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LITFIRE USER'S GUIDE
Third Edition

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Abstract

This document contains instructions for using the LITFIRE lithium fire simulation code in its form as of April 1989. The code is capable of simulating fires in a single compartment connected to an optional second compartment, or in an insulated pan suspended in one compartment. Lithium or lithium-lead eutectic may be used as the fuel, reacting with an atmosphere of oxygen, nitrogen, water vapor, or any mixture thereof. Any inert gas may be included in the compartment atmosphere and lithium only may be burned in a carbon dioxide atmosphere without oxygen. An option for liquid metal-concrete interaction exists as well as the following options for mitigating the effects of the fire: gas flooding, emergency space cooling, emergency floor cooling, aerosol removal and gas injection. The guide also includes the following:

- a description of the workings of the code, including the various options available to the user
- a description of the physics of lithium fires and heat and mass transfer
- instructions for running the code
- a list of sample input files
- a listing of the code with a glossary defining code variables

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1 Introduction

LITFIRE is a computer code which simulates lithium fires in fusion reactors by generating the time histories of the temperature and pressure profiles occurring in a reactor containment in response to a lithium or lithium-lead eutectic spill and fire. The fire may take place in a single cell connected to an optional second cell, or in an insulated pan in a single cell. The lithium or lithium-lead may react with any mixture of oxygen, nitrogen or water vapor; an inert gas may also be included in the cell atmospheres. Lithium only may be burned in a carbon dioxide atmosphere without oxygen. An option for liquid metal-concrete interaction is available as well as the following options for mitigating the effects of a fire: gas flooding, emergency space cooling, emergency floor cooling, aerosol removal and gas injection. This user's guide includes a brief description of the physics of lithium fires, the workings of the code and the options available to users, and also includes a listing of the code with a complete glossary of variables used in LITFIRE.

The present version of LITFIRE is available on the PFCVAX at MIT and on the Crays at the National Magnetic Fusion Energy Computer Center (NMFECC, hereafter referred to as MFE) It is written in FORTRAN 77 and is compatible with the computing facilities at which it is located. The instructions present in this guide will enable a user to execute the code at either location.

Other information on LITFIRE such as more detailed descriptions of physical models or correlations used in the code are available in the references listed in the reference section of the guide.

2 Program Description

To assist the new user of LITFIRE in understanding the code, a brief descriptive section is included. The description of the code sections is presented in the order that they are executed. For a description of code options, see Section 2.3. This section is broken down into an initial routine and a dynamic cycle. The initial routine prepares the code for execution; then the dynamic cycle integrates the time rate of change of the code variables over the time step to calculate their values. The dynamic cycle is repeated until execution is terminated either by the code or as predetermined by the user.

2.1 Initial Routine

The four parts of the initial routine are:

1. read in the input data
2. write the input data to a file

3. initialize the variables
4. spray fire calculation

2.1.1 Input Data

The input data consists of titles and headings, control flags for the choice of options, geometries, initial conditions and material properties. User chosen options are described in Section 2.3. Input variables are described in Section 3 and examples of the input data files are given in Appendix D.

2.1.2 Print out the Input

The input is printed out to a file, which should be examined by the user to ensure that the input was properly entered into the input files. Misaligned input data is a common source of error that can easily be caught by examining the printed input.

2.1.3 Variable Initialization

The initialization section sets all time rates of change to zero for the first step. Some constants are defined and initial conditions are applied using the input data. In addition there is a short sub-section where the units of the input data are changed to the following to become consistent with the rest of the code:

BTU, pounds mass, feet, seconds

2.1.4 Spray Fire Calculations

The spray fire calculation simulates the effect of lithium reacting as a spray at the beginning of a spill. The amount reacted in the spray is user specified. A difficulty does arise in that the specific heats of the reaction products are calculated as functions of temperature. The spray fire calculation is not a spray fire model *per se* in that the lithium reacting in the spray is consumed instantaneously, adiabatically and stoichiometrically, with the equilibrium temperatures being determined by iteration.

2.2 Dynamic Cycle

The dynamic cycle in LITFIRE calculates the temperature, pressure and mass profiles of the reactor containment over the time of the run. Most of the dynamic cycle consists of calculating the thermal admittances between nodes, which are then used in conjunction with the nodal temperatures, to determine the time rates of change of the nodal temperatures. The heat flow to or from a node is determined by calculating the thermal resistances to conduction or convection between adjacent nodes and then adding on radiative heat transfer to or from nodes within a line of sight. All of the

calculations performed in the dynamic cycle are listed below in the order which they are performed:

1. Perform gas injection if necessary
2. Calculate temperature dependent heat capacities
3. Calculate individual gas fractions
4. Calculate gas emissivities and radiative interchange factors
5. Perform an energy balance to determine the gas temperature if the steam in containment option is used
6. Calculate natural convection gas heat transfer coefficients
7. Calculate thermal admittances
8. Perform steam injection if necessary
9. Perform lithium-lead diffusion calculation if necessary
10. Test for and calculate lithium or lithium-lead combustion
11. Calculate temperature rates of change from heat flow
12. Calculate lithium-concrete reaction if necessary
13. Calculate gas overpressure and leakage
14. Calculate aerosol removal rate via aerosol sticking
15. Perform integrations
16. Check for terminating execution
17. Perform time step control
18. Write the output to data files
19. Display error pointers if necessary

Short descriptions of the subsections appear below.

2.2.1 Preliminary Calculations

Before any calculations are performed by the code, the material properties of all of the nodes must be calculated. Most properties are assumed to be constant with respect to temperature, but the specific heats of some gases and combustion products, and most lithium properties, are calculated as functions of temperature. These are calculated at the beginning of each time step. The mass fraction and total mass of each of the individual gases is also calculated so that the total heat capacity of the gas may be calculated.

2.2.2 Radiative Heat Transfer

Radiative heat transfer rates in LITFIRE are calculated using the following basic equation:

$$Q_{1 \rightarrow 2} = f A_1 \sigma (T_1^4 - T_2^4) \quad (1)$$

where $Q_{1 \rightarrow 2}$ = heat transfer rate (W) from node 1 to node 2

A_1 = exposed area of node 1

f = radiative interchange factor based on A_1

σ = Stefan-Boltzmann constant

T_n = temperature of node n

The radiative interchange factor f is determined by the emissivities of the surfaces of the two nodes and the view factor between them. Thus the radiative emissivity of each node is required to account for radiative heat transfer within the containment building.

The emissivities of the solid elements in the containment building are specified by the input data and are assumed to be constant. The emissivity of the lithium pool is assumed by the code to be governed by the buildup of reaction products (Li_2O , Li_3N and Li_2CO_3) on the pool surface.

The emissivity of the cell gas (in the absence of steam) is determined by the aerosol size and concentration in the gas and by the optical path length in the cell. The aerosol particle area and the optical path length are defined by the user in the input data and the concentration is calculated from the amount of aerosol reaction product generated by the fire. In the presence of steam the emissivity of the cell gas is also governed by the partial pressure of the water vapor in the cell. Radiative heat transfer is discussed in greater detail in reference[2].

2.2.3 Gas Node Temperature Determination

If the steam in containment option is being used, the presence of a condensible gas requires that a different method be used to determine the temperature of the gas than the integral method described in Section 2.2.9, as the latent heat of vaporization of the steam must be taken into account. In this option, the code performs an iterative

energy balance by solving the equation:

$$\text{TEMP} = U_v - M_a c_{v_a} T - M_s u_s \quad (2)$$

where U_v is the total internal energy of the gas, M_a is the mass of the non-condensable gas, c_{v_a} is the specific heat of the non-condensable gas, M_s is the mass of the steam and u_s is the specific internal energy of the steam. Values of the temperature are guessed, and along with the specific volume of the steam (which is known), are used to determine the other properties of the steam. These values are then used to solve for the error, TEMP. When TEMP is a sufficiently small fraction of the total gas internal energy, the final guess is taken as the gas temperature. For further discussion, see reference[2].

2.2.4 Natural Convection Heat Transfer

The heat transfer coefficients for convective heat transfer between surfaces and gases h are calculated from the temperature of the surface T_s , the temperature of the gas T_g , and the density of the gas ρ_g :

$$h = CF(T_s, T_g, \rho_g) \quad (3)$$

where C is a user defined constant. In the presence of steam the heat transfer coefficients used are the Uchida heat transfer coefficients determined empirically as functions of the ratio of the mass of water to the mass of non-condensibles in the cell atmosphere. A more detailed description is given in reference[2].

2.2.5 Conductive Heat Transfer

Once the heat capacities, the radiative interchange factors and the convective heat transfer coefficients for all of the nodes have been calculated, the thermal resistances between the nodes are calculated. Knowledge of the thermal resistance allows the temperature rate of change due to heat conduction and heat convection to be calculated. In LITFIRE the thermal resistance between adjacent nodes i and j is calculated as follows:

$$R_{ij} = \frac{l_i}{2k_i A} + \frac{l_j}{2k_j A} \quad (4)$$

or

$$R_{ij} = \frac{l_i}{2k_i A} + \frac{1}{h_{ij} A} \quad (5)$$

where l_n = characteristic length (thickness) of node n

k_n = thermal conductivity of node n

A = area of contact between nodes i and j

h_{ij} = convective heat transfer coefficient between nodes i and j ,

depending on whether or not node j is a solid (Equation 4) or a gas (Equation 5).

The thermal resistance between the lithium pool and the combustion zone is determined somewhat differently, as the lithium is considered to vaporize and then react with the gases in the combustion zone. Details of the calculation are given in reference[2].

2.2.6 Temperature Rates of Change

The rates of heat transfer between all thermally adjacent nodes are calculated from the temperatures of the nodes, and the thermal resistances and radiative interchange factors between them. Once the rates of heat transfer to and from all of the nodes have been calculated, they are summed for each node, and the temperature rate of change of each node is calculated using its own heat capacity. The heat flow to or from a given node is determined by summing the heat flow by conduction, convection and radiation to and from thermally adjacent nodes:

$$Q_1 = \frac{(T_1 - T_i)}{\sum_i R_{1i}} + \sum_j A_1 f_{1j} \sigma (T_1^4 - T_j^4) \quad (6)$$

where: Q_1 = heat flow rate to or from node 1
 T_n = temperature of node n
 i = designation for physically adjacent node
 R_{1i} = thermal resistance between nodes 1 and i
 (see Eqns. 4 and 5)
 j = designation for optically adjacent node
 A_1 = surface area of node 1
 f_{1j} = radiative interchange factor between nodes 1 and j

Temperature rates of change for each node are calculated by dividing the energy gain or loss rate by the heat capacity of the node:

$$\frac{dT_1}{dt} = \frac{Q_1}{m_1 c_{p1}} \quad (7)$$

where t is time, m_1 is the mass of node 1 and c_{p1} is the specific heat of node 1. The combustion zone node adds the heat of combustion and the heat of vaporization of the lithium combusted to the above terms, while the lithium pool subtracts the heat of vaporization of the lithium combusted. That is due to the assumption that the lithium reaction takes place in the vapor phase.

2.2.7 Lithium Combustion

The temperature rates of change in the containment can differ greatly depending whether or not the lithium pool is actually combusting (reacting with the containment atmosphere). The criteria used to determine whether or not the lithium is combusting are:

- Liquid lithium must be available (between 180 and 1347°C)
- Oxygen, nitrogen, carbon dioxide or water vapor must be available
- If only nitrogen is present, the combustion zone temperature must be less than 1127°C

If none of the above conditions are met, then the combustion zone is considered to be nonexistent, and heat transfer from the lithium to the rest of the containment building is performed normally. If combustion is occurring, then the combustion rate and the heat liberated by the lithium reactions is calculated.

In LITFIRE the lithium combustion rate is governed by the flow rate of gas or (if lithium-lead is being burned) the diffusion of lithium to the combustion zone. The gas flow rate is determined by natural convection using Reynold's analogy between heat and mass transfer.

Once the gas flow rate to the combustion zone has been calculated, the lithium reaction rate may be calculated. The lithium is assumed to react with the gas quickly as it flows to the combustion zone, unless the chemical kinetics serves to further limit the reaction rate. The unhindered lithium reaction rate is given by:

$$RR_{Li} = A_{\text{pool}} \sum_i RR_i \quad (8)$$

where

$$RR_i = h_m \rho_i R_{s,i} \quad (9)$$

where A_{pool} = surface area of the lithium pool

h_m = natural convection mass transfer coefficient

ρ_i = total density of the gas i (mass/containment volume)

$R_{s,i}$ = stoichiometric combustion ratio between lithium and the gas i
(mass of lithium/mass of gas)

The kinetics of the lithium reactions with nitrogen, oxygen and steam may serve to either reduce the reaction rates below those expected from the gas flow rate to the reaction site. After the gas flow rates of each of the constituent gases of the atmosphere have been determined, reaction kinetics effects are applied to the preliminary reaction rates to determine their final values. Lithium reaction kinetics are covered in detail in reference[2].

Once the reaction rates have been calculated, the heat generated by combustion is calculated by summing the products of the reaction rates RR_i and the heats of combustion ΔH_i of each of the reacting gases:

$$Q_c = \sum_i RR_i \Delta H_i \quad (10)$$

2.2.8 Overpressure, Leakage, and Aerosol Behavior

The masses of each cell gas component and the cell gas temperature are integrated in the integration section. From this, the cell gas pressure is determined and thus leakage from containment can be calculated. Aerosol adhesion to the containment walls is a user specified option and changes the concentration of aerosol combustion products in the containment atmosphere.

2.2.9 Integrals

All time rates of change are integrated over each time step to calculate the values of the quantities during the execution of the code. The form of the integrals is:

$$P = \text{INTGRL} \left(P_o, \frac{dP}{dt} \right) \quad (11)$$

where P_o is the initial value of function P (mass, temperature or energy), and $\frac{dP}{dt}$ is the time dependent rate of change of P .

INTGRL is an integration function that uses a fourth order Runge-Kutta Method or Simpson's Rule (user specified) to simultaneously solve all of the differential equations used in the code. For a more detailed description, see the listing of the code, Appendix F.

2.2.10 Termination Checks

The conditions that will terminate the code are:

- the lithium temperature reaches a value at which the lithium vaporizes (1347°C) or solidifies (180°C)
- the primary cell gas temperature returns to ambient temperature with no over-pressurization
- the code reaches the user specified stopping point ($\text{TIME} \geq \text{TIMEF}$)

2.2.11 Time Step Control

Three criteria are used to determine the size of the time step used during each dynamic cycle. They are:

1. The time step must be smaller than a user defined fraction of the inverse rates of change:

$$\text{DELT} < \text{RELERR} \ T / \left(\frac{dT}{dt} \right)$$

2. The conduction heat transfer limit must be satisfied:

$$\frac{\alpha \Delta t}{(\Delta x)^2} < 0.3$$

3. The user imposed maximum and minimum time steps must be observed. The maximum time step is indicated by DELOUT and the minimum by DTMIN. DELOUT and DTMIN are read from the first input file.

2.2.12 Output Section

The output from LITFIRE is written into data files as the code is executed. Examples of the output files are shown in Appendix E, generated by the input files found in Appendix D.

2.2.13 Error Pointers

This section is not actually part of the dynamic cycle, although if an error during execution should occur, an error message would be written into file *out1.dat* and code execution would halt.

2.3 Modeling Options

The basic version of LITFIRE is capable of simulating a wide variety of spill conditions as indicated by the user in the first input data file. The containment volume, height, wall and floor areas, atmosphere, and material composition may be specified as well as the mass and surface area of the lithium spilled. Optional reaction geometries include a primary cell containing the lithium, surrounded by a larger secondary cell; a partially insulated pan holding the lithium inside the basic primary cell; or a primary cell surrounded by blanket and shield structures producing decay heat, further surrounded by a larger secondary cell. A concrete floor and wall for the containment are optional as is a liquid metal-concrete reaction routine. Also instead of elemental lithium, a lithium-lead eutectic may be selected for the spill with the composition chosen by the user. Finally an option to simulate a lithium or lithium-lead spill in the presence of a steam-air atmosphere may be chosen.

In addition to the above options, several options involving the mitigation of lithium fires are available. These include:

- gas flooding
- emergency space cooling
- emergency floor liner cooling
- aerosol removal

- gas injection

Each option is discussed below.

2.3.1 One Cell Option

The single cell model is the simplest version of LITFIRE that may be run. All other options are constructed as subroutines added on to the one cell version of the code. The nodes existing in the one cell version are shown in Figure 1. There may be up to twenty concrete wall or floor nodes of any thickness. As stated earlier all material properties may be chosen by the user as may the composition of the containment atmosphere. Lithium or lithium-lead may react with any mixture of oxygen, nitrogen or water vapor and lithium only may react with carbon dioxide in the absence of oxygen. Any inert gas may also be included in the cell atmosphere. Lastly, any containment or spill geometry may be chosen as stated above.

The heat transfer correlations are fixed by the code so that accurate results may be obtained, although some modification is possible from the input data as shown in Section 2.2.4. The heat transfer pathways are also fixed by the code and are shown in Figure 1. The heat transfer mechanisms and their applications to the code are further discussed in reference[2].

2.3.2 Two Cell Option

The two cell option was developed to model the effects of a fire inside a tokamak fusion reactor and to determine its effects on the structural integrity of the the torus. In this option a separate secondary cell with its own material composition, atmosphere and geometry exists surrounding the primary cell. (See Figure 1) The provision for a crack between the primary and secondary cells, allowing the exchange of cell gases also exists. The code follows the composition, pressure and temperature of both cell gases during the run. The heat and mass flow paths in two cell LITFIRE are shown in Figures 2 and 3. High velocity gas flows, as would be encountered in the event of a breach in a vacuum torus have been successfully modeled by LITFIRE. (See reference[3])

2.3.3 Pan Option

Figure 4 shows the pan option available in LITFIRE. This option may be used with either the one or two cell option, but not with the concrete reaction option. This option was created to model the lithium fire experiments performed at HEDL. The pan dimensions and composition are user defined. The pan is surrounded by two separate insulation nodes.

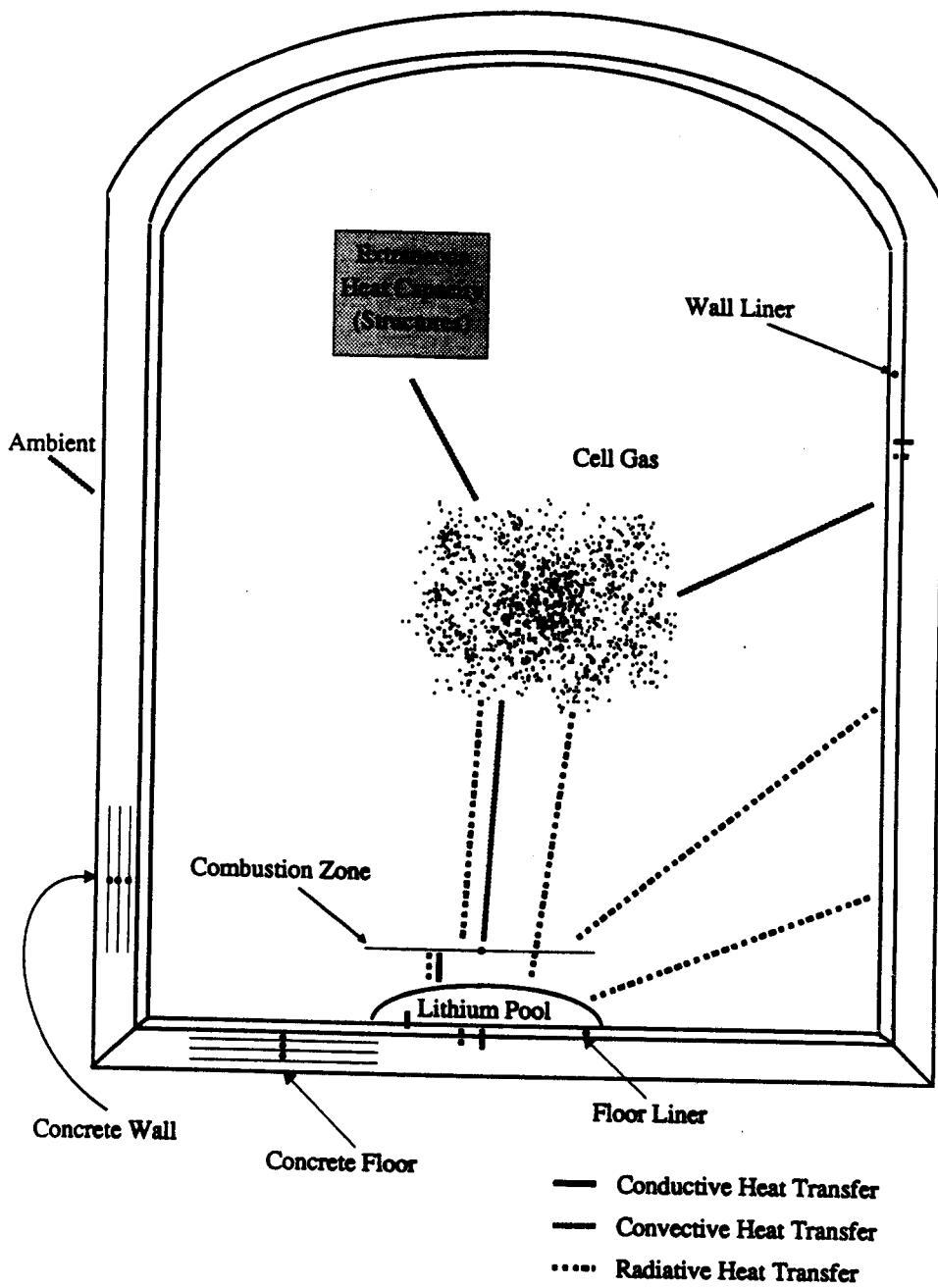


Figure 1: One-cell option in LITFIRE

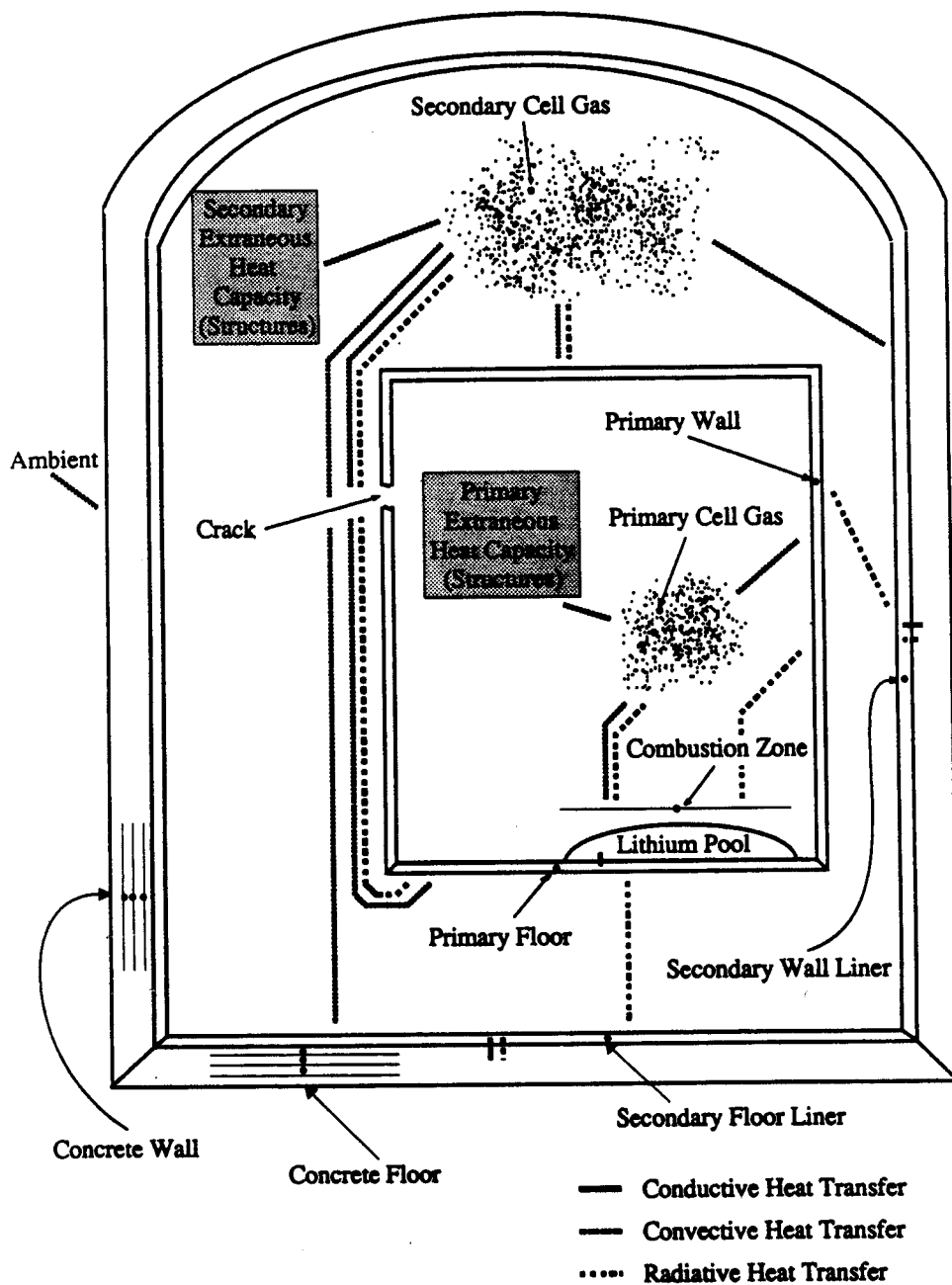


Figure 2: Two-cell option in LITFIRE

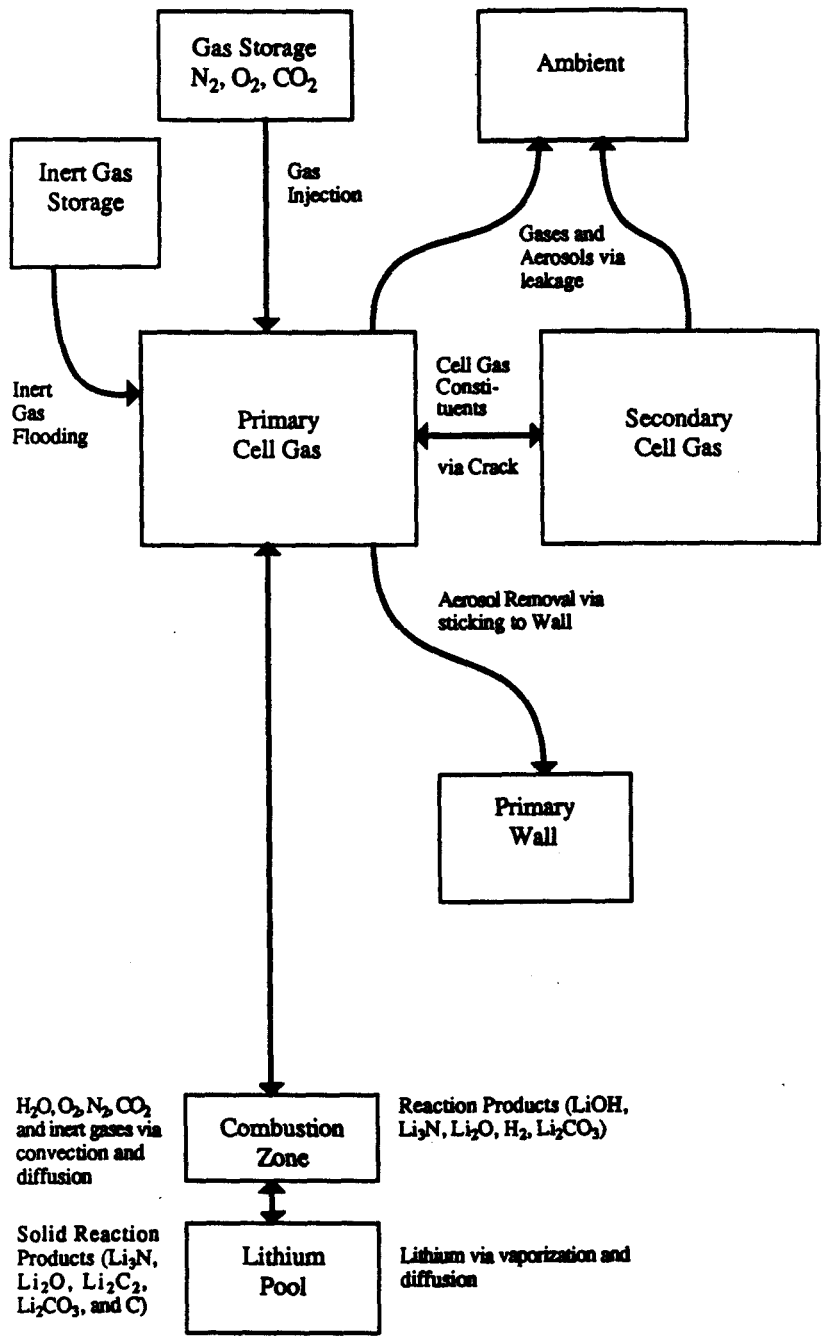


Figure 3: Mass flow in LITFIRE

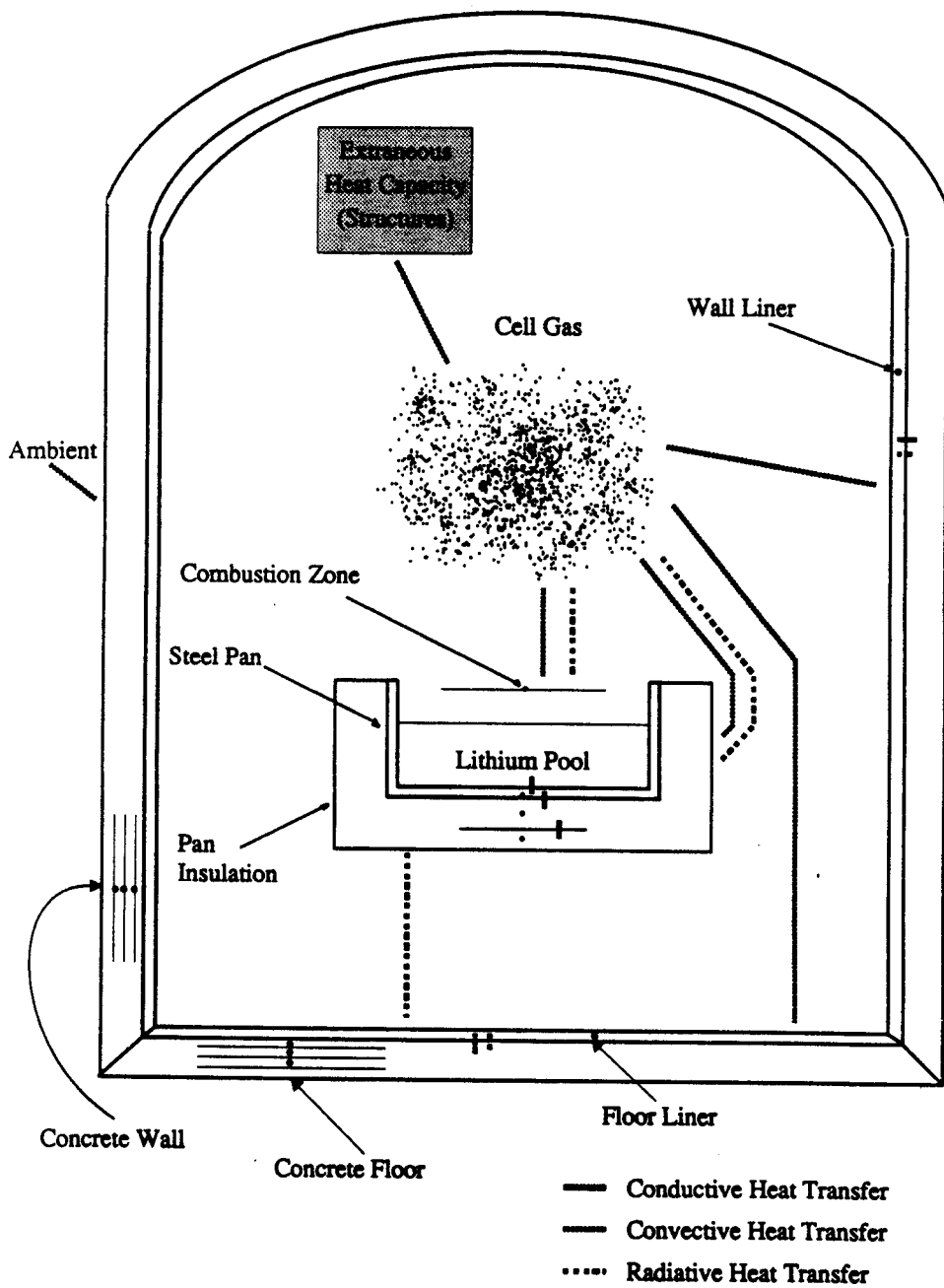


Figure 4: Pan option in LITFIRE

2.3.4 Concrete Reaction

The liquid metal-concrete reaction subroutine allows for the reaction of lithium with the concrete floor under the liner. This includes lithium reactions with water driven from the concrete and certain components of the concrete itself. For further discussion, see reference[2].

2.3.5 Lithium-Lead Combustion

This option allows for the substitution of a lithium-lead eutetic in the place of elemental lithium as the source of the fire. All LITFIRE options are compatible with the lithium-lead combustion option except for the initial spray fire calculation. In addition, this option allows the user to choose either a layered or turbulent pool reaction, allowing for optimistic or pessimistic results respectively, depending on the user's view of lithium-lead fires. Reference[2] discusses the lithium-lead option in greater detail.

2.3.6 Steam-Air Atmosphere Option

The steam-air atmosphere option allows for the reaction of lithium or lithium-lead with a mixture of steam and other non-condensable gases. It also includes modifications of the convective heat transfer coefficients to account for condensation and the provision for steam condensation into a water pool node above the cell floor liner. Gas temperature is determined by an iterative energy balance routine (as shown in Section 2.2.3) to account for the presence of the condensable vapor, rather than in the usual integral method described earlier. The steam in the atmosphere may be present as humidity or may be injected into the primary or secondary cell atmosphere, with the time, mass flow rate and enthalpy of the steam injected selected by the user. The development of the steam-air atmosphere option is discussed in reference[2].

2.3.7 Torus Fire Option

This option allows LITFIRE to model a lithium or lithium-lead fire inside the plasma chamber of a tokamak during a loss of flow or loss of coolant accident. The reactor blanket and shield structures are represented by six extra nodes surrounding the primary cell, shown in Figure 5. During a loss of flow accident the nodes are thermally connected via conduction. During a loss of coolant accident some of them are also connected via radiation as shown in the figure. The emissivities of, and the view factors between the nodes are user specified. The radioactive decay heat generated in the first wall (primary wall and floor) and the blanket and shield structures is included as an extra heat generation term for each node:

$$\frac{dT_i}{dt} = \sum_r \frac{q_{o_i}''' e^{-\lambda t}}{\rho_i c_{p_i}} \quad (12)$$

where: i = individual node
 r = each individual isotope in the node i
 q''_{oi} = initial decay heat density of an isotope r
 λ = decay constant of an isotope r
 ρ_i = density of node i

Up to three different isotopes may be modeled in each node; the initial decay heat density and the decay coefficient are specified by the input data for each isotope. In the coding of the torus fire option, the breeder region of the blanket (see Figure 5) is represented by the node, in the two-cell option, that normally represents the secondary extraneous heat capacity. In the torus fire option, the extraneous heat capacity in the outer cell is represented by the magnets node. The torus fire option is incompatible with the two-cell, pan and concrete reaction options.

2.3.8 Mitigation Options

The following is a list of options available to evaluate the effectiveness of certain techniques used to attempt to mitigate the consequences of a lithium fire:

- gas flooding
- emergency space cooling
- emergency floor liner cooling
- aerosol removal
- gas injection

Each option allows the user to select additional heat removal mechanisms as desired. These options are discussed further in reference[4].

3 Execution of LITFIRE

The execution of the LITFIRE code requires certain system commands depending upon the location at which it is being run. The specific commands for compiling, loading (linking), and running the code will be discussed in this section in the following order:

1. Obtaining the source code and sample input files
2. Execution on the PFCVAX
3. Execution on the MFE Crays

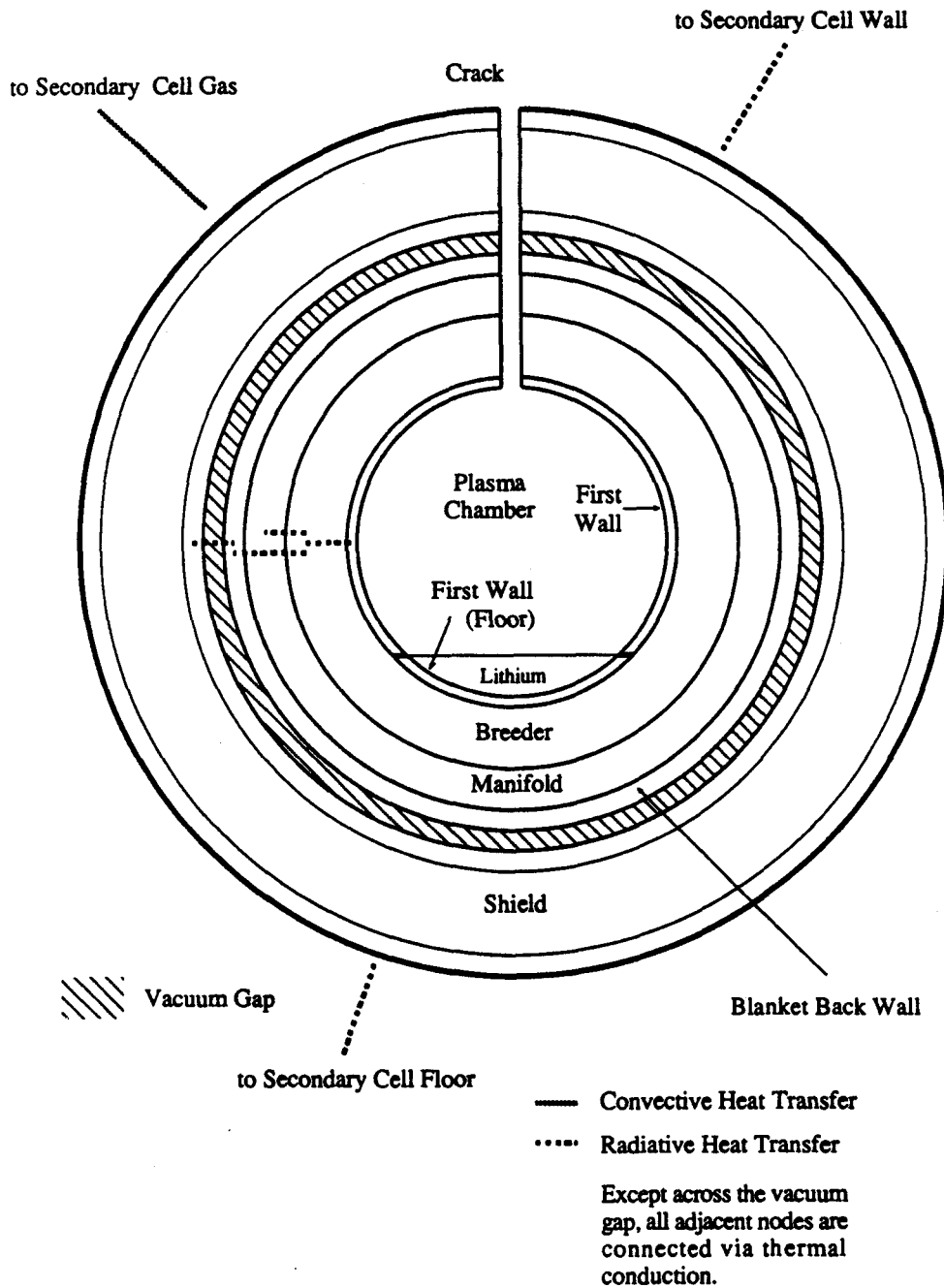


Figure 5: Torus fire option in LITFIRE

3.1 Obtaining Copies of LITFIRE and the Input Data Files

There are currently two locations at which a copy of the source code of LITFIRE can be found: the PFCVAX at MIT, and the MFE FILEM disk storage.

To use the PFCVAX copy, the user must first obtain a PFCVAX account. This may be done by contacting the Plasma Fusion Center at MIT. Introductory information may be found on the VAX by using the HELP command, which will define most of the commands used on the PFCVAX.

To get a copy of LITFIRE for personal use, the following commands must be used:

```
copy [barnett.litfire]litfire.for [username]*.*
```

This will copy the code *litfire.for* into the user's main directory.

To get a copy of the sample input files, the *copy* command must also be used, substituting the following filenames for *litfire.for*:

```
head.dat  
uumak.w  
uumak.x  
uumak.y  
uumak.z  
steamop.  
torus.
```

After obtaining copies of the input files, they may be viewed by using the *type* command or edited by using any line or text editor. (e.g. EMACS or EDT).

To obtain a copy of the LITFIRE source code on one of the MFECC machines, the user must be logged onto a machine and then use the *filem* command to obtain a personal copy:

```
filem read .15467 litfire
```

This will copy *litfire* into the user's personal directory on that particular machine.

To obtain copies of the input files, the command

```
read .15467 filename
```

must be used for each input file (the names are the same for MFE and the PFCVAX) while still in *filem*.

Once copies of LITFIRE and the sample input files have been obtained, they may be moved to a different machine 'n' by using the *netout* command as follows:

```
netout filename site=nma
```

3.2 Organization of LITFIRE for Execution

One of the most important steps in the execution of LITFIRE is the preparation of the input data files. Most errors in code execution occur due to mistakes in the input data files. The input data files and the options they control are listed below. As stated in Section 2.3, some options are incompatible with each other.

uwmak.w: one cell
uwmak.x: two cell
uwmak.y: pan, concrete reaction and lithium lead combustion
uwmak.z: gas flooding, emergency space cooling, emergency floor liner cooling, aerosol removal and gas injection
steamop.: steam injection with steam-air atmosphere
torus.: torus fire

3.2.1 One Cell Option

The one cell option is the simplest version of LITFIRE. The first input file must exist to run any other code options. The order in which the input variables must appear in the file *uwmak.w* is shown below (British units are given in the Glossary, SI units may be used for all input data files by setting the input variable IFLAGISI = 1):

line	variables
1	IFLAGW,IFLAGF,IFLAGP,IFLAG2,IFLAGS,IFLAGC, IFLAGU,IFLAGB,IBLOW,IESC,ISFLC,ISWICH, IAROSL,IFLAGD,IFLAGISI,IFLAGCO,IFLAGT IFLAGR
2	NL,NL1
3	L(1) to L(NL)
4	L1(1) to L1(NL1)
5	VP,CHP,CPAP,XMOLA
6	TEHCZP,XMEHCP,AEHCP,CPEHCP,HINECP
7	THWC,THFC,GAP,KGAP,KLEAK
8	ESTLWP,CPSWP,KSTLWP,RHSWP,AWP,THWP
9	ESTLFP,CPSFP,KSTLFP,RHSFP,AFP,THFP
10	EMLI,CPLI,AKLI,RHLI
11	EMCONC,CPCON,KCON,RHCON
12	RHOLIO,RHOLIN,RHOLIH,EMGPF,EMCZ,TAUCZ
13	QCO1,QCO2,QCN,QCW,QCW2
14	RCMBO1,RCMBO2,RCMBN,RCMBW,RCMBW2,RCMBH2
15	TMELT,TVAP,QVAP,PERCEN
16	CONF1,CONF2,C2FAC,FLIOH,FLI2O
17	HIN,HINGSP,HINGSS,HINPS,HINSAM,HINEAN
18	HINFGS,HINFGS
19	ASLI,SPILL,SPRAY,FRA,RA
20	TCZI,TGPZER,TSPZER,TSFPI,TA,TLII
21	PAPZER,WO2P,HUM,WAP,WCP
22	IMETH,DTMIN,TIMEF,RELERR,DELOUT,OUTPUT

The formats for the input lines are:

line	format
1	(1x,14(i1,1x))
2	(i4,i4)
3,4	(10f5.3)
5	(f12.2,3f12.4)
6-21	(6f12.4)
22	(i4,5f12.4)

An example of this data file (British units) is *uwmak.w* in Appendix D.

PFCVAX The statement:

```
open(unit=2,file='uwmak.w',status='old')
```

must be included in the code for the code to execute, assuming that the input data file is named *uwmak.w*. A similar OPEN statement must be included for each input data

file used by the code. These statements are currently located after the "common" blocks at the beginning of the code.

