, NEQP1 CAS05420
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL CAS05430
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV CAS05440
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY CAS05450
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF CAS05460
COMMON/D2D1/ARSL(22,10), RSLINE(22,10) CAS05470
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400) CAS05480
7, RHD(484), EMU(484) CAS05490
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH CAS05500

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IF(J.NE.JPP) GO TO 1160
STORE(J)=0.0
GO TO 116
1160 I=IMON(J)+IZERO(J)
STORE(J)=F(I)
116 CONTINUE
WRITE(6,1104) IXMON,IYMON
WRITE(6,1105) (STORE(J),J=1,JP)
KTRIP=0
----- KTRIP IS A LOCAL 'TRIPPING CONTROL SWITCH'
GO TO 1170
1140 KTRIP=KTRIP+1
IF(KTRIP.GT.1) GO TO 1141
WRITE(6,1114)
WRITE(6,1110) IXMON,IYMON
WRITE(6,9999)
WRITE(6,1111) (ITITLE(K),K=1,JP)
1141 WRITE(6,1112) ISTEP,(RSSUM(J),J=1,JPP)
DO 117 J=1,JP
IF(J.NE.JPP) GO TO 1142
STORE(J)=0.0
GO TO 117
1142 I=IMON(J)+IZERO(J)
STORE(J)=F(I)
117 CONTINUE
WRITE(6,1113) ISTEP,(STORE(J),J=1,JP)
1170 CONTINUE
1100 FORMAT(/1X,14HITERATION NO. ,13,2X,70(1H=),4X,14HITERATION NO. ,
1 13//
1 1X,63HALGEBRAIC SUM OF RESIDUAL SOURCES AT EACH LINE--RSLINE(1X,
1JPHI)//)
1101 FORMAT(1X,13HIX NO. TRAVS,2X,10(3X,I4,3X))
1102 FORMAT(1X,12,6X,I2,3X,1P10E10.2)
1103 FORMAT(/1X,37HSUM OF ABS. VALUES OF RSLINE(IX,JPHI)//
11X,13(1H-),1P10E10.2//)
1104 FORMAT(/1X,31HVALUES AT MONITORING LOCATION (.I2,1H.,I2,1H)/
1 1X,6X,1P10E10.2)
1105 FORMAT(1X,13(1H-),1P10E10.2)
1110 FORMAT(/1X,58HSUM OF ABS. VALUES OF RSLINE(IX,JPHI), PRECEDED BY
1*****/1X,30HVALUES AT MONITORING LOCATION(.I2,1H.,I2,1H),
2 22H, PRECEDED BY -----)
1111 FORMAT(/1X,6X,5HITER.,3X,10(3X,I4,3X))
1112 FORMAT(/1X,6H-*****,1X,I3,3X,1P10E10.2)
1113 FORMAT(1X,6H-----,1X,I3,3X,1P10E10.2)
1114 FORMAT(/1X,60(1H-))
9999 FORMAT(/1X,56H( 1 = U, 2 = V, 3 = H, 4 = PP, 5 = P, 6 = RHO, 7 = E
1MU ))/
RETURN
CHAPTER 5 5 5 5 5 5
ENTRY OUTP2
DO50 IX=2,NXM1
I=2+(IX-1)*NY
50 STGRE(IX)=TKE(I)/ABS(TAUTW1(IX))/RHO(I)
WRITE(6,500) (IX,TAUTW1(IX),YPUST1(IX),STORE(IX),IX=2,NXM1)
500 FORMAT(/1X,20H VALUES OF WALL//1X,3H IX,2X,11H TUU ,

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CAS06060  
CAS06070  
CAS06080  
CAS06090  
CAS06100  
CAS06110  
CAS06120  
CAS06130  
CAS06140  
CAS06150  
CAS06160  
CAS06170  
CAS06180  
CAS06190  
CAS06200  
CAS06210  
CAS06220  
CAS06230  
CAS06240  
CAS06250  
CAS06260  
CAS06270  
CAS06280  
CAS06290  
CAS06300  
CAS06310  
CAS06320  
CAS06330  
CAS06340  
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CAS06360  
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CAS06550  
CAS06560  
CAS06570  
CAS06580  
CAS06590  
CAS06600

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111H Y+ ,11H K/UTAU**2 /((1X,I3,2X,1P3E11.3))
DO 59 IX=2,NXM1
I=NXM1+(IX-1)*NY
59 STORE(IX)=TKE(I)/ABS(TAUTW2(IX)/RHO(I))
WRITE(6,500) (IX,TAUTW2(IX),YPUST2(IX),STORE(IX),IX=2,NXM1)
FACTOR=CD/CD25
C-----CALAULATE AND PRINT OUT LENGTH SCALE
DO 503 IX=1,NX
DO 503 IY=1,NY
I=IY+(IX-1)*NY
503 TED(I)=FACTOR*TKE(I)*SQRT(TKE(I))/(TKE(I)+RPIPE+TINY)
CALL PRINT(JTED)
RETURN
END
SUBROUTINE CONST
COMMON
1/CASE1/ UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3 , EMUW(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10)
COMMON
6/DC/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IDEF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON /PREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEQ, NEQ1
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NDCMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PROP/ EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/ U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(484)
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YPUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, INLY1, INLY2, IOUT1, IOUT2, I1M1, I2P1, I3M1, I4P1
COMMON/ABC/AREAE
DIMENSION F(3766)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (PHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1))

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CAS06610
CAS06620
CAS06630
CAS06640
CAS06650
CAS06660
CAS06670
CAS06680
CAS06690
CAS06700
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CAS07080
CAS07090
CAS07100
CAS07110
CAS07120
CAS07130
CAS07140
CAS07150

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	EQUIVALENCE (F(1),U(1))	CAS07160
	DIMENSION A(22),B(22)	CAS07170
	EQUIVALENCE(A(1),AN(1)),(B(1),AS(1))	CAS07180
C	----- CONSTANTS RELATED TO NX AND NY -----	CAS07190
	ENTRY CONST2	CAS07200
	NXM1=NX-1	CAS07210
	NXM2=NX-2	CAS07220
	NYM1=NY-1	CAS07230
	NYM2=NY-2	CAS07240
C	----- TOTAL NUMBER OF NODES FOR DIFFERENT VARIABLES -----	CAS07250
	NXYG=NX*NY	CAS07260
	NXYP=NXM2+NYM2	CAS07270
	NXYU=NXM1+NY	CAS07280
	NXYV=NX+NYM1	CAS07290
	INLY1=INLY(1)	CAS07300
	INLY2=INLY(KIN)	CAS07310
	IOUT1=IOUT(1)	CAS07320
	IOUT2=IOUT(KOUT)	CAS07330
	I1M1=INLY1-1	CAS07340
	I2P1=INLY2+1	CAS07350
	I3M1=IOUT1-1	CAS07360
	I4P1=IOUT2+1	CAS07370
	RETURN	CAS07380
C	----- CONSTANTS RELATED TO VARIABLES -----	CAS07390
	ENTRY CONST3	CAS07400
	JVP1=JV+1	CAS07410
	NEQ1=NEQ+1	CAS07420
	KPHOMU=KSOLVE(JRHO)+KSOLVE(JEMU)	CAS07430
C	----- IZERO,ILAST AND IEW FOR DIFFERENT VARIABLES -----	CAS07440
	IZERO(1)=0	CAS07450
	DO 35 J=1,JLAST	CAS07460
	IF(J-JU) 310,301,310	CAS07470
310	IF(J-JV) 320,302,320	CAS07480
320	IF(J-JP) 330,303,330	CAS07490
330	IF(J-JPP) 305,304,305	CAS07500
301	IL=NXYU	CAS07510
	ILMAX=(NXMAX-1)*NYMAX	CAS07520
	IEW(J)=NY	CAS07530
	GO TO 34	CAS07540
302	IL=NXYV	CAS07550
	ILMAX=NXMAX*(NYMAX-1)	CAS07560
	IEW(J)=NYM1	CAS07570
	GO TO 34	CAS07580
303	IL=NXP	CAS07590
	ILMAX=(NXMAX-2)*(NYMAX-2)	CAS07600
	IEW(J)=NYM2	CAS07610
	GO TO 34	CAS07620
304	IL=NY	CAS07630
	ILMAX=NYMAX	CAS07640
	IEW(J)=0	CAS07650
	GO TO 34	CAS07660
305	IL=NXYG	CAS07670
	ILMAX=NXMAX=NYMAX	CAS07680
	IEW(J)=NY	CAS07690
34	ILAST(J)=IZERO(J)+IL	CAS07700



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IF(J.EQ.JLAST) GO TO 35
JP1=J+1
IZERO(JP1)=IZERO(J)+ILMAX
35 CONTINUE
C ----- ASSIGNING VALUES TO JGROUP(JPHI)
DO 351 J=1,NEQ
JGROUP(J)=5
IF(J.EQ.JU) JGROUP(J)=1
IF(J.EQ.JV) JGROUP(J)=2
IF(J.GE.JLIM1.AND.J.LE.JLIM2) JGROUP(J)=3
IF(J.GE.JLIM3.AND.J.LE.JLIM4) JGROUP(J)=4
351 CONTINUE
C ----- ASSIGNING NAMES TO THE TITLE-ARRAY
ITITLE(JU)=JU
ITITLE(JV)=JV
ITITLE(JP)=JP
ITITLE(JPP)=JPP
ITITLE(JTKE)=JTKE
ITITLE(JTED)=JTED
ITITLE(JRHO)=JRHO
ITITLE(JEMU)=JEMU
ITITLE(JH)=JH
RETURN
C ----- CONSTANTS RELATED TO CHAP. 5 OF MAIN -----
ENTRY CONSTS
IPREF=IYPREF-1+(IXPREF-2)*NYM2
DO 56 J=1,JLAST
IF(J.EQ.JPP) GO TO 56
IMON(J)=IYMON+(IXMON-1)*IEW(J)
IF(J.EQ.JP) IMON(J)=IYMON-1+(IXMON-2)*IEW(J)
56 CONTINUE
RETURN
END
SUBROUTINE ADJUST
COMMON
1/CASE1/ UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), RDYG(22), RDYV(22)
2,RSYG(22),RSYV(22),RV(22),RVCB(22),SYG(22),SYV(22),Y(22),YV(22)
3/DNYONX/AE(22),AN(22),AP(22),AS(22),AW(22),C(22),D(22),DIFE(22)
3,DIFN(22),DUW(22),DIFW(22),DU(22),DV(22),EMUE(22),EMUN(22)
3,EMUW(22),HCONE(22),HCONN(22),HCONW(22)
3.PHIOLD(22),RHOE(22),RHON(22),RHOW(22),SP(22),SU(22)
3,VOLUME(22),CONN(22),CONS(22),CONE(22),CONW(22),ESMPHI(22)
4/DNX/ DXG(22),DXU(22),FU(22),FUNODE(22),KOUNT(22),RDYG(22)
4,RSXU(22),RSXG(22),RSXU(22),STORE(22),SXG(22),SXU(22),X(22),XU(22)
5/DJPHI/ IEW(10),JLAST(10),IMON(10),IXNY(10),IZERO(10)
5,JGROUP(10),KADSOR(10),KSDLVE(10),KRS(10),RELAX(10),RSREF(10)
5,RSSUM(10),ITITLE(10)
COMMON
6/DO/CCHECK,DP,FLOWPC,FLOWST,FLOWUP,GREAT,ILINE,IPLRS,IPREF,IPRINT
6,ISTEP,IX,IX1NY,IX1NY1,IX2NY2,IXMON,IXP1,IXPREF,IYMON,IYPREF
6,JEMU,JH,JLAST,JLIM1,JLIM2,JLIM3,JLIM4,JP,JPP, JRHO
6,JU,JV,JVP1,KINPRI,KMPA,KRAD,KRHOMU,KTEST,LABPHI
6,LASTEP,LINEF,LINEL,NEQ,NEQP1
6,NODEF,NODEF1,MODEL,MODEL1,NODLP1,NTDMA,NUMCOL

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CAS07710
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6,NX,NXMAX,NXM1,NXM2,NXYG,NXYP,NXYU,NXYV	CAS08260
6,NY,NYMAX,NYM1,NYM2,PI,RSCHK,RSMAX,TINY	CAS08270
COMMON/PROCP/EMUREF,PRL(10),PRT(10),RHOEF	CAS08280
COMMON/D2D1/ARSL(22,10),RSLINE(22,10)	CAS08290
COMMON/D2D2/U(462),V(462),TKE(484),TED(484),H(484),PP(22),P(400)	CAS08300
7,RHO(484),EMU(484)	CAS08310
7,INLY(10),IDOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH	CAS08320
COMMON	CAS08330
9/TURB/C1,C2,CD, SORTCD,CD25,ECONST,CTAUTW,CYPTW,TAUTW1(22)	CAS08340
9,TAUTW2(22),YPUST1(22),YPUST2(22)	CAS08350
9,TAULW(22),XPUSLW(22),CTAULW,CXPLW	CAS08360
9,GENK(22),FACTKE,FACTED,JTKE,JTED,CAPPA	CAS08370
9,INLY1,INLY2,IDOUT1,IDOUT2,I1M1,I2P1,I3M1,I4P1	CAS08380
COMMON/ABC/AREA	CAS08390
DIMENSION F(3765)	CAS08400
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22)	CAS08410
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1))	CAS08420
EQUIVALENCE (RHOS(2),RHON(1)), (AREA,AREAW)	CAS08430
EQUIVALENCE (HCONS(2),HCONN(1))	CAS08440
EQUIVALENCE (F(1),U(1))	CAS08450
DIMENSION A(22),B(22)	CAS08460
EQUIVALENCE(A(1),AN(1)),(B(1),AS(1))	CAS08470
CHAPTER 1 1 1 1 1 OVERALL-CONTINUITY CORRECTION 1 1 1 1 1	CAS08480
ENTRY DVACON	CAS08490
IF(IX.EQ.NXM1) RETURN	CAS08500
C----- ADJUST MEAN PRESSURE	CAS08510
FLOWST=0.0	CAS08520
SUMA=0.0	CAS08530
SUMRA=0.0	CAS08540
DO 104 IY=NODEF,NODEL	CAS08550
I=IY+IX1NY	CAS08560
IE=I+NY	CAS08570
AREA=SYG(IY)*R(IY)	CAS08580
SUMA=SUMA+AREA	CAS08590
RA=0.5*(RHO(I)+RHO(IE))*AREA	CAS08600
SUMRA=SUMRA+RA	CAS08610
FLOWST=FLOWST+RA*U(I)	CAS08620
104 CONTINUE	CAS08630
DELU=(FLOWUP-FLOWST)/SUMRA	CAS08640
DP=-DELU*(FLOWUP+FLOWST)/SUMA	CAS08650
FLOWPC=0.0	CAS08660
DO 105 IY=NODEF,NODEL	CAS08670
C----- CORRECT P AT DOWNSTREAM PLANE	CAS08680
IP=IY-1+IX2NY2+NYM2	CAS08690
P(IP)=P(IP)+DP	CAS08700
C----- CORRECT U'S	CAS08710
I=IY+IX1NY	CAS08720
IE=I+NY	CAS08730
ROE=0.5*(RHO(I)+RHO(IE))	CAS08740
U(I)=U(I)+DELU	CAS08750
FLOWPC=FLOWPC+U(I)*POE*SYG(IY)*R(IY)	CAS08760
105 CONTINUE	CAS08770
IF(IX.EQ.NXM2) RETURN	CAS08780
C----- ADD DP TO ALL OTHER DOWNSTREAM LOCATIONS	CAS08790
I1=NYM2+NYM2+IX2NY2+1	CAS08800

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DO 1075 IP=I1,NXYP
1075 P(IP)=P(IP)+DP
RETURN
CHAPTER 2 2 2 2 CELL-WISE CONTINUITY CORRECTION 2 2 2 2
ENTRY CELCON
IF(KSOLVE(JU).EQ.0) GO TO 200
IF(IX.EQ.NXM1) GO TO 200
C----- CORRECT U'S ON TDMA LINE.
DO 21 IY=NODEF,NODEL
I=IY+IX1NY
U(I)=U(I)+DU(IY)+PP(IY)
IW=I-NY
U(IW)=U(IW)-DUW(IY)+PP(IY)
21 CONTINUE
C----- CORRECT V'S ON TDMA LINE
200 IF(KSOLVE(JV).EQ.0) GO TO 210
DO 201 IY=NODEF,NODEL1
IV=IY+IX1NY1
201 V(IV)=V(IV)+DV(IY)*(PP(IY)-PP(IY+1))
C----- CORRECT P'S ON TDMA LINE
210 IF(KSOLVE(JPP).EQ.0) RETURN
ICONST=IX2NY2-1
RF=RELAX(JP)
DO 211 IY=NODEF,NODEL
IF=IY+ICONST
P(IP)=P(IP)+PP(IY)*RF
211 PP(IY)=0.0
RETURN
END
SUBROUTINE BOUND(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2,RSYG(22),RSYV(22),RV(22),RVCB(22),SYG(22),SYV(22),Y(22),YV(22)
3/DNYCNX/AE(22),ANI(22),AP(22),AS(22),AW(22),C(22),D(22),DIFE(22)
3,DIFN(22),DUW(22),DIFW(22),DU(22),DV(22),EMUE(22),EMUN(22)
3,EMUW(22),HCONE(22),HCONN(22),HCONW(22)
3,PHIOLD(22),RHCE(22),RHON(22),PHOW(22),SP(22),SU(22)
3,VOLUME(22),CONN(22),CONS(22),CONE(22),CONW(22),ESMPHI(22)
4/DNX/ DXG(22),DXU(22),FU(22),FUNODE(22),KOUNT(22),RDXG(22)
4,RDXU(22),RSXG(22),RSXU(22),STORE(22),SXG(22),SXU(22),X(22),XU(22)
5/DJPHI/ IEW(10),ILAST(10),IMON(10),IXNY(10),IZERO(10)
5,JGROUP(10),KADSOR(10),KSOLVE(10),KRS(10),RELAX(10),RSREF(10)
5,RSSUM(10),ITITLE(10)
COMMON
6/DO/CCHECK,DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6,1STEP,IX,IX1NY,IX1NY1,IX2NY2,IXMON,IXP1,IXPREF,IYMON,IYPREF
6,JEMU,JH,JLAST,JLIM1,JLIM2,JLIM3,JLIM4,JP,JPP,JRHQ
6,JU,JV,JVP1,KINPRI,KMPA,KRAD,KRHOMU,XTEST,LABPHI
6,LASTEP,LINEL,LINEL,NEQ,NEQP1
6,NODEF,NODEF1,NODEL,NODEL1,NODLP1,NTDMA,NUMCOL
6,NX,NXMAX,NXM1,NXM2,NXYG,NXYP,NXYU,NXYV
6,NY,NYMAX,NYM1,NYM2,PI,RSCHK,RSMAX,TINY
COMMON/PRCP/EMUREF,PRL(10),PRT(10),RHOREF
COMMON/D2D1/ARSL(22,10),RSLINE(22,10)

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COMMON/D2D2/U(462),V(462),TKE(484),TED(484),H(484),PP(22),P(400)	CAS09360
7,RHO(484),EMU(484)	CAS09370
7,INLY(10),IOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH	CAS09380
COMMON	CAS09390
9/TURB/C1,C2,CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)	CAS09400
9,TAUTW2(22),YPUST1(22),YPUST2(22)	CAS09410
9,TAULW(22),XPUSLW(22),CTAULW,CXPLW	CAS09420
9,GENK(22),FACTKE,FACTED,JTKE,JTED,CAPPA	CAS09430
9,INLY1,INLY2,IOUT1,IOUT2,I1M1,I2P1,I3M1,I4P1	CAS09440
COMMON/ASC/AREAE	CAS09450
DIMENSION F(3768)	CAS09460
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22)	CAS09470
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1))	CAS09480
EQUIVALENCE (RHOS(2),RHON(1)), (AREAE,AREAW)	CAS09490
EQUIVALENCE (HCONS(2),HCONN(1))	CAS09500
EQUIVALENCE (F(1),U(1))	CAS09510
DIMENSION A(22),B(22)	CAS09520
EQUIVALENCE (A(1),AN(1)), (B(1),AS(1))	CAS09530
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1	CAS09540
JPHI=LPHI	CAS09550
IF(JPHI.EQ.JU) GO TO 20	CAS09560
IF(JPHI.EQ.JH) GO TO 30	CAS09570
IF(JPHI.EQ.JEMU) GO TO 40	CAS09580
IF(JPHI.EQ.JTKE) GO TO 50	CAS09590
IF(JPHI.EQ.JTED) GO TO 60	CAS09600
IF(JPHI.EQ.JV) GO TO 70	CAS09610
IF(JPHI.EQ.JRHO) GO TO 80	CAS09620
RETURN	CAS09630
CHAPTER 2 2 2 2 2 UPDATING OF U ON BOUNDARIES 2 2 2 2 2	CAS09640
20 CONTINUE	CAS09650
RETURN	CAS09660
30 CONTINUE	CAS09670
CHAPTER 3 3 3 3 3 UPDATING OF H ON BOUNDARIES 3 3 3 3 3	CAS09680
RETURN	CAS09690
40 CONTINUE	CAS09700
CHAPTER 4 4 4 4	CAS09710
C-----LADLE FREE SURFACE	CAS09720
IF(IX.NE.2) RETURN	CAS09730
DO 41 IY=2,NYM1	CAS09740
I=IY+IX1NY	CAS09750
IW=I-NY	CAS09760
IF(IY.GE.INLY1.AND.IY.LE.INLY2) GO TO 41	CAS09770
IF(IY.GE.IOUT1.AND.IY.LE.IOUT2) GO TO 41	CAS09780
EMU(IW)=EMU(I)	CAS09790
41 CONTINUE	CAS09800
RETURN	CAS09810
CHAPTER 5 5 5 5 UPDATING OF TKE	CAS09820
50 CONTINUE	CAS09830
C-----FREE SURFACE	CAS09840
IF(IX.NE.2) GO TO 5001	CAS09850
DO 501 IY=2,I1M1	CAS09860
I=IY+IX1NY	CAS09870
IW=I-NY	CAS09880
501 TKE(IW)=TKE(I)	CAS09890
DO 502 IY=I2P1,I3M1	CAS09900

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      I=IY+IX1NY
      IW=I-NY
502  TKE(IW)=TKE(I)
      DO 503 IY=I4P1,NYM1
      I=IY+IX1NY
      IW=I-NY
503  TKE(IW)=TKE(I)
5001 CONTINUE
C-----LADLE WALL
      IL=1+IX1NY
      IR=NY+IX1NY
      TKE(IL)=0.0
      TKE(IR)=0.0
      RETURN
60  CONTINUE
CHAPTER 6 6 6 6 6  UPDATING OF TED
C-----FREE SURFACE
      IF(IX.NE.2) GO TO 6001
      DO 601 IY=2,I1M1
      I=IY+IX1NY
      IW=I-NY
601  TED(IW)=TED(I)
      DO 602 IY=I2P1,I3M1
      I=IY+IX1NY
      IW=I-NY
602  TED(IW)=TED(I)
      DO 603 IY=I4P1,NYM1
      I=IY+IX1NY
      IW=I-NY
603  TED(IW)=TED(I)
6001 CONTINUE
C-----LADLE WALL
      IL=1+IX1NY
      IR=NY+IX1NY
      TED(IL)=0.0
      TED(IR)=0.0
      RETURN
CHAPTER 7 7 7 7 7  UPDATING OF V
70  CONTINUE
C-----FREE SURFACE
      IF(IX.NE.2) RETURN
      III=I1M1-1
      DO 701 IY=2,III
      I=IY+IX1NY1
      IW=I-NYM1
701  V(IW)=V(I)
      III2=I3M1-1
      DO 702 IY=I2P1,III2
      I=IY+IX1NY1
      IW=I-NYM1
702  V(IW)=V(I)
      DO 703 IY=I4P1,NYM2
      I=IY+IX1NY1
      IW=I-NYM1
703  V(IW)=V(I)

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CAS10390
CAS10400
CAS10410
CAS10420
CAS10430
CAS10440
CAS10450