MFE Crays For these machines the statement:

```
call link("unit1=filename,read1//")
```

must be used for each input data file. These statements are also currently located after the "common" blocks at the beginning of the code.

3.2.2 Two Cell Option

If the two cell option is chosen, the following are the variable listing and formats for the second data file (units are given in the glossary as for the first input file):

line	variables
1	VS,CHS,PASZER,TGSZER,TSSZER,TFSZER
2	CRACK,HUM2,WO2S,WAS,CPAS,WCO2S
3	TEHCZS,XMEHCS,AEHCS,CPEHCS,HINECS
4	ESTLWS,CPSWS,KSTLWS,RHSWS,AWS,THWS
5	ESTLFS,CPSFS,KSTLFS,RHSFS,AFS,THFS
6	TSWICH

The format for all lines is: (6f12.4)

PFCVAX If this option is used, the statement:

```
open(unit=3,file='filen.ame',status='old')
```

must be included in LITFIRE in the same place as the OPEN statement for the first input data file. An example of this data file (British units) is given in Appendix D.

MFE Crays For these machines, the statement:

```
call link("unit3=filename,read3//")
```

must be used in the same location as the CALL LINK statement for the first input data file.

3.2.3 Pan, Concrete Reaction and Lithium-Lead Combustion

The following is a variable listing for each of the above options (British units are given in the Glossary):

Pan Option	
line	variables
1	KPAN, RHPAN, CPPAN, RHINS, CPINS, EMINS
2	TPANZO, APAN, BREDTH, AINS, HINGPF
3	THKPAN, THKIN1, THKIN2

Concrete Reaction Option†	
line	variables
1	ZZDIN, QCCONC, CRACON, XMH2OI, TCIGNI, RCMBC

Lithium-Lead Option‡	
line	variables
4(1)	CPLEAD, KLEAD, RHLEAD, ALLOYI, QDISS, CPLIPB
5(2)	DFLVAR

†: The pan option cannot be chosen with the concrete reaction option.

‡: Lithium-lead data is entered on line 1 if the concrete reaction option is not chosen.

The format for all lines except 5(2) for the lithium-lead option is: (6f12.4) The format for line 5(2) is: (e12.5)

PFCVAX The statement:

```
open(unit=4, file='flen.ame', status='old')
```

must be used. An example of this file (British units) is given in Appendix D.

MFE Crays For these machines, the statement:

```
call link("unit4=filename, read4//")
```

must be used in the same location as the CALL LINK statement for the first input data file.

3.2.4 Gas Flooding, Emergency Space Cooling, Emergency Floor Liner Cooling and Gas Injection

Each of these options is included in one input data file. The following is a variable listing for each of the options. Only the variable lines of the options used need be entered, although the lines used must be in the order shown below (British units are given in the Glossary):

line		variables
1	(gas flooding)	WO2B,WWAB,WN2B,XMOLAB,CPAB,TBLOW
2		BLOWV,EXHSTV,TBLIN,TBLOUT,WAB
3	(emerg. space cooling)	ESCR,ESCTIN,ESCEND
4	(emerg. floor cooling)	SFLCR,SFLTIN,SFLEND
5	(aerosol removal)	BETA
6	(gas injection)	TONE,TTWO,TTHREE,DP1,DP2,DP3,FCT1,FCT2,FCT3

The format for lines 1-5 is: (6f12.4). For the gas injection option (line 6) it is: (3f10.2,6f8.4).

PFCVAX The statement:

```
open(unit=5,file='flen.ame',status='old')
```

must be used. An example of this file (British units) is given in Appendix D.

MFE Crays For these machines, the statement:

```
call link("unit5=filename,read5//")
```

must be used in the same location as the CALL LINK statement for the first input data file.

3.2.5 Steam Injection to Containment

The following is a variable listing for the steam injection to containment available in the steam-air atmosphere option (British units are given in the Glossary):

line	variables
1	STMIN,STMOUT,MINJR,HINJ
2	STMIN2,STOUT2,MINJR2,HINJ2

The format for all lines is: (6f12.4)

PFCVAX The statement:

```
open(unit=6,file='flen.ame',status='old')
```

must be used. An example of this file (British units) is given in Appendix D.

MFE Crays For these machines, the statement:

```
call link("unit6=filename,read6//")
```

must be used in the same location as the CALL LINK statement for the first input data file.

3.2.6 Torus Fire

The following are the variable listing and the formats for the torus fire option. (British units are given in the Glossary).

line	variables
1	VS,CHS,PASZER,TGSZER,TSSZER,TFSZER
2	CRACK,HUM2,WO2S,WAS,CPAS,WCO2S
3	TEHCZS,XMEHCS,AEHCS,CPEHCS,HINECS,KEHCS
4	ESTLWS,CPSWS,KSTLWS,RHSWS,AWS,THWS
5	ESTLFS,CPSFS,KSTLFS,RHSFS,AFS,THFS
6	CLEHCS,EEHCS,EBLI,EFWI,VIEWM
7	TSHLZ,THSHL,KSHL,XMSHL,CPSHL,ASHL
8	ESHL,HINSHL,TMAGZ,AMAG,XMMAG,CPMAG
9	HINMAG,KHE,THE,LOCA,VIEWG,VIEWB
10	KBLI,THBLI,CPBLI,ABLI,XMBLI,TBLIO
11	TSHIO,TSHOO,THSHI,THSHO,XMSHI,XMSHO
12	THMAN,XMMAN,CPMAN,AMAN,TMANO,KMAN
13	QOFW1,EXPFW1,QOFW2,EXPFW2,QOFW3,EXPFW3
14	QOBL1,EXPBL1,QOBL2,EXPBL2,QOBL3,EXPBL3
15	QOBL4,EXPBL4,QOBL5,EXPBL5,QOBL6,EXPBL6
16	QOBLI1,EXPBI1,QOBLI2,EXPBI2,QOBLI3,EXPBI3
17	QOSH1,EXPSH1,QOSH2,EXPSH2,QOSH3,EXPSH3
18	QOSHI1,QOSHI2,QOSHI3,QOSHO1,QOSHO2,QOSHO3

The format for lines 1-12 is: (6f12.4)

The format for lines 13-18 is: (6e9.2)

PFCVAX If this option is used, the statement:

```
open(unit=7,file='flen.ame',status='old')
```

must be included in LITFIRE in the same place as the OPEN statement for the first input data file.

MFE Crays For these machines, the statement:

```
call link("unit7=filename,read7//")
```

must be used in the same location as the CALL LINK statement for the first input data file.

3.3 PFCVAX Execution

To execute LITFIRE on the PFCVAX, the user must ensure that all necessary OPEN statements are included for the data files necessary to run the code as indicated in Section 3.2. The input data file *head.dat* must always be included as it provides headings for the output data files that LITFIRE will create. The statement necessary to include *head.dat* is:

```
open(unit=1,file='head.dat',status='old')
```

It should be noted that all input data files must be in the same directory as LITFIRE in order to execute the code.

OPEN statements are also needed for the output files created by LITFIRE. These statements are placed right after the OPEN statements for the input data files and take the form of:

```
open(unit=10,file='out1.dat',status='new')
```

There are ten output data files named *out1.dat* through *out10.dat*, and an OPEN statement is needed for each one.

Optional output files may be created to allow graphs to be made of code variables vs. time. These files may be used in conjunction with the graphics routines available on the PFCVAX to create the actual graphs. The optional files require OPEN statements like the ones for *out1.dat* through *out10.dat*, but use the filename *for0nn.dat*, where *nn* is any number from 01 to 99. Steps must be added to the code in the output section to write values of TIME and the variable desired to the file. Some optional output file OPEN and WRITE statements which have been commented out may be found in the appropriate sections of the code. The output files created may be used with the McCool graphics routine available on the PFCVAX to create the graphs.

There are three separate steps involved in the execution of LITFIRE: compiling, linking and running the code.

To compile LITFIRE, the command:

for litfire.for

must be used and will create the file *litfire.obj*.
To link LITFIRE, the command:

link litfire.obj

must be used and will create the file *litfire.exe*.
To run LITFIRE, the command:

run litfire.exe

must be used. If the input data files were entered properly, the code should run until terminated by a user defined time limit (i.e., TIME=TIMEF) or by the code itself. (e.g., 'the temperature of the lithium pool has reached the melting point'). If the code stops due to an error, an error message will be given. Refer to Appendix C—Troubleshooting.

3.4 MFE Crays Execution

To execute LITFIRE on the Crays, the necessary CALL LINK statements must be present for all of the input data files as indicated in Section 3.2 The input data file *head.dat* must be included to provide headings for the output data files that LITFIRE will create. The statement needed to include *head.dat* is:

call link("unit1=head.dat,read1//")

CALL LINK statements are needed for the ten output files as well. Those statements take the form of:

call link("unit10=(out1,text,create),print1//")

for each of the ten output files *out1* through *out10*. They should be placed directly after the CALL LINK statements for the input data files.

To compile, load and run LITFIRE on the Crays, the following commands should be used:

rcft†i=litfire,x=xlitfire / t p
xlitfire / t p

where *t* is the total CPU time allowed in minutes and *p* sets the priority of the run. One minute and a priority of 2 should be sufficient to run *xlitfire* unless the steam option is being used, in which case up to five minutes may be required (and the priority would be 10).

†: on the *b* machine, *civic* should be used instead of *rcft*.

3.5 Sample Input and Output Files

To check whether LITFIRE has been properly executed, a set of sample input and output files are given in Appendices D and E. Execution of the code using the sample input files on the PFCVAX or the Crays will produce approximately the same results as given in the sample output files.

Using the input data files:

head.dat, uwmak.w, uwmak.x, uwmak.y, uwmak.z, steamop., torus.,

the following output files should be generated:

*out1.dat, out2.dat, out3.dat, out4.dat, out5.dat, out6.dat, out7.dat, out8.dat
out9.dat, out10.dat, blank*

It should be noted that only the input files *head.dat, uwmak.w* and *uwmak.x* were used for the examples in the Appendices.

A Nomenclature

A	heat transfer surface areas
C	user defined heat transfer correlation constant
c_p	specific heat
c_{v_a}	specific heat at constant volume
f	radiative interchange factor, including emissivity
ΔH	heat of combustion
h	convective heat transfer coefficient
h_m	convective mass transfer coefficient
k, k_j	thermal conductivity
$L, l_{i,j}$	characteristic length
M, m	mass
q'''	decay heat density
$Q, dq/dt$	heat flow rate
$R_{i,j}$	thermal resistance
RR	reaction rate
t	time
T	temperature
u	specific internal energy
U_v	total internal energy
x	linear distance
α	thermal diffusivity
β	coefficient of volumetric expansion
ρ	density
σ	Stefan-Boltzmann constant

B Variable Listing

AA	Exponent used in expression for GRPR or GRPRF
ABLI	Cross sectional area of the blanket back wall (ft ²)
ACTVTY	Calculates activity of lithium in lithium-lead eutectic
AEHCP	Surface area of primary extraneous heat capacity (ft ²)
AEHCS	Surface area of secondary extraneous heat capacity (cross sectional area of breeder with torus fire option) (ft ²)
AFP	Surface area of primary floor liner, must be equal to or greater than the area of the lithium spill ASLI. (ft ²)
AFS	Surface area of the secondary floor liner (ft ²)
AHT	Area of the lithium pool-pan interface (ft ²)
AINS	Outside exposed area of insulating layer on the pan (ft ²)
AIRFAC	Density weighting factor for calculating steam-air mixture properties
AK1	Product of thermal conductivity and Prandtl number of the primary gas (BTU/sec-ft deg. F.) See associated film temperature T1.
AKEXX	Function used to calculate heat transfer coefficients
AKLEAD	Thermal conductivity of lead (input as BTU/hr-ft deg. F.)
AKLI	Thermal conductivity of lithium (input as BTU/hr-ft deg. F.)
AKLIX	Thermal conductivity of lithium used during LC-2 lithium transfer simulation (BTU/sec-ft-deg. F.)
AKVAP	Product of thermal conductivity and Prandtl number of water vapor at the lithium pool surface (BTU/sec-ft deg. F.)
ALLOYI	Initial atom percent of lithium in lithium-lead
ALPHA	Used to determine whether or not LILP should be fixed at an amount equal to AKLI/(RHLI*CPLI)
ALPHA2	Used in determining PYU. Also tests conduction limit on time step for the pan or floor liner.
AMAG	Surface area of the magnets (secondary extraneous heat capacity) (ft ²)
AMAN	Cross sectional area of the blanket manifold (ft ²)
AMIN1	FORTTRAN function that determines the minimum of the arguments used
APAN	Pan external heat transfer area (ft ²)
ASHL	Outer surface area of the reactor shield (ft ²)
ASLI	Surface area of the lithium spilled (ft ²)
ASURF	Surface area of the liquid water pool (ft ²)
AWP	Surface area of the primary wall liner (ft ²)
AWS	Surface area of the secondary wall liner (ft ²)
B	Used in calculating the thermal resistance between the wall liner, the gap and the wall concrete
BB	Analogous to B, but for the floor liner, gap and concrete
B1	Coefficient of volumetric expansion for gas (β) (1/deg. F.) See associated film temperature T1

BETA	Inverse sticking coefficient for particles impinging on the wall (sec.)
BETAB	Volumetric expansion coefficient β for the water pool-gas boundary (1/deg. F.)
BETAF	Volumetric expansion coefficient β for the water pool (1/deg. F.)
BIL	Fractional change between BILGE and DELT, used in determining minimum time step
BILGE	Equal to the minimum value of DT1,DT2,DT3,DT4 or DT5, used in calculating the time step length (sec.)
BLIN	Time after spill at which inert gas flooding and exhaust begins (sec.)
BLOUT	Time after spill at which inert gas flooding and exhaust ends (sec.)
BLOWR	Inert gas input rate (lbm/sec)
BLOWV	Inert gas volumetric input rate (ft ³ /sec)
BREAKS	Outer cell gas temperature rate of change due to gas flow between cells and leakage. (deg. R./sec)
BREDTH	Perimeter of the pan (ft)
Cxxx	'C' is used to indicate a thermal admittance between nodes (i.e., the inverse of the product of effective thermal resistance between the nodes and the heat capacity of one of them (hA/mc_p) (sec ⁻¹))
C1	Primary gas to primary wall liner in gas
C2	Pan to primary gas in gas
C3	Wall liner to concrete in concrete
C4(i)	Concrete wall node i to node i+1 in concrete
C5	Concrete wall to ambient in concrete
C6	Primary gas to primary wall in wall liner
C7	Wall liner to concrete in wall liner
C8	Floor liner to concrete floor in floor liner
C9	Floor liner to concrete floor in concrete
C10(i)	Concrete floor node i to node i+1 in concrete
C11	Wall liner to ambient (no concrete option) in wall liner
C12	Floor liner to ambient (no concrete option) in floor liner
C13	Pan to primary gas in pan
C14	Secondary floor liner to secondary gas in floor liner
C15	Secondary floor liner to secondary gas in gas
C16	Primary floor liner to primary gas in floor liner
C17	Primary floor liner to primary gas in gas
C18	Primary floor liner to secondary gas in floor liner
C19	Primary floor liner to secondary gas in gas
C20	Primary wall liner to secondary gas in wall liner
C21	Secondary wall liner to secondary gas in wall liner
C22	Primary wall liner to secondary gas in gas
C23	Secondary wall liner to secondary gas in gas
C2FAC	Fraction of Li-CO ₂ reaction which produces Li ₂ C ₂
CA	Coefficient in expression for GRPR or GRPRF
'C'BIMAN	Blanket back wall to manifold in manifold

'C'BLMAN	Breeder to manifold in manifold
CCZ	Heat generation rate in the combustion zone (BTU/sec)
'C'CZP	Lithium pool to combustion zone in pool
CD	Coefficient of discharge between the two cells (near unity)
'C'EHC GP	Primary extraneous heat capacity to primary gas in gas
'C'EHC GS	Secondary extraneous heat capacity to secondary gas in gas
'C'EHC SH	Blanket back wall to shield inside region in shield inside region
'C'EHC FP	First wall (floor) to breeder in first wall (floor)
'C'EHC WP	First wall to breeder in first wall
'C'FPEHC	First wall (floor) to breeder in breeder
'C'GCZ	Combustion zone to primary gas in combustion zone
'C'GLI	Lithium Pool to primary gas (no combustion) in pool
'C'GPEHC	Primary gas to primary extraneous heat capacity in heat capacity
'C'GSEHC	Secondary gas to secondary extraneous heat capacity in heat capacity
'C'GSMAG	Secondary gas to magnets in magnets
'C'GSSHL	Shield outside region to secondary gas in shield outside region
CHP	Primary cell optical path length (ft)
CHS	Secondary cell optical path length (ft)
'C'IN1PN	Pan to inner insulation in insulation
'C'IN12	Inner pan insulation to outer pan insulation in inner insulation
'C'IN21	Inner pan insulation to outer pan insulation in outer insulation
CLEHCS	Thickness of the breeder node (ft)
'C'LIG	Lithium pool to primary gas (no combustion) in gas
'C'LIPAN	Lithium pool to pan in pool (suspended pan option)
'C'LIST	Lithium pool to primary floor liner in pool
'C'MAGGS	Magnets to secondary gas in secondary gas
'C'MANBI	Manifold to blanket back wall in blanket back wall
'C'MANBL	Manifold to breeder in breeder
CMBR	Total combustion rate (lb Li/sec-ft ²)
CMBRC2	Combustion rate for the carbon reaction (lb Li/sec-ft ²)
CMBRCO	Combustion rate for the lithium-carbonate producing reaction (lb Li/sec-ft ²)
CMBRH	Total combustion rate (lb Li/hr-ft ²)
CMBRHH	CMBRH in g Li/min-cm ²
CMBRHI	Initial combustion rate (lb Li/hr-ft ²)
CMBRN	Combustion rate for the nitrogen reaction (lb Li/sec-ft ²)
CMBRNH	CMBRN in g Li/min-cm ²
CMBRO	Total of CMBRO1 and CMBRO2 (lb Li/sec-ft ²)
CMBRO1	Combustion rate for the oxygen reaction (lb Li/sec-ft ²)
CMBRO2	Combustion rate for the Li-CO ₂ reaction producing lithium-oxide (lb Li/sec-ft ²)
CMBROH	CMBRO in g Li/min-cm ²
CMBRW	Combustion rate for the water vapor reaction producing LiOH (lb Li/sec-ft ²)

CMBRW2 Combustion rate for the water vapor reaction producing Li_2O
 (lb Li/sec-ft²)
 CMBRWH CMBRW in g Li/min-cm²
 CMRC2H CMBRC2 in g Li/min-cm²
 CMRCOH CMBRO2 in g Li/min-cm²
 CO2 A subroutine which sets up the pure CO_2 atmosphere
 CO2LFS Carbon dioxide left after spray fire (lb)
 CONDR Condensation mass flow rate (lb/sec)
 CONF1 Fraction of Li- CO_2 reaction which produces Li_2O
 CONF2 Fraction of Li- CO_2 reaction which produces Li_2CO_3
 CPxxx Gaseous specific heats are all specific heats at constant volume
 CPA Primary non-condensable gas specific heat (BTU/lb deg. F.)
 CPA2 Secondary non-condensable gas specific heat (BTU/lb deg. F.)
 CPAB Flooding gas specific heat (BTU/lb deg. F.)
 'C'PANLI Lithium pool to pan in pan
 CPAP Specific heat of primary cell inert gas (BTU/lb deg. F.)
 CPAS Specific heat of secondary cell inert gas (BTU/lb deg. F.)
 CPB Specific heat of the water pool-gas boundary (BTU/lb deg. F.)
 CPBLI Specific heat of the blanket back wall (BTU/lb deg. F.)
 CPCARP Specific heat of carbon in the primary gas (BTU/lb deg. F.)
 CPCO2P Specific heat of carbon dioxide in the primary gas (BTU/lb deg. F.)
 CPCO2S Specific heat of carbon dioxide in the secondary gas (BTU/lb deg. F.)
 CPCON Heat capacity of floor and wall concrete (BTU/lb deg. F.)
 'C'PCZ Lithium pool to combustion zone in combustion zone
 CPEHCP Specific heat of primary extraneous heat capacity (BTU/lb deg. F.)
 CPEHCS Specific heat of secondary extraneous heat capacity (breeder with
 torus fire option) (BTU/lb deg. F.)
 CPFAC Used in calculating CPLI (CPFAC=.004938^{TLI}-6.20741)
 CPH2 Specific heat of hydrogen gas (2.48 BTU/lb deg. F.)
 CPINS Specific heat of insulation (BTU/lb deg. F.)
 CPLC2P Specific heat of lithium carbide in the primary gas (BTU/lb deg. F.)
 CPLC3P Specific heat of Li_2CO_3 in the primary gas (BTU/lb deg. F.)
 CPLC3S Specific heat of Li_2CO_3 in the secondary gas (BTU/lb deg. F.)
 CPLEAD Specific heat of pure lead (BTU/lb deg. F.)
 CPLI Specific heat of lithium (BTU/lb deg. F.)
 CPLIX Specific heat of lithium (used during LC-2 lithium transfer
 simulation (BTU/lb deg. F.))
 CPLIH Specific heat of lithium hydroxide (0.67 BTU/lb deg. F.)
 CPLIN Specific heat of lithium nitride (BTU/lb deg. F.)
 CPLINP Specific heat of lithium nitride in primary (BTU/lb deg. F.)
 CPLINS Specific heat of lithium nitride in secondary (BTU/lb deg. F.)
 CPLIO Specific heat of lithium oxide (BTU/lb deg. F.)
 CPLIOH Molar specific heat of lithium hydroxide (BTU/lb-mol deg. F.)
 CPLIOP Specific heat of lithium oxide in primary (BTU/lb deg. F.)

CPLIOS	Specific heat of lithium oxide in secondary (BTU/lb deg. F.)
CPLIPB	Specific heat of lithium-lead (BTU/lb deg. F.)
CPLV	Specific heat of water for secondary floor liner-secondary water pool heat transfer (at TAVE) (BTU/deg. F.)
CPMAG	Specific heat of the magnets (secondary extraneous heat capacity) (BTU/lb deg. F.)
CPMAN	Specific heat of the manifold (BTU/lb deg. F.)
CPMCOP	Heat capacity of carbon dioxide in primary (BTU/deg. F.)
CPMCOS	Heat capacity of carbon dioxide in secondary (BTU/deg. F.)
CPMCZ	Effective heat capacity of combustion zone (BTU/deg. F.)
CPMH2	Heat capacity of hydrogen in containment (BTU/deg. F.)
CPMLCP	Heat capacity of lithium carbonate in primary (BTU/deg. F.)
CPMLCS	Heat capacity of lithium carbonate in secondary (BTU/deg. F.)
CPMLOP	Heat capacity of lithium oxide in primary (BTU/deg. F.)
CPMLOS	Heat capacity of lithium oxide in secondary (BTU/deg. F.)
CPMNIP	Heat capacity of nitrogen in primary (BTU/deg. F.)
CPMNIS	Heat capacity of nitrogen in secondary (BTU/deg. F.)
CPMOXP	Heat capacity of oxygen in primary (BTU/deg. F.)
CPMOXS	Heat capacity of oxygen in secondary (BTU/deg. F.)
'C'PNIN1	Pan to inner insulation in pan
CPN2P	Specific heat of nitrogen gas in primary (BTU/lb deg. F.)
CPN2S	Specific heat of nitrogen gas in secondary (BTU/lb deg. F.)
CPSFP	Specific heat of primary floor liner (BTU/lb deg. F.)
CPSFS	Specific heat of secondary floor liner (BTU/lb deg. F.)
CPSHL	Specific heat of the reactor shield (BTU/lb deg. F.)
CPSWP	Specific heat of primary wall liner (BTU/lb deg. F.)
CPSWS	Specific heat of secondary wall liner (BTU/lb deg. F.)
CPWV	Specific heat of water vapor in primary (BTU/lb deg. F.)
CRACON	Area of concrete exposed to lithium in concrete combustion model (ft ²)
CRACK	Area of the orifice between the two cells (square inches)
'C'SBLI	Lithium pool to primary floor liner in floor liner
'C'SHEHC	Blanket back wall to shield inside region in blanket back wall
'C'SHISH	Shield bulk to shield inside region in shield bulk
'C'SHLGS	Shield outside region to secondary gas in secondary gas
'C'SHOSH	Shield bulk to shield outside region in shield bulk
'C'SHSHO	Shield bulk to shield outside region in shield outside region
'C'SHSHI	Shield bulk to shield inside region in shield inside region
CSTM	Steam catalytic factor
CSTMA	Steam catalytic factor in air
CSTMN	Steam catalytic factor in nitrogen
DAB	Diffusion coefficient for air and water (ft ² /sec)
DCOCZ	Depth of concrete combustion zone (ft) used to calculate volume of zone for heat generation
DECBL	Total decay heat density in the breeder (BTU/ft ³ sec)

DECBLI Total decay heat density in the blanket back wall (BTU/ft³ sec)
 DECFW Total decay heat density in the first wall (BTU/ft³ sec)
 DECMAN Total decay heat density in the manifold (BTU/ft³ sec)
 DECSH Total decay heat density in the shield bulk (BTU/ft³ sec)
 DECSHI Total decay heat density in the shield inside region (BTU/ft³ sec)
 DECSHO Total decay heat density in the shield outside region (BTU/ft³ sec)
 DELMP Fractional exchange rate of primary gas used in determining the minimum time step (sec)
 DELMS Fractional exchange rate of secondary gas used in determining the minimum time step (sec)
 DELOUT User defined maximum time step length (sec)
 DELT Time step length (sec)
 DFILM Lithium vapor film thickness (ft)
 DFLIPB Diffusion coefficient for lithium through lead (ft²/sec)
 DFLVAR Constant used to calculate DFLIPB (6.5E-08) (ft²/sec)
 DIFF Gas mass diffusion coefficient to the combustion zone (ft²/sec)
 DIFFLI Lithium diffusion coefficient to the combustion zone (ft²/sec)
 DMPBDT Mass rate of change of lead in lead layer (lb/sec)
 DP1,..DP3 Increase in cell gas pressure due to each injection (psi)
 DTBDT(i) Concrete floor temperature rate of change, node i (deg. F./sec)
 DTCDT(i) Concrete wall temperature rate of change, node i (deg. F./sec)
 DTMIN User defined minimum time step length (sec)
 DT1..DT5 $X/(dx/dt) * RELERR$, used in determining the time step length (sec)
 DT1 X = Lithium pool temperature
 DT2 X = Primary gas temperature
 DT3 X = Primary wall liner temperature
 DT4 X = Combustion rate
 DT5 X = Combustion zone temperature*.05
 DYNAMI Subroutine used in controlling integration loops
 D1 Kinematic viscosity of the cell gas (squared) at the film temperature (ft⁴/sec²), See related film temperature T1.
 EBLI Thermal emissivity of the interior of the blanket
 EEHCS Thermal emissivity of the exterior of the blanket (facing the shield)
 EFWI Thermal emissivity of the interior of the first wall
 EFILM Film depth of depleted zone above combustion zone (in)
 EMCONC Thermal emissivity of concrete
 EMCZ Thermal emissivity of combustion zone
 EMF Used in fixing minimum emissivity of the lithium pool (.9 in code)
 EMGP Thermal emissivity of primary gas (minimum of .005 in code)
 EMGPF Constant used in determining EMGP, usually chosen at .04
 EMGS Thermal emissivity of secondary gas (minimum of .005 in code)
 EMINS Thermal emissivity of pan insulation

(There is no page 38.)

EMLI	Thermal emissivity of lithium pool
ESCR	Heat removal rate by emergency space cooling (BTU/sec)
ESCTIN	Time after spill when ESCR begins (sec)
ESHL	Thermal emissivity of the reactor shield
ESTAIR	Thermal emissivity of the cell steam-air mixture (without aerosols)
ESTLFP	Thermal emissivity of the primary floor liner
ESTLFS	Thermal emissivity of the secondary floor liner
ESTLWP	Thermal emissivity of the primary wall liner
ESTLWS	Thermal emissivity of the secondary wall liner
EW1	Thermal emissivity of water vapor at one atmosphere and cell temperature
EXHSTR	Rate of primary gas exhaust (lb/sec)
EXHSTV	Rate of primary gas exhaust (ft ³ /sec)
EXPBIn	Decay constant of decay heat producing isotope in the blanket back wall (n=1-3) (sec ⁻¹)
EXPBLn	Decay constant of decay heat producing isotope in the breeder node (n=1-3) (sec ⁻¹)
EXPBLn	Decay constant of decay heat producing isotope in the manifold (n=4-6) (sec ⁻¹)
EXPSHn	Decay constant of decay heat producing isotope in the reactor shield (n=1-3) (sec ⁻¹)
EXX	Temporary variable used in calculating heat and mass diffusion coefficients (ft ⁻³)
EX1	Used in calculating mass and heat transfer coefficients (ft ⁻¹) See related film temperature T1.
FCO2P	Weight fraction of CO ₂ in primary gas
FCO2S	Weight fraction of CO ₂ in secondary gas
FCT1,FCT2	Fraction of nitrogen in each injection (by number)
FCT3	
FF1,FF2	Used in heat balance equations for spray fire
FLI2O	Mass fraction of Li reacting with H ₂ O that produces Li ₂ O
FLIOH	Mass fraction of Li reacting with H ₂ O that produces LiOH
FMLEAK	Fraction of mass of gas leaked out of primary
FMLEFT	Fraction of mass of gas remaining in containment
FNIP	Weight fraction of nitrogen in primary gas
FNIS	Weight fraction of nitrogen in secondary gas
FOUTP	Loss rate of primary gas which is either exhausted or changes cells
FOUTS	Loss rate of secondary gas which is either exhausted or changes cells
FOUTT	Total loss rate from outermost gas cell (FOUTS+LEAK)
FOXP	Weight fraction of oxygen in primary gas
FOXS	Weight fraction of oxygen in secondary gas
FPG	Radiative view factor from lithium pool to primary gas (1.0 w/o pan)
FPW	Radiative view factor from lithium pool to primary wall liner
FRA	Fraction of combustion products evolved into cell gas

FWAP	Weight fraction of water vapor in primary gas
FWAS	Weight fraction of water vapor in secondary gas
GAP	Air gap between floor liner and concrete (ft)
GAMMA	Ratio of specific heats c_p/c_v (set to 1.4 in the code)
GIN	Acceleration due to gravity (32.2 ft/sec ²)
GRPR	Product of the Grashof and Prandtl numbers of the water pool-gas boundary
GRPRF	Product of the Grashof and Prandtl numbers of the water pool
H2LEFT	Current water content of concrete (lb/ft ³)
HA	Heat transfer coefficient between exterior wall and ambient (BTU/ft ² sec deg. F.)
HAMF	Heat transfer coefficient between exterior floor and ambient (BTU/ft ² sec deg. F.)
HB	Heat transfer coefficient between lithium pool and primary gas (BTU/ft ² sec deg. F.)
HBINF	Equilibrium value of HB
HCOND	Total heat transfer coefficient between the water pool and the cell gas (BTU/ft ² sec deg. F.)
HEHCP	Heat transfer coefficient between primary extraneous heat capacity and primary gas (BTU/ft ² sec deg. F.)
HEHCS	Heat transfer coefficient between secondary extraneous heat capacity and secondary gas (BTU/ft ² sec deg. F.)
HEVAP	Heat flux to water pool from gas mixture due to evaporation (BTU/sec-ft ²)
HF	Mass transport coefficient to the lithium pool (ft/sec)
HFG	Latent heat of vaporization of water vapor in the primary gas (BTU/lb)
HFG2	Latent heat of vaporization of water vapor in the secondary gas (BTU/lb)
HFINF	Equilibrium value of HF (BTU/ft ² sec deg. F.)
HFPGP	Heat transfer coefficient between primary floor liner and primary gas (BTU/ft ² sec deg. F.)
HFPGAS	Heat transfer coefficient between primary floor liner and secondary gas (BTU/ft ² sec deg. F.)
HFSGAS	Heat transfer coefficient between secondary floor liner and secondary gas (BTU/ft ² sec deg. F.)
HGWP	Heat transfer coefficient between primary wall and gas (BTU/ft ² sec deg. F.)
HINxxx	Heat transfer coefficients are determined by LITFIRE as indicated in Section 2.2.4. The coefficients C are indicated in the code as HINxxx and are dimensionless
HINECP	Correlation for HEHCP
HINECS	Correlation for HEHCS
HINFAM	Correlation for HAMF
HINFGS	Correlation for HFPGAS
HINFGS	Correlation for HFSGAS
HINGPF	Correlation for HFPGP

HINGSP	Correlation for HGWP
HINGSS	Correlation for HSEC
HINJ	Specific enthalpy of steam injected to primary cell (BTU/lb)
HINJ2	Specific enthalpy of steam injected to secondary cell (BTU/lb)
HINMAG	Correlation for HMAG
HINPS	Correlation for HWPGAS
HINSAM	Correlation for HA
HINSHL	Correlation for HSHL
HLP	Specific enthalpy of the primary liquid water pool (BTU/lb)
HLP2	Specific enthalpy of the secondary liquid water pool (BTU/lb)
HLPFLR	Heat transfer coefficient between the liquid water pool and the secondary floor liner (BTU/ft ² sec deg. F.)
HMAG	Heat transfer coefficient between magnets and secondary gas (BTU/ft ² sec deg. F.)
HPAN	Heat transfer coefficient between the pan and primary gas (BTU/ft ² sec deg. F.)
HPRIME	Increased value of HSENS due to a large condensation/evaporation rate (BTU/ft ² sec deg. F.)
HRATIO	Molar fraction of hydrogen in the primary gas
HRAT2	Molar fraction of hydrogen in the secondary gas
HSAT	Specific enthalpy of saturated liquid water at cell pressure (BTU/lb)
HSEC	Heat transfer coefficient between secondary floor liner and secondary gas (BTU/ft ² sec deg. F.)
HSENS	Sensible heat transfer coefficient from the water pool to the vapor mixture (BTU/ft ² sec deg. F.)
HSHL	Heat transfer coefficient between the shield outside region and secondary gas (BTU/ft ² sec deg. F.)
HTCPGP	Heat capacity of the primary gas (BTU/deg. F.)
HTCPGS	Heat capacity of the secondary gas (BTU/deg. F.)
HU(x,y)	Chart of Uchida heat transfer coefficients vs. MR
HUCH	Uchida heat transfer coefficient for condensing steam (BTU/ft ² sec deg. F.)
HUM	Initial relative humidity of the primary cell (1.0=100%)
HUM2	Initial relative humidity of the secondary cell (1.0=100%)
HWPGAS	Heat transfer coefficient between primary wall liner and secondary gas (BTU/ft ² sec deg. F.)
HWV	Specific enthalpy of water vapor in the primary gas (BTU/lb)
HWV2	Specific enthalpy of water vapor in the secondary gas (BTU/lb)
I	General purpose DO loop counter
IAM	DO loop counter for wall and floor concrete node initialization
IB	DO loop counter for floor concrete iterations
INIT	Initializing subroutine for integrations
INJEC1..3	Flags for gas injection. INJEC _n indicates the injection has occurred.

INTDSx	Interpolation factor used in reading steam tables
INTGRL	Arithmetic statement function for finding integrals
IPAGE	Number of lines of output between headings
IPASS	Used during integration routine to tell INTGRL to perform certain special functions during the first two executions of the section
KAIR	Thermal conductivity of non-condensable gas (air) (BTU/sec ft deg. F.)
KAIRB	Thermal conductivity of air at the water pool-gas boundary (BTU/sec ft deg. F.)
KAIRG	Thermal conductivity of air in a cell gas (BTU/sec ft deg. F.)
KB	Water condensation mass transfer coefficient (lb mol/sec-ft ²)
KBLI	Thermal conductivity of the blanket back wall (BTU/hr ft deg. F.)
KBNDRY	Thermal conductivity of the water pool-gas boundary (BTU/sec ft deg. F.)
KCON	Thermal conductivity of concrete (input as BTU/hr ft deg. F.)
KEHCS	Thermal conductivity of the breeder node (BTU/hr ft deg. F.)
KFILM	Thermal conductivity of pool/combustion zone film (BTU/sec ft deg. F.)
KGAP	Thermal conductivity of the gap between the liner and concrete (BTU/hr ft deg. F.)
KH2O	Thermal conductivity of water vapor (BTU/sec ft deg. F.)
KH2OB	Thermal conductivity of water vapor at the water pool-gas boundary (BTU/sec ft deg. F.)
KH2OG	Thermal conductivity of water vapor in a cell gas (BTU/sec ft deg. F.)
KHE	Thermal conductivity of the vacuum (He filled) gap (BTU/hr ft deg. F.)
KIN1	Thermal conductivity of inner insulation layer (BTU/hr ft deg. F.)
KIN2	Thermal conductivity of outer insulation layer (BTU/hr ft deg. F.)
KLEAK	Leak rate constant from containment (sec ⁻¹ psi ^{-0.5}) Reference value: 2.588·10 ⁻⁹
KMAN	Thermal conductivity of the manifold (BTU/hr ft deg. F.)
KPAN	Thermal conductivity of the pan (BTU/hr ft deg. F.)
KSHL	Thermal conductivity of the reactor shield (BTU/hr ft deg. F.)
KSTLFP	Thermal conductivity of the primary floor liner (BTU/hr ft deg. F.)
KSTLFS	Thermal conductivity of the secondary floor liner (BTU/hr ft deg. F.)
KSTLWP	Thermal conductivity of the primary wall liner (BTU/hr ft deg. F.)
KSTLWS	Thermal conductivity of the secondary wall liner (BTU/hr ft deg. F.)
KWAT	Thermal conductivity of liquid water (BTU/sec ft deg. F.)
L	Thickness of a wall concrete node (ft)
L1	Thickness of a floor concrete node (ft)
LEAK	Gas leakage rate from outermost cell (sec ⁻¹)
LEAKO	Initial gas leakage rate from outermost cell (sec ⁻¹)
LIBP	Lithium consumed in pool fire (lb)
LIL	Amount of lithium remaining in pool—limited to LIT/10 for numerical stability during calculations
LILC2	Amount of Li ₂ C ₂ in the pool (lb)
LILCA	Amount of Li ₂ CO ₃ in the pool (lb)

LILCAR	Amount of carbon in the pool (lb)
LILNI	Amount of Li_3N in the pool (lb)
LILOX	Amount of Li_2O in the pool (lb)
LILP	True amount of lithium in the pool (lb)
LIS	Amount of lithium consumed in the spray fire (lb)
LIT	Initial mass of lithium in the pool (lb)
LOCA	View factor between the first wall and the breeder node (may be zero)
MAIP	Initial mass of inert gas in the primary gas (lb)
MAIS	Initial mass of inert gas in the secondary gas (lb)
MAIRP	Mass of primary non-condensable gas (lb)
MAIRS	Mass of secondary non-condensable gas (lb)
MAP	Mass of inert gas in the primary gas (lb)
MAS	Mass of inert gas in the secondary gas (lb)
MBOIL	Mass of water boiled off from the water pool in one time step (lb)
MCO2IP	Initial mass of carbon dioxide in the primary gas (lb)
MCO2IS	Initial mass of carbon dioxide in the secondary gas (lb)
MCO2P	Mass of carbon dioxide in the primary gas (lb)
MCO2S	Mass of carbon dioxide in the secondary gas (lb)
MCONDE	Condensation rate of water on an extraneous heat capacity (lb/sec)
MCONDF	Condensation rate of water on the secondary floor liner (lb/sec)
MCONDP	Condensation rate of water on the pan insulation (lb/sec)
MCONDW	Condensation rate of water on a wall liner (lb/sec)
MCONFP	Condensation rate of water on the primary floor liner from the secondary gas (lb/sec)
MCONWP	Condensation rate of water on the primary wall liner from the secondary gas (lb/sec)
MFAB	Molar fraction of air at the water pool-gas boundary
MFAG	Molar fraction of air in the cell gas
MFVB	Molar fraction of water vapor at the water pool-gas boundary
MFVG	Molar fraction of water vapor in the cell gas
MGB	Molecular weight of the mixture at the water pool-gas boundary
MH2P	Mass of hydrogen in the primary gas (lb)
MH2S	Mass of hydrogen in the secondary gas (lb)
MINJR	Mass flow rate of steam injected to primary cell (lb/sec)
MINJR2	Mass flow rate of steam injected to secondary cell (lb/sec)
MLC2P	Mass of lithium carbide in the primary gas (lb)
MLC2S	Mass of lithium carbide in the secondary gas (lb)
MLC3IP	Initial mass of lithium carbonate in the primary gas (lb)
MLC3IS	Initial mass of lithium carbonate in the secondary gas (lb)
MLC3P	Mass of lithium carbonate in the primary gas (lb)
MLC3S	Mass of lithium carbonate in the secondary gas (lb)
MLEAD	Mass of lead in the lead layer above the lithium-lead pool (lb)
MLIHP	Mass of lithium-hydroxide in the primary gas (lb)
MLIHS	Mass of lithium-hydroxide in the secondary gas (lb)

MLINIP	Initial mass of lithium-nitride in the primary gas (lb)
MLINIS	Initial mass of lithium-nitride in the secondary gas (lb)
MLINP	Mass of lithium-nitride in the primary gas (lb)
MLINS	Mass of lithium-nitride in the secondary gas (lb)
MLIOH	Mass of LiOH produced (moles)
MLIOIP	Initial mass of lithium-oxide in primary gas (lb)
MLIOIS	Initial mass of lithium-oxide in secondary gas (lb)
MLIOP	Mass of lithium-oxide in primary gas (lb)
MLIOS	Mass of lithium-oxide in secondary gas (lb)
MNIINJ	Rate of nitrogen injection during a one minute interval (lb/sec)
MNIIP	Initial mass of nitrogen in the primary gas (lb)
MNIIS	Initial mass of nitrogen in the secondary gas (lb)
MNIP	Mass of nitrogen in the primary gas (lb)
MNIS	Mass of nitrogen in the secondary gas (lb)
MNINJ1..3	Mass of nitrogen injected in gas injection (lb)
MOINJ1..3	Mass of oxygen injected in gas injection (lb)
MOXINJ	Rate of oxygen injection during a one minute interval (lb/sec)
MOXIP	Initial mass of oxygen in the primary gas (lb)
MOXIS	Initial mass of oxygen in the secondary gas (lb)
MOXP	Mass of oxygen in the primary gas (lb)
MOXS	Mass of oxygen in the secondary gas (lb)
MR	Mass ratio of air to water vapor in the cell gas
MUAIR	Viscosity of air in the cell gas (lb/sec-ft)
MUAIRB	Viscosity of air at the water pool-gas boundary (lb/sec-ft)
MUAIRG	Viscosity of air in the cell gas (lb/sec-ft)
MUB	Viscosity of the mixture at the water pool-gas boundary (lb/sec-ft)
MUDIFF	Viscosity of the mixture at the lithium pool surface (lb/sec-ft)
MUV	Viscosity of water vapor in the cell gas (lb/sec-ft)
MUVB	Viscosity of water vapor at the water pool-gas boundary (lb/sec-ft)
MUV CZ	Viscosity of water vapor at the lithium pool surface (lb/sec-ft)
MWL	Mass of liquid water in the primary water pool (lb)
MWL2	Mass of liquid water in the secondary water pool (lb)
MWLV	Mass of liquid water in the primary gas (lb)
MWLV2	Mass of liquid water in the secondary gas (lb)
MWLZ	Time rate of change of the mass of liquid water in the primary water pool (lb/sec)
MWLZ2	Time rate of change of the mass of liquid water in the secondary water pool (lb/sec)
MWV	Total mass of water in the primary gas (lb)
MWV2	Total mass of water in the secondary gas (lb)
MWVV	Mass of water vapor in the primary gas (lb)
MWVV2	Mass of water vapor in the secondary gas (lb)

MWVZ Time rate of change of the total mass of water in the primary gas (lb/sec)
 MWVZ2 Time rate of change of the total mass of water in the secondary gas (lb/sec)
 N Index used to transfer to section of subroutines, and as a DO loop counter
 NAME(i) Input variable containing program name and output headings
 NL Number of concrete wall nodes
 NL1 Number of concrete floor nodes
 NLM1 Number of concrete wall nodes minus one
 NL1M1 Number of concrete floor nodes minus one
 NS Index used to control transfer to sections of the steam-air subroutines
 NULV Kinematic viscosity of water at the secondary floor liner (ft²/sec)
 OFAC Oxygen inhibition factor (lithium-steam reaction)
 OUTINT Fraction of the outermost cell gas leaked to ambient
 OVERPP Primary cell overpressure (psig)
 OVERPS Secondary cell overpressure (psig)
 OXLB Mass of oxygen consumed in the fire (lb)
 OXLBI Mass of oxygen consumed in the spray fire (lb)
 OXLFS Mass of oxygen remaining after the spray fire (lb)
 PAP Primary gas pressure (psia)
 PAPZER Initial primary gas pressure (psia)
 PAS Secondary gas pressure (psia)
 PASZER Initial secondary gas pressure (psia)
 PERCEN Molecular percentage of lithium-peroxide (vs. monoxide) formed during combustion
 PH2O Partial pressure of water vapor in the primary gas (psia)
 PH2O2 Partial pressure of water vapor in the secondary gas (psia)
 PH2OB Partial pressure of water vapor at the primary water pool-gas boundary (psia)
 PH2OB2 Partial pressure of water vapor at the secondary water pool-gas boundary (psia)
 PHASE =1 if primary cell is saturated, =2 if superheated
 PHASE2 =1 if secondary cell is saturated, =2 if superheated
 PHIA Baroczy two-phase flow correction factor at the lithium pool surface
 PHIW Baroczy two-phase flow correction factor at the lithium pool surface
 PHIAWB Baroczy two-phase flow correction factor at the water pool surface
 PHIWAB Baroczy two-phase flow correction factor at the water pool surface
 PLIV Partial pressure of lithium vapor (psia)
 PRSC Prandtl number divided by the Schmidt number
 PSAT Saturation pressure of water at the primary gas temperature (psia)
 PSAT2 Saturation pressure of water at the secondary gas temperature (psia)
 PYU Used in setting the time step length calculated from the heat conduction rate to the pan or primary floor liner from the lithium pool
 PZEROP Primary gas pressure after the spray fire (psia)
 QCxxx Heat of combustion (BTU/lb Li)

(There is no page 46.)

QCC	Li-CO ₂ producing lithium carbonate reaction
QCCONC	Concrete reaction
QCN	Nitrogen reaction
QCO	Oxygen reaction
QCO1	Monoxide reaction
QCO2	Peroxide reaction
QCW	Water vapor reaction producing LiOH
QCW2	Water vapor reaction producing Li ₂ O
QDISS	Heat of dissociation of LiPb (BTU/lb)
QIN	Heat addition to primary gas from spray fire (BTU)
QL2C2	Heat of combustion for the carbon reaction (BTU/lb Li)
QLFLR	Heat flux from the secondary water pool to the secondary floor liner (BTU/ft ²)
QLIOH	Heat of fusion of LiOH (BTU/lb mol)
QOFW _n	Volumetric decay heat generation rate in the first wall for an isotope (n=1-3) (BTU/sec ft ³)
QOBL _n	Volumetric decay heat generation rate in the breeder for an isotope (n=1-3) (BTU/sec ft ³)
QOBL _n	Volumetric decay heat generation rate in the manifold for an isotope (n=4-6) (BTU/sec ft ³)
QOBL _n	Volumetric decay heat generation rate in the blanket back wall for an isotope (n=1-3) (BTU/sec ft ³)
QOSH _n	Volumetric decay heat generation rate in the shield bulk for an isotope (n=1-3) (BTU/sec ft ³)
QOSH _n	Volumetric decay heat generation rate in the inside of the shield for an isotope (n=1-3) (BTU/sec ft ³)
QOSH _{On}	Volumetric decay heat generation rate in the outside of the shield for an isotope (n=1-3) (BTU/sec ft ³)
QOUT1..5	Used in heat balance equations for the spray fire (BTU)
QQQ	Used as a counter in the lithium transfer simulation
QRAD _{xx}	Indicates a radiative heat flow (BTU/sec)
QRADB	Floor liner (or pan) to ambient or floor concrete
QRADC	Wall liner to ambient or wall concrete
QRADCG	Pan to primary gas
QRADEB	Breeder to blanket back wall
QRADEM	Breeder to manifold
QRADES	Blanket back wall to shield inside region
QRADFB	First wall (floor) to breeder
QRADFG	Primary floor liner to secondary gas
QRADFS	Primary floor liner to secondary floor liner
QRADG	Combustion zone (or Li pool without combustion) to primary gas
QRADP	Combustion zone to lithium pool (only during combustion)
QRADPG	Primary wall liner to secondary gas

QRADPS	Primary wall liner to secondary wall liner
QRADS	Pan to primary floor liner
QRADW	Combustion zone (or lithium pool) to primary wall liner
QRADWB	First wall to breeder
QRSHFS	Radiative heat flow from the shield outside region to the secondary floor (BTU/sec)
QRSHGS	Radiative heat flow from the shield outside region to the secondary gas (BTU/sec)
QRSHWS	Radiative heat flow from the shield outside region to the secondary wall (BTU/sec)
QU	Heat flux from the primary gas to primary wall liner due to condensation (BTU/sec-ft ²)
QVAP	Heat of vaporization of lithium (BTU/lb)
QVEHC	Heat flux from the cell gas to the extraneous heat capacity due to condensation (BTU/sec-ft ²)
QVPAN	Heat flux from the primary gas to the pan insulation due to condensation (BTU/sec-ft ²)
QVSEC	Heat flux from the secondary gas to secondary wall liner due to condensation (BTU/sec-ft ²)
QVFLR	Heat flux from the cell gas to cell floor liner due to condensation (BTU/sec-ft ²)
QVFPGS	Heat flux from the secondary gas to primary floor liner due to condensation (BTU/sec-ft ²)
QVWPGS	Heat flux from the secondary gas to primary wall liner due to condensation (BTU/sec-ft ²)
RA	Mean radius of combustion product particles (microns)
RADxxx	'RAD' or 'R' indicates a temperature rate of change in one node due to radiative heat transfer to or from another (deg. F./sec)
'RAD'B	Floor liner to ambient or floor concrete
'RAD'C	Wall liner to ambient or wall concrete
'RAD'CB	Floor concrete from floor liner
'RAD'CC	Wall concrete from wall liner
RAIR	Gas constant for primary non-condensable gas (RIN/XMOLP)
RAIR2	Gas constant for secondary non-condensable gas (RIN/XMOLS)
'R'BFF	Breeder node from first wall (floor)
'R'BFW	Breeder node from first wall
'R'BIEHC	Blanket back wall from breeder
RBREAK	Temperature rate of change of primary gas due to leakage (R/sec)
RC2	Li-CO ₂ reaction rate inhibition factor (Li ₂ CO ₃ reaction)
RC2LB	Rate of carbon consumption (lb/sec)
RCMBC	Stoichiometric combustion ratio for lithium and concrete (lb Li/lb concrete)
RCMBC2	Stoichiometric combustion ratio for lithium and carbon (lb Li/lb C)

RCMBCO	Stoichiometric combustion ratio for lithium and carbon dioxide for lithium carbonate producing reaction (lb Li/lb CO ₂)
RCMBCS	Stoichiometric ratio of lithium consumed in Li ₂ CO ₃ producing reaction to Li ₂ CO ₃ produced (lb Li/lb Li ₂ CO ₃)
RCMBH2	Stoichiometric combustion ratio for lithium and hydrogen (lb Li/lb H)
RCMBN	Stoichiometric combustion ratio for lithium and nitrogen (lb Li/lb N)
RCMBO	Stoichiometric combustion ratio for lithium and oxygen (lb Li/lb O)
RCMBO1	Stoichiometric combustion ratio for monoxide reaction (lb Li/lb O)
RCMBO2	Stoichiometric combustion ratio for peroxide reaction (lb Li/lb O)
RCMBW	Stoichiometric combustion ratio for lithium and water for reaction producing LiOH (lb Li/lb H ₂ O)
RCMBW2	Stoichiometric combustion ratio for lithium and water for reaction producing Li ₂ O (lb Li/lb H ₂ O)
RCMCA1	Stoichiometric ratio of lithium consumed in Li-CO ₂ reaction producing Li ₂ O and carbon to carbon produced (lb Li/lb C)
RCMCA2	Stoichiometric ratio of lithium consumed in Li-CO ₂ reaction producing Li ₂ CO ₃ and carbon to carbon produced (lb Li/lb C)
RCMCCO	Stoichiometric combustion ratio for lithium and carbon dioxide for lithium oxide producing reaction (lb Li/lb CO ₂)
RCOLB	Rate of carbon dioxide consumption (lb CO ₂ /sec)
'R'CZG	Primary gas from combustion zone
'R'CZP	Lithium pool from combustion zone
'R'CZW	Primary wall liner from combustion zone
'R'EHCBI	Breeder from blanket back wall
'R'EHCMN	Breeder from manifold
'R'EHCSH	Blanket back wall from shield inside region
RELERR	Fraction of $X/(dx/dt)$ allowed as the maximum time step (sec)
'R'FFB	First wall (floor) from breeder node
'R'FPFS	Primary floor liner from secondary floor liner
'R'FPGAS	Primary floor liner from secondary gas
'R'FSFP	Secondary floor liner from primary floor liner
'R'FSSH	Secondary floor liner from shield outside region
'R'FWB	First wall from breeder node
'R'GASFP	Secondary gas from primary floor liner
'R'GASPA	Pan to primary gas
'R'GLI	Lithium pool to primary gas (without combustion)
'R'GSSH	Secondary gas from shield outside region
RHCON	Density of concrete (lb/ft ³)
RHINS	Density of insulation (lb/ft ³)
RHLEAD	Density of pure lead (lb/ft ³)
RHLI	Density of pure lithium (lb/ft ³)
RHLIX	Density of pure lithium (used in LC-2 lithium transfer simulation) (lb/ft ³)
RHOAIP	Initial density of primary non-condensable gas (lb/ft ³)

RHOAIS	Initial density of secondary non-condensable gas (lb/ft ³)
RHOAP	Density of primary non-condensable gas (lb/ft ³)
RHOAS	Density of secondary non-condensable gas (lb/ft ³)
RHOB	Density of the water pool-gas boundary layer (lb/ft ³)
RHOCAR	Density of carbon (lb/ft ³)
RHOLC2	Density of Li ₂ C ₂ (lb/ft ³)
RHOLC3	Density of Li ₂ CO ₃ (lb/ft ³)
RHOLIH	Density of LiOH (lb/ft ³)
RHOLIN	Density of Li ₃ N (lb/ft ³)
RHOLIO	Density of Li ₂ O (lb/ft ³)
RHOLIV	Density of lithium vapor above the pool (lb/ft ³)
RHOTOT	Total gas density at the lithium pool surface (lb/ft ³)
RHPAN	Density of lithium spill pan (lb/ft ³)
RHSFP	Density of primary floor liner (lb/ft ³)
RHSFS	Density of secondary floor liner (lb/ft ³)
RHSWP	Density of primary wall liner (lb/ft ³)
RHSWS	Density of secondary wall liner (lb/ft ³)
RIFxxx	Radiative interchange factor—used in radiative heat transfer
RIFBBI	Breeder node to blanket back wall
RIFBM	Breeder node to manifold
RIFCZG	Combustion zone and primary gas
RIFCZP	Combustion zone and primary wall liner
RIFES	Blanket back wall to shield inside region
RIFFFB	First wall (floor) to breeder node
RIFFPS	Primary floor liner and secondary floor liner
RIFFWB	First wall to breeder node
RIFPAG	Pan to primary gas
RIFPAS	Pan to floor liner
RIFPG	Lithium pool to primary gas
RIFPGA	Primary wall liner to secondary gas
RIFPS	Primary wall liner to secondary wall liner
RIFPW	Lithium pool to primary wall liner
RIFSCF	Secondary floor to concrete floor
RIFSCW	Secondary wall to concrete wall
RIFSLC	Wall or floor liner to concrete
RIFSF	Shield outside region to secondary floor
RIFSW	Shield outside region to secondary wall
RIN	Universal gas constant (1545 ft-lbf/lb-mol-deg. F.)
RINP	Gas constant for the primary gas (RIN/XMOLP)
RINS	Gas constant for the secondary gas (RIN/XMOLS)
RISHGS	Radiative interchange factor between the shield outer region and the secondary cell gas
'R'LIG	Gas from lithium pool (without combustion)
'R'LIW	Wall liner from lithium pool (without combustion)

'R'MNEHC	Manifold from breeder
RN2	Lithium-nitrogen reaction rate inhibition factor
RNxx	Expressions used to calculate RN2 as a function of gas composition and lithium temperature
RNILB	Rate of nitrogen combustion (lb/sec)
RO2	Lithium-oxygen reaction rate inhibition factor
ROXLB	Rate of oxygen combustion (lb/sec)
'R'PAGAS	Primary gas from pan
'R'PANST	Primary wall liner from pan
RR	Function which generates the lithium-nitrogen kinetics limit curve
RRTLI	Lithium-nitrogen reaction kinetics limit modified by the presence of steam
'R'SHEHC	Shield inside region from blanket back wall
'R'SHFS	Shield outside region from secondary floor
'R'SHGS	Shield outside region from secondary gas
'R'SHWS	Shield outside region from secondary wall
'R'SPGS	Secondary gas from primary wall liner
'R'STPAN	Pan from primary wall liner
RWALB	Rate of water vapor consumption (lb/sec)
'R'WLI	Lithium pool from primary wall liner (without combustion)
'R'WPGAS	Primary wall liner from secondary gas
'R'WPWS	Primary wall liner from secondary wall liner
'R'WSSH	Secondary wall liner from shield outside region
'R'WSWP	Secondary wall liner from primary wall liner
SAT(x,y)	Saturated steam table
SFLCR	Heat removal rate by emergency cooling of floor liner (BTU/sec)
SFLEND	Time after spill when SFLCR ends (sec)
SFLTIN	Time after spill when SFLCR begins (sec)
SH(x,y,z)	Superheated steam table
SIGMA	Stefan-Boltzmann constant ($1.713 \cdot 10^{-9}$ BTU/ft ² -hr-deg. R. ⁴)
SPILL	Total mass of lithium spilled (lb)
SPRAY	Mass fraction of lithium consumed in the spray fire
STICK	Rate at which aerosols are removed from the primary cell due to sticking to the wall. If STICK > 1.0, execution stops. STICK may be reduced by increasing BETA.
STMFAC	Density weighting factor for calculating steam-air mixture properties
STMIN	Time to begin steam injection to primary cell (sec)
STMIN2	Time to begin steam injection to secondary cell (sec)
STMOUT	Time to end steam injection to primary cell (sec)
STOUT2	Time to end steam injection to secondary cell (sec)
TA	Ambient temperature (deg. R.)
TAU	Time constant for transient natural convection
TAUCZ	Radiative transmissivity used to model pool-combustion zone coupling rather than (1.-EMCZ)

TAVE	Average of secondary floor and secondary water pool temperature (deg. R.)
TAVHI	Variable used to read steam tables
TAVLO	Variable used to read steam tables
TB(i)	Temperature of ith node of concrete floor (deg. R.)
TBIC(i)	Initial temperature of ith node of concrete floor (deg. R.)
TxxxxF	Corresponding temperature to Txxxx in Fahrenheit
TBLI	Temperature of blanket back wall (deg. R.)
TBLIO	Initial temperature of blanket back wall (deg. R.)
TBLOW	Inert gas inlet temperature (deg. R.)
TC(i)	Temperature of ith node of concrete wall (deg. R.)
TCIC(i)	Initial temperature of ith node of concrete wall (deg. R.)
TCIGNI	Ignition temperature of lithium-concrete reaction (deg. R.)
TCON	Concrete combustion zone temperature (deg. R.)
TCZ	Combustion zone temperature (deg. R.)
TCZI	Initial combustion zone temperature (deg. R.)
TE	Equilibrium temperature resulting from spray fire (deg. R.)
TEHCP	Primary extraneous heat capacity temperature (deg. R.)
TEHCS	Secondary extraneous heat capacity (breeder with torus fire option) temperature (deg. R.)
TEHCZP	Initial primary extraneous heat capacity temperature (deg. R.)
TEHCZS	Initial secondary extraneous heat capacity (breeder with torus fire option) temperature (deg. R.)
TET1	Used in calculating thermal conductivity of inner pan insulation See KIN1
TET2	Used in calculating thermal conductivity of outer pan insulation See KIN2
TEZ	Average of combustion zone temperature and lithium pool temperature Used in test for combustion (deg. R.)
TFEFF	Normalized temperature of combustion zone-lithium pool temperature (deg. R.)
TFHI	Variable used to read steam tables
TFLO	Variable used to read steam tables
TFS	Secondary floor liner temperature (deg. R.)
TGP	Primary gas temperature (deg. R.)
TGPZER	Initial primary gas temperature (deg. R.)
TGS	Secondary gas temperature (deg. R.)
TGSZER	Initial secondary gas temperature (deg. R.)
THBLI	Thickness of blanket back wall (ft)
THE	Thickness of vacuum gap (ft)
THFC	Thickness of concrete floor (ft)
THFP	Thickness of primary floor liner (ft)
THFS	Thickness of secondary floor liner (ft)
THI	Temporary variable used to read steam tables

THKIN1 Thickness of inner pan insulation (ft)
 THKIN2 Thickness of outer pan insulation (ft)
 THKPAN Thickness of spill pan (ft)
 THMAN Thickness of blanket manifold (ft)
 THPB Thickness of lead layer above the lithium-lead pool (ft)
 THSHI Thickness of inside region of reactor shield (ft)
 THSHL Thickness of bulk region of reactor shield (ft)
 THSHO Thickness of outside region of reactor shield (ft)
 THWC Thickness of concrete wall (ft)
 THWP Thickness of primary wall liner (ft)
 THWS Thickness of secondary wall liner (ft)
 TIME Time elapsed after spill has occurred (sec)
 TIMEF User defined time to stop execution of the code (sec)
 TIMEO Time at which code prints output data to a file (sec)
 TINS1 Inner pan insulation layer temperature (deg. R.)
 TINS1I Initial inner pan insulation layer temperature (deg. R.)
 TINS2 Outer pan insulation layer temperature (deg. R.)
 TINS2I Initial outer pan insulation layer temperature (deg. R.)
 TLEAD Temperature of the lead layer above the Li-Pb pool (deg. R.)
 TLEADI Initial temperature of the lead layer above the Li-Pb pool (deg. R.)
 TLI Lithium pool temperature (deg. R.)
 TLIBS Lithium pool temperature before spray fire (deg. R.)
 TLII Initial lithium pool temperature (deg. R.)
 TLO Temporary variable used to read steam tables
 TLP Temperature of the primary liquid pool (deg. R.)
 TMAG Temperature of the magnets (secondary extraneous heat capacity) (deg. R.)
 TMAGZ Initial temperature of the magnets (secondary extraneous heat capacity) (deg. R.)
 TMAN Temperature of the blanket manifold (deg. R.)
 TMANO Initial temperature of the blanket manifold (deg. R.)
 TMELT Melting temperature of lithium (deg. R.)
 TO Primary gas temperature before spray fire (deg. R.)
 TONE,TTWO,TTHREE Time at which each injection occurs (sec)
 TPAN Pan temperature (deg. R.)
 TPANZO Initial pan temperature (deg. R.)
 TSAT Saturation temperature of water based on its partial pressure (deg. F.)
 TSFP Primary floor liner temperature (deg. R.)
 TSFPI Initial primary floor liner temperature (deg. R.)
 TSFSI Initial secondary floor liner temperature (deg. R.)
 TSHI Shield inside region temperature (deg. R.)
 TSHIO Initial shield inside region temperature (deg. R.)
 TSHL Shield bulk region temperature (deg. R.)

TSHLZ	Initial shield bulk region temperature (deg. R.)
TSHO	Shield outside region temperature (deg. R.)
TSHOO	Initial shield outside region temperature (deg. R.)
TSP	Primary wall liner temperature (deg. R.)
TSPZER	Initial primary wall liner temperature (deg. R.)
TSS	Secondary wall liner temperature (deg. R.)
TSSZER	Initial secondary wall liner temperature (deg. R.)
TVAP	Vaporization temperature of lithium (deg. R.)
T1	Film temperature between primary gas and lithium pool (deg. R.)
T2,T3	Temporary variables used in setting up steam table
UA	Internal energy of non-condensable gas in a cell (BTU)
UGPB	Specific internal energy of saturated water vapor at boiling (BTU/lb)
UL	Internal energy of the primary water pool (BTU)
UL2	Internal energy of the secondary water pool (BTU)
ULP	Specific internal energy of the primary water pool (BTU/lb)
ULP2	Specific internal energy of the secondary water pool (BTU/lb)
ULPB	Specific internal energy of liquid needed for boiling to occur (BTU/lb)
ULZ	Time rate of change of UL (BTU/sec)
ULZ2	Time rate of change of UL2 (BTU/sec)
USUBA	Heat transfer coefficient between the outermost containment node and the ambient (BTU/sec-ft ² -deg. F.)
UV	Internal energy of the primary gas (BTU)
UV2	Internal energy of the secondary gas (BTU)
UVZ	Time rate of change of the internal energy of the primary gas (BTU/sec)
UVZ2	Time rate of change of the internal energy of the secondary gas (BTU/sec)
UWV	Specific internal energy of water vapor in the primary gas (BTU/lb)
UWV2	Specific internal energy of water vapor in the secondary gas (BTU/lb)
VA	Specific volume of non-condensable primary gas (ft ³ /lb)
VAB	Specific volume of non-condensable gas at the water pool-gas boundary (ft ³ /lb)
VCONC	Volume of concrete in the first node of concrete (ft ³)
VG	Specific volume of water in the primary gas (ft ³ /lb)
VG2	Specific volume of water in the secondary gas (ft ³ /lb)
VHI	Variable used to read steam tables
VIEWB	View factor from the breeder to the blanket back wall
VIEWG	View factor across the vacuum gap
VIEWM	View factor from the breeder to the manifold
VL	Volume of the primary water pool (ft ³)
VL2	Volume of the secondary water pool (ft ³)
VLO	Variable used to read steam tables
VLP	Specific volume of the primary water pool (ft ³ /lb)
VLP2	Specific volume of the secondary water pool (ft ³ /lb)

VLPF	Specific volume of saturated liquid water at the secondary floor liner temperature (ft ³ /lb)
VLPV	Specific volume of saturated liquid water for heat transfer between the secondary floor liner and the secondary water pool (ft ³ /lb)
VP	Volume of primary cell (ft ³)
VS	Volume of secondary cell (ft ³)
VSF	Specific volume of water vapor at the water pool-gas boundary (ft ³ /lb)
VST	Specific volume of water vapor at the lithium pool surface (ft ³ /lb)
VVB	Specific volume of saturated water vapor at the primary water pool temperature (ft ³ /lb)
VVB2	Specific volume of saturated water vapor at the secondary water pool temperature (ft ³ /lb)
VVG	Specific volume of saturated water vapor in the primary gas (ft ³ /lb)
VVG2	Specific volume of saturated water vapor in the secondary gas (ft ³ /lb)
VVT	Temporary variable used to determine steam properties for condensation
WAB	Mass fraction of inert gas in the flooding gas
WAP	Mass fraction of inert gas in the primary gas
WAS	Mass fraction of inert gas in the secondary gas
WATER	Amount of water that should be left in the top concrete node as time $\rightarrow \infty$ (lb/ft ³)
WCB	Mass fraction of carbon dioxide in the flooding gas
WCP	Mass fraction of carbon dioxide in the primary gas
WCO2S	Mass fraction of carbon dioxide in the secondary gas
WN2B	Mass fraction of nitrogen in the flooding gas
WN2P	Mass fraction of nitrogen in the primary gas
WN2S	Mass fraction of nitrogen in the secondary gas
WO2B	Mass fraction of oxygen in the flooding gas
WO2P	Mass fraction of oxygen in the primary gas
WO2S	Mass fraction of oxygen in the secondary gas
WWAB	Mass fraction of water vapor in the flooding gas
WWAP	Mass fraction of water vapor in the primary gas
WWAS	Mass fraction of water vapor in the secondary gas
XALLOY	Atom percent of lithium in lithium-lead pool
XAM	Logarithmic mean molar fraction of air (see MFAB and MFAG)
XBLOW	Used in conjunction with IBLOW
XESC	Used in conjunction with IESC
XINJ	Indicates whether steam injection to the primary is in effect
XINJ2	Indicates whether steam injection to the secondary is in effect
XLI	Mass fraction of lithium in lithium-lead pool
XLIDOT	Mass flow rate of lithium through the lead layer above the Li-Pb pool (lb/sec)
XMAIRP	Amount of non-condensable primary gas after spray fire (lb-mol)
XMAIRS	Amount of non-condensable secondary gas after spray fire (lb-mol)

XMBLI	Mass of the blanket back wall (lb)
XMCO CZ	Mass of concrete combustion zone (lb)
XMDOT	Mass flow rate of gas between primary and secondary cells (lb/sec)
XMEHCP	Mass of primary extraneous heat capacity (lb)
XMEHCS	Mass of secondary extraneous heat capacity (breeder with torus fire option) (lb)
XMH20I	Initial water content of concrete (lb/ft ³)
XMMAG	Mass of the magnets (secondary extraneous heat capacity) (lb)
XMMAN	Mass of the blanket manifold (lb)
XMOLP	Molecular weight of non-condensable primary gas (lb/lb-mol)
XMOLS	Molecular weight of non-condensable secondary gas (lb/lb-mol)
XMOLA	Molecular weight of containment inert gas (lb/lb-mol)
XMOLAB	Molecular weight of flooding inert gas (lb/lb-mol)
XMSHI	Mass of shield inside region (lb)
XMSHL	Mass of shield bulk region (lb)
XMSHO	Mass of shield outside region (lb)
XSFL	Indicates whether emergency floor cooling is currently in effect
YALIG	Effective thermal admittance between the pool and primary gas (BTU/sec-deg. F.)
YAPCZ	Effective thermal admittance between the pool and combustion zone (BTU/sec-deg. F.)
YPAGAS	Effective thermal admittance between the pan and primary gas (BTU/sec-deg. F.)
ZLI	Thickness of the lithium pool (ft)
ZP	Used to determine EMLI if EMLI < 0.9
ZZxxxx	Temperature rate of change of a node (deg. R./sec)
ZZ1	Lithium pool
ZZ2	Lithium spill pan
ZZ3	Secondary cell gas
ZZ4	Primary cell gas
ZZ5	Primary wall liner
ZZ6	Combustion zone
ZZ7	Primary floor liner
ZZ8	Inner insulation layer
ZZ9	Outer insulation layer
ZZ99	Change in combustion rate with respect to time (lb Li/sec ² ft ²)
'ZZ'C	Concrete combustion zone
'ZZ'BLI	Blanket back wall
ZZD	Rate of change of concrete combustion zone thickness (ft/sec)
ZZDIN	Initial rate of change of concrete combustion zone thickness (ft/sec)
'ZZ'EP	Primary extraneous heat capacity
'ZZ'ES	Secondary extraneous heat capacity
'ZZ'FS	Secondary floor liner
'ZZ'MAG	Magnets (secondary extraneous heat capacity)

'ZZ'MAN Blanket manifold
 'ZZ'PB Lead layer above Li-Pb pool
 'ZZ'S Secondary wall liner
 'ZZ'SHI Shield inside region
 'ZZ'SHL Shield bulk region
 'ZZ'SHO Shield outside region

PROGRAM DECISION FLAGS

IAROSL =1 to use aerosol removal from containment by sticking option
 IBLOW =1 Containment flooding with inert gas
 =0 No containment flooding
 ICMB =0 No oxygen left after spray fire
 =1 Still oxygen left after spray fire (initially =1, reset by code)
 ICNI =0 Nitrogen reactions not possible
 =1 Nitrogen reactions possible
 ICO2I =1 to use pure CO₂ atmosphere
 ICZ =0 Combustion zone model not used
 =1 Combustion zone model used
 IESC =1 to use emergency space cooling option
 IFLAG2 =1 to use two-cell geometry option
 IFLAGB =1 to use lithium-lead option
 IFLAGC =1 to use concrete combustion option
 IFLAGCO =1 to use pure CO₂ atmosphere option
 IFLAGD =1 to use layered lithium-lead pool option
 IFLAGF =1 to use floor concrete option
 IFLAGISI =1 to enter input data in SI units
 IFLAGP =1 to use pan option
 IFLAGR =1 to use torus fire option
 IFLAGS =1 to use dry gas injection option
 IFLAGT =1 to use steam-air mixture option
 IFLAGU =1 to get output in SI units
 IFLAGW =1 to use wall concrete option
 ILIT =0 No lithium left to burn
 =1 Lithium left to burn
 IMETH =1 Runge-Kutta method of integration used
 =3 Simpson's Rule method of integration used
 ISFLC =1 to use emergency floor cooling option
 ISWICH =0 Crack size remains constant
 Crack size reset to zero after primary and secondary cell
 gas pressure equilibrate (note: this should not be used when
 either cell is small compared to the other or the volume of gas
 being consumed by the fire)

OPTION AND LOGICAL DECISION FLAGS

FLAG2 = .TRUE.	Two cell geometry
FLAGAS = .TRUE.	Injection of dry gas during run
FLAGC = .TRUE.	Concrete combustion
FLAGCO = .TRUE.	Pure CO ₂ containment atmosphere
FLAGD = .TRUE.	Concrete combustion has stopped (set by code)
FLAGDF = .TRUE.	Lithium-lead layered pool combustion model
FLAGF = .TRUE.	Floor concrete
FLAGISI = .TRUE.	Code accepts input in SI units
FLAGL = .TRUE.	LILP is fixed at a minimum (set by code)
FLAGM = .TRUE.	Sonic gas flow between cells (set by code)
FLAGN = .TRUE.	Indicates first run through a subroutine (set by code)
FLAGPB = .TRUE.	Lithium-lead combustion
FLAGPN = .TRUE.	Pan option
FLAGSI = .TRUE.	Code prints output in SI units
FLAGST = .TRUE.	Steam-air mixture in containment
FLAGTR = .TRUE.	Torus fire option
FLAGW = .TRUE.	Wall concrete

C Troubleshooting

"There exists no large computer code which runs perfectly 100% of the time."

-ANONYMOUS-

The user of this code may encounter problems while trying to execute LITFIRE. The most common error statement is generated by the computer itself: *DIVIDE BY ZERO* and stops the code. This indicates that an attempt was made to divide by zero or something very close to zero. The first step when encountering an error message is to check the output file *out1.dat* and ensure that the input was properly entered into the code. If it was, the error may occur if the value of EXHSTV is too high or LILP is too low. This problem may be mitigated to an extent by reducing DTMIN, the minimum time step length, although this will increase computation time.

Another common error message is generated by LITFIRE: *EXX IS NEGATIVE — CANNOT TAKE ROOT*. When this occurs, it indicates that the code is trying to take the square root of a negative number — the code has diverged numerically and the combustion zone temperature is negative. This may occur when the combustion rate CMBRH is very small (i.e., $\ll 1.0$ lb Li/hr-ft²), the oxygen and nitrogen concentrations are low, or when the gas pressure is low. This problem occurs when ZZ6 and DELT are large enough to produce a negative TCZ. This problem may be solved by reducing the value of DELOUT to limit the time step size, so extrapolations of TCZ over a long time step do not cause problems. Unfortunately, this can increase computation time considerably. The variation of the combustion zone temperature over time is a good indicator of whether or not the code is running properly. During combustion, TCZ should be 100° F. or more higher than TLI. Once combustion stops, TCZ should drop rapidly to a value just barely above TLI. (TLI is hypothetical at this point if the lithium has been consumed, but it is continuously calculated for numerical reasons.) If TCZ oscillates rapidly or falls below TLI, it is an indication of trouble. As stated earlier, this may be mitigated by decreasing the value of DELOUT.

If the statement: *LITHIUM TEMP. ABOVE BOILING POINT* occurs, this may indicate that the rate of change of the lithium pool temperature was very large. This may be due to the fact that TCZ has diverged to a very large value. This generally occurs as LILP nears zero, as the pool then has a lower heat capacity, and a sudden influx of energy would cause the pool to heat up rapidly.

Other signs of trouble include a rapid drop in containment gas mass (MNIP, MOXP), or an oscillating combustion zone temperature, TCZ; combustion rate, CMBRH; or time step length DELT. In general, DELT should increase after the start of the run and then level off until combustion stops, when it may change more rapidly. Sudden large changes in DELT indicate that the temperature rates of change are varying rapidly, which usually should not be the case. If reducing DELT does not help solve the problem, print out values of the code quantities like ZZ5 and ZZ6 or UVZ and MWVZ to help find the problem.

Other messages indicate that the user is attempting to use incompatible options together, or that the code has been stopped because there is no point in continuing further (i.e. the lithium temperature has dropped below the melting point, or containment gas temperature and pressure have returned to normal).

D Sample Input Data Files

INPUT DATA FILE HEAD.DAT

THIS IS THE INPUT DATA FOR THE EXECUTION
 OF THE CODE LITFIRE
 THESE ARE THE OUTPUT VALUES CORRESPONDING
 TO THE PRIMARY CELL ENVIRONMENT
 TIME DELT TCZF TLIF TGPF PAP TSPF TSFPF
 THESE ARE THE OUTPUT VALUES CORRESPONDING
 TO THE SECONDARY CELL ENVIRONMENT
 TIME TGSF TFSF PAS XMDOT MOXS MNIS MCO2S
 THESE ARE THE OUTPUT VALUES CORRESPONDING
 TO THE PAN OUTPUT OPTION
 TIME TLIF TPANF TINS1F TINS2F PAP
 THESE ARE ADDITIONAL OUTPUT VALUES CORRESPONDING
 TO THE PRIMARY CELL ENVIRONMENT
 TIME MNIP MOXP MCO2P RN2 R02 LIBP
 THESE ARE THE OUTPUT VALUES CORRESPONDING
 TO THE LITHIUM/LEAD DIFFUSION OPTION
 TIME XLIDOT TLEADF MLEAD THPB ZLI

INPUT DATA FILE UWMK.W

```

1 1 0 1 0 0 1 0 0 0 0 0 0 0 0 0 0 0
5 5
.20 .20 .20 .20 .20
.20 .20 .20 .20 .20
497.88 10.14 0.1247 39.90
725.0 123.00 51.00 0.1199 0.09
0.833 2.080 0.002 0.015 0.00
0.15 0.1189 30.00 497.500 572.3 0.0580
0.15 0.1189 30.00 497.500 38.35 0.0580
0.2 0.9960 33.80 30.00
0.9 0.2650 0.0227 144.00
124.00 86.9400 160.00 0.04 0.9 0.1
18510.0 0.0 4080.0 13784.0 10964.1
0.8764 0.0 1.487 0.383 0.766 6.93
816.60 2916.0 8431.0 0.0
0.87 0.13 0.01 0.11 0.89
0.16 0.85 0.112 0.07 0.01 0.01
0.07 0.07
2.153 22.05 0.000 0.050 5.0
1752.6 851.4 851.2 815.2 530.99 1751.8
14.70 0.2320 0.0 0.0000 0.0000
00030000000.02000000900.0000000000.00300000001.0000000100.0000
  
```

INPUT DATA FILE UWMK.X

```

8855700.0000000140.0000000014.70000000538.10000000538.20000000538.3000
15.5 00.00 0.232 0.0 522.0000 0.0
1482.0 1696200.0 9709.00 0.6921 0.09
0.85 0.1199 12.40 497.50 188164.00 0.0208
0.85 0.1199 12.40 497.50 59038.00 0.0208
350.0
  
```

INPUT DATA FILE UWMMAK.Y

0000030.00000000497.50000000000.12000000008.11500000000.20000000000.9000
1750.00 7.00 5.9055 12.32 0.09
0.0210 0.1667 0.0833
0.0350 9.3000 708.0000 0.1700 3315.0000 0000.0415
6.45600E-08

INPUT DATA FILE UWMMAK.Z

0000100.00000000000.00000000000.00000000004.00000000000.12470000535.0000
24.0 0.0 310.0 325.0 0.00

INPUT DATA FILE STEAMOP.

0001000.00000003000.00000000000.00900001190.300

INPUT DATA FILE TORUS.

8855700.00000000150.00000000014.70000000538.10000000538.20000000538.3000
15.5 00.70 0.232 0.0 522.0000 0.0
1482.0 115468.0 7796.00 0.1189 0.09 1.498
0.85 0.1199 12.40 497.50 188164.00 0.0208
0.85 0.1199 12.40 497.50 59038.00 0.0208
1.344 0.500 0.1 0.1 .648
672.0 1.903 14.202 3500000.0 0.1653 12110.0
0.500 0.0001 538.0 14000.0 9000000.0 0.1199
0.09 0.000 0.0656 0.889 1.0 .278
17.90 .1312 .1189 9472.0 149816.0 1300.0
670.0 585.0 .1312 .1312 260000.0 260000.0
.656 522842.0 .188 8890.0 1392.0 11.387
8.16e+00 4.41e-06 4.43e-01 9.57e-08 1.75e-01 2.90e-07
1.03e-01 4.41e-06 6.46e-03 9.57e-08 1.09e+00 3.08e-02
8.46e-02 2.56e-08 1.91e+00 7.41e-05 3.32e-02 2.92e-06
2.84e-02 4.41e-06 8.21e+00 3.08e-03 2.88e-03 2.90e-07
1.85e+00 7.41e-05 2.72e-03 2.56e-08 1.70e-04 3.84e-12
1.77e+01 2.81e-02 1.69e-04 7.51e-03 7.34e-06 1.69e-04
350.0

E Sample Output Data Files

OUTPUT DATA FILE OUT2.DAT

THESE ARE THE OUTPUT VALUES CORRESPONDING
TO THE PRIMARY CELL ENVIRONMENT

TIME	DELT	TCZF	TLIF	TGPF	PAP	TSPF	TSFPF
0.0	0.10	700.67	700.22	200.00	101.70	199.89	179.89
100.0	0.32	810.60	609.64	198.78	102.11	198.41	489.57
200.2	0.47	827.90	622.37	197.98	102.89	196.93	573.67
300.1	0.22	855.77	650.31	197.09	103.66	195.49	613.54
400.1	0.43	900.09	679.50	196.39	104.42	194.17	643.92
500.0	0.82	911.94	715.02	195.21	105.32	192.62	680.06
600.1	0.48	922.62	742.62	194.11	106.13	191.23	709.36
700.0	0.04	935.18	757.36	193.89	106.63	190.38	725.33
800.0	0.17	950.40	765.30	193.60	106.92	189.91	733.84
900.1	0.04	967.46	773.17	193.30	107.21	189.45	741.89

program execution stopped by program
values 0.233e+02 0.604e+03 0.181e+03 0.692e+01 0.619e+00

OUTPUT DATA FILE OUT3.DAT

THESE ARE THE OUTPUT VALUES CORRESPONDING
TO THE SECONDARY CELL ENVIRONMENT

TIME	TGSF	TFSF	PAS	XMDOT	MOXS	MNIS	MCO2S
0.0	25.94	26.06	101.38	-0.2194e+00	0.1508e+06	0.4994e+06	0.
100.0	28.12	26.06	102.11	0.	0.1508e+06	0.4994e+06	0.
200.2	30.40	26.06	102.89	0.	0.1508e+06	0.4994e+06	0.
300.1	32.69	26.08	103.67	0.	0.1508e+06	0.4994e+06	0.
400.1	34.90	26.10	104.41	0.	0.1508e+06	0.4994e+06	0.
500.0	37.56	26.15	105.32	0.	0.1508e+06	0.4994e+06	0.
600.1	39.96	26.20	106.13	0.	0.1508e+06	0.4994e+06	0.
700.0	41.44	26.25	106.63	0.3826e-01	0.1508e+06	0.4994e+06	0.
800.0	42.30	26.28	106.92	0.	0.1508e+06	0.4994e+06	0.
900.1	43.15	26.31	107.21	0.3610e-01	0.1508e+06	0.4994e+06	0.

OUTPUT DATA FILE OUT5.DAT

THESE ARE ADDITIONAL OUTPUT VALUES CORRESPONDING
TO THE PRIMARY CFLL ENVIRONMENT

TIME	MNIP	MOXP	MCO2P	RN2	RO2	LIBP
0.0	0.8074e+01	0.2439e+01	0.	0.00000	0.97120	0.
100.0	0.8153e+01	0.2426e+01	0.	0.35110	0.97098	0.1015e+00
200.2	0.8272e+01	0.2399e+01	0.	0.33125	0.97059	0.2476e+00
300.1	0.8395e+01	0.2372e+01	0.	0.28269	0.97020	0.4156e+00
400.1	0.8510e+01	0.2345e+01	0.	0.23668	0.96982	0.6179e+00
500.0	0.8662e+01	0.2305e+01	0.	0.18993	0.96929	0.8597e+00
600.1	0.8806e+01	0.2264e+01	0.	0.16182	0.96875	0.1074e+01
700.0	0.8892e+01	0.2236e+01	0.	0.16819	0.96841	0.1209e+01
800.0	0.8937e+01	0.2221e+01	0.	0.18553	0.96823	0.1297e+01
900.1	0.8988e+01	0.2208e+01	0.	0.20478	0.96805	0.1393e+01

OUTPUT DATA FILE OUT9.DAT

These outputs are the weights of react on products in LB

Time	Lilox	Lilni	Lilca	Lilc2	Lilcar	Mliop	Mlc3p
0.0	0.	0.	0.	0.	0.	0.	0.
100.0	0.193e+00	0.205e+00	0.	0.	0.	0.101e-01	0.
200.2	0.503e+00	0.474e+00	0.	0.	0.	0.262e-01	0.
300.1	0.837e+00	0.802e+00	0.	0.	0.	0.435e-01	0.
400.1	0.119e+01	0.124e+01	0.	0.	0.	0.614e-01	0.
500.0	0.165e+01	0.173e+01	0.	0.	0.	0.846e-01	0.
600.1	0.209e+01	0.213e+01	0.	0.	0.	0.107e+00	0.
700.0	0.238e+01	0.238e+01	0.	0.	0.	0.121e+00	0.
800.0	0.255e+01	0.255e+01	0.	0.	0.	0.128e+00	0.
900.1	0.273e+01	0.275e+01	0.	0.	0.	0.136e+00	0.

OUTPUT DATA FILE OUT10.DAT

These outputs are the reaction rates in gram Li/min-cm2

Time	Cmbrhh	Cmbrnh	Cmbrbh	Cmbrwh	Cmrcbh	Cmrc2f
0.0	0.	0.3050e-05	0.2866e-05	0.	0.	0.
100.0	0.3885e-01	0.2047e-01	0.1839e-01	0.	0.	0.
200.2	0.4243e-01	0.2292e-01	0.1951e-01	0.	0.	0.
300.1	0.4672e-01	0.2678e-01	0.1993e-01	0.	0.	0.
400.1	0.5183e-01	0.3112e-01	0.2071e-01	0.	0.	0.
500.0	0.4680e-01	0.2599e-01	0.2081e-01	0.	0.	0.
600.1	0.4365e-01	0.2289e-01	0.2076e-01	0.	0.	0.
700.0	0.4509e-01	0.2433e-01	0.2076e-01	0.	0.	0.
800.0	0.4833e-01	0.2739e-01	0.2094e-01	0.	0.	0.
900.1	0.5207e-01	0.3091e-01	0.2116e-01	0.	0.	0.

F Listing of the LITFIRE code

C *- fortran *-

C *****
C ***** LITFIRE Mod 7: a simulation of a lithium *****
C ***** spill in a tokamak fusion reactor *****
C *****
C *****

C LITFIRE Mod 7: includes the following modifications of
C LITFIRE Mod 6 (see User's Guide insert)

C Change in the Li-N reaction rate RR(T)
C Change in nitrogen reaction hindrance factor,
C applying the experimental results of Gil
C Change in thermal resistance of the Li pool from
C the combustion zone to more correctly model deep pools
C Addition of multiple lithium water reactions
C (Li--Li20, Li--LiOH)
C Addition of lithium hydrogen reaction (Li--LiH)

C Plasma Chamber Fire Model with decay heat generation included

C lithium--steam reaction modeling included

C lipb combustion modeling included

C akexx subroutine included

C modeled with: tau cz, emgp=1.0 etc., emgf is included, knit/klit.
C beta and stick
C separate emissivities and steel properties.
C new floor node in secondary.