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RETURN	CAS10460
CHPTER B B B B UPDATING OF RHO	CAS10470
80 CONTINUE	CAS10480
RETURN	CAS10490
END	CAS10500
SUBROUTINE SOURCE(LPHI)	CAS10510
COMMON	CAS10520
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL	CAS10530
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)	CAS10540
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)	CAS10550
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)	CAS10560
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)	CAS10570
3, EMUX(22), HCDNE(22), HCONN(22), HCONW(22)	CAS10580
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)	CAS10590
3, VOLUME(22), CCNN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22)	CAS10600
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KDUNT(22), RDXG(22)	CAS10610
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)	CAS10620
5/DIPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)	CAS10630
5, IGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)	CAS10640
5, RSSUM(10), ITITLE(10)	CAS10650
COMMON	CAS10660
6/D2/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT	CAS10670
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF	CAS10680
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO	CAS10690
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI	CAS10700
6, LASTEP, LINEF, LINEL, NEO, NECP1	CAS10710
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL	CAS10720
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXU, NXYV	CAS10730
6, NY, NYMAX, NYM1, NYM2, P1, RSCHEK, RSMAX, TINY	CAS10740
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF	CAS10750
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)	CAS10760
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)	CAS10770
7, RHO(484), EMU(484)	CAS10780
7, INLY(10), IOUT(10), KIN, KDUT, RELTKE, RELTED, ISTCH	CAS10790
COMMON	CAS10800
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)	CAS10810
9, TAUTW2(22), YPUST1(22), YPUST2(22)	CAS10820
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW	CAS10830
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA	CAS10840
9, INLY1, INLY2, IOUT1, IOUT2, I1M1, I2P1, I3M1, I4P1	CAS10850
COMMON/ABC/AREAE	CAS10860
DIMENSION F(3766)	CAS10870
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)	CAS10880
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))	CAS10890
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)	CAS10900
EQUIVALENCE (HCONS(2), HCONN(1))	CAS10910
EQUIVALENCE (F(1), U(1))	CAS10920
DIMENSION A(22), B(22)	CAS10930
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))	CAS10940
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1	CAS10950
JPHI=LPHI	CAS10960
IF(JPHI.EQ.JU) GO TO 20	CAS10970
IF(JPHI.EQ.JV) GO TO 30	CAS10980
IF(JPHI.EQ.JPP) GO TO 40	CAS10990
IF(JPHI.EQ.JH) GO TO 50	CAS11000

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        IF(JPH1.EQ.JTKE) GO TO 60
        IF(JPH1.EQ.JTED) GO TO 70
        RETURN
CHAPTER 2 2 2 2 2  ADDITIONAL SOURCE TERMS FOR U  2 2 2 2
20  CONTINUE
    RETURN
CHAPTER 3 3 3 3 3  ADDITIONAL SOURCE TERMS FOR V  3 3 3 3
30  CONTINUE
    RETURN
CHAPTER 4 4 4 4 4  ADDITIONAL SOURCE TERMS FOR P'  4 4 4 4
40  CONTINUE
    RETURN
CHAPTER 5 5 5 5 5  ADDITIONAL SOURCE TERMS FOR H  5 5 5 5
50  CONTINUE
    RETURN
CHAPTER 6 6 6 6 6 6  ADDITIONAL SOURCE TERM FOR K
60  CONTINUE
    C2M1=C2-1.0
    DO 61 IY=NODEF,NODEL
        I=IY+IX1NY
        IW=I-NY
        IN=I+1
        INW=IW+1
        IS=I-1
        ISW=IW-1
        IV=IY+IX1NY1
        ISV=IV-1
        IEV=IV+NYM1
        ISEV=IEV-1
        IWV=IV-NYM1
        ISWV=IWV-1
        DUDX=(U(I)-U(IW))*RSXG(IX)
        DVDY=(V(IV)-V(ISV))*RSYG(IY)
        DUDY=0.5*(U(IN)+U(INW)-U(IS)-U(ISW))/(Y(IY+1)-Y(IY-1))
        DVDX=0.5*(V(IEV)+V(IEV)-V(IWV)-V(ISWV))/(X(IX+1)-X(IX-
1  1))
        IF(KRAD.EQ.2) GO TO 63
62  GENK(IY)=(EMU(I)-EMUREF)*(2.0*(DUDX**2+DVDY**2)+(DUDY+
1  DVDX)**2)
        GO TO 64
63  VP=V(ISV)+(V(IV)-V(ISV))*FVNODE(IY)
        VPDR=VP/R(IY)
        GENK(IY)=(2.0*(DUDX**2+DVDY**2+VPDR**2)+(DUDY+DVDX)**2)*
1  (EMU(I)-EMUREF)
64  CONTINUE
        SU(IY)=(1.5*GENK(IY)+C2M1*RHO(I)*TED(I))*VOLUME(IY)
61  SP(IY)=-C2*RHO(I)*TED(I)+0.5*GENK(IY))*VOLUME(IY)/
1  (TKE(I)+TINY)
        RETURN
CHAPTER 7 76 7 7 7  TURBULENT ENERGY DISSIPATION 7 7 7 7
70  CONTINUE
    C2M1=C2-1.0
    TC2M1=2.0*C2-1.0
    DO 71 IY=NODEF,NODEL
        I=IY+IX1NY

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CAS11010
CAS11020
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CAS11530
CAS11540
CAS11550

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IF(JPH1.EQ.JTKE) GO TO 60
IF(JPH1.EQ.JTED) GO TO 70
RETURN
CHAPTER 2 2 2 2 2 . MODIFICATIONS TO THE U-EQUATION COEFFICIENTS
20 CONTINUE
COMMENT -----AT LET-SIDE WALL
AS(2)=0.0
I=2+IX1NY
TAUA1=0.5*(TAUTW1(IX)+TAUTW1(IXP1))
TAUA1=ABS(TAUA1)
UI=U(I)
ABSUI=ABS(UI)
SP(2)=SP(2)-TAUA1*SXU(IX)/ABSUI
C -----AT RIGHT SIDE WALL
I=NYM1+IX1NY
AN(NYM1)=0.0
TAUA2=0.5*(TAUTW2(IX)+TAUTW2(IXP1))
TAUA2=ABS(TAUA2)
UI=U(I)
ABSUI=ABS(UI)
SP(NYM1)=SP(NYM1)-TAUA2*SXU(IX)/ABSUI
C-----NEAR FREE SURFACE
IF(IX.NE.2) GO TO 250
DO 210 IY=2, I1M1
210 AW(IY)=0.0
DO 211 IY=I2P1, I3M1
211 AW(IY)=0.0
DO 212 IY=I4P1, NYM1
212 AW(IY)=0.0
250 CONTINUE
IF(IX.NE.NXM2) RETURN
DO 251 I=2, NYM1
251 AE(IY)=0.0
RETURN
30 CONTINUE
CHAPTER 3 3 3 3 3 . MODIFICATIONS TO THE V-EQUATION COEFFICIENTS
C -----AT FREE SURFACE
IF(IX.NE.2) GO TO 310
III=I1M1-1
DO 311 IY=2, III
311 AW(IY)=0.0
III2=I3M1-1
DO 312 IY=I2P1, III2
312 AW(IY)=0.0
DO 313 IY=I4P1, NYM2
313 AW(IY)=0.0
310 IF(IX.NE.NXM1) RETURN
DO 340 IY=2, NYM2
I=IY+IX1NY1
AE(IY)=0.0
TAUA=0.5*(TAULW(IY)+TAULW(IY+1))
TAUA=ABS(TAUA)
VI=V(I)
ABSVI=ABS(VI)
340 SP(IY)=SP(IY)-TAUA*SYV(IY)/ABSVI

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CAS12110
CAS12120
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CAS12570
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CAS12630
CAS12640
CAS12650

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      RETURN
CHAPTER 4 4 4 4 4  MODIFICATIONS TO THE P'-EQUATION COEFFICIENTS
40  CONTINUE
C-----PUT P'=0 NEAR EXIT
      AS(2)=0.0
      AN(NYM1)=0.0
      IF(IX.NE.NXM1) RETURN
      DO 47 IY=2,NYM1
47  AE(IY)=0.0
      RETURN
CHAPTER 5 5 5 5 5  MODIFICATIONS TO THE H-EQUATION COEFFICIENTS
50  CONTINUE
      RETURN
CHAPTER 6 6 6 6 6  ----MODIFY OF K-EQUATION
60  CONTINUE
      SP1=0.0
      SU1=0.0
      SP2=0.0
      SU2=0.0
C-----FREE SURFACE
      IF(IX.NE.2) GO TO 610
      DO 61 IY=2,I1M1
61  AW(IY)=0.0
      DO 62 IY=I2P1,I3M1
62  AW(IY)=0.0
      DO 63 IY=I4P1,NYM1
63  AW(IY)=0.0
      AN(NYM1)=0.0
      AS(2)=0.0
610 CONTINUE
C-----LEFT SIDE WALL
      IY1=2
      AS(IY1)=0.0
      I=IY1+IX1NY
      IW1=I-NY
      INW=IW1+1
      IN=I+1
      UP=U(IW1)+(U(I)-U(IW1))*FUNODE(IX)
      UN=U(INW)+(U(IN)-U(INW))*FUNODE(IX)
      UN=ABS(0.5*(UP+UN))
      IF(IX.EQ.2.AND.UN.LE.TINY) UN=TINY
      ABSTAU=ABS(TAUTW1(IX))
      SU(IY1)=ABSTAU*UN-SXG(IX)*R(IY)
      SP(IY1)=-CD*RHO(I)*2*TKE(I)*UN*SXG(IX)*R(IY1)/(ABSTAU+TINY)
      SU1=SU(2)
      SP1=SP(2)
C-----RIGHT SIDE WALL
      IY2=NYM1
      AN(IY2)=0.0
      I=IY2+IX1NY
      IW=I-NY
      ISW=IW-1
      IS=I-1
      UP=U(IW)+(U(I)-U(IW))*FUNODE(IX)
      US=U(ISW)+(U(IS)-U(ISW))*FUNODE(IX)

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CAS12660
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CAS13200

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US=ABS(0.5*(UP+US))
IF(IX.EQ.2.AND.US.LE.TINY) US=TINY
ABSTAU=ABS(TAUTW2(IX))
SU(IY2)=ABSTAU+US+SXG(IX)*R(IY2)
SP(IY2)=-CD*RHO(I)**2*TKE(I)*US+SXG(IX)*R(IY2)/(ABSTAU+TINY)
SU2=SU(IY2)
SP2=SP(IY2)
C-----LADLE BOTTOM
IF(IX.NE.NXM1) RETURN
DO 650 IY=2,NYM2
AE(IY)=0.0
I=IY+IX1NY
IV=IY+IX1NY1
ISV=IV-1
ISW=ISV-NYM1
IWV=IV-NYM1
VP=V(ISV)+(V(IV)-V(ISV))*FVNODE(IY)
VW=V(ISW)+(V(IWV)-V(ISW))*FVNODE(IY)
VW=ABS(0.5*(VP+VW))
ABSTAU=ABS(TAULW(IY))
SU(IY)=ABSTAU+VW*SYG(IY)*R(IY)
SP(IY)=-CD*RHO(I)**2*TKE(I)*VW*SYG(IY)*R(IY)/(ABSTAU+TINY)
650 CONTINUE
SU(2)=SU(2)+SU1
SU(NYM1)=SU(NYM1)+SU2
SP(2)=SP(2)+SP1
SP(NYM1)=SP(NYM1)+SP2
660 CONTINUE
RETURN
CHAPTER 7 7 7 7 7 MODIFY TO THE E-EQUATION COEFF.
70 CONTINUE
SP1=0.0
SU1=0.0
C
C
IF(IX.NE.2) GO TO 750
DO 71 IY=2,I1M1
71 AW(IY)=0.0
DO 72 IY=I2P1,I3M1
72 AW(IY)=0.0
DO 73 IY=I4P1,NYM1
73 AW(IY)=0.0
750 CONTINUE
C-----LADLE WALL LEFT
IY1=2
I=IY1+IX1NY
CDK=SQRTCD*TKE(I)
TEDI=CDK*SQRT(CDK)/(CAPPA*DYG(NY))
PHIOLD(IY)=TEDI
SU(IY1)=GREAT*TEDI
SP(IY1)=-GREAT
SU1=SU(2)
SP1=SP(2)
C-----LADLE WALL RIGHT
IY2=NYM1

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CAS13210
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CAS13680
CAS13690
CAS13700
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CAS13730
CAS13740
CAS13750

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I=IY2+IX1NY	CAS13760
CDK=SQRTCD+TKE(I)	CAS13770
TEDI=CDK*SQRT(CDK)/(CAPPA+DYG(NY))	CAS13780
PHIOLD(IY2)=TEDI	CAS13790
SU(IY2)=GREAT+TEDI	CAS13800
SP(IY2)=-GREAT	CAS13810
SU2=SU(NYM1)	CAS13820
SP2=SP(NYM1)	CAS13830
760 CONTINUE	CAS13840
C-----LADLE BOTTOM	CAS13850
IF(IX.NE.NXM1) RETURN	CAS13860
TERM=1./(CAPPA+DXG(NX))	CAS13870
DO 700 IY=2,NYM1	CAS13880
I=IY+IX1NY	CAS13890
CDK=SQRTCD-TKE(I)	CAS13900
TEDI=CDK*SQRT(CDK)*TERM	CAS13910
PHIOLD(IY)=TEDI	CAS13920
SU(IY)=GREAT+TEDI	CAS13930
SP(IY)=-GREAT	CAS13940
700 CONTINUE	CAS13950
SU(2)=SU(2)+SU1	CAS13960
SP(2)=SP(2)+SP1	CAS13970
SU(NYM1)=SU(NYM1)+SU2	CAS13980
SP(NYM1)=SP(NYM1)+SP2	CAS13990
701 CONTINUE	CAS14000
RETURN	CAS14010
END	CAS14020
SUBROUTINE GEOM	CAS14030
COMMON	CAS14040
1/CASE1/ UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL	CAS14050
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)	CAS14060
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)	CAS14070
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)	CAS14080
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)	CAS14090
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)	CAS14100
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)	CAS14110
3, VOLUME(22), CONN(22), CON5(22), CONE(22), CONW(22), ESMPHI(22)	CAS14120
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)	CAS14130
4, RDXU(22), RSXG(22), RSXU(22), STCRE(22), SXG(22), SXU(22), X(22), XU(22)	CAS14140
5/DJPHI/ IEW(10), ILAST(10), IYON(10), IXNY(10), IZERO(10)	CAS14150
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)	CAS14160
5, RSSUM(10), ITITLE(10)	CAS14170
COMMON	CAS14180
6/DC/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT	CAS14190
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF	CAS14200
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO	CAS14210
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMJ, KTEST, LABPHI	CAS14220
6, LASTEP, LINEF, LINEL, NEQ, NEQF1	CAS14230
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL	CAS14240
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXV	CAS14250
6, NY, NYMAX, NYM1, NYM2, P1, RSCHEK, RSMAX, TJNY	CAS14260
COMMON/PROCP/ EMUREF, PRL(10), PRT(10), RHOREF	CAS14270
COMMON/D2D1/ ARSL(22,10), RSLINE(22,10)	CAS14280
COMMON/D2C2/ U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)	CAS14290
7, RHO(484), EMU(484)	CAS14300

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7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH          CAS14310
COMMON                                                         CAS14320
9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22) CAS14330
9, TAUTW2(22), YPUST1(22), YPUST2(22)                         CAS14340
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW                       CAS14350
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA               CAS14360
9, INLY1, INLY2, IOUT1, IOUT2, I1M1, I2P1, I3M1, I4P1        CAS14370
COMMON/ABC/AREAE                                             CAS14380
DIMENSION F(3766)                                             CAS14390
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)            CAS14400
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))           CAS14410
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)                CAS14420
EQUIVALENCE (HCONS(2), HCONN(1))                             CAS14430
EQUIVALENCE (F(1), U(1))                                     CAS14440
DIMENSION A(22), B(22)                                       CAS14450
EQUIVALENCE(A(1), AN(1)), (B(1), AS(1))                      CAS14460
CHAPTER 1 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1           CAS14470
GO TO(21,22), KRAD                                           CAS14480
CHAPTER 2 2 2 2 2 2 2 RADII 2 2 2 2 2 2 2 2                CAS14490
21 DO 25 IY=1, NY                                             CAS14500
25 R(IY)=1.                                                    CAS14510
GO TO 23                                                       CAS14520
22 DO 26 IY=1, NY                                             CAS14530
26 R(IY)=Y(IY)                                                CAS14540
23 CONTINUE                                                  CAS14550
CHAPTER 3 3 3 3 3 3 3 CELL-NODE DISTANCES 3 3 3 3 3 3 3 3 CAS14560
C----- GRID-NODE DISTANCES                                CAS14570
DXG(1)=0.0                                                    CAS14580
DYG(1)=0.0                                                    CAS14590
DO 30 IX=2, NX                                               CAS14600
30 DXG(IX)=X(IX)-X(IX-1)                                     CAS14610
RDXG(IX)=1./DXG(IX)                                         CAS14620
DO 31 IY=2, NY                                               CAS14630
31 DYG(IY)=Y(IY)-Y(IY-1)                                    CAS14640
RDYG(IY)=1./DYG(IY)                                         CAS14650
C----- U-NODE DISTANCES                                CAS14660
XU(1)=X(1)                                                    CAS14670
DO 32 IX=2, NXM2                                             CAS14680
32 XU(IX)=0.5*(X(IX)+X(IX+1))                                CAS14690
XU(NXM1)=X(NX)                                               CAS14700
XU(NX)=0.0                                                    CAS14710
DXU(1)=0.0                                                    CAS14720
DO 33 IX=2, NXM1                                             CAS14730
33 DXU(IX)=XU(IX)-XU(IX-1)                                  CAS14740
RDXU(IX)=1./DXU(IX)                                         CAS14750
DXU(NX)=0.0                                                  CAS14760
C----- V-NODE DISTANCES AND V-CELL BOUNDARY RADII      CAS14770
YV(1)=Y(1)                                                    CAS14780
RV(1)=R(1)                                                    CAS14790
RVCB(1)=R(1)                                                 CAS14800
DO 34 IY=2, NYM2                                             CAS14810
34 YV(IY)=0.5*(Y(IY)+Y(IY+1))                               CAS14820
RV(IY)=0.5*(R(IY)+R(IY+1))                                  CAS14830
RVCB(IY)=R(IY)                                               CAS14840
RVCB(2)=R(1)                                                 CAS14850

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YV(NYM1)=Y(NY)
RV(NYM1)=R(NY)
RVCB(NYM1)=R(NY)
YV(NY)=0.0
RV(NY)=0.0
RVCB(NY)=0.0
DYV(1)=0.0
DC 35 IY=2,NYM1
DYV(IY)=YV(IY)-YV(IY-1)
35 RDYV(IY)=1./DYV(IY)
DYV(NY)=0.0
CHAPTER 4 4 4 4 4 4 CELL DIMENSIONS 4 4 4 4 4 4 4
C----- GRID-NODE CELLS
SXG(1)=0.0
DD 40 IX=3,NXM2
40 SXG(IX)=0.5*(DXG(IX)+DXG(IX+1))
SXG(2)=DXG(2)+0.5*DXG(3)
SXG(NXM1)=0.5*DXG(NXM1)+DXG(NX)
SXG(NX)=0.0
SYG(1)=0.0
DD 41 IY=3,NYM2
41 SYG(IY)=0.5*(DYG(IY)+DYG(IY+1))
SYG(NY)=0.0
SYG(2)=DYG(2)+0.5*DYG(3)
SYG(NYM1)=DYG(NY)+0.5*DYG(NYM1)
DO 45 IX=2,NXM1
45 RSXG(IX)=1./SXG(IX)
DO 46 IY=2,NYM1
46 RSYG(IY)=1./SYG(IY)
C----- U-VELOCITY CELLS
SXU(1)=0.0
SXU(2)=X(3)-X(1)
NXM3=NX-3
DO 42 IX=3,NXM3
42 SXU(IX)=X(IX+1)-X(IX)
SXU(NXM2)=X(NX)-X(NXM2)
SXU(NXM1)=0.0
SXU(NX)=0.0
DD 47 IX=2,NXM2
47 RSXU(IX)=1./SXU(IX)
C----- V-VELOCITY CELLS
SYV(1)=0.0
SYV(2)=Y(3)-Y(1)
NYM3=NY-3
DO 43 IY=3,NYM3
43 SYV(IY)=Y(IY+1)-Y(IY)
SYV(NYM2)=Y(NY)-Y(NYM2)
SYV(NYM1)=0.0
SYV(NY)=0.0
DO 48 IY=2,NYM2
48 RSYV(IY)=1./SYV(IY)
CHAPTER 5 5 5 5 5 5 FACTORS FOR INTERPOLATING U AND V 5 5 5
FU(1)=0.0
DO 50 IX=2,NXM1
50 FU(IX)=(X(IX)-XU(IX-1))/(XU(IX)-XU(IX-1))
CAS14860
CAS14870
CAS14880
CAS14890
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CAS15400

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FU(NX)=0.0
DO 52 IX=1,NX
52 FUNODE (IX)=FU(IX)
FV(1)=0.0
DO 51 IY=2,NYM1
51 FV(IY)=(Y(IY)-YV(IY-1))/(YV(IY)-YV(IY-1))
FV(NY)=0.0
DO 53 IY=1,NY
53 FVNODE (IY)=FV(IY)
FU(2)=0.0
FU(NXM1)=1.0
FV(2)=0.0
FV(NYM1)=1.0
RETURN
END
SUBROUTINE COEFF(LPHI)
COMMON
1/CASE1/ UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DHY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2,RSYG(22),RSYV(22),RV(22),RVCB(22),SYG(22),SYV(22),Y(22),YV(22)
3/DNYONX/AE(22),AN(22),AP(22),AS(22),AW(22),C(22),D(22),DIFE(22)
3,DIFN(22),DUW(22),DIFW(22),DU(22),DV(22),EMUE(22),EMUN(22)
3,EMUW(22),HCONE(22),HCONN(22),HCONW(22)
3,PHIOLD(22),RHOE(22),RHON(22),RHOW(22),SP(22),SU(22)
3,VOLUME(22),CONN(22),CONS(22),CONE(22),CONW(22),ESMPHI(22)
4/DNX/ DXG(22),DXU(22),FU(22),FUNODE(22),KOUNT(22),RDXG(22)
4,RDXU(22),RSXG(22),RSXU(22),STORE(22),SXG(22),SXU(22),X(22),XU(22)
5/DJPHI/ IEW(10),ILAST(10),IMON(10),IXNY(10),IZERO(10)
5,JGROUP(10),KADSOR(10),KSOLVE(10),KRS(10),RELAX(10),RSREF(10)
5,RSSUM(10),ITITLE(10)
COMMON
6/DD/CCHECK,DP,FLOWPC,FLOWST,FLOWUP,GREAT,ILINE,IPLRS,IPREF,IPRINT
6,ISTEP,IX,IX1NY,IX1NY1,IX2NY2,IXMON,IXP1,IXPREF,IYMON,IYPREF
6,JEMU,JH,JLAST,JLIM1,JLIM2,JLIM3,JLIM4,JP,JPP,JRHO
6,JU,JV,JVP1,KINPRI,KMPA,KRAD,KRHOMU,KTEST,LABPHI
6,LASTEP,LINEF,LINEL,NEQ,NEOP!
6,NODEF,NODEF1,NODEL,NODEL1,NODLP1,NTDMA,NUMCOL
6,NX,NXMAX,NXM1,NXM2,NXYG,NXYP,NXYU,NXYV
6,NY,NYMAX,NYM1,NYM2,PI,RSCHK,RSMAX,TINY
COMMON/PROF/EMUREF,PRL(10),PRT(10),RHOREF
COMMON/D2D1/ARSL(22,10),RSLINE(22,10)
COMMON/D2D2/U(462),V(462),TKE(484),TED(484),H(484),PP(22),P(400)
7,RHO(484),EMU(484)
7,INLY(10),IOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH
COMMON
9/TURB/C1,C2,CD,SORTCD,CD25,ECONST,CTAUTW,CYPTW,TAUTW1(22)
9,TAUTW2(22),YFUS1(22),YFUS2(22)
9,TAULW(22),XPUSLW(22),CTAULW,CXPLW
9,GENK(22),FACTKE,FACTED,JTKE,JTED,CAPPA
9,INLY1,INLY2,IOUT1,IOUT2,I1M1,I2P1,I3M1,I4P1
COMMON/ABC/AREAE
DIMENSION F(3766)
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22)
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1))
EQUIVALENCE (RHOS(2),RHON(1)), (AREAE,AREAW)

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CAS15410
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CAS15950

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EQUIVALENCE (HCONS(2),HCONN(1))
EQUIVALENCE (F(1),U(1))
DIMENSION A(22),B(22)
EQUIVALENCE(A(1),AN(1)),(B(1),AS(1))
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1
C----- DEFINE ARITHMETIC FUNCTION FOR COMBINING
C APPROPRIATELY CONVECTION AND DIFFUSION CONTRIBUTIONS
C----- HYBRID SCHEME
C CONDIF(DIFF,FCONV,CONV)=AMAX1(0.,DIFF+FCONV,CONV)
C----- UPWIND SCHEME
CONDIF(DIFF,FCONV,CONV)=AMAX1(DIFF,DIFF+CONV)
JPHI=LPHI
IF(KRAD.EQ.2) GO TO 12
ASSIGN 1001 TO LG
ASSIGN 201 TO LU1
ASSIGN 211 TO LU2
ASSIGN 301 TO LV1
ASSIGN 311 TO LV2
ASSIGN 401 TO LP
GO TO 13
12 ASSIGN 1002 TO LG
ASSIGN 202 TO LU1
ASSIGN 212 TO LU2
ASSIGN 302 TO LV1
ASSIGN 312 TO LV2
ASSIGN 402 TO LP
13 IF(KSOLVE(JRHO).EQ.0) GO TO 120
C----- CELL-WALL DENSITIES
IF(JPHI.GT.JVP1) GO TO 120
IF(JPHI.EQ.JU) CALL CELPHI(JPHI,JRHO)
IF(JPHI.EQ.JV) CALL CELPHI(JPHI,JRHO)
IF(JPHI.EQ.JVP1) CALL CELPHI(JPHI,JRHO)
C----- TRANSFER DENSITIES STORED IN AN( ) TO RHON( ),ETC.
N2=NODEL
IF(JPHI.EQ.JV) N2=NODEL1
RHOS(NODEF)=AS(NODEF)
DO 111 IY=NODEF,N2
RHON(IY)=AN(IY)
RHOE(IY)=AE(IY)
111 RHOW(IY)=AW(IY)
120 IF(KSOLVE(JEMU).EQ.0) GO TO 130
C----- CELL-WALL VISCOSITIES
IF(JPHI.GT.JVP1) GO TO 130
IF(JPHI.EQ.JU) CALL CELPHI(JPHI,JEMU)
IF(JPHI.EQ.JV) CALL CELPHI(JPHI,JEMU)
IF(JPHI.EQ.JVP1 .AND. JPHI.NE.JPP) CALL CELPHI(JPHI,JEMU)
C----- TRANSFER VISCOSITIES STORED IN AN( ) TO EMUN( ), ETC.
N2=NODEL
IF(JPHI.EQ.JV) N2=NODEL1
EMUS(NODEF)=AS(NODEF)
DO 121 IY=NODEF,N2
EMUN(IY)=AN(IY)
EMUE(IY)=AE(IY)
121 EMUW(IY)=AW(IY)
130 IF(JPP.EQ.JVP1) GO TO 140

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CAS15960
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CAS16490
CAS16500

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IF(JPH1.NE.JVP1) GO TO 140
C----- CONVECTION TERMS AND DIFFUSION-TERM*PRANDTL
C          NUMBER FOR GENERAL PHI EQUATIONS
SXGIX=SXG(IX)
AREA=SXG(IX)*RV(NODEF1)
DIFS(NCDEF)=EMUS(NODEF)*AREA*RDYG(NODEF)
ISV=NODEF1+IX1NY1
HCONS(NODEF)=0.5*RHOS(NODEF)*V(ISV)*AREA
RDXGIX=RDXG(IX)
RDXGI1=RDXG(IXP1)
DO 156 IY=NODEF,NODEL
IYM1=IY-1
I=IY+IX1NY
IW=I-NY
IV=IY+IX1NY1
AREAN=SXGIX
AREAE=SYG(IY)
GO TO LG.(1001,1002)
1002 AREAN=AREAN*RV(IY)
AREAE=AREAE*R(IY)
C AREAW=AREAE , THROUGH EQUIVALENCE
1001 VOLUME(IY)=AREAE*SXGIX
C DIFS(IY)=DIFN(IYM1) , THROUGH EQUIVALENCE
DIFN(IY)=EMUN(IY)*AREAN*RDYG(IY+1)
DIFE(IY)=EMUE(IY)*AREAE*RDXGI1
DIFW(IY)=EMUW(IY)*AREAW*RDXGIX
C HCONS(IY)=HCONN(IYM1) , THROUGH EQUIVALENCE
HCONN(IY)=0.5*RHON(IY)*V(IV)*AREAN
HCONE(IY)=0.5*RHOE(IY)*U(I)*AREAE
HCONW(IY)=0.5*RHOW(IY)*U(IW)*AREAW
CONN(IY)=HCONN(IY)+HCONN(IY)
CONS(IY)=HCONS(IY)+HCONS(IY)
CONE(IY)=HCONE(IY)+HCONE(IY)
CONW(IY)=HCONW(IY)+HCONW(IY)
ESMPHI(IY)=CONS(IY)-CONN(IY)+CONW(IY)-CONE(IY)
156 ESMPHI(IY)=A*MAX(0.0, -ESMPHI(IY))
140 IF(JPH1.EQ.JU) GO TO 20
IF(JPH1.EQ.JV) GO TO 30
IF(JPH1.EQ.JPP) GO TO 40
GO TO 50
CHAPTER 2 2 2 2 2 COEFFICIENTS FOR U-EQUATION 2 2 2 2 2
C----- FOR Y-DIRECTION TDMA TRAVERSES
C CALCULATE DIFFUSION AND CONVECTION COEFFICIENTS FOR SOUTH BOUNDARY
C OF BOTTOM CELL
20 AREA=SXU(IX)*RV(NCDEF1)
DN=EMUS(NCDEF)*AREA*RDYG(NODEF)
ISV=NODEF1+IX1NY1
ISEV=ISV+NYM1
HCN=0.25*RHOS(NODEF)*(V(ISV)+V(ISEV))*AREA
C----- COEFFICIENTS FOR ALL CELLS ON THE STRIP
FUIX=FU(IX)
OMFUIX=1.-FUIX
FUIXP1=FU(IXP1)
SXUIX=SXU(IX)
RDXUIX=RDXU(IX)

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CAS17030
CAS17040
CAS17050

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	RDXUI1=RDXU(IXP1)	CAS17060
	RSXUIX=RSXU(IX)	CAS17070
C	SET DU(IY)	CAS17080
	IF(IX.NE.2) GO TO 281	CAS17090
	DO 280 IY=NODEF,NODEL	CAS17100
280	DU(IY)=0.0	CAS17110
281	CONTINUE	CAS17120
	DO 285 IY=NODEF,NODEL	CAS17130
285	DUW(IY)=DU(IY)	CAS17140
	ASSIGN 27 TO NGOTO	CAS17150
	IF(KRHOMU.NE.0) GO TO 28	CAS17160
	ASSIGN 25 TO NGOTO	CAS17170
28	DO 26 IY=NODEF,NODEL	CAS17180
	I=IY+IX1NY	CAS17190
	IE=I+NY	CAS17200
	IW=I-NY	CAS17210
	IV=IY+IX1NY1	CAS17220
	IEV=IV+NYM1	CAS17230
	ISV=IV-1	CAS17240
	ISEV=IEV-1	CAS17250
	IP=IY-1+IX2NY2	CAS17260
	IEP=IP+NYM2	CAS17270
	IYP1=IY+1	CAS17280
	AREAN= SXUIX	CAS17290
	AREAE= SYG(IY)	CAS17300
	GO TO LU1,(201,202)	CAS17310
202	AREAN=AREAN+RV(IY)	CAS17320
	AREAE=AREAE+R(IY)	CAS17330
C	AREAW=AREAE , THROUGH EQUIVALENCE	CAS17340
201	VOLUME(IY)=AREAE* SXUIX	CAS17350
	DS=DN	CAS17360
	DN=EMUN(IY)*AREAN-RDYG(IYP1)	CAS17370
	DE=EMUE(IY)*AREAE-RDXU(IXP1)	CAS17380
	DW=EWUW(IY)*AREAW-RDXUIX	CAS17390
	HCS=HCN	CAS17400
	HCN=RHON(IY)+0.25*(V(IV)+V(IEV))*AREAN	CAS17410
	CN=HCN+HCN	CAS17420
	CS=HCS+HCS	CAS17430
	CE=RHOE(IY)*AREAE*(U(I)+(U(IE)-U(I))*FUIXP1)	CAS17440
	CW=RHOW(IY)*AREAW*(U(IW)+(U(I)-U(IW))*FUIX)	CAS17450
	FCE=FUIXP1*CE	CAS17460
	FCW=DMFUIX*CW	CAS17470
C	----- ERROR SOURCE OF MASS	CAS17480
	ESMASS=CS-CN+CW-CE	CAS17490
	FM=AMAX1(0.0,-ESMASS)	CAS17500
C	----- COMBINING DIFFUSION AND CONVECTION CONTRIBUTIONS	CAS17510
	AN(IY)=CONDIF(DN,-HCN,-CN)	CAS17520
	AS(IY)=CONDIF(DS, HCS, CS)	CAS17530
	AE(IY)=CONDIF(DE,-FCE,-CE)	CAS17540
	AW(IY)=CONDIF(DW, FCW, CW)	CAS17550
C	----- SOURCE TERMS	CAS17560
	DJ(IY)=AREAE	CAS17570
	SU(IY)=FM*U(I)+DJ(IY)*(P(IP)-P(IEP))	CAS17580
	SP(IY)=-FM	CAS17590
	GO TO NGOTO, (25,27)	CAS17600

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27  DUDXW=(U(I)-U(IW))*RDXUIX          CAS17610
    DUDXE=(U(IE)-U(I))*RDXUI1          CAS17620
    STERM=(EMUE(IY)*DUDXE-EMUW(IY)*DUDXW)*RSXUIX  CAS17630
    DVDXN=(V(IEV)-V(IV))*RSXUIX       CAS17640
    DVDXS=(V(ISEV)-V(ISV))*RSXUIX     CAS17650
    GO TO LU2,(211,212)                CAS17660
211 STERM=STERM+(EMUN(IY)*DVDXN-EMUS(IY)*DVDXS)/AREAE CAS17670
    GO TO 213                          CAS17680
212 STERM=STERM+(EMUN(IY)*RV(IY)*DVDXN-EMUS(IY)*RV(IY-1)*DVDXS)/AREAE CAS17690
213 SU(IY)=SU(IY)+STERM*VOLUME(IY)    CAS17700
C----- STORE U IN PHIOLD             CAS17710
25  PHIOLD(IY)=U(I)                   CAS17720
26  CONTINUE                          CAS17730
C----- PUT BOUNDARY END VALUES IN PHIOLD CAS17740
    I1=NODEF1+IX1NY                   CAS17750
    I2=NODLP1+IX1NY                   CAS17760
    PHIOLD(NODEF1)=U(I1)              CAS17770
    PHIOLD(NODLP1)=U(I2)             CAS17780
C----- ADDITIONAL SOURCE TERMS IF REQUIRED CAS17790
    IF(KADSOR(JU).NE.0) CALL SOURCE(JU) CAS17800
    RETURN                            CAS17810
CHAPTER 3 3 3 3 3 COEFFICIENTS FOR V-EQUATION 3 3 3 3 3 CAS17820
C----- FOR Y-DIRECTION TDMA TRAVERSES  CAS17830
C CALCULATE DIFFUSION AND CONVECTION COEFFICIENTS FOR SOUTH BOUNDARY CAS17840
C OF BOTTOM CELL                        CAS17850
30  AREA=SXG(IX)*RV(NODEF1)           CAS17860
    ISV=NODEF1+IX1NY1                 CAS17870
    DN=EMUS(NODEF)*AREA*RDYV(NODEF)   CAS17880
    CN=RHOS(NODEF)*V(ISV)*AREA        CAS17890
C----- COEFFICIENTS FOR ALL CELLS ON THE STRIP CAS17900
    SXGIX=SXG(IX)                    CAS17910
    RDXGIX=RDXG(IX)                  CAS17920
    RDXG11=RDXG(IXP1)               CAS17930
    RSXGIX=RSXG(IX)                 CAS17940
    ASSIGN 38 TO NGOTO                CAS17950
    IF(KRHOMU.NE.0) GO TO 34          CAS17960
    ASSIGN 37 TO NGOTO                CAS17970
34  DO 36 IY=NODEF,NODEL1             CAS17980
    I=IY+IX1NY                       CAS17990
    IN=I+1                            CAS18000
    IW=I-NY                           CAS18010
    INW=IW+1                          CAS18020
    IV=IY+IX1NY1                     CAS18030
    INV=IV+1                          CAS18040
    ISV=IV-1                          CAS18050
    IP=IY-1+IX2NY2                   CAS18060
    INP=IP+1                          CAS18070
    IYP1=IY+1                         CAS18080
    AREAN=SXGIX                       CAS18090
    AREAE=SYV(IY)                    CAS18100
    GO TO LV1,(301,302)              CAS18110
302 AREAN=AREAN*RVCB(IYP1)           CAS18120
    AREAE=AREAE*RV(IY)               CAS18130
C AREAW=AREAE THROUGH EQUIVALENCE    CAS18140
301 VOLUME(IY)=AREAE*SXGIX          CAS18150

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DS=DN
DN=EMUN(IY)*AREAN+RDYV(IYP1)
DE=EMUE(IY)*AREAE+RDXGI1
DW=EMUW(IY)*AREAW+RDXGIX
CS=CN
VN=V(IV)+(V(INV)-V(IV))*FV(IYP1)
CN=RHON(IY)*VN*AREAN
FCS=(1.-FV(IY))*CS
FCN=FV(IYP1)*CN
HCE=0.25*RHOE(IY)*(U(I)+U(IN))*AREAE
HCW=0.25*RHOW(IY)*(U(INW)+U(IW))*AREAW
CE=HCE+HCE
CW=HCW+HCW
----- CALCULATE ERROR SOURCE OF MASS
ESMASS=CS-CN+CW-CE
FM=AMAX1(0.0,-ESMASS)
----- COMBINING DIFFUSION AND CONVECTION CONTRIBUTIONS
AN(IY)=CONDIF(DN,-FCN,-CN)
AS(IY)=CONDIF(DS,FCS,CS)
AE(IY)=CONDIF(DE,-HCE,-CE)
AW(IY)=CONDIF(DW,HCW,CW)
----- SOURCE TERMS
DV(IY)=VOLUME(IY)-RSYV(IY)
SU(IY)=FM*V(IV)+DV(IY)*(P(IP)-P(INP))
SP(IY)=-FM
GO TO NCOTO, (37,38)
37 STERM=0.0
IF(KRAD.EQ.2) STERM=STERM-0.5*(EMUN(IY)+EMUS(IY))*V(IV)/RV(IY)**2
GO TO 313
38 DUDYE=(U(IN)-U(I))*RSYV(IY)
DUDYW=(U(INW)-U(IW))*RSYV(IY)
STERM=(EMUE(IY)+DUDYE-EMUW(IY)+DUDYW)*RSXGIX
DVDYN=(V(INV)-V(IV))*RDYV(IYP1)
DVDYS=(V(IV)-V(ISV))*RDYV(IY)
GO TO LV2,(311,312)
311 STERM=STERM+(EMUN(IY)+DVDYN-EMUS(IY)+DVDYS)/AREAE
GO TO 313
312 STERM=STERM+(EMUN(IY)*R(IYP1)+DVDYN-EMUS(IY)*R(IY)+DVDYS)/AREAE
STERM=STERM-(EMUN(IY)+EMUS(IY))*V(IV)/RV(IY)**2
313 SU(IY)=SU(IY)+STERM*VOLUME(IY)
----- STORE V IN PHIOLD
PHIOLD(IY)=V(IV)
36 CONTINUE
----- PUT BOUNDARY END VALUES IN PHIOLD
IV1=NODEF1+IX1NY1
PHIOLD(NODEF1)=V(IV1)
IV=NODEL+1+IX1NY1
PHIOLD(NODEL)=V(IV)
----- ADDITIONAL SOURCE TERMS IF REQUIRED
IF(KADSOR(JV).NE.0) CALL SOURCE(JV)
RETURN
CHAPTER 4 4 4 4 COEFFICIENTS FOR PRESSURE-CORRECTION EQUATION
----- FOR Y-DIRECTION TDMA TRAVERSES
40 SXGIX= SXG(IX)
DO 46 IY=NODEF,NODEL

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CAS18680
CAS18690
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I=IY+IX1NY
IW=I-NY
IV=IY+IX1NY1
ISV=IV-1
ARHON= SXGIX * RHON(IY)
ARHOS= SYGIX * RHOS(IY)
APHOE= SYG(IY) * RHOE(IY)
ARHOW= SYG(IY) * RHOW(IY)
IYM1=IY-1
GO TO LP,(401,402)
402 ARHON= ARHON * RV(IY)
ARHOS= ARHOS * RV(IYM1)
APHOE= ARHOE * R(IY)
ARHOW= ARHOW * R(IY)
401 AN(IY)= ARHON * DV(IY)
AS(IY)= ARHOS * DV(IYM1)
AE(IY)= ARHOE * DU(IY)
AW(IY)= ARHOW * DUW(IY)
C----- CALCULATE ERROR SOURCE OF MASS
ESMASS= -ARHON * V(IY) + ARHOS * V(ISV) - ARHOE * U(I) + ARHOW * U(IW)
RSLINE(IX,JPP)= RSLINE(IX,JPP) + ESMASS
C----- SOURCE TERMS
SU(IY)= ESMASS
SP(IY)= 0.0
C----- SET PHIOLD TO ZERO
PHIOLD(IY)= 0.0
46 CONTINUE
C----- PUT BOUNDARY END VALUES IN PHIOLD
PHIOLD(NODEF1)= 0.0
PHIOLD(NODLP1)= 0.0
C----- ADDITIONAL SOURCE TERMS IF REQUIRED
IF(KADSOR(JPP).NE.0) CALL SOURCE(JPP)
RETURN
CHAPTER 5 5 5 5 5 PHI EQUATION 5 5 5 5 5 5 5 5 5 5
50 RPRT= 1./PRT(JPHI)
C----- COEFFICIENTS FOR ALL CELLS ON THE STRIP
ICNST= IXNY(JPHI) + IZERO(JPHI)
IEWPHI= IEW(JPHI)
DO 56 IY= NODEF, NODEL
I= IY + 1 * ICNST
IE= I + IEWPHI
IW= I - IEWPHI
DS= DIFS(IY) * RPRT
DN= DIFN(IY) * RPRT
DE= DIFE(IY) * RPRT
DW= DIFW(IY) * RPRT
C----- ERROR SOURCE OF MASS
FM= ESMPhi(IY)
C----- COMBINING DIFFUSION AND CONVECTION CONTRIBUTIONS
AN(IY)= CONDIF(DN, -HCONN(IY), -CONN(IY))
AS(IY)= CONDIF(DS, HCONS(IY), CONS(IY))
AE(IY)= CONDIF(DE, -HCONE(IY), -CONE(IY))
AW(IY)= CONDIF(DW, HCONW(IY), CONW(IY))
PHIOLD(IY)= F(I)
C----- STORING PHI IN PHIOLD

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CAS19250

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C-----	SOURCE TERMS	CAS19260
	SU(IY)=FM*PHIOLD(IY)	CAS19270
	SP(IY)=-FM	CAS19280
56	CONTINUE	CAS19290
C-----	PUT BOUNDARY END VALUES IN PHIOLD	CAS19300
	I1=NODEF-1+ICONST	CAS19310
	IL=NODEL+1+ICONST	CAS19320
	PHIOLD(NODEF1)=F(I1)	CAS19330
	PHIOLD(NODLP1)=F(IL)	CAS19340
C-----	ADDITIONAL SOURCE TERMS IF REQUIRED	CAS19350
	IF(KADSOR(JPHI).NE.0) CALL SOURCE(JPHI)	CAS19360
	RETURN	CAS19370
	END	CAS19380
	SUBROUTINE CELPHI(JCELL,LPHI)	CAS19390
	COMMON	CAS19400
	1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL	CAS19410
	2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)	CAS19420
	2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)	CAS19430
	3/DNYGNX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)	CAS19440
	3, DIFN(22), DUX(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)	CAS19450
	3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)	CAS19460
	3, PHIOLD(22), RHDF(22), RHDN(22), RHOW(22), SP(22), SU(22)	CAS19470
	3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22)	CAS19480
	4/DNX/ DXG(22), DXJ(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)	CAS19490
	4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)	CAS19500
	5/DUPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)	CAS19510
	5, JGPOUP(10), KADSOR(10), KCOLVE(10), KRS(10), RELAX(10), RSREF(10)	CAS19520
	5, PSSUM(10), ITITLE(10)	CAS19530
	COMMON	CAS19540
	6/DO/CHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT	CAS19550
	6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF	CAS19560
	6, JEMJ, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO	CAS19570
	6, JU, JV, JVP1, KINPR1, KMPA, KRAD, KRHOMU, KTEST, LABPHI	CAS19580
	6, LASTEP, LINEF, LINEL, NEO, NEOP1	CAS19590
	6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL	CAS19600
	6, NX, NXMAX, NXM1, NXY2, NXYG, NXYP, NXYU, NXYV	CAS19610
	6, NY, NYMAX, NYM1, NYM2, PI, RSCHK, RSMAX, TINY	CAS19620
	COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF	CAS19630
	COMMON/D2D1/ARSL(22,10), RSLINE(22,10)	CAS19640
	COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)	CAS19650
	7, RHO(484), EMU(484)	CAS19660
	7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH	CAS19670
	COMMON	CAS19680
	9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)	CAS19690
	9, TAUTW2(22), YPUST1(22), YPUST2(22)	CAS19700
	9, TAULW(22), XPUSLW(22), CTAULW, CXPLW	CAS19710
	9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA	CAS19720
	9, INLY1, INLY2, IOUT1, IOUT2, I1M1, I2P1, I3M1, I4P1	CAS19730
	COMMON/ABC/AREAE	CAS19740
	DIMENSION F(3766)	CAS19750
	DIMENSION DIFS(22), EMUS(22), HCONS(22), RHDS(22)	CAS19760
	EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))	CAS19770
	EQUIVALENCE (JS(2), RHON(1)), (AREAE, AREAW)	CAS19780
	EQUIVALENCE (HCONS(2), HCDNN(1))	CAS19790
	EQUIVALENCE (F(1), U(1))	CAS19800

DIMENSION A(22),B(22)	CAS19810
EQUIVALENCE(A(1),AN(1)),(B(1),AS(1))	CAS19820
JPHI=LPHI	CAS19830
IF(JCELL.EQ.JU) GO TO 10	CAS19840
IF(JCELL.EQ.JV) GO TO 20	CAS19850
GO TO 30	CAS19860
C----- CELL-WALL PROPERTIES FOR U-CELLS	CAS19870
10 CONTINUE	CAS19880
COMMENT...AE,AW,AN,AS ARE USED AS TEMPORARY STORAGES, VALUES THERE	CAS19890
COMMENT...SHOULD BE APPROPRIATELY TRANSFERRED IN THE CALLING SUBROUTINE	CAS19900
C----- INDICES TO ACCOUNT FOR EFFECTS OF ENDS	CAS19910
C----- BOUNDARIES (EAST AND WEST)	CAS19920
LE=0	CAS19930
LW=0	CAS19940
IF(IX.EQ.2) LW=NY	CAS19950
IF(IX.EQ.NXM2) LE=NY	CAS19960
C----- EAST AND WEST WALLS	CAS19970
ICONST=IX1NY+IZERO(JPHI)-LW	CAS19980
NYLE=NY+LE	CAS19990
DO 11 IY=NODEF,NODEL	CAS20000
I=IY-ICONST	CAS20010
IE=I+NYLE	CAS20020
AW(IY)=F(I)	CAS20030
11 AE(IY)=F(IE)	CAS20040
C----- NORTH AND SOUTH WALLS	CAS20050
I=NODEF1+ICONST	CAS20060
IE=I+NYLE	CAS20070
AS(NODEF)=0.5*(F(I)+F(IE))	CAS20080
IF(NODEF.GT.2) AS(NODEF)=0.25*(AE(NODEF)+AW(NODEF))+0.5*AS(NODEF)	CAS20090
DO 12 IY=NODEF,NODEL1	CAS20100
IYP1=IY+1	CAS20110
AN(IY)=0.25*(AE(IY)+AW(IY)+AE(IYP1)+AW(IYP1))	CAS20120
C----- AN FOR LAST CELL	CAS20130
IN=NODEL+1+ICONST	CAS20140
INE=IN+NYLE	CAS20150
AN(NODEL)=0.5*(F(IN)+F(INE))	CAS20160
IF(NODEL.LT.NYM1) AN(NODEL)=0.25*(F(IN-1)+F(INE-1))+0.5*AN(NODEL)	CAS20170
RETURN	CAS20180
C----- CELL-WALL PROPERTIES FOR V-CELLS	CAS20190
20 CONTINUE	CAS20200
COMMENT...AE,AW,AN,AS ARE USED AS TEMPORARY STORAGES, VALUES THERE	CAS20210
COMMENT...SHOULD BE APPROPRIATELY TRANSFERRED IN THE CALLING SUBROUTINE	CAS20220
C----- FACTORS TO ACCOUNT FOR EFFECTS OF END	CAS20230
C----- BOUNDARIES (EAST AND WEST)	CAS20240
BWW=0.25	CAS20250
BEW=0.25	CAS20260
IF(IX.EQ.2) BWW=0.5	CAS20270
IF(IX.EQ.NXM1) BEW=0.0	CAS20280
BWE=0.5-BWW	CAS20290
BEE=0.5-BEW	CAS20300
C----- EAST AND WEST WALLS	CAS20310
ICONST=IX1NY+IZERO(JPHI)	CAS20320
DO 21 IY=NODEF,NODEL1	CAS20330
I=IY+ICONST	CAS20340
IN=I+1	CAS20350