C implicit real (i,k,l,m)
C logical flagw, flagf, flagl, flagpn, flagas, flagm, flag2, flagsi, flagn,
C flagc, flagpb, flagisi, flagdf, flagco, flagst, flagtr
C integer iflagw, iflagf, iflag2, iflag2, iflags, iflagc, iflagr,
C iflagu, iflagb, iblow, iesc, isflc, iswich, iarosl,
C iflagd, iflagisi, iflagco, iflagt, num, imeth, ipage,
C icz, icount, istore, inoin, ipass,
C il0, il1, il2, il3, il4, il5, il6, il7, il8, il9, i
C real intgr1, nulv
C common // name(340), flag2, flagas, flagc, flagf, flagpn, flagn, flagst, flagtr,
C flagpn, flagw, ipage, iswich, iarosl, flagdf, icz, flagco
C COMMON /looper/ il0, il1, il2, il3, il4, il5, il6, il7, il8, il9
C common /lith/ akli, asli, cpli, csbli, hb, libp, lil, lilp, lit,
C rhli, spill, tli, tlii, zli
C common /lead/ cplead, klead, rhlead, mlibp, xalloy, atml, atmpb, cmbr
C common /pbpool/ dmpbdt, zspb, mlead, tlead, xwli, dflipb, xlidot,
C thpb, tleadf, foo
C common /steel/ cpsfp, cpsw, cpswp, cpsws, estlfp, estlwp, kstlfp,
C kstlfs, kstlwp, kstlws, rhsfp, rhsfs, rhswp, rhsws
C common /misc/ aff, afs, awp, aws, c7, c21, gin,
C ha, hinfam, hinsam, htcpgp, gradc, radc, rczw,
C rhoap, rliw, rwpws, sigma, ta, tc(20), tfs,
C tfszer, tgp, tgs, tgpzer, tsfp, tsp, tss,
C tsszer, thfp, thfs, thwp, thws, zzes, zzs, zz1, zz7,
C rair
C common /intgl/ imeth, icount, istore, inoin, ipass, delt,
C xic(101), zzz(501)
C common /injop/ dp1, dp2, dp3, mnin, j, mxin, j, time, vp


```

c*****
c see litfire users guide for definitions and dimensions of input variables @
c*****
c***** read in title and headings *****
c
c read (1,700) (name(i),i=1,340)
700 format(20a4)
750 format (2x,'TIME',9x,'TSPF',3x,'TEHCSF',5x,'TMANF',3x,
'TBLIF',3x,'TSHIF',3x,'TSHLF',3x,'TSHOP'//)
c***** read in flags and options *****
c
c the next bunch of statements are here because of compile trouble at
c livermore. hopefully this will be corrected soon. (1/25/82).
c
c read (2,701) iflagw,iflagf,iflagp,iflag2,iflags,iflagc,
iflagu,iflagb,iblow,iesc,isflc,iswich,iaros1,
iflagd,iflagisi,iflagco,iflagt,iflagr
701 format(1x,18(1l,1x))
flagw=.false.
flagf=.false.
flagpn=.false.
flag2=.false.
flagas=.false.
flagc=.false.
flagsi=.false.
flagpb=.false.
flagdf=.false.
flagisi=.false.
flagco=.false.
flagst=.false.
flagtr=.false.
if (iflagw .eq. 1) flagw=.true.
if (iflagf .eq. 1) flagf=.true.
if (iflagp .eq. 1) flagpn=.true.
if (iflag2 .eq. 1) flag2=.true.
if (iflags .eq. 1) flagas=.true.
if (iflagc .eq. 1) flagc=.true.
if (iflagu .eq. 1) flagsi=.true.
if (iflagb .eq. 1) flagpb=.true.
if (iflagd .eq. 1) flagdf=.true.
if (iflagisi .eq. 1) flagisi=.true.
if (iflagco .eq. 1) flagco=.true.
if (iflagt .eq. 1) flagst=.true.
if (iflagr .eq. 1) flagtr=.true.
c***** read in primary containment specifications *****
c
c read (2,703) nl,nl1
read (2,704) (1(i),i=1,nl)
read (2,704) (11(i),i=1,nl1)
read (2,707) vp,chnp,cpap,xmola
read (2,702) tehczp,xmehcp,aehcp,cpehcp,hinecp
702 format (6f12.4)
703 format (i4,i4)
704 format (10f5.3/10f5.3)
706 format (7f12.4)
707 format (f12.2,3f12.4)
c***** read in parameters associated with *****
c outermost containment shell and concrete

```

```

C      read (2,702) thwc,thfc,gap,kgap,kleak
      if (thwc.lt. 0.001) flagw=.false.
      if (thfc.lt. 0.001) flagf=.false.

C*****      read in physical constants      *****
C      and emissivities

C
C      read (2,702) estlwp,cpswp,kstlwp,rhswp,awp,thwp
      read (2,702) estlfp,cpsfp,kstlfp,rhsfp,afp,thfp
      read (2,702) emli,cpli,akli,rhli
      read (2,702) emconc,cpcon,kcon,rhcon
      read (2,702) rho1io,rholin,rholih,emgpf,emcz,taucz

C*****      read in reaction constants      *****
C
      read (2,702) qcol,qco2,qcn,qcw,qw2
      read (2,702) rcmbol,rcmbo2,rcmbn,rcmbw,rcmbw2,rcmbh2
      read (2,702) tmelt,tvap,qvap,percen
      read (2,702) conf1,conf2,c2fac,flloh,fl12o
      rcmbol=((100.-percen)*rcmbol+percen*rcmbo2)/100.
      qco=((100.-percen)*rcmbol*qcol+percen*rcmbo2*qco2)/(rcmbo*100.)

C*****      read in heat transfer correlation coefficients      *****
C
      read (2,702) hin,hingsp,hingss,hinps,hinsam,hinfam
      read (2,702) hinfgs,hinfgs

C*****      read in spill parameters      *****
C
      read (2,702) asli,spill,spray,fra,ra
      zli=spill/rhli/asli

C*****      read in initial conditions      *****
C
      read (2,702) tczi,tgpzr,tspzr,tsfpi,ta,tlii
      read (2,702) papzr,wo2p,hum,wap,wcp

C*****      read in integration control parameters      *****
C
      read (2,705) imeth,dtmin,timef,relerr,delout,output
      705 format(i4,5f12.4)

C*****      add needed physical constants & parameters      *****
C*****      for Lithium-CO2 reactions      *****
C
      rho1c3=131.6
      rho1c2=102.9
      rho1car=124.7
      qcc=19288.
      q12c2=7139.
      rcmbccom=.22
      rcmbc2=.5783
      rcmbccs=.2313
      rcmbcal=2.3133
      rcmbca2=2.3133
      rcmbcco=0.6309

C*****      *****
C*****      options      *****
C*****      *****
C*****      *****

```

```

C***** containment flooding with inert gas option *****
C
C data tblin,tblout,blowv,exhstv,xblow,wo2b,wn2b,wab,wcb,xmolab,
C cpab,tblow/9*0.0,3*1.0/
C
C** read in gas flooding parameters if using option **
C
C 900 continue
C wab=1.-wo2b-wn2b-wab-wcb
C***** emergency space cooling of containment option *****
C
C data xesc,escr,escstin,escend/4*0.0/
C if (iesc.eq.1) read (5,702) escr,escstin,escend
C***** emergency steel floor liner cooling option *****
C
C data xsfl,sflcr,sfltin,sflend/4*0.0/
C if (isflc.eq.1) read (5,702) sflcr,sfltin,sflend
C***** aerosol removal from primary containment *****
C
C if (iarosl .eq. 1) read (5,702) beta
C***** steam injection in steam option *****
C
C if (flagst) read (6,702) stmin,stmout,minjr,hinj
C if (flagst.and.flag2) read (6,702) stmin2,stmout2,minjr2,hinj2
C***** closure of crack between primary and secondary *****
C
C***** print out the input *****
C*****
C*****
C write (10,800) (name(i),i=1,40)
C write (10,801) iblow,iesc,isflc,iswich,iarosl,flagpn,flag2,
C flagsi,flagas,flagc,flagw,flagf,flagisi,
C flagpb,flagdf,flagco,flagst,flagtr
C write (10,802) emconc,cpccon,kcon,rhcon,emli,cpli,akli,rhli,
C rholio,rholin,rholih,emgpf,emcz,taucz,
C rhoic3,rholc2,rhocar
C write (10,803) vp,chn,cpap,xmola,fra,ra
C write (10,804) tehczp,xmehcp,aehcp,cpehcp,hinecp
C write (10,805) asli,spill,spray,zi
C write (10,2101) conf1,conf2,c2fac,flioh,fli2o
C write (10,806) nl,nl1
C write (10,807) l(i),i=1,nl)
C write (10,808) (l1(i),i=1,nl1)
C write (10,809) thwc,thfc,gap,kgap,kleak
C write (10,810) estlwp,cpswp,kstlwp,rhswp,awp,thwp
C write (10,811) estlfp,cpsfp,kstlfp,rhsfp,afp,thfp
C write (10,812) hin,hinsam,hingsp,hingss,hinps,hinfam,hinfgs,
C hinfg
C write (10,813) qco,rcmbo,tvap,rcmbh2,percen,qco1,qco2,rcmbol,

```

```

      rcmbo2,qcn,rcmbn,tmelt,qcw,qcw2,rcmbw,rcmbw2,qvap,
      gcc,ql2c2,rcmbco,rcmbc2,rcmcal,rcmca2,rcmbcs,rcmcco
write (10,814) tgpzer,tspzer,tczi,tlii,tsfpi,
      ta,wo2p,wap,hum,papzer,wcp
write (10,815) imeth,dtmin,timef,relerr,delout,output
C*****
C      the following parameters are associated with the *****
C      different options and are written only when used
C
C      if (iblow.eq.1.or.isflc.eq.1.or.iesc.eq.1) write (10,819) wo2b,
      blow,cpap,wab,tblout,cpab,wn2b,tblin,exhstv,tblow,
      xmolab,sfltin,sflcr,sflend,esctin,escr,escend,wcb
C
C      if (iarosl .eq. 1) write (10,820) beta
C
C      if (flagst) write (10,821) stmin,stmout,minjr,hinj
C
C      if (flagst.and.(flag2.or.flagtr)) write (10,822)
      stmin2,stout2,minjr2,hinj2
C*****
C*****
C      800 format (' ',3(20a4,/,),/)
      801 format(' options in effect',/1x,17(1h-)//t10,'iblow = ',i4,t25,
      .iesc = ',i4,t40,'isflc = ',i4,t55,'iswich = ',i4//t10,'iarosl = ',
      .i4,t25,'flagpn = ',i4,t40,'flag2 = ',i4,t55,'flagsi = ',i4//t10,
      .flags = ',i4,t25,'flagc = ',i4,t40,'flagw = ',i4,t55,'flagf = ',
      .i4//t10,'flagisi = ',i4,t25,'flagpb = ',i4,t40,'flagdf = ',i4,
      .t55,'flagco = ',i4//t10,'flagst = ',i4,t25,'flagtr = ',i4//)
      802 format(' physical properties',/1x,19(1h-)//t10,'emconc = ',f12.4,
      .t35,'cpcon = ',f12.4,t60,'kcon = ',f12.4//t10,'rhcon = ',f12.4,
      .t35,'emli = ',f12.4,t60,'cpli = ',f12.4//t10,'akli = ',f12.4,
      .t35,'rhli = ',f12.4,t60,'rholio = ',f12.4//t10,'rholin = ',f12.4,
      .t35,'rholih = ',f12.4,t60,'emgpf = ',f12.4//t10,'emcz = ',f12.4,
      .t35,'taucz = ',f12.4,t60,'rholc3 = ',f12.4//t10,'rholc2 = ',f12.4,
      .t35,'rholc4 = ',f12.4//)
      803 format(' inner containment dimensions',/1x,28(1h-)//t10,'vp = ',
      .f12.2,t35,'chp = ',f12.4,t60,'cpap = ',f12.4//t10,'xmola = ',
      .f12.4,t35,'fra = ',f12.4,t60,'ra = ',f12.4//)
      804 format(/, extraneous heat capacity node data',/1x,33(1h-)//t10,
      .tehczp = ',f12.4,t35,'xmehcp = ',f12.4,t60,'aehcp = ',f12.4//
      .t10,'cpehcp = ',f12.4,t35,'hinecp = ',f12.4//)
      805 format(' spill parameters',/1x,16(1h-)//t10,'asli = ',f12.4,t35,
      .spill = ',f12.4,t60,'spray = ',f12.4//t10,'zli = ',f12.4//)
      806 format(/, wall and floor node data',/1x,24(1h-)//t10,'nl = ',
      .i2,t35,'n11 = ',i2//)
      807 format(' thickness of concrete wall nodes',/1x,31(1h-)//t10,
      .10(f5.3)//t10,10(f5.3)//)
      808 format(/, thickness of concrete floor nodes',/1x,32(1h-)//t10,
      .10(f5.3)//t10,10(f5.3))
      809 format(/, parameters associated with outermost containment',/1x,
      .48(1h-)//t10,'thvc = ',f12.4,t35,'thfc = ',f12.4,t60,
      .gap = ',f12.4//t10,'kgap = ',f12.4,t35,'kleak = ',f12.4//)
      810 format(' primary steel wall data',/1x,23(1h-)//t10,
      .estlwp = ',f12.4,t35,'cpswp = ',f12.4,t60,'kstlwp = ',f12.4//t10,
      .rhswp = ',f12.4,t35,'awp = ',f12.4,t60,'thwp = ',f12.4//)
      811 format(' primary steel floor data',/1x,24(1h-)//t10,
      .estlfp = ',f12.4,t35,'cpsfp = ',f12.4,t60,'kstlfp = ',f12.4//t10,
      .rhswp = ',f12.4,t35,'afp = ',f12.4,t60,'thfp = ',f12.4//)
      812 format(' heat transfer correlation coefficients',/1x,38(1h-)//
      .t10,'hin = ',f12.4,t35,'hinsam = ',f12.4,t60,'hingsp = ',f12.4//
      .t10,'hingss = ',f12.4,t35,'hings = ',f12.4,t60,'hinfam = ',f12.4//

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```

.t10,'hinfgs' = ,f12.4,t35,'hinfgs' = ,f12.4//)
813 format(' Combustion parameters'//1x,21(1h-)//t10,'qco = ',f12.4,
.t35,'rcmbo = ',f12.4,t60,'tvap = ',f12.4//t10,'rcmbh2 = ',f12.4,
.t35,'percen = ',f12.4,t60,'qco1 = ',f12.4//t10,'qco2 = ',f12.4,
.t35,'rcmbol = ',f12.4,t60,'rcmbol2 = ',f12.4//t10,'qcn = ',f12.4,
.t35,'rcmbn = ',f12.4,t60,'tmelt = ',f12.4//t10,'qcv = ',f12.4,
.t35,'qcv2 = ',f12.4,t60,'rcmbw = ',f12.4//t10,'rcmbw2 = ',f12.4,
.t35,'qvap = ',f12.4//t10,'qcc = ',f12.4,
.t35,'ql2c2 = ',f12.4,t60,'rcmbo = ',f12.4//t10,'rcmbc2 = ',f12.4,
.t35,'rcmcal = ',f12.4,t60,'rcmca2 = ',f12.4//t10,'rcmbcs = ',f12.4,
.t35,'rcmcco = ',f12.4//)
814 format(' initial conditions'//1x,18(1h-)//5x,'primary'//
.t10,'tgpzer = ',f12.4,t35,'tspzer = ',f12.4,t60,'tczi = ',f12.4//
.t10,'tlli = ',f12.4,t35,'tsfpi = ',f12.4,t60,'ta = ',f12.4//
.t10,'wo2p = ',f12.4,t35,'wap = ',f12.4,t60,'hum = ',f12.4//
.t10,'papzer = ',f12.4,t35,'wcp = ',f12.4//)
815 format(' integration control parameters'//1x,30(1h-)//t10,
.imeth = ,i4,t35,'dtmin = ',f12.4,t60,'timef = ',f12.4//t10,
.relefr = ',f12.4,t35,'delout = ',f12.4,t60,'output = ',f12.4//)
819 format(' miscellaneous input associated with various options'//1x
.51(1h-)//5x,'inert gas flooding'//t10,'wo2b = ',f12.4,t35,
.'blowv = ',f12.4,t60,
.'cpap = ',f12.4//t10,'wwab = ',f12.4,t35,'tblout = ',f12.4,t60,
.'cpab = ',f12.4//t10,
.'wn2b = ',f12.4,t35,'tblin = ',f12.4,t60,'exhstv = ',f12.4//t10,
.'tblow = ',f12.4,t35,'xmoliab = ',f12.4//5x,
.'steel floor cooling'//t10,'sfltin = ',f12.4,t35,'sflcr = ',f12.4,
.t60,'sflend = ',f12.4//5x,'emergency space cooling'//t10,
.'esctin = ',f12.4,t35,'escr = ',f12.4,t60,'escend = ',f12.4//5x,
.t10,'wcb = ',f12.4//)
820 format(' aerosol removal from primary containment'//1x,41(1h-)//
.t10,'beta = ',f12.4//)
821 format(' steam injection to containment'//1x,31(1h-)//t10,
.'stmin = ',f12.4,t35,'stout = ',f12.4,t60,'minjr = ',f12.4//5x,
.t10,'hinj = ',f12.4//)
822 format(' steam injection to secondary'//1x,29(1h-)//t10,
.'stmin2 = ',f12.4,t35,'stout2 = ',f12.4,t60,'minjr2 = ',f12.4//5x,
.t10,'hinj2 = ',f12.4//)
2101 format(' combustion branching factor or ratio'//1x,37(1h-)//
.t10,'conf1 = ',f12.4,t35,'conf2 = ',f12.4,t60,'c2fac = ',f12.4//
.t10,'flioh = ',f12.4,t35,'fli2o = ',f12.4//)
C*****
C***** options *****
C*****
C see litfire users guide for dimensions of option variables *
C
C in this step the secondary cell, pan geometry, and concrete wall *
C and floor variables are read in and written *****
C*****
C check for compatibility of options *
C
num=0
if (flagpb .and. spray .gt. 0.) go to 984
if (flagc .and. flagpn) go to 980
if (flagco .and. flagas) go to 2001
if (flagco .and. flagpb) go to 2003
if (flagco .and. wo2p.ne. 0.) go to 2005
if (flagtr .and. flag2) go to 2007
if (flagtr .and. flagc) go to 2009
if (flagtr .and. flagpn) go to 2011

```

```

flagn=.true.
if (flag2) call cell2
if (flagtr) call torus
if (flagpn) call pan
if (flagas) call injec
if (flagc) call conc
if (flagpb) call lipb
if (flagdf) call lidiff
if (flagst) call table
flagn=.false.
if (flagisi) call si

C*****
C initialize program variables *****
C*****
C flagl=.false.
C
C icz=1
C icmb=1
C ilit=1
C icni=1
C ico2i=0
C
C timeo=-.001
C tau=120.
C tau should be time dependent see note by mst.
C sigma=4.7619e-13
C gin=32.2
C ipage=40
C delt=dtmin
C
C call sub. CO2 if CO2 atmosphere option is used.
C
C if (flagco) call co2(icmb,icni,ico2i,n)
C if (flagco) ico2i=1
C*****
C initialize primary containment variables *****
C
C data cmbro,cmbrn,cmbrw,cmbrhi,dfilm,hf,hb,libp,lilox,lilni,leako,
.   mlinip,mlihp,mlihp,mh2p,oxlb,oxlbi,outint,roxlb,rnilb,rwalb,
.   cmbrco,cmbrc2,lilca,lilc2,lilcar,mco2ip,mic3p,mic2p,rcolb,
.   rc2lb,time,zzi,zz2,zz4,zz5,zz6,zz7,zz8,zz9,zzep,
.   ul,ulz,uv,uvz,mwl,mvlz,mvz,mvz,fpw,fpw/49*0.0,2*1.0/
C the next step is needed due to compiler errors at MIT
C   ul=0.0
C
C fmlft=1.0
C lis=spill*spray
C lit=spill-lis
C lilp=lit
C lil=lilp
C wn2p=1.-wo2p-wap-wcp
C xmolp=wo2p*32.+wn2p*28.+wap*xmola+wcp*44.
C rinp=1545./xmolp
C rair=rinp
C tehcp=tehczp
C tli=tlil
C tcz=tczi
C tsp=tspzr
C tsfp=tsfpi
C*****
C initialize the amount of water vapor in containment ***

```

```

flagn=.true.
if (flagst) call steam
flagn=.false.
c *****
rhoaip=papzer*144./rinp/tgpzer
if (flagst) rhoaip=(papzer-ph2o)*144./rinp/tgpzer
rhoap=rhoaip
mniip=wn2p*rhoaip*vp
moxip=wo2p*rhoaip*vp
mniip=mniip
mco2ip=wcp*rhoaip*vp
mco2p=mco2ip
mlioip=lis*(1.+rcmbo)/rcmbo
if (ico2i .eq. 1) mlcoip=0.
if (ico2i .eq. 1) mlc3ip=lis*(1.+rcmbs)/rcmbs
maip=wap*rhoaip*vp
map=maip
if (flagst) wvap=mvv/(mniip+moxip+map+mvv)
c ***** initialize option variables *****
c
if (flag2) call cell2
if (flagtr) call torus
if (.not. (flag2 .or. flagtr)) rbreak=0.0
if (flagpn) call pan
if (flagc) call conc
flagn=.true.
if (flagw) call concw
if (flagf) call conf
flagn=.false.
blowr=1.35e-03*blowv
exhstr=1.35e-03*exhstv
stick=0.0
if (iarosl .eq. 1) stick=awp/(vp*beta)/12.
if (stick .ge. 1.0) go to 986
if (stick .gt. .25) write (11,823)
823 format (' aerosol removal fraction is greater than one quarter
. of aerosol', inventory. time step has been decreased to insure
. stability.')
if (stick .gt. .25) ipage=ipage+2
c ***** conversion to ft. - lb. - sec. *****
c
akli=akli/3600.
kstlwp=kstlwp/3600.
kstlfp=kstlfp/3600.
kcon=kcon/3600.
kgap=kgap/3600.
c
c *****
c spray fire computation started *
c *****
c
c** check that enough oxygen or CO2 is left for pool fire after spray fire ***
c
if (ico2i .ne. 1) then
oxlfs=wo2p*rhoap*vp-lis/rcmbo
if (oxlfs .lt. 0.0) then
lis=rcmbo*wo2p*rhoaip*vp
oxlfs=0.0

```

```

endif
else
co2lfs=wcp*rhoap*vp-lis/rcmbco
if (co2lfs.lt. 0.0)then
lis=rcmbco*wcp*rhoaip*vp
co2lfs=0.0
endif
end if

if (lis.le.0.0) go to 902
to=vgpzer
if (ico2i .ne. 1)then
qin=lis*(qco+cpli*(tli-to))
else
qin=lis*(gcc+cpli*(tli-to))
endif
ff2=qin
te=vgpzer+1.
901 continue
c*****
c      cp = .0602*t**.326      t = deg. r      for lithium oxide      *****
c      cp = .761      for lithium carbonate
c      if a different reaction product is desired, the integral of the *
c      desired product must be substituted in gout1.
c*****
cplc3p=.761
cpco2p=.201
if (ico2i .ne. 1) then
gout1=(1.+rcmbo)/rcmbo*lis*(0.0602/1.326)*(te**1.326-to**1.326)
gout3=oxlfs*(.184*(te-to)+3.2e-6/2.*(te**2.-to**2.))+1.36e04*
      (1./te-1./to)
gout5=wcp*rhoap*vp*cpco2p*(te-to)
else
gout1=(1.+rcmbs)/rcmbs*lis*cplc3p*(te-to)
gout3=co2lfs*cpco2p*(te-to)
end if
gout2=wn2p*rhoap*vp*(.172*(te-to)+8.57e-06/2.*(te*te-to*to)+
      1.02e-09/3.*(te**3.-to**3.))
gout4=mvv*(0.44*(te-to))+wap*rhoap*vp*cpap*(te-to)
ff1=qin-gout1-gout2-gout3-gout4
if (ico2i .ne. 1) ff1=ff1-gout5
if (ff1*ff2.lt.0.) go to 903
te=te+1.
if (te.gt.1.0e06) go to 979
ff2=ff1
902 continue
c***** portion of program for getting initial gas temp. and press. ***
903 continue
te=vgpzer
tgp=te
moxp=moxip-lis/rcmbo
if (ico2i .eq. 1) moxp=0.0
moxip=moxp
if (ico2i .eq. 1) mco2p=mco2ip-lis/rcmbco
mliop=mlioiop
xmairp=manip/28.+moxp/32.+map/xmola+mco2p/44.
pzerop=1545.*xmairp*tgp/144./vp
if (flagst) pzerop= pzerop+ph2o
pap=pzerop
tgpzer=tgp

```

```

c ***determine the initial energy of the vapor region***
  if(flagst)call steam
c *****
  write (10,825) tgp,pzerop
  825 format (/// spray fire results//1x,18(1h-)//5x,'tgpzer = ',f6.1,
  . , pzerop = ',f8.3///)
  ggg=20.
c***** spray fire computation concluded *****
c
c call init
c
c*****
c* start of dynamic cycle *
c* ----- *
c* start of integration cycle *
c*****
c 200 continue
c
c***** reset rates of change to zero *****
c
  zz1=0.0
  zz2=0.0
  zz4=0.0
  zz5=0.0
  zz6=0.0
  zz7=0.0
  zz8=0.0
  zz9=0.0
  zzep=0.0
  ulz=0.0
  uvz=0.0
  mwlz=0.0
  mvz=0.0
  ulz2=0.0
  uvz2=0.0
  mwlz2=0.0
  mvz2=0.0
c
c***** injection of gases to model hedl experiment *****
  moxinj=0.0
  mninij=0.0
  if (flagas) call injec
c
c***** compute physical properties dependent on temperature *****
c***** calculate air composition and specific heat at const. volume *****
c
  maair=moxp+mnip+mh2p+map+mco2p
  xmolp=(28*mnip+32*moxp+2*mh2p+xmola*map+44*mco2p)/maair
  rair=1545./xmolp
  rhoap=maair/vp
  foxp=moxp/maair
  fwap=mvv/(mwv+maairp)
  fnip=mnip/maair
  fwcp=mco2p/maair
  cpo2p=(0.184+3.2e-06*tgp-1.36e04/(tgp*tgp))
  cpmoxp=cpo2p*moxp
  cpn2p=(0.172+8.57e-06*tgp+1.02e-09*tgp*tgp)
  cpnair=cpn2p*mnip
  cpwa=0.44
  cph2=2.48

```

```

cpc2p=0.193
cpmcp=cpc2p*mco2p
cplih=0.67
cplio=0.0602*tg** .326
cplip=0.3368+3.67e-04*tg
cpmlp=cplio*cplip
cplc3p=0.761
cpmlcp=cplc3p*mlc3ip
cplc2p=0.7
cpcarp=0.17

rhl=33.49-.0035*(tli-460.)
akli=(10.48+2.767e-03*(tli-817.)-0.322e-06*(tli-817.))**2)/1488.
cpfac=0.004938*tli-6.20741
cpli=1.0037-.01063*cpfac+.00564*cpfac**2-.001279*cpfac**3
cpli=((lit-libp)*cplililca+rholc3+lilni*cplinp+lilca*cplc3p+
. lilcar*cpcarp+lilc2*cplc2p)/lilp

C The following statements are made in order to simulate HEDL LC-2
C experiment in which the lithium was transferred into the pan
C during 0 to 150 sec period.
C In addition, the following statements will not be used in normal
C cases; the first column of these statement will be filled with
C "C" which make them inactive. If you want to try this option,
C delete these "C"'s and use appropriate input files (see T.K. Gil
C master thesis). And make sure to insert the "C"'s again for
C normal case runs.
C
C if (qqq .ge. 150.) goto 11
C if (time .ge. qqq) then
C lit=lit+0.14667
C qqq=qqq+1.
C rhlix=33.39-.0035*(tli-460.)
C aklix=(10.48+2.767e-03*(tli-817.)-0.322e-06*(tli-817.))**2)/
C 1488.
C cpfacx=0.004938*tli-6.20741
C cplix=1.0037-.01063*cpfac+.00564*cpfac**2-.001279*cpfac**3
C cplix=0.14667*cplix
C cpli=cpli+cplix
C rhli=rhli*(lit-0.14667)/(lit+.14667)+rhlix*0.14667*(lit+
C 0.14667)
C akli=akli*(lit-0.14667)/(lit+.14667)+aklix*0.14667*(lit+
C 0.14667)
C else
C continue
C end if
C 11 continue
C up to the above line is used for LC-2 lithium transfer simulation
C *****
C if (flagpb) call lipb
C *****
C two millimeters are assumed to cover the pool optically *****
C zp=(lilox/rholio+lilni/rholin+lilca/rholc3+lilc2/rholc2+
C lilcar/rhocar)/asli
C emf=0.9
C if (emli.lt.emf)emli=0.2+(emf-0.2)*zp/0.00656
C
C htcgpb=cpmoxp+cpnanip+cpmlp+cpap*map+cplinp*mlinp+cplih*mlihp+
C cph2*mh2p+cpmcp+cpmlcp

```



```

C account for steam effects on diffusion
C if(flagst)then
  vst=vvg
  va=1./rhoap
  rhotot=rhoap+1./vg
  muvcz=(11.4/((tl/1.8)**2-884*tl/1.8+1.36e06))/1.488
  temp2=(sqrt(d1)*rhoap/mucvz)**.5
  phiaw=218942*(1.+0.88808*temp2)**2
  phiw=.277605*(1.+1.2603/temp2)**2
  stmfac=vst/(vst+va*phia)
  airfac=va/(va+vst*phiw)
  mudiff=airfac*mucvz+stmfac*(sqrt(d1)*rhoap)
  dl=(mudiff/rhotot)**2
  akvap1=mucvz*cpwv
  ak1=stmfac*akl+airfac*akvap1
endif
C *****
C if (ic2 .eq. 1) exx=(gin*b1*abs(tc2-tgp))/d1
C if (ic2 .eq. 0) exx=(gin*b1*abs(tli-tgp))/d1
C if (exx .le. 0.0) go to 985
  ex1 = (exx)**0.3333
  hfinf=hin*diff*ex1
  hbinf=hin*ak1*ex1
  if (tau .lt. delt) tau=delt
  hf=hf+(hfinf-hf)*delt/tau
  hb=hb+(hbinf-hb)*delt/tau
C *****
C ***** check for boiling or condensation if water is present *****
C ***** and calculate gas heat transfer coefficients *****
C if(flagst)call steam
C *****
C ***** without steam, calculate the coefficients normally *****
C
C primary gas to primary steel liner
  hgwp=hingsp*akexx(tgp,tsp,rhoap)
C primary gas to primary extraneous heat capacity
  hehpc=hinecp*akexx(tgp,tehpc,rhoap)
C **calculate heat transfer coefficients with steam present**
C if(flagst) call steam
C *****
C primary steel liner to ambient if not two cell, torus or concrete option
  if (.not. (flag2 .or. flagw .or. flagtr))
    ha=hinsam*akexx(tsp,ta,.074)
C primary steel floor to ambient (if not two cell, torus or concrete)
  if (.not. (flag2 .or. flagf .or. flagtr))
    hamf=hinfam*akexx(tsfp,ta,.074)
C ***** calculating thermal diffusivities between nodes *****
  if (flagw) call concv
  if (flagf) call concf
  cehgcp=nehcp*aehcp/htcpgp
  cgehc=hehpc*aehcp/xnehcp/cpehpc
  c1=kstlwp*hgwp*awp/htcpgp/(thwp*hgwp/2.+kstlwp)
  c6=kstlwp*hgwp/(rhswp*cpswp*thwp*(thwp*hgwp/2.+kstlwp))
C the next thermal diffusivity is valid only if no wall concrete and
C no secondary containment cell, and is between steel liner and ambient
  if (.not. (flagw .or. flag2 .or. flagtr)) c11=
    . kstlwp*ha/(rhswp*cpswp*thwp*
    . (kstlwp+thwp*ha/2.))
  if (.not. (flagw .or. flag2 .or. flagtr)) c12=
    . kstlwp*hamf/(rhswp*cpswp*thwp*
    . (kstlwp+thwp*hamf/2.))

```



```

ofac=1.0
if (foxp.gt.0.0) ofac=(1.0-0.3*xmfoxp/0.2)
c *****
rrtli=rr(tli)*cstm
if (rrtli.le.cmbrn) cmbrn=rrtli
if (tez.le.2520.) then
  tlic=tli/1.8-273.
  tlin=tlic/750.
  tlin2=tlic/1100.
  if (tlic.lt.500.)rn21=1.0
  if (tlic.ge.500.)rn21=11.751-41.255*tlin+53.002*tlin**2.
  -22.962*tlin**3.
  if (tlic.ge.750.)rn21=13.173-55.058*tlin2+77.625*tlin2**2.
  -35.276*tlin2**3.
  if (tlic.lt.350.)rn22=1.0
  if (tlic.ge.350.)rn22=-0.176+5.295*tlin-6.998*tlin**2.
  +2.218*tlin**3.
  if (tlic.ge.750.)rn22=16.936-73.32*tlin2+104.629*tlin2**2.
  -48.067*tlin2**3.
  if (tlic.lt.200.)rn23=1.0
  if (tlic.ge.200.)rn23=0.391+4.128*tlin-8.161*tlin**2.
  +3.8*tlin**3.
  if (tlic.ge.750.)rn23=26.456-109.284*tlin2+148.31*tlin2**2.
  -65.412*tlin2**3.
  if (foxp.gt.0.20)rn2=rn23-(foxp-.20)/.20*(rn22-rn23)
  if (foxp.le.0.20)rn2=rn23+(.20-foxp)/.10*(rn22-rn23)
  if (foxp.le.0.10)rn2=rn22+(.10-foxp)/.05*(rn21-rn22)
  if (foxp.le.0.05)rn2=1.0-foxp/0.05*(1.0-rn21)
  if (rn2.lt.0.0)rn2=0.0
endif
if (tez.gt.2520. .or. foxp.gt.0.28) rn2=0.0
if (foxp.ne.0.0) ro2=(1-fnip/(foxp+fnip))*0.02
c
c rc2 is the inhibition factor for the lithium-CO2 reaction rate
c which is strongly depending on the degree of carbonate layer
c buildup. Here, 1 inch of carbonate is assumed to stop the
c reaction completely when the lithium pool temp. is below 400 C.
c
22 if (tli.le.1000.) rc2=0.0
if (lilca.le.0. .or. tli.gt.1180) rc2=1.
ratio=lilca/rholc3/asli
if (ratio1.gt.0.08333 .and. tli.le.1180.) rc2=0.
if ((ratio1.le.0.08333 .and. ratio1.gt.0.) .and. tli.le.
1180.) rc2=(1-ratio1/.08333)**1.5
cmbro1=hf*foxp*rhoap*rcmbo*ro2
cmbro2=hf*fwcp*rhoap*rcmcco*conf1
cmbro=cmbro1+cmbro2
cmbrn=cmbrn*rn2
if (flagst)cmbrw=hf/vg*rcmbw*flloh*ofac
if (flagst)cmbrw2=hf/vg*rcmbw2*fl12o*ofac
cmbrco=rc2*hf*fwcp*rhoap*rcmbco*conf2
cmbrc2=c2fac*(cmbrco+cmbro2)*rcmbc2
33 if (ico21.eq.1 .and. tli.gt.1180.) cmbro=hf*fwcp*rhoap*
rcmcco*conf1
if (ico21.eq.1 .and. tli.gt.1180.) cmbrco=hf*fwcp*rhoap*
rcmbco*conf2
if (ico21.eq.1) cmbrc2=c2fac*(cmbrco+cmbro)
cmbr = cmbro + cmbrn + cmbrw + cmbrw2 + cmbrco + cmbrc2
if (.not. flagdf) go to 1909
if (cmbr.lt.xlidot) go to 1909
cmbro=cmbro*xlidot/cmbr
cmbrn=cmbrn*xlidot/cmbr

```

```

cmbrw=cmbrw*xlidot/cmbr
cmbrw2=cmbrw2*xlidot/cmbr
cmbrco=cmbrco*rlidot/cmbr
cmbrc2=cmbrc2*xlidot/cmbr
cmbr=cmbr+cmbrn+cmbrw+cmbrw2+cmbrco+cmbrc2
1909 continue
if (cmbr*3600. .lt. 0.2) go to 910
rnilb=cmbrn*asli/rcmbn
roxlb=cmbr*asli/rcmbo
rwalb=asli*(cmbrw/rcmbw+cmbrw2/rcmbw2)
rcolb=cmbrco*asli/rcmbco
rc2lb=cmbrc2*asli/rcmbc2
C
C***** computation of lithium vapor diffusion *****
tfeff=0.002*(tcz+tli)/2.-3.92
pliv=(10.** (4.8831-14180.2/tli))*14.
if (flagpb) pliv=actvty(xalloy)*pliv
rholiv=pliv*144./rinp/tli
dfliv=3.56e-03*(tli/460.)*1.81)/pap
dffilm=dffli*rholiv/cmbr
effilm=dffilm*12.
C
knit=.0432+tfeff*(.0078-tfeff*(8.2e-04+tfeff*2.08e-04))
klit=0.55+tfeff*(-4.99e-04+tfeff*1.206e-07)
kfilm=(pliv*(klit-knit)+pap*knit)/14.7
C***** computation of heat transfer coefficients *****
depth=zli
if (zli/2. .gt. 0.375) depth=0.75
yapcz=kfilm*akli*asli/(dffilm*akli+kfilm*depth/2.)
C***** this heat capacity is sheer guess work the 0.1 is for low comb. rates
cpmcz=asli*(1.+rcmbo)/rcmbo*cmbr*cpliopt+(1.+rcmbn)/rcmbn*cmbrn*
. cplinp+(1.+rcmbcs)/rcmbcs*cmbrco*cplc3p+(1.+rcmbc2)/rcmbc2*
. cmbrc2*cplc2p+
. lilcar*cpccarp+(1.+rcmbw)/rcmbw-(1./rcmbh2))*cmbrw*cpwv+
. (1.+rcmbh2)/rcmbh2*cmbrw*cph2+
. ((1.+rcmbw2)/rcmbw2-(1./rcmbh2))*cmbrw2*cpwv+
. (1.+rcmbh2)/rcmbh2*cmbrw2*cph2+
. rn2*hf*fnip*rhoap*cpn2p)*450.+1.
C***** in this case of Li-CO2 reaction, cpmcz may vary. *****
C***** the following is a sheer guess work. *****
if (ico2i .eq. 1) cpmcz=(cpmcz-1.)/300.*100.
if (cpmcz/asli .le. 0.001) cpmcz=0.001*asli
cgcz=hb*asli/cpmcz
cczg=hb*asli/htcpgp
cpcz=yapcz/cpmcz
cczp=yapcz/(cpli*lil)
ccz=(cmbrco*qco+cmbrn*qcnc+cmbrw*qcw+cmbrw2*qcw2+cmbrco*qcct
. if (ico2i .eq. 1 .and. tli .gt. 1180.) ccz=(cmbrco*qco+cmbrco*qcct
. cmbrc2*ql2c2)*asli
. clist=2.*asli*akli*kstlfp/(lil*cpli*(zli*kstlfp+thfp*akli))
. csbli=2.*asli*akli*kstlfp/(rhsfp*asli*thfp*cpsfp*(zli*kstlfp+
. thfp*akli))
. qradp=sigma*asli*(tcz**4-tli**4)*rifczp
. qradw=sigma*asli*(tcz**4-tsp**4)*rifczw
. qradg=sigma*asli*(tcz**4-tgp**4)*rifczg
. rczw=gradw/(thwp*awp*rhswp*cpswp)
. rczp=gradp/(lil*cpli)
. rczg=gradg/htcpgp
. qrady=sigma*asli*(tli**4-tsp**4)*rifpw
. qradz=sigma*asli*(tli**4-tgp**4)*rifpg
. rliw=grady/(thwp*awp*rhswp*cpswp)

```

```

C
C      rwli=grady/cpli/lil
C      rgli=gradz/cpli/lil
C      rlig=gradz/htcpgp
C
C*****
C* calculating temperature rates of change with combustion *
C*****
C
C***** calculate comb. zone temp. rate of change deg. r/sec. *****
      zz6=(ccz-(gradg+gradw+gradg))/cpmcz+qvap*cubr*asli/cpmcz
      .   -cpcz*(tcz-tli)-cgcz*(tcz-tgp)
C
C***** calc. lithium temp. rate of change deg. r/sec. *****
      zz1=cczp*(tcz-tli)+rczp-clist*(tli-tsfp)-qvap*cubr*asli*cczp/yapcz
      .   -rwli-rgli
C
C***** calc. cell gas temp. rate of change deg. r/sec. *****
      if(.not.flagst)zz4=c1*(tsp-tgp)+cczg*(tcz-tgp)+rczg+rbreak+xblow*
      .   blowr*cpab*(tblog-tgp)/htcpgp-escr*xesc/htcpgp+
      .   cehcgp*(tehcp-tgp) + rlig
C
C***** calc. wall steel temp. rate of change deg. r/sec. *****
      if(mv.1e.0.0)zz5=zz5+c6*(tgp-tsp)+rczw+rliw
C
C***** computations with steam present *****
C
C vapor region energy rate of change
      if(flagst)uvz=uvz+cczg*htcpgp*(tcz-tgp)+gradg+gradz+
      .   xblow*blowr*cpab*tblog-xesc*escr
      .   if(flagst.and. mv.1e.0.0)uvz=uvz+c1*(tsp-tgp)*htcpgp+
      .   cehcgp*(tehcp-tgp)*htcpgp
C wall liner temp rate of change
      if(mv.gt.0.0)zz5=zz5+rczw+rliw
C
C      go to 911
C
C*****
C* computations without combustion zone model *
C*****
C
C 910 continue
      icz=0
      cmbr=0.0
      rn2=0.0
      yalig=akli*hb*asli/(akli+hb*zli/2.)
      clig=yalig/htcpgp
      gradw=sigma*asli*(tli**4-tsp**4)*rifpw
      gradg=sigma*asli*(tli**4-tgp**4)*rifpg
      rliw=gradw/(thwp*awp*rhswp*cpswp)
      rwli=gradw/cpli/lil
      rgli=gradg/cpli/lil
      rlig=gradg/htcpgp
      cgli=yalig/(lil*cpli)
      clist=2.*asli*akli*kstlfp/(lil*cpli*(zli*kstlfp+thfp*akli))
      csbli=2.*asli*akli*kstlfp/(rhswp*asli*thfp*cpsfp*(zli*kstlfp+
      .   thfp*akli))
C
C*****
C* calculating temperature rates of change *

```



```

C*****
C** calculating overpressure **
C*****
xmairp=moxp/32.+mnip/28.+map/xmola+mco2p/44.+mh2p/2.
pap=1545.*xmairp*tmp/144./vp
if(flagst)pap=pap+ph2o
overpp=pap-papzer
if(time.gt.tblin) xblow=1.
if(time.gt.tblout) xblow=0.

C*****
C** calcu. total leakage ***
C*****
leak=0.0
if(flag2) call cell2
if(flagtr) call torus
if(flag2.or.flagtr) go to 932
if(pap.gt. 14.7) leak=kleak*(pap-14.7)**0.5
xmdot=0.0
fouts=0.0
foutp=exhstr/mairp*xblow+leak
932 continue
fmleft= exp(-outint)
fmleak=1.--fmleft

C **** calculate hydrogen ratio (moles H2 to total moles of gas)
C hratio=mh2p/2./((xmairp+mvv/18.))

C*****
C* do integrations *
C*****
libp=intgrl(0.,cmbr*asli)
lilox=intgrl(0.,(1.+rcmbo)/rcmbo*(cmbro+cmbrw2)*asli*(1.--fra))
if(ico2i.eq. 1) lilox=intgrl(0.,(1+.535)*cmbro*asli)
lilni=intgrl(0.,(1.+rcmbn)/rcmbn*cmbrn*asli*(1.--fra))
lilca=intgrl(0.,(1.+rcmbcs)/rcmbcs*cmbrco*asli*(1.--fra))
lilc2=intgrl(0.,(1.+rcmbc2)/rcmbc2*cmbrc2*asli)
lilcar=intgrl(0.,cmbrco/rcmca2*asli+cmbrw2/rcmcal*asli-
.cmbrc2/rcmbc2*asli)
if(ico2i.eq. 1 .and. tli .gt. 1180.) lilcar=intgrl(0.,
.cmbrco/rcmca2*asli+cmbro/rcmcal*asli-cmbrc2/rcmbc2*asli)
oxlb=intgrl(oxlbi,roxlb)
if(ico2i .eq. 1) oxlb=0.0
tcz=intgrl(tczi,zz6)
tli=intgrl(tlii,zz1)
if(.not.flagst)tmp=intgrl(tgpzer,zz4)
tsp=intgrl(tspzer,zz5)
tehcp=intgrl(tehczp,zzep)
tsfpi=intgrl(tsfpj,zz7)
if(ico2i .eq. 1) then
moxp=0.0
else
moxp=intgrl(moxip,wo2b*blowr*xblow+moxs*fouts-moxp*foutp-
roxlb+moxinj)
endif
mnip=intgrl(mniip,wn2b*blowr*xblow+mnis*fouts-mnip*foutp
-rnilb+mniinj)
mco2p=intgrl(mco2ip,wcb*blowr*xblow+mco2s*fouts-mco2p*foutp
-rcolb)
map=intgrl(maip,wab*blowr*xblow+mas*fouts-map*foutp)