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IW=I-NY
INW=IW+1
IE=I+NY
INE=IE+1
FPN=F(I)+F(IN)
AW(IY)=BWW*(F(IW)+F(INW))+BWE*FPN
21 AE(IY)=BEW*FPN+BEE*(F(IE)+F(INE))
C----- NORTH AND SOUTH WALLS
I=NODEF1+ICONST
AS(NODEF)=F(I)
IF(NODEF.GT.2) AS(NODEF)=F(I+1)
N2=NODEL1-1
ICONST=1+IX1NY+IZERO(JPHI)
DO 22 IY=NODEF,N2
IN=IY+ICONST
22 AN(IY)=F(IN)
C----- AN FOR LAST CELL
INN=NODEL+ICONST
AN(NODEL1)=F(INN)
IF(NODEL1.LT.NYM2) AN(NODEL1)=F(INN-1)
RETURN
C----- CELL-WALL PROPERTIES FOR G-CELL
30 CONTINUE
COMMENT...AE,AW,AN,AS ARE USED AS TEMPORARY STORAGES, VALUES THERE
COMMENT...SHOULD BE APPROPRIATELY TRANSFERRED IN THE CALLING SUBROUTINE
C----- FACTORS TO ACCOUNT FOR EFFECTS OF END
C----- BOUNDARIES (EAST AND WEST)
BWW=0.5
BEW=0.5
IF(IX.EQ.2) BWW=1.
IF(IX.EQ.NXM1) BEW=0.
BWE=1.-BWW
BEE=1.-BEW
C----- ALL FOUR CELL WALLS
ICONST=IX1NY+IZERO(JPHI)
I=NODEF1+ICONST
AS(NODEF)=F(I)
IF(NODEF.GT.2) AS(NODEF)=0.5*(F(I)+F(I+1))
DO 31 IY=NODEF,NODEL
J=IY+ICONST
IN=I+1
IE=I+NY
IW=I-NY
AN(IY)=0.5*(F(I)+F(IN))
AW(IY)=BWW*F(IW)+BWE*F(I)
31 AE(IY)=BEW*F(I)+BEE*F(IE)
IF(NODEL.LT.NYM1) RETURN
C----- CORRECT AN FOR THE LAST CELL
IN=NODEL+ICONST
AN(NODEL)=F(IN)
RETURN
END
SUBROUTINE SOLVE(LPHI)
COMMON
1/CASE1/UIINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL

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CAS20360
CAS20370
CAS20380
CAS20390
CAS20400
CAS20410
CAS20420
CAS20430
CAS20440
CAS20450
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CAS20490
CAS20500
CAS20510
CAS20520
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CAS20680
CAS20690
CAS20700
CAS20710
CAS20720
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CAS20800
CAS20810
CAS20820
CAS20830
CAS20840
CAS20850
CAS20860
CAS20870
CAS20880
CAS20890
CAS20900

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2/DNY/ DYG(22),DYV(22),FV(22),FVNODE(22),R(22),RDYG(22),RDYV(22) CAS20910
2,RSYG(22),RSYV(22),RV(22),RVCB(22),SYG(22),SYV(22),Y(22),YV(22) CAS20920
3/DNYONX/AE(22),AN(22),AP(22),AS(22),AW(22),C(22),D(22),DIFE(22) CAS20930
3,DIFN(22),DUW(22),DIFW(22),DU(22),DV(22),EMUE(22),EMUN(22) CAS20940
3,EMUW(22),HCONE(22),HCONN(22),HCONW(22) CAS20950
3,PHIOLD(22),RHOE(22),RHON(22),RHOW(22),SP(22),SU(22) CAS20960
3,VOLUME(22),CONN(22),CONS(22),CONE(22),CONW(22),ESMPHI(22) CAS20970
4/DNX/ DXG(22),DXU(22),FU(22),FUNODE(22),KOUNT(22),RDXG(22) CAS20980
4,RDXU(22),RSXG(22),RSXU(22),STORE(22),SXG(22),SXU(22),X(22),XU(22) CAS20990
5/DUPHI/ IEW(10),ILAST(10),IMON(10),IXNY(10),IZERO(10) CAS21000
5,JGROUP(10),KADSOR(10),KSOLVE(10),KRS(10),RELAX(10),RSREF(10) CAS21010
5,PSSUM(10),ITITLE(10) CAS21020
COMMON CAS21030
6/DO/CHECK,DP,FLOWPC,FLOWST,FLOWUP,GREAT,ILINE,IPLRS,IPREF,IPRINT CAS21040
6,ISTEP,IX,IXINY,IX1NY1,IX2NY2,IXMON,IXP1,IXPREF,IYMON,IYPREF CAS21050
6,JEMU,JH,JLAST,JLIM1,JLIM2,JLIM3,JLIM4,JP,JPP,JRHO CAS21060
6,JU,JV,JVP1,KINPRI,KMPA,KRAD,KRHOMU,KTEST,LABPHI CAS21070
6,LASTEP,LINEL,LINEL,NEO,NEQP1 CAS21080
6,NODEF,NODEF1,NODEL,NODEL1,NODLP1,NTDMA,NUMCOL CAS21090
6,NX,NXMAX,NXM1,NX2,NXYG,NXYP,NXYU,NXYV CAS21100
6,NY,NYMAX,NYM1,NYM2,PI,RSCHK,RSMAK,TINY CAS21110
COMMON/PROP/EMUREF,PRL(10),PRT(10),RHOREF CAS21120
COMMON/D2D1/ARSL(22,10),RSLINE(22,10) CAS21130
COMMON/D2D2/U(462),V(462),TKE(484),TED(484),H(484),PP(22),P(400) CAS21140
7,FHD(454),EMU(484) CAS21150
7,INLY(10),IOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH CAS21160
COMMON CAS21170
9/TURB/C1,C2,CD,SOFTCD,CD25,ECONST,CTAUTW,CYPTW,TAUTW1(22) CAS21180
9,TAUTW2(22),YFUST1(22),YPUST2(22) CAS21190
9,TAULW(22),XPUSSLW(22),CTAULW,CXPLW CAS21200
9,GENK(22),FACTKE,FACTED,JTKE,JTED,CAPPA CAS21210
9,INLY1,INLY2,IOUT1,IOUT2,I1M1,I2P1,I3M1,I4P1 CAS21220
COMMON/ABC/AREAE CAS21230
DIMENSION F(3756) CAS21240
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22) CAS21250
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1)) CAS21260
EQUIVALENCE (RHOS(2),RHON(1)), (AREAE,AREAW) CAS21270
EQUIVALENCE (HCONS(2),HCONN(1)) CAS21280
EQUIVALENCE (F(1),U(1)) CAS21290
DIMENSION A(22),B(22) CAS21300
EQUIVALENCE (A(1),AN(1)), (B(1),AS(1)) CAS21310
COMMENT..... A AND B HAVE BEEN MADE EQUIVALENT TO AN, AS RESPECTIVELY CAS21320
JPHI=LPHI CAS21330
RRELAX=1./RELAX(JPHI) CAS21340
RELAX1=1.-RELAX(JPHI) CAS21350
KRSPHI=KRS(JPHI) CAS21360
ICNST=IXNY(JPHI)+IZERO(JPHI) CAS21370
IEWPHI=IEW(JPHI) CAS21380
NCDE2=NODEL CAS21390
IF(JPHI.EQ.JV) NODE2=NODEL1 CAS21400
NF2=NODEF+NODE2 CAS21410
A(NODEF1)=0.0 CAS21420
C(NODEF1)=PHIOLD(NODEF1) CAS21430
C----- FOR Y-DIRECTION TDMA TRAVERSES CAS21440
IF(JPHI.NE.JPP) GO TO 12 CAS21450

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C----- FOR P' EQUATION ONLY
DO 11 IY=NODEF,NODE2
IYM1=IY-1
D(IY)=AE(IY)+AW(IY)+AN(IY)+AS(IY)-SP(IY)+TINY
C(IY)=SU(IY)
TERM=1./(D(IY)-B(IY)*A(IYM1))
A(IY)=A(IY)*TERM
11 C(IY)=(C(IY)+C(IYM1)*B(IY))*TERM
C----- BACK SUBSTITUTION FOR P'
DO 111 IY=NODEF,NODE2
IYBACK=NF2-IY
PHIOLD(IYBACK)=A(IYBACK)+PHIOLD(IYBACK+1)+C(IYBACK)
111 PP(IYBACK)=PHIOLD(IYBACK)
RETURN
12 IF(RELAX(JPHI).EQ.1.) GO TO 13
C----- FOR PHI WITH RELAX. FACTOR .NE. 1
DO 14 IY=NODEF,NODE2
IYM1=IY-1
I=IY+ICONST
IE=I+IEWPHI
IW=I-IEWPHI
AP(IY)=AN(IY)+AS(IY)+AE(IY)+AW(IY)
SU(IY)=SU(IY)+AE(IY)*F(IE)+AW(IY)*F(IW)
C----- STORE AN IN STORE FOR RESIDUAL-SOURCE CAL.
STORE(IY)=AN(IY)
C----- INCLUDE RELAXATION FACTOR IN TDMA COEFFICIENTS
D(IY)=(AP(IY)-SP(IY))*RRELAX+TINY
C(IY)=SU(IY)+RELAX1*D(IY)*PHIOLD(IY)
C----- MODIFY TDMA COEFFICIENTS FOR BACK SUBSTITUTION
TERM=1./(D(IY)-B(IY)*A(IYM1))
A(IY)=A(IY)*TERM
14 C(IY)=(C(IY)+C(IYM1)*B(IY))*TERM
GO TO 110
C----- FOR PHI --- NO RELAXATION
13 DO 18 IY=NODEF,NODE2
IYM1=IY-1
I=IY+ICONST
IE=I+IEWPHI
IW=I-IEWPHI
AP(IY)=AN(IY)+AS(IY)+AE(IY)+AW(IY)
SU(IY)=SU(IY)+AE(IY)*F(IE)+AW(IY)*F(IW)
C----- STORE AN IN STORE FOR RESIDUAL-SOURCE CAL.
STORE(IY)=AN(IY)
D(IY)=AP(IY)-SP(IY)+TINY
C(IY)=SU(IY)
C----- MODIFY TDMA COEFFS. FOR BACK SUBSTITUTION
TERM=1./(D(IY)-B(IY)*A(IYM1))
A(IY)=A(IY)*TERM
18 C(IY)=(C(IY)+C(IYM1)*B(IY))*TERM
110 IF(KRSPHI.EQ.0) GO TO 120
C----- RESIDUAL-SOURCE CALCULATIONS
DO 115 IY=NODEF,NODE2
IF(SP(IY).LE.-1.E20) GO TO 115
RS=(AP(IY)-SP(IY))*PHIOLD(IY)-SU(IY)
1 -STORE(IY)*PHIOLD(IY+1)-AS(IY)*PHIOLD(IY-1)

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CAS21460
CAS21470
CAS21480
CAS21490
CAS21500
CAS21510
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CAS21930
CAS21940
CAS21950
CAS21960
CAS21970
CAS21980
CAS21990
CAS22000

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115 RSLINE(IX,JPHI)=RSLINE(IX,JPHI)+RS CAS22010
C----- BACK SUBSTITUTION IN TDMA OPERATIONS CAS22020
120 DO 100 IY=NODEF,NODE2 CAS22030
    IYBACK=NF2-IY CAS22040
    PHIOLD(IYBACK)=A(IYBACK)*PHIOLD(IYBACK+1)+C(IYBACK) CAS22050
    I=IYBACK+ICONST CAS22060
100 F(I)=PHIOLD(IYBACK) CAS22070
C----- MODIFY DU AND DV FOR NON-UNITY D(IY) CAS22080
    IF(JPHI.NE.JU) GO TO 102 CAS22090
    DO 103 IY=NODEF,NODE2 CAS22100
103 DU(IY)=DU(IY)/D(IY) CAS22110
    RETURN CAS22120
102 IF(JPHI.NE.JV) RETURN CAS22130
    DO 106 IY=NODEF,NODE2 CAS22140
106 DV(IY)=DV(IY)/D(IY) CAS22150
    RETURN CAS22160
    END CAS22170
    SUBROUTINE PRINT(LPHI) CAS22180
    COMMON CAS22190
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL CAS22200
2/DNY/ OYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22) CAS22210
2.RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22) CAS22220
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22) CAS22230
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22) CAS22240
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22) CAS22250
3, PHIOLD(22), RHDE(22), RHON(22), RHOW(22), SP(22), SU(22) CAS22260
3, VOLUME(22), CONN(22), CONE(22), CONW(22), ESMPHI(22) CAS22270
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22) CAS22280
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22) CAS22290
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10) CAS22300
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10) CAS22310
5, RSSUM(10), ITITLE(10) CAS22320
    COMMON CAS22330
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT CAS22340
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF CAS22350
6, JEMU, JH, JLAST, JLIN1, JLIN2, JLIN3, JLIN4, JP, JPP, JRHO CAS22360
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI CAS22370
6, LASTEP, LINEF, LINEL, NEO, NEOP1 CAS22380
6, NODEF, NODEF1, NODEL, NODEL1, MODLP1, NTDMA, NUMCOL CAS22390
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV CAS22400
6, NY, NYMAX, NYM1, NYM2, PI, RSCHK, RSMAX, TINY CAS22410
    COMMON/PROP/ EMUREF, PRL(10), PRT(10), RHOREF CAS22420
    COMMON/D2D1/ AFSL(22,10), RSLINE(22,10) CAS22430
    COMMON/D2D2/ U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400) CAS22440
7, RHU(484), EMU(484) CAS22450
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH CAS22460
    COMMON CAS22470
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTWI(22) CAS22480
9, TAUTW2(22), YPUST1(22), YPUST2(22) CAS22490
9, TAULW(22), XPUELW(22), CTAULW, CXPLW CAS22500
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA CAS22510
9, INLY1, INLY2, IOUT1, IOUT2, I1M1, I2P1, I3M1, I4P1 CAS22520
    COMMON/ABC/AREAE CAS22530
    DIMENSION F(3766) CAS22540
    DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22) CAS22550

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310 WRITE(6,3100) IY,Y(IY),(STORE(IX),IX=LIMIT1,LIMIT2)          CAS23110
GO TO 39                                                         CAS23120
311 WRITE(6,3101) IY,YV(IY),(STORE(IX),IX=LIMIT1,LIMIT2)      CAS23130
39 CONTINUE                                                     CAS23140
IF(JPHI-JU) 320,321,320                                         CAS23150
320 WRITE(6,3102) (IX,X(IX),IX=LIMIT1,LIMIT2)                  CAS23160
GO TO 360                                                         CAS23170
321 WRITE(6,3103) (IX,XU(IX),IX=LIMIT1,LIMIT2)                 CAS23180
360 IF(JPHI.EQ.JU) GO TO 350                                     CAS23190
IF(JPHI.EQ.JP) GO TO 350                                        CAS23200
C----- FOR ALL PHI'S OTHER THAN U AND P                       CAS23210
IF(LIMIT2.EQ.NX) RETURN                                         CAS23220
KOLUM1=KOLUM1+NUMCOL                                           CAS23230
KOLUM2=KOLUM2+NUMCOL                                           CAS23240
GO TO 10                                                         CAS23250
C----- FOR U AND P                                           CAS23260
350 IF(LIMIT2.EQ.NXM1) RETURN                                    CAS23270
KOLUM1=KOLUM1+NUMCOL                                           CAS23280
KOLUM2=KOLUM2+NUMCOL                                           CAS23290
IF(JPHI.EQ.JU) GO TO 10                                         CAS23300
GO TO 13                                                         CAS23310
3100 FORMAT(1X,1X,2HY(.12,2H)=,1PE9.3,2X,10(1PE9.2,1X))      CAS23320
3101 FORMAT(1X,3HYV(.12,2H)=,1PE9.3,2X,10(1PE9.2,1X))        CAS23330
3102 FORMAT(/5X,5HX(1X), 9X,10(12,1H=,F6.2,1X)//)            CAS23340
3103 FORMAT(/5X,5HXU(1X), 8X,10(12,1H=,F6.2,1X)//)            CAS23350
9999 FORMAT(/1X,5GH( 1 = U, 2 = V, 3 = H, 4 = PP, 5 = P, 6 = RHO, 7 = E
1MU ))                                                         CAS23360
RETURN                                                         CAS23370
END                                                             CAS23380
SUBROUTINE TEST                                               CAS23390
COMMON                                                         CAS23400
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL    CAS23410
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22) CAS23420
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22) CAS23430
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22) CAS23440
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22) CAS23450
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22) CAS23460
3, PHIOLD(22), RHOE(22), RHOH(22), RHOW(22), SP(22), SU(22) CAS23470
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPhi(22) CAS23480
4/DNX/ DNG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22) CAS23490
4, SDXU(22), RSYG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22) CAS23500
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10) CAS23510
5, JGROUP(10), KAUSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10) CAS23520
5, RSSUM(10), ITITLE(10) CAS23530
COMMON                                                         CAS23540
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT CAS23550
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF CAS23560
6, JMU, JM, JLAST, JLIN1, JLIN2, JLIN3, JLIN4, JP, JPP, JRHO CAS23570
6, JU, JV, JVF1, KINPRI, KMPA, KRAD, KRHOWU, KTEST, LABPHI CAS23580
6, LASTEP, LINEF, LINEL, NEO, NEOP1 CAS23590
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL CAS23600
6, NX, NXMAX, NXM1, NXM2, NXYG, NXP, NXYU, NXYV CAS23610
6, NY, NYMAX, NYM1, NYM2, P1, RSCHEK, RSMAX, TINY CAS23620
COMMON/PROP/EMUREF, PRL(10), PRT(10), RMDREF CAS23630
COMMON/D2D1/ARSL(22,10), RSLINE(22,10) CAS23640

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COMMON/D2D2/U(462),V(462),TKE(484),TED(484),H(484),PP(22),P(400) CAS23660
7,RHD(484),EMU(484) CAS23670
7,INLY(10),IOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH CAS23680
COMMON CAS23690
9/TURB/C1,C2,CD,SQRTCD,CD25,ECONST,CTAUTW,CYPTW,TAUTW1(22) CAS23700
9,TAUTW2(22),YPOST1(22),YPOST2(22) CAS23710
9,TAULW(22),XPLSLW(22),CTAULW,CXPWL CAS23720
9,GENK(22),FACTKE,FACTED,JTKE,JTED,CAPPA CAS23730
9,INLY1,INLY2,IOUT1,IOUT2,I1M1,I2P1,I3M1,I4P1 CAS23740
COMMON/ABC/AREAE CAS23750
DIMENSION F(3766) CAS23760
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22) CAS23770
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1)) CAS23780
EQUIVALENCE (RHOS(2),RHON(1)), (AREAE,AREAW) CAS23790
EQUIVALENCE (HCONS(2),HCONN(1)) CAS23800
EQUIVALENCE (F(1),U(1)) CAS23810
DIMENSION A(22),S(22) CAS23820
EQUIVALENCE (A(1),AN(1)), (B(1),AS(1)) CAS23830
CHAPTER 1 1 1 1 PRINT-OUT FOR LEVEL 1 ONWARDS 1 1 1 1 1 CAS23840
C----- GEOMETRICAL QUANTITIES RELATED TO GRID CAS23850
ENTRY TEST 11 CAS23860
WRITE(6,200) KTEST CAS23870
200 FORMAT(/1X,2GHDIAGNOSING PRINT-OUT LEVEL,14,2X,30(1H-)) CAS23880
WRITE(6,201) (K,X(K),DXG(K),SXG(K),K=1,NX) CAS23890
201 FORMAT(/1X,2HIX,1X,10H X,10H DXG,10H SXG/ CAS23900
1(1X,12,1X,1P3E10.2)) CAS23910
WRITE(6,202) (K,XU(K),DXU(K),SXU(K),FU(K),FUNODE(K),K=1,NX) CAS23920
202 FORMAT(/1X,2HIX,1X,10H XU,10H DXU,10H SXU, CAS23930
1 10H FU,10H FUNODE/(1X,12,1X,1P5E10.2)) CAS23940
WRITE(6,203) (K,Y(K),R(K),DYG(K),SYG(K),K=1,NY) CAS23950
203 FORMAT(/1X,2HIY,1X,10H Y,10H R,10H DYG, CAS23960
1 10H SYG/(1X,12,1X,1P4E10.2)) CAS23970
WRITE(6,204) (K,YV(K),RV(K),RVCB(K),DYV(K),SYV(K),FV(K), CAS23980
1 FVNODE(K),K=1,NY) CAS23990
204 FORMAT(/1X,2HIY,1X,10H YV,10H RV,10H RVCB, CAS24000
1 10H DYV,10H SYV,10H FV,10H FVNODE/ CAS24010
2(1X,12,1X,1P7E10.2)) CAS24020
RETURN CAS24030
C----- VARIABLE INFORMATION CAS24040
ENTRY TEST12 CAS24050
WRITE(6,300) CAS24060
300 FORMAT(/1X,30HDEPENDENT VARIABLE INFORMATION,20(1H-)/) CAS24070
WRITE(6,9999) CAS24080
301 WRITE(6,301) NEQ.(ITITLE(K),K=1,NEQ) CAS24090
FORMAT(/1X,4HNEQ=,14,1X,5(1H-),20(14,1H,,1X)) CAS24100
IF(KSOLVE(JPP).EQ.0) GO TO 38 CAS24110
WRITE(6,302) CAS24120
302 FORMAT(1X,14X,44HPRESSURE CORRECTION EQUATION IS ALSO SOLVED.) CAS24130
38 WRITE(6,303) CAS24140
303 FORMAT(/1X,4H J .4HJPHI,6H JGROUP,8H KSOLVE,8H KADSOR, CAS24150
1 8H KRS,8H RELAX,8H IZERO,8H ILAST,8H IEW) CAS24160
WRITE(6,304) (K,ITITLE(K),JGROUP(K),KSOLVE(K),KADSOR(K), CAS24170
1 KRS(K),RELAX(K),IZERO(K),ILAST(K),IEW(K),K=1,JLAST) CAS24180
304 FORMAT(1X,12,2X,14,4I8,F9.2,3I8) CAS24190
WRITE(6,305) JLIM1,JLIM2,JLIMS,JLIM4 CAS24200

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305  FORMAT(/1X,8H  JLIM1,8H  JLIM2,8H  JLIM3,8H  JLIM4/1X,4I8)  CAS24210
9999  FORMAT(/1X,56H( 1 = U, 2 = V, 3 = H, 4 = PP, 5 = P, 6 = RHO, 7 = E
1MU )/)  CAS24220
      RETURN  CAS24230
      CAS24240
C----- INITIAL VALUES IN FIELD  CAS24250
      ENTRY TEST 13  CAS24260
      J1=1  CAS24270
      IF(KINPRI.GT.0) J1=JP  CAS24280
      DO 521 JPHI=J1,ULAST  CAS24290
      IF(JPHI.EQ.JPP) GO TO 521  CAS24300
      CALL PRINT(JPHI)  CAS24310
521  CONTINUE  CAS24320
      RETURN  CAS24330
CHAPTER 2  2  2  2  2  PRINT-OUTS FOR LEVEL 2 ONWARDS  2  2  2  CAS24340
C----- STARRED VELOCITIES AND THEIR RESIDUAL SOURCES ON TDMA LINE  CAS24350
      ENTRY TEST 21  CAS24360
      IF(KTEST.GT.2) GO TO 804  CAS24370
      IF(LABPHI.EQ.1) WRITE(6,803) IX,KOUNT(IX)  CAS24380
      IF(LABPHI.EQ.2.AND.IX.EQ.NXM1) WRITE(6,803) IX,KOUNT(IX)  CAS24390
803  FORMAT(/1X,53(1H-),4H IX=,I2,12H, KOUNT(IX)=,I3)  CAS24400
804  ISYMBL=1  CAS24410
      IF(LABPHI.GT.JV) ISYMBL=0  CAS24420
      K2=1EW(LABPHI)  CAS24430
      WRITE(6,9999)  CAS24440
      WRITE(6,800) IX,ISYMBL,ITITLE(LABPHI),(PHIOLD(K),K=1,K2)  CAS24450
800  FORMAT(/1X,3HIX=,I2,1H,,1X,I1,11H VALUES OF ,I4,1H*,1P5E10.2,
1 5(/1X,24X,1P5E10.2))  CAS24470
      WRITE(6,801) ITITLE(LABPHI),IX,RSLINE(IX,LABPHI)  CAS24480
801  FORMAT(1X,38HALGEBRAIC SUM OF RESIDUAL SOURCES OF ,I4,6HAT IX=,
1 12,4H 1S,10X,1P5E10.2)  CAS24490
9998  FORMAT(/1X,56H( 1 = U, 2 = V, 3 = H, 4 = PP, 5 = P, 6 = RHO, 7 = E
1MU )/)  CAS24510
      RETURN  CAS24520
      CAS24530
C----- MEAN-PRESSURE-CORRECTION QUANTITIES  CAS24540
      ENTRY TEST 22  CAS24550
      WRITE(6,1090) IX,FLOWUP,FLOWST,DP  CAS24560
1080  FORMAT(/1X,3HIX=,I2,5H.....7HFLOWUP,,7HFLOWST,,20HMEAN-P CORRECTI
1DN =,1P3E10.2)  CAS24580
      WRITE(6,1082) FLOWPC  CAS24590
1082  FORMAT(1X,36HMEAN-PRESSURE CORRECTED FLOW RATE = ,8X,1P5E10.2)  CAS24600
      K1=1+IX1NY  CAS24610
      K2=K1+NYM1  CAS24620
      WRITE(6,1081) (U(K),K=K1,K2)  CAS24630
1081  FORMAT(1X,24HMEAN-PRESS. C. U(1 - NY),1P5E10.2,
1 5(/1X,24X,1P5E10.2))  CAS24650
      RETURN  CAS24660
C----- P'-CORRECTION QUANTITIES  CAS24670
      ENTRY TEST 23  CAS24680
      WRITE(6,1093) IX,RSLINE(IX,JPP)  CAS24690
1093  FORMAT(/1X,42HALGEBRAIC SUM OF ERROR MASS SOURCES AT IX=,I3,
1 5H 1S,14X,1P5E10.2)  CAS24710
      WRITE(6,1090) IX,(PP(K),K=1,NY)  CAS24720
1090  FORMAT(/1X,3HIX=,I2,2X,12HPP(1 TO NY) ,5X,1P5E10.2,
1 5(/1X,24X,1P5E10.2))  CAS24730
      K1=1+IXNY(JU)  CAS24750