```

```

C ***** with steam present *****
if(flagst)then
if(mvz.gt.(mvl/delt))mvz=mvl/delt
mvv=intgrl(mvzer,mvz+wbab*blowr*xblow-rwalb+xinj*minj+r
mv2*fouts-mv*foutp)
mvl=intgrl(mvlzer,mvlz)
uv=intgrl(uvzer,uvz+xinj*minj+rwalb*hwv-
(mv*hwv+htcpgp*1.4*ttg)*foutp+
(mv2*hwv2+htcpgs*1.4*tgs)*fouts)
ul=intgrl(ulzer,ulz)
if(mvl.lt.1.0e-06 .and. ipass.ne.0 .and. icount.eq.1)then
ul=0.0
xic(inoin)=0.0
endif
endif
C *****
if (ico2i .ne. 1)mliop=intgrl(mliop,-mliop*foutp+(1.+rcmbo)/rcmbo
*(cmbrw+cmbrw2)*asli*fra+mlios*fouts-mliop*stick)
mhc3p=intgrl(mhc3p,-mhc3p*foutp+(1.+rcmbs)/rcmbs*cmbrco*
asli*fra+mhc3s*fouts-mhc3p*stick)
mlihp=intgrl(mlihp,-mlihp*foutp+(1.+rcmbn)/rcmbn*cmbrn*asli*fra+
mlios*fouts-mlihp*stick)
mlihp=intgrl(0.,-mlihp*foutp+cmbrw*asli*((1.+rcmbw)/rcmbw-
1./rcmbh2)+mlihs*fouts-mlihp*stick)
mh2p=intgrl(0.,mh2s*fouts-mh2p*foutp+1./rcmbh2*
(cmbrw+cmbrw2)*asli)
outint=intgrl(leako,leak)
C *** pan integrations *****
if (flagpn)then
tpan=intgrl(tpanzo,zz2)
tins1=intgrl(tinsli,zz8)
tins2=intgrl(tins2i,zz9)
endif
C *** secondary cell integrations *****
if (flag2.or.flagtr)then
moxs=intgrl(moxis,moxp*foutp-moxs*foutt)
mniis=intgrl(mniis,mnip*foutp-mnis*foutt)
mco2s=intgrl(mco2is,mco2p*foutp-mco2is*foutt)
mas=intgrl(mais,mas*foutp-mas*foutt)
mlios=intgrl(mlios,mliop*foutp-mlios*foutt)
mlins=intgrl(mlinis,mlihp*foutp-mlins*foutt)
mlc3s=intgrl(mlc3is,mlc3p*foutp-mlc3s*foutt)
mlihs=intgrl(0.,mlihp*foutp-mlihs*foutt)
mh2s=intgrl(0.,mh2p*foutp-mh2s*foutt)
if(.not.flagst)tgs=intgrl(tgszer,zz3)
tss=intgrl(tsszer,zzs)
tfs=intgrl(tfszer,zzfs)
tehcs=intgrl(tehczs,zzes)
endif
C *** torus integrations *****
if(flagtr)then
tman=intgrl(tmano,zzman)
tbli=intgrl(tblio,zzbli)
tmag=intgrl(tmagz,zzmag)
tshl=intgrl(tshlz,zzshl)
tshi=intgrl(tshio,zzshi)
tsho=intgrl(tshoo,zzsho)
endif
C *** secondary cell steam effects *****
if(flagst.and.(flag2.or.flagtr))then
if(mvz2.gt.(mvl2/delt))mvz2=mvl2/delt
mvv2=intgrl(mvzr2,mvz2+xinj2*minj2+mvv*foutp-mv2*foutt)

```

```

mw12=intgr1(mw1zr2,mw1z2)
uv2=intgr1(uvzr2,uvz2+xinj2*minjr2*hinj2-
(mwv2*hwv2+htcpgs*1.4*tgs)*foutt+
(htcpgp*1.4*tcgp+mwv*hwv)*foutp)
ul2=intgr1(ulzr2,ulz2)
if(mw12.lt.1.0e-06 .and. ipass.ne.0 .and. icount.eq.1)then
ul2=0.0
xic(inoin)=0.0
endif
endif
c *****
if (flagw)then
do 1300 i=1,nl
tc(i)=intgr1(tcic(i),dtcdt(i))
1300 continue
endif
do 1310 i=1,nll
tb(i)=intgr1(tbic(i),dtbdt(i))
1310 continue
endif
if (flagc)then
tcon=intgr1(tsfpi,zzc)
dcoz=intgr1(0.01,zzd)
h2left=intgr1(xmh2oi,-relese)
endif
if (flagdf) mlead=intgr1(0.,dmpbdt)
if (flagdf) tlead=intgr1(tleadi,zzpb)
c call dynami(time,200)
c *****
c* post integration section
c check overp and tli for stop condition
c check and correct for lithium and oxygen supply
c *****
c 950 continue
if (thpb .gt. .333*zli) go to 987
if (tli .ge. tvap) go to 978
lilp=lit-libp+lilox+lilinl
if (lilp .le. 0.) lilp=0.0
if (.not. flagpb) zli=lilp/rhli/asli
alpha=akli/(rhli*cpli)
if ((lilp .lt. 0.1*lit) .and. (alpha*delt .gt. zli*zli .or. lilp
.lt. 1.0) .and. (.not. flagpb)) flagl=.true.
if (flagl) lil=lit/10.
if (.not. flagl .and. .not. flagpb) lil=lilp
if (tgp .lt. 500. .and. overpp .lt. 1. .and. abs(xmdot)
.lt. 0.1) go to 977
if (tli .lt. tmelt) go to 976
if (icmb .ne. 0 .and. moxp .le. 0.01)then
oxlb=oxlfs
icmb=0
cmbro=0.0
roxlb=0.0
endif
if (ilil .ne. 0. .and. (lit-libp) .lt. 0.01)then
oxlb=lit/rcmbo
if (ico2i .eq. 1) colb=lit/rcmbco
if (ico2i .eq. 1) oxlb=0.0
ilil=0

```



```

lit=libp
cmbr=0.0
cmbro=0.0
cmbrn=0.0
cmbrco=0.0
cmbrc2=0.0
cmbrw=0.0
cmbrw2=0.0
roxlb=0.0
rnilb=0.0
rwalb=0.0
rcolb=0.0
rc2lb=0.0
endif
if (mnip .lt. 0.0)then
  mnip=0.0
  icni=0
  cmbrn=0.
  rnilb=0.0
endif
if (mwv .lt. 0.0) then
  mwv=0.0
  uv=vgp*htcpgp
  cmbrw=0.0
  cmbrw2=0.0
  rwalb=0.0
endif
if (mco2p .lt. 0.0) then
  mco2p=0.0
  cmbrco=0.0
  rcolb=0.0
  cmbrc2=0.0
  rc2lb=0.0
  if (ico2i .eq. 1 .and. tli .gt. 1180.) cmbro=0.0
  if (ico2i .eq. 1 .and. tli .gt. 1180.) roxlb=0.0
endif
cmbrh=3600.*(cmbro+cmbrn+cmbrw+cmbrw2+cmbrco+cmbrc2)
if (cmbrh .lt. 0.1 .and. time .gt. 10.) then
  icz=0
  cmbro=0.0
  cmbrn=0.0
  cmbrw=0.0
  cmbrw2=0.0
  cmbrh=0.0
  cmbrco=0.0
  cmbrc2=0.0
  roxlb=0.0
  rnilb=0.0
  rwalb=0.0
  rcolb=0.0
  rc2lb=0.0
endif
C *****
C* convert temp. to deg. f
C *****
C
tsfpf=tsfp -460.
tczf=tcz-460.
tlif=tli-460.

```

```

tgpff=tgp-460.
tspf=tsp-460.
tehcpf=tehcp-460.
if (flagst) then
  tlpf=tlp-460.
  tlpf2=tlpf2-460.
endif
if (flag2.or.flagtr) then
  tgsf=tgs-460.
  tfsf=tfs-460.
  tssf=tss-460.
  tehcsf=tehcs-460.
endif
if (flagpn) then
  tpanf=tpan-460.
  tins1f=tins1-460.
  tins2f=tins2-460.
endif
if (flagw) then
  do 1001 i=1,20
    tcf(i)=tc(i)-460.
  1001 continue
endif
if (flagf) then
  do 1002 i=1,20
    tbf(i)=tb(i)-460.
  1002 continue
endif
tconf=tcon-460.
if (flagdf) tleadf=tlead-460.
if (flagst) tlpf=tlp-460.

C*****
C*   time step control   *
C*****

dt1=abs(releirr*tl/zzi)
if (flagst.and.uvz.ne.0.0) then
  dt2=abs(releirr*uv/uvz)
  elseif (zz4.ne.0.0) then
    dt2=abs(releirr*tgp/zz4)
  else
    dt2=dtmin
  endif
dt3=abs(releirr*tsp/zz5)
if (ilit.eq.0.or.icz.eq.0) go to 965
dt5=abs(releirr*tcz/zz6*.05)
zz99=(cmbrh-cmbrhi)/delt
if (zz99.eq.0.) go to 965
dt4=abs(releirr*cmbrh/zz99)
cmbrhi=cmbrh
if (ipass.eq.1) dt4=1.e06
go to 966

965 continue
dt4=1.0e06
dt5=1.0e06

966 continue
if (flagdf .and. zspb .lt. 1.0e-15) zspb=1.0e-15
if (flagdf) dt6=abs(releirr*tlead/zspb)
bilge=amin1(dt1,dt2,dt3,dt4,dt5)
if (flagdf) bilge=amin1(bilge,dt6)
bil=(bilge-delt)/delt

```

```

c this condition is to remove instability due to steep
c nitrogen reaction curve
  if (tcz.gt.1900..and.abs(bil).gt.0.1) then
    delt=delt+(bilge-delt)/10.
  else
    delt=bilge
  endif
c
c**** test conduction limits on time step ***
c limiting conduction rate is determined from pool to pan
c (if using pan option) otherwise from pool to steel liner
c
  if (flagpn) alpha2=((thkpan+zli)/(zli/akli+thkpan/kpan))/
    ((thli*cpli*zli+rhpan*cpan*thkpan)/(thkpan+zli))
  if (flagpn) pyu=0.075*(thkpan+zli)**2/alpha2
  if (.not. flagpn) alpha2=((thfp+zli)/(zli/akli+thfp/kstlfp))/
    ((rthli*cpli*zli+rthsfp*cpsfp*thfp)/(thfp+zli))
  if (.not. flagpn) pyu=0.075*(thfp+zli)**2/alpha2
  if (delt.gt.pyu) delt=pyu
c conduction test for pool layers if using diffusion model
  if (flagdf.and.delt.gt.pyup) delt=pyup
c testing two cell exchange rate on time step
  if (.not.(flag2.or.flagtr).or.abs(xmdot).lt.0.0001) go to 959
  if ((abs(pap-pas)).lt..01.and.delt.gt..04) delt=.04
  delmp=airp/abs(xmdot)/250.
  delms=airs/abs(xmdot)/250.
  if (delt.gt.delmp) delt=delmp
  if (delt.gt.delms) delt=delms
959 continue
c aerosol removal time step check
  if (delt*stick.gt..40) delt=.40/stick
c steam effects time step checks
  if (flagst)then
    if (uvz.ne.0.)then
      deluv=abs(uv/uvz)*relerr
      if (delt.gt.deluv)delt=deluv
    endif
    if (mwvz.ne.0.)then
      delmwv=abs(mwv/mwvz)*relerr
      if (delt.gt.delmwv)delt=delmwv
    endif
    if (ulz.ne.0..and.mw1.gt.1.0e-06)then
      delul=abs(ul/ulz)*relerr
      if (delt.gt.delul)delt=delul
    endif
    if (mw1z.ne.0.)then
      delmw1=abs(mw1/mw1z)*relerr
      if (delt.gt.delmw1)delt=delmw1
    endif
    if (mwvz2.ne.0.)then
      delmw2=abs(mwv2/mwvz2)*relerr
      if (delt.gt.delmw2)delt=delmw2
    endif
    if (uvz2.ne.0.)then
      deluv2=abs(uv2/uvz2)*relerr
      if (delt.gt.deluv2)delt=deluv2
    endif
    if (mw1z2.ne.0.)then
      delmw12=abs(mw12/mw1z2)*relerr
      if (delt.gt.delmw12)delt=delmw12
    endif
    if (ulz2.ne.0..and.mw12.gt.1.0e-06)then

```

```

delul2=abs(ul2/ulz2)*relerr
if (delt.gt.delul2)delt=delul2
endif
c***** general time step controls *****
if (delt .gt. 0.1 .and. time .lt. 3.0) delt=0.1
if (delt .gt. 0.2 .and. time .lt. 25.0) delt=0.2
if (delt .gt. 1.0 .and. time .lt. 2000.0) delt=1.0
c***** user defined time step controls *****
if (delt.lt.dtmin) delt=dtmin
if (delt .gt. delout) delt=delout
c*****
c* output section *
c*****
c
if (time.lt.timeo) go to 975
timeo=timeo+output
if (ipage.lt.40) go to 974
write (11,830) (name(i),i=41,100)
write (20,1112)
1112 format (//,' Time Cbrhnh Cbrbrh Cbrbrh Cbrbrh Cbrbrh
. cm2',//,5x,' Time Cbrhnh Cbrbrh Cbrbrh Cbrbrh Cbrbrh
. Cmrcoh Cmr2h',//)
write (18,1113)
1113 format (//,' These outputs are the weights of reaction products in
. LB',//,5x,' Time Lilox Lilni Lilca Lilc2 Lilcar
. Mliop Mic3p',//)
if (flag2.or.flagtr) write (12,830) (name(i),i=101,160)
if (flagpn) write (13,830) (name(i),i=161,220)
write (14,830) (name(i),i=221,280)
if (flagdf) write (15,830) (name(i),i=281,340)
c write (16,829) i10,i11,i12,i13,i14
c write (17,833) i15,i16,i17,i18,i19
c 830 format( , ,2(20a4,)//,20a4)
974 continue
if (ipage.ge.40) ipage=0
ipage=ipage+1
if (time .le. 0.) then
tval = 0.1
else
tval = time
endif
c **** changing RR from lb li/sec-ft2 to gram li/min-cm2
cmbrnh=cmbrn*3600./122.78
cmbroh=cmbro*3600./122.78
cmbrwh=(cmbrw+cmbrw2)*3600./122.78
cmbrhh=cmbr*3600./122.78
cmrcoh=cmbrco*3600./122.78
cmrc2h=cmbrc2*3600./122.78
if (iflagu .ne. 1) go to 1054
c
c*** this step converts output variables to si ***
c*** added due to some difficult in compiling from Sub. si ***
c
cmbrh=cmbrh*4.8824
libp=libp/2.2046
map=map/2.2046
mrip=mnip/2.2046
moxp=moxp/2.2046
mwap=mwap/2.2046
mco2p=mco2p/2.2046

```

```

pap=pap/1.450e-01
tczf=tcz/1.8-273.
tehcpf=tehcf/1.8-273.
tgpf=tgp/1.8-273.
tlif=tlf/1.8-273.
tsfpf=tsfp/1.8-273.
tspf=tsp/1.8-273.
zli=zli/3.281
if (flag2.or.flagtr) then
pas=pas/1.450e-01
tehcsf=tehcs/1.8-273.
tgsf=tgs/1.8-273.
tfsf=tfs/1.8-273.
tssf=tss/1.8-273.
xmdot=xmdot/2.2046
endif
if (flagtr) then
tmanf=tman/1.8-273.
tblif=tblf/1.8-273.
tmagf=tmag/1.8-273.
tshlf=tshf/1.8-273.
tshif=tshi/1.8-273.
tshof=tsho/1.8-273.
endif
if (flagst) then
mw1=mw1/2.2046
mw12=mw12/2.2046
mwv=mwv/2.2046
mwv2=mwv2/2.2046
tlpf=tlp/1.8-273.
tlpf2=tlp2/1.8-273.
endif
if (flagpn) tpanf=tpan/1.8-273.
if (flagpn) tinsf=tins1/1.8-273.
if (flagpn) tins2f=tins2/1.8-273.
if (flagc) tconf=tcon/1.8-273.
if (flagdf) then
mlead=mlead/2.2046
thpb=thpb/3.281
tleadf=tlead/1.8-273.
xlidot=xlidot*4.8824*3600.
endif
if (flagw) then
do 1500 i=1,20
tcf(i)=tc(i)/1.8-273.
1500 continue
endif
if (flagf) then
do 1490 i=1,20
tbf(i)=tb(i)/1.8-273.
1490 continue
endif
1054 continue
endif
write (11,826) time,delt,tczf,tlif,tgpf,pap,tspf,tsfpf
write (98,751) time,tspf,tehcsf,tmanf,tblif,tshif,tshof
C *****this step writes the output into files to be plotted*****
C *** these steps create files for a graphics routine to be plotted on
C *** graphs of the variable indicated vs. time. Plots of other variables
C *** may be created as desired by adding new open (or call link) statements
C *** at the beginning of the code as described in the user's guide.
C

```

```

write (21,1070) time,tspf
write (22,1070) time,pap
write (23,1070) time,tgpf
write (24,1070) time,tsfpf
write (40,1070) time,tczf
write (99,1070) time,tlif
if(flagtr)then
write (25,1070) time,tehcsf
write (26,1070) time,tshlf
write (27,1070) time,pas
write (28,1070) time,tgsf
write (29,1070) time,tmagf
write (30,1070) time,tfsf
write (31,1070) time,tssf
endif
if(flagst)then
write(41,1070) time,mv
write(42,1070) time,mvl
write(43,1070) time,tlpf
write(44,1070) time,hratio
endif
1070 format (2f10.3)
751 format (x,f9.1,2x,f7.2,f9.2,f9.2,4(1x,f7.2))
c*****
c write (20,849) tval,tlif,pap,tgpf
num=num+1
if (flag2.or.flagtr) write (12,832) time,tgsf,tfsf,pas,xmdot,
moxs,mnis,mco2s
if (flagpn) write (13,3999) time,tlif,tpanf,tinsif,tins2f,pap
write (14,831) time,mnip,moxp,mco2p,rn2,ro2,libp
write (20,1120) time,cnbrh,cnbrhh,cnbrnh,cnbrwh,cmarcoh,cmarc2h
format (3x,f9.1,6e11.4)
1120 write (18,1114) time,lilox,lilni,lilca,lilc2,lilcar,mliop,mlc3p
1114 format (1x,f7.1,7e10.3)
if (flagdf) write (15,3999) time,xlidot,tleadf,mlead,thpb,zli
write (16,834) time,tbf(il1),tbf(il2),tbf(il3),tbf(il4)
write (17,834) time,tcf(il5),tcf(il6),tcf(il7),tcf(il8),tcf(il9)
c 826 format(3x,f9.1,f6.2,f10.2,f10.2,4(1x,f7.2))
3999 format(3x,f9.1,5e13.4)
849 format(f9.1,f10.2,f8.2,e13.4)
829 format(' nodal concrete floor temperatures',///,5x,'time',
6x,'tb(' ,il,')',6x,'tb(' ,il,')',6x,'tb(' ,il,')',
6x,'tb(' ,il,')',6x,'tb(' ,il,')')
831 format(3x,f9.1,3e12.4,2f9.5,e12.4)
832 format(f8.1,3f8.2,4e11.4)
833 format(' nodal concrete wall temperatures',///,5x,'time',
6x,'tc(' ,il,')',6x,'tc(' ,il,')',6x,'tc(' ,il,')',
6x,'tc(' ,il,')',6x,'tc(' ,il,')')
834 format(f9.1,5f11.2)
if (iflagu .ne. 1) go to 975
c**** this step converts output from si to english after ****
c output is printed so that program can calculate
c things in english again. not needed for output temps.
c
cnbrh=cnbrh/4.8824
libp=libp*2.2046
map=map*2.2046
mnip=mnip*2.2046
moxp=moxp*2.2046
mwap=mwap*2.2046
mco2p=mco2p*2.2046

```

```

pap=pap*1.450e-01
zli=zli*3.281
if (flag2.or.flagtr) pas=pas*1.450e-01
if (flag2.or.flagtr) xmdot=xmdot*2.2046
if (flagdf) xlidot=xlidot/3600./4.8824
if (flagdf) mlead=mlead*2.2046
if (flagdf) thpb=thpb*3.281
if (flagst) then
  mw1=mw1*2.2046
  mw12=mw12*2.2046
  mwv=mwv*2.2046
  mwv2=mwv2*2.2046
endif
975 continue
if (time.gt.timef) go to 990
***** return to top of dynamic cycle *****
go to 200
C
C*****
C* error pointers *
C*****
C
976 continue
write (11,835)
835 format(' pool temp. has dropped to lithiums melting temp.')
```

```

write (11,2002)
2002 format(1x,'CO2 atmosphere and gas injec. option cannot be used
./ix,concurrently',//)
go to 990
2003 continue
write (11,2004)
2004 format(1x,'CO2 atm. and lithium lead combustion options cannot
./ix,used concurrently',//)
go to 990
2005 continue
write (11,2006)
2006 format(1x,'CO2 atm. option is not allowed when oxygen is present'
//)
go to 990
2007 continue
write (11,2008)
2008 format(1x,'Torus option is incompatible with two-cell option'//)
go to 990
2009 continue
write (11,2010)
2010 format(1x,'Torus option is incompatible with concrete
reaction option'//)
go to 990
2011 continue
write (11,2012)
2012 format(1x,'Torus option is incompatible with pan option'//)
go to 990
987 continue
848 format(' lead layer thickness is greater than zli/3. diffusion'//
. ' model is no longer valid'//)
990 continue
write (11,867)
867 format(' program execution stopped by program')
write (11,868) dt1,dt2,dt3,dt4,dt5
write (10,869) num
869 format(' ,',the number of data points is ',i4)
868 format(' values', 5e10.3)
call exit
end

```

c these 3 subroutines are designed to be used in a main program which
c simulates a dynamic system expressed as a set of ode's. these ode's
c may be reexpressed as a set of integrals which must be integrated
c simultaneously through the domain of interest starting with the appropriate
c initial conditions. for example, the function y may be found from the
c solution of $dy/dt = \text{rate} = f(y,t)$ and $y=y_0$ at $t=t_0$. this may be
c rewritten $y = \text{intgrl}(y_0, \text{rate})$, the open integral of rate over t starting
c at y_0 . a set of ode's may be treated in a similar manner.
c the main program should consist of two main parts, the initialization
c section and the dynamic section. the dynamic section is further divided
c into integration and post-integration sections.
c the initial section should be used for input, calculation of necessary
c constants, and for calculating and setting of initial conditions. it
c should contain the real intgrl, common, and call init statements.
c the integration section should start with a numbered continue
c statement and end with the call dynami statement. it should contain


```

c all calculations of program variables and non-constant rates. all intgrl
c function statements should appear in a group immediately preceding the
c call dynami statement.
c the integration section will be looped several times during each
c integration step (simpson's rule uses 4 loops per step, runge-kutta uses
c 5 loops per step). dynami controls the integration by telling the
c intgrl function what step it should perform next. the integration
c variable time is also controlled by dynami. it may or may not be increment-
c ed during each loop. time should be initialized in the intial section.
c dynami utilizes multiple returns to control program flow. the statement
c number passed to dynami should be that of the first statement in the
c integration section. this causes the proper integration looping. at the
c end of each integration step a normal return is executed and control
c returns to the first statement following call dynami. this should be
c the first statement of the post-integration section.
c because variable values may differ from their true value during the
c integration looping, all program logic and variable time step calculations
c executed once at the end of each integration step. time and all variables
c contained within the integration section will be updated to their 'true',
c values before control is transferred to the post-integration section.
c this section should contain at least one if statement which stops program
c execution. and the last statement should be a go to st.no. where st.no.
c is the statement number of the first statement in the integration section.
c approximately 100 integrations may be performed simultaneously.
c
c variable list
c
c a matrix which stores the intermiate values calculated during each loop
c delt integration time step
c dxdt rate being integrated. calculated using integral value as
c returned by intgrl during the previous loop and time set by
c dynami. used by intgrl as called for by icount.
c icount tells intgrl which integration loop is presently being done
c imeth = 1 use runge-kutta method
c = 3 use simpson's rule
c incin tell dynami how many intgrl statements there are in the main
c program.
c ipass tells intgrl to do two special functions during the first two
c executions of the integration section.
c istore tells intgrl where to store the result of its intermediate
c calculation in matrix a.
c xic matrix which store intial conditions and then is updated to the
c present integral value at the end of each integration step.
c xxic initial condition
c
c subroutine dynami(time,*)
common /intgrl/ imeth,icount,istore,incin,ipass,delt,
. xic(101),a(501)
if (ipass.eq.0) go to 40
if (imeth.eq.1) go to 10
c
c simpson's rule (default) imeth>2
c
c if (icount.eq.4) go to 4
c if (icount.eq.3) go to 3
c time=time+delt/2.
c icount=icount+1
c return 1
c 4 continue
c istore=0
c icount=1
c ipass=ipass+1

```


reaction which is strongly depending on the lithium pool
 temp. This gives the experimental RR of W. Ijams. This
 function is used in order to control the RR of Li-N2, since
 the former version of LITFIRE assumes a continuous increase
 in the RR without limit as the gas arrival rate to the
 the combustion zone increases.

```

function rr(tli)
  tli=tli/1.8-273.
  if (tli .ge. 200. .and. tli .lt. 400.) rr=.0080/200.*(tli-200.)
  if (tli .ge. 400. .and. tli .lt. 450.) rr=
    .0080+.0010*(tli-400.)/50.
  if (tli .ge. 450. .and. tli .lt. 500.) rr=
    .0090+.0080*(tli-450.)/50.
  if (tli .ge. 500. .and. tli .lt. 550.) rr=
    .0170+.011*(tli-500.)/50.
  if (tli .ge. 550. .and. tli .lt. 600.) rr=
    .028+.022*(tli-550.)/50.
  if (tli .ge. 600. .and. tli .lt. 650.) rr=
    .050+.043*(tli-600.)/50.
  if (tli .ge. 650. .and. tli .lt. 700.) rr=
    .093+.307*(tli-650.)/50.
  if (tli .ge. 700. .and. tli .lt. 725.) rr=.40+.225*(tli-700.)/25.
  if (tli .ge. 725. .and. tli .lt. 750.) rr=.625+.125*(tli-725.)/25.
  if (tli .ge. 750. .and. tli .lt. 800.) rr=.75+.0667*(tli-750.)/50.
  if (tli .ge. 800. .and. tli .lt. 950.) rr=.89*sin(tli/600-.175)
  if (tli .ge. 950. .and. tli .lt. 1050.) rr=
    .875+.015*(950.-tli)/50.
  if (tli .ge. 1050. .and. tli .lt. 1100.) rr=
    .86+.235*(1050.-tli)/50.
  if (tli .ge. 1100. .and. tli .lt. 1127.) rr=.625*(1127-tli)/27.
  if (tli .gt. 1127. .or. tli .lt. 200.) rr=0.0
  rr=.034106*rr
  tli=(tli+273.)*1.8
  return
end
  
```

C
C
C

```

function akexx(t01,t02,rhobar)
  ginbar=32.2
  tbar=0.5*(t01+t02)
  bbar=1.0/tbar
  dbar=((4.94e-05*tbar+0.0188)/(rhobar*3600.))**2
  akbar=(0.014+1.92e-05*(tbar-460.))/3600.
  exbar=(ginbar*bbar*abs(t01-t02)/dbar)**0.3333
  akexx=akbar*exbar
  return
end
  
```

C
C
C
C

```

this function is for calculating the partial pressure of lithium in
lithium-lead as a function of concentration
function actvty(xali)
  aliln=8.835*(xali**2.219)-6.0
  if (aliln .gt. 0.0) aliln=0.0
  actvty=xali*exp(aliln)
  return
end
  
```

C these subroutines are used to modularize litfire. they include the
 C options of two cell geometry and pan geometry as well as floor and
 C concrete combustion.

```

C this is the secondary cell subroutine.
C subroutine cell2
implicit real (i,k,l,m)
logical flagn,flagw,flagv,flagf,flag2,flagst,flagtr,
common // name(340),flag2,flagas,flagc,flagf,flagn,flagst,flagtr,
      flagpn,flagw,ipage,ishwch,iarosl,flagdf,icz,flagco
common /looper/ i10,i11,i12,i13,i14,i15,i16,i17,i18,i1
common /intgl/ imeth,icount,istore,inoin,ipass,delt,
      xic(101),zzz(501)
common /lith/ akli,asli,cpli,csbli,hb,libp,lil,lilp,lit,
      rli,spil,tli,tlii,zli
common /steel/ cpsfp,cpsfs,cpswp,cpsws,estlfp,estlwp,kstlfp,
      kstlfs,kstlwp,kstlws,rhsfp,rhsfs,rhswp,rhsws
common /misc/ afp,afs,awp,aws,c7,c21,gin,
      ha,hinfam,hinsam,htcpgp,gradc,radc,rczw,
      rhoap,rliw,rwpws,sigma,ta,tc(20),tfs,
      tfszer,tgp,tgs,tgpzer,tspf,tsp,tss,
      tsszer,thfp,thfs,thwp,thws,zzes,zz5,zzs,zz1,zz7,
      rair
common /conop/ c8,cpccon,dtbdt(20),dtcddt(20),gap,kcon,kgap,
      l(20),ll(20),nl,nll,gradb,radb,rhcon,
      sflcr,tb(20),tbf(20),tbic(20),tcf(20),
      tcic(20),thfc,thwc,tsfpi,tspzer,xfsl,qlflr,qvflr
common /injop/ dpi,dp2,dp3,mninij,moxinj,time,vp
common /secop/ aehcs,c11,c20,chs,cpehcs,cph2,cplih,cpwa,crack,
      foutp,fouts,foutt,hinfgs,hinfgs,hinfgs,hinfgs,hinfgs,hinfgs,kleak,
      leak,mairp,mairs,mais,mas,mh2s,mlihs,mlinis,mllins,
      mliois,mlios,mniis,mnis,moxs,moxs,mwais,
      mlc3s,mlc2s,mcs,mco2s,rholc3,rholc2,rhocar,
      mwas,pap,pas,passer,ra,rbreak,rholih,
      rholin,rholio,rwpgas,tehcs,tehcsf,tehczs,tgssf,
      tfsf,tgszer,tssf,vs,xmdot,xmehcs,xmola,zz3,zzfs
common /steam/ tgps,vg,xg,sat(35,10),sh(7,110,5),uwv,hwv,cpwv,vvg,
      ph2o,ulp,tlp,vlp,hlp,vvb,hfg,ph2ob,cpvb,hu(15,2),
      phase,hum,cpa,mwl,mwv,ul,uv,ulz,uvz,mwlz,
      mwvz,uvzer,ulzer,mwv,mwlv,vl,zzep,mwvzer,mwlzer,
      xmoip,cell
common /steam2/cpa2,cpvb2,emgs,hfg2,hlp2,htcpgs,hum2,mwl2,
      mwlv2,mwlz2,mwlr2,mwv2,mwvz2,mwvz2,mwvzr2,
      phase2,ph2ob2,ph2ob2,rair2,tlp2,ul2,ulp2,ulz2,
      ulzer2,uv2,uvz2,uvzer2,uvz2,vg2,vl2,vlp2,vvb2,
      vvg2,xg2,xmols,stain2,stout2,xinj2,rhoas
common /heat2/ hinecs
C
C if (flagn) n=1
C go to (1,2,3,4,5)n
C 1 continue
C
C***** read in secondary cell parameters and *****
C initial conditions
C
C read (3,701) vs,chs,passer,tgszer,tsszer,tfszer
C read (3,701) crack,hum2,wo2s,was,cpas,wco2s
C read (3,701) tehczs,xmehcs,aehcs,cpehcs,hinecs
C read (3,701) estlws,cpsws,kstlws,rhsws,aws,thws
C read (3,701) estlfs,cpsfs,kstlfs,rhsfs,afs,thfs
C if (ishwch .eq. 1) read (3,701) tswich
C
C write (10,800) chs,vs,wo2s,hum2,was,cpas,crack,wco2s
C write (10,801) tehczs,xmehcs,aehcs,cpehcs,hinecs
C write (10,802) tgszer,tsszer,tfszer,passer

```

```

write (10,803) estlws,cpsws,kstlws,rhsws,aws,thws
write (10,804) estlfs,cpsfs,kstlfs,rhsfs,afs,thfs
if (iswich .eq. 1) write (10,810) tswich

C
700 format(20a4)
701 format (6f12.4)
800 format (' secondary containment dimensions'/lx,32(1h-)//t10,
. 'chs = ',f12.4,t35,'vs = ',f12.4,t60,'wo2s = ',f12.4//t10,
. 'hum2 = ',f12.4,t35,'was = ',f12.4,t60,'cpas = ',f12.4//t10,
. 'crack = ',f12.4,t35,'wco2s = ',f12.4//)
801 format(' extraneous heat capacity node data'/lx,33(1h-)//t10,
. 'tehcxs = ',f12.4,t35,'xmechs = ',f12.4,t60,'aehcs = ',f12.4//
. t10,'cpehcs = ',f12.4,t35,'hinecs = ',f12.4//)
802 format (' secondary initial conditions'/lx,28(1h-)//t10,
. 'tgszr = ',f12.4,t35,'tsszr = ',f12.4,t60,'tfszr = ',f12.4//t10,
. 'paszr = ',f12.4//)
803 format (' secondary steel wall data'/lx,25(1h-)//t10,
. 'estlws = ',f12.4,t35,'cpsws = ',f12.4,t60,'kstlws = ',f12.4//t10,
. 'rhsws = ',f12.4,t35,'aws = ',f12.4,t60,'thws = ',f12.4//)
804 format (' secondary steel floor data'/lx,26(1h-)//t10,
. 'estlfs = ',f12.4,t35,'cpsfs = ',f12.4,t60,'kstlfs = ',f12.4//t10,
. 'rhsfs = ',f12.4,t35,'afs = ',f12.4,t60,'thfs = ',f12.4//)
810 format (' closing of crack between primary and secondary cells
. is'/'allowed when time is greater than tswich = ',f11.2//)

C
n=2
return
2 continue
c***** initialize secondary cell containment variables *****
data braks,foutp,fouts,foutt,mh2s,mlihs,mlihs,mlihs,mlihs,mlihs,mlihs
. ,mlc3s,mlc3is,rbreak,xmdot,zz3,zzes,ul2,ulz2,uv2,uvz2,
. ,mw12,mw1z2,mwv2,mwvz2/24*0.0/

flagm=.false.
gamma=1.4
cd=1.
tehcxs=tehcxs
tss=tsszr
thfs=thfp
tfs=tfszr
tgs=tgszr

C
c *** initialize the amount of water vapor in the secondary cell ***
flagn=.true.
if(flagst) call steam2
flagn=.false.
c *****
c *****
C
wn2s=1.-wo2s-was-wco2s
xmols=1./((wo2s/32.+wn2s/28.+was/xmola+wco2s/44.))
rins=i545./xmols
rhoais=paszr*144./rins/tgszr
if(flagst)rhoais=(paszr-ph2o2)*144./rins/tgszr
rhoas=rhoais
mniis=wn2s*rhoais*vs
mniis=mniis
moxis=wo2s*rhoais*vs
moxis=moxis
mais=was*rhoais*vs
mais=mais
mco2is=wco2s*rhoais*vs
mco2is=mco2is

```

```

C      if(flagst)wvas=mwv2/(mnis+moxis+mas+mwv2)
C**** determine the initial energy of the secondary vapor region ***
C      if(flagst)call steam2
C***** conversion to ft. - lb. - sec. *****
C      crack=crack/144.
C      kstlws=kstlws/3600.
C      kstlfs=kstlfs/3600.
C      n=3
C      return
C      3 continue
C *** zero temperature rates of change *****
C      zzes=0.0
C      zzfs=0.0
C      zzs=0.0
C**** compute physical properties dependent on temperature *****
C**** calculate air composition and specific heat at const. volume *****
C      maixs=moxs+mnis+mh2s+mas+mco2s
C      xmolS=(28.*mnis+32.*moxs+2.*mh2s+xmola*mas+44.*mco2s)/maixs
C      rair2=1545./xmolS
C      rhoas=maixs/vs
C      foxs=moxs/maixs
C      fwas=mwv2/(mwv2+maixs)
C      fnis=mnis/maixs
C      fco2s=mco2s/maixs
C      cpo2s=(0.184+3.2e-06*tgs-1.36e04/(tgs*tgs))
C      cpmoxs=cpo2s*moxs
C      cpn2s=(0.172+8.57e-06*tgs+1.02e-09*tgs*tgs)
C      cpc02s=.201
C      cpmcos=cpc02s*mco2s
C      cplc3s=.761
C      cpm1cs=cplc3s*mlc3s
C      cpmnis=cpn2s*mnis
C      cplios=0.0602*tgs**326
C      cplins=0.3368+3.67e-04*tgs
C      cpmlos=cplios*malios
C      htcpgs=cpmoxs+cpmnis+cpmlcs+cpmlos+cpas*mas+cplins*mlins+cplih*mlih+
C      .   cph2*mh2s+cpmcos+cpmlcs
C      cpa2=htcpgs/(maixs+mlins+mlih+mlc3is)
C**** calculating radiative interchange factors *****
C      emgs=1.-exp(-(mlios/rholio+mlins/rholin+mlih/rholih+mlc3s/rholc3)
C      *2.27e05*chs/vs/ra)
C      if (emgs .le. 0.005) emgs=0.005
C *** calculate emissivity and temperature of secondary cell gas ***
C      if(flagst)call steam2
C *****
C      rifps=1./((1.-estlwp)/estlwp+(1.-estlws)/estlws*(awp/aws)+
C      (1.+awp/aws)/(1.+awp/aws*(1.-emgs)))
C      rifpga=(estlwp*emgs)/((1.-estlwp)*emgs+estlwp)
C      rifpps=1./((1.-estlfp)/estlfp+(1.-estlfs)/estlfs*(asli/afs)+
C      (1.+asli/afs)/(1.+asli/afs*(1.-emgs)))
C      riffs=(estlfp*emgs)/((1.-estlfp)*emgs+estlfp)
C      rifsCW=(estlws*emconc)/((estlws+emconc)-estlws*emconc)
C      rifsCF=(estlfs*emconc)/((estlfs+emconc)-estlfs*emconc)
C *** check for boiling and condensation, calculate heat transfer *****
C      if(flagst)call steam2
C

```

```

C *** calculating gas heat transfer coefficients (without steam) *****
  if (.not. flagst .or. mvv.le.0.0) then
C secondary gas to secondary extraneous heat capacity
  hehcs=hinesc*akexx(tgs,tehcs,rhoas)
C secondary steel liner to secondary gas
  hsec=hingsc*akexx(tgs,tss,rhoas)
C primary steel wall liner to secondary containment gas
  hwpgas=hinpsc*akexx(tsp,tgs,rhoas)
C primary steel floor liner to secondary containment gas
  hfpgas=hinfpsc*akexx(tsfp,tgs,rhoas)
C secondary steel floor to secondary cell gas
  hfsgas=hinfsg*akexx(tfs,tgs,rhoas)
  endif
C secondary steel liner to ambient (superceded by concrete to ambient
C if concrete option in use)
  if (.not. flagw) ha=hinsam*akexx(tss,ta,.074)
C secondary steel floor liner to ambient
  if (.not. flagf) hamf=hinfam*akexx(tfs,ta,.074)
100 continue
C **** calculate gas heat transfer coefficients with steam present ***
  if (flagst) call steam2
C
C **** calculating thermal diffusivities between nodes *****
  c11=kstlws*ha/(rhsws*cpsws*thws*(kstlws+thws*ha/2.))
  c12=kstlfs*hamf/(rhfs*cpsfs*afsf*(kstlfs+thfs*hamf/2.))
  c14=kstlfs*hfsgas/(rhfs*cpsfs*thfs*(thfs*hfsgas/2.+kstlfs))
  c15=kstlfs*hfsgas*afsf/htcpgs/(thfs*hfsgas/2.+kstlfs)
  c18=kstlfp*hfpgas/(rhfs*cpsfp*thfp*(thfp*hfpgas/2.+kstlfp))
  c19=kstlfp*hfpgas*afsf/htcpgs/(thfp*hfpgas/2.+kstlfp)
  c20=kstlwp*hwpgas/(rhswp*cpswp*thwp*(thwp*hwpgas/2.+kstlwp))
  c21=kstlwp*hwpgas*afsf/htcpgs/(thswp*hwpgas/2.+kstlwp)
  c22=kstlws*hsec/(rhsws*cpsws*thws*(thws*hsec/2.+kstlws))
  c23=kstlws*hsec*afsf/htcpgs/(thws*hsec/2.+kstlws)
  cehcgs=hehcs*aehcs/htcpgs
  cgsehc=hehcs*aehcs/xmechcs/cpehcs
C
C *** steam injection into secondary cell option *****
  xinj2=0.0
  if (flagst.and.(time.ge.stain2 .and. time.le.stout2)) xinj2=1.
C
C **** calculating radiative heat transfer between nodes *****
  qradps=sigma*awp*(tsp**4-tss**4)*rifps
  rwpws=qradps/(thwp*awp*rhswp*cpswp)
  rswps=qradps/(thws*aws*rhsws*cpsws)
  qradfs=sigma*asli*(tsfp**4-tfs**4)*riffs
  rfps=qradfs/(thfp*asli*rhfs*cpsfp)
  rffps=qradfs/(thfs*afsf*rhfs*cpsfs)
  qradpg=sigma*awp*(tsp**4-tgs**4)*rifpga
  rwpgas=qradpg/(thwp*awp*rhswp*cpswp)
  rpgps=qradpg/htcpgs
  qradfg=sigma*asli*(tsfp**4-tgs**4)*riffgs
  rfpgas=qradfg/(thfp*asli*rhfs*cpsfp)
  rgasfp=qradfg/htcpgs
  n=4
  return
4 continue
C **** calculating radiation from outer steel liners *****
  if (.not. flagw) qradc=sigma*aws*(tss**4-ta**4)*estlws
  if (flagw) qradc=sigma*aws*(tss**4-tc(1)**4)*rifscw
  radc=qradc/(thws*aws*rhsws*cpsws)
  if (.not. flagf) qradb=sigma*afsf*(tfs**4-ta**4)*estlfs
  if (flagf) qradb=sigma*afsf*(tfs**4-tb(1)**4)*rifscf

```



```

radb=qradb/(thfs*afs*rhsfs*cpsfs)
c* modifying primary steel wall and floor temperature rates of change
zz5=zz5-c20*(tsp-tgs)-rwpws-rwpgas
if (mwv2.gt.0.0)zz5=zz5-c20*(tsp-tgs)
zz7=zz7+csbli*(tli-tsfp)-c18*(tsfp-tgs)-rfpfs-rfpgas
if (mwv2.gt.0.0)zz7=zz7-c18*(tsfp-tgs)
if ((mw12*vlp2/afs).gt.0.1)zz7=zz7+rfpfs
calculate extraneous heat capacity temperature rate of change
zses=zses+cgsehc*(tgs-tehcs)
if (mwv2.gt.0.0)zses=zses-cgsehc*(tgs-tehcs)
calculate outer cell gas temperature rate of change deg r/sec
if (.not.flagst)then
zz3=breaks+rspgs+c22*(tsp-tgs)+c19*(tsfp-tgs)+rgasfp+c15*(tfs-tgs)
+cehcgs*(tehcs-tgs)+c19*(tsfp-tgs)+rgasfp+c15*(tfs-tgs)
else
uvz2=uvz2+gradpg+qradfg
if (mwv.le.0.0)uvz2=uvz2+c22*(tsp-tgs)*htcpgs+c23*(tss-tgs)*htcpgs
+cehcgs*(tehcs-tgs)*htcpgs+c19*(tsfp-tgs)*htcpgs
+rgasfp*htcpgs+c15*(tfs-tgs)*htcpgs
endif
calculate outer wall steel temperature rate of change deg r/sec
if (.not.flagw) zzs=zzs+c21*(tgs-tss)-c11*(tss-ta)+rwswp-radc
if (flagw) zzs=zzs+c21*(tgs-tss)-c7*(tss-tc(l))+rwswp-radc
if (mwv2.gt.0.0) zzs=zzs-c21*(tgs-tss)
calculate outer floor steel temperature rate of change deg r/sec
if (.not.flagw) zzfs=zzfs+c14*(tgs-tfs)-c12*(tfs-ta)+rfsfp-radb
if (flagw) zzfs=zzfs+c14*(tgs-tfs)-c8*(tfs-tb(l))+rfsfp-radb
if (mwv2.gt.0.0) zzfs=zzfs-c14*(tgs-tfs)
if ((mw12*vlp2/afs).gt.0.1) zzfs=zzfs-rfsfp
n=5
return
5 continue
c*****
c** calculating overpressure **
c*****
xmairs=moxs/32.+mnis/28.+mas/xmola+mco2s/44.
pas=1545.*xmairs*tgs/144./vs
if (flagst)pas=pas+ph2o2
overps=pas-paszer
c*****
c** calcu. total leakage ***
c*****
leak=kleak*(abs(pas-14.7))*.0.5
if (pas.lt.14.7) leak=0.
if (abs(pap-pas).lt.0.0006 .and. iswich .eq. 1 .and.
time.gt.tswich) crack=0.0
if (crack .eq. 0.0 .and. iswich .eq. 1) write (11,815) time
815 format (' cell pressures have equilized at time = ',f11.2/
. 'crack size has been set to zero for remainder of calculation')
if (crack .eq. 0.0) iswich=0
if (crack .eq. 0.0) go to 112
if (abs(pap-pas).lt.0.0006) go to 106
if (pap-pas)101,106,107
c**** flow out of secondary into primary *****
101 fouthp=0.
if (pap/pas .ge. 0.53) go to 103
c**** sonic *****
if (flagm) go to 102
c**** first time sonic *****
write (12,816)
ipage=ipage+1
flagm=.true.

```

```

102 xmdot=cd*crack*12.*sqrt(0.94*gin*pap*rhoas)
if(flagst)xmdot=cd*crack*12.*sqrt(0.94*gin*pap*(rhoas+1./vg2))
go to 105
c**** subsonic ****c
103 if (.not. flagm) go to 104
c**** first time back to normal subsonic ****c
write (12,817)
ipage=ipage+1
flagm=.false.
104 xmdot=cd*crack*sqrt(2.*gin*(pap-pap)*rhoas)*12.
if(flagst)xmdot=cd*crack*sqrt(2.*gin*(pap-pap)*(rhoas+1./vg2))*12.
105 fouts=xmdot/mairs
if(flagst)fouts=xmdot/(mairs+mwv2)
rbreak=xmdot*(gamma*tgs-tgp)/(mairp+mwv+delt*xmdot)
breaks=xmdot*tgs*(1.-gamma)/(mairs+mwv2-delt*xmdot)
go to 112
c**** no flow ****c
106 fouts=0.
fouts=0.
xmdot=0.
rbreak=0.
breaks=0.
go to 112
c**** flow out of primary into secondary ****c
107 fouts=0.
if (pap/pap.ge. 0.53) go to 109
c**** if (flagm) go to 108 ****c
c**** first time sonic ****c
write (12,816)
ipage=ipage+1
flagm=.true.
108 xmdot=cd*crack*12.*sqrt(0.94*gin*pap*rhoap)
if(flagst)xmdot=cd*crack*12.*sqrt(0.94*gin*pap*(rhoap+1./vg))
go to 111
c**** subsonic ****c
109 if (.not. flagm) go to 110
c**** first time back to normal subsonic ****c
write (12,817)
ipage=ipage+1
flagm=.false.
110 xmdot=cd*crack*sqrt(2.*gin*(pap-pap)*rhoap)*12.
if(flagst)xmdot=cd*crack*sqrt(2.*gin*(pap-pap)*(rhoap+1./vg))*12.
111 fouts=abs(xmdot)/(mairp+mwv)
rbreak=abs(xmdot)*tgp*(1.-gamma)/(mairp+mwv-delt*abs(xmdot))
breaks=abs(xmdot)*(gamma*tgp-tgs)/(mairs+mwv2+delt*abs(xmdot))
xmdot=0.-xmdot
816 format (' flow between primary and secondary has become sonic')
817 format (' flow between primary and secondary has returned to subson
.ic')
112 continue
fouts=fouts+leak
c *** calculate hydrogen buildup in secondary cell ***
hrat2=mh2s/2./((xmairs+mwv2/18.))
c
n=3
return
end
c
c
c this is the torus fire subroutine.
subroutine torus

```

```

implicit real (i,k,l,m)
logical flagn,flagm,flagw,flagf,flag2,flag3,flagtr,flagst,flagtr,
common // name(340),flag2,flag3,flagf,flag2,flag3,flagtr,flagst,flagtr,
      flagpn,flagw,ipage,ismwch,iarosl,flagdf,icz,flagco
common /looper/ il0,il1,il2,il3,il4,il5,il6,il7,il8,il
common /intgl/ imeth,icount,istore,inoin,ipass,delt,
      xic(101),zzz(501)
common /lith/ akli,asli,cpli,csbli,hb,libp,lil,lilp,lit,
      rhli,spill,tli,tlii,qli
common /steel/ cpsfp,cpsfs,cpswp,cpsws,estlfp,estlwp,kstlfp,
      kstlfs,kstlwp,kstlws,rhsfp,rhsfs,rhswp,rhsws
common /misc/ afp,afw,awp,aws,c7,c21,gin,
      ha,hinfam,hinsam,hctpgp,gradc,radc,rczw,
      rhoap,rliw,rwpws,sigma,ta,tc(20),tfs,
      tfszer,tgp,tgs,tdpzer,tsp,tss,
      tsszer,thfp,thfs,thwp,thws,zzes,zzs,zzz,zz1,zz7
common /injop/ dp1,dp2,dp3,mnininj,moxinj,time,vp
common /conop/ c8,cpccon,dtdt(20),dtdt(20),gap,kcon,kgap,
      l(20),li(20),nl,nli,gradb,radb,rhcon,
      sficr,tb(20),tbf(20),tbic(20),tcf(20),
      tffc(20),thfc,thwc,tsfpi,tspzer,xsfl,qlflr,qvflr
common /secop/ aehcs,c11,c20,chs,cpehcs,cph2,cplih,cpwa,crack,
      foup,fouts,foutt,hinfgs,hinfg,hinfgs,hinps,kleak,
      leak,mairp,mairs,majs,mah2s,mlihs,mlinis,mmins,
      mliois,mlios,mnis,mnis,moxis,moxs,mwais,
      mlc3s,mlc2s,mcs,mco2s,rholc3,rholc2,rhocar,
      mwas,pap,pas,passer,ra,rbreak,rholih,
      rholin,rholio,rwpgas,tehcs,tehcsf,tehczs,tgsf,
      tfsf,tgszer,tssf,vs,xmdot,xmehcs,xmola,zz3,zzfs
common /torus/ amag,ashl,clchcs,cpmag,cpshl,eehcs,eshl,
      hinmag,hinshl,kehcs,khe,kshl,the,thshl,tmag,tmagf,
      tmagz,tshl,tshlf,tshlz,zzshl,zzmag
common /face/ tblio,tshio,tshoo,zzbli,zzshi,zzsho,tbli,tshi,tsho,
      tmano,tman,xmsho,xmag,zzman
common /steam/ tgps,vg,xg,sat(35,10),sh(7,110,5),uvw,hvv,cpwv,vvg,
      ph2o,ulp,tlp,vlp,hlp,vvb,hfg,ph2ob,cpvb,hu(15,2),
      phase,hum,cpa,mvl,mvv,ul,uv,ulz,uvz,mvlz,
      mvz,uvzer,ulzer,mvv,mvlv,vl,zzep,mvzzer,mvlzer,
      xmolp,cell
common /steam2/cpa2,cpvb2,emgs,hfg2,hlp2,htcpgs,hum2,mw12,
      mwlv2,mwlvz2,mwlvz2,mwv2,mwvz2,mwvzr2,
      phase2,ph2o2,ph2ob2,rair2,tlp2,ulp2,ulz2,
      ulzer2,uv2,uvz2,uvzer2,uvw2,vg2,vl2,vlp2,vvb2,
      vvg2,xg2,xmols,stmin2,stout2,xinj2,rhoas
common /heat2/ hinecs
common /decay/ gofw1,gofw2,gofw3,expfw1,expfw2,expfw3,
      gob11,gob12,gob13,expb11,expb12,expb13,
      gob14,gob15,gob16,expb14,expb15,expb16,
      qosh1,qosh2,qosh3,expsh1,expsh2,expsh3,
      gob111,gob112,gob113,expb11,expb12,expb13,
      qosh11,qosh12,qosh13,qosh1,qosh2,qosh3
      if (flagn) n=1
      go to (1,2,3,4,5)n
      1 continue
C***** read in secondary cell parameters and *****
C      initial conditions
C
      read (7,701) vs,chs,passer,tgszer,tsszer,tfszer
      read (7,701) crack,hum2,wo2s,was,cpas,wco2s
      read (7,701) tehczs,xmehcs,aeahcs,cpehcs,hinecs,kehcs

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read (7,701) estlws,cpsws,kstlws,rhsws,aws,thws
read (7,701) estlfs,cpsfs,kstlfs,rhsfs,afs,thfs
read (7,701) clehcs,eehcs,ebli,efwi,vieww
read (7,701) tshlz,thshl,kshl,xmshl,cpshl,ashl
read (7,701) eshl,hinshl,tmagz,amag,xmag,cpmag
read (7,701) hinmag,khe,the,loca,viewg,viewb
read (7,701) kbli,thbli,cpbli,abli,xmbli,tblio
read (7,701) tshio,tshoo,thshi,thsho,xmshi,xmsho
read (7,701) thman,xman,cpman,aman,tmano,kman
read (7,702) qofw1,expfw1,qofw2,expfw2,qofw3,expfw3
read (7,702) qobl1,expbl1,qobl2,expbl2,qobl3,expbl3
read (7,702) qobl4,expbl4,qobl5,expbl5,qobl6,expbl6
read (7,702) qobl11,expbl11,qobl12,expbl12,qobl13,expbl13
read (7,702) qosh1,expsh1,qosh2,expsh2,qosh3,expsh3
read (7,702) qosh11,qosh12,qosh13,qosh1,qosh2,qosh3
if (iswch .eq. 1) read (3,701) tswich

write (10,800) chs,vs,w02s,hum2,was,cpas,crack,wco2s
write (10,801) tehczs,xmehcs,aeahcs,cpehcs,hinecs,kehcs,clehcs,
    eehcs,loca,ebli,efwi,viewg,viewb,vieww
write (10,802) tgszser,tsszser,tfszser,paszser
write (10,803) estlws,cpsws,kstlws,rhsws,aws,thws
write (10,804) estlfs,cpsfs,kstlfs,rhsfs,afs,thfs
write (10,805) tshlz,thshl,kshl,xmshl,cpshl,ashl,eshl,hinshl,
    khe,the,xmshi,xmsho,thshi,thsho,tshio,tshoo

write (10,806) tmagz,amag,xmag,cpmag,hinmag
write (10,809) kbli,thbli,cpbli,abli,xmbli
write (10,808) thman,xman,cpman,aman,tmano,kman
write (10,807) qofw1,qofw2,qofw3,expfw1,expfw2,expfw3,
    qobl1,qobl2,qobl3,expbl1,expbl2,expbl3,
    qobl4,qobl5,qobl6,expbl4,expbl5,expbl6,
    qosh1,qosh2,qosh3,expsh1,expsh2,expsh3,
    qobl11,qobl12,qobl13,expbl11,expbl12,expbl13,
    qosh11,qosh12,qosh13,qosh1,qosh2,qosh3

if (iswch .eq. 1) write (10,810) tswich

700 format(20a4)
701 format(6f12.4)
702 format(6e9.2)
800 format (' secondary containment dimensions'/lx,32(1h-)//t10,
    ,chs = ,f12.4,t35,vs = ,f12.4,t60,w02s = ,f12.4//t10,
    ,hum2 = ,f12.4,t35,was = ,f12.4,t60,cpas = ,f12.4//t10,
    ,crack = ,f12.4,t35,wco2s = ,f12.4//)
801 format(' reactor blanket node data'/lx,25(1h-)//t10,
    ,tehczs = ,f12.4,t35,xmehcs = ,f12.4,t60,aeahcs = ,f12.4//
    ,t10,cpehcs = ,f12.4,t35,hinecs = ,f12.4//t10,kehcs = ,f12.4,
    ,t35,clehcs = ,f12.4,t60,eehcs = ,f12.4//t10,loca = ,f12.4//
    ,t10,ebli = ,f12.4,t35,efwi = ,f12.4,t60,viewg = ,f12.4//
    ,t10,viewb = ,f12.4,t35,vieww = ,f12.4//)
802 format (' secondary initial conditions'/lx,28(1h-)//t10,
    ,tgszser = ,f12.4,t35,tsszser = ,f12.4,t60,tfszser = ,f12.4//t10,
    ,paszser = ,f12.4//)
803 format (' secondary steel wall data'/lx,25(1h-)//t10,
    ,estlws = ,f12.4,t35,cpsws = ,f12.4,t60,kstlws = ,f12.4//t10,
    ,rhsws = ,f12.4,t35,aws = ,f12.4,t60,thws = ,f12.4//)
804 format (' secondary steel floor data'/lx,26(1h-)//t10,
    ,estlfs = ,f12.4,t35,cpsfs = ,f12.4,t60,kstlfs = ,f12.4//t10,
    ,rhsfs = ,f12.4,t35,afs = ,f12.4,t60,thfs = ,f12.4//)
805 format (' blanket shield data'/lx,19(1h-)//t10,tshlz = ,
    ,f12.4,t35,thshl = ,f12.4,t60,ksh1 = ,f12.4//t10,xmsh1 = ,
    ,f12.4,t35,cpsh1 = ,f12.4,t60,ashl = ,f12.4//t10,eshl = ,f12.4,
    ,t35,hinsh1 = ,f12.4,t60,khe = ,f12.4//t10,the = ,f12.4,

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```

.t35,'xmshi'='f12.4,t60,'xmsho'='f12.4//
.t10,'thshi'='f12.4,t35,'thsho'='f12.4,t60,'tshio'='f12.4//
.t10,'tshoo'='f12.4//
806 format (' secondary extraneous heat capacity data'/'lx,40(1h-))//
.t10,'tmagz'='f12.4,t35,'amag'='f12.4,t60,'xmag'='f12.4//t10,
.'cpmag'='f12.4,t35,'hinmag'='f12.4//)
807 format (' blanket internal heat generation data'/'lx,37(1h-
'/'t10,'qofw1'='e9.2,t35,'qofw2'='e9.2,t60,'qofw3'='e9.2
'/'t10,'expfw1'='e9.2,t35,'expfw2'='e9.2,t60,'expfw3'='e9.2
'/'t10,'qobl1'='e9.2,t35,'qobl2'='e9.2,t60,'qobl3'='e9.2
'/'t10,'expbl1'='e9.2,t35,'expbl2'='e9.2,t60,'expbl3'='e9.2
'/'t10,'qobl4'='e9.2,t35,'qobl5'='e9.2,t60,'qobl6'='e9.2
'/'t10,'expbl4'='e9.2,t35,'expbl5'='e9.2,t60,'expbl6'='e9.2
'/'t10,'qosh1'='e9.2,t35,'qosh2'='e9.2,t60,'qosh3'='e9.2
'/'t10,'expsh1'='e9.2,t35,'expsh2'='e9.2,t60,'expsh3'='e9.2
'/'t10,'qobl1'='e9.2,t35,'qobl2'='e9.2,t60,'qobl3'='e9.2
'/'t10,'expbl1'='e9.2,t35,'expbl2'='e9.2,t60,'expbl3'='e9.2
'/'t10,'qosh1'='e9.2,t35,'qosh2'='e9.2,t60,'qosh3'='e9.2
'/'t10,'qosh1'='e9.2,t35,'qosh2'='e9.2,t60,'qosh3'='e9.2//)
808 format (' blanket manifold node data'/'lx,27(1h-
'/'t10,'thman'='f12.4,t35,'xman'='f12.4,t60,'cpman'='f12.4
'/'t10,'aman'='f12.4,t35,'tmano'='f12.4,t60,'kman'='f12.4//)
809 format (' blanket interface node data'/'lx,28(1h-
'/'t10,'kbli'='f12.4,t35,'thbli'='f12.4,t60,'cpbli'='f12.4
'/'t10,'abli'='f12.4,t35,'xmbli'='f12.4//)
810 format (' closing of crack between primary and secondary cells
.is'/'allowed when time is greater than tswich'='f11.2//)
C
n=2
return
2 continue
c***** initialize secondary cell containment variables *****
data breaks,foutp,fouts,foutt,mh2s,mlihs,mlinis,mliins,mliois,mlios
,mlc3s,mlc3is,rbreak,xmdot,zz3,zzes,zzmag,zzshl,
ul2,ulz2,uv2,uvz2,mwl2,mwlz2,mwv2,mwvz2/26*0.0/
flagm=.false.
gamma=1.4
cd=1.
tehcs=tehczs
tbli=tblio
tman=tmano
tss=tsszer
tfs=tfszer
tgs=tgsszer
tmag=tmagz
tshi=tshtz
tshi=tshtio
tsho=tshtoo
C
C *** initialize the amount of water vapor in the secondary cell ***
flagn=.true.
if(flagst) call steam2
flagn=.false.
C *****
C
wn2s=1.-wo2s-was-wco2s
xmols=1./((wo2s/32.+wn2s/28.+was/xmola+wco2s/44.))
rins=1545./xmols
rhoais=paszer*144./rins/tgszer
if(flagst)rhoais=(paszer-ph2o2)*144./rins/tgszer
rhoas=rhoais
aniis=wn2s*rhoais*vs

```

```

mnis=mnis
moxis=wo2s*rhoais*vs
moxs=moxis
mais=was*rhoais*vs
mas=mais
mco2is=wco2s*rhoais*vs
mco2s=mco2is
if(flagst)was=mvv2/(mnis+moxis+mas+mvv2)

C**** determine the initial energy of the secondary vapor region ***
if(flagst)call steam2

C***** conversion to ft. - lb. - sec. *****
crack=crack/144.
kstlws=kstlws/3600.
kstlfs=kstlfs/3600.
kehcs=kehcs/3600.
kman=kman/3600.
kbli=kbli/3600.
khe=khe/3600.
kshl=kshl/3600.
n=3
return
3 continue
C *** zero temperature rates of change *****
zzes=0.0
zzfs=0.0
zzmag=0.0
zszs=0.0
zzsho=0.0

C***** compute physical properties dependent on temperature *****
C***** calculate air composition and specific heat at const. volume *****
mairs=moxs+mnis+mh2s+mas+mco2s
xmols=(28.*mnis+32.*moxs+2.*mh2s+32.*mas+44.*mco2s)/mairs
rair2=1545./xmols
rhoas=mairs/vs
foxs=moxs/mairs
fwas=mvv2/(mvv2+mairs)
fnis=mnis/mairs
fco2s=mco2s/mairs
cpo2s=(0.184+3.2e-06*tgs-1.36e04/((tgs*tgs)))
cpmoxs=cpo2s*moxs
cpn2s=(0.172+8.57e-06*tgs+1.02e-09*tgs*tgs)
cpcos=.201
cpmcos=cpcos*mco2s
cplc3s=.761
cpmlcs=cplc3s*mlc3s
cpmnis=cpn2s*mnis
cplios=0.0602*tgs**.326
cplins=0.3368+3.67e-04*tgs
cpmls=cplios*mlios
htcpgs=cpmoxs+cpmnis+cpmls+cpas*mas+cplins*mlins+cplih*mlih+
      cph2*mh2s+cpmcos+cpmlcs
cpa2=htcpgs/(mairs+mlins+mlih+mlc3is)
C***** calculating radiative interchange factors *****
emgs=1.-exp(-(mlios/rholio+mlins/rholin+mlih/rholih+mlc3s/rholc3)
      *2.27e05*chs/vs/ra)
      if (emgs .le. 0.005) emgs=0.005

C *** calculate emissivity and temperature of secondary cell gas ***
if(flagst)call steam2

```

```

C *****
C
rifbs=1./((1./eehcs+1./eshl-1.))
riffwb=1./((1./efwi+1./ebli-1.))
rifffb=1./((1./efwi+1./ebli-1.))
riffbbi=1./((1./ebli+1./ebli-1.))
rifbm=rifbbi
afacs=ashl/(afp+awp)
rifsw=1./((1.-eshl)/eshl+(1.-estlws)/estlws*awp/awf+afacs*afac+
(1.+awp/awf*afacs)/(1.+awp/awf*afacs*(1.-emgs)))
rifsf=1./((1.-eshl)/eshl+(1.-estlfs)/estlfs*afp/afsf*afacs*afac+
(1.+afp/afsf*afacs)/(1.+afp/afsf*afacs*(1.-emgs)))
rifsgs=(eshl*emgs)/((1.-eshl)*emgs+eshl)
rifscw=(estlws*emconcc)/(estlws+emconcc-estlws*emconcc)
rifscf=(estlfs*emconcc)/(estlfs+emconcc-estlfs*emconcc)
C
C *** check for boiling and condensation, calculate heat transfer *****
C if(flagst)call steam2
C
C ***** calculating gas heat transfer coefficients (without steam) *****
C if(.not. flagst .or. mwv2.le. 0.0)then
C secondary gas to secondary extraneous heat capacity
hmag=hinmag*akexx(tgs,tmag,rhoas)
C secondary steel liner to secondary gas
hsec=hingss*akexx(tgs,tss,rhoas)
C blanket shield to secondary gas
hshi=hinshi*akexx(tgs,tsho,rhoas)
C secondary steel floor to secondary cell gas
hfgas=hinfsg*akexx(tfs,tgs,rhoas)
endif
C secondary steel liner to ambient (superceded by concrete to ambient
C if concrete option in use)
if (.not. flagw) ha=hinsam*akexx(tss,ta,.074)
C secondary steel floor liner to ambient
if (.not. flagf) hamf=hinfam*akexx(tfs,ta,.074)
100 continue
C *** calculate gas heat transfer coefficients with steam present ***
C if(flagst)call steam2
C
C ***** calculating thermal diffusivities between nodes *****
c11=kstlws*ha/(rhsws*cpsws*thws*(kstlws+thws*ha/2.))
c12=kstlfs*hamf/(rhslfs*cpslfs*thslfs*(kstlfs+thslfs*hamf/2.))
c14=kstlfs*hfgas/(rhslfs*cpslfs*thslfs*(thslfs+hfgas/2.+kstlfs))
c15=kstlfs*hfgas*afp/htcpgs/(thslfs*hfgas/2.+kstlfs)
c21=kstlws*hsec/(rhsws*cpsws*thws*(thws+hsec/2.+kstlws))
c23=kstlws*hsec*awf/htcpgs/(thws*hsec/2.+kstlws)
if (khe.eq.0.) then
cshehc=0.
else
cshehc=2.*abli/(xmbli*cpbli)/(thshi/kshl+thbli/kbli+
2.*the/khe)
endif
cwphehc=2.*awp/xmehcs/cpehcs/(thwp/kstlwp+clehcs/kehcs)
cfpehc=2.*afp/xmehcs/cpehcs/(thfp/kstlfp+clehcs/kehcs)
cehcwp=2./((thwp*rhswp*cpswp)/(thwp/kstlwp+clehcs/kehcs)
cehcfp=2./((thfp*rhslfp*cpsfp)/(thfp/kstlfp+clehcs/kehcs)
cmanbl=2.*aman/xman/cpman/(thman/kman+clehcs/kehcs)
cbiman=2.*aman/xman/cpman/(thman/kman+clehcs/kehcs)
cmanbi=2.*abli/xmbli/cpbli/(thbli/kbli+thman/kman)
if (khe.eq.0.) then
cehcsh=0.

```

```

else
cehcs=2.*abli/xmshi/cpshl/(tshsi/kshl+thbli/kbli+
2.*the/khe)
endif
cshosh=2.*ashl*kshl/xmshl/cpshl/(tshsi+thsho)
cshish=2.*ashl*kshl/xmshl/cpshl/(tshsi+thsho)
cshsho=2.*ashl*kshl/xmsho/cpshl/(tshsi+thsho)
cshshi=2.*ashl*kshl/xmshi/cpshl/(tshsi+thsho)
cgsshl=2.*ashl*hshl/xmsho/cpshl/(tsho*hshl/kshl+2.)
cshlgs=2.*ashl*hshl/htcpgs/(tsho*hshl/kshl+2.)
cgsmag=hmag*amag/xmag/cpmag
cmaggs=hmag*amag/htcpgs

C *** steam injection into secondary cell option *****
xinj2=0.0
if(flagst.and.(time.ge.stmin2 .and. time.le.stout2))xinj2=1.

C ***** calculating radiative heat transfer between nodes *****
C *****from first wall to blanket (loca only)*****
gradwb=sigma*awp*(tsp**4-tehcs**4)*riffwb*loca
rfwb=gradwb/awp/thwp/rhswp/cpswp
rbfw=gradwb/xmehcs/cpehcs
C *****from first wall (floor) to blanket (loca only)*****
gradfb=sigma*afp*(tsfp**4-tehcs**4)*riffb*loca
rffb=gradfb/afp/thfp/rhsfp/cpsfp
rbff=gradfb/xmehcs/cpehcs
C *****from blanket to blanket interface (loca only)*****
if(loca.gt.0.0)then
gradeb=sigma*aehcs*(tehcs**4-tbli**4)*riffb1*viewb
rehcb1=gradeb/xmehcs/cpehcs
rblehcb1=gradeb/xmbli/cpbli
endif
C *****from blanket to manifold (loca only)*****
if(loca.gt.0.)then
gradem=sigma*aehcs*(tehcs**4-tman**4)*riffm*viewm
rehcmn=gradem/xmehcs/cpehcs
rmnehc=gradem/xmman/cpman
endif
C *****from shield to blanket*****
grades=sigma*abli*(tbli**4-tshi**4)*riffes*viewg
rehcsh=grades/xmbli/cpbli
rshchc=grades/xmshi/cpshl
C *****from shield to secondary wall*****
qrshws=sigma*ashl*(tsho**4-tss**4)*rifsw
rshws=qrshws/xmsho/cpshl
rwssh=qrshws/(aws*thws*rhsws*cpsws)
C *****from shield to secondary floor*****
qrshfs=sigma*ashl*(tsho**4-tfs**4)*rifsf
rshfs=qrshfs/xmsho/cpshl
rfssh=qrshfs/(afs*thfs*rhfs*cpsfs)
C *****from shield to secondary gas*****
qrshgs=sigma*ashl*(tsho**4-tgs**4)*rifshg
rshgs=qrshgs/xmsho/cpshl
rgssh=qrshgs/htcpgs
C ***** calculating decay heat densities for first wall, blanket and shield
decfw=qofw1*exp(-expfv1*time)+qofw2*exp(-expfw2*time)+
.   qofw3*exp(-expfv3*time)
.   decbl=qobl1*exp(-expbl1*time)+qobl2*exp(-expbl2*time)+
.   qobl3*exp(-expbl3*time)
.   decman=qobl4*exp(-expbl4*time)+qobl5*exp(-expbl5*time)+
.   qobl6*exp(-expbl6*time)
.   decbli=qobl11*exp(-expbl11*time)+qobl12*exp(-expbl12*time)+

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      gobli3*exp(-expbi3*time)
      decsh=qoshi1*exp(-expsh1*time)+qosh2*exp(-expsh2*time)+
      qosh3*exp(-expsh3*time)
      decshi=qoshi1*exp(-expsh1*time)+qoshi2*exp(-expsh2*time)+
      qoshi3*exp(-expsh3*time)
      decsho=qoshol*exp(-expsh1*time)+qoshol2*exp(-expsh2*time)+
      qoshol3*exp(-expsh3*time)
      n=4
      return
4 continue
c**** calculating radiation from outer steel liners ****
if (.not. flagw) qradc=sigma*aws*(tss**4-ta**4)*estlws
if (flagw) qradc=sigma*aws*(tss**4-tc(1)**4)*rifscw
radc=qradc/(thws*aws*rhsws*cpsws)
if (.not. flagf) qradb=sigma*afs*(tfs**4-ta**4)*estlfs
if (flagf) qradb=sigma*afs*(tfs**4-tb(1)**4)*rifscf
radb=qradb/(thfs*afs*rhfs*cpsfs)
c* modifying primary steel wall and floor temperature rates of change
zz5=zz5-cehcwp*(tsp-tehcs)+decfw/rhswp/cpswp-rfwb
zz7=zz7+csbli*(tli-tsfp)-cehcfp*(tsfp-tehcs)+decfw/rhsfp/cpsfp
      -rffb
calculate reactor blanket temperature rate of change
zzes=cwpehc*(tsp-tehcs)+cfpehc*(tsfp-tehcs)-cmanbl*(tehcs-tman)
      +decbl*clehcs*ahcs/xmehcs/cpehcs+rbfw+rbbf-rehcbi-rehcmn
calculate blanket manifold temperature rate of change
zzman=cblman*(tehcs-tman)-cblman*(tman-tbli)+rmnehc+
      decman*thman*aman/xmaan/cpman
calculate blanket interface temperature rate of change
zzbli=cmanbi*(tman-tbli)-cshehc*(tbli-tshi)-rehcsh
      +decbli*thbli*abli/xabli/cpbli+rbiehc
calculate blanket shield temperature rate of change
zzshl=decsh*ashl*thshl/xmshl/cpschl+cshish*(tshi-tshl)
      -cshosh*(tshl-tsho)
calculate shield inner face temperature rate of change
zzshi=rshehc+cehcsh*(tbli-tshi)+decshi*ashl*thshi/xmshi/cpschl
      -cshshi*(tshi-tshl)
calculate shield outer face temperature rate of change
zzsho=zzsho+cshsho*(tshl-tsho)-rshws-rshfs-cgsshl*(tsho-tgs)
      -rshgs+decsho*ashl*thsho/xmsho/cpschl
if (mwv2.gt.0.0)zzsho=zzsho+cgsshl*(tsho-tgs)
if ((mw12*vlp2/afs).gt.0.1)zzsho=zzsho+rshfs
calculate magnet temperature rate of change
zzmag=zzmag+cgsmag*(tgs-tmag)
if (mwv2.gt.0.0)zzmag=zzmag-cgsmag*(tgs-tmag)
calculate outer cell gas temperature rate of change deg r/sec
if (.not. flagst)then
      zz3=breaks+c23*(tss-tgs)+c15*(tfs-tgs)+cshlgs*(tsho-tgs)+
      . cmaggs*(tmag-tgs)+rgssh
else
      uvz2=uvz2+qrshgs
      if (mwv.le.0.0)uvz2=uvz2+c23*(tss-tgs)*htcpgs
      +cmaggs*(tmag-tgs)*htcpgs+cshlgs*(tsho-tgs)*htcpgs
      +rgssh*htcpgs+c15*(tfs-tgs)*htcpgs
endif
calculate outer wall steel temperature rate of change deg r/sec
if (.not. flagw) zzs=zzs+c21*(tgs-tss)-c11*(tss-ta)+rwssh-radc
if (flagw) zzs=zzs+c21*(tgs-tss)-c7*(tss-tc(1))+rwssh-radc
if (mwv2.gt.0.0) zzs=zzs-c21*(tgs-tss)
calculate outer floor steel temperature rate of change deg r/sec
if (.not. flagw) zzfs=zzfs+c14*(tgs-tfs)-c12*(tfs-ta)+rfssh-radb
if (flagw) zzfs=zzfs+c14*(tgs-tfs)-c8*(tfs-tb(1))+rfssh-radb
if (mwv2.gt.0.0) zzfs=zzfs-c14*(tgs-tfs)

```

```

if ((mw12*vlp2/afs).gt.0.1) zzfs=zzfs-rfssh
n=5
return
5 continue
C*****
C** calculating overpressure **
C*****
xmairs=moxs/32.+tnis/28.+mas/xmola+mco2s/44.
pas=1545.*xmairs*tgs/144./vs
if(flagst)pas=pas+ph2o2
overps=pas-paszer
C*****
C** calcu. total leakage ***
C*****
leak=kleak*(abs(pas-14.7))*0.5
if (abs(pap-pas) .lt. 0.0006 .and. iswich .eq. 1 .and.
time .gt. tswich) crack=0.0
815 if (crack .eq. 0.0 .and. iswich .eq. 1) write (11,815) time
. ,crack size has been set to zero for remainder of calculation')
if (crack .eq. 0.0) iswich=0
if (crack .eq. 0.0) go to 112
if (abs(pap-pas) .lt. 0.0006) go to 106
if (pap-pas) 101,106,107
C***** flow out of secondary into primary *****
101 foutp=0.
if (pap/pas .ge. 0.53) go to 103
C***** sonic *****C
if (flagm) go to 102
C***** first time sonic *****c
write (12,816)
ipage=ipage+1
flagm=.true.
102 xmdot=cd*crack*12.*sqrt(0.94*gin*pas*rhoas)
if(flagst)xmdot=cd*crack*12.*sqrt(0.94*gin*pas*(rhoas+1./vg2))
go to 105
C***** subsonic *****c
103 if (.not. flagm) go to 104
C***** first time back to normal subsonic *****c
write (12,817)
ipage=ipage+1
flagm=.false.
104 xmdot=cd*crack*sqrt(2.*gin*(pas-pap)*rhoas)*12.
if(flagst)xmdot=cd*crack*sqrt(2.*gin*(pas-pap)*(rhoas+1./vg2))*12.
105 fouts=xmdot/mairs
if(flagst)fouts=xmdot/(mairs+mwv2)
rbreak=xmdot*(gamma*tgs-tgp)/(mairp+mwv+delt*xmdot)
breaks=xmdot*tgs*(1.-gamma)/(mairs+mwv2-delt*xmdot)
go to 112
C***** no flow *****c
106 foutp=0.
fouts=0.
xmdot=0.
rbreak=0.
breaks=0.
go to 112
C***** flow out of primary into secondary *****c
107 fouts=0.
if (pas/pap .ge. 0.53) go to 109
C***** sonic *****c
if (flagm) go to 108

```

```

c**** first time sonic *****c
write (12,816)
ipage=ipage+1
flagm=.true.
108 xmdot=cd*crack*12.*sqrt(0.94*gin*pap*rhoap)
if(flagst)xmdot=cd*crack*12.*sqrt(0.94*gin*pap*(rhoap+1./vg))
go to 111
c**** subsonic *****c
109 if (.not. flagm) go to 110
c**** first time back to normal subsonic *****c
write (12,817)
ipage=ipage+1
flagm=.false.
110 xmdot=cd*crack*sqrt(2.*gin*(pap-pas)*rhoap)*12.
111 fouth=abs(xmdot)/(mairp+mwv)
break=abs(xmdot)*tgp*(1.-gamma)/(mairp+mwv-delt*abs(xmdot))
breaks=abs(xmdot)*(gamma*tgp-tgs)/(mairs+mwv2+delt*abs(xmdot))
xmdot=0.-xmdot
816 format (' flow between primary and secondary has become sonic')
817 format(' flow between primary and secondary has returned to subson
.ic')
112 continue
fouth=fouts+leak
c *** calculate hydrogen buildup in secondary cell ***
hrat2=mh2s/2./((xmairs+mwv2/18.))
c
n=3
return
end
c
c this is the pan geometry subroutine.
subroutine pan
implicit real (i,k,l,m)
integer tavhi,tavlo,tfhi,tflo
logical flagn,flag2,flagst
real nulv
common // name(340),flag2,flagc,flagf,flagn,flagst,flagtr,
flagpn,flagv,ipage,iswich,iarosl,flagdf,icz,flagco
common /looper/ il0,il1,il2,il3,il4,il5,il6,il7,il8,il9
common /lith/ akli,asli,cpli,csbli,hb,libp,lil,lilp,lit,
rhli,spill,tli,tlii,zli
common /steel/ cpsfp,cpsfs,cpswp,cpsws,estlfp,estlwp,kstlfp,
kstlfs,kstlwp,kstlws,rhsfp,rhsfs,rhswp,rhsws
common /misc/ afp,afs,awp,aws,c7,c21,gin,
ha,hinfam,hinsam,htcpgp,qradc,radc,rczw,
rhoap,rliw,rwpws,sigma,ta,tc(20),tfs,
tfszer,tgp,tgs,tgpzer,tspf,tsp,tss,
tsszer,thfp,thfs,thwp,thws,zzes,zz5,zzs,zzl,zz7,
rair
common /panop/ ains,apan,bredth,clist,cpins,cppan,emgp,fp9,fpw,
kpan,rhins,rhpan,thkini1,thkini2,thkpan,
tins1,tinslf,tinsli,tins2,tins2f,tins2i,
tpan,tpanf,tpanzo,zz2,zz4,zz8,zz9
common /steam/ tgps,v9,xg,sat(35,10),sh(7,110,5),uvw,hwv,cpwv,vvg,
ph2o,ulp,tlp,vlp,hlp,vvb,hfg,ph2ob,cpvb,hu(15,2),
phase,hum,cpa,mvl,mwv,ul,uv,ulz,uvz,mwiz,
mwvz,uvzer,ulzer,mwv,mlv,vl,zzep,mwvzer,mwizer,
xmoldp,cell
common /stmpn/ tsat,hsat,huch
c
if (flagn) n=1

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```

go to (1,2,3)n
1 continue
C***** read in pan geometry parameters *****
C (only if using pan option)
C
C read (4,701) kpan,rhpan,cppan,rhins,cpins,emins
C read (4,701) tpanzo,apan,bredth,ains,hingpf
C read (4,701) thkpan,thkini,thkin2
C
C write (10,800) tpanzo,apan,cppan,thkpan,bredth,kpan,rhpan
C write (10,801) thkini,thkin2,ains,thins,cpins,emins,hingpf
C
C 700 format(20a4)
C 701 format(6f12.4)
C 800 format(////, data for suspended pan optional geometry: '//,ix,
.41(lh-)//t10,'tpanzo =',f12.4,t35,'apan =',f12.4,t60,
. 'cppan =',f12.4//t10,'thkpan =',f12.4,t35,'bredth =',f12.4//t10,
. 'kpan =',f12.4,t35,'rhpan =',f12.4//)
C 801 format(//t10,'thkini =',f12.4,t35,'thkin2 =',f12.4,t60,'ains =',
. 'f12.4//t10,'rhins =',f12.4,t35,'cpins =',f12.4,t60,
. 'emins =',f12.4//t10,'hingpf =',f12.4//)
C
n=2
return
2 continue
C***** initialize pan geometry variables *****
fp9=0.23
fpw=0.384
tins1i=0.5*(tpanzo+tgprer)
tins2i=tgprer
tins1=tins1i
tins2=tins2i
kpan=kpan/3600.
C convert thermal conductivity of li pan to btu/sec-ft-deg R
n=3
return
3 continue
C***** compute physical properties dependent on temperature *****
C***** radiative interchange factors *****
rifpas=1./((1.-emins)/emins+(1.-estlfp)/estlfp*ains/afp+
. (ains/afp+1.)/(1.+ains/afp*(1.-emgp)))
rifpag=emins*emgp/(emins+emgp-emins*emgp)
C***** calculating gas heat transfer coefficients *****
C***** and insulation thermal conductivity *****
hfpgp=hingpf*akexx(tgp,tsfp,rhoap)
hpan=0.714*hb
tet1=0.0025*(tins1-460.)-2.5
kin1=(-.70892+.36584*tet1+.04565*tet1**2-.00791*tet1**3)/43200.
tet2=0.0025*(tins2-460.)-2.5
kin2=(-.70892+.36584*tet2+.04565*tet2**2-.00791*tet2**3)/43200.
C *** modifications to heat transfer due to steam condensation **
C
C if(flagst.and. mvv.gt.0.0)then
C *** liquid pool to primary floor *****
if(mw1.gt.1.0e-02)then
C determine average fluid properties
tave=(tlp+tsfp)/2.

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```

tavhi=int(tave/20.)-23.
tavlo=tavhi-1.
intdsr=(tave/20.)-int(tave/20.)
mulv=(25.3/((tave/1.8)**2.+91.*tave/1.8-8.58e04))/1.488
cplv=(sat(tavhi,9)-sat(tavlo,9))*intdsr+sat(tavlo,9)
vlpv=(sat(tavhi,3)-sat(tavlo,3))*intdsr+sat(tavlo,3)
nulv=mulv*vlpv
kwat=(0.686-5.87e-06*(abs(tave/1.8-415.))**2.+7.3e-10*pap*6895.)
kwat=kwat/1.73/3600.
if(tave.gt.1165.)then
  nulv=1.46e-06
  kwat=8.667e-05
  cplv=1.368
  vlpv=sat(34,3)
endif
tfhi=int(tsfp/20.)-23.
tflo=tfhi-1.
intdsf=(tsfp/20.)-int(tsfp/20.)
vlpf=(sat(tfhi,3)-sat(tflo,3))*intdsf+sat(tflo,3)
if(tsfp.gt.1165.)vlpf=sat(34,3)
betaf=abs(1./vlp*(vlpf-vlp)/(tsfp-tlp2))
c determine h from GrPr
  grprf=32.2*betaf*abs(tsfp-tlp)*afp**1.5
  /vlpv/kwat*cplv/nulv
  if((tsfp.gt.tlp).and.((1.e05.le.grprf).and.
    (grprf.le.2.e07)))then
    ca=0.54
    aa=0.25
  elseif((tsfp.gt.tlp).and.(2.e07.lt.grprf).and.
    (grprf.le.3.e010))then
    ca=0.14
    aa=0.333
  elseif(grprf.gt.3.e010)then
    ca=0.021
    aa=0.4
  elseif((tsfp.lt.tlp).and.(3.e05.le.grprf).and.(grprf.le.3.e10))
  then
    ca=0.27
    aa=0.25
  elseif(tlp.eq.tsfp)then
    ca=0.0
    aa=1.0
  else
    ca=1.0
    aa=1.0
  grprf=1.0
endif
hlpflr=kwat/afp**.5*ca*grprf**aa
zh2o=mw1*vlp/afp
if(hlpflr.lt.(2.*kwat/zh2o))hlpflr=2.*kwat/zh2o
qlflr=2.*(tlp-tsfp)/(thfp/kstlfp+1./hlpflr)
ulz=ulz-qlflr
zz7=zz7+qlflr/rhsfp/afp/thfp/cpsfp
c
else
c primary gas to primary floor--no liquid water
qvflr=2.*(tsat-tsfp)*afp/(thfp/kstlfp+2./huch)
if(tsfp.gt.tsat)then
  rhogp=rhoap+1./vg
  hfpgp=hingp*akexx(tgp,tsfp,rhogp)
  qvflr=2.*(tgp-tsfp)*afp/(thfp/kstlfp+2./hfp9p)

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```

endif
mcondf=qvflr/hfg
if(tsfp.gt.tsat.or.qvflr.le.0.0)mcondf=0.0
mwvz=mwvz-mcondf
mwlz=mwvz+mcondf
uvz=uvz-qvflr
ulz=ulz+mcondf*hsat
zz7=zz7+qvflr/rhsfp/afp/thfp/cpsfp
endif
c gas to pan insulation
qvpans=ains/(thkin2/2./kin2+1./huch)*(tsat-tins2)
if(tins2.gt.tsat)then
hpan=0.714*hb
qvpans=ains/(thkin2/2./kin2+1./hpan)*(tgp-tins2)
endif
mcondp=qvpan/hfg
if(tins2.gt.tsat .or. qvpan.le.0.0)mcondp=0.
mwvz=mwvz-mcondp
mwlz=mwvz+mcondp
uvz=uvz-qvpan
ulz=ulz+mcondp*hsat
zz9=zz9+qvpan/thkin2/rhins/cpins/ains
endif
C ***** calculations with suspended lithium spill pan *****
C
aht=asli+zli*bredth
if(.not.flagst)ypagas=ains/(thkin2/2./kin2+1./hpan)
c2=ypagas/htcpgp
cl3=ypagas/(rhins*ains*thkin2*cpins)
cl6=kstlfp*hfpgp/(rhsfp*cpsfp*thfp*(thfp*hfpgp/2.+kstlfp))
cl7=kstlfp*hfpgp*afp/htcpgp/(thfp*hfpgp/2.+kstlfp)
grads=sigma*ains*(tins2**4-tsfp**4)*rifpas
gradcg=sigma*ains*(tins2**4-tgp**4)*rifpag
rpanst=grads/(rhsfp*afp*thfp*cpsfp)
rstpan=grads/(rhins*ains*thkin2*cpins)
rgaspa=gradcg/(rhins*ains*thkin2*cpins)
rpagas=gradcg/htcpgp
clipan=2.*aht/(lil*cpli)/(zli/akli+thkpan/kpan)
cpanli=2.*aht/(rhpan*apan*thkpan*cpan)/(zli/akli+thkpan/kpan)
cpnini=2./(rhpan*apan*thkpan*cpan)/(thkpan/kpan/apan+thkin1/
kin1/ains)
cinlpn=2./(rhins*ains*thkin1*cpins)/(thkpan/kpan/apan+thkin1/
kin1/ains)
cinl2=2./(rhins*cpins*thkin1)/(thkin1/kin1+thkin2/kin2)
cin2l=cinl2*thkin1/thkin2
C *****modifying primary cell temperature rates of change due to pan ***
zz1=zz1+clist*(tli-tsfp)-clipan*(tli-tpan)
if(.not.flagst)zz4=zz4+c2*(tins2-tgp)+rpagas+c17*(tsfp-tgp)
if(flagst)uvz=uvz+gradcg
zz7=zz7-csbli*(tli-tsfp)+c16*(tgp-tsfp)+rpanst
if(flagst)zz7=zz7-cl6*(tgp-tsfp)
if(flagst.and.(mw1*vlp/afp).gt.0.1)zz7=zz7-rpanst
C ***** calculate li spill pan temp. rate of change deg r/sec *****
zz2=cpanli*(tli-tpan)+cpnini*(tins1-tpan)
C calculate insulation temperature rate of change
zz8=cinlpn*(tpan-tins1)+cinl2*(tins2-tins1)
zz9=zz9+cin21*(tins1-tins2)+c13*(tgp-tins2)-rstpan-rgaspa
if(flagst)zz9=zz9-cl3*(tgp-tins2)
if(flagst.and.(mw1*vlp/afp).gt.0.1)zz9=zz9+rstpan
return

```

```

end
c this is the wall concrete subroutine
subroutine concw
implicit real (i,k,l,m)
integer i,iam
dimension c4(20)
logical flagn,flag2
common // name(340),flag2,flagas,flagc,flagf,flagn,flagst,flagtr,
flagpn,flagv,ipage,iswich,iaros1,flagdf,iczf,flagco
common /looper/ i10,i11,i12,i13,i14,i15,i16,i17,i18,i19
common /lith/ akli,asli,cpli,csbli,hb,libp,i1l,i1lp,lit,
rhli,spili,tli,tlii,zi1
common /steel/ cpsfp,cpsfs,cpswp,cpsvs,estlfp,estlwp,kstlfp,
kstlfs,kstlwp,kstlws,rhsfp,rhsfs,rhswp,rhsws
common /misc/ afp,afs,awp,aws,c7,c21,gin,
ha,hinfam,hinsam,hpcpgp,gradc,radc,rczw,
rhoap,rliw,rwpws,sigma,ta,tc(20),tfs,
tfszer,tgpp,tgs,tgppzer,tspf,tsp,tss,
tsszer,thfp,thfs,thwp,thws,zzes,zz5,zzs,zz1,zz7,
zair
common /intgl/ imeth,icount,istore,inoin,ipass,delt,
xic(101),zzz(501)
common /conop/ c8,cpcon,dtdt(20),dtdt(20),gap,kcon,kgap,
l(20),ll(20),nl,nl1,gradb,radb,rhcon,
sficr,tb(20),tbf(20),tbic(20),tcf(20),
tcic(20),thfc,thwc,tsfpi,tspzer,xsfl,qf1r,qvflr

c
if (flagn) n=1
go to (1,2,3)n
1 continue
i10=1
i11=int(.25*n1)
i12=int(.5*n1)
i13=int(.75*n1)
i14=n1
nl1=nl-1
c***** initialize wall concrete variables *****
data c3,c5,c7,radcc/4*0.0/
if (flag2) go to 100
aws=awp
cpsws=cpswp
kstlws=kstlwp
rhsws=rhswp
thws=thwp
tsszer=tspzer
100 continue
do 1001 iam=1,20
c4(iam)=0.
1001 dtdt(iam)=0.
do 1002 i=1,n1
tcic(i)=tsszer
tc(i)=tsszer
1002 l(i)=thwc*l(i)
n=2
return
2 continue
c***** calculating gas heat transfer coefficient from outermost *****
c
concrete node to ambient
tcnl=tc(nl)
ha=hinsam*akexx(tcnl,ta,.074)
c ***** calculating thermal diffusivities between nodes *****
usuba=kcon*ha/(kcon+ha*l(nl)/2.)