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	K2=K1+NYM1	CAS24760
	WRITE(6,1091) IX,(U(K),K=K1,K2)	CAS24770
1091	FORMAT(1X,3HIX=,I2,2X,17HPP C. U(1 TO NY) ,1P5E10.2,	CAS24780
	1 5(/1X,24X,1P5E10.2))	CAS24790
	K1=1+IXNY(JV)	CAS24800
	K2=K1+NYM2	CAS24810
	WRITE(6,1092) IX,(V(K),K=K1,K2)	CAS24820
1092	FORMAT(1X,3HIX=,I2,2X,17HPP C. V(1 - NYM1),1P5E10.2,	CAS24830
	1 5(/1X,24X,1P5E10.2))	CAS24840
	RETURN	CAS24850
CHAPTER 3	3 3 3 3 PRINT-CUTS FOR LEVEL 3 ONWARDS 3 3 3 3	CAS24860
C-----	COEFFICIENTS OF FINITE-DIFFERENCE EQUATIONS	CAS24870
	ENTRY TEST 31	CAS24880
	IF(LABPHI.EQ.1) WRITE(6,2030) IX,KOUNT(IX)	CAS24890
	IF(LABPHI.EQ.2.AND.IX.EQ.NXM1) WRITE(6,2030) IX,KOUNT(IX)	CAS24900
2030	FORMAT(/1X,53(1H-),4H IX=,I2,12H, KOUNT(IX)=,I3)	CAS24910
	WRITE(6,9997)	CAS24920
	WRITE(6,2020) ITITLE(LABPHI),IX	CAS24930
2020	FORMAT(/1X,15HCOEFFICIENTS OF ,I4,2X,17HEQUATION FOR IX =,I4,2X,2	CAS24940
	10(1H-)//1X,2HIY,2X,10H AN,10H AS,10H AE,	CAS24950
	11CH AW,10H SU,10H SP,10H PHIOLD)	CAS24960
	WRITE(6,2021) (K,AN(K),AS(K),AE(K),AW(K),SU(K),SP(K),PHIOLD(K),K=1	CAS24970
	1,NY)	CAS24980
2021	FORMAT(1X,I2,2X,1P7E10.2)	CAS24990
9997	FORMAT(/1X,56H( 1 = U, 2 = V, 3 = H, 4 = PP, 5 = P, 6 = RHO, 7 = E	CAS25000
	1MU )//	CAS25010
	RETURN	CAS25020
	END	CAS25030



APPENDIX B  
THE COMPUTER PROGRAM FOR PARTICLE COAGULATION

## FORTRAN SYMBOL

<u>Symbols</u>	<u>Meaning</u>
CPART1 (I) } CPART10 (I) }	The number of particles in the 1st ~ 10th class of sizes.
OCP (J,I)	The number of particles in the I-th class of sizes at the previous time step.
FF (I)	Array used to store the variables, CPART 1 (I) ~ CPART10 (I).
FFF (I)	Array used to store the variables, OCP (J,I). FF (I) and FFF (I) are made equivalent to the total length of the individual variable array.
COEN (I) } COES (I) } COEE (I) } COEW (I) }	Coefficient in the finite difference equations. These values are calculated before entering time loop.
JCP1 } JCP10 }	Index controlling the class of particle sizes.
DELT	Time interval which is used for transient finite-difference equations.
STAN1 } STAN2 } STAN3 }	Mass transference coefficient for particle deposition to the left hand side, the right side, the right hand side and the bottom wall, respectively.
XCP (I,J)	The variable which are made equivalent to the CPART 1 ~ CPART 10
MONTOR (I)	The number of grid point which is used for printing out the calculated result at every time step.
CPINP (I)	The initial value of particle numbe in I-th size class.
TIMEF	Final time step.
ACCOM	The accomodation factor for the particle coalescenc (now taken as 0.3)
ALPH (I,J,K)	The coagulation factor between the I-th and the J-th class particles at the grid point K.

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BLOCK DATA
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCS(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AX(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUW(22), HCONE(22), HCCNN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOJNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMDN(10), IXNY(10), IZERO(10)
5, JGROUP(10), KASOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)
COMMON
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPR1, KMPA, KRAD, KRROMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEO, NECP1
6, NODEF, NODEF1, NCDL1, NODL1, NODLP1, NTDMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXP, NXYU, NXYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(484)
COMMON
9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YPUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)
COMMON/PART1/CCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER
1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPH1, KKLAST, MONTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCCNS(22), RHOS(22)
EQUIVALENCE (HCCNS(2), HCCNN(1)), (FF(1), CPART1(1))
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (F(1), U(1)), (OCP(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
CHAPTER 1 ----- GENERAL FLOW PARAMETERS
DATA GREAT, TINY, PI/1.E30, 1.E-30, 3.1415926/
DATA RPIPE, XPIPE, UINLET, HINLET, HWALL/
1 250., 250., 72., 0.0, 0.0/
DATA KTEST/0/
DATA RP/0.0002, 0.0004, 0.0006, 0.0009, 0.001, 0.0012, 0.0014, 0.0016
1, 0.0018, 0.002/

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BLO00010
BLO00020
BLO00030
BLO00040
BLO00050
BLO00060
BLO00070
BLO00080
BLO00090
BLO00100
BLO00110
BLO00120
BLO00130
BLO00140
BLO00150
BLO00160
BLO00170
BLO00180
BLO00190
BLO00200
BLO00210
BLO00220
BLO00230
BLO00240
BLO00250
BLO00260
BLO00270
BLO00280
BLO00290
BLO00300
BLO00310
BLO00320
BLO00330
BLO00340
BLO00350
BLO00360
BLO00370
BLO00380
BLO00390
BLO00400
BLO00410
BLO00420
BLO00430
BLO00440
BLO00450
BLO00460
BLO00470
BLO00480
BLO00490
BLO00500
BLO00510
BLO00520
BLO00530
BLO00540
BLO00550

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CHAPTER 2 ----- GRID	BLO00560
DATA NXMAX,NYMAX/22,22/	BLO00570
DATA KRAD/1/	BLO00580
DATA FXSTEP/1.0/	BLO00590
CHAPTER 3 ----- VARIABLES	BLO00600
DATA JU, JV, JTKE, JTED, JH, JPP, JP, JRHO, JEMU, JLAST/	BLO00610
1 1, 2, 3, 4, 5, 6, 7, 8, 9, 9/	BLO00620
DATA JCP1, JCP2, JCP3, JCP4, JCP5, JCP6, JCP7, JCP8, JCP9, JCP10, KKLAST/	BLO00630
11, 2, 3, 4, 5, 6, 7, 8, 9, 10, 10/	BLO00640
DATA KSOLVE /10*1/	BLO00650
DATA KRS/10*1/	BLO00660
DATA KADSOR/10*1/	BLO00670
CHAPTER 4 ----- PROPERTY DATA	BLO00680
DATA RHOREF, EMUREF/7.2, 0.06/	BLO00690
DATA PRL.PRT/20*1.0/	BLO00700
CHAPTER 5 ----- STARTING PREPARATIONS	BLO00710
DATA IXPREF, IYPREF/2.2/	BLO00720
DATA KINPRI/0/	BLO00730
CHAPTER 6 ----- STEP CONTROL	BLO00740
CHAPTER 7 ----- BOUNDARY CONDITIONS	BLO00750
DATA C1, C2, CD, CAPP, ECONST/	BLO00760
1 1.43, 1.92, 0.09, 0.4, 9.0/	BLO00770
DATA SORTCD, CD25/ 0.3, 0.54722/	BLO00780
DATA FACTKE, FACTED/0.005, 0.03/	BLO00790
CHAPTER 8 ----- ADVANCE	BLO00800
DATA NTDMA/1/	BLO00810
CHAPTER 9 ----- COMPLETE	BLO00820
CHAPTER 10 ----- ADJUST	BLO00830
DATA KMPA/0/	BLO00840
CHAPTER 11 ----- PRINT	BLO00850
DATA NUMCOL/10/	BLO00860
CHAPTER 12 ----- DECIDE	BLO00870
END	BLO00880

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C MAIN PROGRAM
COMMON
1/CASE1/ UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPhi(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)
COMMON
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPR1, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEQ, NEQ1
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXU, NXYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PROP/ EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/ U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(484)
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YPUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)
COMMON/PART1/ OCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER
1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MDNTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))
EQUIVALENCE (F(1), U(1)), (OCP(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
DIMENSION XCP(484,10)
EQUIVALENCE (XCP(1,1), CPART1(1))
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1
CASE1..... LAMINAR, UNIFORM-PROPERTY, DEVELOPING FLOW IN A PIPE
COMMENT..... ALL NUMERICAL DATA ARE PUT IN VIA BLOCK DATA
READ(5,1300) KTEST

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MAI00010
MAI00020
MAI00030
MAI00040
MAI00050
MAI00060
MAI00070
MAI00080
MAI00090
MAI00100
MAI00110
MAI00120
MAI00130
MAI00140
MAI00150
MAI00160
MAI00170
MAI00180
MAI00190
MAI00200
MAI00210
MAI00220
MAI00230
MAI00240
MAI00250
MAI00260
MAI00270
MAI00280
MAI00290
MAI00300
MAI00310
MAI00320
MAI00330
MAI00340
MAI00350
MAI00360
MAI00370
MAI00380
MAI00390
MAI00400
MAI00410
MAI00420
MAI00430
MAI00440
MAI00450
MAI00460
MAI00470
MAI00480
MAI00490
MAI00500
MAI00510
MAI00520
MAI00530
MAI00540
MAI00550

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READ(5,1300) NX,NY	MA100560
READ(5,1301) (X(I),I=1,NX)	MA100570
READ(5,1301) (Y(I),I=1,NY)	MA100580
READ(5,1301) (F(I),I=1,3766)	MA100590
READ(5,1302) (RELAX(I),I=1,10)	MA100600
READ(5,1305) NTDMA,LASTEP,NOUTP1	MA100610
READ(5,1302) CNREL,TIMEF,DELT,ACCOM	MA100620
READ(5,1301) (CPINP(I),I=1,10)	MA100630
READ(5,1305) (MONTOR(I),I=1,10)	MA100640
1302 FORMAT(8F10.0)	MA100650
1305 FORMAT(10I5)	MA100660
ISTEP=0	MA100670
ILINE=0	MA100680
TIME=0.0	MA100690
NUMBER=0	MA100700
C----- PRINT OUT HEADINGS	MA100710
CALL OUTPH	MA100720
CHAPTER 2 2 2 2 2 GRID 2 2 2 2 2 2 2 2 2 2	MA100730
C----- QUANTITIES RELATED TO NX AND NY	MA100740
CALL CONST2	MA100750
C----- CALCULATE GRID QUANTITIES	MA100760
CALL GEOM	MA100770
IF(KTEST.GT.0) CALL TEST 11	MA100780
CHAPTER 3 3 3 3 3 VARIABLES 3 3 3 3 3 3 3 3 3 3	MA100790
C----- CONSTANTS RELATED TO VARIABLES	MA100800
CALL CONST3	MA100810
IF(KTEST.GT.0) CALL TEST 12	MA100820
CHAPTER 4 4 4 4 4 PROPERTY DATA 4 4 4 4 4 4 4 4 4 4	MA100830
C----- PUT REFERENCE VALUES IN FIELD	MA100840
C----- CELL-WALL DENSITY AND VISCOCITY	MA100850
DO 41 IY=1,NY	MA100860
RHON(IY)=RHOREF	MA100870
RHUS(IY)=RHOREF	MA100880
RHDS(IY)=RHOREF	MA100890
RHOW(IY)=RHOREF	MA100900
EMUN(IY)=EMUREF	MA100910
EMUS(IY)=EMUREF	MA100920
EMUE(IY)=EMUREF	MA100930
41 EMUW(IY)=EMUREF	MA100940
CHAPTER 5 5 5 5 5 STARTING PREPARATIONS 5 5 5 5 5 5 5	MA100950
C----- I INDICES FOR REFERENCE-PRESSURE POINT AND MONITORING LOCATION	MA100960
C----- CALCULATE FLOWIN AND REF. RES.-SOURCE VALUES	MA100970
RSREF(JCP1)=CPINP(1)	MA100980
RSREF(JCP2)=CPINP(2)	MA100990
RSREF(JCP3)=CPINP(3)	MA101000
RSREF(JCP4)=CPINP(4)	MA101010
RSREF(JCP5)=CPINP(5)	MA101020
RSREF(JCP6)=CPINP(6)	MA101030
RSREF(JCP7)=CPINP(7)	MA101040
RSREF(JCP8)=CPINP(8)	MA101050
RSREF(JCP9)=CPINP(9)	MA101060
RSREF(JCP10)=CPINP(10)	MA101070
C----- INITIALIZE VARIABLE STORAGES	MA101080
C CONSTANS FOR Y+	MA101090
CYPTW=CD25*DYG(NY)/EMUREF	MA101100

C	CTAUTW=EMUREF/DYG(NY)	MAI01110
	CONSTANTS FOR X+	MAI01120
	CXPLW=CD25*DXG(2)/EMUREF	MAI01130
	CTAULW=EMUREF/DXG(2)	MAI01140
C	ZERO CLEAR	MAI01150
	DO 499 I=1,4840	MAI01160
	FFF(1)=0.	MAI01170
499	FF(1)=0.	MAI01180
	DO 50 KPHI=1,KKLAST	MAI01190
	I1=KZERO(KPHI)+1	MAI01200
	I2=KZERO(KPHI)+(NX-1)*NY	MAI01210
	DO 51 I=I1,I2	MAI01220
	FFF(1)=CPINP(KPHI)	MAI01230
51	FF(1)=CPINP(KPHI)	MAI01240
50	CONTINUE	MAI01250
C	-----INITIALIZE TDMA-LINE STORAGE	MAI01260
	DO 554 IX=1,NXM1	MAI01270
	I1=(IX-1)*NY+1	MAI01280
	I2=(IX-1)*NY+NY	MAI01290
	CPART1(I1)=0.	MAI01300
	CPART1(I2)=0.	MAI01310
	CPART2(I1)=0.	MAI01320
	CPART2(I2)=0.	MAI01330
	CPART3(I1)=0.	MAI01340
	CPART3(I2)=0.	MAI01350
	CPART4(I1)=0.	MAI01360
	CPART4(I2)=0.	MAI01370
	CPART5(I1)=0.	MAI01380
	CPART5(I2)=0.	MAI01390
	CPART6(I1)=0.	MAI01400
	CPART6(I2)=0.	MAI01410
	CPART7(I1)=0.	MAI01420
	CPART7(I2)=0.	MAI01430
	CPART8(I1)=0.	MAI01440
	CPART8(I2)=0.	MAI01450
	CPART9(I1)=0.	MAI01460
	CPART9(I2)=0.	MAI01470
	CPART0(I1)=0.	MAI01480
	CPART0(I2)=0.	MAI01490
	DO 553 KPHI=1,KKLAST	MAI01500
	OCP(I1,KPHI)=0.	MAI01510
	OCP(I2,KPHI)=0.	MAI01520
553	CONTINUE	MAI01530
554	CONTINUE	MAI01540
	DO 555 IY=1,NXYP	MAI01550
555	P(IY)=0.0	MAI01560
	DO 501 IY=1,NY	MAI01570
	AN(IY)=0.0	MAI01580
	DV(IY)=0.0	MAI01590
	AS(IY)=0.0	MAI01600
	AE(IY)=0.0	MAI01610
	AW(IY)=0.0	MAI01620
	SU(IY)=0.0	MAI01630
	SP(IY)=0.0	MAI01640
	DU(IY)=0.0	MAI01650

VOLUME(IY)=0.0	MAI01660
PP(IY)=0.0	MAI01670
501 PHI0LD(IY)=0.0	MAI01680
C-----INITIALIZE Y-DIRECTION ARRAYS	MAI01690
DO 502 IX=1,NX	MAI01700
YPUST1(IX)=0.0	MAI01710
YPUST2(IX)=0.0	MAI01720
TAUTW1(IX)=0.0	MAI01730
502 TAUTW2(IX)=0.0	MAI01740
C-----INITIALIZE Y-DIRECTION ARRAYS	MAI01750
DO 503 IY=1,NY	MAI01760
TAULW(IY)=0.0	MAI01770
503 XPUSLW(IY)=0.0	MAI01780
CHAPTER 7 7 7 7 7 BOUNDARY CONDITIONS 7 7 7 7 7 7 7	MAI01790
C-----CALCULATE TAU AND Y+ FOR LADLE WALL LEFT	MAI01800
NODEL=NY-1	MAI01810
NODEF=2	MAI01820
NODEF1=NODEF-1	MAI01830
IXP1=IX+1	MAI01840
DO 7999 IX=2,NX	MAI01850
IX1NY=(IX-1)*NY	MAI01860
IX1NY1=(IX-1)*(NY-1)	MAI01870
DO 7699 KPHI=1,KKLAST	MAI01880
7699 IXNY(KPHI)=(IX-1)*NY	MAI01890
I=2+IX1NY	MAI01900
IE=I-NY	MAI01910
UP=U(IE)+(U(I)-U(IE))*FUNODE(IX)	MAI01920
ABSUP=ABS(UP)	MAI01930
IF(IX.EQ.2.AND.ABSUP.LE.TINY) UP=TINY	MAI01940
RSQRTK=RHO(I)*SQRT(TKE(I))	MAI01950
YPUST1(IX)=RSQRTK-CYPTW	MAI01960
IF(YPUST1(IX).GT.11.5) GO TO 701	MAI01970
TAUTW1(IX)=CTAUTW*UP	MAI01980
GO TO 710	MAI01990
701 TAUTW1(IX)=CAPPA*UP*RSQRTK*CD25/ALOG(ECONST*YPUST1(IX))	MAI02000
710 CONTINUE	MAI02010
C-----CALCULATE TAU AND Y+ FOR LADLE WALL- RIGHT	MAI02020
I=NYM1+IX1NY	MAI02030
IW=1-NY	MAI02040
UP=U(IW)+(U(I)-U(IW))*FUNODE(IX)	MAI02050
ABSUP=ABS(UP)	MAI02060
IF(IX.EQ.2.AND.ABSUP.LE.TINY) UP=TINY	MAI02070
RSQRTK=RHO(I)*SQRT(TKE(I))	MAI02080
YPUST2(IX)=RSQRTK-CYPTW	MAI02090
IF(YPUST2(IX).GT.11.5) GO TO 702	MAI02100
TAUTW2(IX)=CTAUTW*UP	MAI02110
GO TO 711	MAI02120
702 TAUTW2(IX)=CAPPA*UP*RSQRTK*CD25/ALOG(ECONST*YPUST2(IX))	MAI02130
711 CONTINUE	MAI02140
C CALCULATE TAU AND X+ FOR LADLE BOTTOM	MAI02150
IF(IX.NE.NXM1) GO TO 720	MAI02160
DO 721 IY=2,NYM1	MAI02170
I=IY+IX1NY	MAI02180
IV=IY+IX1NY1	MAI02190
ISV=IV-1	MAI02200



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VP=V(ISV)+(V(IV)-V(ISV))*FVNODE(IY)
RSQRTK=RHO(I)*SQRT(TKE(I))
XPUSLW(IY)=RSQRTK*CXPLW
IF(XPUSLW(IY).GT.11.5) GO TO 722
TAULW(IY)=CTAULW*VP
GO TO 721
722 TAULW(IY)=CAPPA*VP*RSQRTK*CD25/ALOG(ECONST*XPUSLW(IY))
721 CONTINUE
720 CONTINUE
KPHI=1
CALL COEFF(KPHI)
DO 53 IY=2,NYM1
I=IY+IX1NY
COEE(I)=AE(IY)
COEN(I)=AN(IY)
COES(I)=AS(IY)
COEW(I)=AW(IY)
53 VOLG(I)=VOLUME(IY)
7999 CONTINUE
DO 7998 IX=2,NXM1
IX1NY=(IX-1)*NY
IX1NY1=(IX-1)*(NY-1)
DO 7998 KPHI=1,KKLAST
I=IX1NY+2
COES(I)=0.
IW=I-NY
UA=0.5*(U(I)+U(IW))
FRIC=ABS(TAUTW1(IX)/(RHO(I)*UA*UA))
SQHF=SQRT(FRIC/2.)
SPLS=4.*RHO(I)/(18.*EMUREF**2)*0.05*UA**2*SQHF*RP(KPHI)**2
STAN1(IX,KPHI)=(FRIC/2.)/(1.+SQHF*(1525./SPLS**2-50.6))*UA

C
C
C
I=IX1NY+NYM1
COEN(I)=0.
IW=I-NY
UA=0.5*(U(I)+U(IW))
FRIC=ABS(TAUTW2(IX)/(RHO(I)*UA*UA))
SQHF=SQRT(FRIC/2.)
SPLS=4.*RHO(I)/(18.*EMUREF**2)*0.05*UA**2*SQHF*RP(KPHI)**2
STAN2(IX,KPHI)=(FRIC/2.)/(1.+SQHF*(1525./SPLS**2-50.6))*UA

C
C
C
IF(IX.NE.NXM1) GO TO 7998
DO 7997 IY=2,NYM1
I=IY +IX1NY
IV=IY +IX1NY1
COEE(I)=0.
ISV=IV-1
VA=0.5*(V(I)+V(ISV))
FRIC=ABS(TAULW(IY)/(RHO(I)*VA*VA))
SQHF=SQRT(FRIC/2.0)
SPLS=4.*RHO(I)/(18.*EMUREF**2)*0.05*VA**2*SQHF*RP(KPHI)**2

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MAI02210
MAI02220
MAI02230
MAI02240
MAI02250
MAI02260
MAI02270
MAI02280
MAI02290
MAI02300
MAI02310
MAI02320
MAI02330
MAI02340
MAI02350
MAI02360
MAI02370
MAI02380
MAI02390
MAI02400
MAI02410
MAI02420
MAI02430
MAI02440
MAI02450
MAI02460
MAI02470
MAI02480
MAI02490
MAI02500
MAI02510
MAI02520
MAI02530
MAI02540
MAI02550
MAI02560
MAI02570
MAI02580
MAI02590
MAI02600
MAI02610
MAI02620
MAI02630
MAI02640
MAI02650
MAI02660
MAI02670
MAI02680
MAI02690
MAI02700
MAI02710
MAI02720
MAI02730
MAI02740
MAI02750

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          STAN3(1Y,KPHI)=(FRIC/2.)/(1.+SQHF*(1525./SPLS**2-50.6))*VA
7997 CONTINUE
7998 CONTINUE
C----- PRINT OUT STARTING VALUES
4000 CONTINUE
      NUMBER=NUMBER+1
      TIME=TIME+DELT
      ISTEP=1
      IF(KTEST.GT.0) CALL TEST_13
      IF(KINPRI.GT.0) CALL OUTPF
      GO TO 60
55 IF(ISTEP.GT.1) GO TO 65
CHAPTER 6 6 6 6 STEP CONTROLL
60 CONTINUE
      DO 69 KPHI=1,KKLAST
69 RSSUM(KPHI)=0.0
      IF(ISTEP.GT.1) GO TO 64
      IF(ILINE.GT.0) GO TO 65
C-----Y-DIRECTION TDMA TRAVERSES
62 LINEF=2
      LINEL=NXM1
      NODEF=2
      NODEL=NYM1
C----- FOR BOTH X- AND Y-DIRECTION TRAVERSES
      NODEF1=NODEF-1
      NODEL1=NODEL-1
      NODLP1=NODEL+1
64 ILINE=LINEF
C-----QUANTITIES RELATED TO IX VALUE OF TDMA LINE
65 CONTINUE
      IX=ILINE
      IXP1=IX+1
      IX1NY=(IX-1)*NY
      IX1NY1=(IX-1)*NYM1
      IX2NY2=(IX-2)*NYM2
      DO 66 KPHI=1,KKLAST
66 IXNY(KPHI)=IX1NY
CHAPTER 8 8 8 8 ADVANCE 8 8 8 8 8 8 8 8 8 8
80 CONTINUE
C----- PUT NTRAVS EQUAL TO NTDMA,OR TO OTHER VALUES TO GIVE
C MULTI-TRAVERSE ON SELECTED LINES
      NTRAVS=NTDMA
C----- PUT GREAT INTO ARSL'S
      DO 85 J=1,KKLAST
85 ARSL(IX,J)=GREAT
C - OUTER LOOP FOR CARRYING OUT A MAX. OF NTRAVS TRAVERSES ON LINE IX
      KOUNT(IX)=NT
      RSMAX=0.
C - INNER LOOP FOR ALL VARIABLES (PLUS ONE FOR PREPARATIONS FOR TRANSFER
C TO NEXT LINE OR TO NEXT SWEEP OF FIELD)
      DO 1001 KPHI=1,KKLAST
      IF(NT.EQ.NTRAVS) GO TO 83
C----- UPDATE JPHI ON TDMA LINE
83 RSLINE(IX,KPHI)=0.0
      LABPHI=KPHI