```

```

b=1(1)/(kcon*2.)+gap/kgap+thws/(kstlws*2.)
c3=1./(b*1(1)*rhcon*cpcon)
do 1004 i=1,nlml
c4(i)=2.*kcon/(rhcon*cpcon*1(i)*1(i)+1(i+1))
1004 continue
c5=usuba/(rhcon*cpcon*1(nl))
c7=1./(b*thws*rhsws*cpsws)
n=3
return
3 continue
if (.not. flag2) tss=tsp
radcc=gradc/(1(1)*aws*rhcon*cpcon) *****
c*****
dtdct(1)=c3*(tss-tc(1))+c4(1)*(tc(2)-tc(1))+radcc
dtdct(nl)=c4(nlml)*(tc(nlml)-tc(nl))-c5*(tc(nl)-ta)
do 1006 i=2,nlml
1006 dtdct(i)=c4(i)*(tc(i+1)-tc(i))+c4(i-1)*(tc(i-1)-tc(i))
return
end
c
c
c this is the floor concrete subroutine
subroutine concf
implicit real (i,k,l,m)
integer i,iam,ib
dimension cl0(20)
logical flagn,flag2,flag3,flagd,flagst
common // name(340),flag2,flag3,flagc,flagf,flagg,flagh,flagi,flagj,flagk,flagl,flagm,flagn,flago,flagp,flagq,flagr,
common /looper/ i10,i11,i12,i13,i14,i15,i16,i17,i18,i19
common /lith/ akli,asli,asli,cpli,csbli,hb,libp,lil,lilp,lit,
common /steel/ cpsfp,cpsfs,cpswp,cpsws,estlfp,estlwp,kstlfp,
kstlfs,kstlwp,kstlws,rhsfp,rhsfs,rhswp,rhsws
common /misc/ afp,afs,awp,aws,c7,c21,gin,
ha,hinfam,hinsam,hrcpfp,gradc,radc,rczw,
rhoap,rliw,rwpws,sigma,ta,tc(20),tfs,
tfszer,tgp,tgs,tgpzer,tsfp,tsp,tss,
tsszer,thfp,thfs,thwp,thws,zzes,zz5,zzs,zzi,zz7,
rair
common /intgl/ imeth,icount,istore,inoin,ipass,delt,
xic(101),zzz(501)
common /conop/ c8,cpcon,dtdct(20),dtdct(20),gap,kcon,kgap,
l(20),ll(20),nl,nll,gradb,radb,rhcon,
sf1cr,tb(20),tbf(20),tbc(20),tcf(20),
tcic(20),thc,thwc,tsfpi,tspzer,xf1,qlflr,qvflr
if (flagn) n=1
go to (1,2,3)n
1 continue
i15=1
i16=int(.25*nl)
i17=int(.5*nl)
i18=int(.75*nl)
i19=nl
if (flag2) go to 100
afs=asli
cpsfs=cpsfp
kstlfs=kstlfp
rhfs=rhfsfp
thfs=thfp

```



```

tfszer=tsfpi
100 continue
nllm1=nll-1
c***** initialize floor concrete variables *****
data c8,c9,radcb/3*0.0/
c
do 1001 iam=1,20
c10(iam)=0.
1001 dtbdt(iam)=0.
do 1003 i=1,nll
tbic(i)=tfszer
tb(i)=tfszer
1003 ll(i)=thfc*ll(i)
n=2
return
c
2 continue
c ***** calculating thermal diffusivities between nodes *****
bb=ll(1)/(kcon*2.)*gap/kgap+thfs/(kstlfs*2.)
c8=1./(bb*thfs*rhfs*cpsfs)
c9=1./(bb*ll(1)*rhcon*cpcon)
do 1005 i=1,nllm1
c10(i)=2.*kcon/(rhcon*cpcon*ll(i)*(ll(i)+ll(i+1)))
1005 continue
n=3
return
c
3 continue
if (.not. flag2) tfs=tsfp
radcb=gradb/(ll(1)*afs*rhcon*cpcon)
c *****
floor concrete temperature change
dtbdt(1)=c9*(tfs-tb(1))+c10(1)*(tb(2)-tb(1))+radcb
dtbdt(nll)=c10(nllm1)*(tb(nllm1)-tb(nll))
do 1007 ib=2,nllm1
1007 dtbdt(ib)=c10(ib)*(tb(ib+1)-tb(ib))+c10(ib-1)*(tb(ib-1)-tb(ib))
n=2
return
end
c
c
c this is the gas injection subroutine
subroutine injec
implicit real (i,k,l,m)
logical flagn,flagas
common // name(340),flag2,flagas,flagc,flagf,flagn,flagst,flagtr,
common /looper/ i10,i11,i12,i13,i14,i15,i16,i17,i18,i19
common /injob/ dpi,dp2,dp3,mninj,moxinj,time,vp
common /misc/ afp,afs,awp,aws,c7,c21,gin,
ha,hinfam,hinsam,hrcp,gradc,radc,rczw,
rhoap,rliw,rpws,sigma,ta,tc(20),tfs,
tfszer,tgp,tgs,tgpzer,tsp,tss,
tsszer,thfp,thfs,thwp,thws,zzes,zz5,zzs,zz1,zz7,
rair
c
if (flagn) n=1
go to (1,2)n
1 continue
c ***** read in gas injection variables *****
(only if using gas injection option)
read (5,700) tone,ttwo,tthree,dpi,dp2,dp3,fct1,fct2,fct3
700 format (3f10.2,6f8.4)

```



```

.      1(20),l1(20),n1,n11,qradb,radb,rhcon,
.      sf1cr,tb(20),tbf(20),tbic(20),tcf(20),
.      tcic(20),thfc,thwc,tsfpi,tsper,ksfl,qflr,qvflr
.      common /ccop/ cmbro,cracon,dcoz,h2left,qcconc,rcmb,rcmbw,
.      relese,tcigni,tcon,tconf,xmh2oi,zzc,zzd,zzdin
C
      if (flagn) n=1
      go to (1,2,3)n
      1 continue
C**** read in concrete combustion parameters ****
      read (4,700) zzdin,qcconc,cracon,xmh2oi,tcigni,rcmbc
      700 format (6f12.4)
C
      write (10,800) zzdin,qcconc,cracon,xmh2oi,tcigni,rcmbc
      800 format (// concrete combustion input data//ix,30(lh-)//t10,
.      'zzdin =',f12.4,t35,'qcconc =',f12.4,t60,'cracon =',f12.4//
.      t10,'xmh2oi =',f12.4,t35,'tcigni =',f12.4,t60,'rcmbc =',f12.4//)
C
      n=2
      return
      2 continue
      data ccocoz,ccoczp,ccozco,ccocz,release,zzc/6*0.0/
      zzd=zzdin
      tcon=tsfpi
      dcoz=0.01
      xmcocz=1.0
      flagd=.false.
      h2left=xmh2oi
      vconca=afp*11(1)
      n=3
      return
      3 continue
C water release from concrete --- correlation based on drying tests
C of magnitude. see r.d. peak "caceco a containment analysis code-
C users guide"
      relese=0.
      if (tb(1).ge. 658.5 .and. tb(1) .lt. 1960.) water=(1.-exp(26.207
.      +tb(1)*(-0.0721+tb(1)*(6.96e-05-tb(1)*2.26e-08)))/11.7)*xmh2oi
C "water" is the amount that should be left at tb(1) in units of lbs./ft**3
      if (tb(1) .ge. 658.5 .and. (h2left-water) .gt. 0. .and. tb(1)
.      .lt. 1960.) relese=(h2left-water)*vconca/30.
      if (tb(1) .ge. 1960. .and. h2left .gt. 0.) relese=h2left*vconca/30.
C in other words the release rate of water is such that the difference
C between the actual amount and the correct amount ( according to the
C correlation used) is given off in thirty seconds.
C**** calculate thermal diffusivities ****
      xmcocz=dcoz*cracon*rhcon
      cpcoz=2.*cracon*kcon*akli/(kcon*zli+akli*dcoz)/xmcocz
      ccoczp=2.*cracon*kcon*akli/(kcon*zli+akli*dcoz)/lil
      ccocz=2.*cracon*kcon/(dcoz+l1(1))/xmcocz
      ccozco=2.*cracon*kcon/(dcoz+l1(1))/(rhcon*cpccon*11(1)*afp)
C flagd is true when concrete combustion stops
      flagd=.false.
      if (lilp .lt. 0.1 .or. tcon .lt. tcigni) flagd=.true.
      zzd=zzdin
      if (flagd) zzd=0.0
      zzc=cpcoz*(tli-tcon)+ccocz*(tb(1)-tcon)+zzd*cracon*qcconc*rhcon
.      /xmcocz/cpccon+relese*gcw*rcmbw/xmcocz/cpccon
      zzi=zzl+ccoczp*(tcon-tli)
      dtbdt(1)=dtbdt(1)+ccocz*(tcon-tb(1))
      cmbro=relese*rcmba+zzd*cracon*rhcon*rcmbc
      n=3

```

```

return
end

this is the lithium lead combustion subroutine

subroutine lipb
implicit real (i,k,l,m)
logical flagl,flagl,flagdf,flagst,flagc
common /lith/ akli,asli,cpli,csbli,hb,libp,lil,lilp,lit,
. rhi,spill,tli,tlii,zli
. common // name(340),flag2,flagas,flagc,flagf,flagn,flagst,flagtr,
. flagpn,flagw,ipage,iswich,iarosl,flagdf,icz,flagco
common /looper/ i10,i11,i12,i13,i14,i15,i16,i17,i18,i19
common /lead/ cplead,klead,rhlead,mliplib,xalloy,atml,atmpb,cmbr
common /pbpool/ dmpbdt,zzpb,mlead,tlead,xwli,dflipb,xlidot,
. thpb,tleadf,foo
. common /pbdif/ cczp,cgli,clig,cpcz,cpmcz,dfilm,kfilm,pyup,
. gradp,rczp,rgli,rifczp,rifpg,rifpw,rlig,rwli,
. tlead,yapcz,zz6,dflvar

if (flagn) n=1
go to (1,2,3)n
1 continue

foo = 1.0

c***** read in lead parameters *****
c
c read (4,701) cplead,klead,rhlead,alloyi,qdiss,cplipb
c read (4,702) dflvar
c
c write (10,800) cplead,klead,rhlead,alloyi,qdiss,cplipb,dflvar
c
c 701 format (6f12.4)
c 702 format (e12.5)
c 800 format(//,' data for lithium lead combustion option: ',/,1x,40(1h-),
. //t10,'cplead =',f12.4,t35,'klead =',f12.4,t60,'rhlead =',f12.4//
. t10,'alloyi =',f12.4,t35,'qdiss =',f12.4,t60,'cplipb =',f12.4//
. t10,'dflvar =',e12.5//)
c
klead=klead/3600.
atmpb=spill/(6.941*alloyi+(1.-alloyi)*207.2)
atmpb=(1.-alloyi)*atmpb
atml=alloyi*atmpb
mlipbi=spill
spill=atmpb*6.941*alloyi

c
c write (10,801) spill
c 801 format(' modified parameters for lithium in lithium lead pool',/,
. 1x,52(1h-),//t10,' amount of lithium available for combustion =',
. f12.4//t10,' thickness of lipb pool is less than zli above and',//
. t35,' is calculated in program')
c n=2
c return

c
c 2 continue
c***** modifying lithium pool properties to include lead *****
c
c if (flagdf) go to 100
c mliplib=mlipbi-libp

```



```

. tsszer, thfp, thfs, thwp, thws, zzes, zz5, zzs, zzi, zz7,
. rail
. common /panop/ ains, apan, bredth, clist, cpins, cpan, emgp, fpg, fpw,
. kpan, rhins, rhpam, thkini, thkin2, thkpan,
. tins1, tinsif, tinsli, tins2, tins2f, tins2i,
. tpan, tpanf, tpanzo, zz2, zz4, zz8, zz9
. common /units/ aehcp, beta, chp, cambrh, cpap, cpehcp, map, mnip,
. mop, wap, papzer, qcn, qco, qcol, qco2, qcw, qvap,
. tcz, tczf, tczi, tehcp, tehcpf, tehczp, tgpf,
. tlif, tmelt, tsfpf, tspf, tvap, xmehcp
. common /intgl/ imeth, icount, istore, inoin, ipass, delt,
. xic(101), zzz(501)
. common /pbdif/ cczp, cgli, cliq, cpcz, cpmcz, dfilm, kfilm, pyup,
. gradp, rczp, rgli, rificzp, rifpg, rifpw, rlig, rqli,
. tlead, yapcz, zz6, dflvar
. common /steam/ tgps, vg, xg, sat(35, 10), sh(7, 110, 5), uvv, hvv, cpwv, vvg,
. ph2o, ulp, tip, vip, hlp, vvb, hfg, ph2ob, cpvb, hu(15, 2),
. phase, hum, cpa, mw1, mwv, ul, uv, ulz, uvz, mw1z,
+ mwvz, uvzer, ulzer, mvv, mwlv, vl, zzep, mvvzer, mw1zer,
. xmolp, cell

c   if (flagn) n=1
   go to (1,2,3)n
   1 continue
   tlead=tlii
   zzpb=0.
   n=2
   return

c   2 continue
   thpb=mlead/rhlead/asli
   if (thpb .lt. 1.0e-16) thpb=1.0e-16
   dflipb=dflvar*exp(-1224./tlii)!this is the diffusion coefficient (6.5E-08)
   xlidot=dflipb*rhli*xvli/thpb
   dmpbdt=(1.-xalloy)/xalloy*cmbrr*asli*207.2/6.941
   n=3
   return

c   3 continue

c   zli1=.667*zli
   zli2=.333*zli
   klipb1=(mlead*klead+.333*li1*akli)/(mlead+.223*li1)
   cplpb1=(mlead*cplead+.333*li1*cpli)
   thpb1=zli2+thpb

c ***** modify pool, combustion zone and primary cell temp rates of change
100 continue
   if (icx .eq. 0) go to 110
   zzi=zzi-cczp*(tcz-tli)-rczp+qvap*cmbrr*asli*cczp/yapcz+rqli+rgli
   if(flagst)uvz=uvz-gradz
   if(.not.flagst)zz4=zz4-rliq
   zz5=zz5-rliw
   zz6=zz6+cpcz*(tcz-tli)+gradp/cpmcz

c   cclipb=2.*asli*klipb1*akli/
   (.667*li1*cpli*(zli1*klipb1+thpb1*akli))
   ccpb1=2.*klipb1*akli*asli/(cplpb1*(zli1*klipb1+thpb1*akli))
   yapcz=kfilm*klipb1*asli/(dfilm*klipb1+kfilm*thpb1/2.)
   cpcz=yapcz/cpmcz
   cczp=yapcz/cplpb1
   gradp=sigma*asli*(tcz**4-tlead**4)*rificzp
   rczp=gradp/cplpb1

```

```

C
grady=sigma*asli*(tlead**4-tsp**4)*rifpw
gradz=sigma*asli*(tlead**4-tgp**4)*rifpw
rliw=qrady/(thwp*awp*rhswp*cpswp)
rqli=qradz/cplpb1
rliw=qradw/(thwp*awp*rhswp*cpswp)
rqli=qradw/cplpb1

zpb=cczp*(tcz-tlead)+rczp-qvap*cubr*asli/cplpb1
      -rqli-rqli-ccpbli*(tlead-tli)
zsl=zz1+cclipb*(tlead-tli)
if(flagst)uvz=uvz+qradz
if(.not.flagst)zz4=zz4+rliw
zz5=zz5+rliw
zz6=zz6-qradp/cpmcz-cpcz*(tcz-tlead)
go to 120
110 continue
C**** modify temps without combustion zone modeling ****
zsl=zz1-cgli*(tgp-tli)+rqli+rqli
if(flagst)uvz=uvz-yalig*(tli-tgp)-qradz
if(.not.flagst)zz4=zz4-clig*(tli-tgp)-rliw
zz5=zz5-rliw

yalig=klipb1*hb*asli/(klipb1+hb*thpb1/2.)
clig=yalig/htcpgp
qradw=sigma*asli*(tlead**4-tsp**4)*rifpw
qradg=sigma*asli*(tlead**4-tgp**4)*rifpw
rliw=qradw/(thwp*awp*rhswp*cpswp)
rqli=qradw/cplpb1
rqli=qradg/cplpb1
rliw=qradg/htcpgp
cgli=yalig/cplpb1
cclipb=2.*asli*klipb1*akli/
      (.667*li1*cpli*(zli1*klipb1+thpb1*akli))
ccpbli=2.*klipb1*asli*akli/(cplpb1*(zli1*klipb1+thpb1*akli))

zpb=cgli*(tgp-tlead)-rqli-rqli-ccpbli*(tlead-tli)
zsl=zz1+cclipb*(tlead-tli)
if(flagst)uvz=uvz+yalig*(tlead-tgp)+qradg
if(.not.flagst)zz4=zz4+clig*(tlead-tgp)+rliw
zz5=zz5+rliw
zz6=(tli-tcz)/delt
120 continue
alphap=((thpb1+zli1)/(zli1+akli+thpb1/klipb1))/
      ((rqli*cpli*zli1)+(cplpb1/asli))/(thpb1+zli1)
pyup=0.075*(thpb1+zli1)**2/alphap
n=2
return
end

C
C this is the subroutine which sets CO2 only atmosphere option.
C
subroutine co2 (icmb,icni,ico2i,n)
icmb=0
icni=0
ico2i=1
if (n.eq. 1) write (10,100)
100 format(' CO2 atmosphere option is selected',/ ,ix,33(1h_)/)
return
end

C
C this is the subroutine for the steam in containment option
C

```

```

subroutine steam
implicit real (i,k,l,m)
integer p,tlo,thi
logical flagn,lts(2),fr
dimension ts(2)
real nulv
common // name(340),flag2,flag3,flagc,flagf,flagg,flagh,flagi,flagj,flagk,flagl,flagm,flagn,flago,flagp,flagq,flagr,flagv,flagw,flagx,flagy,flagz,flagaa,flagab,flagac,flagad,flagae,flagaf,flagag,flagah,flagai,flagaj,flagak,flagal,flagam,flagan,flagao,flagap,flagaq,flagar,flagav,flagaw,flagax,flagay,flagaz,flagaa,flagab,flagac,flagad,flagae,flagaf,flagag,flagah,flagai,flagaj,flagak,flagal,flagam,flagan,flagao,flagap,flagaq,flagar,flagav,flagaw,flagax,flagay,flagaz
common /steam/ tgs,vg,xg,sat(35,10),sh(7,110,5),uvw,hvw,cpvw,vvg,ph2o,uiP,tip,vlp,hlp,vvb,hfg,ph2ob,cpvb,hu(15,2),phase,hum,cpa,mw,mwv,ul,uv,ulz,uvz,mwlz,mvz,uvzer,uzer,mvv,mwlv,vi,zzep,mvzzer,mwlzer,xmolp,cell
common /lith/ akli,asli,cpli,cbli,hb,libp,lil,lilp,lit,rhli,spil,tlil,tlil,zli
common /steel/ cpsfp,cpsfs,cpswp,cpsws,estlf,estlp,estlw,kstlfp,kstlfs,kstlwp,kstlws,rhsfp,rhsfs,thswp,thsws
common /units/ aehcp,beta,chp,cmbrh,cpap,cpehpc,mpap,mnip,mco2p,moxp,mwap,papzer,qcn,qco,qcol,qco2,qcw,qvap,qcc,ql2c2,tcz,tcf,tcki,tehcp,tehcpf,tehczp,tgpf,tlif,tmelt,tsfpf,tsfp,tvap,xmehcp
common /misc/ afp,afs,awp,aws,c7,c21,gin,ha,hinfam,hinsam,hrcp9p,gradc,radc,rczw,rhoap,rliw,rpws,sigma,ta,tc(20),tfs,tfszer,tgp,tgs,tgpzer,tsfp,tsp,tss,tsszer,thfp,thfs,thwp,thws,zz5,zzs,zz1,zz7,rair
common /injop/ dpi,dp2,dp3,mninj,moxinj,time,vp
common /secop/ aehcs,c11,c20,chs,cpehcs,cph2,cplih,cpwa,crack,foutp,fouts,foutt,hinfgs,hinfgs,hinfgs,hings,hings,kleak,leak,mairp,mairs,mais,mah2s,mlihs,mlinis,mmins,mlois,mlios,mnis,mnis,moxis,moxs,mwals,m1c3s,m1c2s,mcs,mco2s,rholc3,rholc2,rhocar,mwas,pap,pas,paszer,ra,rbreak,rholih,rholin,rholio,rwpqas,tehcs,tehcsf,tehczs,tgsf,tgsf,tgszer,tssf,vs,xmdot,xmehcs,xmola,zz3,zzfs
common /conop/ c8,cpccon,dtdt(20),dtdct(20),gap,kcon,kgap,1(20),11(20),nl,nl1,qraddb,radb,rhcon,tf1cr,tb(20),tbf(20),tbic(20),tcf(20),tcic(20),thfc,thwc,tsfpi,tspzer,xsfl,qlflr,qvflr
common /panop/ ains,apan,bredth,clist,cpins,cppan,emgp,fpf,fpw,kpan,rhins,rhpan,thkin1,thkin2,thkpan,tins1,tinslf,tinsli,tins2,tins2f,tins2i,tpan,tpanf,tpanzo,zz2,zz4,zz8,zz9
common /stapn/ tsat,hsat,huch
common /intgl/ imeth,icount,istore,inoin,ipass,delt,xic(101),zzz(501)
common /heat/ hingssp,hinecp
C
if (flag)ns=1
go to (1,2,3,4,5)ns
1 continue
C***** initialize the amount of water vapor in containment ***
C
tlo=int(tgpzer/20.)-24.
thi=tlo+1.
intdis= (tgpzer/20.)-int(tgpzer/20.)
psat= (sat(thi,2)-sat(tlo,2))*intdis+sat(tlo,2)
ph2o= psat*hum
vvg= (sat(thi,4)-sat(tlo,4))*intdis+sat(tlo,4)
mwv= vp*hum/vvg

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```

mvzzer=mvv
mvvv=mvv
mwizer=mvv
vg=1.0e20
if(hum.gt.0.0)vg= vvg/hum
tgps=tgpzer
cell=1.
call proptv
ns=2
return
2 continue
C *****
C
C determine the initial energy of the vapor region
mairp=mnip+mxp+map+mco2p
cpn2p=(0.172+8.57e-06*tgp+1.02e-09*tgp*tgp)
cpo2p=(0.184+3.2e-06*tgp-1.36e04/tgp/tgp)
cpc02p=0.29
ua=(mnip*cpn2p+mxp*cpo2p+map*cpap+mco2p*cpc02p)*tgp
uv=ua+uvv*mvv
uvzer=uv
ulzer=ul
ns=3
return
3 continue
C *****
C ***** calculate the emissivity of the air-vapor mixture ***
C
if((ph2o/14.7*chp/4.)<.le. 0.5)then
ewl= 0.37*(ph2o/14.7*chp/4.)**0.67
else
ewl= 0.28+0.11*log(ph2o/14.7*chp/4.)
endif
estair= 0.0476*(ph2o+pap)*ewl
if(estair.gt.(1.4*ewl))estair= 1.4*ewl
emgp=emgp+estair
if(emgp.gt.1.0)emgp=1.0
if (emgp .le. 0.005) emgp=0.005
C ***** determining primary air-vapor mixture temperature ***
htcair=mairp*cpa
if(mvv.le.0.)go to 70
lts(1)=.false.
lts(2)=.false.
fr=.true.
ts(1)=491.0
ts(2)=1940.0
if(tgp.lt.ts(1))tgp=ts(1)
vg=(vp-vl)/mvv
tgps=tgp
cell=1.
call proptv
temp=uv-htcair*tgp-mvv*uvv
j=2
if((temp.gt.0.)j)=1
ts(j)=tgp
lts(j)=.true.
if(fr) go to 57
if(abs(temp/uv).le.0.0005)go to 56
if(.not.(lts(1).and.lts(2)))go to 58
if(abs(ts(1)-ts(2)).le.0.005)go to 56
51
52
55

```

```

58 temp3= temp2-temp
   if(temp3.eq.0.)go to 1902
   temp4= deltat/temp3
   if(temp4.le.0.)go to 1902
   deltat=temp*temp4
61 j=j+1
   if(j.eq.3)j=1
   temp3=ts(j)-tgp
   if(abs(deltat).le.abs(temp3))go to 60
   if(lts(j))go to 59
   deltat=temp3
   tgp=ts(j)
   go to 64
59 deltat=0.9*temp3
60 tgp=tgp+deltat
64 temp2=temp
   go to 51
57 fr=.false.
   deltat=sign(0.5,temp)
   go to 61
56 if(phase.eq.2.)xg=1.0
   mvv=xg*mvv
   mwlv=mvv-mvv
   pap=ph2o+mairp*rair*tgp/(vp-vl)/144.
   go to 1903
1902 deltat=0.5*(ts(1)+ts(2))-tgp
   go to 60
70 ph2o=0.0
   mvv=0.0
   mwlv=0.0
   tgp=uv/htcpgp
   pap=mairp*rair*tgp/vp/144.
1903 continue
   ns=4
   return
4 continue
c *****
c ***** check for boiling or condensation if water is present *****
   if(mwlv.gt.1.0e-02)then
     ulp=ul/mwlv
     cell=1.
     call proptu
     do 1480 n=1,34
       p=n+1.
       if(pap.lt.sat(p,2))then
         intdsp=(pap-sat(n,2))/(sat(p,2)-sat(n,2))
         ulpb=(sat(p,5)-sat(n,5))*intdsp+sat(n,5)
         ugpbb=(sat(p,6)-sat(n,6))*intdsp+sat(n,6)
         go to 444
       endif
1480 continue
444 continue
     if(ulp.gt.ulpb)then
       boil=1.
       mboil=(ul-mwlv*ulpb)/(ugpbb-ulpb)
       uvz=uvz+ugpbb*mboil/delt
       mwlvz=mwlvz+mboil/delt
       mvvz=mvvz+mboil/delt
       ulz=ulz-ugpbb*mboil/delt

```

```

endif
vl=mvl*vlp

c without boiling, check for evaporation and condensation
c q"=hb(tgp-tilp)+[kb.18(hfg+hf)(mfvg-mfvb)]/xam
c is the expression for heat transferred during evaporation
c
if(boil.eq.0.)then
mfvg=mvv/(vp-vl)/18./((mvv/(vp-vl)/18.+mairp/(vp-vl)/xmolph)
if(mfvg.eq.1.0)mfvb=0.9999999
mfaq=1.-mfvg
c at the liquid-vapor boundary:
mfvb=1./vvb/18./((1./vvb/18.+(pap-ph2ob)*144./rair/tilp/xmolph)
if(mfvb.eq.1.0)mfvb=0.9999999
mfab=1.-mfvb
mflag=mfab/mfaq
xam=(mfab-mfaq)/alog(mflag)
c determine h from the product GrPr
c find steam and air properties at the boundary and in the bulk vapor
do 1470 n=1,2
temp=abs(tilp/1.8)
if(n.eq.1)temp=abs(tgp/1.8)
kair=.02665+6.013e-05*(temp-310.93)
kair=kair/1.731/3600
muair=1.912e-05+4.152e-08*(temp-310.93)
muair=muair/1.488
vvt=vvb
if(n.eq.1)vvt=vvg
kh2o=17.6+5.87e-02*(temp-273.)+1.04e-04*(temp-273.)**2
-4.51e-08*(temp-273.)**3+(103.51+4198*(temp-273.)-2.771e-05*
(temp-273.)**2)*16.02/vvt*.001+2.148e08/(temp-273.)**4.2/
(vvt/16.02)**2
kh2o=kh2o*.001/1.729/3600.
muv=11.4/(temp**2-884*temp+1.36e06)
muv=muv/1.488
if(n.eq.2)then
kairb=kair
muairb=muair
kh2ob=kh2o
muvb=muv
else
kairg=kair
muairg=muair
kh2og=kh2o
muvg=muv
endif
1470 continue
temp2=(muairb/muvb)**.5
phiawb=.218942*(1.+88808*temp2)**2
phiwab=.277605*(1.+1.2603/temp2)**2
vab=1.0e20
if(pap.gt.ph2ob)vab=1./rhoap
vsb=vvb*ph2ob/pap
mub=vsb*muairb/(vsb+vab*phiawb)+vab*muvb/(vab+vsb*phiwab)
betab=1./tilp
rhob=1./vab+1./vsb
cpb=(vsb*cpa+vab*cpvb)/(vab+vsb)
kbndry=vsb*kairb/(vsb+vab*phiawb)+vab*kh2ob/(vab+vsb*phiwa)
asurf=(afp-asli)
c calculate the heat transfer from GrPr
grpr=betab*rhob*cpb*32.2*abs(tgp-tilp)/kbndry*asurf**1.5/mub
dab=1.742e-09*tgp**2.334/pap

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```

if(tgp.lt.tlp)then
  if(grpr.lt.2.e07)then
    ca=.54
    aa=.25
  else
    ca=.14
    aa=.3333
  endif
elseif(tgp.gt.tlp)then
  ca=.27
  aa=.25
elseif((vzb.eq.(vp-vl)/mwv).and.(tgp.eq.tlp))then
  go to 1999
else
  ca=0.
  aa=1.0
endif
c calculate the sensible heat transfer coefficient
hsens=ca*kbndry/asurf**.5*grpr**aa
mgb=18.*mfvb+xmolv*mfab
prsc=cpb*rhob*dab/kbndry
kb=hsens/cpb/mgb*(prsc)**.666
c without a temperature difference, the mass transfer coefficient must be
c calculated differently than with one
if(tgp.eq.tlp) kb=1.02*pap*dab/(asurf**.5*1545.*tlp)*
. (asurf**.15*32.2*abs(mwv/(vp-vl)-1./vzb)/mub/dab)**.373
c
a=kb*mgb*cpb*(mfvg-mfvb)/hsens/xam
c mass condensation/evaporation rate
condr=kb*18.*(mfvg-mfvb)/xam*asurf
if(condr.lt.(-1.*mwl/delt))condr=-1.*mwl/delt
c account for greater heat transfer with large mass transfer rates
hprime=(a/(exp(a)-1.))*hsens
c heat transfer rate
hcond=hprime*(tgp-tlp)+condt/asurf*(hlp+hfg)
c transfer heat and mass to and from liquid and vapor regions
mwvz=mwvz-condr
mwlz=mwvz+condr
uvz=uvz-hcond*asurf
ulz=ulz+hcond*asurf
endif
1999 continue
endif
c***** calculating gas heat transfer coefficients *****
c
c determine the effects of steam on the heat transfer coefficients
c find the saturation temperature and the Uchida heat transfer coeff.
if(mwv.gt.0.0)then
  do 1460 n=1,34
    p=n+1.
    if(ph2o.lt.sat(p,2))then
      intdsp=(ph2o-sat(n,2))/(sat(p,2)-sat(n,2))
      tsat=intdsp*(sat(p,1)-sat(n,1))+sat(n,1)+460.
      hsat=intdsp*(sat(p,7)-sat(n,7))+sat(n,7)
      go to 1111
    endif
  1460 continue
  1111 continue
  nr=mairp/mwv
  do 1450 n=1,14
    p=n+1

```

```

if (mr.gt.hu(p,1)) then
intdsh=(mr-hu(p,1))/(hu(n,1)-hu(p,1))
huch= hu(p,2)-intdsh*(hu(p,2)-hu(n,2))
go to 2222
endif
1450 continue
2222 continue
if (mr.ge.50.) huch=2.
if (mr.le.0.1) huch=280.
huch=huch/3600.
endif
ns=5
return
5 continue
c ***calculate heat transfer coefficients with steam present***
if (mwv.gt.0.0) then
rhoqp=rhoap+1./vg
c
c gas to wall
qu=2.*(tsat-tsp)*awp/(thwp/kstlwp+2./huch)
if (tsp.gt.tsat) then
hgwp=hingsp*akexx(tgp,tsp,rhogp)
qu=2.*(tgp-tsp)*awp/(thwp/kstlwp+2./hgwp)
endif
mcondw=qu/hfg
if (tsp.gt.tsat .or. qu.le.0.0) mcondw=0.
mwvz=mwvz-mcondw
mwlz=mwvz+mcondw
uvz=uvz-qu
ulz=mcondw*hsat+ulz
zz5=zz5+qu/rhswp/awp/thwp/cpswp
c
c gas to extraneous heat capacity
qvehc=huch*(tsat-tehcp)*aehcp
if (tehcp.gt.tsat) then
hehcp=hinecp*akexx(tgp,tehcp,rhogp)
qvehc=(tgp-tehcp)*hehcp*aehcp
endif
mconde=qvehc/hfg
if (tehcp.gt.tsat .or. qvehc.le.0.0) mconde=0.
mwvz=mwvz-mconde
mwlz=mwvz+mconde
uvz=uvz-qvehc
ulz=ulz+mconde*hsat
zzep=zzep+qvehc/xmehcp/cpehcp
c
c
ns=3
return
end
c *****
c this is the subroutine for the steam in the secondary cell option
c
subroutine steam2
implicit real (i,k,l,m)
integer p,tavhi,tavlo,tfhi,tflo,thi,tlo
logical flagn,lts(2),fr,flagtr
dimension ts(2)

```

```

real nulv
common // name(340), flag2, flag3, flagc, flagf, flagn, flagst, flagtr,
.   flagpn, flagw, ipage, iswich, iarosl, flagdf, icz, flagco
common /steam/  tgps, vg, xg, sat(35,10), sh(7,110,5), uwv, hww, cpwv, vvg,
.   ph2o, ulp, tlp, vlp, hlp, vvb, hfg, ph2ob, cpvb, hu(15,2),
.   phase, hum, cpa, awl, mwv, ul, uv, uvz, mwiz,
+   mwvz, uvzer, ulzer, mwv, mwlv, vl, zzep, mwvzer, mwlzer,
.   xmolp, cell
common /steel/  cpsfp, cpsfs, cpsvp, cpsws, estlfp, estlwp, kstlfp,
.   kstlfs, kstlwp, kstlws, rhsfp, rhsfs, rhswp, rhsws
common /misc/  afp, afs, awp, aws, c7, c21, gin,
.   ha, hinfam, hinsam, htcpgp, gradc, radc, rczw,
.   rhoap, rliw, rwpws, sigma, ta, tc(20), tfs,
.   tfszer, tgp, tgs, tgpzer, tsfp, tsp, tss,
.   tsszer, thfp, thfs, thwp, thws, zzes, zz5, zzs, zzi, zz7,
.   rair
common /secop/ aehcs, cil, c20, chs, cpehcs, cph2, cplih, cpwa, crack,
.   foutp, fouts, fouth, hinfgs, hinfsg, hinfss, hinps, kleaf,
.   leak, maifp, mairs, mais, mas, mh2s, mlihs, mlinis, mlins,
.   mliois, mlios, mniis, mnis, moxis, moxs, mwais,
.   mlc3s, mlc2s, mcs, mco2s, rhoclc3, rhoclc2, rhocar,
.   mwas, pap, pas, paszer, ra, rbreak, rholi,
.   rholin, rholio, rvpgas, tehcs, tehcsf, tehczs, tgsf,
.   tfsf, tgszer, tssf, vs, xmdot, xmehcs, xmola, zz3, zzfs
common /steam2/ cpa2, cpvb2, emgs, hfg2, hlp2, htcpgs, hum2, mw12,
.   mwlv2, mwlvz2, mwlvzr2, mwv2, mwvz2, mwvzr2,
.   phase2, ph2o2, ph2ob2, rair2, tlp2, ul2, ulp2, ulz2,
.   ulzer2, uv2, uvz2, uvzer2, uvv2, vg2, vl2, vlp2, vvb2,
.   vvg2, xg2, xmols, stmin2, stout2, xinj2, rhoas
common /intgl/ imeth, icount, istore, inoin, ipass, delt,
.   xic(101), zzz(501)
common /heat2/ hinecs
common /torus/  amag, ash1, clehcs, cpmag, cpshi, eehcs, eshl,
.   hinmag, hinsh1, kehcs, khe, ksh1, the, thsh1, tmag, tmagf,
.   tmagz, tsh1, tshlf, tshlz, zzshi, zzmag
common /face/  tblio, tshio, tshoo, zzbli, zzshi, zzsho, tbli, tshi, tsho,
.   tmano, tman, xmsho, xmmag, zzman

C   if (flagn)ns=1
go to (1,2,3,4,5)ns
1 continue

C ***** initialize the amount of water vapor in the secondary cell ***
C
tlo=int(tgszer/20.)-24.
thi=tlo+1.
intdis= (tgszer/20.)-int(tgszer/20.)
psat2= (sat(thi,2)-sat(tlo,2))*intdis+sat(tlo,2)
ph2o2= psat2*hum2
vvg2= (sat(thi,4)-sat(tlo,4))*intdis+sat(tlo,4)
mwv2= vs*hum2/vvg2
mwvzr2=mwv2
mwv2= mwv2
mwlvzr2=mwlv2
vvg2=1.0e20
if(hum2.gt.0.0)vvg2= vvg2/hum2
tgps=tgszer
cell=2.
call proptv
ns=2
return
2 continue

```

```

C *** determine the initial energy of the secondary cell vapor region ***
C
mairs=mnis+moxs+mas+mco2s
cpn2s=(0.172+8.57e-06*tgs+1.02e-09*tgs*tgs)
cpo2s=(0.184+3.2e-06*tgs-1.36e04/tgs/tgs)
cpcO2s=0.29
ua=(mnis*cpn2s+moxs*cpo2s+mas*cpas+mco2s*cpcO2s)*tgs
uv2=ua+uwv2*mwv2
uvzer2=uv2
ulzer2=ul2
ns=3
return
3 continue

C ***** calculate the emissivity of the air-vapor mixture ***
C
if((ph2o2/14.7*chs/4.).le.0.5)then
ew1=0.37*(ph2o2/14.7*chs/4.)*0.67
else
ew1=0.28+0.11*log(ph2o2/14.7*chs/4.)
endif
estair=0.0476*(ph2o2+pas)*ew1
if(estair.gt.(1.4*ew1))estair=1.4*ew1
emgs=emgs+estair
if(emgs.gt.1.0)emgs=1.0
if(emgs.le.0.005)emgs=0.005

C ***** determining secondary air-vapor mixture temperature ***
C
htcar2=mairs*cpa2
if(mwv2.le.0.)go to 70
lts(1)=.false.
lts(2)=.false.
fr=.true.
ts(1)=491.0
ts(2)=1940.0
if(tgs.lt.ts(1))tgs=ts(1)
vg2=(vs-vl2)/mwv2
tgps=tgs
cell=2.
call proptv
temp=uv2-htcar2*tgs-mwv2*uvv2
j=2
if(temp.gt.0.)j=1
ts(j)=tgs
lts(j)=.true.
if(fr)go to 57
if(abs(temp/uv2).le.0.0005)go to 56
if(.not.(lts(1).and.lts(2)))go to 58
if(abs(ts(1)-ts(2)).le.0.005)go to 56
temp3=temp2-temp
if(temp3.eq.0.)go to 1902
temp4=delat/temp3
if(temp4.le.0.)go to 1902
delat=temp*temp4
j=j+1
if(j.eq.3)j=1
temp3=ts(j)-tgs
if(abs(delat).le.abs(temp3))go to 60
if(lts(j))go to 59
delat=temp3
tgs=ts(j)