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MAI02760
MAI02770
MAI02780
MAI02790
MAI02800
MAI02810
MAI02820
MAI02830
MAI02840
MAI02850
MAI02860
MAI02870
MAI02880
MAI02890
MAI02900
MAI02910
MAI02920
MAI02930
MAI02940
MAI02950
MAI02960
MAI02970
MAI02980
MAI02990
MAI03000
MAI03010
MAI03020
MAI03030
MAI03040
MAI03050
MAI03060
MAI03070
MAI03080
MAI03090
MAI03100
MAI03110
MAI03120
MAI03130
MAI03140
MAI03150
MAI03160
MAI03170
MAI03180
MAI03190
MAI03200
MAI03210
MAI03220
MAI03230
MAI03240
MAI03250
MAI03260
MAI03270
MAI03280
MAI03290
MAI03300

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184 map 185

	DO 899 IY=2,NYM1	MAI03310
	DO 899 I=1,10	MAI03320
	DO 899 J=1,10	MAI03330
	II=IX1NY+IY	MAI03340
899	ALPH(I,J,IY)=1.67*((RP(I)+RP(J))*0.5)**3*(TED(II)/EMUREF*RHOREF)**	MAI03350
1	0.5*ACCOM	MAI03360
	KCONST=IXNY(KPHI)+KZERO(KPHI)	MAI03370
	KEWPHI=KEW(KPHI)	MAI03380
	DO 898 IY=NODEF,NODEL	MAI03390
	I=IY+KCONST	MAI03400
898	PHIOLD(IY)=FF(1)	MAI03410
	I1=NODEF-1+KCONST	MAI03420
	I2=NODEL+1+KCONST	MAI03430
	PHIOLD(NODEF1)=FF(I1)	MAI03440
	PHIOLD(NODEL1)=FF(I2)	MAI03450
	CALL SOURC1(KPHI)	MAI03460
	CALL MODIFY(KPHI)	MAI03470
	CALL SOLVE(KPHI)	MAI03480
	IF(ILINE.NE.2) GO TO 8201	MAI03490
	I1=IX1NY+5	MAI03500
	I2=IX1NY+6	MAI03510
	I3=IX1NY+14	MAI03520
	I4=IX1NY+15	MAI03530
	XCP(I2,KPHI)=XCP(I3,KPHI)	MAI03540
	XCP(I1,KPHI)=XCP(I4,KPHI)	MAI03550
8201	CONTINUE	MAI03560
	CALL BOUND(KPHI)	MAI03570
	RSLINE(IX,KPHI)=RSLINE(IX,KPHI)/RSREF(KPHI)	MAI03580
	ABSRS=ABS(RSLINE(IX,KPHI))	MAI03590
	ARSL(IX,KPHI)=ABSRS	MAI03600
	RSMAX=AMAX1(RSMAX,ABSRS)	MAI03610
1001	CONTINUE	MAI03620
	IF(ILINE.EQ.LINEL) GO TO 110	MAI03630
	ILINE=ILINE+1	MAI03640
	GO TO 65	MAI03650
C-----	END OF INNER J-LOOP	MAI03660
C-----	END OF OUTER NTRAVS LOOP	MAI03670
CHAPTER 11	11 11 11 11 PRINT 11 11 11 11 11 11 11 11	MAI03680
110	CONTINUE	MAI03690
	ILINE=0	MAI03700
C-----	PRINT OUT RESIDUAL SOURCES AND VARIABLE VALUES	MAI03710
C	AT MONITORING LOCATION (IXMON,IYMON)	MAI03720
CHAPTER 12	12 12 12 12 DECIDE 12 12 12 12 12 12 12 12	MAI03730
C-----	CONVERGENCE CHECK	MAI03740
C-----	CHECK IF LAST STEP IS REACHED	MAI03750
	CALL OUTP1	MAI03760
	IF(ISTEP.GE.LASTEP) GO TO 129	MAI03770
128	ISTEP=ISTEP+1	MAI03780
	GO TO 60	MAI03790
129	CONTINUE	MAI03800
	IF(NUMBER.EQ.2) DELT=20.	MAI03810
	IF(NUMBER.EQ.4) DELT=30	MAI03820
	IF(NUMBER.EQ.6) DELT=60.	MAI03830
	IF(NUMBER.EQ.9) DELT=100.	MAI03840
	ISTEP=0	MAI03850

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IF(NUMBER.EQ.6) CALL OUTPF
IF(NUMBER.EQ.9) CALL OUTPF
DO 1299 I=1,4840
1299 FFF(I)=FF(I)
IF(TIME.LT.TIMEF) GO TO 4J00
CALL OUTPF
STOP
1300 FORMAT(2I4)
1301 FORMAT(5E13.5)
END
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MA103860  
MA103870  
MA103880  
MA103890  
MA103900  
MA103910  
MA103920  
MA103930  
MA103940  
MA103950

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SUBROUTINE SOLVE(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CONS(22), CDNE(22), CONW(22), ESMPhi(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KCUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STDR(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)
COMMON
6/DO/CHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEO, NEOP1
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV
6, NY, NYMAX, NYM1, NYM2, P1, RSCHK, RSMAX, RTINY
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(462), V(462), TKE(494), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(484)
7, INLY(10), IDUT(10), KIN, KDUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YPUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)
COMMON/PART1/QCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBR
1, CNREL, CDFE(484), CDEN(484), CDES(484), CDEW(484), CPINP(10), VOLG(484)
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))
EQUIVALENCE (F(1), U(1)), (QCP(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
COMMENT..... A AND B HAVE BEEN MADE EQUIVALENT TO AN, AS RESPECTIVELY
KPHI=LPHI
RRELAX=1./RELAX(KPHI)
RELAX1=1.-RELAX(KPHI)
KRSPhi=KRS(KPHI)
KCONST=IXNY(KPHI)+KZERO(KPHI)

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SOL00010
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SOL00190
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SOL00210
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SOL00240
SOL00250
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SOL00270
SOL00280
SOL00290
SOL00300
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SOL00370
SOL00380
SOL00390
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SOL00500
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SOL00520
SOL00530
SOL00540
SOL00550

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      IEWPHI=KEW(KPHI)
      NODE2=NODEL
      NF2=NODEF+NODE2
      A(NODEF1)=0.0
      C(NODEF1)=PHIOLD(NODEF1)
C----- FOR Y-DIRECTION TDMA TRAVERSES
12  IF(RELAX(KPHI).EQ.1.) GO TO 13
C----- FOR PHI WITH RELAX. FACTOR .NE. 1
      DO 14 IY=NODEF,NODE2
      IYM1=IY-1
      I=IY+KCONST
      IE=I+IEWPHI
      IW=I-IEWPHI
      AP(IY)=AN(IY)+AS(IY)+AE(IY)+AW(IY)
      SU(IY)=SU(IY)+AE(IY)*F(IE)+AW(IY)*F(IW)
C----- STORE AN IN STORE FOR RESIDUAL-SOURCE CAL.
      STORE(IY)=AN(IY)
C----- INCLUDE RELAXATION FACTOR IN TDMA COEFFICIENTS
      D(IY)=(AP(IY)-SP(IY))*RRELAX+TINY
      C(IY)=SU(IY)+RELAX1*D(IY)+PHIOLD(IY)
C----- MODIFY TDMA COEFFICIENTS FOR BACK SUBSTITUTION
      TERM=1./(D(IY)-B(IY)+A(IYM1))
      A(IY)=A(IY)*TERM
14  C(IY)=(C(IY)+C(IYM1)+B(IY))*TERM
      GO TO 110
C----- FOR PHI --- NO RELAXATION
13  DO 18 IY=NODEF,NODE2
      IYM1=IY-1
      I=IY+KCONST
      IE=I+IEWPHI
      IW=I-IEWPHI
      IMT=IY+(IX-1)*NY
      IME=IMT+NY
      IMW=IMT-NY
      IMN=IMT+1
      IMS=IMT-1
      AE(IY)=COEE(IMT)
      AN(IY)=COEN(IMT)
      AS(IY)=COES(IMT)
      AW(IY)=COEW(IMT)
      VOLUME(IY)=VOLG(IMT)
      SP(IY)=VOLUME(IY)*SP(IY)+RHOREF
      AP(IY)=((RHO(IMT)*VOLUME(IY))/(CNREL*DELT))+AN(IY)
1  +AS(IY)+AW(IY)+AE(IY)
      SU(IY)=AE(IY)*FF(IE)+AW(IY)*FF(IW)+SU(IY)+RHO(IMT)*VOLUME(IY)
1  +(VOLUME(IY)*RHO(IMT))/(CNREL*DELT)+OCP(IMT,KPHI)
C----- STORE AN IN STORE FOR RESIDUAL-SOURCE CAL.
      STORE(IY)=AN(IY)
      D(IY)=AP(IY)-SP(IY)+TINY
      C(IY)=SU(IY)
C----- MODIFY TDMA COEFFS. FOR BACK SUBSTITUTION
      TERM=1./(D(IY)-B(IY)+A(IYM1))
      A(IY)=A(IY)*TERM
18  C(IY)=(C(IY)+C(IYM1)+B(IY))*TERM
110 IF(KRSPHI.EQ.0) GO TO 120

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SOL00560
SOL00570
SOL00580
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SOL00600
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SOL00690
SOL00700
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SOL00990
SOL01000
SOL01010
SOL01020
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SOL01080
SOL01090
SOL01100

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C----- RESIDUAL-SOURCE CALCULATIONS
DO 115 IY=NODEF,NODE2
IF(SP(IY).LE.-1.E20) GO TO 115
RS=(AP(IY)-SP(IY))*PHIOLD(IY)-SU(IY)
1 -STORE(IY)=PHIOLD(IY+1)-AS(IY)+PHIOLD(IY-1)
115 RSLINE(IX,KPHI)=RSLINE(IX,KPHI)+RS
C----- BACK SUBSTITUTION IN TDMA OPERATIONS
120 DO 100 IY=NODEF,NODE2
IYBACK=NF2-IY
PHIOLD(IYBACK)=A(IYBACK)+PHIOLD(IYBACK+1)+C(IYBACK)
I=IYBACK+KCONST
100 FF(I)=PHIOLD(IYBACK)
RETURN
END
```

SOL01110  
SOL01120  
SOL01130  
SOL01140  
SOL01150  
SOL01160  
SOL01170  
SOL01180  
SOL01190  
SOL01200  
SOL01210  
SOL01220  
SOL01230  
SOL01240

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SUBROUTINE SOURC1(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOV(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPI(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)
COMMON
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6, ISTEP, IX, IXINY, IXINY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEO, NEOP1
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTOMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NAYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHK, RSMAX, TINY
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7, PHO(484), EMU(484)
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SQRTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YFUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)
COMMON/PART1/JCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER
1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONITOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))
EQUIVALENCE (F(1), U(1)), (OCP(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
DIMENSION XCP(484,10)
EQUIVALENCE (XCP(1,1), CPART1(1))
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1
KPHI=LPHI
DO 10 IY=1,NY
SU(IY)=0.

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SOU0010
SOU0020
SOU0030
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SOU0060
SOU0070
SOU0080
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SOU0100
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SOU0180
SOU0190
SOU0200
SOU0210
SOU0220
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SOU0240
SOU0250
SOU0260
SOU0270
SOU0280
SOU0290
SOU0300
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SOU0370
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SOU0390
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SOU0500
SOU0510
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SOU0530
SOU0540
SOU0550

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10	SP(IY)=0.	SOU00560
	IF(KPHI.EQ.JCP1) GO TO 100	SOU00570
	IF(KPHI.EQ.JCP2) GO TO 200	SOU00580
	IF(KPHI.EQ.JCP3) GO TO 300	SOU00590
	IF(KPHI.EQ.JCP4) GO TO 400	SOU00600
	IF(KPHI.EQ.JCP5) GO TO 500	SOU00610
	IF(KPHI.EQ.JCP6) GO TO 600	SOU00620
	IF(KPHI.EQ.JCP7) GO TO 700	SOU00630
	IF(KPHI.EQ.JCP8) GO TO 800	SOU00640
	IF(KPHI.EQ.JCP9) GO TO 900	SOU00650
	IF(KPHI.EQ.JCP10) GO TO 1000	SOU00660
	RETURN	SOU00670
C		SOU00680
C		SOU00690
100	CONTINUE	SOU00700
	DO 101 IY=2,NYM1	SCU00710
	I=IY+IX1NY	SCU00720
101	SU(IY)=0.0	SOU00730
	DO 102 IY=2,NYM1	SOU00740
	I=IY+IX1NY	SOU00750
	DO 103 J=2,10	SOU00760
103	SP(IY)=-ALPH(1,J,IY)*XCP(I,1)*XCP(I,J)/XCP(I,KPHI)+SP(IY)	SOU00770
	SP(IY)=SP(IY)-0.1428*ALPH(1,1,IY)*XCP(I,1)**2./XCP(I,KPHI)	SCU00780
102	CONTINUE	SCU00790
	RETURN	SOU00800
C		SOU00810
C		SOU00820
200	CONTINUE	SOU00830
	DO 201 IY=2,NYM1	SOU00840
	I=IY+IX1NY	SOU00850
201	SU(IY)=0.5*ALPH(1,1,IY)*XCP(I,1)**2+0.1428	SOU00860
	DO 202 IY=2,NYM1	SOU00870
	I=IY+IX1NY	SOU00880
	DO 203 J=3,10	SOU00890
203	SP(IY)=-ALPH(2,J,IY)*XCP(I,2)*XCP(I,J)/XCP(I,KPHI)+SP(IY)	SOU00900
	SP(IY)=-ALPH(2,1,IY)*XCP(I,1)*XCP(I,2)+0.0526/XCP(I,KPHI)	SCU00910
1	-ALPH(2,2,IY)*XCP(I,2)**2+0.4216+0.5/XCP(I,KPHI)+SP(IY)	SOU00920
202	CONTINUE	SOU00930
	RETURN	SOU00940
C		SOU00950
C		SOU00960
C		SOU00970
300	CONTINUE	SOU00980
	DO 301 IY=2,NYM1	SOU00990
	I=IY+IX1NY	SCU01000
301	SU(IY)=0.0526*ALPH(2,1,IY)*XCP(I,1)*XCP(I,2)+0.4210*ALPH(2,2,IY)	SCU01010
1	*XCP(I,2)**2+0.5	SCU01020
	DO 303 IY=2,NYM1	SOU01030
	I=IY+IX1NY	SOU01040
	DO 302 J=4,10	SOU01050
302	SP(IY)=-ALPH(3,J,IY)*XCP(I,3)*XCP(I,J)/XCP(I,KPHI)+SP(IY)	SOU01060
	SP(IY)=SP(IY)-0.027*ALPH(1,3,IY)*XCP(I,1)-0.2162	SOU01070
1	*ALPH(2,3,IY)*XCP(I,2)-0.7296*ALPH(3,3,IY)*XCP(I,3)	SOU01080
303	CONTINUE	SOU01090
	RETURN	SOU01100

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C          SOU01110
C          SOU01120
C          SOU01130
400 CONTINUE          SOU01140
      DO 401 IY=2,NYM1 SOU01150
      I=IY+IX1NY      SOU01160
401 SU(IY)=0.027*ALPH(3,1,IY)*XCP(I,3)+XCP(I,1)+0.2162*ALPH(2,3,IY) SOU01170
      1 *XCP(I,3)+XCP(I,2)+0.7296*ALPH(3,3,IY)*XCP(I,3)**2.*0.5 SOU01180
      DO 403 IY=2,NYM1 SOU01190
      I=IY+IX1NY      SOU01200
      DO 402 J=4,10    SOU01210
402 SP(IY)=-ALPH(4,J,IY)*XCP(I,4)*XCP(I,J)/XCP(I,KPHI)+SP(IY) SOU01220
      SP(IY)=SP(IY)-0.0163*ALPH(1,4,IY)*XCP(I,1)-0.1311*ALPH(2,4,IY) SOU01230
      1 *XCP(I,2)-0.4425*ALPH(3,4,IY)*XCP(I,3) SOU01240
403 CONTINUE          SOU01250
      RETURN          SOU01260
C          SOU01270
C          SOU01280
C          SOU01290
500 CONTINUE          SOU01300
      DO 501 IY=2,NYM1 SOU01310
      I=IY+IX1NY      SOU01320
501 SU(IY)=0.0163*ALPH(4,1,IY)*XCP(I,4)*XCP(I,1)+0.1311*ALPH(4,2,IY)* SOU01330
      1 XCP(I,4)*XCP(I,2)+0.4425*ALPH(4,3,IY)*XCP(I,4)*XCP(I,3)+ SOU01340
      1 0.9671*ALPH(4,4,IY)*XCP(I,4)**2.*0.5 SOU01350
      DO 503 IY=2,NYM1 SOU01360
      I=IY+IX1NY      SOU01370
      DO 502 J=5,10    SOU01380
502 SP(IY)=-ALPH(5,J,IY)*XCP(I,5)*XCP(I,J)/XCP(I,KPHI)+SP(IY) SOU01390
      SP(IY)=SP(IY)-0.0109*ALPH(5,1,IY)*XCP(I,1)-0.0878*ALPH(2,5,IY) SOU01400
      1 *XCP(I,2)-0.2966*ALPH(3,5,IY)*XCP(I,3)-0.7031*ALPH(4,5,IY)*XCP(I SOU01410
      1 ,4) SOU01420
503 CONTINUE          SOU01430
      RETURN          SOU01440
C          SOU01450
C          SOU01460
C          SOU01470
C          SOU01480
600 CONTINUE          SOU01490
      DO 601 IY=2,NYM1 SOU01500
      I=IY+IX1NY      SOU01510
601 SU(IY)=0.0329*ALPH(4,4,IY)*XCP(I,4)**2.*0.5+0.0109*ALPH(1,5,IY)* SOU01520
      1 XCP(I,1)+XCP(I,5)+0.0878*ALPH(5,2,IY)*XCP(I,5)*XCP(I,2)+ SOU01530
      1 0.2966*ALPH(5,3,IY)*XCP(I,3)+XCP(I,5)+0.7031*ALPH(5,4,IY) SOU01540
      1 *XCP(I,5)*XCP(I,4)+0.7324*ALPH(5,5,IY)*XCP(I,5)**2.*0.5 SOU01550
      DO 603 IY=2,NYM1 SOU01560
      I=IY+IX1NY      SOU01570
      DO 602 J=6,10    SOU01580
602 SP(IY)=-ALPH(6,J,IY)*XCP(I,6)*XCP(I,J)/XCP(I,KPHI)+SP(IY) SOU01590
      SP(IY)=SP(IY)-0.0077*ALPH(6,1,IY)*XCP(I,1)-0.0629*ALPH(6,2,IY)* SOU01600
      1 XCP(I,2)-0.2125*ALPH(6,3,IY)*XCP(I,3)-0.5038*ALPH(6,4,IY)* SOU01610
      1 XCP(I,4)-0.9840*ALPH(6,5,IY)*XCP(I,5) SOU01620
603 CONTINUE          SOU01630
      RETURN          SOU01640
C          SOU01650

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C		SOU01660
C		SOU01670
700	CONTINUE	SOU01680
	DO 701 IY=2,NYM1	SOU01690
	I=IY+IX1NY	SOU01700
701	SU(IY)=0.2676*ALPH(5,5,IY)*XCP(I,5)**2.*0.5+0.0077*ALPH(1,6,IY)*	SOU01710
1	XCP(I,6)*XCP(I,1)+0.0629*ALPH(2,6,IY)*XCP(I,2)*XCP(I,6)+	SOU01720
1	0.2125*ALPH(3,6,IY)*XCP(I,3)*XCP(I,6)+0.5038*ALPH(5,4,IY)*	SOU01730
1	XCP(I,6)*XCP(I,4)+0.9840*ALPH(6,5,IY)*XCP(I,6)*XCP(I,5)+	SOU01740
1	0.4736*ALPH(6,6,IY)*XCP(I,6)**2.*0.5	SOU01750
	DO 703 IY=2,NYM1	SOU01760
	I=IY+IX1NY	SOU01770
	DO 702 J=6,10	SOU01780
702	SP(IY)=-ALPH(7,J,IY)*XCP(I,7)*XCP(I,J)/XCP(I,KPHI)+SP(IY)	SOU01790
	SP(IY)=SP(IY)-0.0058*ALPH(1,7,IY)*XCP(I,1)-0.0472*ALPH(2,7,IY)*	SOU01800
1	XCP(I,2)-0.1596*ALPH(3,7,IY)*XCP(I,3)-0.3785*ALPH(4,7,IY)*XCP(I	SOU01810
1	,4)-0.7394*ALPH(5,7,IY)*XCP(I,5)	SOU01820
703	CONTINUE	SOU01830
	RETURN	SOU01840
C		SOU01850
C		SOU01860
C		SOU01870
800	CONTINUE	SOU01880
	DO 801 IY=2,NYM1	SOU01890
	I=IY+IX1NY	SOU01900
801	SU(IY)=0.5264*ALPH(6,6,IY)*XCP(I,6)**2.*0.5+0.0056*ALPH(7,1,IY)*	SOU01910
1	XCP(I,7)*XCP(I,1)+0.0472*ALPH(7,2,IY)*XCP(I,7)*XCP(I,2)+0.1596*ALP	SOU01920
1	H(7,3,IY)*XCP(I,7)*XCP(I,3)+0.3785*ALPH(7,4,IY)*XCP(I,7)*XCP(I,4)	SOU01930
1	+0.7394*ALPH(7,5,IY)*XCP(I,7)*XCP(I,5)+0.7836*ALPH(7,6,IY)*XCP(I,7	SOU01940
1	)*XCP(I,6)+0.1984*ALPH(7,7,IY)*XCP(I,7)**2.*0.5	SOU01950
	DO 803 IY=2,NYM1	SOU01960
	I=IY+IX1NY	SOU01970
	DO 802 J=8,10	SOU01980
802	SP(IY)=-ALPH(8,J,IY)*XCP(I,8)*XCP(I,J)/XCP(I,KPHI)+SP(IY)	SOU01990
	SP(IY)=SP(IY)-0.0044*ALPH(8,1,IY)*XCP(I,1)-0.0367*ALPH(8,2,IY)	SOU02000
1	*XCP(I,2)-0.1242*ALPH(8,3,IY)*XCP(I,3)-0.2947*ALPH(8,4,IY)	SOU02010
1	*XCP(I,4)-0.5758*ALPH(8,5,IY)*XCP(I,5)-0.9951*ALPH(8,6,IY)*	SOU02020
1	XCP(I,6)-0.5353*ALPH(8,7,IY)*XCP(I,7)	SOU02030
803	CONTINUE	SOU02040
	RETURN	SOU02050
C		SOU02060
C		SOU02070
C		SOU02080
900	CONTINUE	SOU02090
	DO 901 IY=2,NYM1	SOU02100
	I=IY+IX1NY	SOU02110
901	SU(IY)=0.2164*ALPH(7,6,IY)*XCP(I,7)*XCP(I,6)+0.8016*ALPH(7,7,IY)	SOU02120
1	*XCP(I,7)*XCP(I,7)+0.5+0.0044*ALPH(8,1,IY)*XCP(I,8)*XCP(I,1)	SOU02130
1	+0.0367*ALPH(8,2,IY)*XCP(I,8)*XCP(I,2)+0.1242*ALPH(8,3,IY)	SOU02140
1	*XCP(I,8)*XCP(I,3)+0.2947*ALPH(8,4,IY)*XCP(I,8)*XCP(I,4)+	SOU02150
1	0.5758*ALPH(8,5,IY)*XCP(I,8)*XCP(I,5)+0.9951*ALPH(8,6,IY)*	SOU02160
1	XCP(I,8)*XCP(I,6)+0.5353*ALPH(8,7,IY)*XCP(I,8)*XCP(I,7)	SOU02170
	DO 903 IY=2,NYM1	SOU02180
	I=IY+IX1NY	SOU02190
	DO 902 J=7,10	SOU02200

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902 SP(IY)=-ALPH(9,J,IY)*XCP(I,9)*XCP(I,J)/XCP(I,KPHI)+SP(IY)      SOU02210
   SP(IY)=SP(IY)-0.0035*ALPH(9,1,IY)*XCP(I,1)-0.0293*ALPH(9,2,IY)* SOU02220
1 XCP(I,2)-0.0994*ALPH(9,3,IY)*XCP(I,3)-0.2359*ALPH(9,4,IY)*     SOU02230
1 XCP(I,4)-0.4610*ALPH(9,5,IY)*XCP(I,5)-0.7967*ALPH(9,6,IY)*     SOU02240
1 XCP(I,6)                                                           SOU02250
903 CONTINUE                                                         SOU02260
   RETURN                                                            SOU02270
C                                                                      SOU02280
C                                                                      SOU02290
C                                                                      SOU02300
C                                                                      SOU02310
1000 CONTINUE                                                         SOU02320
   DO 1001 IY=2,NYM1                                                SOU02330
   I=IY+IX1NY                                                       SOU02340
1001 SU(IY)=0.4647*ALPH(8,7,IY)*XCP(I,8)-XCP(I,7)+0.9278*ALPH(8,8,IY) SOU02350
1 -XCP(I,8)+*2.*0.5+0.0035*ALPH(9,1,IY)*XCP(I,9)*XCP(I,1)+     SOUC2360
1 0.0293*ALPH(9,2,IY)*XCP(I,9)*XCP(I,2)+0.0994*ALPH(9,3,IY)*     SOU02370
1 XCP(I,9)*XCP(I,3)+0.2359*ALPH(9,4,IY)*XCP(I,9)*XCP(I,4)+     SOU02380
1 0.4610*ALPH(9,5,IY)*XCP(I,9)*XCP(I,5)+0.7967*ALPH(9,6,IY)*     SOU02390
1 XCP(I,9)*XCP(I,6)+0.7828*ALPH(9,7,IY)*XCP(I,9)*XCP(I,7)+     SOU02400
1 0.2722*ALPH(9,6,IY)*XCP(I,9)*XCP(I,8)                            SOUC2410
   DO 1003 IY=2,NYM1                                                SOU02420
   I=IY+IX1NY                                                       SOU02430
   DD 1002 J=6,10                                                  SOU02440
1002 SP(IY)=-ALPH(10,J,IY)*XCP(I,10)*XCP(I,J)/XCP(I,KPHI)+SP(IY) SOU02450
   SP(IY)=SP(IY)-0.0027*ALPH(10,1,IY)*XCP(I,1)-0.0239*ALPH(10,2,IY) SOUC2460
1 -XCP(I,2)-0.0813*ALPH(10,3,IY)*XCP(I,3)-0.1931*ALPH(10,4,IY)* SOU02470
1 XCP(I,4)-0.3773*ALPH(10,5,IY)*XCP(I,5)                          SOU02480
1003 CONTINUE                                                         SOU02490
   RETURN                                                            SOU02500
   END                                                                SOU02510

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SUBROUTINE PRINT(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2,RSYG(22),RSYV(22),RV(22),RVCB(22),SYG(22),SYV(22),Y(22),YV(22)
3/DNYONX/AE(22),AN(22),AP(22),AS(22),AW(22),C(22),D(22),DIFE(22)
3,DIFN(22),DUW(22),DIFW(22),DU(22),DV(22),EMUE(22),EMUN(22)
3,EMUW(22),HCONE(22),HCONN(22),HCONW(22)
3,PHIOLD(22),RHOE(22),RHON(22),RHOW(22),SP(22),SU(22)
3,VOLUME(22),CONN(22),CONC(22),CONE(22),CONW(22),ESMPHI(22)
4/DNX/ DXG(22),DXU(22),FU(22),FUNODE(22),KOUNT(22),RDXG(22)
4,RDXU(22),RSXG(22),RSXU(22),STORE(22),SXG(22),SXU(22),X(22),XU(22)
5/DUPHI/ IEW(10),ILAST(10),IMON(10),IXNY(10),IZERO(10)
5,JGROUP(10),KADSOR(10),KSOLVE(10),KRS(10),RELAX(10),RSREF(10)
5,RSSUM(10),ITITLE(10),KTITLE(10),KEW(10),KLAST(10),KZERO(10)
COMMON
6/DO/CCHECK,DP,FLOWPC,FLOWST,FLOWUP,GREAT,ILINE,IPLRS,IPREF,IPRINT
6,ISTEP,IX,IX1NY,IX1NY1,IX2NY2,IXMON,IXP1,IXPREF,IYMON,IYPREF
6,JEMU,JH,JLAST,JLIM1,JLIM2,JLIM3,JLIM4,JP,JPP,JRHO
6,JU,JV,JVP1,KINPRI,KMPA,KRAD,KRHOMU,KTEST,LABPHI
6,LASTEP,LINEF,LINEL,NEQ,NEGP1
6,NODEF,NODEF1,NODEL,NODEL1,NODLP1,NTDMA,NUMCOL
6,NX,NXMAX,NXM1,NXM2,NXYG,NXYP,NXYU,NXYV
6,NY,NYMAX,NYM1,NYM2,PI,RSCHK,RSMAX,TINY
COMMON/PROP/EMUREF,PRL(10),PRT(10),RHOREF
COMMON/D2D1/ARSL(22,10),RSLINE(22,10)
COMMON/D2D2/U(462),V(462),TKE(464),TED(464),H(484),PP(22),P(400)
7,RHO(484),EMU(484)
7,INLY(10),IOUT(10),KIN,KOUT,RELTKE,RELTED,ISTCH
COMMON
9/TURB/C1,C2,CD, SORTCD,CD25,ECONST,CTAUTW,CYPTW,TAUTW1(22)
9,TAUTW2(22),YPUST1(22),YPUST2(22)
9,TAULW(22),XPUSLW(22),CTAULW,CXPLW
9,GENK(22),FACTKE,FACTED,JTKE,JTED,CAPPA
9,CPART1(484),CPART2(484),CPART3(484),CPART4(484),CPART5(484)
9,CPART6(484),CPART7(484),CPART8(484),CPART9(484),CPART0(484)
COMMON/PART1/OCF(484,10),ALPH(10,10,22),RP(10),DELT,TIME,NUMBER
1,CNREL,COEE(484),COEN(484),COES(484),CDEW(484),CPINP(10),VOLG(484)
1,STAN1(22,10),STAN2(22,10),STAN3(22,10),JCP1,JCP2,JCP3,JCP4,JCP5
1,JCP6,JCP7,JCP8,JCP9,JCP10,KPHI,KKLAST,MONTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766),FF(4840),FFF(4840)
DIMENSION DIFS(22),EMUS(22),HCONS(22),RHOS(22)
EQUIVALENCE (DIFS(2),DIFN(1)), (EMUS(2),EMUN(1))
EQUIVALENCE (RHOS(2),RHON(1)), (AREAE,AREAW)
EQUIVALENCE (HCONS(2),HCONN(1)), (FF(1),CPART1(1))
EQUIVALENCE (F(1),U(1)), (DCP(1,1),FFF(1))
DIMENSION A(22),B(22)
EQUIVALENCE (A(1),AN(1)), (B(1),AS(1))
CHAPTER 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1
KPHI=LPHI
----- FOR ALL PHI'S EXCEPT P
KOLUM1=1
KOLUM2=NUMCOL
LIMIT1=KOLUM1

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PRI00010
PRI00020
PRI00030
PRI00040
PRI00050
PRI00060
PRI00070
PRI00080
PRI00090
PRI00100
PRI00110
PRI00120
PRI00130
PRI00140
PRI00150
PRI00160
PRI00170
PRI00180
PRI00190
PRI00200
PRI00210
PRI00220
PRI00230
PRI00240
PRI00250
PRI00260
PRI00270
PRI00280
PRI00290
PRI00300
PRI00310
PRI00320
PRI00330
PRI00340
PRI00350
PRI00360
PRI00370
PRI00380
PRI00390
PRI00400
PRI00410
PRI00420
PRI00430
PRI00440
PRI00450
PRI00460
PRI00470
PRI00480
PRI00490
PRI00500
PRI00510
PRI00520
PRI00530
PRI00540
PRI00550

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LIMIT2=KOLUM2
LTOP=KEW(KPHI)
LBOT=1
C----- FOR OTHER PHI'S
11 IF(LIMIT1.GT.NX) LIMIT1=NX
IF(LIMIT2.GT.NX) LIMIT2=NX
GO TO 20
C----- FOR P
CHAPTER 2 2 2 2 PRINT TITLE OF VARIABLES 2 2 2 2
20 CONTINUE
WRITE(6,9999)
WRITE(6,200) KTITLE(KPHI),KTITLE(KPHI)
200 FORMAT(/1X,15HFIELD VALUES OF,1X,14,2X,22(1H-),14,22(1H-))
CHAPTER 3 3 3 3 PRINT FIELD VALUES 3 3 3 3 3
DO 39 IY=LBOT,LTOP
IY=LTOP-IY+LBOT
DO 30 IX=LIMIT1,LIMIT2
31 I=IY+(IX-1)*NY
3000 I=I+KZERO(KPHI)
30 STORE(IX)=FF(I)
310 WRITE(6,3100) IY,Y(IY),(STORE(IX),IX=LIMIT1,LIMIT2)
39 CONTINUE
320 WRITE(6,3102) (IX,X(IX),IX=LIMIT1,LIMIT2)
C----- FOR ALL PHI'S OTHER THAN U AND P
IF(LIMIT2.EQ.NX) RETURN
KOLUM1=KOLUM1+NUMCOL
KOLUM2=KOLUM2+NUMCOL
GO TO 10
C----- FOR U AND P
3100 FORMAT(1X,1X,2HY(,12,2H)=,1PE9.3,2X,10(1PE9.2,1X))
3101 FORMAT(1X,3HYV(,12,2H)=,1PE9.3,2X,10(1PE9.2,1X))
3102 FORMAT(/5X,5HX(IX),9X,10(12,1H=,F6.2,1X)//)
3103 FORMAT(/5X,6HXU(IX),8X,10(12,1H=,F6.2,1X)//)
9999 FORMAT(/1X,56H( 1 = U, 2 = V, 3 = H, 4 = PP, 5 = P, 6 = RHO, 7 = E
1MU ))
RETURN
END

```

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PRI00560
PRI00570
PRI00580
PRI00590
PRI00600
PRI00610
PRI00620
PRI00630
PRI00640
PRI00650
PRI00660
PRI00670
PRI00680
PRI00690
PRI00700
PRI00710
PRI00720
PRI00730
PRI00740
PRI00750
PRI00760
PRI00770
PRI00780
PRI00790
PRI00800
PRI00810
PRI00820
PRI00830
PRI00840
PRI00850
PRI00860
PRI00870
PRI00880
PRI00890
PRI00900
PRI00910
PRI00920

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SUBROUTINE OUTPUT

COMMON

1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL	OUT00010
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)	OUT00020
2, PSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)	OUT00030
3/DNYDNX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)	OUT00040
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)	OUT00050
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)	OUT00060
3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22)	OUT00070
3, VOLUME(22), CONN(22), CONS(22), COHE(22), CCNW(22), ESMPhi(22)	OUT00080
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)	OUT00090
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)	OUT00100
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)	OUT00110
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)	OUT00120
5, RSSUM(10), I TITLE(10), K TITLE(10), KEW(10), KLAST(10), KZERO(10)	OUT00130
COMMON	OUT00140
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT	OUT00150
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF	OUT00160
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO	OUT00170
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI	OUT00180
6, LASTEP, LINEF, LINEL, NEQ, NEOP1	OUT00190
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL	OUT00200
6, NX, NXMAX, NXM1, NXM2, NXYG, NXP, NXYU, NXYV	OUT00210
6, NY, NYMAX, NYM1, NYM2, PI, RSCHK, RSMAX, TINY	OUT00220
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF	OUT00230
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)	OUT00240
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)	OUT00250
7, RHO(484), EMU(484)	OUT00260
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH	OUT00270
COMMON	OUT00280
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)	OUT00290
9, TAUTW2(22), YPUST1(22), YPUST2(22)	OUT00300
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW	OUT00310
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA	OUT00320
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)	OUT00330
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)	OUT00340
COMMON/PART1/DCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER	OUT00350
1, CNREL, COEE(484), CDEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)	OUT00360
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5	OUT00370
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPH1, KKLAST, MONTOR(10)	OUT00380
COMMON/ABC/AREAE	OUT00390
DIMENSION F(3766), FF(4840), FFF(4840)	OUT00400
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)	OUT00410
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))	OUT00420
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)	OUT00430
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))	OUT00440
EQUIVALENCE (F(1), U(1)), (DCP(1,1), FFF(1))	OUT00450
DIMENSION A(22), B(22)	OUT00460
EQUIVALENCE(A(1), AN(1)), (B(1), AS(1))	OUT00470
DATA KTRIP/0/	OUT00480
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1 1	OUT00490
CHAPTER 2 2 2 2 HEADINGS 2 2 2 2 2 2 2 2 2 2 2	OUT00500
ENTRY OUTPH	OUT00510
C----- THE PROBLEM	OUT00520
20 WRITE(6,201)	OUT00530
	OUT00540
	OUT00550

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201  FORMAT (///1X,10X,50HLAMINAR,UNIFORM-PROPERTY FLOW IN A CIRCULAR PIPE) OUT00560
      1PE /1X,10X,50(1H-)) OUT00570
C----- PROBLEM INFORMATION OUT00580
      REY=RHOREF*UINLET*2.*RPIPE/EMUREF OUT00590
      WRITE(6,210) XPIPE,RPIPE,UINLET,REY,HINLET,HWALL OUT00600
210  FORMAT (/1X,10H XPIPE,10H RPIPE,10H UINLET, OUT00610
      110H REY,NO,10H HINLET,10H HWALL/1X,1P6E10.2) OUT00620
      WRITE(6,250) NX,NY,NXMAX,NYMAX OUT00630
      WRITE(6,251) KRAD,NTDMA,KMPA,LASTEP,RSCHEK,CCHECK OUT00640
250  FORMAT (/1X,10H NX,10H NY,10H NXMAX,10H NYMAX) OUT00650
      1/1X,4I10) OUT00660
251  FORMAT (/1X,10H KRAD,10H NTDMA,10H KMPA,10H LASTEP) OUT00670
      1,10H RSCHEK,10H CCHECK/1X,4I10,1P2E10.2) OUT00680
      RETURN OUT00690
CHAPTER 3 3 3 3 3 FIELD VALUES 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 OUT00700
      ENTRY OUTPF OUT00710
      DO 31 KPHI=1,KKLAST OUT00720
32  CALL PRINT(KPHI) OUT00730
31  CONTINUE OUT00740
      KTRIP=0 OUT00750
      RETURN OUT00760
CHAPTER 4 4 4 4 PRINT OUT OF RESIDUAL SOURCES AND MONITORING VALUES OUT00770
      ENTRY OUTP1 OUT00780
      WRITE(6,1000) TIME OUT00790
      DO 50 I=1,10 OUT00800
      J=MONTOR(I) OUT00810
      WRITE(6,1001) J,CPART1(J),CPART2(J),CPART3(J),CPART4(J),CPART5(J) OUT00820
50  WRITE (6,1002) CPART6(J),CPART7(J),CPART8(J),CPART9(J),CPART0(J) OUT00830
1000 FORMAT (/1X,5HTIME=F7.2) OUT00840
1001 FORMAT (14,5E12.5) OUT00850
1002 FORMAT (4X,5E12.5) OUT00860
      RETURN OUT00870
      END OUT00880

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SUBROUTINE MODIFY(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, MINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2,RSYG(22),RSYV(22),RV(22),RVCB(22),SYG(22),SYV(22),Y(22),YV(22)
3/DNYONX/AE(22),AN(22),AP(22),AS(22),AX(22),C(22),D(22),DIFE(22)
3,DIFN(22),DUW(22),DIFW(22),DU(22),DV(22),EMUE(22),EMUN(22)
3,EMUW(22),HCONE(22),HCONN(22),HCONW(22)
3,PHIOLD(22),RHOE(22),RHON(22),RHCW(22),SP(22),SU(22)
3,VOLUME(22),CONN(22),CONS(22),CONE(22),CONW(22),ESMPHI(22)
4/DNX/ DXG(22),DXU(22),FU(22),FUNODE(22),KOUNT(22),RDXG(22)
4,RDXU(22),RSXG(22),RSXU(22),STORE(22),SXG(22),SXU(22),X(22),XU(22)
5/DJPHI/ IEW(10),ILAST(10),IMON(10),IXNY(10),IZERD(10)
5,JGROUP(10),KADSOR(10),KSOLVE(10),KRS(10),RELAX(10),RSREF(10)
5,RSSUM(10),ITITLE(10),KTITLE(10),KEW(10),KLAST(10),KZERO(10)
COMMON
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6,ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6,JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6,JU, JV, JVP1, KINPR1, KMPA, KRAD, KRHCOW, KTEST, LABPHI
6,LASTEP, LINEF, LINEL, NEO, NEOP1
6,NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL
6,NX, NXMAX, NXM1, NXM2, NXYG, NXP, NXYU, NXYV
6,NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHGREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7,RHO(484), EMU(484)
7,INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9,TAUTW2(22), YPUST1(22), YPUST2(22)
9,TAULW(22), XPUSLW(22), CTAULW, CXPLW
9,GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9,CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9,CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPARTC(484)
COMMON/PART1/OCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER
1,CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)
1,STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1,JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))
EQUIVALENCE (F(1), U(1)), (OCP(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1 1
KPHI=LPHI
SP(2)=SP(2)
SP(NYM1)=SP(NYM1)
IF(IX.NE.NXM1) RETURN

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MOD00010
MOD00020
MOD00030
MOD00040
MOD00050
MOD00060
MOD00070
MOD00080
MOD00090
MOD00100
MOD00110
MOD00120
MOD00130
MOD00140
MOD00150
MOD00160
MOD00170
MOD00180
MOD00190
MOD00200
MOD00210
MOD00220
MOD00230
MOD00240
MOD00250
MOD00260
MOD00270
MOD00280
MOD00290
MOD00300
MOD00310
MOD00320
MOD00330
MOD00340
MOD00350
MOD00360
MOD00370
MOD00380
MOD00390
MOD00400
MOD00410
MOD00420
MOD00430
MOD00440
MOD00450
MOD00460
MOD00470
MOD00480
MOD00490
MOD00500
MOD00510
MOD00520
MOD00530
MOD00540

```

10 SP(IY)=SP(IY)  
RETURN  
END

MOD00560  
MOD00570  
MOD00580

SUBROUTINE CONST	CONC0010
COMMON	CONC0020
1/CASE1/UIINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL	CONC0030
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)	CONC0040
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)	CONC0050
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)	CONC0060
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)	CONC0070
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)	CONC0080
3, PHIOLD(22), RHCE(22), RHON(22), RHOW(22), SP(22), SU(22)	CONC0090
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPhi(22)	CONC0100
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)	CONC0110
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)	CONC0120
5/DJPHI/ IEW(10), ILAST(10), I'MON(10), IXNY(10), IZERO(10)	CONC0130
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)	CONC0140
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)	CONC0150
COMMON	CONC0160
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT	CONC0170
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF	CONC0180
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO	CONC0190
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI	CONC0200
6, LATEST, LINEF, LINEL, NEQ, NEQ1	CONC0210
6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL	CONC0220
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYP, NXYU, NXYV	CONC0230
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY	CONC0240
COMMON/PROP/ EMUREF, PRL(10), PRT(10), RHOREF	CONC0250
COMMON/D2D1/ ARSL(22,10), RSLINE(22,10)	CONC0260
COMMON/D2D2/ U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)	CONC0270
7, RHO(484), EMU(484)	CONC0280
7, INLY(10), IDUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH	CONC0290
COMMON	CONC0300
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)	CONC0310
9, TAUTW2(22), YPUST1(22), YPUST2(22)	CONC0320
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW	CONC0330
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA	CONC0340
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)	CONC0350
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)	CONC0360
COMMON/PART1/DCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER	CONC0370
1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)	CONC0380
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5	CONC0390
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONTOR(10)	CONC0400
COMMON/ABC/AREAE	CONC0410
DIMENSION F(3766), FF(4840), FFF(4840)	CONC0420
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)	CONC0430
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))	CONC0440
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)	CONC0450
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))	CONC0460
EQUIVALENCE (F(1), U(1)), (DCP(1,1), FFF(1))	CONC0470
DIMENSION A(22), B(22)	CONC0480
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))	CONC0490
----- CONSTANTS RELATED TO NX AND NY -----	CONC0500
ENTRY CONST2	CONC0510
NXM1=NX-1	CONC0520
NXM2=NX-2	CONC0530
NYM1=NY-1	CONC0540
NYM2=NY-2	CONC0550

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C ----- TOTAL NUMBER OF NODES FOR DIFFERENT VARIABLES CON00560
  NXYG=NX*NY CON00570
  NXP=NXM2*NYM2 CON00580
  NXYU=NXM1*NY CON00590
  NXYV=NX*NYM1 CON00600
  RETURN CON00610
C ----- CONSTANTS RELATED TO VARIABLES ----- CON00620
  ENTRY CONST3 CON00630
  KRHOMU=KSOLVE(JRHO)+KSOLVE(JEMU) CON00640
C ----- IZERO, ILAST AND IEW FOR DIFFERENT VARIABLES CON00650
  IZERO(1)=0 CON00660
  DO 35 J=1, JLAST CON00670
  IF(J-JU) 310, 301, 310 CON00680
310 IF(J-JV) 320, 302, 320 CON00690
320 IF(J-JP) 330, 303, 330 CON00700
330 IF(J-JPP) 305, 304, 305 CON00710
301 IL=NXYU CON00720
  ILMAX=(NXMAX-1)*NYMAX CON00730
  IEW(J)=NY CON00740
  GO TO 34 CON00750
302 IL=NXYV CON00760
  ILMAX=NXMAX*(NYMAX-1) CON00770
  IEW(J)=NYM1 CON00780
  GO TO 34 CON00790
303 IL=NXP CON00800
  ILMAX=(NXMAX-2)*(NYMAX-2) CON00810
  IEW(J)=NYM2 CON00820
  GO TO 34 CON00830
304 IL=NY CON00840
  ILMAX=NYMAX CON00850
  IEW(J)=0 CON00860
  GO TO 34 CON00870
305 IL=NXYG CON00880
  ILMAX=NXMAX*NYMAX CON00890
  IEW(J)=NY CON00900
34 ILAST(J)=IZERO(J)+IL CON00910
  IF(J.EQ.JLAST) GO TO 35 CON00920
  JP1=J+1 CON00930
  IZERO(JP1)=IZERO(J)+ILMAX CON00940
35 CONTINUE CON00950
C ----- ASSIGNING NAMES TO THE TITLE-ARRAY CON00960
  KZERO(1)=0 CON00970
  DO 45 K=1, KKLAST CON00980
  IL=NXYG CON00990
  ILMAX=NXMAX*NYMAX CON01000
  KLAST(K)=KZERO(K)+IL CON01010
  KEW(K)=NY CON01020
  IF(K.EQ.KKLAST) GO TO 45 CON01030
  KP1=K+1 CON01040
  KZERO(KP1)=KZERO(K)+ILMAX CON01050
45 CONTINUE CON01060
  ITITLE(JU)=JU CON01070
  ITITLE(JV)=JV CON01080
  ITITLE(JP)=JP CON01090
  ITITLE(JPP)=JPP CON01100

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ITITLE(JTKE)=JTKE	CCN01110
ITITLE(JTED)=JTED	CCN01120
ITITLE(JRHO)=JRHO	CON01130
ITITLE(JEMU)=JEMU	CON01140
ITITLE(JH)=JH	CON01150
KTITLE(JCP1)=JCP1	CON01160
KTITLE(JCP2)=JCP2	CON01170
KTITLE(JCP3)=JCP3	CON01180
KTITLE(JCP4)=JCP4	CON01190
KTITLE(JCP5)=JCP5	CON01200
KTITLE(JCP6)=JCP6	CON01210
KTITLE(JCP7)=JCP7	CON01220
KTITLE(JCP8)=JCP8	CON01230
KTITLE(JCP9)=JCP9	CON01240
KTITLE(JCP10)=JCP10	CON01250
RETURN	CON01260
END	CON01270

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SUBROUTINE COEFF(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYDNX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHOV(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CDNS(22), CONE(22), CONW(22), ESMPHI(22)
4/DNX/ DAG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DUPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)
COMMON
6/D0/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEO, NEQP1
6, NDEF, NDEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXP, NXYU, NXYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(464)
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YPUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)
COMMON/PART1/OCF(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER
1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)
1, STAN1(22,10), STAN(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))
EQUIVALENCE (F(1), U(1)), (OCF(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 ; 1 1 1 1 1 1 1 1
C----- DEFINE ARITHMETIC FUNCTION FOR COMBINING
C APPROPRIATELY CONVECTION AND DIFFUSION CONTRIBUTIONS
C----- HYBRID SCHEME
C CONDIF(DIFF, FCONV, CONV)=AMAX1(0., DIFF+FCONV, CONV)
C----- UPWIND SCHEME

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CONDIF(DIFF,FCONV,CONV)=AMAX1(DIFF,DIFF+CONV)
KPHI=LPHI
IF(KRAD.EQ.2) GO TO 12
ASSIGN 1001 TO LG
GO TO 13
12 ASSIGN 1002 TO LG
13 CONTINUE
C----- TRANSFER VISCOSITIES STORED IN AN( ) TO EMUN( ), ETC.
CALL CELPHI(KPHI,JEMU)
N2=NODEL
EMUS(NODEF)=AS(NODEF)
DO 121 IY=NODEF,N2
EMUN(IY)=AN(IY)
EMUE(IY)=AE(IY)
121 EMUW(IY)=AW(IY)
C----- CONVECTION TERMS AND DIFFUSION-TERM*PRANDTL
C NUMBER FOR GENERAL PHI EQUATIONS
SXGIX=SXG(IX)
AREA=SXG(IX)*RV(NODEF1)
DIFS(NODEF)=EMUS(NODEF)*AREA*RDYG(NODEF)
ISV=NODEF1+IX1NY1
HCONS(NODEF)=0.5*RHOS(NODEF)*V(ISV)*AREA
RDXGIX=RDXG(IX)
RDXGI1=RDXG(IXP1)
DO 156 IY=NODEF,NODEL
IYM1=IY-1
I=IY+IX1NY
IW=1-NY
IV=IY+IX1NY1
AREAN=SXGIX
AREAE=SYG(IY)
GO TO LG,(1001,1002)
1002 AREAN=AREAN*RV(IY)
AREAE=AREAE*R(IY)
C AREAW=AREAE , THROUGH EQUIVALENCE
1001 VOLUME(IY)=AREAE*SXGIX
C DIFS(IY)=DIFN(IYM1) , THROUGH EQUIVALENCE
DIFN(IY)=EMUN(IY)*AREAN*RDYG(IY+1)
DIFE(IY)=EMUE(IY)*AREAE*RDXGI1
DIFW(IY)=EMUW(IY)*AREAW*RDXGIX
C HCONS(IY)=HCONN(IYM1) , THROUGH EQUIVALENCE
HCONN(IY)=0.5*RHON(IY)*V(IV)*AREAN
HCONE(IY)=0.5*RHOE(IY)*U(I)*AREAE
HCONW(IY)=0.5*RHOW(IY)*U(IW)*AREAW
CONN(IY)=HCONN(IY)+HCONN(IY)
CONS(IY)=HCONS(IY)+HCONS(IY)
CONE(IY)=HCONE(IY)+HCONE(IY)
CONW(IY)=HCONW(IY)+HCONW(IY)
ESMPHI(IY)=CONS(IY)-CONN(IY)+CONW(IY)-CONE(IY)
156 ESMPHI(IY)=AMAX1(0.0,-ESMPHI(IY))
CHAPTER 5 5 5 5 5 PHI EQUATION 5 5 5 5 5 5 5 5 5
50 RPRT=1./PRT(KPHI)
C----- COEFFICIENTS FOR ALL CELLS ON THE STRIP
KCONST=IXNY(KPHI)+KZERO(KPHI)
KEWPHI=KEW(KPHI)

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COE00560
COE00570
COE00580
COE00590
COE00600
COE00610
COE00620
COE00630
COE00640
COE00650
COE00660
COE00670
COE00680
COE00690
COE00700
COE00710
COE00720
COE00730
COE00740
COE00750
COE00760
COE00770
COE00780
COE00790
COE00800
COE00810
COE00820
COE00830
COE00840
COE00850
COE00860
COE00870
COE00880
COE00890
COE00900
COE00910
COE00920
COE00930
COE00940
COE00950
COE00960
COE00970
COE00980
COE00990
COE01000
COE01010
COE01020
COE01030
COE01040
COE01050
COE01060
COE01070
COE01080
COE01090
COE01100

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DD 56 IY=NODEF,NODEL	COE01110
I=IY+KCONST	COE01120
KE=1+IEWPHI	COE01130
IW=I-KEWPHI	COE01140
DS=DIFS(IY)*RPRT	COE01150
DN=DIFN(IY)*RPRT	COE01160
DE=DIFE(IY)*RPRT	COE01170
DW=DIFW(IY)*RPRT	COE01180
C----- ERROR SOURCE OF MASS	COE01190
FM=ESMPHI(IY)	COE01200
C----- COMBINING DIFFUSION AND CONVECTION CONTRIBUTIONS	COE01210
AN(IY)=CONDIF(DN,-HCONN(IY),-CONN(IY))	COE01220
AS(IY)=CONDIF(DS, HCONS(IY), CONS(IY))	COE01230
AE(IY)=CONDIF(DE,-HCONE(IY),-CONE(IY))	COE01240
AW(IY)=CONDIF(DW, HCONW(IY), CONW(IY))	COE01250
C----- STORING PHI IN PHIOLD	COE01260
C----- SOURCE TERMS	COE01270
56 CONTINUE	COE01280
C----- PUT BOUNDARY END VALUES IN PHIOLD	COE01290
C----- ADDITIONAL SOURCE TERMS IF REQUIRED	COE01300
RETURN	COE01310
END	COE01320



SUBROUTINE CELPHI(JCELL,LPHI)

COMMON

1/CASE1/UIINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL CEL00010  
 2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22) CEL00020  
 2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22) CEL00030  
 3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22) CEL00040  
 3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22) CEL00050  
 3, EMUW(22), HCDNE(22), HCONN(22), HCONW(22) CEL00060  
 3, PHIOLD(22), RHOE(22), RHON(22), RHOW(22), SP(22), SU(22) CEL00070  
 3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22) CEL00080  
 4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KOUNT(22), RDXG(22) CEL00090  
 4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22) CEL00100  
 5/DJPHI/ IEW(10), ILAST(10), IMON(10), IXNY(10), IZERO(10) CEL00110  
 5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10) CEL00120  
 5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10) CEL00130  
 COMMON CEL00140  
 6/DO/CHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT CEL00150  
 6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF CEL00160  
 6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO CEL00170  
 6, JU, JV, JVP1, KINPRI, KMPA, KRAD, KRHOMU, KTEST, LABPHI CEL00180  
 6, LATEST, LINEF, LINEL, NEQ, NEQP1 CEL00190  
 6, NODEF, NODEF1, NODEL, NODEL1, NODLP1, NTDMA, NUMCOL CEL00200  
 6, NX, NXMAX, NXM1, NXM2, NXYG, NXP, NXYU, NXYV CEL00210  
 6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY CEL00220  
 COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF CEL00230  
 COMMON/D2D1/ARSL(22,10), RSLINE(22,10) CEL00240  
 COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400) CEL00250  
 7, RHO(484), EMU(484) CEL00260  
 7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH CEL00270  
 COMMON CEL00280  
 9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22) CEL00290  
 9, TAUTW2(22), YPUST1(22), YPUST2(22) CEL00300  
 9, TAULW(22), XPUSLW(22), CTAULW, CXPLW CEL00310  
 9, GENX(22), FACTKE, FACTED, JTKE, JTED, CAPPa CEL00320  
 9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484) CEL00330  
 9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART10(484) CEL00340  
 COMMON/PART1/OCF(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMDER CEL00350  
 1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484) CEL00360  
 1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5 CEL00370  
 1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONTOR(10) CEL00380  
 COMMON/ABC/AREAE CEL00390  
 DIMENSION F(3766), FF(4840), FFF(4840) CEL00400  
 DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22) CEL00410  
 EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1)) CEL00420  
 EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW) CEL00430  
 EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1)) CEL00440  
 EQUIVALENCE (F(1), U(1)), (DCP(1,1), FFF(1)) CEL00450  
 DIMENSION A(22), B(22) CEL00460  
 EQUIVALENCE (A(1), AN(1)), (B(1), AS(1)) CEL00470  
 JPHI=LPHI CEL00480  
 30 CONTINUE CEL00490  
 COMMENT...AE,AW,AN,AS ARE USED AS TEMPORARY STORAGES, VALUES THERE CEL00500  
 COMMENT...SHOULD BE APPROPRIATELY TRANSFERRED IN THE CALLING SUBROUTINE CEL00510  
 C----- FACTORS TO ACCOUNT FOR EFFECTS OF END CEL00520  
 C----- BOUNDARIES (EAST AND WEST) CEL00530  
 CEL00540  
 CEL00550

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BW=0.5
BEW=0.5
IF(IX.EQ.2) BW=1.
IF(IX.EQ.NXM1) BEW=0.
BWE=1.-BW
BEE=1.-BEW
```