```

```

59 go to 64
60 deltat=0.9*temp3
61 tgs=tgs+deltat
62 temp2=temp
63 go to 51
64 fr=.false.
65 deltat=sign(0.5,temp)
66 go to 61
67 if(phase2.eq.2.)xg2=1.0
68 mvv2=xg2*mvv2
69 mvlv2=mvv2-mvvv2
70 pas=ph2o2+mairs*rair2*tgs/(vs-vl2)/144.
71 go to 1903
1902 deltat=0.5*(ts(1)+ts(2))-tgs
72 go to 60
73 ph2o2=0.0
74 mvv2=0.0
75 mvv2=0.0
76 mvlv2=0.0
77 tgs=uv2/htcpgs
78 pas=mairs*rair2*tgs/vs/144.
1903 continue
79 ns=4
80 return
81 4 continue
82 c *****
83 c ***** check for boiling or condensation if water is present *****
84 if(mvl2.gt.1.0e-02)then
85   ulp2=ul2/mvl2
86   cell=2.
87   call proptu
88   do 1440 n=1,34
89     p=n+1.
90     if(pas.lt.sat(p,2))then
91       intdsp=(pas-sat(n,2))/(sat(p,2)-sat(n,2))
92       ulpb=(sat(p,5)-sat(n,5))*intdsp+sat(n,5)
93       ugpb=(sat(p,6)-sat(n,6))*intdsp+sat(n,6)
94       go to 444
95     endif
96     continue
97     1440 continue
98     444 continue
99     boil=0.
100    if(ulp2.gt.ulpb)then
101      boil=1.
102      mboil=(ul2-mvl2*ulpb)/(ugpb-ulpb)
103      if(mboil.gt.mvl2)mboil=mvl2
104      uvz2=uvz2+ugpb*mboil/delt
105      mvlz2=mvlz2-mboil/delt
106      mvvz2=mvvz2+mboil/delt
107      ulz2=ulz2-ugpb*mboil/delt
108    endif
109    vl2=mvl2*vlp2
110  c without boiling, check for evaporation and condensation
111  c q=hb(tgs-tlp2)+[kb.18(hfg2+hkf2)(mfvg-mfvb)]/xam
112  c is the expression for heat transferred during evaporation c
113  if(boil.eq.0.)then
114    mfvg=mvv2/(vs-vl2)/18./((mvv2/(vs-vl2)/18.+mairs/(vs-vl2))/xmols)
115    if(mfvg.eq.1.0)mfvg=0.9999999
116    mfvb=1.-mfvg
117  c at the liquid-vapor boundary:

```



```

mfvb=1./vzb2/18./(1./vzb2/18.+(pas-ph2ob2)*144./rair2/tlp2/xmols)
if(mfvb.eq.1.0)mfvb=0.9999999
mfab=1.-mfvb
mflog=mfab/mfag
if(mflog.eq.1.0)xam=1.0
if(mflog.eq.1.0)go to 99
xam=(mfab-mfag)/alog(mflog)
99 continue
c determine h from the product GrPr
c find steam and air properties at the boundary and in the bulk vapor
do 1430 n=1,2
temp=abs(tlp2/1.8)
if(n.eq.1)temp=abs(tgs/1.8)
kair=.02665+6.013e-05*(temp-310.93)
kair=kair/1.731/3600
muair=1.912e-05+4.152e-08*(temp-310.93)
muair=muair/1.488
vvt=vvb2
if(n.eq.1)vvt=vvg2
kh2o=17.6+5.87e-02*(temp-273.)+1.04e-04*(temp-273.)**2
-4.51e-08*(temp-273.)**3+(103.51+4198*(temp-273.)-2.771e-05*
(temp-273.)**2)*16.02/vvt*.001+2.148e08/(temp-273.)**4.2/
(vvt/16.02)**2
kh2o=kh2o*.001/1.729/3600.
muv=11.4/(temp**2-884*temp+1.36e06)
muv=muv/1.488
if(n.eq.2)then
kair=kair
muairb=muair
kh2ob=kh2o
muvb=muv
else
kairg=kair
muairg=muair
kh2og=kh2o
muvg=muv
endif
1430 continue
temp2=(muairb/muvb)**.5
phiawb=.218942*(1.+88808*temp2)**2
phiwab=.277605*(1.+1.2603/temp2)**2
vab=1.0e20
if(pas.gt.ph2ob2)vab=1./rhoas
vsb=vvb2*ph2ob2/pas
mub=vsb*muairb/(vsb+vab*phiawb)+vab*muvb/(vab+vsb*phiwab)
betab=1./tlp2
rhob=1./vab+1./vsb
cpb=(vsb*cpa2+vab*cpvb2)/(vab+vsb)
kbndry=vsb*kairb/(vsb+vab*phiaw)+vab*kh2ob/(vab+vsb*phiwa)
asurf=afs
c calculate the heat transfer from GrPr
grpr=betab*rhob*cpb*32.2*abs(tgs-tlp2)/kbndry*asurf**1.5/mub
dab=1.742e-09*tgs**2.334/pas
if(tgs.gt.tlp2)then
if(grpr.lt.2.e07)then
ca=.54
aa=.25
else
ca=.14
aa=.3333
endif
elseif(tgs.lt.tlp2)then

```

```

ca=.27
aa=.25
elseif((vvb2.eq.(vs-vl2)/mwv2).and.(tgs.eq.tlp2))then
go to 1999
else
ca=0.
aa=1.0
endif
c calculate the sensible heat transfer coefficient
hsens=ca*kbndry/asurf**.5*grpr**aa
mgb=18.*mfvb+xmols*mfab
prsc=cpb*rhob*dab/kbndry
kb=hsens/cpb/mgb*(prsc)**.666
c without a temperature difference, the mass transfer coefficient must be
c calculated differently than with one
if(tgs.eq.tlp2) kb=1.02*pas*dab/(asurf**.5*1545.*tlp2)*
(asurf**.15*32.2*abs(mwv2/(vs-vl2)-1./vvb2)/mub/dab)**.373
c
a=kb*mgb*cpb*(mfvg-mfwb)/hsens/xam
c mass condensation/evaporation rate
condr=kb*18.*(mfvg-mfwb)/xam*asurf
if(condr.lt.(-1.*mw12/delt))condr=-1.*mw12/delt
c account for greater heat transfer with large mass transfer rates
hprime=(a)/(exp(a)-1.))*hsens
c heat transfer rate
hcond=hprime*(tgs-tlp2)+condr/asurf*(hlp2+hfg2)
c transfer heat and mass to and from liquid and vapor regions
mwv2=mwv2-condr
mw12=mw12+condr
uvz2=uvz2-hcond*asurf
ulz2=ulz2+hcond*asurf
endif
1999 continue
endif
c***** calculating gas heat transfer coefficients *****
c
c determine the effects of steam on the heat transfer coefficients
c find the saturation temperature and the Uchida heat transfer coeff.
if(mwv2.gt.0.0)then
do 1420 n=1,34
p=n+1.
if(ph2o2.lt.sat(p,2))then
intdsp=(ph2o2-sat(n,2))/(sat(p,2)-sat(n,2))
tsat=intdsp*(sat(p,1)-sat(n,1))+sat(n,1)+460.
hsat=intdsp*(sat(p,7)-sat(n,7))+sat(n,7)
go to 1111
endif
1420 continue
1111 continue
mr=mairs/mwv2
do 1410 n=1,14
p=n+1
if(mr.gt.hu(p,1))then
intdsh=(mr-hu(p,1))/(hu(n,1)-hu(p,1))
huch=hu(p,2)-intdsh*(hu(p,2)-hu(n,2))
go to 2222
endif
1410 continue
2222 continue
if(mr.le.0.1)huch=280.

```

```

huch=huch/3600.
endif
ns=5
return
5 continue
c **calculate heat transfer coefficients with steam present***
c
  if (mwv2.gt.0.0)then
    rhogs=rhoap+1./vg2
  secondary gas to secondary wall
  qvsec=2.*(tsat-tss)*aws/(thws/kstlws+2./huch)
  if (tss.gt.tsat)then
    hsec=hingss*akexx(tgs,tss,rhogs)
    qvsec=2.*(tgs-tss)/(thws/kstlws+2./hsec)
  endif
  mcondw=qvsec/hfg2
  if (tss.gt.tsat .or. qvsec.le.0.0)mcondw=0.
  mwvz2=mwvz2-mcondw
  mw1z2=mw1z2+mcondw
  uvz2=uvz2-qvsec
  ulz2=mcondw*hsat+ulz2
  zzs=zzs+qvsec/rhws/aws/thws/cpsws
c
c secondary gas to primary wall (or shield outer face)
  if (.not.flagtr)then
    qvpgs=2.*(tsat-tsp)*awp/(thwp/kstlwp+2./huch)
    if (tsp.gt.tsat)then
      hwpgas=hinpss*akexx(tsp,tgs,rhogs)
      qvpgs=2.*(tgs-tsp)*awp/(thwp/kstlwp+2./hwpgas)
    endif
  else
    qvpgs=2.*(tsat-tsho)*ashl/(thsho/kshl+2./huch)
    if (tsho.gt.tsat)then
      hshl=hinshl*akexx(tsho,tgs,rhogs)
      qvpgs=2.*(tgs-tsho)*ashl/(thsho/kshl+2./hshl)
    endif
  endif
  mconwp=qvpgs/hfg2
  if (tsp.gt.tsat .and. .not.flagtr).or.
    (tsho.gt.tsat .and. flagtr) .or. qvpgs.le.0.0)mconwp=0.
  mwvz2=mwvz2-mconwp
  mw1z2=mw1z2+mconwp
  uvz2=uvz2-qvpgs
  ulz2=mconwp*hsat+ulz2
  if (.not.flagtr)zz5=zz5+qvpgs/rhswp/awp/thwp/cpswp
  if (flagtr)zzsho=zzsho+qvpgs/xmsho/cpshl
c
c secondary gas to primary floor
  if (.not.flagtr)then
    qvfpgs=2.*(tsat-tsfp)*afp/(thfp/kstlfp+1./huch)
    if (tsfp.gt.tsat)then
      hfpgas=hinfps*akexx(tsfp,tgs,rhogs)
      qvfpgs=2.*(tgs-tsfp)*afp/(thfp/kstlfp+2./hfpgas)
    endif
  mconfp=qvfpgs/hfg2
  if (tsfp.gt.tsat .or. qvfpgs.le.0.0)mconfp=0.
  mwvz2=mwvz2-mconfp
  mw1z2=mw1z2+mconfp
  uvz2=uvz2-qvfpgs
  ulz2=mconfp*hsat+ulz2
  zz7=zz7+qvfpgs/rhsfp/afp/thfp/cpsfp
  endif

```

```

c
c
c*** liquid pool to secondary floor *****
c
c determine average fluid properties
tave=(t1p2+tfs)/2.
tavhi=int(tave/20.)-23.
tavlo=tavhi-1.
intdsr=(tave/20.)-int(tave/20.)
nulpv=(25.3/((tave/1.8)**2.+91.*tave/1.8-8.58e04))/1.488
cplv=(sat(tavhi,9)-sat(tavlo,9))*intdsr+sat(tavlo,9)
vlpv=(sat(tavhi,3)-sat(tavlo,3))*intdsr+sat(tavlo,3)
nulpv=nulpv*vlpv
kwat=(0.686-5.87e-06*(abs(tave/1.8-415.))**2.+7.3e-10*pas*6895.)
kwat=kwat/1.73/3600.
if(tave.gt.1165.)then
  nulpv=1.46e-06
  kwat=8.667e-05
  cplv=1.368
  vlpv=sat(34,3)
endif
tfhi=int(tfs/20.)-23.
tflo=tfhi-1.
intdsf=(tfs/20.)-int(tfs/20.)
vlpf=(sat(tfhi,3)-sat(tflo,3))*intdsf+sat(tflo,3)
if(tfs.gt.1165.)vlpf=sat(34,3)
betaf=abs(1./vlp2*(vlpf-vlp2)/(tfs-tlp2))
c determine h from GrPr
grprf=32.2*betaf*abs(tfs-tlp2)*afs**1.5
/vlpv/kwat*cplv/nulpv
if((tfs.gt.tlp2).and.(grprf.le.2.e07))then
  ca=0.54
  aa=0.25
elseif((tfs.gt.tlp2).and.(2.0e07.lt.grprf).and.
  (grprf.le.3.0e10))then
  ca=0.14
  aa=0.333
elseif(grprf.gt.3.0e10)then
  ca=0.021
  aa=0.4
elseif((tfs.lt.tlp2).and.(grprf.le.3.e10)) then
  ca=0.27
  aa=0.25
elseif(tlp2.eq.tfs)then
  ca=0.0
  aa=1.0
endif
h1pflr=kwat/afs**5*ca*grprf**aa
zh2o2=mw12*vlp2/afs
if(h1pflr.lt.(2.*kwat/zh2o2))h1pflr=2.*kwat/zh2o2
qlflr=2.*(tlp2-tfs)/(thfs/kstlfs+1./h1pflr)
ulz2=ulz2-qlflr
zzfs=zzfs+qlflr/rhsfs/afs/thfs/cpsfs
elseif(mwv2.gt.0.0 .and. mw12.le.1.0e-06)then
c
c
c secondary gas to secondary floor--no liquid water
qvflr=2.*(tsat-tfs)*afs/(thfs/kstlfs+1./huch)
if(tfs.gt.tsat)then
  hfsgas=hinfgs*akexx(tfs,tgs,rhogs)
  qvflr=2.*(tgs-tfs)*afs/(thfs/kstlfs+2./hfsgas)

```

```

endif
mcondf=qvflr/hfg2
if(tfs.gt.tsat.or.qvflr.le.0.0)mcondf=0.0
mwvz2=mwvz2-mcondf
mw1z2=mw1z2+mcondf
uvz2=uvz2-qvflr
ulz2=ulz2+mcondf*hsat
zfs=zfs+qvflr/rhsfs/afs/thfs/cpsfs
endif
C
C secondary gas to secondary extraneous heat capacity (or magnets)
if(mwv2.gt.0.0)then
C
  if(.not.flagtr)then
    qvehc=huch*(tsat-tehcs)*aehcs
    if(tehcs.gt.tsat)then
      hehcs=hinecs*akexx(tgs,tehcs,rhogs)
      qvehc=(tgs-tehcs)*hehcs*aehcs
    endif
  else
    qvehc=huch*(tsat-tmag)*amag
    if(tmag.gt.tsat)then
      hehcs=hinmag*akexx(tgs,tmag,rhogs)
      qvehc=(tgs-tmag)*hehcs*amag
    endif
  endif
  mconde=qvehc/hfg2
  if((tehcs.gt.tsat.and..not.flagtr).or.
    (tmag.gt.tsat.and.flagtr).or.qvehc.le.0.0)mconde=0.
    mwvz2=mwvz2-mconde
    mw1z2=mw1z2+mconde
    uvz2=uvz2-qvehc
    ulz2=ulz2+mconde*hsat
    if(.not.flagtr)zses=zses+qvehc/xnehcs/cpehcs
    if(flagtr)zsmag=zsmag+qvehc/xmag/cpmag
C
  endif
C
  ns=3
  return
  end
C *****
C
C this is the subroutine that creates the steam tables for the
C lithium-steam reaction option
C
  subroutine table
  implicit real (i,k,l,m)
  integer r
  common /steam/ tgps,vg,xg,sat(35,10),sh(7,110,5),uvw,hwv,cpwv,vvg,
  ph2o,ulp,tlp,vlp,hlp,vvb,hfg,ph2ob,cpvb,hu(15,2),
  phase,hum,cpa,mw1,mwv,ul,uv,ulz,uvz,mw1z,
  + mwvz,uvzcr,ulzcr,mwvz,mwlv,vl,zsep,mwvzcr,mvlzcr,
  + xmolp,cell
C
  the following data statements are used to define constants used
  C
  C in determining the properties of water and steam
  data tsc1,tsc2,tsexp /9.0395, 255.2, 0.223/
  data cps1,cps2,cpsexp /9.5875e02, 0.00132334, -0.8566/
  data g11,g12,g13 /2.6194106e06, -4.995e10, 3.403e05/

```

```

data g14,g15,g16 /1.0665544, 1.02e-08, -2.548e-15/
data g17 /-5.096e-15/
data hl0,hl1,hl2,hl3,hl4,hl5 /5.7474718e05, 2.0920624e-01,
-2.8051070e-08, 2.3809828e-15, -1.0042660e-22, 1.6586960e-30/
data hv0,hv1,hv2,hv3,hv4 /2.7396234e06, 3.758844e-02,
-7.1639909e-09, 4.2002319e-16, -9.8507521e-24/
data tcrin,tcrin /647.3, .00154488/
data cc,cci,ccm /1.3, .76923, 0.3/
data rl0,rl1,rl2,rl3 /1735.3320, -4.6406842, 1.0431090e-02,
-9.4367085e-06/
data rh0,rh1,rh2,rh3,rh4 /-1.1755984e06, 8.1437361e03,
-21.136559, 2.4381598e-02, -1.0549747e-05/
data rp0,rp1,rp2 /-14.643890, 1.1283357e-03, 1.2670366e-02/
data sp0,sp1,sp2,sp3 /-42.0218, 0.2116, -4.4587e-04, 3.251e-07/
data sp22,sp33 /-8.9174e-04, 9.753e-07/
data sl0,sl1,sl2,sl3,sl4 /-460268.18, -2863.4045, 27.450693,
-4.8108323e-02, 3.2059316e-05/
data sl22,sl33,sl44 /54.901386, -14.432497, 1.2823726e-04/
data sh0,sh1,sh2,sh3,sh4 /1.2426455e09, -8608225.1, 22364.564,
-25.815959, 1.1178766e-02/
data sh22,sh33,sh44 /44729.128, -77.447877, 4.4715064e-02/
data al1,al2,al3 /1.2959e-03, 593.59, 1.6847e-03/

```

```

c create the array "sat(35,10)" for saturated properties
c
c

```

```

t=277.6
do 1400 n=1,35
p=((t-tsc2)/tsc1)**(1./tsexp)
sat(n,2)=p/6895.
c find the saturated enthalpies
hg= hv0+p*(hv1+p*(hv2+p*(hv3+p*(hv4))))
hf= hl0+p*(hl1+p*(hl2+p*(hl3+p*(hl4+p*(hl5))))
sat(n,7)= hf/2321.
sat(n,8)= hg/2321.

```

```

c find the saturated internal energy

```

```

t1= 1.-t*tcrin
if(t1.lt.0.0)t1=1.0e-10
cps= cps1*(t1**cpsexp)
t2= 1./((g13+p)
t1= t2*g12
es= g11+t1
sat(n,6)= es/2321.
gams= g14+p*(g15+p*g16)
gamsm= gams-1.
dp= p-1.5e07

```

```

deldp= -exp(sp0+t*(sp1+t*(sp2+t*sp3)))

```

```

del= deldp*dp
ul= sl0+t*(sl1+t*(sl2+t*(sl3+t*sl4)))+del
if(t.ge.576.5)ul= sh0+t*(sh1+t*(sh2+t*(sh3+t*sh4)))+del
sat(n,5)= ul/2321.

```

```

c find the specific heat at constant volume

```

```

deldt= sl1+t*(sl2+t*(sl3+t*sl4)) + del*(sp1+t*(sp2+t*sp3))
if(t.ge.576.5)deldt= sh1+t*(sh2+t*(sh3+t*sh4)) + del*(sp1+
t*(sp2+t*sp3))

```

```

devdt= cps*cci

```

```

sat(n,9)= deldt/4187.
sat(n,10)= devdt/4187.

```

```

c find the specific volumes

```

```

drldp= exp(rp0+rp1*exp(rp2*t))

```

```

drl= drldp*dp

```

```

rol= rl0+ t*(rl1+t*(rl2+t*rl3))+ drl

```

```

if(t.ge.576.5)rol= rho+ t*(rh1+t*(rh2+t*(rh3+t*rh4)))+drl

```

```
sat(n,3)= 1./((rov/16.02)
ev= es
rov= p/gamsm/ev
sat(n,4)= 1./((rov/16.02)
sat(n,1)= t*1.8-460
t=t+11.11
1400 continue
```

C these data statements are necessary to correct inaccuracies in the
C steam table formulae used in the subroutine

```
sat(1,2)=0.1217
sat(2,2)=0.2563
sat(3,2)=0.5073
sat(4,2)=0.9503
sat(5,2)=1.695
sat(6,2)=2.892
sat(7,2)=4.745
sat(8,2)=7.515
c spec. vol. sat. liq.
sat(28,3)=.02278
sat(29,3)=.02363
sat(30,3)=.02465
sat(31,3)=.02593
sat(32,3)=.02767
sat(33,3)=.03032
sat(34,3)=.03666
sat(35,3)=.090
```

```
c spec. vol. sat. vap.
sat(1,4)=2445.
sat(2,4)=1207.
sat(3,4)=632.8
sat(4,4)=350.0
sat(5,4)=203.0
sat(6,4)=122.9
sat(7,4)=77.2
sat(8,4)=50.2
sat(23,4)=.8187
sat(24,4)=.6761
sat(25,4)=.5605
sat(26,4)=.4658
sat(27,4)=.3877
sat(28,4)=.3225
sat(29,4)=.2677
sat(30,4)=.2209
sat(31,4)=.1805
sat(32,4)=.1446
sat(33,4)=.1113
sat(34,4)=.0744
sat(35,4)=-.0140
```

```
c spec. enth. sat. liq.
sat(1,7)=8.02
sat(2,7)=28.08
sat(3,7)=48.09
sat(4,7)=68.05
sat(5,7)=88.0
sat(6,7)=107.96
sat(7,7)=127.96
sat(8,7)=147.99
sat(9,7)=168.07
sat(10,7)=188.2
sat(11,7)=208.4
sat(12,7)=228.8
```

```

c spec. enthalpy sat vap.
  sat(13,7)=249.2
  sat(35,7)=1118.3
  sat(1,8)=1078.9
  sat(2,8)=1087.7
  sat(3,8)=1096.4
  sat(4,8)=1105.0
  sat(5,8)=1113.5
  sat(6,8)=1121.9
  sat(7,8)=1130.1
  sat(8,8)=1138.2
  sat(9,8)=1145.9
  sat(34,8)=990.2
  sat(35,8)=665.4
c spec. energy sat liq.
  sat(1,5)=8.02
  sat(34,5)=801.7
  sat(35,5)=1064.3
c spec. energy sat. vap.
  sat(1,6)=1023.9
  sat(2,6)=1030.4
  sat(3,6)=1037.0
  sat(4,6)=1043.5
  sat(5,6)=1049.9
  sat(6,6)=1056.2
  sat(7,6)=1062.3
  sat(8,6)=1068.3
  sat(28,6)=1098.9
  sat(29,6)=1090.0
  sat(30,6)=1078.5
  sat(31,6)=1063.2
  sat(32,6)=1042.3
  sat(33,6)=1011.0
  sat(34,6)=947.7
  sat(35,6)=669.6

```

c create the array "sh(7,110,5)" for superheated steam properties

```

P= 6895.
do 1390 n=1,7
t=310.9
  tsat= tscl*p**tsexp
  tsat= tsat+tsc2
  t1= 1.-tsat*tcrlnv
  cps= cps1*t1**cpsexp
  t2= 1./(g13+p)
  t1= t2*g12
  es= g11+t1
  gams= g14+p*(g15+p*g16)
  gamsm= gams-1.
  t1= 1./(all*cps-1.)
  beta= tsat**2*(1.-t1**2)
  t2= tsat*t1
do 1380 r=1,110
c find the specific internal energy
  dt= t-tsat
  t3=abs(t**2-beta)
  de= al2*(dt+sqrt(t3)-t2)
  ev=es+de
  sh(n,r,3)= ev/2321.
  if(n.eq.1 .and. r.le.13)sh(n,r,3)=sh(n,r,3)*.986
c find specific volume
  t4=1./(gamsm*es+ccm*de)

```



```

rov=p*t4
sh(n,r,2)=1./((rov/16.02)
if(n.eq.1)sh(n,r,2)=sh(n,r,2)*1.05
c find specific enthalpy
sh(n,r,4)=(ev+p/rov)/2321.
sh(n,r,1)=t*1.8-460.
c find specific heat at constant volume
sh(n,r,5)=cps*cci/4187.
t= t+11.11
1380 continue
if(n.eq.1)p=p+27580.
if(n.eq.2)p=p+34475.
if(n.ge.3)p=p+68950.
1390 continue
c these data statements are necessary to correct inaccuracies
c in the formulae used to create the steam table
c
sh(1,1,2)=333.6
sh(1,2,2)=345.2
sh(1,3,2)=356.8
sh(1,4,2)=368.6
sh(1,5,2)=380.5
sh(1,6,2)=392.5
sh(1,7,2)=404.5
sh(1,8,2)=416.4
sh(1,9,2)=428.4
sh(1,10,2)=440.3
sh(1,11,2)=452.3
sh(1,12,2)=464.2
sh(1,13,2)=476.1
sh(1,14,2)=488.1
sh(1,15,2)=500.0
sh(1,16,2)=511.9
sh(1,17,2)=523.8
sh(1,18,2)=535.7
sh(1,19,2)=547.7
sh(1,20,2)=559.5
sh(1,21,2)=571.5
c create a table of Uchida heat transfer coefficients for
c steam condensation. Table "hu(15,2)"
c
data hu(1,1),hu(2,1),hu(3,1),hu(4,1),hu(5,1),hu(6,1),
. hu(7,1),hu(8,1),hu(9,1),hu(10,1),hu(11,1),
. hu(12,1),hu(13,1),hu(14,1),hu(15,1)/50., 20.,
. 18., 14., 10., 7., 5., 4., 3.0, 2.3, 1.8, 1.3, 0.8, 0.5,0.1/
data hu(1,2),hu(2,2),hu(3,2),hu(4,2),hu(5,2),hu(6,2),
. hu(7,2),hu(8,2),hu(9,2),hu(10,2),hu(11,2),
. hu(12,2),hu(13,2),hu(14,2),hu(15,2)/2., 8., 9.,
. 10., 14., 17., 21., 24., 29., 37., 46., 63., 98., 140.,280./
return
end
c
c these are the subroutines used to determine the properties of water
c in the containment, using the table created in the previous subroutine.
c
subroutine proptv
implicit real (i,k,l,m)
integer k,p,phi,plo,q,r,thi,this,tlo,tlos
dimension tabtmp(10),proprt(10)

```

```

common /steam/  tgps,vq,xg,sat(35,10),sh(7,110,5),uwv,hwv,cpwv,vvg,
.               ph2o,ulp,tlp,vlp,hlp,vvb,hfg,ph2ob,cpvb,hu(15,2),
.               phase,hum,cpa,mw1,mwv,ul,uv,ulz,uvz,mw1z,
+               mwvz,uvzer,ulzer,mwv,mlv,vl,zzep,mwvzer,mw1zer,
.               xmolp,cell
common /steam2/cpa2,cpvb2,emgs,hfg2,hlp2,htcpgs,hum2,mw12,
.               mwlv2,mw1z2,mwlvz2,mwv2,mwvz2,mwvzr2,
.               phase2,ph2o2,ph2ob2,rair2,tlp2,ul2,ulp2,ulz2,
.               ulzer2,uv2,uvz2,uvzer2,uwv2,vg2,vl2,vlp2,vvb2,
.               vvg2,xg2,xmols,stmin2,stout2,xinj2,rhoas

c  determine whether the mixture is saturated or superheated
c  find the temperatures between which to interpolate
  if(cell.eq.1.)vgs=vvg
  if(cell.eq.2.)vgs=vg2
  tlo= int(tgps/20.)-24.
  thi= tlo+1.
  intdis= tgps/20.--int(tgps/20.)
  if(tgps.gt.1165.)then
    thi=35.
    tlo=34.
    intdis=1.0
  endif
c  check to see if the mixture is saturated or superheated
  vvg= (sat(thi,4)-sat(tlo,4))*intdis+ sat(tlo,4)
  if(vgs.gt.vvg .or. tgps.gt.1165.)then
    phases=2.
c  mixture is superheated
    tlo= tlo-3
    thi= tlo+1
c  check to see if the properties fit on the chart
    vcheck=.5937*tgps
    if(tlos.le.0.0 .or. vgs.gt.vcheck)then
      ph2os=1545./18.*tgps/vgs/144.
      cpwvs=sh(1,this,5)
      if(tlos.le.0.0)then
        uwvs=1044.0-16.4*(560.-tgps)/48.3
        hwvs=1105.8-21.7*(560.-tgps)/48.3
      else
        uwvs=(sh(1,this,3)-sh(1,tlos,3))*intdis+sh(1,tlos,3)
        hwvs=(sh(1,this,4)-sh(1,tlos,4))*intdis+sh(1,tlos,4)
      endif
      go to 500
    endif
c  do 1370 n=1,6
  r=n+1
  vlo=(sh(n,this,2)-sh(n,tlos,2))*intdis +sh(n,tlos,2)
  vhi=(sh(r,this,2)-sh(r,tlos,2))*intdis +sh(r,tlos,2)
  if(vhi.lt.vgs)then
    phi=r
    plo=n
    intdsv=(1./vgs-1./vlo)/(1./vhi-1./vlo)
    go to 100
  endif
  1370 continue
  100 continue
c  determine the water vapor partial pressure
  if(n.eq.1)ph2os= 1.+4.*intdsv
  if(n.eq.2)ph2os= 5.+5.*intdsv
  if(n.ge.3)ph2os= (plo-2.+ intdsv)*10.
c  determine the other properties

```

```

do 1360 j=3,5
k=j+1
proprr(k)=(sh(phi,this,j)-sh(phi,tlos,j))*intdis +sh(phi,tlos,j)
      -(sh(plo,this,j)-sh(plo,tlos,j))*intdis -sh(plo,tlos,j))
      *intdsv+ (sh(plo,this,j)-sh(plo,tlos,j))*intdis
      +sh(plo,tlos,j)
1360 continue
else
c mixture is saturated
phases=1.
do 1350 n=1,10
tabtmp(n)=(sat(thi,n)-sat(tlo,n))*intdis+ sat(tlo,n)
1350 continue
c find mixture quality
xgs=(vgs-tabtmp(3))/(tabtmp(4)-tabtmp(3))
c find the mixture properties
do 1340 n=4,6
p= 2*(n-1)
q= p-1
proprr(n)=( tabtmp(p)-tabtmp(q))*xgs+ tabtmp(q)
1340 continue
endif
c assign properties
if(phases.eq.1.)ph2os=tabtmp(2)
uwvs=proprr(4)
hwvs=proprr(5)
cpwvs=proprr(6)
vvgv=tabtmp(4)
500 continue
hfgs=(sat(thi,8)-sat(tlo,8))*intdis+sat(tlo,8)-(sat(thi,7)-
      sat(tlo,7))*intdis-sat(tlo,7)
c assign primary cell properties
if(cell.eq.1.)then
ph2o=ph2os
uwv=uwvs
hvv=hwvs
cpwv=cpwvs
vvg=vvgs
hf9=hfgs
xg=xgs
phase=phases
endif
c assign secondary cell properties if needed
if(cell.eq.2.)then
ph2o2=ph2os
uwv2=uwvs
hwv2=hwvs
cpwv2=cpwvs
vvg2=vvgs
hf92=hfgs
xg2=xgs
phase2=phases
endif
return
end
c this subroutine is used to determine the properties of liquid water
c
c
subroutine proptu
implicit real (i,k,l,m)
integer p,q

```

```

dimension proprt(10)
common /steam/ tgps,vg,xg,sat(35,10),sh(7,110,5),uwv,hwv,cpwv,vvg,
. ph2o,ulp,tlp,vlp,hip,vvb,hfg,ph2ob,cpvb,hu(15,2),
. phase,hum,cpa,mw1,mwv,ul,uv,ulz,uvz,mw1z,
+ mwvz,uvzer,ulzer,mwv,mwlv,vl,zzep,mwvzer,mw1zer,
. xmo1p,cell
. common /steam2/cpa2,cpvb2,emgs,hfg2,hlp2,htcpgs,hum2,mw12,
. mwlv2,mw1z2,mw1zr2,mwv2,mwvz2,mwvzr2,mwvzr2,
. phase2,ph2o2,ph2ob2,rair2,tlp2,vlp2,ulp2,ulz2,
. ulzer2,uv2,uvz2,uvzer2,uwv2,vg2,vl2,vlp2,vvb2,
. vvg2,xg2,xmols,stain2,stout2,xinj2,rhoas

c
if(cell.eq.2.)ulps=ulp2
if(cell.eq.1.)ulps=ulp
do 1330 n=1,34
p=n+1.
if(ulps.lt.sat(p,5))then
intdsu=(ulps-sat(n,5))/(sat(p,5)-sat(n,5))
go to 333
endif
1330 continue
333 continue
do 1320 q=1,10
proprt(q)=(sat(p,q)-sat(n,q))*intdsu+sat(n,q)
1320 continue
tips=proprt(1)+460.
vlps=proprt(3)
hips=proprt(7)
c boundary layer properties
vvbs=proprt(4)
ph2obs=proprt(2)
cpvbs=proprt(10)
hfgs=proprt(8)-proprt(7)
c convert to primary cell properties
if(cell.eq.1.)then
tlp=tlps
vlp=vlps
hip=hlps
vvb=vvbs
ph2ob=ph2obs
cpvb=cpvbs
hfg=hfgs
endif
c convert to secondary cell properties
if(cell.eq.2.)then
tlp2=tlps
vlp2=vlps
hip2=hlps
vvb2=vvbs
ph2ob2=ph2obs
cpvb2=cpvbs
hfg2=hfgs
endif
return
end

```

```

c
c this is the system international unit conversion subroutine allowing
c the input and output to be prepared and written in si units.
subroutine si
implicit real (i,k,l,m)
logical flagw,flagf,flag2,flagpn,flagc,flaga,flagn,flagdf,flagst,

```

```

common /flagtr
common // name(340),flag2,flagas,flagc,flagf,flagg,flagh,flagi,flagj,flagk,flagl,flagm,flagn,flago,flagp,flagq,flagr,flagv,ipage,iswich,iarosl,flagdf,icz,flagco
common /looper/ il0,il1,il2,il3,il4,il5,il6,il7,il8,il9
common /lith/ akli,asli,cpli,csbli,hb,libp,lil,lilp,lit,
rlli,spil,lli,tlil,zli
common /steel/ cpsfp,cpsfs,cpswp,cpsws,estlfp,estlwp,kstlfp,
kstlfs,kstlwp,kstlws,rhsfp,rhsfs,rhswp,rhsws
common /misc/ afp,afw,awp,aws,c7,c21,gin,
ha,hinfam,hinsam,hcpgp,gradc,radc,rczw,
rhoap,rliw,rwpws,sigma,ta,tc(20),tfs,
tfszer,tgp,tgs,tgpzer,tspf,tss,
tsszer,thfp,thfs,thwp,thws,zses,zz5,zzs,zz1,zz7,
rair
common /injob/ dpl,dp2,dp3,mninj,moxinj,time,vp
common /panop/ ains,apan,bredth,clist,cpins,cppan,emgp,fpq,fpw,
kpan,rhins,rhpan,thkini,thkin2,thkpan,
tins1,tinslf,tinsli,tins2,tins2f,tins2i,
tpan,tpanf,tpanzo,zz2,zz4,zz8,zz9
common /conop/ c8,cpcon,dtdt(20),dtdt(20),gap,kcon,kgap,
l(20),ll(20),nl,nll,qrdb,radb,rhcon,
sflcr,tb(20),tbf(20),tbc(20),tcf(20),
tcic(20),thfc,thwc,tsfpi,tspzer,xsfl,qlflr,qvflr
common /ccop/ cmbro,cracn,dcozc,h2left,qcconc,rcmbo,rcmbw,
relese,tcigni,tcon,tconf,xmh2oi,zzc,zzd,zzdin
common /pbpool/ dmpbdt,zpb,mlead,tlead,xwli,dflipb,xlidot,
thpb,tleadf,foo
common /pbdif/ cczp,cgli,clig,cpcz,cpmcz,dfilm,kfilm,pyup,
qrzp,rczp,rgli,rifczp,rifpg,rifpw,rliq,rwli,
tlead,yapcz,zz6
common /secop/ aehcs,c1l,c20,chs,cpehcs,cph2,cplih,cpwa,crack,
fouthp,fouts,foutt,hinfgs,hinfgs,hingss,hinps,kleak,
leak,mairp,mairs,mals,mh2s,mlihs,mlihs,mlihs,mlins,
mliois,mlios,mniis,mnis,moxis,moxs,mwais,
mlc3s,mlc2s,mcs,mco2s,rholc3,rholc2,rhocar,
mwas,pap,pas,paszer,ra,rbreak,rholih,
rholin,rholio,rwpgas,tehcs,tehcsf,tehczs,tgsf,
tfsf,tgszer,tssf,vs,xmdot,xmehcs,xmola,zz3,zzfs
common /units/ aehcp,beta,chn,cmbrr,cpap,cpehcp,map,mnip,
moxp,mwap,papzer,qcn,qco,qcol,qco2,qcw,qvap,
tcz,tczf,tczi,tehcp,tehcpf,tehczp,tgpf,
tlif,tmelt,tsfpi,tspf,tvap,xmehcp
common /stmp/ minjr,minjr2,hinj,hinj2
common /torus/ amag,ashl,clehcs,cpmag,cpsli,eehcs,eshl,
hinmag,hinshl,kehcs,khe,kshl,the,thshl,tmag,tmagf,
tmagz,tshl,tshlf,tshlz,zzshl,zzmag
common /face/ tlio,tshio,tshoo,zzbli,zzshi,zzsho,tbli,tshi,tsho,
tmano,tman,xmsho,xmag,zman
common /decay/ qofw1,qofw2,qofw3,expfwi,expfw2,expfw3,
qobl1,qobl2,qobl3,expbli,expbl2,expbl3,
qobl4,qobl5,qobl6,expbl4,expbl5,expbl6,
qoshi,qosh2,qosh3,expshi,expsh2,expsh3,
qobl1,qobl2,qobl3,expbi1,expbi2,expbi3,
qoshi1,qoshi2,qoshi3,qoshol,qosh2,qosh3
common /sitor/ abli,aman,cpbli,cpman,kbli,kman,tbli,tman,thshl,
thsho,xmshl,xmbli,xman,xmshi
if (flagn) n=2
go to (1,2,3)n
1 continue
aehcp=aehcp*10.765
afp=afp*10.765

```

```

akli=akli*0.57803
asli=asli*10.765
awp=awp*10.765
chp=chp*3.281
cpap=cpap*2.389e-04
cpccon=cpccon*2.389e-04
cpehpc=cpehpc*2.389e-04
cp1i=cp1i*2.389e-04
cpsfp=cpsfp*2.389e-04
cpswp=cpswp*2.389e-04
gap=gap*3.281
kleak=kleak*0.03771
kcon=kcon*0.57803
kgap=kgap*0.57803
kstlfp=kstlfp*0.57803
kstlwp=kstlwp*0.57803
papzer=papzer*1.450e-01
qcn=qcn*4.311e-01
qco=qco*4.311e-01
qco1=qco1*4.311e-01
qco2=qco2*4.311e-01
qcw=qcw*4.311e-01
qvap=qvap*4.311e-01
rhcon=rhcon*0.062428
rhli=rhli*0.062428
rhlih=rhlih*0.062428
rholin=rholin*0.062428
rholio=rholio*0.062428
rhsfp=rhsfp*0.062428
rhwsp=rhwsp*0.062428
spill=spill*2.2046
ta=ta*1.8
tczi=tczi*1.8
tehczp=tehczp*1.8
tgpzer=tgpzer*1.8
thfc=thfc*3.281
thwc=thwc*3.281
thfp=thfp*3.281
thwp=thwp*3.281
tlii=tlii*1.8
tmelt=tmelt*1.8
tsfpi=tsfpi*1.8
tspzer=tspzer*1.8
tvap=tvap*1.8
vp=vp*35.32
xmehcp=xmehcp*2.2046
zli=zli*3.281

if (flagst) then
  minjr=minjr*2.2046
  minjr2=minjr2*2.2046
  hinj=hinj/2.326
  hinj2=hinj2/2.326
endif

if (.not. (flag2.or.flagtr)) go to 100
aehcs=aehcs*10.765
afs=afs*10.765
aws=aws*10.765
chs=chs*3.281
cpas=cpas*2.389e-04
cpehcs=cpehcs*2.389e-04

```

c

c

cpsfs=cpsfs*2.389e-04
cpsws=cpsws*2.389e-04
crack=crack*0.1550
kstlfs=kstlfs*0.57803
kstlws=kstlws*0.57803
paszer=paszer*1.450e-01
rhsws=rhsws*0.062428
tehczs=tehczs*1.8
tfszer=tfszer*1.8
tgszer=tgszer*1.8
thfs=thfs*3.281
thws=thws*3.281
tsszer=tsszer*1.8
vs=vs*35.32
xmehcs=xmehcs*2.2046
if(flagtr)then
amag=amag*10.765
ashl=ashl*10.765
abli=abli*10.765
aman=aman*10.765
clehcs=clehcs*3.281
cpmag=cpmag*2.389e-04
cpshl=cps*2.389e-04
cpbli=cpbli*2.389e-04
cpman=cpman*2.389e-04
kehcs=kehcs*0.57803
khe=khe*0.57803
kshl=kshl*0.57803
kbli=kbli*0.57803
kman=kman*0.57803
tmagz=tmagz*1.8
tshlz=tshlz*1.8
tblio=tblio*1.8
tshio=tshio*1.8
tshoo=tshoo*1.8
tmano=tmano*1.8
the=the*3.281
thshl=thshl*3.281
thbli=thbli*3.281
thman=thman*3.281
thshi=thshi*3.281
thsho=thsho*3.281
xmag=xmag*2.2046
xmsl=xmsl*2.2046
xmbli=xmbli*2.2046
xman=xman*2.2046
xmshi=xmshi*2.2046
xmsho=xmsho*2.2046
qofw1=qofw1*26.84
qofw2=qofw2*26.84
qofw3=qofw3*26.84
qobl1=qobl1*26.84
qobl2=qobl2*26.84
qobl3=qobl3*26.84
qobl4=qobl4*26.84
qobl5=qobl5*26.84
qobl6=qobl6*26.84
qosh1=qosh1*26.84
qosh2=qosh2*26.84
qosh3=qosh3*26.84
qobl1=qobl1*26.84

```

qobli2=qobli2*26.84
qobli3=qobli3*26.84
qoshi1=qoshi1*26.84
qoshi2=qoshi2*26.84
qoshi3=qoshi3*26.84
qosho1=qosho1*26.84
qosho2=qosho2*26.84
qosho3=qosho3*26.84
endif
100 continue
c
if (.not. flagpn) go to 101
ains=ains*10.765
apan=apan*10.765
bredth=bredth*3.281
cpins=cpins*2.389e-04
cppan=cppan*2.389e-04
kpan=kpan*0.57803
rhins=rhins*0.062428
rhpan=rhpan*0.062428
thkin1=thkin1*3.281
thkin2=thkin2*3.281
thkpan=thkpan*3.281
tpanzo=tpanzo*1.8
101 continue
c
if (iblow .ne. 1) go to 102
blowv=blowv*2119.2
cpab=cpab*2.389e-04
exhstv=exhstv*2119.2
tblow=tblow*1.8
102 continue
if (isflc .eq. 1) sflcr=sflcr*9.475e-04
if (iesc .eq. 1) escr=escr*9.475e-04
c
if (iarosl .eq. 1) beta=beta/3.281
c
if (.not. flagc) go to 103
cracon=cracon*10.765
qcconc=qcconc*4.311e-01
tcigni=tcigni*1.8
xmh2oi=xmh2oi*2.2046
zzdin=zzdin*3.281
103 continue
c
if (.not. flagas) go to 104
dp1=dp1*1.450e-01
dp2=dp2*1.450e-01
dp3=dp3*1.450e-01
104 continue
2 continue
3 continue
return
end

```


References

- [1] D.S. Barnett, et al. *LITFIRE User's Guide*. MIT Plasma Fusion Center, second edition, August 1987. PFC/RR-87-11.
- [2] D.S. Barnett. *The Chemical Kinetics of the Reactions of Lithium with Steam-Air Mixtures*. PhD thesis, Massachusetts Institute of Technology, April 1989.
- [3] V.J. Gilberti and M.S. Kazimi. *Modeling of Lithium and Lithium-Lead Reactions in Air Using LITFIRE*. Technical Report PFC/RR-83-08, MIT Plasma Fusion Center, January 1983.
- [4] D.A. Dube and M.S. Kazimi. *Analysis of Design Strategies for Mitigating the Consequences of Lithium Fire Within Containment of Controlled Thermonuclear Reactors*. Technical Report MITNE-219, Massachusetts Institute of Technology, July 1978.