C----- ALL FOUR CELL WALLS

```
ICONST=IX1NY+IZERO(JPHI)
I=NODEF1+ICONST
AS(NODEF)=F(I)
IF(NODEF.GT.2) AS(NODEF)=0.5*(F(I)+F(I+1))
DO 31 IY=NODEF,NODEL
I=IY+1
IN=I+1
IE=I+NY
IW=I-NY
AN(IY)=0.5*(F(I)+F(IN))
AW(IY)=BW*F(IW)+BWE*F(I)
31 AE(IY)=BEW*F(I)+BEE*F(IE)
IF(NODEL.LT.NYM1) RETURN
```

C----- CORRECT AN FOR THE LAST CELL

```
IN=NODEL+ICONST
AN(NODEL)=F(IN)
RETURN
END
```

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CEL00560
CEL00570
CEL00580
CEL00590
CEL00600
CEL00610
CEL00620
CEL00630
CEL00640
CEL00650
CEL00660
CEL00670
CEL00680
CEL00690
CEL00700
CEL00710
CEL00720
CEL00730
CEL00740
CEL00750
CEL00760
CEL00770
CEL00780
CEL00790
CEL00800
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SUBROUTINE SOUND(LPHI)
COMMON
1/CASE1/UINLET, FLOWIN, RPIPE, XPIPE, FXSTEP, HINLET, HWALL
2/DNY/ DYG(22), DYV(22), FV(22), FVNODE(22), R(22), RDYG(22), RDYV(22)
2, RSYG(22), RSYV(22), RV(22), RVCB(22), SYG(22), SYV(22), Y(22), YV(22)
3/DNYONX/AE(22), AN(22), AP(22), AS(22), AW(22), C(22), D(22), DIFE(22)
3, DIFN(22), DUW(22), DIFW(22), DU(22), DV(22), EMUE(22), EMUN(22)
3, EMUW(22), HCONE(22), HCONN(22), HCONW(22)
3, PHIOLD(22), RHOE(22), RHON(22), RHQW(22), SP(22), SU(22)
3, VOLUME(22), CONN(22), CONS(22), CONE(22), CONW(22), ESMPHI(22)
4/DNX/ DXG(22), DXU(22), FU(22), FUNODE(22), KCUNT(22), RDXG(22)
4, RDXU(22), RSXG(22), RSXU(22), STORE(22), SXG(22), SXU(22), X(22), XU(22)
5/DJPHI/ IEW(10), ILAST(10), IMON(10), IKNY(10), IZERO(10)
5, JGROUP(10), KADSOR(10), KSOLVE(10), KRS(10), RELAX(10), RSREF(10)
5, RSSUM(10), ITITLE(10), KTITLE(10), KEW(10), KLAST(10), KZERO(10)
COMMON
6/DO/CCHECK, DP, FLOWPC, FLOWST, FLOWUP, GREAT, ILINE, IPLRS, IPREF, IPRINT
6, ISTEP, IX, IX1NY, IX1NY1, IX2NY2, IXMON, IXP1, IXPREF, IYMON, IYPREF
6, JEMU, JH, JLAST, JLIM1, JLIM2, JLIM3, JLIM4, JP, JPP, JRHO
6, JU, JV, JVP1, KINPR1, KMPA, KRAD, KRHOMU, KTEST, LABPHI
6, LASTEP, LINEF, LINEL, NEQ, NEOP1
6, NODEF, NODEF1, NODEL, NODEL1, NDDL1, NTDMA, NUMCOL
6, NX, NXMAX, NXM1, NXM2, NXYG, NXYF, NXYU, NXYV
6, NY, NYMAX, NYM1, NYM2, PI, RSCHEK, RSMAX, TINY
COMMON/PROP/EMUREF, PRL(10), PRT(10), RHOREF
COMMON/D2D1/ARSL(22,10), RSLINE(22,10)
COMMON/D2D2/U(462), V(462), TKE(484), TED(484), H(484), PP(22), P(400)
7, RHO(484), EMU(484)
7, INLY(10), IOUT(10), KIN, KOUT, RELTKE, RELTED, ISTCH
COMMON
9/TURB/C1, C2, CD, SORTCD, CD25, ECONST, CTAUTW, CYPTW, TAUTW1(22)
9, TAUTW2(22), YPUST1(22), YPUST2(22)
9, TAULW(22), XPUSLW(22), CTAULW, CXPLW
9, GENK(22), FACTKE, FACTED, JTKE, JTED, CAPPA
9, CPART1(484), CPART2(484), CPART3(484), CPART4(484), CPART5(484)
9, CPART6(484), CPART7(484), CPART8(484), CPART9(484), CPART0(484)
COMMON/PART1/DCP(484,10), ALPH(10,10,22), RP(10), DELT, TIME, NUMBER
1, CNREL, COEE(484), COEN(484), COES(484), COEW(484), CPINP(10), VOLG(484)
1, STAN1(22,10), STAN2(22,10), STAN3(22,10), JCP1, JCP2, JCP3, JCP4, JCP5
1, JCP6, JCP7, JCP8, JCP9, JCP10, KPHI, KKLAST, MONTOR(10)
COMMON/ABC/AREAE
DIMENSION F(3766), FF(4840), FFF(4840)
DIMENSION DIFS(22), EMUS(22), HCONS(22), RHOS(22)
EQUIVALENCE (DIFS(2), DIFN(1)), (EMUS(2), EMUN(1))
EQUIVALENCE (RHOS(2), RHON(1)), (AREAE, AREAW)
EQUIVALENCE (HCONS(2), HCONN(1)), (FF(1), CPART1(1))
EQUIVALENCE (F(1), U(1)), (DCP(1,1), FFF(1))
DIMENSION A(22), B(22)
EQUIVALENCE (A(1), AN(1)), (B(1), AS(1))
CHAPTER 1 1 1 1 1 PRELIMINARIES 1 1 1 1 1 1 1 1 1 1 1
JPHI=LPHI
IF(KPHI.EQ.JCP1) GO TO 10
IF(KPHI.EQ.JCP2) GO TO 20
IF(KPHI.EQ.JCP3) GO TO 30
IF(KPHI.EQ.JCP4) GO TO 40

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BOU00010
BOU00020
BOU00030
BOU00040
BOU00050
BOU00060
BOU00070
BOU00080
BOU00090
BOU00100
BOU00110
BOU00120
BOU00130
BOU00140
BOU00150
BOU00160
BOU00170
BOU00180
BOU00190
BOU00200
BOU00210
BOU00220
BOU00230
BOU00240
BOU00250
BOU00260
BOU00270
BOU00280
BOU00290
BOU00300
BOU00310
BOU00320
BOU00330
BOU00340
BOU00350
BOU00360
BOU00370
BOU00380
BOU00390
BOU00400
BOU00410
BOU00420
BOU00430
BOU00440
BOU00450
BOU00460
BOU00470
BOU00480
BOU00490
BOU00500
BOU00510
BOU00520
BOU00530
BOU00540
BOU00550

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	IF(KPHI.EQ.JCP5) GO TO 50	BOU00560
	IF(KPHI.EQ.JCP6) GO TO 60	BOU00570
	IF(KPHI.EQ.JCP7) GO TO 70	BOU00580
	IF(KPHI.EQ.JCF8) GO TO 80	BOU00590
	IF(KPHI.EQ.JCP9) GO TO 90	BOU00600
	IF(KPHI.EQ.JCP10) GO TO 100	BOU00610
	RETURN	BOU00620
C		BCU00630
C		BOU00640
	10 CONTINUE	BOU00650
	IF(IX.NE.2) RETURN	BOU00660
	DO 11 IY=1,NYM1	BOU00670
	I=IY+IX1NY	BOU00680
	IW=I-NY	BOU00690
	11 CPART1(IW)=CPART1(I)	BOU00700
	RETURN	BCU00710
C		BOU00720
C		BOU00730
	20 CONTINUE	BCU00740
	IF(IX.NE.2) RETURN	BOU00750
	DO 21 IY=1,NYM1	BCU00760
	IW=I-NY	BOU00770
	21 CPART2(IW)=CPART2(I)	BOU00780
	RETURN	BOU00790
C		BOU00800
C		BOU00810
	30 CONTINUE	BOU00820
	IF(IX.NE.2) RETURN	BOU00830
	DO 31 IY=1,NYM1	BOU00840
	I=IY+IX1NY	BOU00850
	IW=I-NY	BOU00860
	31 CPART3(IW)=CPART3(I)	BOU00870
	RETURN	BOU00880
C		BOU00890
C		BOU00900
	40 CONTINUE	BOU00910
	IF(IX.NE.2) RETURN	BOU00920
	DO 41 IY=1,NYM1	BOU00930
	I=IY+IX1NY	BOU00940
	IW=I-NY	BOU00950
	41 CPART4(IW)=CPART4(I)	BOU00960
	RETURN	BOU00970
C		BOU00980
C		BOU00990
	50 CONTINUE	BOU01000
	IF(IX.NE.2) RETURN	BOU01010
	DO 51 IY=1,NYM1	BOU01020
	I=IY+IX1NY	BOU01030
	IW=I-NY	BOU01040
	51 CPART5(IW)=CPART5(I)	BOU01050
	RETURN	BOU01060
C		BOU01070
C		BOU01080
	60 CONTINUE	BOU01090
	IF(IX.NE.2) RETURN	BOU01100

	DO 61 IY=1,NYM1	BCU01110
	I=IY+IX1NY	BCU01120
	IW=I-NY	BCU01130
61	CPART6(IW)=CPART6(I)	BCU01140
	RETURN	BCU01150
C		BCU01160
C		BCU01170
70	CONTINUE	BCU01180
	IF(IX.NE.2) RETURN	BCU01190
	DO 71 IY=1,NYM1	BCU01200
	I=IY+IX1NY	BCU01210
	IW=I-NY	BCU01220
71	CPART7(IW)=CPART7(I)	BCU01230
	RETURN	BCU01240
C		BCU01250
C		BCU01260
80	CONTINUE	BCU01270
	IF(IX.NE.2) RETURN	BCU01280
	DO 81 IY=1,NYM1	BCU01290
	I=IY+IX1NY	BCU01300
	IW=I-NY	BCU01310
81	CPART8(IW)=CPART8(I)	BCU01320
	RETURN	BCU01330
C		BCU01340
C		BCU01350
90	CONTINUE	BCU01350
	IF(IX.NE.2) RETURN	BCU01370
	DO 91 IY=1,NYM1	BCU01380
	I=IY+IX1NY	BCU01390
	IW=I-NY	BCU01400
91	CPART9(IW)=CPART9(I)	BCU01410
	RETURN	BCU01420
C		BCU01430
C		BCU01440
100	CONTINUE	BCU01450
	IF(IX.NE.2) RETURN	BCU01460
	DO 101 IY=1,NYM1	BCU01470
	I=IY+IX1NY	BCU01480
	IW=I-NY	BCU01490
101	CPARTO(IW)=CPARTO(I)	BCU01500
	RETURN	BCU01510
	END	BCU01520

## References

- 1) K. Nakanishi, J. Szekely, C.W. Chang, Iron making and Steel making (Quarterly) 1975 2 p. 115.
- 2) K. Nakanishi, J. Szekely, T. Fujii, et al., Met. Transaction 1975, 6B, p. 111.
- 3) K. Nakanishi, J. Szekely, Met. Transaction, 1975, 6B, p. 245.
- 4) K. Kinoshita, K. Nakanishi, Tetsu-to-Hagane, 1971, 57, p. 419.
- 5) K. Nakanishi, J. Szekely, Trans. ISIJ, 1975, 15, p. 522.
- 6) J.O. Hinze, "Turbulence, 2nd Edition" 1979, McGraw-Hill, New York
- 7) I. Komasa, R. Kuboi, T. Otake, Chemical Eng. Sci., 1974, 29, p. 641.
- 8) R. Kuboi, I. Komasa, T. Otake, Chemical Eng. Sci., 1974, 29, p. 651.
- 9) R. Kuboi, I. Komasa, T. Otake, Chemical Eng. Sci., 1974, 29, p. 659.
- 10) Y.H. Pao, The Physics of Fluids, 1965, 8, p. 1063.
- 11) R.L. Peskin, "Proceedings of Heat Transfer and Fluid Mechanics Institute", Stanford, U.P., Stanford.
- 12) S.L. Soo, "Fluid Dynamics of Multiphase System", Ginn Blaisdel, Waltham, Mass., 1967.
- 13) N. Sano, S. Shiomi, Y. Matsushita, Tetsu-to-Hagane, 1965, 51, p. 19.
- 14) E.T. Turkdogan, J. of The Iron and Steel Institute, 1972, 210 p. 21.
- 15) E.T. Turkdogan, J. of The Iron and Steel Institute, 1966, 204, p. 914.
- 16) T.B. Braun, J.F. Elliott, M.C. Flemings, Met. Transaction, 1979, 10B, p. 71.
- 17) T.B. Braun, Ph.D. Thesis, "Formation and Clustering of Alumina Particles in Liquid Iron", 1974, M.I.T., Cambridge, MA
- 18) E.T. Turkdogan, Trans. AIME, 1965, 233, p. 2100.
- 19) U. Lindborg, K. Torssell, Trans. AIME, 1968, 242, p. 94.
- 20) Y. Miyashita, Res. Rep., 1968, Nippon Kokan, Japan.
- 21) A. Engh, N. Lindskog, Scan. J. Metallurgy, 4, 1975, p. 49.
- 22) S. Linder, Scan. J. Metallurgy, 3, 1974, p. 137.
- 23) N. Lindskog, H. Sandberg, Scan. J. of Metallurgy, 2, 1973, p. 71.

- 24) S. Linder, "Scaninject", Jernkontoret, 1977, Lulea, Sweden
- 25) R. Gunn, Science, 1965, 150, p. 695.
- 26) P.G. Saffman, J.S. Turner, J. Fluid Mech., 1956, 1, p. 16.
- 27) H.M. Hulburt, S. Katz, Chemical Eng. Sci., 1964, 19, p. 555.
- 28) C.A. Coulaloglou, L.L. Taularides, Chemical Eng. Sci., 1977, 32, p. 1289.
- 29) K.J. Valentas, N.R. Amandson, I & E.C Fundamentals, 1966, 5, p. 533.
- 30) K.J. Valentas, O. Bilous, N.R. Amandson, I & E.C Fundamentals, 1966, 5, p. 271.
- 31) Smolchowski, A., Phys. Chem. 1917, 92, p. 129.
- 32) V.G. Levich "Physicochemical Hydrodynamics" 1962, Prentice-Hall, Englewood Cliff, N.J.
- 33) P.G. Saffman, J. of Fluid Mech., 1965, 22, p. 385.
- 34) P.O. Rouhiainen, J.W. Stachiewicz, J. of Heat Transfer, 1970, 92, p. 69.
- 35) S.K. Friedlander, H.F. Johnstone, Industrial and Engineering Chemistry, 1951, 49, p. 1151.
- 36) C.N. Davis, Proceeding of the Royal Society, London, series A, 1966, 289, p. 235.
- 37) C.D. Danson, E.B. Christiansen, D.L. Salt, AIChE Journal, 1966, 12, p. 589.
- 38) J.T. Davis, "Turbulent Phenomena" 1972, Academic Press, New York.
- 39) C.S. Lin, R.W. Moulton, G.L. Putnam, Inds. and Eng. Chemistry, 1953, 45, p. 636.
- 40) H. Schlichting "Boundary-layer Theory, 7th edition" 1979, McGraw-Hill, New York.
- 41) B.E. Launder, D.B. Spalding "Mathematical Models of Turbulence", 1972, Academic Press, London.
- 42) R.H. Pletcher "Survey of Finite-difference Strategy for Predicting Heat Transfer in Turbulent Channel Flow" in "Turbulent Forced Convection in Channels and Bundles" ed. by Skakac and D.B. Spalding, 1979, McGraw-Hill, New York.
- 43) R.H. Pletcher "Finite-difference Methods for Predicting Channel Flows; Turbulence Models and Some Comparison with Experimental data" *ibid*.
- 44) D.B. Spalding, "Theoretical Prediction of Single-Phase Turbulent Flow and Heat Transfer in Ducts and Rod Bundles I, II and III" *ibid*

- 45) E.R. van Driest, J. of Aero. Sci., 1956, 23, p. 1007.
- 46) W.M. Pun, D.B. Spalding, "A General Computer Program for Two-Dimensional Elliptic Flow", Report Number HTS/76/2, HTS, Imperial College of Science and Technology, 1976.
- 47) S.V. Patankar, "Numerical Heat Transfer and Fluid Flow", 1980, McGraw-Hill, New York.
- 48) B.E. Launder, D.B. Spalding, Computer Method in Applied Mech. and Eng. 3, 1974, p. 269.
- 49) J. Crank, "The mathematics of Diffusion", 1975, Clarendon Press, Oxford.
- 50) J. Crank, P. Nicolson, Proc. Camb. Phil. Soc. Math. Phys. Sci., 43, 1947, p. 50.
- 51) M.C. Flemings "Solidification Processing", 1974, McGraw-Hill, New York
- 52) R.K. Iyengar, W.O. Philbrook, Met. Trans., 3, 1972, p. 1823.
- 53) W.F. Ames, Numerical Method for Partial Differential Equations", 1977, Academic Press, New York.
- 54) Private communication, Nippon Steel